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1 **A novel mariner-based transposon system for the enhanced removal of high strength**  
2 **ammoniacal nitrogen in pharmaceutical effluent**

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## 34 Abstract

35 Industrial wastewater is the major polluting agent in the environment as huge amount of  
36 untreated effluent is discharged from industries causing serious effect to biotic system. The  
37 pharmaceutical industry effluent used in the present study contains high concentration of  
38 ammonical nitrogen ( $\text{NH}_3\text{-N}$ ) about  $500 \text{ mg L}^{-1}$ . In the present study, efficient  $\text{NH}_3\text{-N}$  removing  
39 strain was isolated, and enriched in the effluent with high  $\text{NH}_3\text{-N}$  concentration for its efficient  
40 removal. The strain which showed higher removal efficiency was identified as *Proteus penneri*  
41 by ribotyping. The wild type *P. penneri* exhibited low removal efficiency (64%) in 24 hours  
42 even after the conventional enrichment method. Hence, the strain was mutated to improve its  
43 degradation efficiency using modified mariner based transposon system. It was constructed by  
44 replacing the  $\text{Kan}^r$  gene with  $\text{Gm}^r$  gene to develop pSC189::miniTn(Gm), since the isolated  
45 strain was resistant to kanamycin. Two mutant strains T<sub>55</sub> and T<sub>132</sub> were shown to have enhanced  
46  $\text{NH}_3\text{-N}$  removal efficiency by 84% and 81% respectively, in 24 hours. The kinetic rate constants  
47 such as pseudo first and second order kinetics were evaluated for the degradation of  $\text{NH}_3\text{-N}$  by  
48 wild type *P. penneri* and transposon mutant; both of them followed second order rate kinetics.  
49 The  $\text{NH}_3\text{-N}$  removal was confirmed by Ion chromatography (IC) and Fourier Transform-Infrared  
50 Spectroscopy (FT-IR). To date, there is no report on the strain improvement using transposon  
51 mutagenesis for the treatment of  $\text{NH}_3\text{-N}$ .

52

53 **Keywords:**  $\text{NH}_3\text{-N}$  removal; Random mutagenesis; Transposon mutagenesis; *Proteus penneri*;  
54 Pharmaceutical effluent treatment.

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## 57 1. Introduction

58 Waste water released from various industries becomes the major concerns to  
59 environmentalists since they contain complex nature of chemicals with poor biodegradability.<sup>1</sup>  
60 Ammonium salts are present in certain industrial wastewaters such as leather, chemical,  
61 pharmaceutical and pesticide manufacturing industries.<sup>2</sup> Pharmaceutical industries all over the  
62 world generate large quantities of wastewater that contain considerable concentration of  
63 antibiotics, organic compounds as well as ammoniacal nitrogen ( $\text{NH}_3\text{-N}$ ). The conventional  
64 methods such as chemical precipitation (Magnesium Ammonium Phosphate (MAP) process),<sup>3,4</sup>  
65 air stripping process,<sup>5</sup> ion exchange,<sup>6</sup> etc. have been examined and each process has its own  
66 demerits in field level implementation. The chemical precipitation generates huge amount of  
67 toxic sludge and it needs to be dumped in landfill sites and the landfill leachates cause major  
68 environmental problems. The air stripping process releases the toxic ammonia into the air and  
69 the ion exchange process is not economically viable since it needs to be regenerated after the  
70 removal. Thus, the biological process is preferred, since it overcomes the demerits caused by  
71 physico-chemical treatment methods. Mainly, the biological process is eco-friendly in nature,  
72 since it provides the sludge free treatment. The economic advantage, both in terms of capital  
73 investment and operating costs of biological treatment over other conventional treatment  
74 processes, has cemented its place in any integrated wastewater treatment plant. The major  
75 problem with biodegradation of pharmaceutical effluent is the presence of high concentration of  
76  $\text{NH}_3\text{-N}$  ( $>100 \text{ mg L}^{-1}$ ); such high concentration impairs the biodegradation of antibiotics and  
77 other organic compounds in effluent due to the toxicity of  $\text{NH}_3\text{-N}$  exerted to the microorganisms.  
78 Therefore, in pharmaceutical effluent, it becomes important to remove the  $\text{NH}_3\text{-N}$ , in order to  
79 ease the biodegradation of antibiotics and organic compounds by the microbial consortium.

80 Therefore, the focal theme of the present investigation was to isolate the ammonia utilizing  
81 bacterial strain *Proteus penneri*, enrich and use for the removal of ammonia from pharmaceutical  
82 industry effluent (PIE).

83 Commonly, 16S rDNA molecules are the tools to investigate microbial communities that  
84 avoid limitations of culturability. Several functional genes were to be useful for the same  
85 purpose because their phylogeny are congruent or very similar to phylogenetic relationships  
86 based on 16S rRNA gene (rDNA) analyses and moreover they indicate functional diversity in the  
87 environment.<sup>5</sup>

88 This paper mainly discusses about the biological method for the removal of NH<sub>3</sub>-N in  
89 PIE by *P. penneri*. In addition, the study was aimed to extend the modification and incorporation  
90 of a mariner transposon in the genome of *P. penneri* to generate libraries of random insertion  
91 mutants. The mariner transposons as demonstrated by Linong *et al.*<sup>7</sup> was expected to move  
92 through a DNA intermediate during transposition using a ‘cut-and-paste’ mechanism, resulting in  
93 excision of the transposon from the original location and insertion at novel sites in the genome.  
94 Lionel *et al.*<sup>8</sup> reported that they always integrate into a TA target dinucleotide, which causes  
95 insertional inactivation of the particular site. The libraries are then screened to identify mutants  
96 that are defective in a particular phenotype so that it shows enhanced removal of NH<sub>3</sub>-N in a  
97 short duration of time. This approach is cost-effective and applicable to a wide variety of  
98 bacteria.<sup>9</sup> These “suicide” vectors are rapidly lost but allow the integration of passenger  
99 exogenous DNA carrying selection markers through transposition or homologous recombination  
100 in the chromosomes of recipient strains.

