



Advanced removal of toluene in aerosol by adsorption and photocatalytic degradation of silver doped TiO₂/PU under visible light irradiation

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1 **Advanced removal of toluene in aerosol by adsorption and photocatalytic**
2 **degradation of silver doped TiO₂/PU under visible light irradiation**

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11
12 **Abstract**

13 We synthesized a novel Ag-TiO₂/PU material for the effective removal of gaseous toluene by
14 both adsorption and photocatalytic degradation. The Ag particles, which distributed on the TiO₂
15 surface, and the Ag dopants, which incorporated into the TiO₂ lattice, increased the electron-hole
16 pair separation efficiency of TiO₂. Therefore, Ag-TiO₂/PU exhibited high photocatalytic
17 degradation of toluene even under visible light. Porous polyurethane (PU) was used to
18 immobilize the enhanced TiO₂, to increase the adsorption capacity of the photocatalyst. The
19 synthesized Ag-TiO₂/PU removed gaseous toluene even under dark condition via adsorption.
20 The removal of gaseous toluene by Ag-TiO₂/PU under visible light conditions was due to the
21 combination of both adsorption and photocatalytic degradation. The oxygen content in the gas
22 stream insignificantly affected the toluene adsorption by the Ag-TiO₂/PU. However, the
23 photocatalytic degradation of toluene by Ag-TiO₂/PU increased with increasing oxygen content
24 and stabilized when the oxygen content exceeded 15 %. These results suggest that ambient air
25 can be used economically as an oxygen source for the photocatalytic degradation of gaseous
26 toluene by Ag-TiO₂/PU under visible light condition. Under visible light irradiation, 6 % Ag-

27 TiO₂/PU, which was the Ag/TiO₂ ratio that optimized the photocatalytic degradation activity of
28 TiO₂, removed 85.2 % of the toluene in 100ppm inlet gas, of which 90.3 % was mineralized into
29 CO₂ and H₂O.

30

31 **Keywords:** Ag incorporation; toluene removal; photocatalytic degradation; oxygen content
32 effects; visible light

33

34 1. Introduction

35 Many volatile organic compounds (VOCs), emitted from the combustion of fuels, biomass
36 and waste, smoking, solvent use, and the surfaces of carpet, PVC flooring, adhesive products,
37 coating mediums for furniture, and room decorations, have been regulated due to their human
38 toxicity [1, 2]. In particular, even low-dose exposure to carcinogenic benzene and chlorinated
39 VOCs is strongly associated with acute non-lymphocytic leukemia, aplastic anemia and
40 chromosomal aberrations [3]. The inhalation of toluene, which is one of the most commonly
41 found VOCs, can lead to nervous system complications, such as reduction in thinking, memory
42 and muscular abilities, as well as some level of loss in both hearing and color vision [4]. Despite
43 the availability of many treatment technologies, including absorption, condensation, incineration,
44 biological oxidative filtering, and thermal plasma treatment for VOC removal, most have been
45 considered for industrial applications requiring complicated disposal techniques, high costs and
46 skilled labor [5]. Recently, applications for the photocatalytic degradation and removal of
47 gaseous toluene have become a very attractive and promising alternative [6, 7]. Under or near
48 UV irradiation, TiO₂ photocatalyst can photocatalytically degrade toluene into carbon dioxide,
49 water and simple mineral acids [8]. Compared to conventional treatment methods, the use of

50 photocatalysis for toluene removal exhibited several advantages such as low cost and simplicity
51 [9]. However, the photocatalytic degradation of toluene by TiO_2 photocatalysis is a relative slow
52 process with many limitations for industrial or large-scale application, along with safety issues
53 and high-energy consumption due to UV or near UV irradiation [10].

54 To overcome these disadvantages, numerous studies have investigated enhancing the
55 photocatalytic activity of TiO_2 and expanding the photocatalytic applications in practical systems
56 using visible or solar irradiation to initiate the photocatalysis [11-15]. Ag has been used as a
57 doping or sensitivity agent to enhance the photocatalytic activity of TiO_2 due to silver's ability to
58 act as both an electron sink and donor to increase the electron-hole pair separation efficiency of
59 TiO_2 and thereby enhance its photocatalytic activity [16]. Due to silver's antibacterial activity,
60 the Ag-doped TiO_2 photocatalyst has been mostly used as a disinfection material [17-20]. A few
61 studies have utilized the synthesized Ag-doped TiO_2 to remove other pollutants, particularly, for
62 removal of toluene gas [21-23]. Thus, the present study firstly aimed to use Ag as a doping agent
63 for enhancing the photocatalytic activity of TiO_2 when applied to the removal of gaseous
64 toluene.

65 The photocatalytic activity and degradation efficiency, in particular, the degradation of
66 pollutants in gas phase, are strongly dependent on the adsorption capacity of the photocatalyst
67 [24]. Thus, the second aim of the present study was to immobilize TiO_2 and Ag-doped TiO_2
68 photocatalyst on a polyurethane (PU) substrate, a porous material. We hypothesize that the
69 immobilization and doping would increase the adsorption ability of the photocatalyst for the
70 removal of gaseous toluene. The increased adsorption ability would also increased the
71 degradation rate and hence the toluene removal in aerosol by both adsorption and photocatalytic
72 degradation.

73 In addition, the photocatalytic degradation processes in aerosol are strongly dependent on the
74 reactions of photo-generated electrons and holes with oxygen and H₂O molecules to produce
75 superoxide radicals ($^{\bullet}O_2^-$) and hydroxyl radicals ($^{\bullet}OH$), respectively [25]. Thus, the moisture and
76 oxygen contents are the key factors affecting the photocatalytic degradation of aerosol pollutants.
77 Several studies have investigated the effects of moisture content on the photocatalytic
78 degradation in aerosol, but without focusing on the effects of oxygen on the degradation [25-29].
79 Therefore, the third aim of the present study was to investigate the effects of oxygen content on
80 the photocatalytic degradation of toluene in aerosol using Ag-TiO₂/PU under visible light
81 conditions.

82

83 2. Materials and Methods

84

85 2.1. Synthesis of Ag-TiO₂/PU

86 Before being used as a substrate to immobilize Ag-doped TiO₂, pristine PU was pre-treated
87 by a mixed solution of toluene, toluene-2,4-diisocyanate, and anhydrous triethylamine to
88 introduce isocyanate groups (NCO) onto its surface [17]. The isocyanated PU was immersed into
89 a solution of amino titanasiloxane, containing a Si-O-Ti bonds and an amine group (NH₂), which
90 was prepared based on reaction between titanium tetraisopropoxide with γ -aminopropyl
91 triethoxysilane. During the immersing process, the titanasiloxane was immobilized on PU by
92 reactions between the isocyanate groups of the isocyanated PU and the amino group (NH₂) of the
93 amino titanasiloxane [17]. After 1 h immersing, the PU immobilized titanasiloxane was taken
94 out and a 0.1 M AgNO₃ solution, which was prepared by the dissolution of AgNO₃ in deionized
95 water at 60°C, was slowly added (drop-wise) onto the titanasiloxane immobilized on PU. The

96 obtained material was cleaned using 1 M oxalic acid solution, irradiated with a UV light (60W)
97 for 5 h and calcined under nitrogen at 200°C for 5 h to produce Ag-doped TiO₂ immobilized on
98 PU (Ag-TiO₂/PU). The addition volume of AgNO₃ solution was adjusted in order to synthesize
99 Ag-TiO₂/PU materials with Ag/TiO₂ ratios of 0, 2, 4, 6, 8 and 10 wt %.

100

101 2.2. Material Characterization

102 X-ray photoelectron spectroscopy (XPS) spectra of the synthesized Ag-TiO₂/PU materials
103 were obtained using a Thermo Fisher K-Alpha X-ray Photoelectron Spectrometer system. The
104 Gaussian multi-peak shapes were applied to fit the Ag3d_{5/2} and Ti 2p_{3/2} peaks in the obtained
105 XPS spectra for determining the elemental state of the silver and titanium in Ag-TiO₂/PU. A
106 Bruker AXN model with a Cu-K α radiation ($\lambda = 1.5418 \text{ \AA}$) source was used to obtain X-ray
107 diffraction (XRD) spectra of Ag-TiO₂/PU. The surface morphology of the Ag-TiO₂/PU materials
108 was analyzed using a Hitachi S-4700 scanning electron microscope (SEM). Before the SEM
109 analysis, the Ag-TiO₂/PU samples were coated with Pt to increase the conductivity of the
110 photocatalyst surface. The surface area (S_{BET}) of the synthesized Ag-TiO₂/PU materials was
111 determined using the Brunauer-Emmett-Teller (BET) isotherm carried out by nitrogen adsorption
112 and desorption at 77K. The optical absorption ability of the Ag-TiO₂/PU materials in the
113 wavelength range 300–700 nm was determined by an Evolution 300 spectrophotometer (UV-
114 1700 Shimadzu).

