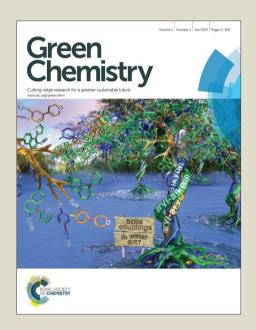
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1 Hydrogenation of oxalic acid using light-assisted water 2 electrolysis for the production of an alcoholic compound

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We demonstrate the production of glycolic acid, an industrially important alcoholic compound, via the electrochemical reduction of oxalic acid, which is procurable from biomass, and electro-oxidation of water with the help of renewable light energy for the first time. In principle, this new synthesis system is achievable while minimizing the consumption of fossil resources. We built a precious-metal free electrosynthesis system by employing a TiO_2 cathode for oxalic acid reduction and a WO_3 photoanode for water oxidation. The alcohol production proceeds during the application of electric power above 2.1 V in the dark. Notably, UV-visible light irradiation of the WO_3 photoanode enables glycolic acid electrosynthesis above 0.5 V, which is lower (by 0.6 V) than the theoretical bias, i.e., 1.1 V. The glycolic acid electrosynthesis with an 80% high Faradaic efficiency was achieved when applying a bias of 1.5 V under UV-visible irradiation ($\lambda > 300$ nm).

Currently, the chemical industry largely depends on fossil fuels, which serve not only to generate power but also as hydrogen and carbon sources; fossil fuels are also believed to be a contributing factor to the global warming due to the increase of CO₂ concentrations. Efficient utilization of biomass resources derived from atmospheric CO₂ could be a useful strategy to curbing global warming by suppressing the consumption of fossil resources as a raw material.¹⁻⁴ Recently, bio-alcohols, such as ethanol⁵ and ethylene glycol,⁶ have been commercialized and utilized as a fuel⁷ and feedstock.⁸ However, carbon resources included in biomass are not efficiently converted into alcohols, i.e., the carbon yield in the bio-alcohol production through fermentation is not beyond 50% and the residual carbon is released back into the air.⁹ Besides, the low production rate is due to the slow enzyme reaction.¹⁰

Catalytic hydrogenation of carboxylic acids has attracted much attention as a novel synthetic route for the production of alcoholic compounds from bio-derived materials.¹¹ Several groups have succeeded in the catalytic hydrogenation of organic acids, such as acetic acid,¹² stearic acid¹³ and aromatic carboxylic acid,^{14, 15} to produce corresponding alcoholic compounds. However, severe reaction conditions are required for the catalytic hydrogenation of organic acids, i.e., high pressure (2-6 MPa) and temperature (100-380 °C)¹⁵ with use of H₂ gas. The other drawback of the organic hydrogenations process is the utilization of highly reactive metal hydrides derived from fossil fuels as a hydrogen source, e.g., LiAlH₄,¹⁶ (BH₃)₂^{17, 18} and HSiEt₃,¹⁹ to activate highly stable carboxyl groups due to their low electrophilicty²⁰ in organic solvents, resulting in the formation of large amounts of waste.²¹

Alternatively, light-energy-driven electrochemical water splitting using a photoelectrode, such as oxide, ²²⁻²⁷ (oxy)nitride²⁸⁻³¹ and sulfide³² is regarded as a clean process for producing hydrogen from water using renewable solar energy and for providing