101 Therefore, in the present study, evaluated the use of *HimarI mariner* transposons<sup>10</sup> for  
102 random mutagenesis of *P. penneri* and the efficient bacterial strains were isolated by screening

103 the transposon mutants from its library. They were further enriched in the industrial effluent and  
104 their efficiency was increased to further enhance the efficient treatment in a short duration of  
105 time. To date, there is no report on the treatment of  $\text{NH}_3\text{-N}$  by the strain which is modified by the  
106 method of transposon mutagenesis.

## 107 **2. Materials and Methods**

### 108 *2.1. Materials*

109 The ammoniacal nitrogen containing pharmaceutical wastewater was obtained from a  
110 pharmaceutical industry, Chennai, India. The chemicals used in the study were purchased from  
111 Himedia and Sigma-Aldrich-Fluka Chemical Co., India. The primers were purchased from  
112 Bioserve, Chennai. All the enzymes used for molecular biology works were purchased from New  
113 England Biolabs (NEB), Chennai, India.

### 114 *2.2. Isolation and identification of ammonia oxidizing microbial strain*

115 The efficient ammonia oxidizing bacterial strains were isolated from the PIE  
116 contaminated soil by the enrichment method. The enrichment was started with the introduction  
117 of contaminated soil in the industrial effluent and incubated it for 96 hours under aeration ( $1 \text{ L}$   
118  $\text{min}^{-1}$ ) and the grown up bacterial cultures were used as mother inocula for the further periodic  
119 enrichment. The culture was then periodically transferred into the fresh effluents in 3 days  
120 interval where the enrichment was continued upto 3 weeks. Then the bacterial strains which  
121 acclimatized with the PIE were screened for the better efficiency in the removal of  $\text{NH}_3\text{-N}$ .  
122 Around 3 different bacterial strains were isolated from the enriched sample. Amongst 3 strains,  
123 the strain which showed higher efficiency in the removal of  $\text{NH}_3\text{-N}$  was subjected to molecular  
124 identification by ribotyping.

125 To identify the strain, fD1 [CGAATTCGTCGACAACAGAGTTTGATCCTGGCTCAG]  
126 and rP1 [CCCGGGATCCAAGCTTACGGTTACCTTGTTACGACTT] primers<sup>11</sup> were used for  
127 amplification of the variable region of the 16S rDNA gene. The deduced sequence was subjected  
128 to BLAST analysis against NCBI database. Phylogenetic analysis was performed by subjecting  
129 the deduced sequence to the 16S rDNA data base to obtain the closely related sequences, and the  
130 phylogenetic tree was constructed, based on evolutionary distances that were calculated by  
131 following the distance matrix method, using the Phylip package.<sup>12</sup> The strain was maintained in  
132 Luria Bertani (LB) medium for the further use.

### 133 2.3. Removal of ammoniacal nitrogen in industrial effluent by wild type strain *Proteus penneri*

134 The removal of ammoniacal nitrogen in PIE was carried out in 1L batch reactor. The  
135 enriched *P. penneri* culture was centrifuged at 10,000 rpm for 10 minutes and the pellet was  
136 collected and inoculated in 1L PIE. The moisture content of the biomass is 0.2 g g<sup>-1</sup> of biomass.  
137 Various parameters were optimized for the enhanced removal of NH<sub>3</sub>-N from PIE by varying the  
138 time (24, 48, 72 and 96 hours), pH (6.0 to 9.0) and biomass (inoculums) concentrations (10, 20,  
139 30, 40 and 50 g (wet weight) L<sup>-1</sup> of effluent. The effect of trace elements on the removal of NH<sub>3</sub>-  
140 N was determined by adding 2 ml of trace element solution per litre of PIE. Trace element  
141 composition was EDTA (5 g L<sup>-1</sup>), ZnSO<sub>4</sub>.7H<sub>2</sub>O (2.2 g L<sup>-1</sup>), CoCl<sub>2</sub>.6H<sub>2</sub>O (1.6 g L<sup>-1</sup>), MnCl<sub>2</sub>.4H<sub>2</sub>O  
142 (5.1 g L<sup>-1</sup>), CuSO<sub>4</sub>.5H<sub>2</sub>O (1.6 g L<sup>-1</sup>), (NH<sub>4</sub>)<sub>2</sub>Mo<sub>7</sub>O<sub>24</sub> (1.1 g L<sup>-1</sup>), CaCl<sub>2</sub>.2H<sub>2</sub>O (5.5 g L<sup>-1</sup>) and  
143 FeSO<sub>4</sub>.7H<sub>2</sub>O (5 g L<sup>-1</sup>). In addition to the trace elements, the salts such as (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (1 g L<sup>-1</sup>),  
144 KH<sub>2</sub>PO<sub>4</sub> (0.07 g L<sup>-1</sup>) and NaHCO<sub>3</sub> (3 g L<sup>-1</sup>) were added to improve the growth of the *P. penneri*  
145 and thus the removal efficiency of NH<sub>3</sub>-N. Aeration was provided at the rate of 1 L min<sup>-1</sup> and  
146 results were analysed for 96 hours in 24 hours interval. The removal of ammonia was analyzed  
147 by using Kjeldhal method<sup>13</sup> and further the nitrite and nitrate which are formed from the

148 conversion of  $\text{NH}_3\text{-N}$  were analyzed using the colorimetric methods followed by Narayana and  
149 Sunil<sup>14</sup>.

#### 150 2.4. Construction of transposon mutant library

151 A transposon mutant library of *P. penneri* was constructed by using a modified mariner  
152 transposon, pSC189::miniTn(Gm), wherein, the Kan<sup>r</sup> gene in the transposable element was  
153 replaced by a Gm<sup>r</sup> gene (Fig.1), since the wild strain was initially found to be sensitive to  
154 gentamycin.

