Accepted Manuscript



This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. We will replace this Accepted Manuscript with the edited and formatted Advance Article as soon as it is available.

You can find more information about *Accepted Manuscripts* in the **Information for Authors**.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard <u>Terms & Conditions</u> and the <u>Ethical guidelines</u> still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.



www.rsc.org/softmatter

1 2	Formation of Thermally Reversible Optically Transparent Emulsion-based Delivery Systems Using Spontaneous
3	Emulsification
4	
5	Amir Hossein Saberi ¹ , Yuan Fang ² and David Julian McClements ^{1,3*}
6 7 0	¹ Biopolymers and Colloids Laboratory, Department of Food Science, University of Massachusetts Amherst, Amherst, MA 01003, USA
8 9	² PepsiCo Global R&D, 100 Stevens Ave, Valhalla, NY 1059, USA
10 11 12 13 14	³ Department of Biochemistry, Faculty of Science, King Abdulaziz University, P. O. Box 12 80203 Jeddah 21589 Saudi Arabia
15	
16	
17	
18	
19	
20	
21	
22	Journal: Soft Matter
23	Submitted: August 2015

^{*}To whom correspondence should be addressed. Tel: (413) 545-1019. Fax: (413) 545-1262. E-mail: mcclements@foodsci.umass.edu.

24 Abstract

25 Transparent emulsion-based delivery systems suitable for encapsulating lipophilic bioactive 26 agents can be fabricated using low-energy spontaneous emulsification methods. These 27 emulsions are typically fabricated from non-ionic surfactants whose hydrophilic head groups are 28 susceptible to dehydration upon heating. This phenomenon may promote emulsion instability 29 due to enhanced droplet coalescence at elevated temperatures. Conversely, the same 30 phenomenon can be used to fabricate optically transparent emulsions through the phase inversion 31 temperature (PIT) method. The purpose of the current study was to examine the influence of oil 32 phase composition and surfactant-to-oil ratio on the thermal behavior of surfactant-oil-water 33 systems containing limonene, medium chain triglycerides (MCT), and Tween 60. Various types 34 of thermal behavior (turbidity versus temperature profiles) were exhibited by these systems 35 depending on their initial composition. For certain compositions, thermoreversible emulsions 36 could be formed that were opaque at high temperatures but transparent at ambient temperatures. 37 These systems may be particularly suitable for the encapsulation of bioactive agents in 38 applications where optical clarity is important. 39 Keywords: nanoemulsion; microemulsion; thermoreversible; limonene; emulsion; delivery

40 systems

42 **1. Introduction**

43 Emulsion-based delivery systems are being developed to encapsulate, protect, and release 44 numerous types of bioactive agents, such as lipophilic drugs, vitamins, nutraceuticals, flavors, colors, and preservatives ¹⁻³. The bioactive agent is usually dissolved within an oil phase, which 45 46 is then homogenized with an aqueous phase containing an emulsifier to form either a 47 conventional emulsion (d > 100 nm) or a nanoemulsion (d < 100 nm). The type of delivery 48 system used depends on the requirements of the specific application, e.g., opacity, stability, and 49 release profile. Nanoemulsions are particularly suitable in low- to high-viscosity products where 50 high optical clarity, high physical stability, and rapid release are required. Conversely, 51 conventional emulsions are more suitable for application in viscous products that are cloudy or 52 turbid, since the large droplets have a tendency to cream/sediment and scatter light strongly. In 53 the remainder of this article, we use the term "emulsions" to refer to both nanoemulsions and 54 conventional emulsions. Emulsions can be fabricated using high-energy approaches (such as 55 high pressure valve homogenization, microfluidization, or sonication) or low-energy approaches 56 (such as spontaneous emulsification, phase inversion temperature, or emulsion inversion point)⁴⁻ ⁶. High-energy methods require specialized mechanical devices ("homogenizers") to form 57 emulsions, but are fairly versatile in the type of oils and emulsifiers that can be utilized $^{7-10}$. On 58 59 the other hand, low-energy methods are simple and inexpensive to implement and can produce emulsions without the need of any specialized equipment ^{5, 11, 12}. However, they are often only 60 suitable for specific combinations of oil and surfactant, and typically require much higher 61 surfactant-to-oil ratios (SOR) than high-energy methods ¹³. Consequently, there is a need to 62 optimize the composition and preparation methods required to produce stable emulsions using 63 64 low-energy methods.

