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1	Synthesis of levulinic acid-based polyol ester and its influence on
2	tribological behavior as potential lubricant
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8	Abstract

9	Levulinic acid (LA) has been identified by the US Department of Energy
10	as a top platform chemical and regarded as one of the twelve most promising
11	molecules derived from biomass. In this study, it was used to prepare lubricant
12	base stocks by esterification with three different polyols including neopentyl
13	glycol (NPG), trimethylolpropane (TMP), and pentaerythritol (PE) in the
14	presence of sulfuric acid. The crude product was distilled to obtain target
15	product with a purity above 95%. These products of polyol ester were
16	characterized using ¹ H NMR and mass spectral techniques. The lubricant
17	properties, such as kinematic viscosity, viscosity index, pour and flash points,
18	were evaluated using standard ASTM methods. Among the base stocks
19	prepared, TMP-tri-LA ester exhibited superior lubricant properties like good
20	kinematic viscosity at 40°C (87.28) and at 100°C (8.42), viscosity index (48),
21	low pour point (-25 °C), high flash point (238 °C), cloud point (-4 °C) , copper $\frac{1}{1}$

strip corrosion (1a) and Volatility at 120°C (0.41%). Wear prevention
 characteristics of this ester was tested and performed low coefficient of friction
 and small wear scar diameters. It was found that this kind of polyol ester was
 suitable for lubricant base stocks.

5 **Keywords:** Levulinic acid, Polyol esters, Biolubricant, Lubricant properties

6 1. Introduction

7 Biodegradable polyol esters, which served as biolubricant components, have aroused more interest because of their excellent lubricity, biodegradability, 8 viscosity-temperature characteristics, and low volatility.¹ However, natural 9 triglycerides are thermally sensitive at high temperature. The main reason of 10 this phenomenon is the presence of hydrogen atoms on the β position of the 11 glycerol molecule backbone,² since this structural feature is prone to the partial 12 13 fragmentation of the molecule and the formation of unsaturated compounds. The formed compounds under polymerization led to the increase of the liquid's 14 15 viscosity and resulted in the formation of precipitate particles.³ Thus, natural 16 triglycerides are generally not appropriate for the applications of lubricant that 17 require heat resistance. This problem could be easily solved by replacing 18 glycerol with another special polyhydric alcohol which does not contain β hydrogen atoms.^{4,5} In previous literatures, researchers used neopentyl polyols 19 20 such as neopentyl glycol (NPG), trimethylolpropane (TMP) and pentaerythritol (PE) for this purpose.⁶⁻⁸ So far, the investigation of polyol esters biolubricant 21 preparation has been conducted using polyols with various fatty acids by 22

1 transesterification or esterification. Most of fatty acids reported in literature are 2 generally obtained from animal oils such as beef tallow, lard, mutton tallow as 3 well as vegetable oils, such as soybean oil, sunflower oil, rapeseed oil, castor oil, olive oil, palm kernel oil and waste cooking oil.⁹⁻¹⁵ These high 4 5 monounsaturated oils have optimal performance as raw materials to generate 6 environment friendly lubricants with high performance. However, part of these 7 oils are edible, and their use for the production of lubricants will indirectly influence the food demand. Hence, more attention is paid for the preparation of 8 non-edible oil-based polyol esters containing any unusual fatty acids. 9

10 Levulinic acid (LA), having five carbon atoms with carboxyl group and 11 ketone functional groups, can be easily produced from glucose, fructose, starch and lignocellulosic residues.¹⁶ It has been identified by the US Department of 12 13 Energy as a top platform chemical and regarded as one of the twelve most 14 promising molecules derived from biomass, because it can be transformed into a variety of other important compounds in the chemical industry.¹⁷⁻¹⁸ In the 15 1990s, there were some patents about the conversion of LA production from 16 lignocellulose by acid degradation at an elevated temperature and the 17 theoretical yield of LA could reach 55% (molar yield based on hexose polymer 18 content of wood feed) under the optimal condition.¹⁹⁻²⁰ Recent research 19 20 demonstrated that LA could be obtained from cellulose in the presence of catalyst such as functionalized ionic liquids,²¹ dilute acid,²² alkaline-treated 21 zeolite,²³ and Fe/HY catalyst.²⁴ LA produced from cellulose has attracted 22 23 considerable attention and become one of the key steps for the biomass

refining.²¹ Meanwhile, the esterification of levulinic acid with polyols could
easily implemented and the polyol esters based on levulinic acid are expected
to have similar properties of lubricant compared to other polyol esters.
Therefore, there might be broader application prospects for it to produce
biolubricant compared to other vegetable oils.