115

116 2.3. Experimental apparatus

117 Figure 1 shows the experimental apparatus for the continuous photocatalytic degradation and
118 removal of gaseous toluene using Ag-TiO₂/PU. The experimental apparatus was composed of

119 three main parts: gas generator, reaction chamber and analyzer system. The gas generator system
120 included a mixer, a humidifier and three gas cylinders of 1000ppm toluene in nitrogen gas,
121 oxygen and nitrogen gases (Figure 1). The mixer and humidifier were adjusted to control the
122 toluene gas concentration and humidity level, respectively. The reaction chamber was composed
123 of a dark cover cask (25 x 50 x 50 cm), two 20 W bulbs and a reactor. The bulbs were placed at
124 the top and bottom of the reaction chamber (Figure 1) to generate visible light in the range of
125 400–700 nm for the photocatalytic irradiation processes. The power density of the generated
126 visible light in the reaction chamber was 0.05 W/cm^2 . A reactor (2 x 4 x 15 cm) was placed in
127 the center of the reaction chamber. The top and bottom of the reactor were made of quartz to
128 allow easy passage of the visible light generated from the light bulbs through the reactor wall.
129 The online analyzer system included a Varian CP-3800 gas chromatograph (GC) equipped with a
130 flame ionization detector and a packed column (Porapak Q 80/100 2 x 2 mm) to analyze the
131 concentration of the outlet toluene. A methanizer, using Ni catalyst, was integrated into the GC
132 system to analyze the CO and CO₂ contents in the outlet gas.

133

134 2.4. Removal experiments

135 Flow rate meters were regulated to achieve a constant flow rate of 100 mL/min of 100ppm
136 toluene in the gas mixture. The humidifier was used to ensure that the relative humidity of the
137 gas mixture remained constant at 50 %. Before the toluene removal experiments, the input gas
138 was oriented through direction A to the GC system to re-check the concentration of the toluene
139 in the gas mixture. When the toluene concentration in the 100mL/min flow of mixed gas was
140 stabilized at 100ppm, the input gas was oriented toward direction B where it passed through the
141 reactor volume containing 36cm^3 of the synthesized Ag-TiO₂/PU porous material. The toluene

142 removal experiments were carried out under conditions of both dark and visible light, achieved
143 by turning the bulbs off/on, respectively, to determine the adsorption and photocatalytic
144 degradation ability of the synthesized Ag-TiO₂/PU, respectively. After the removal experiments,
145 the effluent gas was sent to the GC system using an auto sampling injector, which automatically
146 injected 100 μL of the effluent gas into the packed column in intervals of 10 min from the
147 reaction start time (t₀=0). The reaction start time (t₀=0) was estimated to be the time when the
148 input gas was oriented flowing direction B. Helium was used as a carrier gas with a flow rate of
149 25 mL/min. The removal efficiency and mineralization degree of toluene by Ag-TiO₂/PU were
150 evaluated using equations (1) and (2), respectively:

151 Toluene removal efficiency (%) = $\frac{C_0 - C_t}{C_0} \times 100\%$ (1)

152 Mineralization degree = $\frac{C_{tCO_2}}{7 \times (C_0 - C_t)} \times 100\%$ (2)

153 where:

154 C₀ (100ppm) is the concentration of toluene at the reaction start time (t₀=0), and C_t and C_{tCO₂} are
155 the concentrations of toluene and CO₂ at reaction time (t_i=t), respectively.

156

157 3. Results and Discussion

158

159 3.1. Material Properties

160 3.1.1. Elemental States of Silver

161 The high-resolution XPS spectra of the synthesized Ag-TiO₂/PU indicated that the first
162 elemental state of silver was silver metallic (Ag⁰), with peaks at 374.2 and 368.2 eV (Figure 2)
163 [30]. The obtained XRD results further confirmed the existence of Ag⁰ on the surface of Ag-

164 TiO₂/PU (Figure 3) [31]. The Ag⁰ was produced from the reduction of AgNO₃ under the effects
165 of the UV irradiation and calcination temperature during the Ag-TiO₂/PU preparation processes
166 [16, 32]. The UV irradiation and oxalic acid, rolled as a cleanser for the purification process,
167 enhanced the reduction of AgNO₃ into Ag⁰ [33-36]. In Ag-TiO₂/PU, silver also existed in form of
168 Ag⁺ corresponding to peaks at 373.4 and 367.4 eV in the obtained XPS spectra (Figure 2) [37].
169 However, the absence of any Ag₂O peak in the XRD spectra (Figure 3) implied that most of the
170 Ag⁺ ions had been incorporated into or anchored in the TiO₂ lattice via Ti-O-Ag bonds or that
171 the concentration of Ag⁺ existing in form of Ag₂O was too low to be detected by the XRD
172 analysis [21, 32].

173 The Ag⁺/Ag⁰ ratios in Ag-TiO₂/PU, which are proportional to the ratios of (the area under the
174 Ag⁺ peak)/(the area under the Ag⁰ peak) in the XPS spectra, are shown in Table 1. As the
175 Ag/TiO₂ ratio (controlled by increasing the added AgNO₃ volume) in Ag-TiO₂/PU was increased
176 to 6 wt %, the Ag⁺/Ag⁰ ratio increased to a maximum of approximately 55.6%, but then slightly
177 decreased with the further increase of the Ag/TiO₂ ratio above 6 wt %. It was because only a
178 certain amount of Ag⁺ could be incorporated into or anchored in the TiO₂ lattice via Ti-O-Ag
179 bonds. At the limitation of the incorporation, the additional Ag⁺ in the added AgNO₃ could not
180 be further incorporated into the TiO₂ lattice, and was instead reduced into Ag⁰ and distributed on
181 the surface of the TiO₂ layer. Thus, the Ag⁺/Ag⁰ ratio slightly decreased as the Ag/TiO₂ ratio was
182 increased above 6 wt %.

183

184 3.1.2. Elemental States of Titanium

185 The obtained XPS results indicate that the elemental state of titanium in TiO₂/PU was only
186 Ti⁴⁺, while the elemental states of titanium in the Ag-TiO₂/PU materials were both Ti⁴⁺ and

187 Ti^{3+} (Figure 4) [38, 39]. UV irradiation can reduce any Ti^{4+} on the TiO_2 surface to Ti^{3+} [40].
188 However, the synthesized TiO_2/PU did not contain any Ti^{3+} ions, which indicates that the Ti^{3+}
189 was formed due to the incorporation of silver into the TiO_2 lattice. Atla et al. reported that the
190 incorporated Ag induced a change in the chemical state of TiO_2 leading to the reduction of Ti^{4+}
191 into Ti^{3+} [32]. The incorporation of Ag also induced oxygen vacancies in the TiO_2 lattice,
192 resulting in the reduction of Ti^{4+} to Ti^{3+} [41, 42]. Table 1 shows the calculated Ti^{3+}/Ti^{4+} ratios in
193 the synthesized Ag- TiO_2/PU , which are proportional to the ratios of (the area under the Ti^{3+}
194 peak)/(the area under the Ti^{4+} peak) in the obtained XPS spectra. The results indicate that the
195 Ti^{3+} content in Ag- TiO_2/PU increased rapidly with increasing Ag/ TiO_2 ratio, and gradually
196 stabilized when the Ag/ TiO_2 ratio rose above 6 wt %. The increase in Ti^{3+} content in Ag- TiO_2/PU
197 was attributed to the increase in Ag content, which was incorporated into the TiO_2 lattice.
198 However, the Ag was only incorporated into the TiO_2 lattice up to a certain limit, leading to the
199 stabilization of Ti^{3+} content in Ag- TiO_2/PU even with the further increase in the Ag/ TiO_2 ratio.

200

201 3.1.3. Morphology and Surface Area

202 Figure 5 shows the surface morphology of the synthesized TiO_2/PU , and the 2, 4, 6, 8 and
203 10% Ag- TiO_2/PU materials. The obtained results indicate that the TiO_2 in TiO_2/PU was
204 smoothly immobilized on the PU surface as a thin layer (Figure 5A). Compared to the surface
205 morphology of TiO_2/PU , the Ag- TiO_2/PU materials exhibited a rougher morphology due to the
206 dispersion of the formed small Ag particles on the surface of the TiO_2 layer. The obtained
207 HRTEM results confirmed the existences of Ag particles on surface of TiO_2 (Figure 6). The
208 lattice spacing of approximately 0.24 and 0.25 nm correspond to the interlayer distance of the
209 (111) and (004) crystal planes Ag [43, 44]. The degree of surface roughness of Ag- TiO_2/PU

210 increased with increasing Ag/TiO₂ ratio (increasing in Ag particle content). When the Ag/TiO₂
211 ratios increased up to 8 wt %, the Ag particles began to cluster into larger particles covering the
212 TiO₂ layer.