155 A transposon mutant library of *P. penneri* was constructed by using a modified mariner  
156 transposon, pSC189::miniTn(Gm), which is developed by replacing KanR gene in pSC189 with  
157 GmR gene from pGp-Tn7-Gm. The Gmr gene was PCR amplified with the primer listed in table  
158 1 that introduce the desired restriction sites XhoI and RsrII for further cloning. The PCR  
159 products was digested using XhoI/RsrII restriction enzymes and ligated in pSC189 which is pre-  
160 digested with same enzyme to delete Kmr gene as illustrated in Fig. 1, to give plasmid  
161 pSC::miniTn(Gm). This resultant plasmid is preferred to creating mutant library of *P. Penneri*  
162 since the wild strain was found to be sensitive to gentamycin. The procedure was adapted from  
163 Tn7-based cloning and delivery system developed by Sebastien *et al.*<sup>15</sup> and Neal *et al.*<sup>16</sup> The  
164 cultures with appropriate doses of antibiotics were supplemented at the following concentrations:  
165 Gm, 15 mg ml<sup>-1</sup> (w/v) and Amp, 100 mg ml<sup>-1</sup> (w/v) and they were incubated at 37°C. All the  
166 primers used for vector construction were presented in Table 1. The Gm<sup>r</sup> gene from pGP-Tn7-  
167 Gm was PCR amplified, digested using XhoI/RsrII restriction enzymes and cloned in pSC189  
168 which is pre-digested with same enzyme to delete Km<sup>r</sup> gene as illustrated in Fig. 1, to give  
169 plasmid pSC::miniTn(Gm). The positive clones were further selected on a selective media of LB  
170 supplemented with Amp<sub>50</sub> and Gm<sub>15</sub>.



171 For the conjugal transfer, pSC::miniTn(*Gm*) were further transformed to Mu-free donor  
172 (MFD) cells to act as donor, grown in LB supplemented with 0.3 mM Diaminopimelic acid  
173 (DAP). Conjugation was performed according to the procedure followed by Lionel *et al.*<sup>8</sup> with  
174 little modification as follows: equal volumes of the donor and recipient cells to read optical  
175 density of 1.0 at 600 nm was mixed, centrifuged to collect the pellet and washed twice with LB  
176 broth. The pellet was further suspended in 50 µl of LB broth and spotted on dry LB agar plates to  
177 make tight contact for conjugation. After incubation of plates for 1 hour at 37°C, the cell spot  
178 was harvested and resuspended in fresh LB broth. The transconjugants were further selected on  
179 an LB plate containing Gm<sub>15</sub> by spread plate after overnight incubation at 37°C. The absence of  
180 DAP provided the non selection of MFD donor strain. They were confirmed for the transposon  
181 insertion by colony PCR using R6K primers, which were amplified the R6K origin of replication  
182 located inside the transposable elements. Genomic DNA of the transconjugants was used as the  
183 template for PCR amplification.

#### 184 *2.5. Screening of the mutant with enhanced ammoniacal nitrogen removal*

185 Following mutagenesis, viable mutants were screened for enhanced NH<sub>3</sub>-N removal. The  
186 removal ability of the mutants was verified from reduction profiles of different mutant strains  
187 and compared with wild strain under the optimised conditions. For this purpose, a total of 350  
188 isolates were screened, each of which was inoculated into 1 L of PIE, and incubated for 24 hours  
189 under optimum conditions together with the addition of other trace elements and salts. The  
190 residual NH<sub>3</sub>-N content was determined in the treated effluent by Kjeldhal method.<sup>13</sup> Reduction  
191 profile of each of the mutant strain was plotted and analysed.

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193

194 2.6. Kinetic rate constants for the degradation of  $\text{NH}_3\text{-N}$  by *P. Penneri* wild type and transposan  
195 mutants

196 In order to investigate the kinetic rate constants for the degradation of  $\text{NH}_3\text{-N}$  using *P.*  
197 *penneri*, the non-linear kinetic models were applied. The pseudo first order<sup>17</sup> and pseudo second  
198 order<sup>18</sup> kinetic models were employed, following the equations, Eq. 1 and 2 respectively.

$$199 \quad r_t = r_e(1 - \exp^{-k_1 t}) \quad (1)$$

$$200 \quad r_t = \frac{K_2 r_e^2 t}{1 + K_2 r_e t} \quad (2)$$

201 where  $r_e$  and  $r_t$  are the amounts of  $\text{NH}_3\text{-N}$  (%) degraded at equilibrium and at time ( $t$ ),  $k_1$  and  $k_2$   
202 are the first and second order rate constants.

203 2.7. Fourier transform-infrared spectroscopy (FT-IR) studies

204 A Perkin Elmer infrared spectrometer was used for the investigation of nitrite and nitrate  
205 ions in treated PIE sample. The treated and untreated samples were lyophilized and mixed with  
206 KBr and made into pellets at a pressure of about 1MPa. The pellets with dimensions diameter 10  
207 mm and thickness 1 mm, the samples were scanned in the spectral range of 4000–400  $\text{cm}^{-1}$ .

208 2.8. Quantification of nitrite and nitrate in treated and untreated effluent by colorimetric method  
209 and ion chromatography (IC)

210 The nitrite and nitrate produced from the conversion of  $\text{NH}_3\text{-N}$  by wild and mutant strains  
211 were analyzed using the colorimetric methods followed by Narayana and Sunil<sup>14</sup>. Also, the ion  
212 chromatography was used to confirm the conversion of  $\text{NH}_3\text{-N}$  into nitrite and nitrate ions. The  
213 ion chromatography was performed with Metrohm instrumentation consisting of a 709 IC Pump,  
214 733 IC Separation Centre and a 732 IC conductivity detector. Cation separation was carried out  
215 in non suppressor mode on a Metrosep cation 1-2 analytical column (125 × 4 mm) connected in

216 series with a Metrosep cartridge. The Metrosep cartridge is used as a precolumn to protect the  
217 analytical column. The dilution factor for each of the sample was fixed at 50. Sample injection  
218 volume used was 20  $\mu\text{l}$ . The nitrite and nitrate quantity in  $\text{mg L}^{-1}$  was determined from the peak  
219 area and time in minutes from the chromatogram.

