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Magnetic Starch Nanocomposite as a Green Heterogeneous Support for				
Immobilization of Large Amounts of Copper Ions: Heterogeneous Catalyst	2			
for Click Synthesis of 1,2,3-triazoles	3			
Ali Pourjavadi*, Anahita Motamedi, Seyed Hassan Hosseini, Mojtaba Nazari	4			
Polymer Research Laboratory, Department of Chemistry, Sharif University of Technology, Tehran, Iran	5			

E-mail address: purjavad@sharif.edu; Phone/fax: (982)166165311

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Abstract

A new magnetic heterogeneous copper catalyst was prepared by immobilization of copper 10 ions onto a cross-linked polymeric nanocomposite composed of starch grafted 11 polyacrylamide and functionalized Fe₃O₄ magnetic nanoparticles. The resulting support was 12 loaded with large amounts of copper ions (1.6 mmol g^{-1}). The prepared catalyst is highly 13 active in Huisgen 1,3-dipolar cycloaddition reaction of different azides and alkynes at low 14 catalyst amount. Various corresponding 1,2,3-triazoles were produced with high yields in 15 mild condition. The catalyst was easily recovered and reused for ten cycles of reaction and no 16 significant loss of catalytic activity was observed. 17

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Keywords: Huisgen cycloaddition, copper catalysis, magnetic nanoparticles, polymeric22supports, green catalytic system23

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Introduction

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The concept of click chemistry, first introduced by Sharpless *et al.*, refers to the reactions that are modular, wide in scope and highly efficient, performing with high regio- and sterio-selectivity under mild conditions.¹ In recent years, these kinds of reactions have attracted much attention in different fields of organic chemistry, material science and drug discovery.²⁻ ⁴ The most well-known example of click reactions is catalytic 1,3-dipolar cycloaddition of organic alkynes and azides.^{5,6} This reaction is very attractive since it can be used for synthesis of 1,2,3-triazole derivatives, a class of compounds that have been recognized possessing biological and pharmaceutical activities.^{7,8}

However the original non-catalyzed form of this reaction, known as Huisgen cycloaddition 36 reaction, has slow rate and low yield at room temperature due to high kinetic energy barrier 37 of the reaction.^{9,10} It has been recognized that Cu(I) is an appropriate catalyst for Huisgen 38 reaction since it accelerates the rate of the reaction and significantly improves its 39 regioselectivity.^{11,12} Although both homogeneous and heterogeneous catalysts were used in 40 this reaction, heterogeneous catalysts have more advantages than homogenous ones, because 41 of facile separation and reusability of the catalyst and simple isolation of the product.¹³⁻¹⁶ 42 These properties are especially very important for pharmaceutical purposes since it is 43 essential to remove trace amount of catalysts remained in the final product. Moreover, in 44 drugs synthesis process the supported materials, used for immobilization of copper, should be 45 biocompatible to prevent the possible leached contamination from solid catalysts to final 46 products. 47

A variety of heterogeneous catalytic systems were prepared by immobilization of copper ions 48 onto different solid supports such as magnetic nanoparticles,¹⁷ silica,¹⁸ zeolite,¹⁹ alumina,²⁰ 49 and polymers²¹, and were used for click synthesis of 1,2,3-triazoles. In these systems, the 50

catalyst can be separated from the reaction medium by simple filtration or centrifugation. 51 However, using magnetic nanoparticles makes separation and recovery of the catalyst faster 52 and more convenient in comparison with non-magnetic catalysts. The catalyst can be easily 53 removed after the completion of the reaction by using a magnet.²²⁻²⁴ 54

In spite of the great advantageous of heterogeneous catalytic systems, loading amounts of the 55 active spices (copper ions) in these systems is usually low and thus a large amount of solid 56 catalyst is required to perform the reaction. This resulted to using large amounts of solvent 57 for reaction mixing and catalyst separation. Plus, increasing in the amount of used catalyst 58 leads to an increase in the contamination of final products. In many cases, the activity of the 59 catalyst also decreases after immobilization on solid supports. High catalyst leaching and low 60 thermal stability of the catalyst are other drawbacks of heterogeneous catalytic systems. As a 61 consequence, it is still demanded to develop an efficient heterogeneous catalytic system with 62 high loading, high stability and easy separation. 63