213 The BET surface areas of TiO₂/PU and Ag-TiO₂/PU are shown in Table 1. The BET surface
214 area of TiO₂/PU was 110.9 m²/g, which was much higher than that of commercial TiO₂ powder,
215 such as AEROXIDE[®] TiO₂ P25 obtained from Evonik Degussa Corporation (approximately
216 60 m²/g). This indicates that the surface area of TiO₂ was successfully enhanced by using porous
217 honeycomb PU as a substrate for the immobilization. The obtained BET results also indicate that
218 the surface areas of the synthesized Ag-TiO₂/PU materials were much higher than that of
219 TiO₂/PU. This may have been due to the aforementioned effect of the Ag particles dispersed on
220 the TiO₂ surface in increasing the degree of surface roughness of TiO₂. The BET surface areas of
221 the synthesized Ag-TiO₂/PU materials were also greatly increased with increasing Ag/TiO₂
222 ratios up to 6 wt %. However, the BET surface area of the areas of the 8 % Ag-TiO₂/PU and 10
223 % Ag-TiO₂/PU were slightly lower than that of the 6 % Ag-TiO₂/PU. This was attributed to the
224 gathering or cluster of the Ag into larger particles at the high Ag/TiO₂ ratios, according to the
225 SEM analysis. Thus, 6 % Ag-TiO₂/PU exhibited the highest surface area (186.6 m²/g).

226

227 3.1.4. Optical absorption ability

228 Figure 7 shows the optical absorption in range of 300-700 nm of the synthesized TiO₂/PU
229 and 2, 4, 6, 8 and 10 % Ag-TiO₂/PU materials. TiO₂/PU inherited the optical absorption
230 properties of TiO₂, which exhibits a strong absorption only in the UV region and the absorption
231 edge around 370nm [13, 45]. The optical absorption of the synthesized Ag-TiO₂/PU materials
232 was observed in both the UV and visible regions. The significant enhancement of optical

233 absorption in the visible region of Ag-TiO₂/PU was due to a contribution of the plasmon
234 resonance of the Ag particles dispersed onto the TiO₂ surface [46]. The plasmon resonance of Ag
235 particles excited electrons of the valence band of TiO₂ and transferred the excited electrons from
236 the valence band to the conduction band of TiO₂ [45]. The Ag particles also provided sites for the
237 accumulation of the excited electrons, so that Ag acted as an electron sink to hinder the
238 recombination of the excited electrons in the conduction band with holes in the valence band of
239 TiO₂ [47]. Therefore, Ag-TiO₂/PU absorbed the visible light for the separation of the electrons
240 and holes. The light absorption enhancement of Ag-TiO₂/PU was also due to the role of the
241 incorporated Ag, which bonded to TiO₂ via Ag-O-Ti bonding, leading to oxygen vacancies and
242 the formation of Ti³⁺ in the TiO₂ lattice. It has been reported that the energy level of Ti³⁺ was
243 located in between the conduction band and the valence band of TiO₂ [47]. Therefore, the
244 formed Ti³⁺ also acted as an intermediate agent to enhance the transfer of electrons from the
245 valence band to the conduction band of TiO₂, contributing to the enhancement of the optical
246 absorption of the synthesized Ag-TiO₂/PU.

247 Figure 7 also shows that the optical absorption ability of Ag-TiO₂/PU increased as the Ag
248 weight fraction in Ag/TiO₂ increased up to 6 wt %, but then slightly decreased with further
249 increase in the Ag/TiO₂ ratio. At the high Ag/TiO₂ ratios of 8 and 10 wt %, Ag tended to gather
250 into larger particles on the TiO₂ surface (see section 3.1.3), leading to an uneven distribution of
251 Ag particles on the TiO₂ layer or a decrease in the interfacial surface between Ag and TiO₂
252 (Table 1). Thus, Ag could not act as a more effective electron carrier/sink to enhance the electron
253 hole pair separation efficiency of TiO₂, resulting in the decreased light absorption efficiency of
254 Ag-TiO₂/PU at the high Ag/TiO₂ ratios of 8 and 10 wt %. The large Ag particles also eclipsed
255 the light reaching the TiO₂ surface, thus decreasing the optical absorption of Ag-TiO₂/PU [48].

256 Thus, a further increase of Ag content in Ag-TiO₂/PU further reduced the light absorption
257 intensity (Figure 7 E and F).

258

259 3.2. Toluene Removal

260

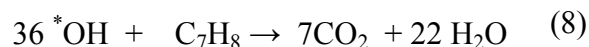
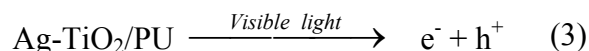
261 3.2.1. Removal Mechanism

262 Figure 8 shows the toluene removal results by TiO₂/PU, and 2, 4, 6, 8 and 10% Ag-TiO₂/PU.

263 The experiments were conducted in dark conditions for the first 180 min, after which visible
264 light was provided for an additional 180min. Under the darkened conditions, the outlet toluene
265 concentration gradually increased up to 100ppm at around 165 min, which is the same as the
266 inlet concentration. This means that toluene saturation at the given adsorbent dose (Ag-TiO₂/PU)
267 occurred at around 165 min (Figure 8A). In addition, no CO₂ corresponding to the photocatalytic
268 degradation of gaseous toluene was detected (Figure 8B). This indicates that gaseous toluene was
269 removed solely by adsorption by Ag-TiO₂/PU in darkened conditions. When Ag-TiO₂/PU was
270 exposed to water vapor, its surface was be hydroxylated, leading to the formation of hydroxyl
271 groups on surface of Ag-TiO₂/PU via Ti-OH or Ag-OH bonds [49, 50]. The hydroxyl groups
272 were thus able to bond with the π -electrons of the aromatic ring of toluene, resulting in the
273 adsorption of toluene on the Ag-TiO₂/PU surface [49]. The toluene was also trapped on the Ag-
274 TiO₂/PU surface by physical bond or electrostatic interaction between the aromatic ring of
275 toluene and the various cations, such as Ti⁴⁺, Ti³⁺ and Ag⁺, existing on the Ag-TiO₂/PU surface
276 [51].

277 Radiation with visible light after saturation did not affect the toluene concentration passing
278 through TiO₂/PU, which indicated that TiO₂/PU did not exhibit any significant photocatalytic

279 degradation activity to remove gaseous toluene under visible light conditions. However, the
 280 outlet toluene passing through the Ag-TiO₂/PU materials suddenly increased to a level exceeding
 281 the inlet concentration, due to the desorption of the toluene adsorbed on Ag-TiO₂/PU (rolled as
 282 an adsorbent) by scrubbing of the CO₂ generated from the photocatalytic degradation of toluene
 283 by Ag-TiO₂/PU (mainly acting as a photocatalyst) under visible light conditions. Because the
 284 doped Ag enhancing the electron-hole pair generation capacity and separation efficiency of TiO₂,
 285 Ag-TiO₂/PU easily generated electron-hole pairs, even under visible. The generated electrons
 286 and holes then participated in reactions with the O₂ and/or H₂O molecules in aerosol to produce
 287 hydroxyl and superoxide radicals, which are strong oxidative agents. The mechanism by which
 288 the hydroxyl and superoxide radicals were generated by Ag-TiO₂/PU under visible light is
 289 described by the following reactions:



290 These generated oxy radicals then participated in the degradation of toluene into CO₂ and
 291 H₂O, accompanied by a sharp increase in the CO₂ concentration, as shown in Figure 8B [51-53].
 292 The scrubbing of the adsorbed toluene by the CO₂ generated from the photocatalytic degradation
 293 of toluene caused desorption of the toluene, which had initially been adsorbed on the Ag-

294 TiO₂/PU surface during the darkened period. This desorption led to a sudden increase in the
295 toluene concentration in the reactor. Although Ag-TiO₂/PU photocatalytically degraded a certain
296 amount of the toluene passing through the reactor, the outlet toluene rose above its inlet
297 concentration (100 ppm) for a short period before the reaction time reached 255 min. After the
298 adsorbed toluene was almost completely desorbed, the outlet toluene concentration displayed a
299 sharp decrease due to the continuous photocatalytic degradation of toluene by the Ag-TiO₂/PU
300 photocatalyst, accompanied by a decrease in the CO₂ concentration with a slight time lag of
301 around 15 min (Figure 8B). After the adsorbed toluene was almost entirely desorbed, the
302 incoming toluene underwent continuous photocatalytic degradation. Thus, the outlet toluene
303 concentration plateaued in the range of 15 to 38 ppm depending on the Ag content in Ag-
304 TiO₂/PU (Figure 8A).

305 When visible light was provided from the beginning of the toluene removal experiments
306 ($t_0=0$), without an adsorption period under dark conditions, the outlet toluene concentrations
307 passing through the Ag-TiO₂/PU materials plateaued at around 10 to 30 ppm after 75 or 90 min
308 (Figure 9A). During the initial experimental period, the toluene was removed by both adsorption
309 and the photocatalytic degradation of Ag-TiO₂/PU. However, the CO₂ gas, generated as a main
310 product of the photocatalytic degradation of toluene, disturbed the adsorption of toluene early on.
311 Thus, if the visible light was provided for longer than 75-90 min, the input toluene was only
312 removed by the photocatalytic degradation activity of Ag-TiO₂/PU.