### 220 **3.0. Results and Discussion**

#### 221 *3.1. Isolation and identification of ammonia oxidizing microbial strain*

222 The strain with enhanced ammonia removal was isolated and identified as *Proteus*  
223 *penneri* by the method of ribotyping. The 16S rDNA sequencing data indicated that the isolate  
224 was *P. penneri* (Fig. 2). The nucleotide sequence reported here has been assigned an accession  
225 number “KM000848” from NCBI Gene Bank database. The BLAST result showed 99%  
226 similarities to those of nearest strain *P. penneri* NCTC 12737.  $\text{NH}_3\text{-N}$  analysis by Kjeldhal  
227 method<sup>13</sup> showed that the major reduction was obtained with enriched wild strain of *P. penneri*  
228 wherein it was reported to have an efficient ammonia removal by 64% in 24 hours.

#### 229 *3.2. Optimization of culture conditions for the removal of ammoniacal nitrogen by wild type* 230 *P. penneri*

##### 231 *3.2.1. Effect of time*

232 The effect of time on percentage removal of ammonia by wild type strain was studied and  
233 was observed that longer the incubation time, the better the efficiency of  $\text{NH}_3\text{-N}$  removal and it  
234 was 64% in 24 hours and 74% in 72 hours (Fig. 3a). It was observed that increase in treatment  
235 period beyond 72 hours decreased the removal percentage for the wild strain. Several factors  
236 such as toxicity of the other chemicals presented in the sample or secondary metabolites  
237 produced during the treatment of PIE could be attributed to the decrease in efficiency. Tang *et*  
238 *al.*<sup>19</sup> reported that they achieved around 78% ammonium removal efficiency with the initial

239 effluent  $\text{NH}_3\text{-N}$  concentration 123-257  $\text{mg L}^{-1}$  by the ammonia oxidizers in the anaerobic  
240 ammonium oxidation (ANAMMOX) process. Comparatively, *Proteus penneri* can be considered  
241 as highly efficient strain for the removal of high strength ammoniacal nitrogen containing  
242 wastewater since it showed 74% efficiency with the initial effluent  $\text{NH}_3\text{-N}$  concentration 500  $\text{mg}$   
243  $\text{L}^{-1}$ . To our knowledge, such a high ammoniacal nitrogen removal capacity for pharmaceutical  
244 wastewater has not been previously reported.

### 245 3.2.2. Effect of pH

246 The pH of the culture is one of the most important environmental parameters affecting  
247 microbial cell growth and enzyme production. The effect of initial pH on the  $\text{NH}_3\text{-N}$  removal by  
248 *P. penneri* was investigated for pH values from pH 6 to 9 as shown in Fig. 3b. The maximum  
249 removal of  $\text{NH}_3\text{-N}$  was observed at pH 8. The oxidation of ammonia by nitrifying bacteria  
250 growing in inorganic liquid media generally occurs optimally within the pH range 7.0-8.5.<sup>20, 21</sup>  
251 Also, the most likely mechanism for inhibition of growth in lower pHs are ionization of  $\text{NH}_3$  to  
252  $\text{NH}_4^+$  at low pH and either the lack of an active ammonium transport system.<sup>20</sup>

### 253 3.2.3. Effect of temperature

254 The temperature has greater role in the removal of  $\text{NH}_3\text{-N}$ . The maximum removal of  
255  $\text{NH}_3\text{-N}$  (64%) was observed at 35°C. The efficiency of the  $\text{NH}_3\text{-N}$  removal was not much  
256 affected at 40°C, but at 45°C and 50°C, the removal efficiency was gradually decreased (Fig.3c).  
257 This indicates that the optimum temperature for the removal of  $\text{NH}_3\text{-N}$  by *P. penneri* was 35°C  
258 and the bacterial strain may be regarded as mesophilic in nature.

259

260

#### 261 3.2.4. Effect of biomass concentration

262 The selection of suitable biomass concentration becomes an important parameter to  
263 improve the NH<sub>3</sub>-N removal efficiency since the efficiency is controlled by the number of cells.  
264 Hence, various concentrations of biomass 10 to 50 g L<sup>-1</sup> (w/v) were added to 1 L PIE at pH 8.0.  
265 The results showed that NH<sub>3</sub>-N removal efficiency was achieved by 64% with biomass  
266 concentration of 40 g L<sup>-1</sup> (w/v) and there was no much difference in NH<sub>3</sub>-N removal efficiency  
267 for increase in biomass concentrations beyond 40 g L<sup>-1</sup>. This infers that 40 g L<sup>-1</sup> of biomass was  
268 required to provide the maximum removal of NH<sub>3</sub>-N in 1 L of PIE (Fig.3d).

#### 269 3.3. Construction of pSC189::miniTn(Gm)

270 In the present study, pSC189 was chosen to be the suitable transposon delivery vector for  
271 *P. penneri*, as they are non-replicative plasmid with R6K origin of replication and hence  
272 replicate only in those system which encodes the λ-pir protein<sup>8</sup>. The wild stain *P. penneri* was  
273 observed to be sensitive to gentamycin and resistant to kanamycin, and thus more versatile  
274 vector was developed in the present investigation by replacing the kanamycin resistant gene with  
275 gentamycin resistant gene (Supplementary file-Fig.1). As suggested by Lionel *et al.*<sup>8</sup> and Chiho  
276 *et al.*<sup>22</sup> the replication of these plasmids requires the pir-encoded protein, which is usually  
277 provided in trans in the donor strain. In the absence of pir site in the recipient strain, these  
278 plasmids cannot replicate.

279 For the conjugal transfer, pSC189::miniTn(Gm) were further transformed to MFD λ-pir  
280 donor strain. After conjugation with *P. penneri*, the transconjugants were selected on LB with  
281 gentamycin in the absence of DAP. The donor MFD λ-pir cells will not survive since it requires  
282 the supplementation of DAP, rather transconjugants alone will survive on the gentamycin plate.