Polymeric materials with different structures, compositions and functionalities have been 64 prepared and employed as supports in heterogeneous catalytic systems.²⁵⁻²⁷ However, natural 65 polymers, especially polysaccharides, are more attractive since they are easily available, 66 inexpensive, nontoxic, and biodegradable.²⁸⁻³⁰ There are also many functional groups in the 67 structure of natural polymers being able to interact with metal ions and nanoparticles. These 68 properties make polysaccharides and other natural polymers excellent candidates for being 69 used as supports in heterogeneous catalytic systems. 70

Herein, we report preparation of copper immobilized magnetic starch-based heterogeneous 71 catalytic system for 1,4-disubstituted 1,2,3-triazols. The catalyst is easily prepared by 72 simultaneous polymerization, grafting and crosslinking of acrylamide onto the starch in the 73 presence of magnetic nanoparticles. 74

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Experimental

Materials

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Acrylamide was purified by recrystallization in methanol. Starch, tetraethylorthosilicate 79 (TEOS), 3-(trimethoxysilyl) propylmethacrylate (MPS), sodium ascorbate, sodium azide 80 N_N - (NaN_3) , FeCl₂.4H₂O, FeCl₃.6H₂O, ammonium persulfate (APS), 81 methylenebisacrylamide (MBA), CuCl₂, ammonia solution (25%) and ethanol all were 82 obtained from Merck and Aldrich and used without further purification. 83 Fourier transform infrared (FTIR) spectra were recorded on ABB Bomem MB 100 84 spectrophotometer. X-ray diffraction (XRD) patterns were obtained by a Siemens D5000 85 diffractometer with Cu K_{α} radiation in 2 θ range of 5-80°. Scanning electron microscopy 86 (SEM) images were taken on Mira3 Tescan microscope. Thermogravimetric analysis (TGA) 87

was performed at heating rate of 10 °C under nitrogen atmosphere using Perkin-Elmer Pyris1 88 instrument. Transmission electron microscopy (TEM) experiments were carried out by a 89 Philips CM30 electron microscope. Nuclear magnetic resonance (NMR) spectra were 90 recorded on Bruker (Avance DRX-400) spectrometer using CDCl₃ as solvent and 91 tetramethylsilane (TMS) as internal standard. The magnetic properties of samples were 92 measured with a vibrating sample magnetometer (VSM, PPMS-9T) in Kashan University, 93 Iran. 94

Synthesis of MPS functionalized silica-coated Fe₃O₄ nanoparticles (MNPs)

 Fe_3O_4 magnetic nanoparticles were prepared by coprecipitation of Fe (II) and Fe (III) salts. 97 Typically, 200 mL distilled water was poured in a round-bottom flask equipped with a 98 mechanical stirrer. 5 mmol (1.0 g) FeCl₂.4H₂O and 10 mmol (2.7 g) FeCl₃.6H₂O were added 99 and stirred to dissolve. Then, ammonia solution was added to the flask dropwise until the pH 100

of the solution reached to 10. The mixture was stirred vigorously at 60 °C for 1 h. The black 101 precipitate was collected by a magnet and washed with water ($5 \times 50 \text{ mL}$) and dried at 60 °C. 102 In order to prepare silica-coated Fe_3O_4 nanoparticles, 1.0 g of the prepared magnetic 103 nanoparticles were dispersed in 80 mL 4:1 ethanol/water solution in a round-bottom flask and 104 sonicated for 20 min. Then, 0.5 mL tetraethylorthosilicate (TEOS) was added and the pH of 105 the solution was adjusted to 10 using ammonia solution. The mixture was refluxed for 12 h. 106 Afterward, the flask was cooled to room temperature and the resulting particles were washed 107 with water $(3 \times 50 \text{ mL})$ and ethanol $(2 \times 25 \text{ mL})$ and dried in an oven at 60 °C. 108