313

314 3.2.2. *Optimal Ag content*

315 Figure 8A shows that under dark condition, the slope in the outlet toluene concentration
316 passing through 6% Ag-TiO₂/PU was the shallowest. The steep slope of an adsorption curve is

317 inversely proportional to the adsorption capacity. A material with a very steep slope in its
318 adsorption curve reaches its adsorption saturation easily or has a low adsorption capacity,
319 whereas a material with a shallower slope has a high adsorption capacity. Thus, among the Ag-
320 TiO₂/PU materials, 6 % Ag-TiO₂/PU exhibited the highest adsorption capacity for toluene
321 removal because it had the highest surface area (Table 1).

322 Figures 8 and 9 show that the outlet toluene and CO₂ concentrations that passed through the
323 Ag-TiO₂/PU materials under visible light irradiation were stabilized at certain values that could
324 be used to calculate the toluene removal efficiency and the mineralization degree of toluene into
325 CO₂ and H₂O by Ag-TiO₂/PU at different Ag/TiO₂ ratios (Table 2). The toluene removal
326 efficiency and the degree of mineralization by Ag-TiO₂/PU showed similar results for both
327 conditions A and B (explained in the note at the bottom of Table 2). The removal efficiency of
328 toluene increased as the Ag/TiO₂ ratio increased up to 6 wt %, but then gradually decreased with
329 further increase in the ratio. These results were matched by those obtained from the XPS and
330 UV-Vis absorption analyses of Ag-TiO₂/PU photocatalyst. The increase in the Ag/TiO₂ ratio led
331 to an increase in the number of both Ag ions, which were incorporated into the TiO₂ lattice, and
332 metallic Ag, which was dispersed onto the TiO₂ layer. Consequently, the electron-hole
333 separation efficiency and lifespan of the excited electrons in TiO₂ were both increased, which
334 further increased the photocatalytic degradation efficiency of TiO₂. However, the incorporation
335 of Ag ions into the TiO₂ lattice was limited by the tendency of the Ag particles, which had
336 dispersed onto the TiO₂ lattice and thus enhanced the electron-hole pair separation efficiency of
337 TiO₂, to gather into large particles at high Ag/TiO₂ ratios of 8 and 10 wt %, which decreased
338 their enhancement role. Thus, the effect of Ag in enhancing the photocatalytic activity of TiO₂
339 seemed to reach a limit when the Ag/TiO₂ ratio was 6 wt %.

340

341

342 *3.2.3. Effects of Oxygen content*

343 Figure 10 shows the toluene removal by 6% Ag-TiO₂/PU carried out under darkened
344 conditions for the first 180 min, followed by visible light irradiation for an additional 180 min, as
345 a function of the oxygen content in the input gas stream. Under the darkened condition, the
346 slopes in the outlet toluene concentrations passing through 6 % Ag-TiO₂/PU, and hence its
347 toluene adsorption ability, were not affected by the oxygen content. This indicated that oxygen
348 and toluene were adsorbed at different sites on the Ag-TiO₂/PU surface, so that the adsorption of
349 oxygen did not compete with toluene adsorption [25].

350 Under visible light conditions, the photocatalytic degradation of gaseous toluene using Ag-
351 TiO₂/PU was significantly affected by the oxygen content in the input gas stream. The
352 photocatalytic degradation of toluene increased with increasing oxygen content up to 15 % and
353 then stabilized (Figure 10A). The O₂ reacted with the electrons generated on the surface of Ag-
354 TiO₂/PU to produce superoxide radicals (reaction 4), which increased the photocatalytic
355 degradation of toluene in the gas stream [54]. The reaction between the oxygen and the photo-
356 generated electrons also prevented the recombination of the generated electrons and holes to
357 prolong the lifetime of the generated holes, thereby increasing the production of hydroxyl
358 radicals (via reactions 5 to 7) and hence increasing the degradation of toluene [55]. The reaction
359 between oxygen and electrons peaked at an oxygen content of 15 %, above which the
360 degradation of toluene in the gas stream was stabilized. These study results supported the
361 conclusion that ambient air, with an oxygen content of 21 %, can provide sufficient oxygen for

362 the economic photocatalytic degradation of gaseous toluene by Ag-TiO₂/PU under visible light
363 condition.

364

365 **4. Conclusion**

366 The synthesized Ag-TiO₂/PU exhibited high adsorption and photocatalytic degradation for
367 the effective removal of gaseous toluene. The high adsorption ability was attributed to the use of
368 porous PU as a substrate for the immobilization of Ag-TiO₂, which greatly increased the surface
369 area of the adsorbents (Ag-TiO₂/PU). The high photocatalytic degradation of toluene was
370 attributed to the Ag particles, which deposited onto the TiO₂ surface, and the Ag dopants, which
371 incorporated into the TiO₂ lattice. The optimal Ag/TiO₂ ratio for enhancing the photocatalytic
372 degradation activity of TiO₂ for toluene removal was 6 wt %. Under dark condition, the
373 synthesized Ag-TiO₂/PU exhibited only adsorption activity for removal of gaseous toluene,
374 whereas under visible light irradiation condition it exhibited a combination of both adsorption
375 and photocatalytic degradation. We investigated that the ambient air can be used economically to
376 provide sufficient oxygen for the photocatalytic degradation of gaseous toluene by Ag-TiO₂/PU
377 under visible light condition. Under visible light irradiation, 6 % Ag-TiO₂/PU successfully
378 removed 85.2 % of the 100ppm toluene in gas stream, while 90.3 % of the removed amount was
379 mineralized into CO₂ and H₂O.

380

381 **Acknowledgments:**

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384

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564 Table 1: The ratios of Ag^0/Ag^+ and $\text{Ti}^{3+}/\text{Ti}^{4+}$ and the BET surface area of the Ag-TiO₂/PU
565 materials

	Ag⁺/Ag⁰ ratios (%)	Ti³⁺/Ti⁴⁺ ratios (%)	BET surface area (m ² /g)
TiO₂/PU	-	0	110.9
2 % Ag-TiO₂/PU	42.4	15.5	129.2
4 % Ag-TiO₂/PU	48.8	19.7	155.7
6 % Ag-TiO₂/PU	55.6	22.6	186.6
8 % Ag-TiO₂/PU	54.3	23.4	176.3
10 % Ag-TiO₂/PU	53.1	24.2	148.1

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581 Table 2: The toluene removal efficiency and the mineralization degree by Ag-TiO₂/PU
 582 photocatalysts at different Ag/TiO₂ ratios under visible light conditions

	Condition A		Condition B	
	Removal efficiency (%)	Mineralization degree (%)	Removal efficiency (%)	Mineralization degree (%)
2 % Ag-TiO₂/PU	62.5	88.2	62.9	88.5
4 % Ag-TiO₂/PU	68.3	89.1	68.7	89.6
6 % Ag-TiO₂/PU	85.2	90.3	85.6	90.8
8 % Ag-TiO₂/PU	81.4	88.4	81.7	89.1
10 % Ag-TiO₂/PU	75.6	89.3	76.5	88.4

583 Note: Condition A: Light was provided after the toluene was adsorbed during the darkened period (0-180 min)
 584 Condition B: Light was provided from the beginning of the toluene removal ($t=t_0$).