283 The transconjugants were confirmed by PCR amplification of R6K origin of vector backbone  
284 (supplementary file-fig.6).

### 285 *3.4. Screening of the mutant with enhanced ammonia removal*

286 About 350 mutant colonies were screened from transposon mutant library. The NH<sub>3</sub>-N  
287 removing mutants were screened by inoculating the mutants in the PIE while the wild type strain  
288 served as control. Of which, 2 mutants (T<sub>55</sub> and T<sub>132</sub>) showed enhanced removal of NH<sub>3</sub>-N  
289 compared to other mutants. NH<sub>3</sub>-N content was estimated for the mutated strains under the  
290 optimized conditions and was found to be 84% and 81% in 24 hours for the transposon mutants  
291 T<sub>55</sub> and T<sub>132</sub> respectively. Since the T<sub>55</sub> mutant strain showed higher efficiency when compared  
292 to T<sub>132</sub>, the T<sub>55</sub> was selected for the further study. The mutant T<sub>55</sub> was proved to have an  
293 improved efficiency of NH<sub>3</sub>-N removal as they showed a high removal efficiency of 84% within  
294 24 hours and 89, 95 and 97% in 48, 72 and 96 hours respectively, whereas the wild type strain  
295 removed NH<sub>3</sub>-N by only 64% in 24 hours and 70% in 96 hours. This indicates that, the  
296 *P. penneri* transposon mutant was an inevitable source for the enhancement of the NH<sub>3</sub>-N  
297 removal. The stability of the transposon mutant strain, T<sub>55</sub> was confirmed even after five  
298 subcultures in non-selective media.

### 299 *3.5. Hydrolysis rate kinetic constants*

300 The validity of the kinetic order of degradation process was based on the regression  
301 coefficients. The first order rate constant  $k_1$  and the second order rate constant  $k_2$  are summarized  
302 in Table 2. The results confirmed that the degradation of NH<sub>3</sub>-N obeyed the second order rate  
303 kinetic model as observed greater R<sup>2</sup> values.

304

305 *3.6. Characterization of the treated sample using FT-IR studies*

306 The FT-IR spectrum of untreated effluent (Fig. 4a) has a wide band at  $3432.71\text{ cm}^{-1}$ , due  
307 to the  $1^\circ$  and  $2^\circ$  amines - stretching vibrations caused due to the presence of ammonium ions  
308 present in industrial effluent. The peak observed at  $2358.3\text{ cm}^{-1}$  is attributed to  $\text{NH}_2$  scissoring  
309 ( $1^\circ$  amines) – bending vibrations and the peak observed at  $1083.637\text{ cm}^{-1}$  are due to C–N  
310 stretching vibrations.

311 The FT-IR spectrum of the PIE treated with wild –type strain (Fig. 4b) shows the peak at  
312  $1398.11\text{ cm}^{-1}$  suggest the presence of aliphatic NO groups and the peaks at  $1666.71\text{ cm}^{-1}$  is due  
313 to the asymmetrical stretching in  $\text{NO}_2$ . The bands at  $834.50\text{ cm}^{-1}$  and  $703.48\text{ cm}^{-1}$  could be  
314 attributed to stretching of  $\pi$  bond of N-O linkage and the presence of  $\text{NO}_2$  bending vibrations.

315 The spectral data of various peaks corresponding to the PIE sample treated with  
316 transposon mutant  $T_{55}$  (Fig. 4c) indicated that the peaks at  $1634.43\text{ cm}^{-1}$  and  $788.964\text{ cm}^{-1}$   
317 correspond to  $\text{NH}_2$  scissoring ( $1^\circ$  amines) – bending vibrations and  $\text{NH}_2$  and NH wagging  
318 respectively. The peak at  $1402.134\text{ cm}^{-1}$  indicates the presence of aliphatic NO groups and peak  
319 at  $788.964\text{ cm}^{-1}$  indicated  $\text{NO}_2$  bending vibrations.

320 Therefore, it is observed that the intensity of the  $1^\circ$  and  $2^\circ$  amines stretching vibrations,  
321 caused due to the presence of ammonium ions, has decreased in the treated effluent when  
322 compared to the untreated sample. Hence, it can be validated that the presence of various nitro  
323 (nitrite and nitrate) groups in the treated sample indicates that the major removal of  $\text{NH}_3\text{-N}$  has  
324 occurred through the conversion of amine groups to nitro groups.

325

326 3.7. Nitrite and nitrate determination in the treated and untreated effluent by colorimetric  
327 method and ion chromatography (IC)

328 The treated PIE sample (24 hours sample) by wild type and mutant strains were subjected  
329 to nitrite and nitrate analysis by colorimetric methods, it shows the nitrite and nitrate production  
330 were enhanced in the treated PIE sample by the mutant strain compared to wild type strain. The  
331 treated PIE by wild type strain contains around 12.6 mg L<sup>-1</sup> of the nitrite and 4.8 mg L<sup>-1</sup> of the  
332 nitrate and the treated PIE by mutant strain contains around 61 mg L<sup>-1</sup> of the nitrite and 26 mg L<sup>-1</sup>  
333 of the nitrate. This was further confirmed with ion chromatography.

334 Ion chromatogram was collected to determine the quantity of nitrite and nitrate ions  
335 present in the treated and untreated PIE sample (Figure not shown). The data obtained from the  
336 chromatogram validates that the quantity of nitrite present in the untreated PIE sample was 23.7  
337 mg L<sup>-1</sup> and the nitrite present in the PIE sample treated with wild type strain *P. penneri* was 26.2  
338 mg L<sup>-1</sup>. This shows that 9.5% conversion of NH<sub>3</sub>-N to nitrite ions has occurred during the  
339 treatment process with the wild strain in 24 hours under optimized conditions. The treatment  
340 efficiency of the transposon treated sample shows a major conversion of 56.7% as nitrite present  
341 in the transposon treated effluent has increased from 23.7 mg L<sup>-1</sup> to 54.8 mg L<sup>-1</sup>. Around 23.6%  
342 nitrate was observed in the transposon treated sample while it is 5.2% in the wild type treated  
343 sample.