- an effective means of energy storage. In this study, we focus on the utilization the hydrogen
- 2 generated photocatalytically from water in chemical syntheses and photovoltaic effects to
- 3 accelerate electrochemical reactions. Thus, the electrochemical reduction of carboxylic
- 4 acids using water as a hydrogen source with the assistance of light energy would achieve
- 5 the highly efficient hydrogenation of carboxylic acid with fossil-free hydrogen, i.e.,
- 6 light-energy-driven alcohol synthesis from fossil-free carboxylic acid and water, as
- shown in Fig. 1. This process is expected to become an excellent, environmentally friendly
- 8 alcohol production route, if it progresses under largely milder conditions (0.1 MPa, <100
- 9 °C) than those of hydrogenation reactions.
- Previously, we have demonstrated the electrochemical reduction of oxalic acid,
- 11 (COOH)₂,**OX**, a divalent carboxylic acid, to produce glycolic acid, HOOC-CH₂OH, **GC**,
- an alcoholic compound $(\alpha$ -hydroxy carboxylic acid)³³ through the 4-electron reduction of
- OX with oxidation of water as described in equation 1-3.
- 14 Cathode: $(COOH)_2 + 4 H^+ + 4 e^- \rightarrow HOOC-CH_2OH + H_2O + 0.13 V vs RHE$ (1).
- 15 Anode: $2H_2O \rightarrow 4H^+ + 4e^- + O_2 + 1.23 \text{ V vs RHE}$ (2).
- 16 Overall: $(COOH)_2 + H_2O \rightarrow HOOC-CH_2OH + O_2$ 1.1 V (3).
- 17 The **OX** is first reduced to GO (HOOC-COH, GO) through two-electron reduction, and
- then **GC** is produced from GO through further two-electron reduction ^{34, 35} (see the scheme
- 19 S1 in ESI†). The GC formation was found to proceed with high selectivity (>98%) and
- 20 Faradaic efficiency (>95%) in an electrochemical cell equipped with a titanium (IV)
- 21 dioxide (TiO₂) cathode for **OX** reduction and a Pt wire anode for water oxidation, which
- 22 corresponds to a direct electric power charge into an alcoholic compound.
- Furthermore, in this study, a light-assisted electrochemical alcohol production
- system was fabricated by adapting oxide semiconductor photoelectrodes as the anode for
- 25 water oxidation to supply protons and electrons for the hydrogenation of a carboxylic acid,

- which enables the direct conversion of light energy into low-carbon alcoholic chemicals.
- 2 Here, we applied Ga₂O₃, ^{36, 37} BiVO₄ ³⁸ and WO₃ ^{24, 39} particles, which are known as highly
- 3 active photocatalysts for water oxidation, as the photoanode to oxidize water and to provide
- 4 electrons and protons for the electro-reduction of **OX** on an anatase-type TiO₂ cathode
- 5 under UV-visible light irradiation. We successfully produced GC from OX through an
- 6 electrochemical reaction in the remarkably low bias potential range, i.e., ~1.5 V, compared
- 7 with the potentials without light irradiation, ~ 2.5 V.
- 8 Commercially supplied Ga₂O₃ and WO₃ powders were used in the electrochemical
- 9 experiments. The BiVO₄ powders were prepared by using the homogeneous-precipitation
- method according to a previous report (see the Experimental section in ESI†).⁴⁰ All samples
- were characterized by X-ray powder diffraction (XRD) and UV-visible diffuse reflection
- measurements. The Ga₂O₃, BiVO₄ and WO₃ powders showed XRD patterns attributable to
- monoclinic structures and photoabsorption spectra, which coincide with the structure and
- spectrum of materials reported as highly active photocatalysts for O₂ evolution by water
- splitting (Figs. S1 and S2†). 24, 36-40 Anodes were prepared by applying a suspended mixture
- of water, acetylacetone (disperser), Toriton-X (thickener) and the oxide powders on
- 17 conductive glass using a squeegee method, 41 followed by calcination at 450°C for 4 h. The
- 18 TiO₂ cathode was prepared by drying a methanolic suspension of TiO₂ nanoparticles (Japan
- 19 Reference Catalyst of TiO₂: JRC-TIO-8, an anatase-type TiO₂) dropped onto Ti foil,
- 20 followed by calcination at 450°C for 0.5 h. Two-electrode systems were equipped using
- 21 two-compartment cells, where the cathode and anode were separately mounted in each cell
- 22 to evaluate an applied bias for **OX** reduction without re-oxidation of the reduced product at
- 23 the anode as shown in Fig. 1. All electro-reduction experiments were conducted by
- introducing 0.16 M **OX** cathode solution containing 0.16 M Na₂SO₄ (pH 1.2) and 0.16 M
- Na₂SO₄ anode solution (pH 5.8) at 25°C. Fig. 2 and Fig. S3† show the current-voltage