 $Fe_3O_4@SiO_2$ nanoparticles were then functionalized with MPS using the same procedure 109 mentioned above for synthesis of $Fe_3O_4@SiO_2$. 0.7 g $Fe_3O_4@SiO_2$, 3 mL MPS and 1 mL 110 ammonia were refluxed in 100 mL 4:1 ethanol/water solution. After 12 h, the prepared 111 particles were washed with water (3×20 mL) and ethanol (2×20 mL) and dried at 60 °C 112 (MNPs). 113

Preparation of the catalyst (MNP@SPAAm/Cu)

Magnetic polymeric support was prepared according to the following procedure: 0.5 g MNPs 115 were dispersed in 20 mL water in a round-bottom flask and sonicated for 20 min. Then, 0.5 g 116 starch was added to flask. After all starch was dissolved, 0.05 g APS was added to solution 117 and mixture was put in an oil bath at 70 °C. Then, a mixture of 2.0 g acrylamide and 0.4 g 118 MBA in 10 mL water was added to flask and polymerization was performed for 1 h. The 119 prepared hydrogels were washed with ethanol, dried at 50 °C and sieved through an 80-mesh 120 sieve for further use. 121

For loading of copper, 0.5 g of the prepared polymeric nanocomposite was added to an 122 aqueous solution of $CuCl_2$ (0.3 g in 25 mL). The mixture was stirred for 24 h at 50 °C and the 123 solid particles were then magnetically separated, washed with water (5×25 mL) and ethanol 124 (2×25 mL) and dried at 60 °C. 125

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126 Alkyne (1 mmol), alkyl halide (1 mmol) and NaN_3 (1.3 mmol) were added to 3 mL water in a 127 round-bottom flask. 3.1 mg of the prepared catalyst and 0.02 g sodium ascorbate (10 mol%) 128 were added and the flask content was stirred at room temperature. The completion of the 129 reaction was monitored by thin layer chromatography (TLC). After completion of the 130 reaction, the catalyst was separated magnetically and the flask content was extracted with 131 ethyl acetate. The catalyst was washed with ethanol three times and dried at 60 °C and used 132 for next runs. All the products are known compounds and the spectral data and melting points 133 were identical to those reported in the literature.¹⁷⁻²⁴ 134 135 **Results and discussion** 136 **Preparation of the Catalyst** 137 The heterogeneous catalyst was prepared by immobilization of Cu (II) ions in the structure of 138 cross-linked solid polymeric nanocomposite. The polymeric support was prepared by 139 simultaneous polymerization, grafting and cross-linking of acrylamide onto starch as a 140 biodegradable backbone. Using starch makes the prepared catalyst more biodegradable and 141 environmentally friendly. The polymerization was performed in the presence of APS as 142 initiator and MBA as cross-linking agent. While cross-linking polymerization was performed, 143 MNPs were entrapped into the polymeric matrix. The presence of acrylate groups on the 144 surface of MNPs causes the covalent attachment of MNPs to polymer. Moreover, acrylate 145 functionalized MNP acts as a second cross-linker and improves the stability of solid support. 146 The presence of magnetic nanoparticles into the polymeric support facilitates the separation 147 and recyclability of the catalyst. The copper ions were then loaded onto the surface of 148 magnetic nanocomposite by complexiton with numerous amide groups of MNP@SPAAm. 149

General procedure for synthesis of 1,2,3-triazoles

This leads to high loading and low leaching of copper ions in the prepared catalyst. The150synthetic route of the prepared catalyst is illustrated in Fig. 1.151



Fig. 1 The synthetic route of MNP@SPAAm/Cu catalyst.