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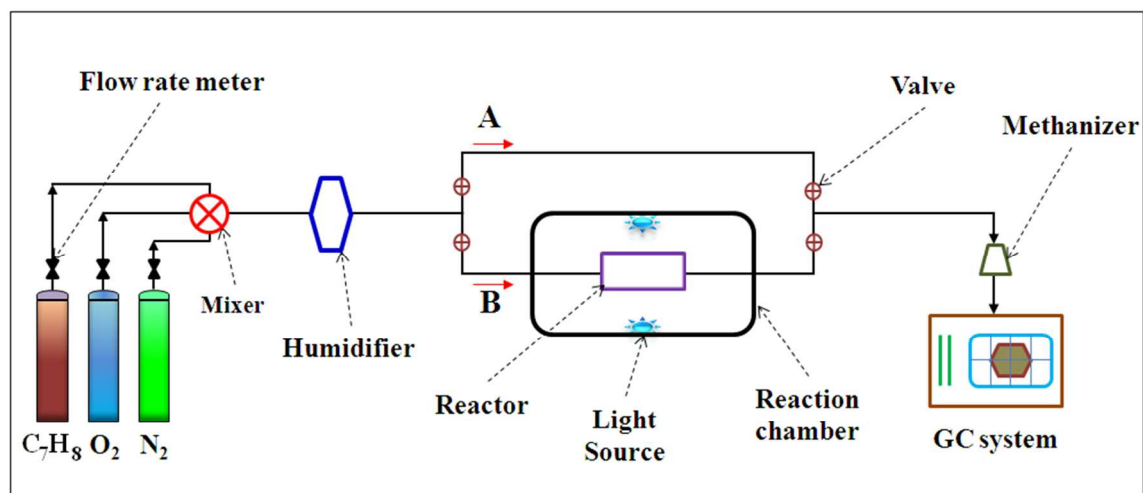
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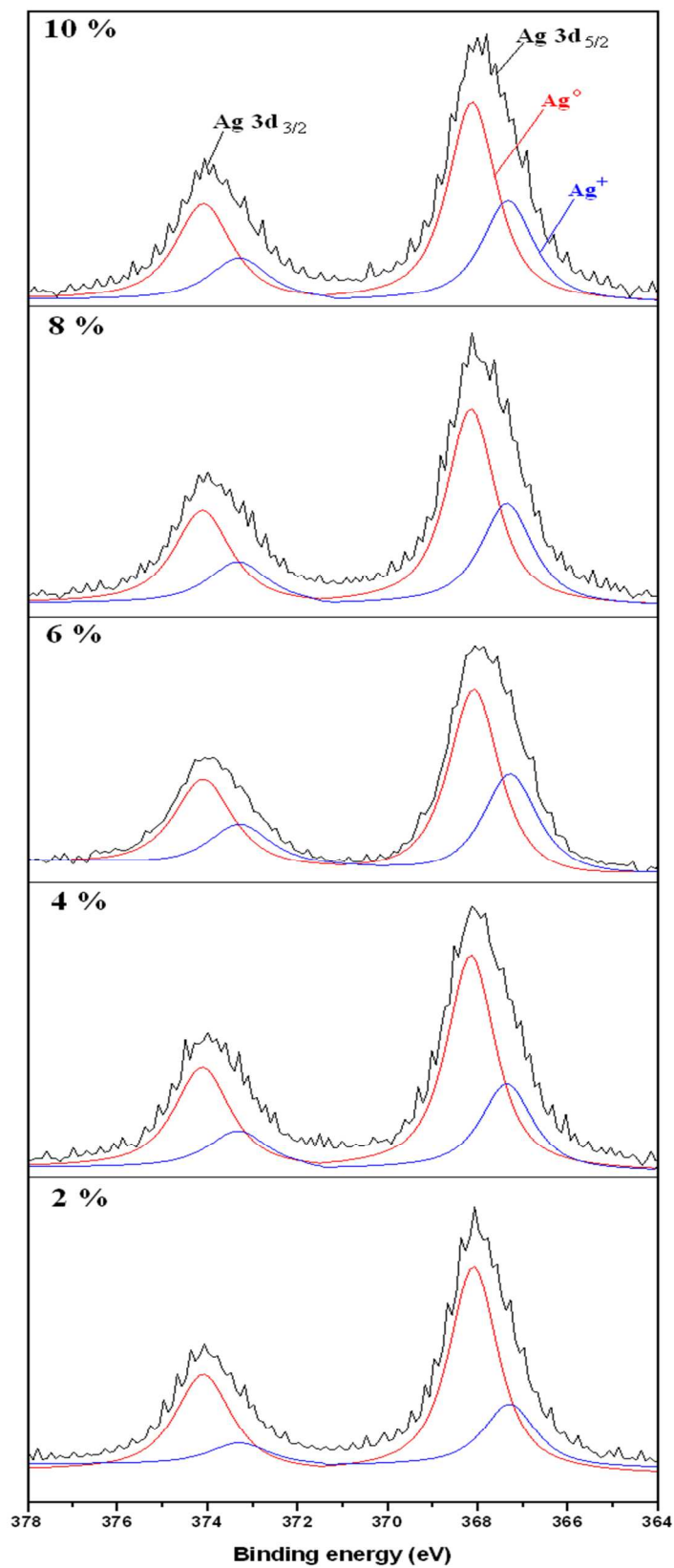
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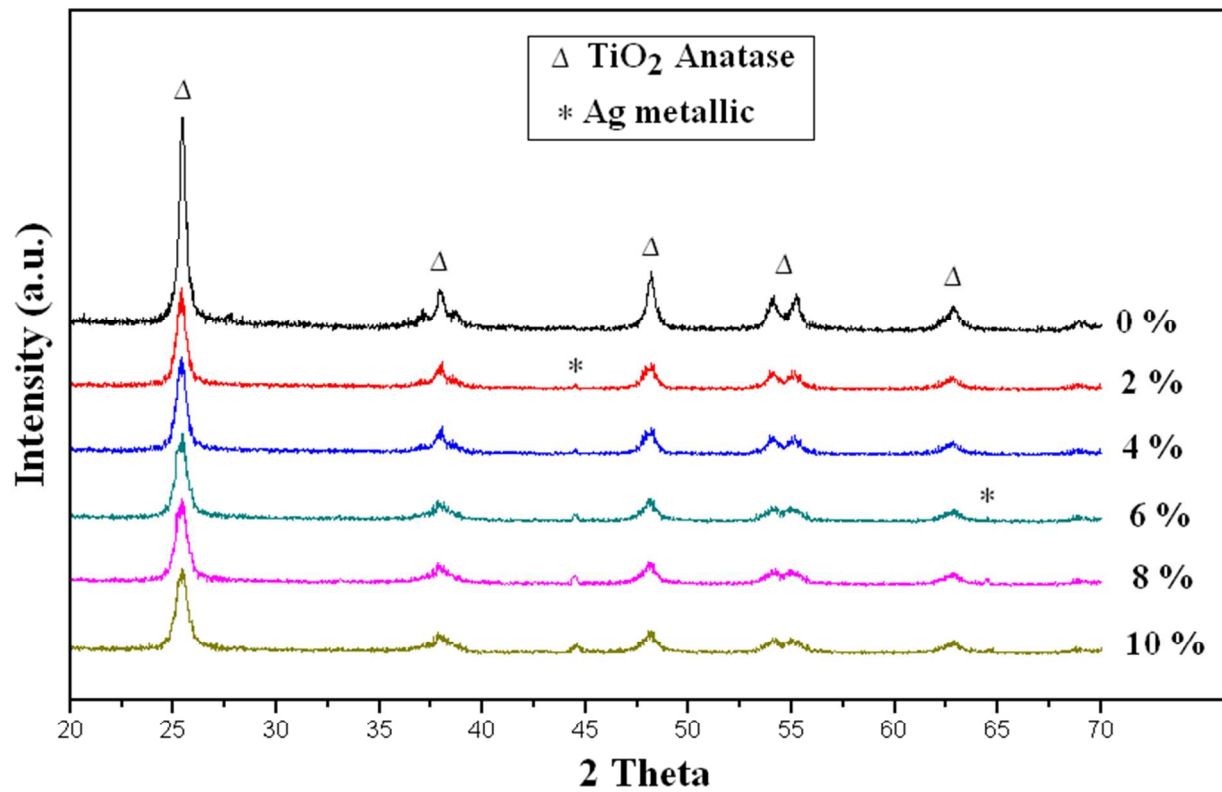
Figure 1: The experimental apparatus for removal of gaseous toluene



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Figure 2: High-resolution XPS spectra of Ag in X % Ag-TiO₂/PU