In this study, we focused on the production of emulsions from a commonly used lipophilic flavoring agent (limonene) and a food-grade non-ionic surfactant (Tween 60). In particular, we examined the influence of oil phase composition and SOR on emulsion formation and thermal stability. The information obtained in this study is useful for optimizing the formulation of emulsion-based delivery systems for lipophilic active ingredients.

Soft Matter Accepted Manuscript

70 2. Materials and methods

71 **2.1. Materials**

Medium chain triglyceride (MCT) oil (MIGLYOL[®] 812) was purchased from Warner
Graham Company (Sasol Germany GmbH). Limonene, non-ionic surfactant (Tween 60), citric
acid, and sodium benzoate were purchased from Sigma–Aldrich Co. (St. Louis, MO). Double
distilled water was used in the preparation of all solutions and nanoemulsions. All concentrations
Aare expressed as a mass percentage (wt%).

77 **2.2. Emulsion preparation**

78 Emulsion formation was carried out using a spontaneous emulsification method explained in our previous study ¹⁴. In brief, spontaneous emulsification was performed by addition of an 79 80 organic phase to an aqueous phase while continuously stirring the system using a magnetic 81 stirrer. The composition of the buffer solution was designed to imitate the aqueous phase of 82 many commercial beverage products. Unless otherwise stated, the experiments were carried out 83 using standardized conditions: (i) *composition* - 10% total oil, 15% surfactant, and 75% aqueous 84 phase; (ii) stirring - magnetic stirrer speed of 600 rpm; (iii) temperature - 45 °C. In these 85 samples, the oil (10 g) and surfactant (15 g) were first mixed together and then the mixture was slowly poured into 75 g of aqueous phase over a 15 min period with continuous stirring. In a 86 87 number of experiments the ratio of limonene to MCT in the oil phase was varied and the total 88 amount of surfactant (5, 10, 15, or 20%).

89 **2.3. Particle size measurements**

90 Particle size distributions were measured using a dynamic light scattering instrument 91 (Zetasizer Nano ZS, Malvern Instruments, Malvern, UK). This instrument determines the 92 particle size from intensity-time fluctuations of a laser beam (633 nm) scattered from a dilute 93 emulsion. Each individual measurement was an average of 13 runs. To avoid multiple scattering 94 effects, samples were diluted before the particle size measurements using acidic buffer solution 95 (pH 3.0). The mean particle diameter (Z-average) was calculated from the particle size 96 distribution. All measurements were conducted at ambient temperature.

97 **2.4. Turbidity measurements**

The influence of thermal treatment on the turbidity (absorbance at 600 nm) of the samples was determined using a UV–visible spectrophotometer with temperature scanning capabilities (Evolution Array, Thermo Scientific). Temperature scanning measurements were carried out by measuring the turbidity of the emulsions as the temperature increased from 25 to 95 °C at 1 °C per minute, and then decreased back to 20 and/or 25 °C at different cooling rates. Isothermal measurements were carried out by measuring the turbidity of the emulsions over time (1 min intervals) when they were held at the constant temperatures for 60 min.

105 **2.5. Statistical analysis**

106 All experiments were carried out at least twice using freshly prepared samples and the 107 results are reported as the calculated mean and standard deviation of these measurements.

108 **3. Results and discussions**

109 **3.1 Influence of organic phase composition**

110 Initially, we examined the influence of organic phase composition on the formation and 111 stability of the emulsions by varying the ratio of limonene-to-MCT, while keeping the total oil 112 content fixed (10%). MCT was used as a carrier oil because it has previously been shown to be 113 capable of forming stable nanoemulsions using the spontaneous emulsification method¹⁴. This stability has been attributed to the ability of MCT to act as a ripening inhibitor that slows down 114 the rate of droplet growth due to Ostwald ripening ^{15, 16}. Ostwald ripening is the process 115 whereby polar lipids (such as limonene) are transported from small to large droplets through the 116 intervening aqueous phase ¹⁷. The driving force for this process is the increase in the water-117 118 solubility of oils with increasing droplet curvature, *i.e.*, decreasing droplet size. Emulsions were 119 formed using four different surfactant concentrations (5, 10, 15, and 20 %), which correspond to 120 four different SOR values (0.5, 1, 1.5, and 2).