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1 curves for the electro-reduction of **OX** on Ga₂O₃, BiVO₄ and WO₃ photoanodes in the dark, and under UV-visible light ($\lambda > 200$ nm) irradiation. We could observe reductive currents 2 on all three anodes by applying external bias above 2.1 V in the dark, as shown in Fig. 2, 3 indicating that the application of 1.0 V as a total over potential, in addition to 1.1 V of the 4 theoretical cell voltage (equation 3), is a requisite for initiating the GC production through 5 **OX** reduction and water oxidation without light irradiation. Under light irradiation, 6 7 minimal biases applied to flow reductive current in the system were drastically decreased compared with those observed in the dark. These results clearly indicate that the external 8 applied bias can be enhanced by photoirradiation, causing photoexcitation over 9 10 photoanodes absorbing UV-visible light energy. The chemical bias in the two-electrode system employing cathode (pH=1.2) and anode (pH=5.8) solutions is calculated to be 0.27 11 12 V based on the following equation:

Chemical bias (V) =
$$0.059 \times |pH_{anode} - pH_{cathode}| = 0.27 \text{ V}$$

Thus, we can beneficially utilize the chemical bias to lower the applied bias required for the reactions. On the other hand, we conducted **OX** reduction experiments both under light irradiation and in the dark to investigate the effects of light irradiation on the applied bias under the same experimental conditions. In acidic aqueous solutions having pH < 2, the photoanode composed of Ga_2O_3 or $BiVO_4$ dissolves and photocatalytic oxidation of co-existing electrolyte anions, SO_4^{2-} , proceeds on the WO₃. Dissolution of the WO₃ also occurs in strong alkaline solutions. Thus, in this study, we utilize an aqueous solution of Na_2SO_4 without pH control, which exhibits neutral pH condition, for the efficient water oxidation reaction.

The onset potential for the reductive current flow under UV-visible irradiation light depended on the photoanodes; the order of onset bias was as follows: $WO_3 < BiVO_4 < Ga_2O_3$. This order coincides with the photovoltaic performance of photoanodes, i.e., $WO_3 > I$

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BiVO₄ > Ga₂O₃. An observed decrease of the onset biases for the electro-reduction of **OX** is therefore associated with the photovoltaic performance, which depends on the amount of optically excited electrons and holes and recombination probabilities between such excited species, and correspond to the activity of photoanodes for water oxidation. Photoexcitation probabilities for the generation of active specie strongly depend on the range of photoanodes achieves more efficient photoexcitation within the entire irradiation range (λ > 200 nm), generating a larger amount of excited electrons and holes. All excited electrons and holes, however, are not available because the recombination between some parts of electrons and holes occurs before the water oxidation proceeds.⁴³ Lower recombination probability enables higher reaction probability of holes and water molecules, resulting in higher activity of water oxidation and a larger amount of available excited electrons, i.e., higher photovoltaic performance.⁴⁴ Therefore, the photoanode, which shows a wide photoabsorption spectrum and low recombination probability, is expected to exhibit large bias decrease due to the high activity for water oxidation and photovoltaic performance.

The Ga₂O₃ photoanode exhibited the smallest bias decrease under light irradiation (0.15 V, as shown in Fig. 2) because the narrowest range of photoabsorption wavelengths of the Ga₂O₃ photoanode (up to 270 nm, as shown in Fig. S2†) corresponds to the smallest amount of excited electrons and holes (as illustrated in Fig. 2), thus, resulting in the low activity for water oxidation and photovoltaic performance. Although the BiVO₄ photoanode showed the widest absorption spectrum (up to 550 nm) of all the photoanodes, **OX** reduction over the photoanode required the application of a relatively high bias potential, i.e., 1.7 V, compared with 0.7 V, which was observed over the WO₃ anode. This observation clearly shows that the recombination probability is more crucial for water oxidation over the BiVO₄ anode. It is known that the BiVO₄ photoanode shows a high recombination