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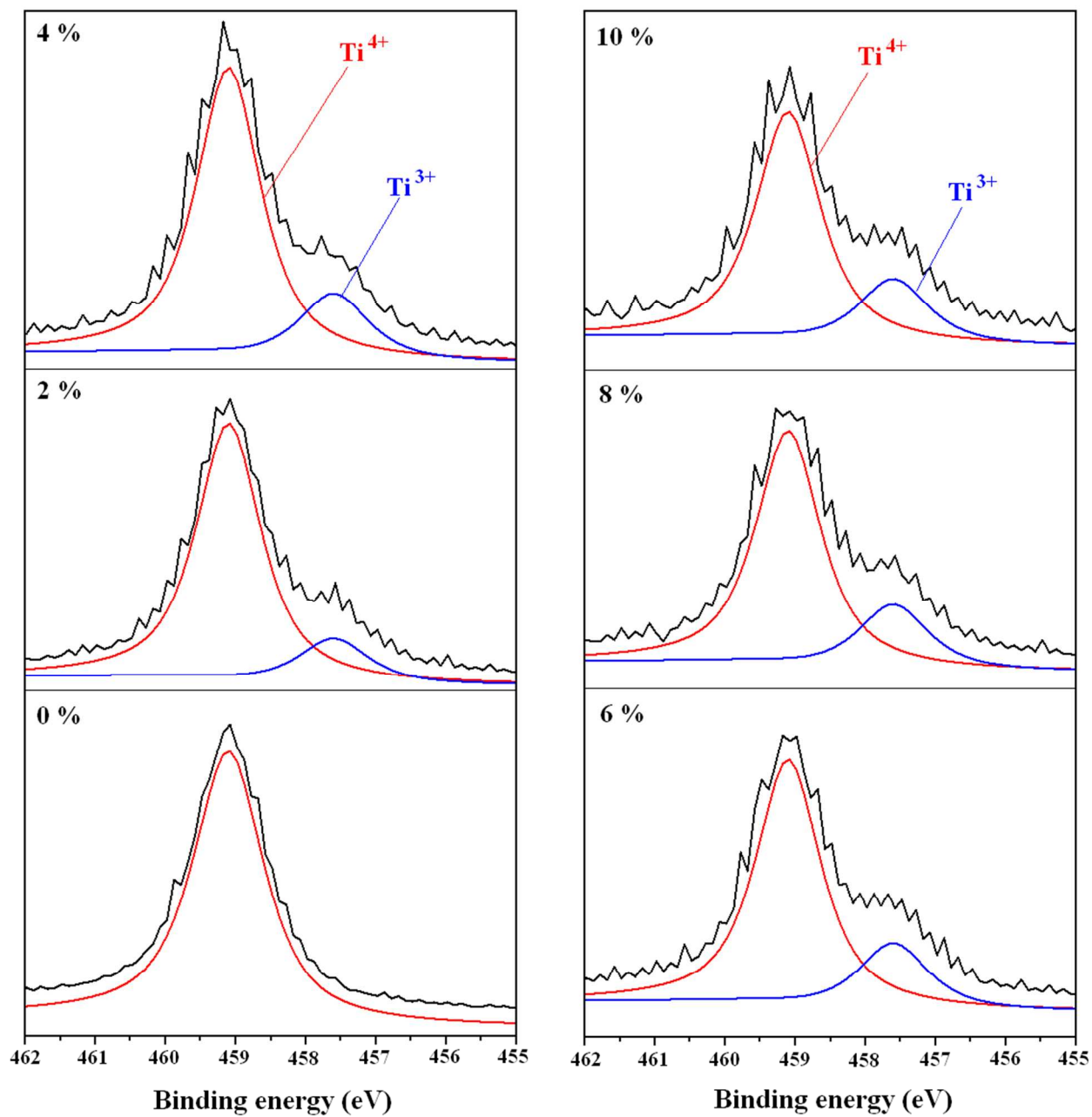
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Figure 3: XRD patterns of X % Ag-TiO₂/PU



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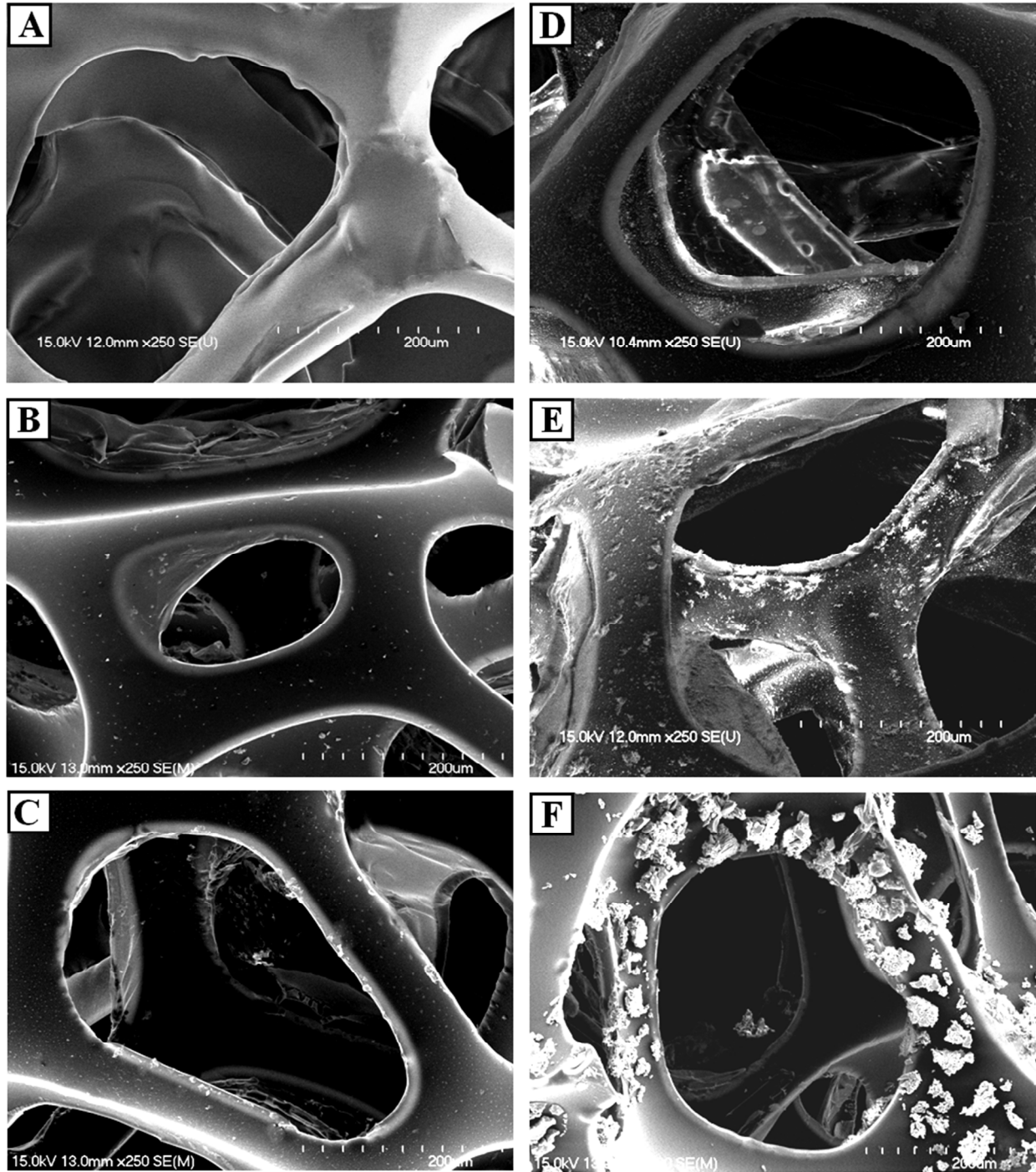
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Figure 4: High-resolution XPS spectra of Ti 2p_{3/2} in X % Ag-TiO₂/PU



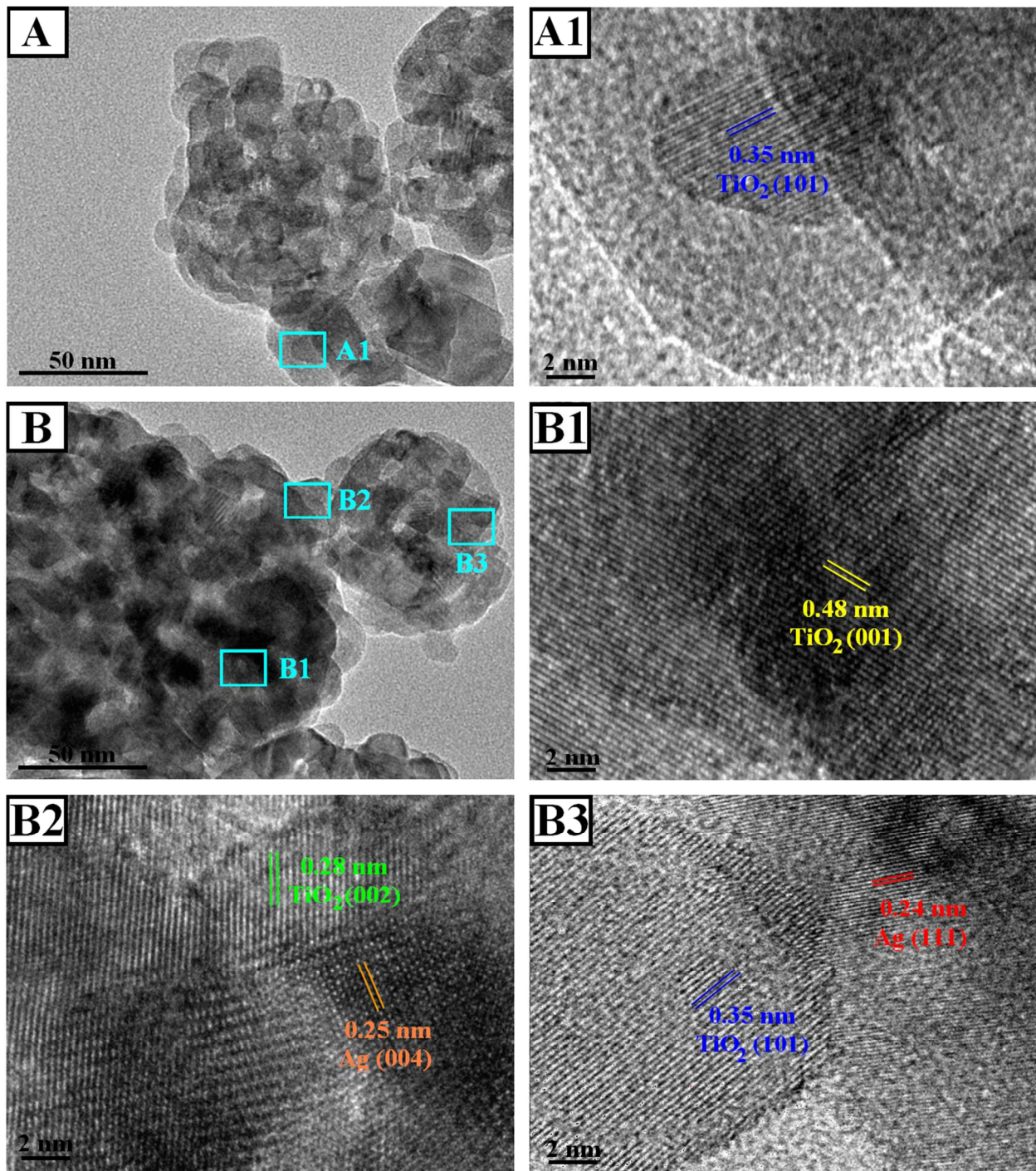
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639 Figure 5: SEM of TiO₂/PU (A), and 2% (B), 4% (C), 6% (D), 8% (E) and 10% (F) Ag-TiO₂/PU