In general, there was initially a decrease in mean particle diameter with increasing limonene concentration until a minimum value was attained, after which the diameter increased upon further limonene addition (**Figure 1**). This kind of phenomenon has been observed previously

124 for emulsions formed by spontaneous emulsification using different kinds of oils, such as vitamin E acetate and MCT^{14,18}. The relatively low molecular weight and polar limonene 125 126 molecules may enhance the formation of small droplets at relatively low concentrations because 127 they alter the optimum curvature, tension, and flexibility of the surfactant monolayer, thereby 128 facilitating the spontaneous generation of oil droplets at the boundary between the organic and 129 aqueous phases. However, when the limonene concentration is too high, the droplet size 130 increases because of Ostwald ripening. Consequently, there is an optimum limonene level (6 to 131 7%) required to form stable nanoemulsions containing small droplets, which corresponds to 60 to 132 70% limonene within the organic phase. The smallest droplets that could be produced were for 133 the systems containing 15 or 20% surfactant and 6% limonene, which had mean droplet 134 diameters around 25 nm.

135 The size of the droplets produced by spontaneous emulsification also depended strongly on 136 the surfactant-to-oil ratio (Figure 1). At low limonene levels, the droplet size decreased with 137 increasing SOR, but at intermediate limonene levels droplet size was minimum at an 138 intermediate SOR. A minimum in the droplet size at an intermediate surfactant concentration has also been reported in other studies using spontaneous emulsification 14,19 . This effect can be 139 140 attributed to the fact that a certain amount of surfactant is required to achieve the surfactant-oil-141 water compositions required at the boundary between the organic and aqueous phases to spontaneously form small droplets ^{5, 20}. The precise physicochemical mechanism responsible for 142 this phenomenon is currently unknown, but it may be associated with the formation of a bi-143 144 continuous microemulsion phase that has nanostructured lipid domains that breakdown into small droplets in the presence of water ^{12, 20}. 145

For certain practical applications, it is important that emulsion-based delivery systems have 146 high optical clarity, e.g., beverages fortified with lipophilic vitamins and nutraceuticals ²¹. We 147 148 therefore examined the influence of oil phase composition and surfactant-to-oil ratio on the 149 turbidity of the emulsions produced by spontaneous emulsification (Figure 2). The turbidity was measured before and after a thermal heat treatment (25 to 90 to 25 °C, at 1 °C/min). Prior to 150 151 heating, a number of the emulsions already had relatively low turbidities, which tended to be clustered at intermediate limonene levels and high surfactant levels (Figure 2a). After heating, 152 153 the range of conditions where low turbidities could be achieved was reduced appreciably: 6-8%

limonene for 20% surfactant; 7-8% limonene for 15% surfactant; and 8-9% limonene for 10%
surfactant (Figure 2b). These results suggest that emulsions that were optically clear and stable
to heating could be produced under certain conditions.

157 When the turbidities were plotted against the droplet diameters of the same systems it was 158 clear that emulsions with relatively low turbidities ($<0.5 \text{ cm}^{-1}$) could only be formed for the 159 systems containing very fine droplets, *i.e.*, d < 50 nm (**Figure 3**). This effect can be attributed to 160 the fact that the scattering of light by colloidal particles decreases appreciably when the droplet 161 dimensions are much smaller than the wavelength of light, *i.e.*, $d < \lambda/10^{22}$.

162 **3.2 Influence of composition on thermal behavior of nanoemulsions**

In commercial applications, emulsion-based delivery systems are often exposed to variations in temperature, which may affect their particle size, turbidity, and physical stability. We therefore measured the influence of a well-controlled heating-cooling cycle on the turbidity of the emulsions: 25 to 95 to 25 °C at 1 °C per minute (**Figure 4**). In general, the behavior of the emulsions could be divided into a number of different categories depending on their turbidity *versus* temperature profiles (**Table 1**). Selected examples of SOW combinations that produced different kinds of thermal behavior are outline below.

Non-thermoreversible-Type 1 (NT-1): These emulsions were turbid prior to heating because spontaneous emulsification did not generate small droplets at these SOW compositions (Figure 4a). They were also turbid after heating suggesting that the heating-cooling cycle did not generate small droplets for these systems. The emulsions appeared physically stable after the thermal treatment, *i.e.*, they had a homogeneous appearance throughout. This kind of behavior can be attributed to the fact that the phase inversion temperature (PIT) was well above the measurement range for these surfactant-oil-water combinations.