Hence, this study was aimed at employing levulinic acid and polyols such
as NPG (dihydric), TMP (trihydric) and PE (tetrahydric) for the synthesis of
polyol esters. The potential of the synthesized esters as base stocks for
biodegradable lubricants was also evaluated.

- 10 **2. Materials and methods**
- 11 *2.1. Chemicals*

12 NPG, TMP and PE were obtained from Fuchen Chemical Co. Ltd. 13 (Tianjin, China); levulinic acid (LA) with the purity of 99% was purchased 14 from Adamas Reagent Co., Ltd.; the sulfuric acid with purity of 98% was 15 procured from Beijing Chemical Factory. The other solvents of analytical grade 16 were obtained from Beijing Chemical Factory; mineral oil with similar 17 viscosity of LA-based TMP ester was provided kindly by SINOPEC in Beijing.

18 2.2. Analysis

¹H NMR spectra were obtained using a Bruker AR X 400 Spectrometer
(400, 200 MHz). Mass spectra were recorded on a VG Auto Spec-M
(Manchester, UK) and the compounds including LA, mono-, di- and
trisubstituted esters in the reaction mixture were quantified using a GC-2010

1	gas chromatography (Shimadzu, Japan) equipping with a DB-1ht capillary
2	column (30m × 0.25mm × 0.1µm; J&W Scientific, USA) and a flame ionizing
3	detector (FID). The column temperature was held at 110°C, then heated to
4	132°C at 12°C/min, and to 180°C at 30°C/min and finally to 300 °C at 20
5	°C/min and then maintained for 5min. The temperatures of the injector and
6	detector were both set at 300 °C.
7	2.3. Viscosity
8	Viscosity measurements were conducted at 40°C and 100°C using Cannon
-	
9	Fenske viscometer tubes in a Cannon Constant Temperature Viscosity Bath
9 10	Fenske viscometer tubes in a Cannon Constant Temperature Viscosity Bath (Hunan Petrochemical Instrument CO., LTD.). Viscosity and the viscosity

13 was reported.

12

14 *2.4 Pour point*

Pour points were determined by ASTM method D97 with an accuracy of
±3°C an using Automatic Pour Point Tester, manufactured by Hunan
Petrochemical Instrument CO., LTD.. All runs were carried out in duplicate.
Sample temperature was measured in 3°C increments at the top of the sample
until it stopped pouring.

All viscosity measurements were carried out in triplicate, and the average value

20 *2.5 Flash point*

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Flash point of the products was determined using a Flash Point Tester (Hunan Petrochemical Instrument CO., LTD.) according to ASTM D93 method. The lowest temperature for application of the test flame, which caused the vapor above the surface of the liquid to ignite, was taken as the flash point of the product at ambient barometric pressure.

6 *2.6 Cloud point*

7 Cloud points were determined by standard ASTM D2500 using Cloud Point

8 Apparatus (Beijing Timepower Measure and Control equipment CO., LTD.).

9 2.7 Copper strip corrosion

10 Copper strip corrosion was determined using Copper Strip Corrosion Tester 11 (Beijing Timepower Measure and Control equipment CO., LTD.). The 12 appearance of the Cu strip was assessed by comparison with Copper Strip 13 Corrosion Standards (ASTM D130).

14 *2.8 The volatility determination*

15 The volatility was determined in agreement with ASTM method D6184 in16 an electrical stove using glass pans of 4 cm in diameter.

17 2.9Themogravimetric analysis (TGA)

18 Themogravimetric analysis (TGA) is a measure to evaluate the thermal 19 stability of materials. A higher TGA onset temperature represents a higher 20 thermal stability of a material. Thermal behavior of the LA-based polyol esters 21 were studied using a PerkinElmer thermo gravimetric differential thermal

3 2.10HFRR (High frequency reciprocating rig) configuration

4 The HFRR wear test was used to investigate the effect of ester under fluid 5 film lubrication as shown in Figure 1. The HFRR test (ASTM D6079) used in 6 this study involves a weighted cast iron pin cylinder (6 mm length) and a 7 stationary cast iron plat (15 mm*15 mm), which is completely submerged in a 8 10 ml of sample. The ball and disk is tested at room temperature and brought 9 into contact with each other and the entire apparatus is vibrated at 50 Hz for 75 10 min with the load 200g. The sliding stroke is maintained at 2 mm. Several 11 blends of LA-based TMP ester including 1%, 3%, 7%, 10%, 20% and 100%, 12 are tested and analyzed. Each test was carried out three times repeatedly to 13 observe any errors need to be analyzed.