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Characterization

FTIR spectra of Fe_3O_4 , $Fe_3O_4@SiO_2$, $Fe_3O_4@SiO_2@MPS$ and MNP@SPAAm are shown in 157 Fig. 2. The peak appeared at 570 cm⁻¹ is characteristic peak of Fe-O stretching vibrations of 158 Fe_3O_4 . The strong peak appeared at 1100 cm⁻¹ is attributed to Si-O stretching vibrations of 159 silica layer coated on Fe_3O_4 . In the spectrum of $Fe_3O_4@SiO_2@MPS$ (Fig. 1c), the extra weak 160 peak appeared at 1725 cm⁻¹ is related to C=O stretching band and confirms that MPS was 161 successfully coated onto $Fe_3O_4@SiO_2$ nanoparticles. The peaks appeared in the spectrum of 162 MNP@SPAAm are due to different functional groups present in the structure of starch and 163

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polyamide. The peaks appeared at 3500, 2950 and 1670 cm⁻¹ are related to O-H, C-H and C=O amide stretching bands of polymer matrix, respectively. 165

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Fig. 2 FTIR spectra of $Fe_3O_4(a)$, $Fe_3O_4(a)SiO_2(b)$, $Fe_3O_4(a)SiO_2(a)MPS(c)$ and MNP(a)SPAAm(d). 168

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Fig. 3a shows the TEM image of Fe_3O_4 nanoparticle, synthesized by coprecipitation method 170 with size of 5-9 nm. These sizes of MNPs are suitable for catalytic application, due to high 171 magnetization and fast separation. The TEM image of MNP@SPAAm/Cu (Fig. 3b) shows 172 that magnetic nanoparticles (dark spots) are well-dispersed in the polymeric matrix (gray 173 shell). The SEM image of MNP@SPAAm/Cu (Fig. 3c) also shows that the prepared particles 174 have semispherical morphology with rough surface. Such rough structure of the catalyst 175 increases surface area of catalyst and improves its catalytic activity. The presence of copper 176



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Fig. 3 HRTEM images of Fe₃O₄ (a) and MNP@SPAAm/Cu (b) and SEM (c) image and EDX analysis181(d) of MNP@SPAAm/Cu.182

The loading of copper on the surface of support was calculated using ICP-OES and the value 184 of 1.6 mmol g⁻¹ was obtained. The high loading of copper obtained here is due to the 185 polymeric nature of support surface with large chelating groups on the surface of support. 186 The loading level of catalytically active species on the surface of solid supports is an 187 important feature of catalysts since high loadings reduce weight percent of catalyst required 188 for the reaction. This feature is especially more prominent for large scale applications. 189 The XRD pattern of MNP@SPAAm/Cu is shown in Fig 4. Six peaks appeared at 2θ values 190 about 30, 36, 43, 53, 57, and 62° are characteristic peaks of Fe₃O₄ particles, indicating the 191

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crystalline phase of Fe_3O_4 nanoparticles did not changed during the catalyst preparation. The broad peak at 20 range of 20-30° is related to amorphous silica layer in MNPs. 193

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Fig. 4 XRD pattern of MNP@SPAAm/Cu.

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Magnetic properties of bare Fe₃O₄ and MNP@SPAAm/Cu were investigated by VSM and 198 the related magnetization curves are depicted in Fig. 5. It is observed that magnetic hysteresis 199 loop of both samples exhibits superparamagnetic characteristic at room temperature. 200 Saturation magnetizations of MNPs and MNP@SPAAm/Cu are 64 and 22 emu g⁻¹, 201 respectively. Although saturation magnetization decreases after embedment of MNPs into the 202 structure of polymeric network, it is still high enough to be readily separated by an external 203 magnetic field. 204



Fig. 5 Magnetization curve of MNPs (a) and MNP@SPAAm/Cu (b).