probability due to its poor mobility for excited electrons (Fig. 2). 45-48 By contrast, the WO₃ 1 photoanode, absorbing photons at wavelengths less than 480 nm, exhibited the largest bias 2 decrease of all the anodes, as shown in Fig. 2 and Fig. S2†. Therefore, the largest decrease 3 of applied bias for **OX** reduction observed on the WO₃ photoanode can be attributed to the 4 relatively wide absorption spectrum and low recombination probability for efficient water 5 oxidation and high photovoltaic performance.²⁴ 6 7 Reaction conditions of the most active WO₃ catalyst were optimized to minimize the 8 applied bias by changing pH values over the anode and cathode to achieve efficient alcohol electrosynthesis. For this purpose, a three-electrode system, as described in Fig. S4[†], was 9 10 applied to determine an applied potential on the TiO₂ cathode by comparing the cathode potential with a reference electrode potential, whereas we could measure the bias applied 11 12 between a cathode and an anode in the two-electrode system. Electrochemical cells were filled with Na₂SO₄ agueous solution (40 ml, 0.2 M) and the pH value in the cathode cell 13 including **OX** (0.03 M) was controlled to be either 1.0 or 11 by adding H₂SO₄ or NaOH 14 15 solution. TiO₂ is known as a sufficiently stable oxide compound in both acidic and alkaline conditions and the TiO₂ cathode stably worked during catalytic experiments conducted in 16 17 this study. Fig. S5† shows the influence of the pH value on the activity for OX reduction and a 18 product distribution in chronoamperometric electro-reduction with application of a constant 19 cathode potential, i.e., -0.7 V vs the reversible hydrogen electrode (RHE) at 50°C for 2 h. 20 At pH values higher than or equal to 7, we could not observe any reduction products, i.e., 21 220% **OX** conversion. Decreasing the pH value to less than or equal to 4 led to the generation 23 of both 2- and 4-electron reduction products, i.e., GO and GC, respectively; yields of both reduction products and the percentage of GC yield increased with decreasing pH value. 24Considering that the production of GC and GO are attained via the hydrogenation of OX, a 25

higher proton concentration under lower pH conditions confers a favorable condition for the hydrogenation reaction.⁴⁹

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The influence of the wavelength of irradiation light on the WO₃ anode were examined by applying a two-electrode system, which comprised a TiO₂ cathode in a solution containing **OX** (0.03 M) and Na₂SO₄ solution (pH 1.0, 40 ml, 0.2 M) and a WO₃ photoanode in a Na₂SO₄ solution (pH 5.6, 40 ml, 0.2 M) at 50°C. Fig. 3 shows the current-voltage curves both in the dark and under the irradiation of light of various wavelengths, such as UV-visible light with $\lambda > 200$ and 300 nm and visible light with $\lambda >$ 400 nm. We observed onsets of approximately 0.5 V under the irradiation of light at all tested wavelengths, which are 0.6 V smaller than the theoretical bias required for GC production via **OX** reduction and water oxidation, i.e., 1.1 V, whereas the onset potentials were observed at approximately 2.1 V in the dark, suggesting that the remarkable bias decrease of 1.6 V was attained by light irradiation. Irradiations of light with $\lambda > 200$ nm and 300 nm cover wide energy regions of absorption spectrum of WO₃. Therefore, the rate determining-step for **OX** reduction under UV-visible light irradiation is probably not the water oxidation over the WO₃ anode, where holes with sufficient positive potentials⁵⁰ are generated, but the electro-reduction of **OX** on the cathode. Thus, we conclude that the irradiation of UV-visible light with $\lambda > 300$ nm efficiently works in the system. Furthermore, almost the same onset potential of reductive current was observed under visible light irradiation, indicating that the WO₃ photoanode could efficiently work for the bias decrease under visible light irradiation. These results indicate that the system has applicability under both the irradiation of solar light and only visible light.