- 14 2.11 Synthesis methods
- 15 2. 11.1 Preparation of NPG diester of LA (NPG-di-LA)

16 Synthesis of NPG-di-LA was according to Figure 2 (A), and the catalyst 17 was sulfuric acid. The reaction was performed in a temperature controlled 18 reactor with mechanical stirring. The reaction mixture contained 500.00g 19 (4.30mol) LA and 149.15g (1.43mol) NPG. It was incubated for 2h at 95°C in 20 presence of 6.49g sulfuric acid (1% of total mixture). The process of the

1	reaction was monitored by GC, and after completion of the reaction, the crude
2	product was distilled by Rotary Film Molecular Distillation (VTA GMBH &
3	Co. KG, Germany) at 140°C and 1mbar to remove sulfuric acid and excess LA.
4	After that, the obtained product from the first distillation was distilled once
5	again at 170°C and 0.3mbar to get the final NPG-di-LA product with purity of
6	96.21%. The structure of the target product was characterized by ¹ HNMR and
7	mass studies.
7 8	mass studies. ¹ H NMR (CDCl ₃ , δ ppm): 0.97 [s, 6H, 2×(-CH ₃)], 2.21 [s, 6H, 2×(-CO-
8	¹ H NMR (CDCl ₃ , δ ppm): 0.97 [s, 6H, 2×(–CH ₃)], 2.21 [s, 6H, 2×(–CO–
8 9	¹ H NMR (CDCl ₃ , δ ppm): 0.97 [s, 6H, 2×(–CH ₃)], 2.21 [s, 6H, 2×(–CO– CH ₃)], 2.59-2.62 [m, 4H, 2×(–CO–CH ₂ –)], 2.76-2.79 [s, 4H, 2×(–CH ₂ –CO-)],

12 Synthesis of TMP-tri-LA was according to Figure 2 (B), and the catalyst 13 was sulfuric acid. The reaction was performed in a temperature controlled reactor with mechanical stirring. The reaction mixture including 500.00g 14 15 (4.30mol) LA and 144.43g (1.08mol) TMP. It was incubated for 2h at 95°C in 16 presence of 6.44g sulfuric acid (1% of total mixture). The process of the 17 reaction was monitored by GC, and after completion of the reaction, the crude 18 product was distilled by Rotary Film Molecular Distillation (VTA GMBH & 19 Co. KG, Germany) at 140°C and 1mbar to remove sulfuric acid and excess

1	LA. Thereafter, the obtained product from the first distillation was distilled
2	once again at 230°C and 0.009mbar to get the final TMP-tri-LA with purity of
3	95.82%. The structure of the target product was characterized by ¹ HNMR and
4	mass studies.
5	¹ H NMR (CDCl ₃ , δ ppm): 0.89-0.92 [s, 3H, (–CH ₃)], 1.48-1.50 [s, 2H, (–
6	CH ₂ -CH ₃)], 2.20 [s, 9H, 3×(-CO-CH ₃)], 2.58-2.60 [s, 6H, 3×(-CO-CH ₂ -)],

- 7 2.76-2.79 [s, 6H, 3×(-CH₂-CO-)], 4.03 [s, 6H, 3×(-CO-CH₂-)]; ESI MS: m/z
 8 451.20 [M+Na]⁺.
- 9 2. 11.3 Preparation of PE tetraester of LA (PE-tetra-LA)

10 Synthesis of PE-tetra-LA was according to Figure 2 (C), and the catalyst 11 was sulfuric acid. The reaction was performed in a temperature controlled 12 reactor with mechanical stirring. The reaction mixture contained 500.00g 13 (4.30mol) LA and 117.24g (0.86mol) TMP. It was incubated for 12h at 115°C in presence of 6.17g sulfuric acid (1% of total mixture). The process of the 14 15 reaction was monitored by GC, and after completion of the reaction, the crude 16 product was distilled by Rotary Film Molecular Distillation (VTA GMBH & 17 Co. KG, Germany) at 140 °C and 1mbar to remove sulfuric acid and excess LA. 18 Afterward, the obtained product from the first distillation was distilled once 19 again at 290 °C and 0.0085mbar to get the final TMP-tri-LA product with

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purity of 95.01%. The structure of the target product was characterized by
 ¹HNMR and mass studies.
 ¹H NMR (CDCl₃, δ ppm): 2.19 [s, 12H, 4×(-CO-CH₃)], 2.57-2.60 [s, 8H,
 4×(-CO-CH₂-)], 2.75-2.78 [s, 8H, 4×(-CH₂-CO-)], 4.12 [s, 8H, 4×(-CO CH₂-)]; ESI MS: m/z 551.21 [M+Na]⁺.