TGA curves of Fe₃O₄@SiO₂, Fe₃O₄@SiO₂@MPS, pure starch and MNP@SPAAm/Cu are 208 shown in Fig. 6a-d. The weight loss observed at about 100 °C in all curves is related to 209 removal of physically adsorbed water molecules. The weight loss occurred at 250-450 °C in 210 TGA curve of Fe₃O₄@SiO₂@MPS is due to degradation of propylmethacrylate groups 211 grafted onto Fe₃O₄@SiO₂. The main thermal degradation of pure starch occurs at 200 °C and 212 about 90 wt% of starch is degraded up to 700 °C. TGA curve of MNP@SPAAm/Cu shows a 213 two-step degradation behavior, the first of which occurs at 250 °C and is related to 214 degradation of starch. The second degradation step of MNP@SPAM/Cu starts at 320 °C and 215 about 40 wt% of the sample is lost in this step due to decomposition of grafted 216 polyacrylamide. 217

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Fig. 6 TGA curves of Fe₃O₄@SiO₂ (a), Fe₃O₄@SiO₂@MPS (b), pure starch (c) and

MNP@SPAAm/Cu (d).

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Catalytic performance of MNP@SPAAm/Cu

The catalytic activity of the prepared catalyst in multicomponent cycloaddition of alkyl 224 halides, sodium azide and terminal alkynes was then examined. The reaction of phenyl 225 acetylene, benzyl bromide and sodium azide was chosen as the control reaction and the effect 226 of different experimental conditions on yield of the reaction was investigated. 227 The results of optimization experiments are listed in Table 1. It can be seen that in the 228 absence of any catalyst, no significant amount of product was obtained even at 70 °C (Entries 229 1,2). The same result was observed in the case of using just MNPs or MNP@SPAAm, and 230 the reaction yield was very low, indicating MNPs and MNP@SPAAm do not have any 231 catalytic activity in this reaction (Entries 3,4). In the presence of 5 mg (0.8 mol%) of 232 MNP@SPAAm/Cu, the reaction yield was increased to 99% in 30 min at 50 °C (Entry 5). 233 However, the reaction was slower at room temperature and only 80% yield was obtained after 234

2 h (Entry 6). Completion of the reaction at room temperature required longer times up to 8 h 235 (Entry 7). The effect of the amount of the catalyst on yield of the reaction was also 236 investigated. Decreasing the amount of MNP@SPAAm/Cu to 0.5 mol% did not change the 237 yield of the reaction (Entry 8). However, further decreasing of the amount of 238 MNP@SPAAm/Cu to 0.3 and 0.1 mol% reduced rate of the reaction, and only 73 and 66% 239 yield were obtained after 1 h (Entries 9,10). Thus, 0.5 mol% was chosen as the optimum 240 amount of MNP@SPAAmCu. In other experiments, the reaction performed in the presence 241 of small amounts of catalyst and the results showed that in longer reaction times only 0.01 242 mol% of catalyst gave 89% yield (Entries 11,12). The reaction was also performed in 243 different solvents such as H₂O/t-BuOH (3:1), t-BuOH, CH₃CN, CH₃OH and toluene (Entries 244 13-17). However, the best result was obtained in pure water or water/alcohol mixture due to 245 NaN_3 dissolves in water. Based on the results obtained here, the reaction of alkyl halides, 246 sodium azide and alkynes in H₂O at 50 °C in the presence of 0.5 mol% MNP@SPAAm/Cu 247 was considered as optimum experimental condition for further experiments. 248

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	Ph Br + NaN ₃	+ Ph-=H	MNP@SP/	AAm/Cu	h N-N N N	
				Sondate	Ph	
Entry	Catalyst	Cat. Amount	Т	Time	Solvent	Yield
		(mol%)	(°C)	(h)		(%) ^b
1	-	-	50	7	H_2O	-
2	-	-	70	8	H_2O	12
3	MNPs	100 mg	50	7	H_2O	$27^{\rm c}$
4	MNP@SPAAm	100 mg	50	7	H_2O	7
5	MNP@SPAAm/Cu	0.8	50	0.5	H_2O	99
6	MNP@SPAAm/Cu	0.8	r.t	2	H_2O	80
7	MNP@SPAAm/Cu	0.8	r.t	8	H_2O	97
8	MNP@SPAAm/Cu	0.5	50	0.5	H_2O	99
9	MNP@SPAAm/Cu	0.3	50	1	H_2O	73
10	MNP@SPAAm/Cu	0.1	50	1	H_2O	66
11	MNP@SPAAm/Cu	0.1	50	10	H_2O	94
12	MNP@SPAAm/Cu	0.01	50	24	H_2O	89
13	MNP@SPAAm/Cu	0.5	50	0.5	H ₂ O/t-BuOH	99
14	MNP@SPAAm/Cu	0.5	50	1	t-BuOH	46
15	MNP@SPAAm/Cu	0.5	50	1	CH ₃ CN	32
16	MNP@SPAAm/Cu	0.5	50	2	CH ₃ OH	68
17	MNP@SPAAm/Cu	0.5	50	3	Toluene	10