Chronoamperometric electro-reduction of **OX** was conducted while applying an external bias of 1.0 or 1.5 V with a two-electrode system employing the TiO₂ cathode in **OX** solution (pH 1.0, 40 ml, 0.03 M **OX**, 0.2 M Na₂SO₄) and the WO₃ photoanode in

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Na₂SO₄ solution (pH 5.6, 40 ml, 0.2 M) at 50°C for 2 h under irradiation of UV-visible light with $\lambda > 300$ nm, visible light with $\lambda > 400$ nm or in the dark. Fig. 4 shows the Faradaic efficiencies calculated based on the amount of GO and GC produced under various conditions. No products were detected in the dark even for an external bias below 1.5 V, which is in accordance with the result that no reductive current was observed in the current-voltage curve below 1.5 V, as shown in Fig. 3, and indicates that the system does not work below 1.5 V without irradiation. By contrast, GO and GC production was achieved under irradiations of both UV-visible and visible light, indicating that **OX** can be reduced with the assistance of light energy absorbed by the WO₃ photoanode through an electrochemical reaction system. Higher Faradaic efficiencies for GO and GC production were achieved through the irradiation of UV-visible light and the application of a bias larger than 1.5 V, compared with efficiencies under the irradiation of visible light at 1.0 V. Note that GO and GC were produced with an 80% Faradaic efficiency in total when applying a bias of 1.5 V under the irradiation of UV-visible light. The anode potential when applying a bias of 1.5 V under the irradiation of UV-visible light was observed to be 1.05 V vs RHE, which is 0.18 V more negative than the theoretical potential of water oxidation, 1.23 V vs RHE, indicating that the hole generated by photoabsorption oxidized water molecules. 51,52 Furthermore, constant reductive-current flow at approximately 0.5 mA cm⁻¹ was observed with applying a bias of 1.5 V under the irradiation of UV-visible light for 2 h, except for the initial period, as shown in Fig. S7[†], indicating that the system can stably work and reductive products are continuously obtained under the examined conditions. Gaseous products generated in both cathode and anode cells were also analyzed to clarify the entire Faradaic efficiency of the system. Fig. S8† shows the Faradaic efficiencies determined based on the amount of GO, GC and H₂ that formed in the cathode cell in OX reduction and O₂ that formed in water oxidation in the anode cell when applying a bias of -1.5 V

under the irradiation of UV-visible light. Faradaic efficiencies for products in each cell reached 100%, indicating that the reaction substrates were only **OX** and water and all electrons formed in water oxidation were consumed for the electro-reduction of **OX** or water to produce GO, **GC** and H₂ through the circuit. H₂ generation occurred with low evolution rate (7.9 µmol h⁻¹) as a side reaction of hydrogenation of **OX** when applying a bias of 1.5 V of bias under irradiation of UV-vis light. In our electrochemical hydrogenation system, protons and electrons are provided from electrolyte and electrode separately and react with oxalic acids as shown in Scheme S1 (ESI†), resulting in glycolic acid production without H₂ gas evolution. Therefore, the suppression of hydrogen evolution reaction (HER) over a TiO₂ electrode is critically important to achieve high Faradaic efficiency for **OX** reduction, which has been discussed in our previous report ³³. The TiO₂ electrode used in this work also exhibited high activities for **OX** reduction but low HER activities in the acidic condition, as reported in Nature Materials⁵³. Based on these results, we succeeded in the first production of alcoholic compound, **GC**, from carboxylic acid, **OX**, via water oxidation using light energy through an electrochemical reaction system.

To improve of the product selectivity, we provide an illustration of the relation between applied potentials on the TiO_2 cathode and Faradaic efficiencies for the electro-reduction of **OX** to GO and **GC** in Fig. 5. The Faradaic efficiencies for GO and **GC** production in the dark were determined using the three-electrode system, which comprised a TiO_2 cathode and Ag/AgCl reference electrode in solution containing **OX** (0.03 M) and Na_2SO_4 solution (pH 1.0, 40 ml, 0.2 M) and a Pt anode in Na_2SO_4 solution (pH 1.0, 40 ml, 0.2 M). Fig. 5 also shows the Faradaic efficiencies obtained using the two-electrode system under the irradiation of UV-visible light with $\lambda > 300$ nm and visible light with $\lambda > 400$ nm, which are displayed in Fig. 4. The Faradaic efficiencies depended on the TiO_2 cathode potential and exhibited a volcano-like tendency regardless of the type of electrode system,