Non-thermoreversible-Type 2 (NT-2): These emulsions had a low turbidity and homogenous appearance prior to heating because spontaneous emulsification successfully generated small oil droplets that did not scatter light strongly at these SOW combinations (Figure 4b). The turbidity of these emulsions remained relatively low as they were heated, until a critical temperature was reached after which it increased steeply. Upon cooling, the emulsions remained highly turbid (after they had been inverted a number of times to make them homogeneous), and they separated

183 into a white cream layer on top of a watery serum layer when they were left to stand (**photo** 184 inset, Figure 4b). This result suggests that extensive droplet coalescence occurred during the 185 heating process, leading to the formation of large droplets that scattered light strongly and 186 creamed rapidly. In this case, it is likely that these emulsions passed through a region just below 187 the PIT (the "coalescence zone") where the droplets were highly susceptible to coalescence 188 because of the change in their surfactant head group hydration. When non-ionic surfactants are 189 heated their head groups become progressively dehydrated, which changes the monolayer packing parameter (p = tail group cross section / head group cross section)²³ and the relative 190 surfactant solubility (oil-to-water partition coefficient)²⁰. These changes alter the interfacial 191 tension and flexibility, and may promote droplet coalescence over a certain temperature range²³. 192

193 Non-thermoreversible-Type 3 (NT-3): These emulsions initially had a low turbidity and 194 homogenous appearance prior to heating because spontaneous emulsification generated small oil 195 droplets that did not scatter light strongly (Figure 4c). When these emulsions were heated the 196 turbidity remained relatively low, until a critical temperature was reached and the turbidity 197 increased dramatically, which can be attributed to rapid droplet coalescence in the temperature 198 range just below the PIT as discussed for the NT-2 systems. However, the turbidity of the 199 emulsions decreased again upon further heating, which can be attributed to the formation of a bi-200 continuous microemulsion at the PIT that only contains small domains that do not scatter light 201 strongly. Nevertheless, upon cooling below a critical temperature the turbidity increased rapidly, 202 suggesting that extensive droplet coalescence occurred leading to stronger light scattering. 203 Interestingly, after cooling these emulsions had a homogeneous appearance with no evidence of 204 creaming, which suggests that the droplets formed were not too large (photo inset, Figure 4c).

205 Non-thermoreversible-Type 4 (NT-4): These emulsions initially had a high turbidity prior to 206 heating because spontaneous emulsification could not produce small oil droplets, or because they 207 were highly susceptible to Ostwald ripening (Figure 4d). Emulsions containing flavor oils (such 208 as lemon or orange oils) have been reported to be highly unstable to droplet growth due to 209 Ostwald ripening, which has been attributed to the relatively higher water-solubility of these oils 210 in water ^{24, 25}. This process involves the diffusion of oil molecules from the small droplets to the 211 large droplets through the intervening aqueous phase, and is driven by the increase in the water-212 solubility of the oil molecules with increasing curvature of the oil-water interface. When these

213 emulsions were heated the turbidity remained relatively high, until a certain temperature was 214 reached and then it fell to a relatively low level due to the formation of a bi-continuous 215 microemulsion at the PIT. Upon further heating the turbidity increased due to phase inversion to 216 a water-in-oil emulsion containing large water droplets that scatter light strongly. Upon cooling 217 the turbidity remained relatively high until a certain temperature was reached, and then it fell 218 steeply. This effect was probably an artefact associated with the creaming of the oil droplets to 219 the top of the cuvettes, thereby decreasing the droplet concentration in the path of the light beam. 220 Indeed, after cooling the emulsions had separated into a cream layer and a serum layer (photo 221 inset, Figure 4d).

222 *Thermoreversible (T)*: These emulsions initially had a relatively low turbidity and 223 homogenous appearance because spontaneous emulsification generated small oil droplets that 224 did not scatter light strongly (Figure 4e). Upon heating, the turbidity fell appreciably above a 225 certain temperature, which suggested that a bi-continuous microemulsion phase was formed. 226 Upon further heating, the turbidity increased again, which can be attributed to phase inversion 227 and the formation of a water-in-oil emulsion containing relatively large water droplets that 228 scattered light strongly. Upon cooling, the turbidity decreased steeply below a certain 229 temperature, leading to the formation of a transparent emulsion with a homogeneous appearance 230 (photo inset, Figure 4d). The formation of ultrafine emulsions using this heating-cooling 231 process is that same as that by the PIT method that has been widely used to prepare nanoemulsions ^{12, 20}. 232

233 It should be noted that the precise thermal behavior observed is specific for the limonene, 234 Tween 60 and water system studied, and may be different when either the oil or surfactant type is 235 changed. For example, we did not observe the same type of behavior when limonene was 236 replaced with vitamin E acetate or when different surfactants were used (ongoing research). It 237 seems that composition, structural organization, and physicochemical properties of the 238 surfactant-oil-water mixtures are responsible for the complicated thermal behavior observed in 239 this type of system. Further research is clearly needed to obtain more insight into the effect of 240 system composition on the thermal behavior of emulsions produced using the spontaneous 241 emulsification method, and to identify the molecular and physicochemical processes involved.