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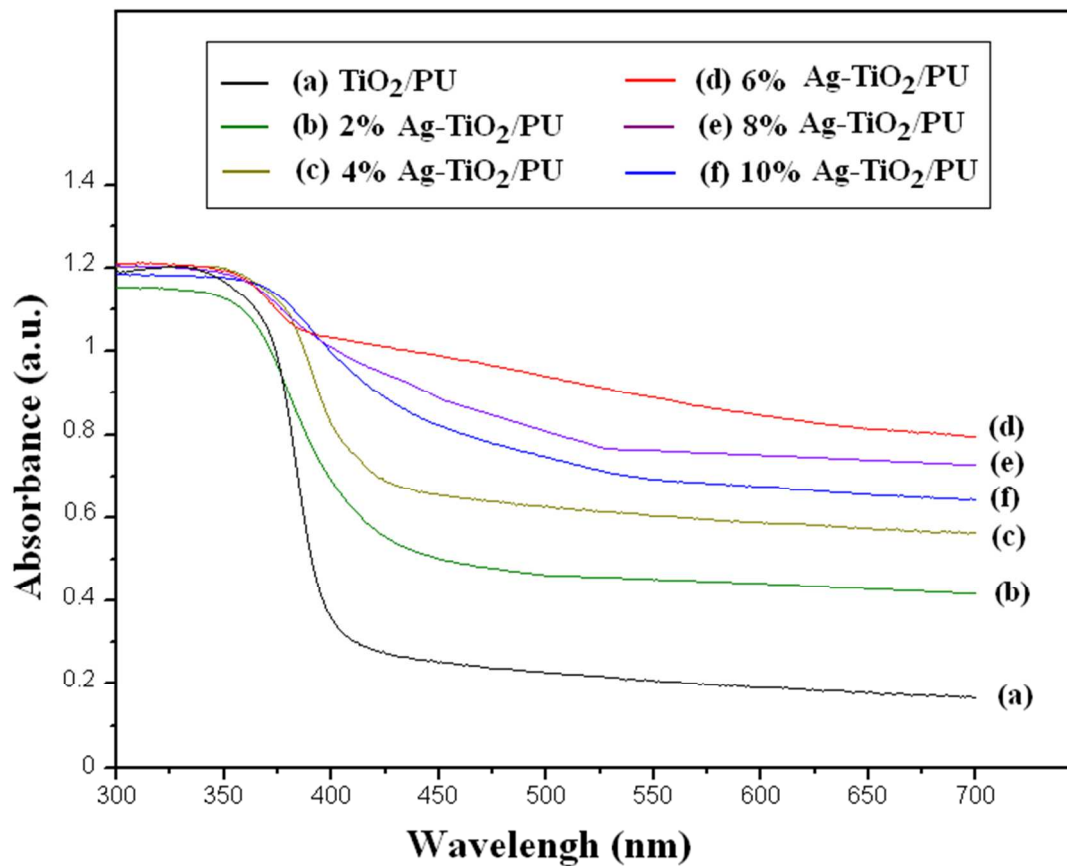


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644 Figure 6: TEM images of TiO_2/PU (A) and $\text{Ag-TiO}_2/\text{PU}$ (B); HRTEM images of the selected645 areas in the TEM images of TiO_2/PU (A1) and $\text{Ag-TiO}_2/\text{PU}$ (B1, B2 and B3).

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Figure 7: UV-Vis absorption spectra of TiO₂/PU and 2, 4, 6, 8 and 10 % Ag-TiO₂/PU

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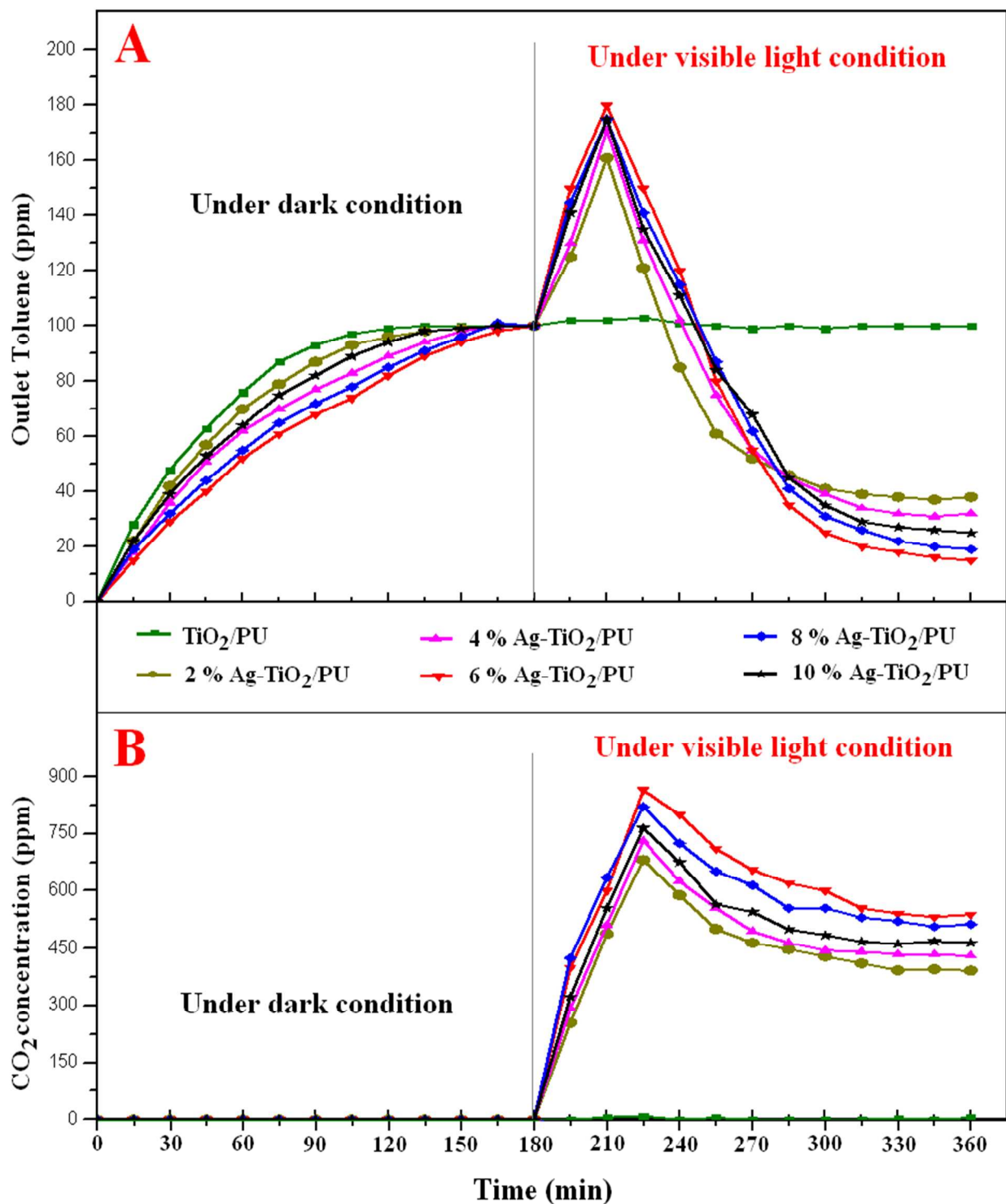
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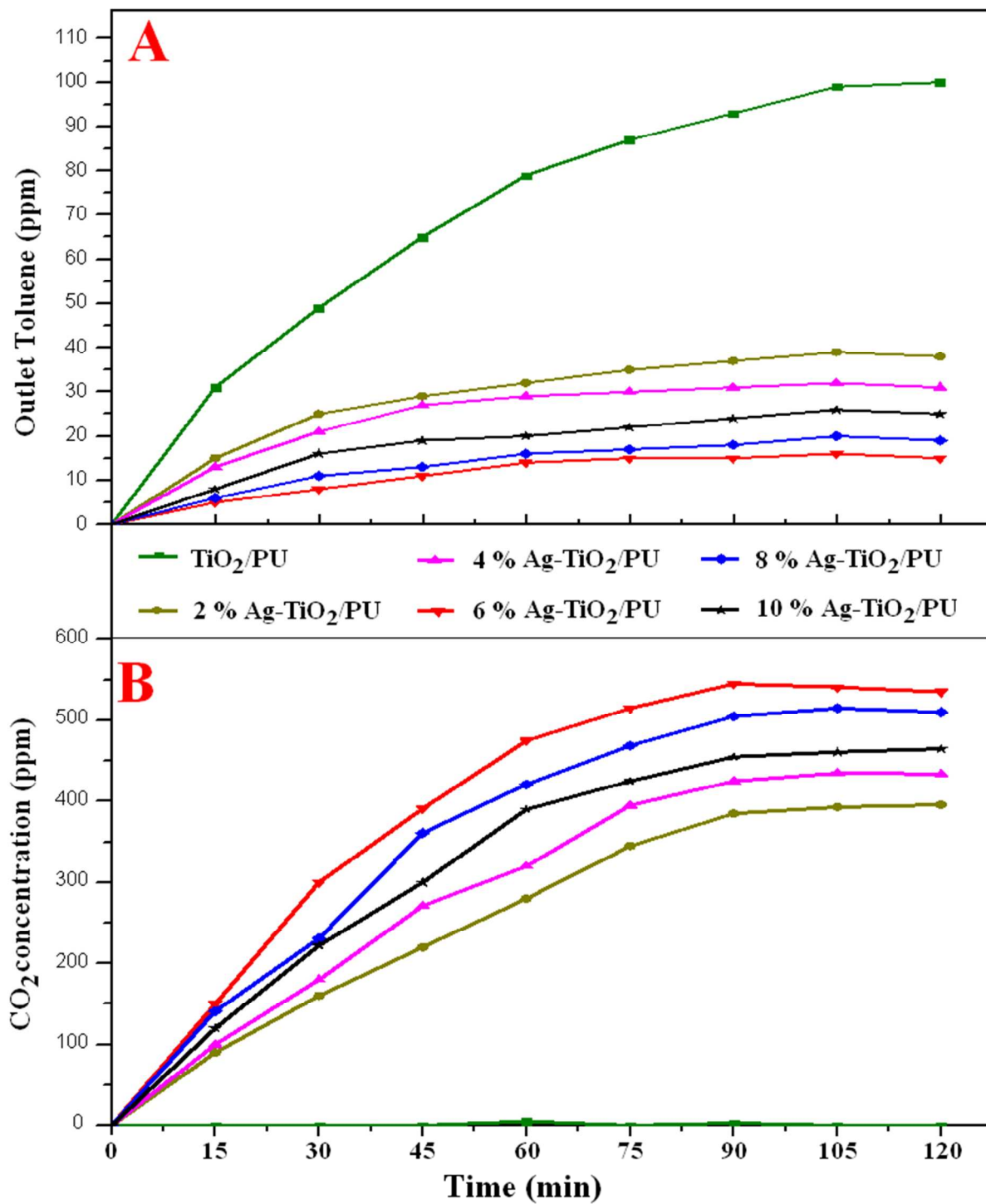
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659 Figure 8: Toluene removal (A) and generated CO_2 concentration (B) by X % $\text{Ag-TiO}_2/\text{PU}$ under