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indicating that the TiO₂ cathode potential was the determining factor in the **OX** reduction system. The highest Faradaic efficiency, i.e., 99%, was achieved at approximately -0.6 V vs RHE in the three-electrode system. Fig. S9† shows cyclic voltammogram curves measured using a three-electrode system employing a TiO₂ cathode, Pt anode and Ag/AgCl reference electrode in the dark recorded in electrolyte solutions with and without the **OX** substrate, respectively. The **OX** reduction current steeply increased below -0.45 V vs RHE, which implicates the larger current density of **OX** reduction at -0.6 V vs RHE of the cathode potential compared to that at -0.45 V vs RHE in the two-electrode system. On the basis of the results, higher Faradaic efficiencies are also expected to be realized by the negative shift of the cathode potential in the two-electrode system employing the WO₃ photoanode. The performances for **OX** reduction in the light-assisted system were compared with those of our previous work and other catalytic hydrogenation researches. The total yields and reaction rates for GO and GC productions in this and previous works and results in the reference 12-15 are summarized in Table S1. The total yields obtained using the two-electrode system employing a standard TiO₂ catalyst in this work are relatively lower than those in the references because of the smaller active sites on the surface of the standard catalyst. On the other hand, the reaction rate using the three-electrode system employing the highly active porous TiO₂ catalyst in our previous work is comparable with those in the references, indicating that the utilization of highly active TiO₂ catalyst having the sufficiently large reactive surface will probably achieve more efficient **OX** reductions. In conclusion, we demonstrated GC production through OX electro-reduction and

potential of more than 2.1~V without light irradiation. Irradiation of UV-visible light to the WO_3 photoanode enables a drastic decrease of minimal bias, i.e., 0.5~V, which is 0.6~V

water oxidation using a light-assisted electrochemical reaction system that applies a TiO₂

cathode and semiconductor oxide photoanodes. The reaction proceeds by applying a bias

1	smaller than the theoretical bias potential, i.e., 1.1 V, required for GC production via OX
2	reduction and water oxidation. GC electrosynthesis with an 80% Faradaic efficiency was
3	achieved when applying a bias of 1.5 V under UV-visible irradiation ($\lambda > 300$ nm). These
4	results are the first demonstration of a green synthetic process for the production of an
5	alcoholic compound from an organic acid procurable from biomass via electro-oxidation of
6	water with the assistance of light energy.

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Figure captions

- 6 Fig. 1 Schematic illustration of light-assisted alcohol electrosynthesis from fossil-free
- 7 carboxylic acid and water.

8

- 9 Fig. 2 (Upper) Current-voltage curves of electro-reduction of **OX** using a two-electrode
- system employing a TiO₂ (JRC-TIO-8) cathode in a solution containing **OX** (0.16 M) and a
- Na₂SO₄ solution (pH 1.2, 40 ml, 0.16 M) and Ga₂O₃, BiVO₄ and WO₃ photoanodes in
- Na₂SO₄ solution (pH 5.8, 40 ml, 0.16 M) at 25 °C under UV-visible light (λ >200 nm)
- irradiation (solid line) or in the dark (broken line). The photographs show photoanodes used
- 14 for the experiment. (Lower) Schematic illustrations of energy diagrams and photovoltaic
- performances for the photoanodes under UV-visible light irradiation.

16

- 17 Fig. 3 Current-voltage curves of electro-reduction of OX using a two-electrode system
- comprising a TiO₂ (JRC-TIO-7) cathode in solution containing **OX** (0.03 M) and Na₂SO₄
- solution (pH 1.0, 40 ml, 0.2 M) and a WO₃ photoanode in Na₂SO₄ solution (pH 5.6, 40 ml,
- 20 0.2 M) under light irradiation, with wavelength >200 nm (red), >300 nm (blue) or >400 nm
- 21 (black), or in the dark (broken line).