The influence of initial system composition (oil phase composition and surfactant level) on the mean particle diameter of the emulsions produced by this heating-cooling process were measured (**Figure 5**). These measurements indicated that nanoemulsions (d < 100 nm) could be formed over a range of intermediate limonene levels, particularly at high surfactant levels. As expected, the range of SOR compositions where small droplets are formed corresponds to the range where low turbidities are obtained (**Figure 2b**).

248 **3.3. Influence of isothermal incubation on turbidity changes**

These two SOW compositions were chosen because they had different optical properties after the heat-cool treatment: (i) *NT-3*: opaque (**Figure 4c**); (ii) *T*: transparent (**Figure 4e**).

251 For the SOW system containing 5% limonene, the turbidity remained relatively low and 252 constant when it was held at 50 °C for 1 hour, indicating that the droplets were stable to growth 253 at this temperature (Figure 6a). The lack of droplet growth can be attributed to the fact that 254 these emulsions were well below the phase inversion temperature (PIT \approx 90 °C, Figure 4c), and 255 were therefore relatively stable to droplet coalescence. However, when this SOW system was 256 held at 75 or 85 °C there was a rapid increase in turbidity over time, which suggested that 257 extensive droplet growth occurred, which can be attributed to coalescence just below the phase 258 inversion temperature (Figure 4c). When this system was held at 90 °C, there was an initial 259 increase in turbidity during the first few minutes, but then the system became transparent. The 260 initial turbidity increase can be attributed to some droplet growth occurring as the emulsion was 261 heating up to the final temperature and passed through the coalescence zone. The high clarity at 262 longer holding times suggests that a bi-continuous microemulsion was formed around the PIT 263 that contained small domains that did not scatter light strongly (Figure 4c).

Quite different behavior was observed for the SOW system containing 7% limonene (**Figure 6b**). In this case, the turbidity remained relatively low and constant when the initial emulsions were held at 50 °C for 1 hour due to the fact that they were well below the phase inversion temperature (PIT \approx 80 °C, **Figure 4e**). There was actually a decrease in turbidity when these SOW systems were held at 75 and 85 °C for 1 hour (**Figure 6b**), which was around the temperature where they became clear during heating (**Figure 4e**). In this region we postulate that a bi-continuous microemulsion was formed around the PIT. There was a rapid increase in Page 11 of 32

Soft Matter

turbidity when these SOW systems were held at 90 °C for 1 hour, which can be attributed to the
formation of a water-in-oil emulsion above the PIT that contained water droplets that scattered
light strongly (Figure 4e).

These isothermal incubation experiments therefore support the results of the temperaturescanning experiments discussed in the previous experiments. They highlight that the optical properties of a given SOW system depend strongly on its composition and holding temperature.

3.4. Influence of cooling rate on nanoemulsion formation

The purpose of these experiments was to examine the influence of cooling rate on the formation of transparent nanoemulsions, since previous studies have highlighted that this parameter can have a major impact on the size of the droplets formed by the PIT method ^{20, 26}. In this series of experiments, the thermoreversible (T) and non-thermoreversible (NT-3) SOW systems studied in the previous section were used again. The SOW systems were heated to 90 °C and then cooled at different rates ranging from around 1 to 67 °C/min (**Figure 7**).

284 For the SOW system containing 5% limonene, the final turbidity depended strongly on the 285 cooling rate used to produce the final emulsions (Figure 7a). When the cooling rate was 286 relatively slow (1 °C/min), there was a large increase in turbidity when the temperature was 287 reduced from 90 to 20 °C, but when it was relatively rapid (67 °C/min) the turbidity remained 288 low indicating that the final systems contained relatively small droplets. Overall, the final 289 turbidity of the emulsions after the heat-cool cycle increased with decreasing cooling rate. This 290 phenomenon can be attributed to the fact that the SOW systems spent a longer time in the 291 temperature range just below the PIT where rapid droplet growth occurred due to coalescence. 292 However, emulsions containing very fine droplets could be produced by quench cooling the 293 SOW systems from above the PIT to a temperature well below the PIT.