6 3. Results and discussion

7 3.1 Characterization and physico-chemical properties of esters

8 Polyol esters, derived from esterification or transesterification using plant 9 oils and animal oils with neopentyl polyols without hydrogen atoms on the β carbon, have been widely used for lubricants. Due to their superior physico-10 11 chemical properties and performances compared with mineral oils, its 12 applications have expanded largely. The present study was focused on the use 13 of non-edible levulinic acid, a promising platform chemical derived from 14 biomass, combined with dihydric, trihydric and tetrahydric alcohols named 15 NPG, TMP and PE respectively to produce LA-based polyol esters. The polyol 16 esters based on levulinic acid were expected to have similar properties of 17 lubricant compared with other polyol esters.

18 The purity of the levulinic acid-based polyol esters was determined by GC19 analysis and found to exceed 95%. The structures of polyol esters were

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pour point and the number of branches in molecule.²⁵⁻²⁶

confirmed using ¹ H NMR (Figure 4) and ESI-MS (Figure 3) spectral studies.		
The molecular ions 323.15 [M+Na] ⁺ , 451.20 [M+Na] ⁺ , 551.21 [M+Na] ⁺		
correspond to compounds NPG-di-LA; (B) TMP-tri-LA; (C) PE-tetra-LA,		
respectively. All the products were characterized for their physico-chemical	Ot	
properties, such as viscosity at 40°C and 100°C, viscosity index (VI), pour		
point, flash point, cloud point and copper strip corrosion (Table 1).	N S	
Kinematic viscosity is an important characteristic to exhibit the	ances Accepted Manuscri	
relationship between viscosity and temperature. The property of the viscosity–	D	
temperature directly represents lubricant's performance and determines its	pte	
application. Table 1 showed the kinematic viscosities of different ester		
products. The NPG-di-LA, TMP-tri-LA and PE-tetra-LA exhibited their	A	
kinematic viscosity at 40 °C in the range of ISO VG10, reaching 17.29, 87.28	COC	
and 417.45, respectively. At 100°C their kinematic viscosities were 3.35, 8.42	an	
and 19.14 cSt. Viscosity of the polyol ester base fluids generally increases with		
the increase of the number of present acyl functionalities. ²⁵ In this study, the	5	
the increase of the number of present acyl functionalities. ²⁵ In this study, the LA based esters prepared with NPG, TMP and PE exhibited similar trend with		
the result of Gryglewicz's and Padmaja's in term of the relationship between		

The viscosity index (VI) is an another parameter generally used for

1	evaluating the performance of a potential lubricant. By detecting the value of
2	viscosity index, variation of the kinematic viscosity with temperature can be
3	known. Generally, the higher its value, the lower variation of viscosity with the
4	temperature, and so the better performance of the lubricant. Table 2 also
5	showed the property of NPG-di-LA, TMP-tri-LA, PE-tetra-LA with viscosity
6	index 30, 48 and 15, respectively. As a high viscosity index means there was
7	little change over a wide temperature range. The performance of the three
8	synthesized esters need futher improvement to become lubricant with high
9	viscosity index which was a desirable property for a lubricant by adding
10	additives in formulated lubricants. The low viscosity index can also be
11	overcome by increasing the molecular weight of the products and altering the
12	structure of their molecules, especially the introduction of double bond in their
13	composition. ^{27,28} The reaction between LA and furfural, which is also a
14	platform chemical from lignocellulosic residues, can be easily implemented in
15	aq. NaOH. ²⁹ The product, 6-furfurylidene levulinic acid, can be used to prepare
16	biolubricant base stocks by esterification with polyols. This kind of polyol
17	esters contains the double bond and the molecular weight is higher than
18	levulinic acid-based polyol esters. So the viscosity index could be improved
19	obviously.

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2	Pour point is an another key parameter to assess the performance and
3	application of a potential lubricant. It is the temperature that a lubricant can't
4	flow when a jar is tilted during cooling environment. Lubricants with a low
5	pour point is conducive to the operation of the engine in cold temperature
6	climates. The pour point of ester products in this study was measured by
7	ASTM D97. Generally, pour points of polyol esters prepared from unsaturated
8	fatty acids were very low, and a similar trend was observed in term of the pour
9	points of NPG-di-LA (-34 °C), TMP-tri-LA(-25 °C) and PE-tetra-LA (-8 °C).
10	It was found that the pour point of NPG-di-LA with less number of acyl chains
11	was lower compared to other polyols, which could be due to more effective
12	disruption of molecules packing compared to PE and TMP esters. However, the
13	pour point of PE-tetra-LA was high. It suggested that the molecular
14	configuration of NPG and TMP esters was more effective at disrupting
15	molecule packing compared to PE ester. Such low pour points were useful for
16	applications in machine tool and hydraulic systems. ³⁰ Compared with recent
17	researches which reported the pour points of other fat acid-based polyol esters,
18	the NPG-di-La and TMP-tri-LA ester exhibited competitive characteristic of
19	lower temperature, it's pour points lower than product (pour point -27 °C) from

castor oil and TMP ¹² and that of the polyol ester (pour point -18 °C) from
 rapeseed oil and TMP, ³² and polyol ester (pour point -6 °C) from rubber seed
 oil and TMP. ³³