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dark and then visible light conditions

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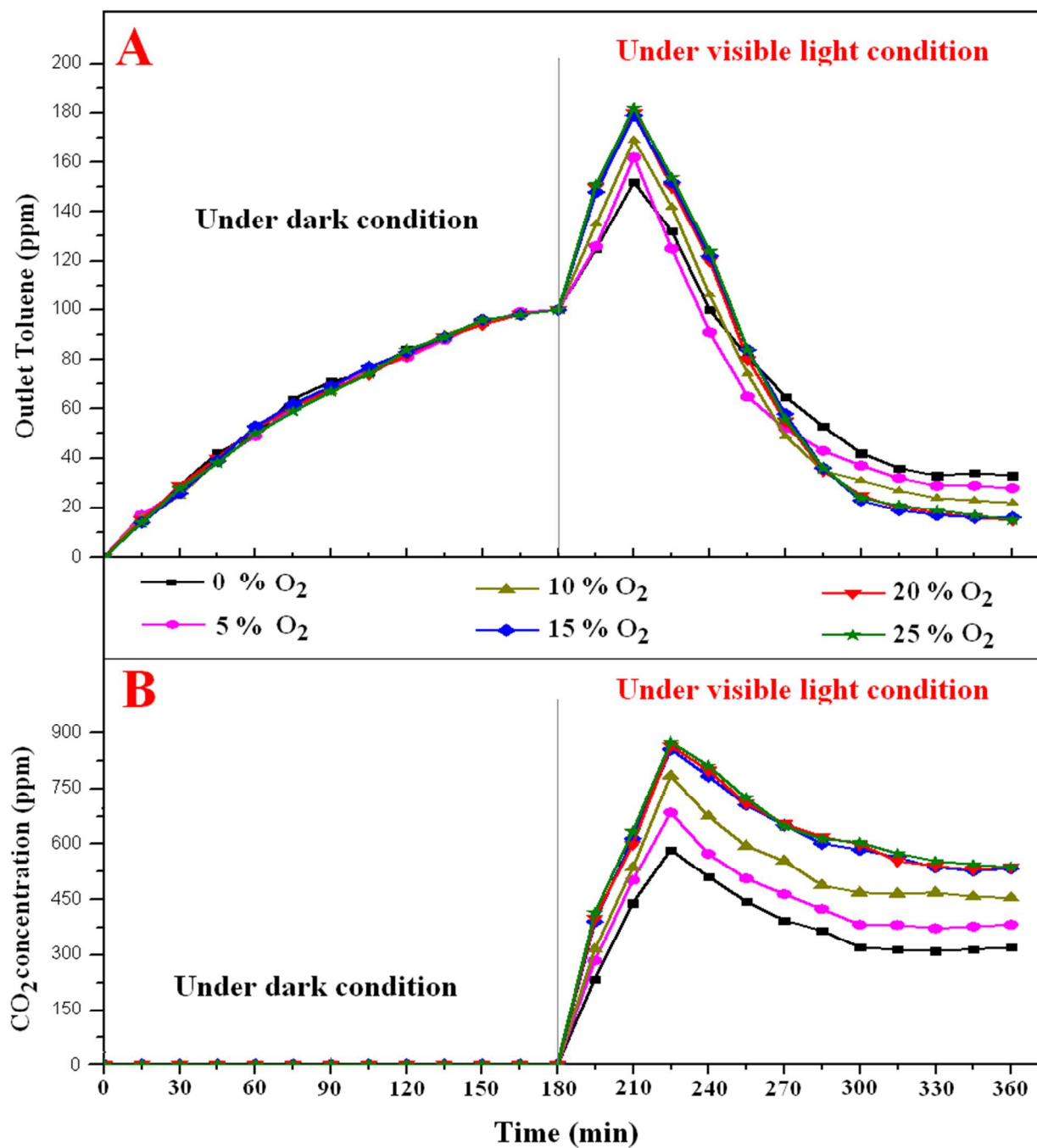


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663 Figure 9: Toluene removal (A) and generated CO₂ concentration (B) by X % Ag-TiO₂/PU under

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visible light conditions



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666 Figure 10: Effect of O₂ content on outlet toluene (A) and generated CO₂ concentration (B)

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passing 6% Ag-TiO₂/PU

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671 **Table captions**

672 Table 1: The ratios of Ag^0/Ag^+ and $\text{Ti}^{3+}/\text{Ti}^{4+}$ and the BET surface area of the Ag-TiO₂/PU
673 materials

674 Table 2: The toluene removal efficiency and the mineralization degree by Ag-TiO₂/PU
675 photocatalysts at different Ag/TiO₂ ratios under visible light conditions

676

677 **Figure captions**

678 Figure 1: The experimental apparatus for removal of gaseous toluene

679 Figure 2: High-resolution XPS spectra of Ag in X % Ag-TiO₂/PU

680 Figure 3: XRD patterns of X % Ag-TiO₂/PU

681 Figure 4: High-resolution XPS spectra of Ti 2p_{3/2} in X % Ag-TiO₂/PU

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683 Figure 6: TEM images of TiO₂/PU (A) and Ag-TiO₂/PU (B); HRTEM images of the selected
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685 Figure 7: UV-Vis absorption spectra of TiO₂/PU and 2, 4, 6, 8 and 10% Ag-TiO₂/PU

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687 dark and then visible light conditions

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689 visible light conditions

690 Figure 10: Effect of O₂ content on outlet toluene (A) and generated CO₂ concentration (B)
691 passing 6% Ag-TiO₂/PU