For the SOW system containing 7% limonene, the final turbidity was low for all cooling rate rates used to produce the emulsions (**Figure 7b**). Interestingly, the only emulsion that gave a slightly higher turbidity than the other samples was the one that was quench cooled (67 °C/min). These results indicate that very different thermal behaviors were obtained depending on the initial SOW compositions of the emulsions used.

Soft Matter Accepted Manuscript

3.5. Storage stability

300 Finally, we measured the storage stability of selected emulsions by measuring the change in 301 the mean particle diameter before and after holding them at ambient temperature for 30 days 302 (Figure 8). There was little change in the particle size during the storage period, which 303 suggested that the emulsions produced using this method had relatively good long-term stability. 304 We also tested the stability of the emulsions to two sequential heat-cool cycles, and found that 305 the particle size remained relatively constant after the repeated cycles (data not shown). In 306 commercial applications, it would be important to test the stability of the emulsions under 307 environmental conditions that the products would be expected to be utilized at, e.g., pH, ionic 308 strength and temperature fluctuations.

309 4. Conclusions

310 In this study, we examined the influence of initial system properties (oil phase composition 311 and surfactant-to-oil ratio) on the thermal stability of emulsions produced by spontaneous 312 emulsification. Emulsions containing very small droplets that do not scatter light strongly could 313 only be produced over a limited range of system compositions using spontaneous emulsification 314 at ambient temperatures: intermediate limonene-to-MCT ratios and high surfactant-to-oil ratios. 315 After being subjected to a slow heating-cooling cycle (25 to 90 to 25 °C at 1 °C/min) some of the 316 emulsions were optically transparent (small droplets), whereas others were opaque (large 317 droplets) highlighting differences in their thermal stability. In addition, some of the emulsions 318 were thermoreversible, whereas others were non-thermoreversible, depending on their initial 319 composition. For non-thermoreversible systems, transparent emulsions could be formed by 320 quench cooling the surfactant-oil-water mixtures to a temperature well below the phase inversion 321 temperature. The main cause of high turbidity after heating-cooling was attributed to the length 322 of time the emulsions remained in the temperature range just below the PIT where rapid droplet 323 coalescence occurred: the longer the time, the higher the final droplet size and turbidity. 324 Interestingly, for the thermoreversible systems there did not appear to be a pronounced droplet 325 coalescence zone, as was observed in the non-thermoreversible systems. In this study, we used a 326 relatively simple surfactant-oil-water system with a fixed total oil concentration. In future, 327 studies it would be useful to examine the impact of oil concentration on the formation and

328 properties of emulsions created by spontaneous emulsification since this parameter may also

- 329 impact their fabrication and functional behavior. These results have important implications for
- the formation and stability of emulsion-based delivery systems for lipophilic active agents.

331 5. Acknowledgements

- 332 This material was partly based upon work supported by the Cooperative State Research,
- 333 Extension, Education Service, USDA, Massachusetts Agricultural Experiment Station (Project
- No. 831) and USDA, NRI Grants (2011-03539, 2013-03795, 2011-67021, and 2014-67021).
- This project was also partly funded by the Deanship of Scientific Research (DSR), King
- Abdulaziz University, Jeddah, under grant numbers 330-130-1435-DSR, 299-130-1435-DSR,
- 87-130-35-HiCi. The authors, therefore, acknowledge with thanks DSR technical and financial
- 338 support. The authors also thank William Mutilangi of PepsiCo for useful advice and discussions
- on this research, and PepsiCo for funding AHS.

340 Disclaimer

- 341 The opinions expressed in this manuscript are those of the authors and do not represent
- 342 statements of position, intention or strategy of PepsiCo Inc.