4 The flash point is defined as the minimum temperature at which the liquid produces a sufficient concentration of vapor above it that it forms an ignitable 5 mixture with air. The lower flash point is, the greater fire hazard. The TMP-tri-6 7 LA ester possessed excellent thermal stability with flash points at 228°C followed by PE-tetra-LA ester at 210°C and NPG-di-LA at 185°C. The TMP-8 9 tri-LA ester had higher thermal stability followed by NPG-di-LA and PE-tetra-LA esters. This trend was different from other synthetic esters.³¹ Flash points of 10 all the polyol esters were found to be very high within the range of 185–228 °C, 11 and the esters with flash point $\geq 165^{\circ}$ C lie well within the range of hydraulic 12 oils.³⁴ 13

14 Cloud point was the temperature at which liquid becomes cloudy in 15 appearance. A high cloud point could lead to filter plugging and poor 16 pumpability in cold weather applications. Among the new three kinds of esters 17 in this paper, NPG-di-LA had the lowest cloud point, which reached -11 oC 18 and even lower. The cloud point of TMP-tri-LA was -4 °C followed by 7 °C of 19 PE-tetra-LA.

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1	Copper corrosion test was also conducted in order to measure the
2	tendency to cause metal deterioration. The result indicated that three kinds of
3	the levulinic acid-based polyol esters were class 1a (slight tarnish). The term
4	"class" represents the property of copper corrosion, and it is judged according
5	to the color of the copper strip. The lower the copper corrosion property the
6	lower the "class" of the oil. 1a was the lowest class in Copper Strip Corrosion
7	Standards (ASTM D130). Thus, all the esters in this study had low corrosion
8	on metal materials.
9	The volatility relates to the potential loss of lubricant and to the
10	environmental impact of the volatile components of the fluid. Both European
10 11	environmental impact of the volatile components of the fluid. Both European and U.S. OEM and industry organizations include volatility in their
11	and U.S. OEM and industry organizations include volatility in their
11 12	and U.S. OEM and industry organizations include volatility in their specifications. ³⁵ In this study, NPG-di-LA, TMP-tri-LA and PE-tetra-LA
11 12 13	and U.S. OEM and industry organizations include volatility in their specifications. ³⁵ In this study, NPG-di-LA, TMP-tri-LA and PE-tetra-LA exhibited very low volatility with only 0.57%, 0.41% and 0.33% of weight
11 12 13 14	and U.S. OEM and industry organizations include volatility in their specifications. ³⁵ In this study, NPG-di-LA, TMP-tri-LA and PE-tetra-LA exhibited very low volatility with only 0.57%, 0.41% and 0.33% of weight loss at 120 °C, respectively. The loss of three kinds of the levulinic acid-based
11 12 13 14 15	and U.S. OEM and industry organizations include volatility in their specifications. ³⁵ In this study, NPG-di-LA, TMP-tri-LA and PE-tetra-LA exhibited very low volatility with only 0.57%, 0.41% and 0.33% of weight loss at 120 °C, respectively. The loss of three kinds of the levulinic acid-based polyol esters due to high-temperature volatility was found to decrease steadily

TGA is a measure to evaluate the thermal stability of materials. Generally,

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1	the higher T_{onset} of a material, the higher is its thermal stability. In previous
2	literatures, some researchers have used this method to measure the thermo-
3	oxidative stability of oils. ³⁶⁻³⁷ According to the TGA analytical results as
4	shown in Figure 5, TGA curves of all samples had similar behavior. The
5	accurate analysis of TGA curves was summarized in Table 2. It was also
6	found that the three prepared levulinic acid-based polyol esters possessed
7	good thermal stability. NPG-di-LA, TMP-tri-LA, and PE-tetra-LA were
8	thermally stable with less than 4% mass weight loss below the temperature of
9	189°C, 255°C and 222°C, respectively. Besides, about 9-10% of weight loss
10	was observed for each sample within the temperature range of 203-205°C,
11	281-286°C and 252-259°C, respectively. The weight loss of the NPG-di-LA,
12	TMP-tri-LA, and PE-tetra-LA reached 97% when each of the temperature
13	achieved 579, 487 and 684°C, respectively. Then, there was no further loss of
14	weight with any increasing temperature. It is known that levulinic acid-based
15	polyol esters are not susceptible to undergo autoxidation reactions. While
16	these TGA measurements provided a preliminary estimate of the stability of a
17	lubricant, further chemical studies would be necessary to check for the
18	stability and functions in these lubricants.