344 Therefore, it is inferred that major removal of NH<sub>3</sub>-N was caused due to the conversion to  
345 nitrite ions and a minor conversion to nitrate ions. Hence, it is studied that the *amoA* gene which  
346 is responsible for the expression of ammonia monooxygenase, which is the first enzyme involved  
347 in the conversion of ammonia<sup>23</sup> to nitrite plays a key role in the process of NH<sub>3</sub>-N removal from  
348 the effluent sample. This is corroborated with the findings of Zhi *et al.*<sup>24</sup> and also with Zhi and



349 Ji<sup>25</sup>. They reported that the ammoniacal nitrogen removal is collectively controlled by amoA and  
350 nxrA gene.

#### 351 4. Conclusion

352 In this study, the *P.penneri* was isolated and enriched in the PIE for the NH<sub>3</sub>-N removal.  
353 The wild strain showed only 64% and 74% NH<sub>3</sub>-N removal in 24 and 72 hours respectively. The  
354 strain improvement was done for the purpose of industrial applications by reducing the reaction  
355 time and increasing the efficiency of the strain by constructing a mutagenesis library of  
356 *P. penneri* by the method of transposon mutagenesis. A series of mutant strains were developed  
357 for the purpose enhanced removal of NH<sub>3</sub>-N in PIE. NH<sub>3</sub>-N removing mutant strains T<sub>55</sub> and T<sub>132</sub>  
358 were acquired from the transposon mutation bank, which exhibited increased NH<sub>3</sub>-N removal  
359 than the wild strain under the optimized conditions and in short duration (24 hours). The selected  
360 mutant strain T<sub>55</sub> were found versatile for the removal of NH<sub>3</sub>-N by 84% in 24 hours. Hence,  
361 random mutagenesis was found to be an efficient method for the strain improvement to enhance  
362 the removal of NH<sub>3</sub>-N in the pharmaceutical industrial effluent. The study has wide applications  
363 for the treatment of high strength NH<sub>3</sub>-N containing pharmaceutical wastewater.

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**Figure Legends**

417 **Fig.1.** Schematic representation of construction of pSC189::miniTn(Gm)

418 **Fig.2.** Maximum likelihood phylogenetic tree of *Proteus penneri* with other closely related  
419 species on 16S rDNA sequences. Numbers in the nodes are the bootstrap values from  
420 1000 replicates.

421 **Fig.3.** Effect of (a) time, (b) pH and (c) temperature and, (d) biomass concentration on  
422  $\text{NH}_3\text{-N}$  removal

423 **Fig.4.** FT-IR spectroscopy of (a) untreated sample, (b) effluent treated with wild strain, and  
424 (c) effluent treated with T<sub>55</sub> mutant strain

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**Table Legends**

427 **Table 1:** Primers used in this study

428 **Table 2.** Kinetic rate constants for the degradation of  $\text{NH}_3\text{-N}$

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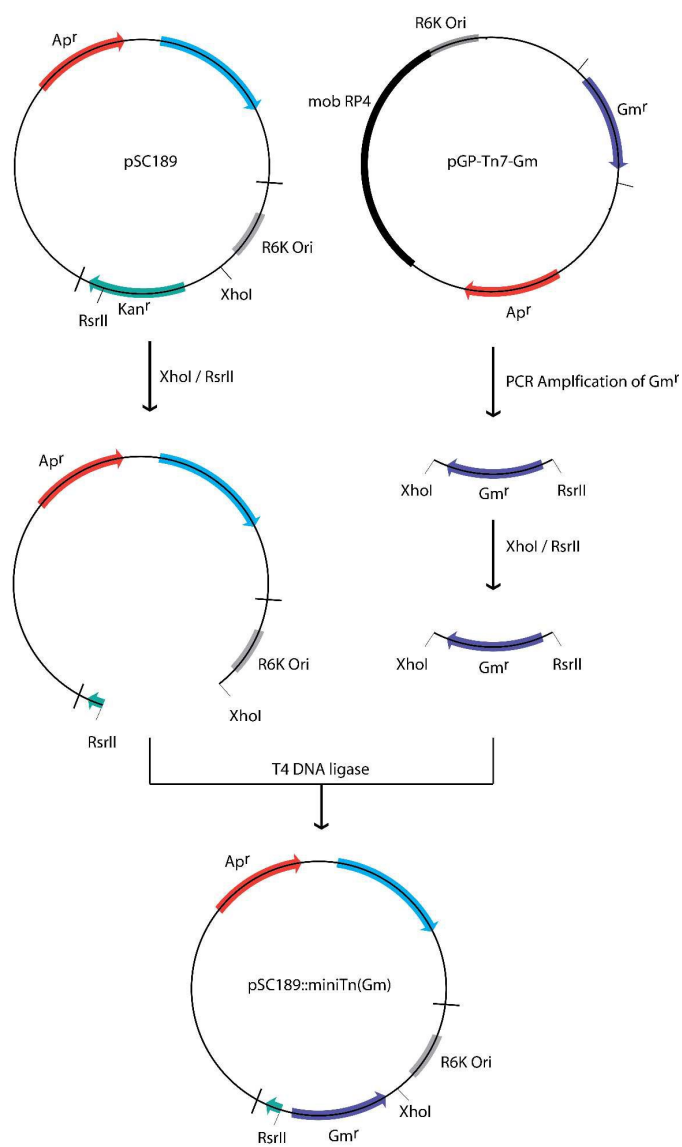
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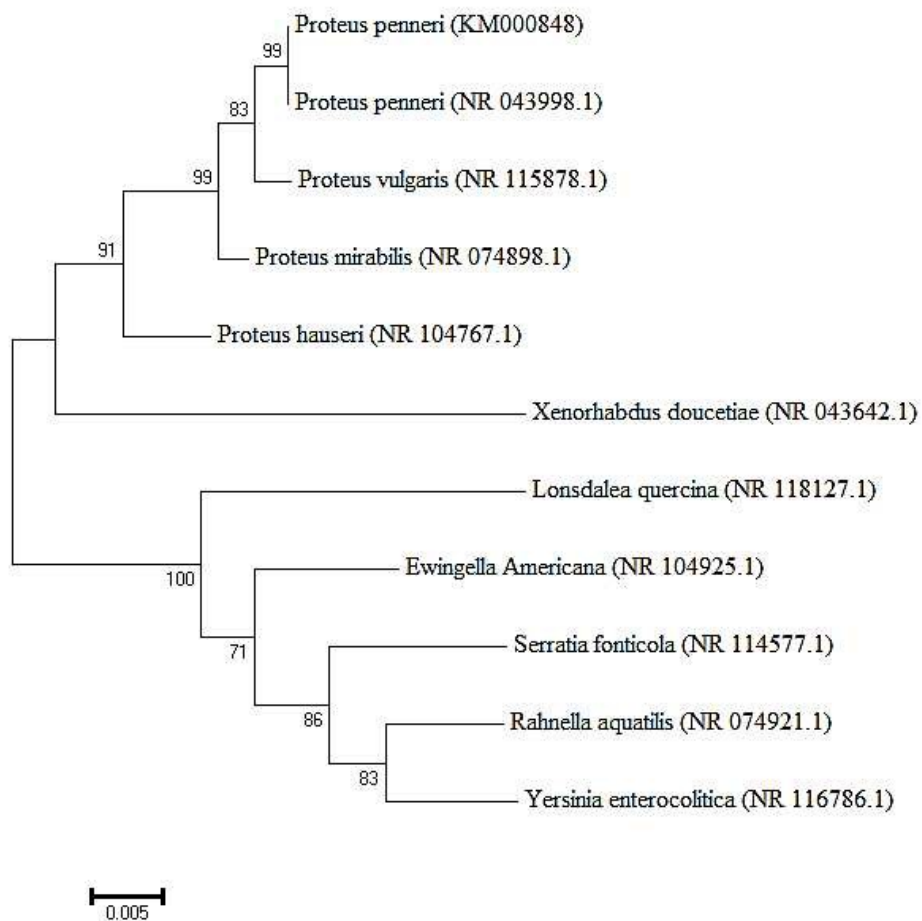
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**Fig. 1. Schematic representation of construction of pSC189::miniTn(Gm)**