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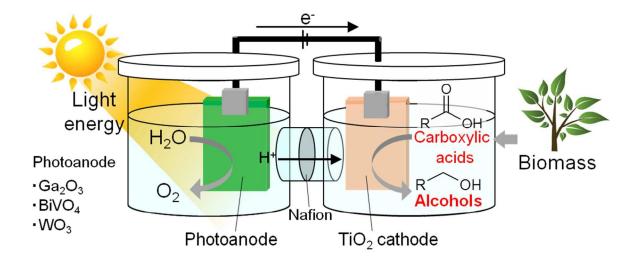
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1	Fig. 4 Faradaic efficiencies calculated based on the amount of GO and GC formed by
2	applying an external bias of 1.0 or 1.5 V in a two-electrode system comprising a ${\rm TiO_2}$
3	(JRC-TIO-7) cathode in \mathbf{OX} solution (pH 1, 40 ml, 0.03 M of OX, 0.2 M Na ₂ SO ₄) and a
4	WO ₃ photoanode in Na ₂ SO ₄ solution (pH 5.6, 40 ml, 0.2 M) at 50°C for 2 h under
5	irradiation of UV-visible light with $\lambda > 300$ nm, visible light with $\lambda > 400$ nm or in the
6	dark.
7	
8	Fig. 5 Faradaic efficiencies (FEs) of GO and GC production versus the TiO ₂ (JRC-TIO-7)
9	cathode potential at 50 °C for 2 h in both the three-electrode system in the dark (square)
10	comprising a TiO ₂ cathode and Ag/AgCl reference electrode in a solution containing OX
11	$(0.03\ M)$ and Na_2SO_4 solution (pH 1.0, 40 ml, 0.2 M) and a Pt anode in a Na_2SO_4 solution
12	(pH 1.0, 40 ml, 0.2 M) and in the two-electrode system comprising a TiO_2 (JRC-TIO-7)
13	cathode in a solution containing \mathbf{OX} (0.03 M) and Na ₂ SO ₄ solution (pH 1.0, 40 ml, 0.2 M)
14	and a WO ₃ photoanode in a Na ₂ SO ₄ solution (pH 1.0, 40 ml, 0.2 M) under irradiation of
15	UV-visible light (triangle) and visible light (circle).

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Fig. 1 Schematic illustration of light-assisted alcohol electrosynthesis from fossil-free carboxylic acid and water.

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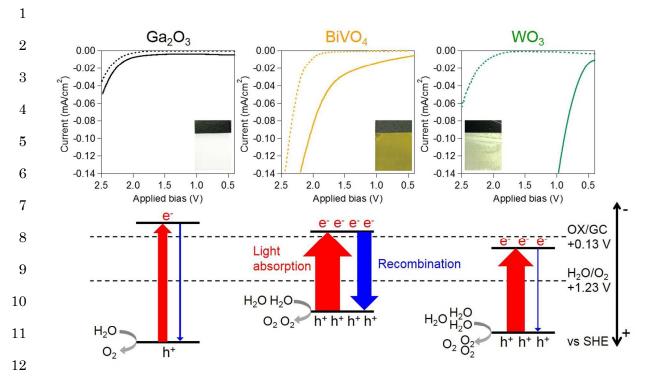


Fig. 2 (Upper) Current-voltage curves of electro-reduction of **OX** using a two-electrode system employing a TiO₂ (JRC-TIO-8) cathode in a solution containing **OX** (0.16 M) and a Na₂SO₄ solution (pH 1.2, 40 ml, 0.16 M) and Ga₂O₃, BiVO₄ and WO₃ photoanodes in Na₂SO₄ solution (pH 5.8, 40 ml, 0.16 M) at 25 °C under UV-visible light (λ >200 nm) irradiation (solid line) or in the dark (broken line). The photographs show photoanodes used for the experiment. (Lower) Schematic illustrations of energy diagrams and photovoltaic performances for the photoanodes under UV-visible light irradiation.