19

Among the three levulinic acid-based polyol esters, TMP ester exhibited

1	superior properties such as pour point, viscosity index and oxidation stability
2	which were similar to that of TMP trioleate. ³⁸ Due to its high viscosity index,
3	high thermal stability and low pour point, TMP-tri-LA ester could be
4	considered as a potential biodegradable lubricant base stock.

5 3.2 Tribological properties of TMP-tri-LA

6 *3.2.1 Coefficient of friction (COF)*

7 Figure 6. showed the friction coefficient plotted against the sliding time for various percentages of TMP-tri-LA biolubricants. The results of the figure 8 9 depict that the value of friction coefficient ranged from 0.007 to 0.17. For ordinary mineral oil (0% ester), it can be seen that the coefficient of friction 10 11 which is 0.15 on average is the highest within the operation time. For samples 12 of 3%, 7%, 10%, 20% TMP-tri-LA in mineral oil, the coefficient of friction 13 was higher at the beginning and then it fell down rapidly. The 100% TMP-tri-LA kept constantly low coefficient of friction which was 0.09 on average 14 15 within the operation time. A considerable improvement of friction coefficient 16 was observed with addition of TMP-tri-LA ester in ordinary mineral oil. This 17 phenomena was consistent with Madankara's work which claimed that friction coefficient was reduced significantly by adding hydroxy ester product to diesel 18 fuel.³⁹ The TMP-tri-LA component of biolubricants formed multi and mono 19

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layer on the surface of the rubbing zone and make stable film to prevent the
 contact between the surfaces.

3 *3.2.2 Wear scar diameter (WSD)*

The frictional wear results by the addition of different percentages of 4 5 TMP-tri-LA ester to mineral oil were studied using HFRR apparatus. Microscope images of wear scar generated on the surface of a test sample were 6 showed in Figure 7 when different percentages of TMP-tri-LA in ordinary 7 mineral oil were used as lubricant contact fluids. It is evident in Figure 8, the 8 9 highest wear scar diameter of 300µm was generated when 1% ester in ordinary mineral oil. The ordinary mineral oil (0% ester) has generated a wear scar 10 diameter of 291µm. There was a significant reduction in wear scar diameter 11 with a higher percentages of TMP-tri-LA in ordinary mineral oil. The 12 significance improvement in wear scar diameter of 132µm was found for the 13 14 100% TMP-tri-LA product. It was reported in previous researches that TMP 15 esters of palm and palm kernel (*E.gue-neensis*) oil had resulted in wear scar diameters of 200–350µm and 200–400µm, respectively.⁴⁰ Comparatively, the 16 17 TMP-tri-LA ester exhibited superior lubricity performance comparing with other biolubricants. 18



The possible mechanism by which the friction was reduced was that the

1	uniform molecule structure of TMP-tri-LA ester formed a monolayer film in
2	the contact area with the addition of different percentages of ester to mineral
3	oil.of lubrication is the good monolayer film formed by the uniform molecule
4	structure of TMP-tri-LA ester in the contact area with the addition of different
5	percentages of ester to mineral oil. Basically, poyol esters are well known that
6	they can provide good lubricity because of its uniform molecule structure. ^{41,42}
7	Fatty acids used to synthesize poyol esters have longer branched chains than
8	ordinary mineral oil. This kind of molecule structure offers formation of good
9	monolayer film on sliding surface. The second possible mechanism of
10	lubrication is the polarity of molecule of TMP-tri-LA ester that contributes to
11	better lubricity characteristic. The property of the molecular structure of the
12	polyol ester is a polar at one end and non-polarity at the other end. The reason
13	that friction was reduced as percentages of ester to mineral oil increased is that
14	molecular adsorption on the surface of metal was enhanced. The friction was
15	reduced as percentages of ester added to mineral oil increased was resulted
16	from the enhancement of molecular adsorption on the surface of metal. One
17	end of the molecular was attracted strongly to metal surface due to the polarity
18	and the other one end was extended out. This distribution of moleculars in the
19	mixture samples produced a strong barrier to avoid direct friction between two