343 **References**

- 1. M. Kakran and M. N. Antipina, *Current Opinion in Pharmacology*, 2014, **18**, 47-55.
- 2. D. J. McClements, *Current Opinion in Colloid & Interface Science*, 2012, **17**, 235-245.
- 346 3. D. J. McClements, E. A. Decker and J. Weiss, *Journal of Food Science*, 2007, 72, R109347 R124.
- 348 4. M. Y. Koroleva and E. V. Yurtov, *Russian Chemical Reviews*, 2012, **81**, 21-43.
- 349 5. C. Solans and I. Sole, Current Opinion in Colloid & Interface Science, 2012, 17, 246-254.
- 350 6. D. J. McClements, Soft Matter, 2011, 7, 2297-2316.
- 351 7. S. M. Jafari, Y. He and B. Bhandari, *European Food Research and Technology*, 2007, 225, 733-741.
- 353 8. S. M. Jafari, Y. H. He and B. Bhandari, Int. J. Food Prop., 2006, 9, 475-485.
- 354 9. T. J. Wooster, M. Golding and P. Sanguansri, *Langmuir*, 2008, **24**, 12758-12765.
- 355 10. C. Qian and D. McClements, *Food Hydrocolloids*, 2010.
- 11. N. Anton, J. P. Benoit and P. Saulnier, Journal of Controlled Release, 2008, 128, 185-199.
- 357 12. K. Roger, B. Cabane and U. Olsson, *Langmuir*, 2010, **26**, 3860-3867.

- 358 13. D. J. McClements and J. Rao, *Critical Reviews in Food Science and Nutrition*, 2011, 51, 285-330.
- 360 14. A. H. Saberi, Y. Fang and D. J. McClements, *Journal of Colloid and Interface Science*,
 361 2013, **391**, 95-102.
- 362 15. Y. Chang, L. McLandsborough and D. J. McClements, *Journal of Agricultural and Food* 363 *Chemistry*, 2012, **60**, 12056-12063.
- 364 16. A. H. Saberi, Y. Fang and D. J. McClements, *Journal of Colloid and Interface Science*,
 2013, 411, 105-113.
- 366 17. P. Taylor, Advances in Colloid and Interface Science, 1998, 75, 107-163.
- 367 18. A. H. Saberi, Y. Fang and D. J. McClements, *Colloids and Surfaces a-Physicochemical and* 368 *Engineering Aspects*, 2014, 449, 65-73.
- 369 19. Y. Yang, C. Marshall-Breton, M. E. Leser, A. A. Sher and D. J. McClements, *Food* 370 *Hydrocolloids*, 2012, **29**, 398-406.
- 371 20. N. Anton and T. F. Vandamme, *International Journal of Pharmaceutics*, 2009, 377, 142 372 147.
- 21. D. T. Piorkowski and D. J. McClements, Food Hydrocolloids, 2014, 42, 5-41.
- 22. D. J. McClements, Advances in Colloid and Interface Science, 2002, 97, 63-89.
- 375 23. A. Kabalnov and H. Wennerstrom, *Langmuir*, 1996, **12**, 276-292.
- 376 24. J. Rao and D. J. McClements, Food Chemistry, 2012, 134, 749-757.
- 377 25. P.-H. Li and B.-H. Chiang, Ultrasonics Sonochemistry, 2012, 19, 192-197.
- 378 26. A. H. Saberi, Y. Fang and D. J. McClements, *Food Chemistry*, 2015, **185**, 254-260.

379

	Limonene (%)										
	0	1	2	3	4	5	6	7	8	9	10
Tween 60 (5%)	NT-1 ^a	NT-1	NT-4	NT-4							
Tween 60 (10%)	NT-2	NT-2	NT-2	NT-2	NT-2	NT-3	NT-3	NT-3	Т	Т	NT-4
Tween 60 (15%)	NT-2	NT-2	NT-2	NT-2	NT-2	NT-3	NT-3	Т	Т	NT-4	NT-4
Tween 60 (20%)	NT-2	NT-2	NT-2	NT-3	NT-3	NT-3	Т	Т	Т	NT-4	NT-4

Table 1. Effect of oil phase composition and surfactant concentration on thermal behavior (thermo-reversibility) of limonene loaded emulsions^{*}.

^a NT-1, -2, -3, -4: Not thermoreversible-type 1, 2, 3, and 4, respectively; T: Thermoreversible.

^{*} Emulsions were prepared initially prepared by spontaneous emulsification using 10 wt% oil phase (limonene + MCT), different concentrations of surfactant phase (Tween-60; 5%, 10%, 15%, and 20%), and the remainder aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. See Figure 4 for selected temperature-turbidity profiles representing different thermal behaviors.