Table 1 Optimization of the reaction conditions for the synthesis of 1,4-disubstituted 1,2,3-triazoles^a

^a Reaction condition: Phenyl acetylene (1 mmol), benzyl bromide (1 mmol), sodium azide (1.3 mmol), sodium ascorbate (10 mol%), solvent (2 ml).

^b Isolated yield

^c A mixture of isomers.

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The activity of the catalyst in multicomponent cycloaddition reaction of sodium azide and 259 various alkyl halides and alkynes were then investigated using optimized experimental 260 conditions obtained previously. The structure of the alkyl halides and alkynes used as 261 substrates and the results of the experiments are shown in Table 2. All reactions were 262 proceeded easily and the corresponding 1,2,3-triazoles were produced with satisfactory 263 yields. The results show that the prepared catalyst is very efficient in synthesis of various 264 1,2,3-triazole compounds. 265

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Table 2 Cycloaddition reaction of different alkyl halides and alkynes catalyzed with MNP@SPAAm/Cu^a.

^a Reaction condition: alkyl halide (1 mmol), NaN₃ (1.3 mmol), alkyne (1 mmol), H₂O (2 mL). ^bIsolated yield.

Reusability of the catalyst

Reusability is an important feature of the catalyst which should be examined in catalytic 271 reactions. The reaction of phenyl acetylene, benzyl bromide and sodium azide was chosen as 272 model reaction and the reusability of MNP@SPAAm/Cu in this reaction was tested. After 273 completion of the reaction, the catalyst was readily separated by using a magnet, washed with 274 ethanol (2×25 mL) and dried at 50 °C and used for next run. This process was repeated for 275 ten runs of reactions and the results are shown in Fig. 7. It can be seen that high yields of the 276 reactions were obtained even after ten cycles of reaction. However, the time required for 277 completion of the reaction was slightly increased. It is also observed that turnover number 278 (TON) of the catalyst did not changed significantly. However, turnover frequency (TOF) of 279

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the catalyst decreased after 6 cycles which resulted from increasing in reaction times. It is notable, that the increasing of the reaction time is attributed to loss of catalyst mass during the separation process. High catalytic activity and high loading of the catalyst along with simple separation, recyclability and reusability of MNP@SPAAm/Cu make it cost effective and environmentally friendly.

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Fig. 7 Recycling experiment.

The structure of the recycled catalyst was investigated by FTIR spectroscopy and was 289 compared with that of the fresh catalyst. Fig. S1 shows that FTIR spectra of both fresh and 290 recycled catalyst are almost similar. Moreover, ICP-OES shows that there are no significant 291 changes in copper content of the recycled catalyst and loading of copper after 10 cycles was 292 1.46 mmol g^{-1} . The results confirm that the catalyst is stable and its structure and composition 293 did not change even after ten times recycling. 294

In order to investigate the leaching of the catalyst, the reaction of phenyl acetylene, benzyl 295 bromide and sodium azide was chosen as the model reaction and performed under optimized 296 condition given in Table 1. The reaction was stopped after half of the reaction time and the 297 catalyst was separated from the reaction mixture by using a magnet. The remaining mixture 298

(without catalyst) was left to stir for another period of half the reaction time. As is shown in 299
Fig. 8, no more products were produced after removal of the catalyst indicating there is no 300
significant leaching of copper ions. Moreover, based on the results of ICP-OES, no free 301
copper ions were detected in the reaction mixture which confirms that the leaching of catalyst 302
is negligible. 303



Fig. 8 Leaching experiment.