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surfaces. ^{43,44,45} So, there is a significant reduction in wear scar diameter with
addition of TMP-tri-LA ester in ordinary mineral oil. This phenomena was
consistent with other researchers' results that wear scar diameter got smaller
and friction was reduced obviously when carboxylate group in ester and the
polarity increased in the ordinary mineral oil. ^{46,47}

6 4. Conclusions

LA was a promising derivative derived from biomass. In this study, a new 7 kind of levulinic acid-based polyol esters was prepared by esterification of 8 9 levulinic acid with three different kinds of polyol. The crude product was distilled to obtain target product with purity of above 95%. Among the three 10 polyol esters obtained in this study, TMP-tri-LA ester exhibited superior 11 12 properties of lubricant like good viscosity index, low pour point, high flash point, low cloud point and copper strip corrosion, low volatility. The 13 biolubricity of TMP-tri-LA ester was tested on a High Frequency 14 15 Reciprocating Rig (HFRR) apparatus. The result exhibited that this kind of 16 biolubricant performed low coefficient of friction and wear scar diameters. It 17 suggested that this kind of polyol ester could be regarded as potential base 18 stocks for production of lubricant with high performance.

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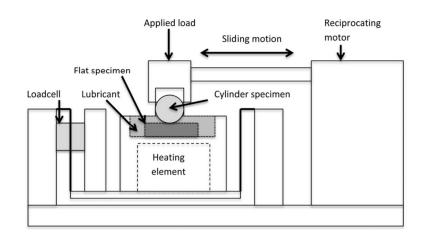


Fig. 1. The schematic diagram of HFRR wear test.

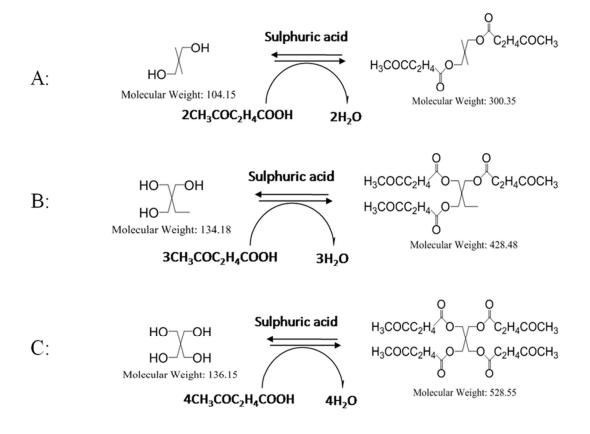


Fig. 2. Schematic representation of esterification reaction between LA and NPG, TMP, PE, respectively.

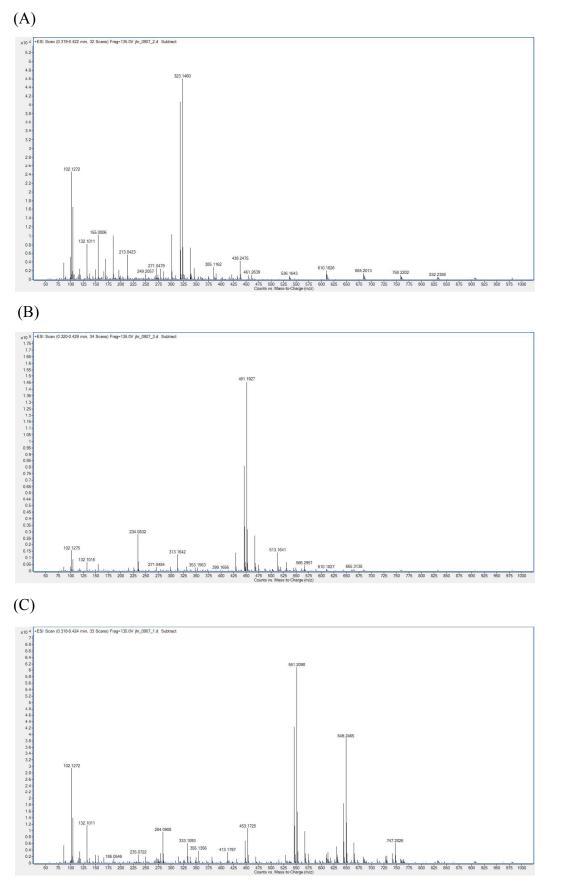


Fig. 3. Mass spectra of levulinic acid-based polyol esters : (A) NPG-di-LA; (B) TMP-tri-LA;

(C) PE-tetra-LA.