16

381



Figure 1. Effect of oil composition (wt.% of limonene in emulsion) on mean particle diameter of emulsion produced by spontaneous emulsification. Emulsions were prepared using 10 % oil phase (limonene + MCT), different concentrations of surfactant phase (Tween-60; 10%, 15%, and 20%), and aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 2a. Effect of oil phase and surfactant phase concentration on the turbidity of emulsion before thermal treatment. Emulsions were prepared by spontaneous emulsification approach using 10 % oil phase (limonene + MCT), different concentrations of surfactant phase (Tween-60; 5%, 10%, 15%, and 20%), and aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 2b. Effect of temperature (heating from 25 to 95 °C followed by cooling from 95 °C to 25 °C using the thermal rate of 1 °C/min) on the turbidity of emulsion containing different oil phase compositions and surfactant concentrations. Emulsions were prepared by spontaneous emulsification approach using 10 % oil phase (limonene + MCT), different concentrations of surfactant phase (Tween-60; 5%, 10%, 15%, and 20%), and aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 3. Plot of the turbidity of the nanoemulsions versus the droplet diameter, which shows that transparent systems can only be formed at very low particle sizes. The line is included to guide the eye.



Figure 4a. Influence of temperature on turbidity of emulsions produced using 10% oil phase (4% limonene & 6% MCT), 5% surfactant phase (Tween 60), and 85% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. This figure is representative of *non-thermoreversible-type-1* (NT-1) emulsion. See Tables 1, 2, and 3. *Key*: I: Emulsion before thermal treatment. II: Emulsion after heating and cooling cycles.



Figure 4b. Influence of temperature on turbidity of emulsions produced using 10% oil phase (3% limonene & 7% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. This figure is representative of Not thermoreversible-type-2 (NT-2) emulsion. See Tables 1, 2, and 3.

- I: Fresh emulsion before thermal treatment.
- II: Emulsion after heating and cooling cycles.



Figure 4c. Influence of temperature on turbidity of emulsions produced using 10% oil phase (5% limonene & 5% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. This figure is representative of non-thermoreversible-type-3 (NT-3) emulsion. See Tables 1, 2, and 3. *Key:* I: Fresh emulsion before thermal treatment. II: Emulsion after heating and cooling cycles.



Figure 4d. Influence of temperature on turbidity of emulsions produced using 10% oil phase (limonene), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. This figure is representative of non-thermoreversible-type-4 (NT-4) emulsion. See Tables 1, 2, and 3. NT-4 underwent phase separation. I: Fresh emulsion before thermal treatment. II: Emulsion after heating and cooling cycles.



Figure 4e. Influence of temperature on turbidity of emulsions produced using 10% oil phase (7% limonene & 3% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. This figure is representative of thermoreversible-type-1 (T-1) emulsion. See Tables 1, 2, and 3. Key: I: Fresh emulsion before thermal treatment. II: Emulsion after heating and cooling cycles.



Figure 5. Effect of oil phase composition and surfactant concentration on the mean particle diameter produced after slow heating followed by cooling. Emulsions were initially prepared by spontaneous emulsification approach using 10 % oil phase (limonene + MCT), different concentrations of surfactant phase (Tween-60; 5%, 10%, 15%, and 20%), and aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45 °C.



Figure 6a. Influence of holding time at different temperatures (different isothermal conditions) on the turbidity of emulsion produced using 10% oil phase (5% limonene & 5% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 6b. Influence of holding time at different temperatures (different isothermal conditions) on the turbidity of emulsion produced using 10% oil phase (7% limonene & 3% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 7a. Influence of cooling rate on the turbidity of emulsion produced using 10% oil phase (5% limonene & 5% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 7b. Influence of cooling rate on the turbidity of emulsion produced using 10% oil phase (7% limonene & 3% MCT), 15% surfactant phase (Tween 60), and 75% aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C.



Figure 8. Effect of storage time on mean particle diameter of emulsion produced using spontaneous emulsification. Emulsions were produced using 10% oil phase (8% limonene & 2% MCT), 10, 15, and 20% surfactant phase (Tween 60), and aqueous phase (pH 3 buffer solution) at a stirring speed of 600 rpm at 45°C. Emulsions were subjected to thermal treatment (heating from 25 to 95 °C followed by cooling from 95 °C to 25 °C using the thermal rate of 1 °C/min) before storage study.

Factors Affecting Thermal Reversibility of Ultrafine Limonene-Enriched Emulsions Produced Using Spontaneous Emulsification, by Amir Hossein Saberi, Yuan Fang, and David Julian McClements *



Oil phase composition and surfactant-to-oil ratio have appreciable impacts on the transparency and thermal behavior of surfactant-oil-water systems containing limonene, medium chain triglycerides (MCT), and Tween 60.