**Fig 2. Maximum likelihood phylogenetic tree of *Proteus penneri* with other closely related species on 16S rDNA sequences. Numbers in the nodes are the bootstrap values from 1000 replicates.**

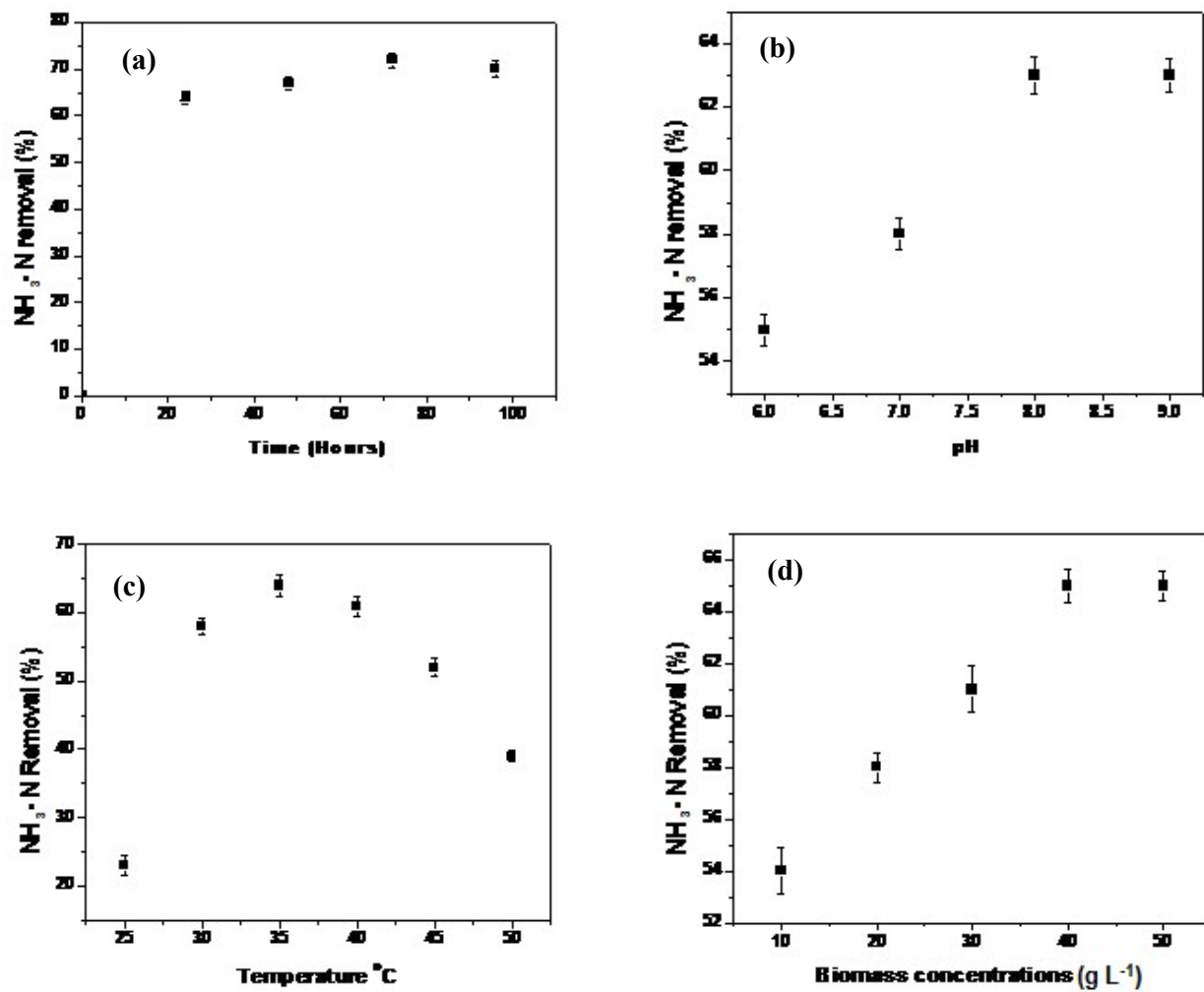


Fig. 3. Effect of (a) time, (b) pH, (c) temperature and, (d) biomass concentration on  $\text{NH}_3\text{-N}$  removal