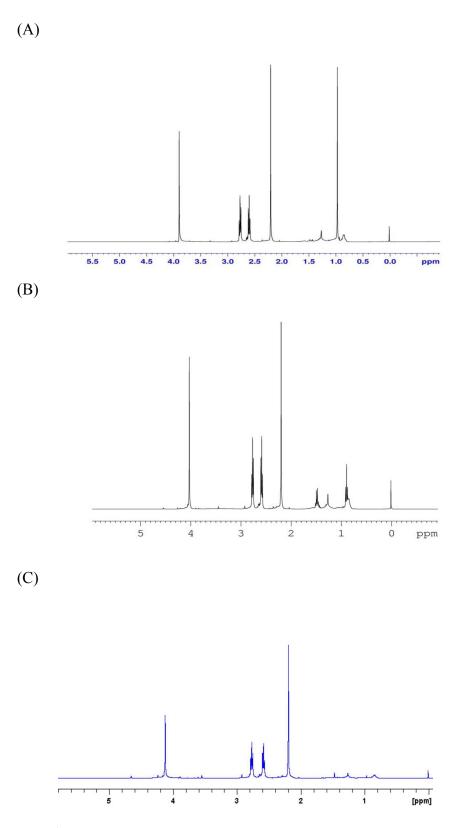


Fig. 4. ¹H NMR spectra of levulinic acid-based polyol esters : (A) NPG-di-LA; (B) TMP-tri-LA; (C)

PE-tetra-LA.

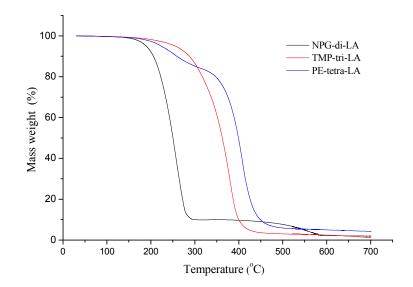


Fig. 5. The TGA curves of of LA-based polyol esters.

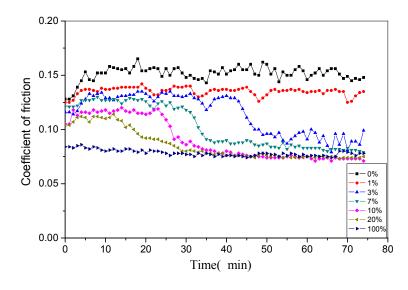


Fig. 6. Variation in coefficient of friction different percentages of TMP-tri-LA in ordinary mineral oil.

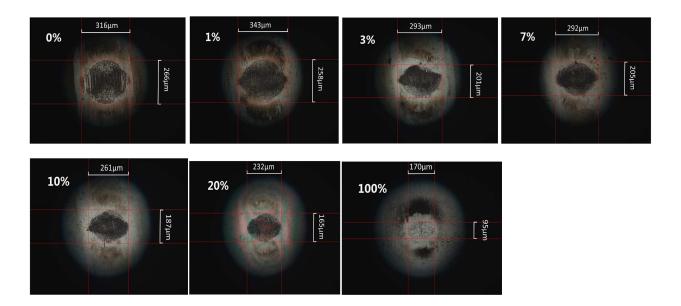


Fig. 7. Microscope of wear scar with different percentages of TMP-tri-LA in ordinary mineral oil.

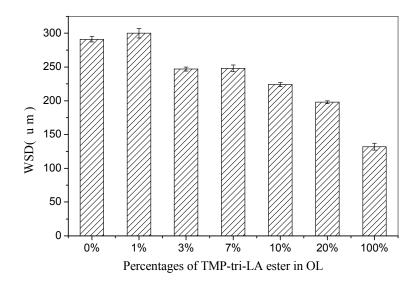


Fig. 8. Wear scar diameter of different percentages of TMP-tri-LA in ordinary mineral oil.

Property	NPG-di-LA	TMP-tri-LA	PE-tetra-LA
Viscosity at 40 $^{\rm o}{\rm C}$, (mm^2/s)	17.29	87.28	417.45
Viscosity at 100 $^{\rm o}C,~$ ($mm^2\!/s$)	3.35	8.42	19.14
Viscosity index	30	48	15
Pour point (°C)	-34	-25	-8
Flash point (°C)	185	228	210
Cloud point (°C)	-11	-4	7
Copper strip corrosion	1a	1a	1a
Volatility at 120 °C (%)	0.57	0.41	0.33

Table 1 Physico-chemical properties of LA-based polyol esters.

Product	$T_{\text{onset}}(\circ \mathbf{C})$	9–10% wt loss (°C)	97% wt loss (°C)
NPG-di-LA	189	203-205	579
TMP-tri-LA	255	281-286	487
PE-tetra-LA	222	252-259	684

Table 2 Thermal stability data of the ester products.