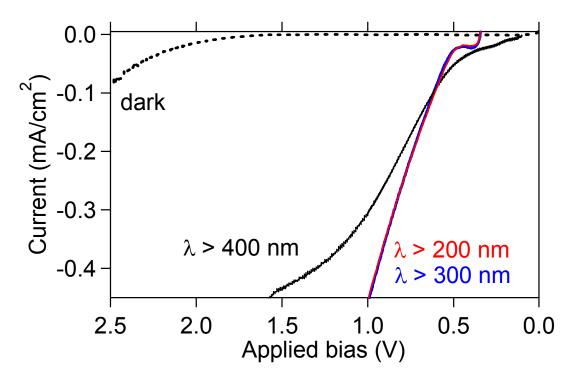


Fig. 3 Current-voltage curves of electro-reduction of **OX** using a two-electrode system comprising a TiO₂ (JRC-TIO-7) cathode in solution containing **OX** (0.03 M) and Na₂SO₄ solution (pH 1.0, 40 ml, 0.2 M) and a WO₃ photoanode in Na₂SO₄ solution (pH 5.6, 40 ml, 0.2 M) under light irradiation, with wavelength >200 nm (red), >300 nm (blue) or >400 nm (black), or in the dark (broken line).

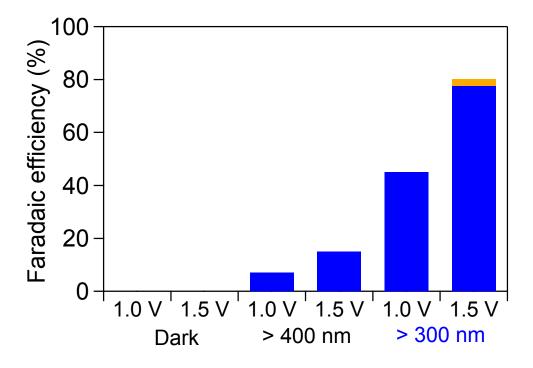


Fig. 4 Faradaic efficiencies calculated based on the amount of GO and **GC** formed by applying an external bias of 1.0 or 1.5 V in a two-electrode system comprising a TiO_2 (JRC-TIO-7) cathode in **OX** solution (pH 1, 40 ml, 0.03 M of OX, 0.2 M Na_2SO_4) and a WO_3 photoanode in Na_2SO_4 solution (pH 5.6, 40 ml, 0.2 M) at 50°C for 2 h under irradiation of UV-visible light with $\lambda > 300$ nm, visible light with $\lambda > 400$ nm or in the dark.

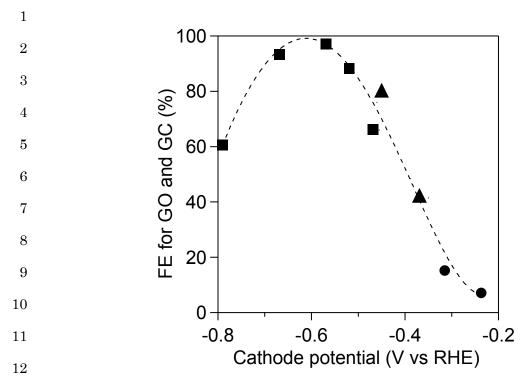


Fig. 5 Faradaic efficiencies (FEs) of GO and **GC** production versus the TiO₂ (JRC-TIO-7) cathode potential at 50 °C for 2 h in both the three-electrode system in the dark (square) comprising a TiO₂ cathode and Ag/AgCl reference electrode in a solution containing **OX** (0.03 M) and Na₂SO₄ solution (pH 1.0, 40 ml, 0.2 M) and a Pt anode in a Na₂SO₄ solution (pH 1.0, 40 ml, 0.2 M) and in the two-electrode system comprising a TiO₂ (JRC-TIO-7) cathode in a solution containing **OX** (0.03 M) and Na₂SO₄ solution (pH 1.0, 40 ml, 0.2 M) and a WO₃ photoanode in a Na₂SO₄ solution (pH 1.0, 40 ml, 0.2 M) under irradiation of UV-visible light (triangle) and visible light (circle).

2 Graphical abstracts