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Comparison with other catalysts

The catalytic performance of MNP@SPAAm/Cu was then compared with that of some other 308 catalysts used for Huisgen cycloaddition of azides and alkynes. The reaction of phenyl 309 acetylene, benzyl bromide and sodium azide was chosen as the model reaction and the data 310 obtained from some catalysts reported recently are summarized in Table 3. It is observed that 311 in most cases the yield of the reactions is high. However the process introduced in this study, 312 is a green approach in which the reaction is performed in water at mild temperature and is 313 completed in short time. The catalyst is partly composed of starch which as a non-toxic 314 natural polymer makes the catalyst more biodegradable and environmentally friendly. 315 Because of its magnetic properties, the catalyst can also be easily and rapidly separated from 316 the reaction mixture by using a magnet. Moreover, the loading of the catalyst prepared here is 317 very high which in turn decreases the amount of catalyst required for the reaction. Due to 318 high loading of the catalyst, only a small amount of catalyst can precede the reaction 319 effectively. 320

Table 3 The comparison of MNP@SPAAm/Cu with other catalysts reported for Huisgen cycloaddition.

Ph Br + NaN ₃ + Ph — H Catalyst Sodium ascorbate Solvent					N ^{-N} N Ph		
Catalyst	Cu loading (mmol g ⁻¹)	Cat. Amount (mg(mol%))	Solvent	<i>Т</i> (°С)	Time (h)	Yield (%)	Ref
Chitosan/Cu	0.80	50(0.4)	H_2O	r.t	4	99	28
Chitosan-coated Fe ₃ O ₄ /Cu	0.77	20(1.54)	CH_2Cl_2	r.t	12	92	22
Cu/SiO2	2.59	38.5(10)	H_2O	70	12	95	31
Hydroxyapatite/Cu (II)	0.1	200(2)	H_2O	50	8	97	32
Cu NPs/Activated carbon	0.3	17(0.5)	H_2O	70	3	98	33
Silica PEI/CuNPs	0.24	2(0.05)	DMSO	r.t	0.17	98	34
MNP@Triazole/Cu	0.51	10(0.5)	H ₂ O/t-BuOH	55	2	99	17
MNP@PILCu	1.87	4(0.7)	H_2O	50	2.5	95	24
Cu NPs/Graphite	0.77	6.5(0.05)	H ₂ O/CH ₃ OH	70	12	91	35
MNP@SPAAm/Cu	1.6	3.1(0.5)	H_2O	50	0.5	99	This study

Conclusion

We have successfully developed a green heterogeneous catalytic system for Huisgen 323 cycloaddition by immobilization of copper ions on magnetic polymeric supports. The solid 324 support was prepared by polymerization and grafting of AAm onto starch in the presence of 325 functionalized Fe₃O₄ magnetic nanoparticles. The presence of starch makes the prepared 326 catalyst more cost effective and eco-friendly. The loading level of copper ions on the cross-327 linked polymeric supports was 1.6 mmol g⁻¹ and no significant loss of catalyst activity was 328 observed. The prepared catalyst exhibits high catalytic activity in Huisgen cycloaddition of 329 various azides and alkynes. 1,2,3-triazoles with good to excellent yields were synthesized by 330 using the prepared catalyst. The catalyst was separated magnetically and reused for ten cycles 331 of reaction without any significant loss of catalytic activity. Finlay, comparison of this 332 protocol with other reported methods showed that the presented catalyst is used in lower 333

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weigh	nt percent. This aspect of catalyst is especially useful in large scale where a small	334
amou	nt of catalyst can produce large amounts of products.	335
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Graphical Abstract

Magnetic Starch Nanocomposite as a Green Heterogeneous Support for

Immobilization of Large Amounts of Copper Ions

Ali Pourjavadi*, Anahita Motamedi, Seyed Hassan Hosseini, Mojtaba Nazari

Polymer Research Laboratory, Department of Chemistry, Sharif University of Technology, Tehran, Iran E-mail address: purjavad@sharif.edu;_Phone/fax: (982)166165311