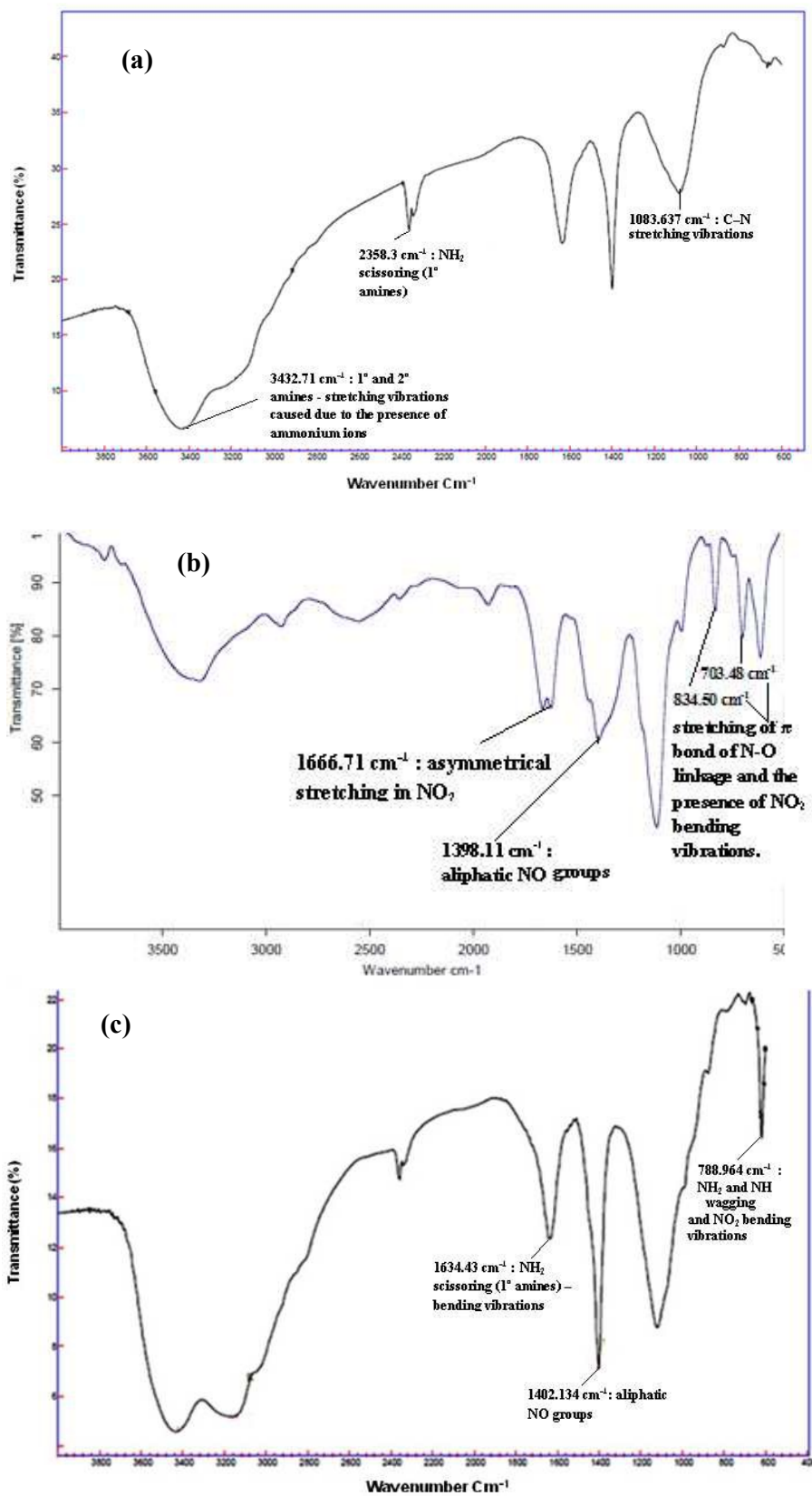


Fig. 4. FT-IR spectroscopy of (a) untreated sample, (b) effluent treated with wild strain, and (c) effluent treated with T<sub>55</sub> mutant strain



**Table 1: Primers used in this study**

<b>Name of the primers</b>	<b>Sequence(5' to 3')</b>	<b>Function</b>
Gm F	CGGWCCGGAATTGTTAGGTGGCGGTACTTGG	Amplification of Gm <sup>r</sup> gene from pGP-Tn7-Gm
Gm R	GAGCTCATGCATGATATCGTCCG CTCGAG	
R6K F	GCCGCTCTAGACCCCTATAGTGAGTC	Amplification of the R6K origin of replication site for the confirmation of transposon integration in the genome
R6K R	GAATTCCTGCACCCTTAATTAACCCCG	

Table 2. Kinetic rate constants for the degradation of NH<sub>3</sub>-N

Microbial strain	Pseudo first order		Pseudo second order	
	$k_1$ (h <sup>-1</sup> )	$R^2$	$k_2$ (mg/L/h)	$R^2$
<i>P. penneri</i> (wild type)	0.028	0.966	$2.56 \times 10^{-3}$	0.999
Transposan mutant	0.039	0.928	$1.75 \times 10^{-3}$	0.999

## Graphical Abstract

