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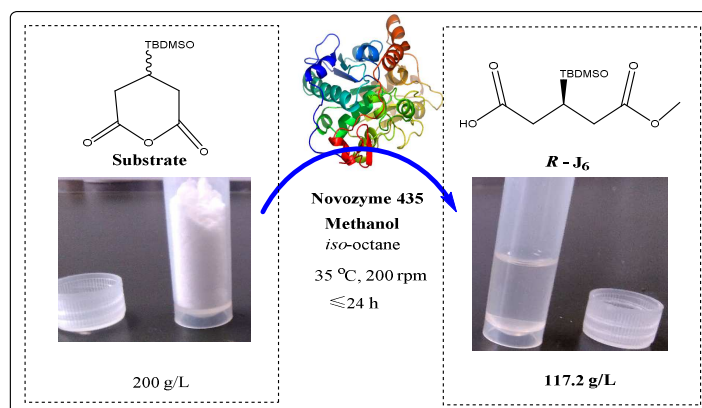
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## Green synthesis of (*R*)-3-TBDMSO glutaric acid methyl monoester using *Novozym* 435 in non-aqueous media

An efficient biocatalytic synthesis of (*R*)-3-TBDMSO glutaric acid methyl monoester (*R*-J<sub>6</sub>), an important intermediate in the synthesis of rosuvastatin, has been developed using a green catalytic route in the presence of lipase, conducted under mild conditions. Enzymes screening indicated *Novozym* 435 to be the most efficient biocatalyst for *R*-J<sub>6</sub> synthesis. Methanol was identified as the best acyl acceptor by molecular docking. The *R*-J<sub>6</sub> titer was up to 117.2 g/L with a yield of 58.6%, and productivity of 4.88 g/L/h. The key factor affecting the yield of *R*-J<sub>6</sub> was the molar ratio of methanol to substrate found by an orthogonal array. The route avoids the use of expensive and polluting chemical reagents, requires only a single step. The desired products can be isolated, purified, and dried easily, and the organic solvents can be recycled by vacuum distillation with no wastewater discharge. This green method holds promise for the preparation of kilogram quantities of (*R*)-3-substituted glutaric acid monoesters.



Green synthesis of (*R*)-3-TBDMSO glutaric acid methyl monoester using *Novozym* 435 by alcoholysis of 3-substituted glutaric anhydride.

# Green synthesis of (*R*)-3-TBDMSO glutaric acid methyl monoester using *Novozym 435* in non-aqueous media

Hongjiang Wang<sup>1,2,3</sup>, Zebiao Li<sup>4</sup>, Xiaoxia Yu<sup>1,2,3</sup>, Xiulai Chen<sup>1,2,3</sup>, Liming Liu<sup>1,2,3,\*</sup>

<sup>1</sup> State Key Laboratory of Food Science and Technology, Jiangnan University, 1800 Lihu Road, Wuxi, Jiangsu 214122, China

<sup>2</sup> The Key Laboratory of Industrial Biotechnology, Ministry of Education, Jiangnan University, 1800 Lihu Road, Wuxi, Jiangsu 214122, China

<sup>3</sup> Laboratory of Food Microbial-Manufacturing Engineering, Jiangnan University, 1800 Lihu Road, Wuxi, Jiangsu 214122, China

<sup>4</sup> Nantong Chanyoo Pharmatech Co., Ltd. Coastal economic development zone, No.2 Tonghaisi Road, Rudong county, Nantong, Jiangsu 226407, China

\* Correspondence and requests for materials should be addressed to Liming Liu (E-mail address: mingll@jiangnan.edu.cn)

Tel: +86-0510-85197875;

Fax: +86-0510-85197875.

Postal address: State Key Laboratory of Food Science and Technology, Jiangnan University, 1800 17 Lihu Road, Wuxi 214122, China

## Abstract

An efficient biocatalytic synthesis of (*R*)-3-TBDMSO glutaric acid methyl monoester (*R*-J<sub>6</sub>), an important intermediate in the synthesis of rosuvastatin, has been developed using a green catalytic route in the presence of lipase, conducted under mild conditions without additional chiral reagents. Enzyme screening indicated *Novozym 435* to be the most efficient biocatalyst for *R*-J<sub>6</sub> synthesis. Methanol, which was the most effective alcohol for synthesis of *R*-monoester, was identified as the best acyl acceptor by molecular docking. The optimal conditions for synthesis of *R*-J<sub>6</sub> were as follows: 50 g/L catalyst, 3:1 molar ratio of methanol:substrate, 200 g/L substrate, *iso*-octane as solvent, orbital shaking at 200 rpm, and an incubation time of 24 h at 35 °C. The key factor affecting the yield of *R*-J<sub>6</sub> was the molar ratio of methanol to substrate found by an orthogonal array experimental design. Consequently, the desired product, *R*-J<sub>6</sub>, was afforded with a titer of 117.2 g/L, a yield of 58.6 %, and productivity of 4.88 g/L/h. This green method holds promise for the preparation of kilogram quantities of (*R*)-3-substituted glutaric acid monoesters.

35

36 **Keywords:** Novozym 435, non-aqueous media, (*R*)-3-TBDMSO glutaric acid methyl ester,  
37 esterification, enzymatic catalysis, green chemistry, desymmetrization.

38

## 39 1. Introduction

40 Statins are a class of pharmaceuticals that inhibit the enzyme  
41 hydroxymethylglutaryl-CoA reductase (HMGR) and are widely used as hypolipidemic  
42 agents to lower the level of cholesterol in the blood.<sup>1</sup> Clinical trials have confirmed that  
43 statins can adjust blood lipid levels<sup>2,3</sup> and reduce the risk of fatal and nonfatal cardiovascular  
44 disease.<sup>4</sup> In particular, rosuvastatin, the so-called “super statin”, has high efficacy, few  
45 side-effects, low toxicity, and outstanding selectivity. Dose-for-dose, rosuvastatin is by far  
46 the most efficacious statin for reducing plasma low-density lipoprotein (LDL) cholesterol,  
47 reducing total cholesterol significantly, and the duration of inhibition is longer than for other  
48 statins such as atorvastatin, simvastatin, and pravastatin.<sup>5, 6</sup> The market for  
49 cholesterol-lowering drugs is the largest in the pharmaceutical sector,<sup>7</sup> and industrial  
50 production of rosuvastatin is significant. Sales of rosuvastatin remain in the world's top ten,  
51 with annual sales of \$5.3 billion recorded in 2013.<sup>8</sup>

52 Current industrial production of rosuvastatin is mainly by chemical synthesis,<sup>9, 10</sup> in  
53 which the pyrimidine nucleus and chiral side chain are condensed using the Wittig reaction.<sup>11</sup>  
54 The chiral side chain acts as the functional group, presenting the pharmacophore for HMGR  
55 recognition.<sup>12</sup> (*R*)-3-substituted glutaric acid monoesters are important intermediates for the  
56 assembly of the chiral side chain. In recent years, several effective methods have been used  
57 for the preparation of (*R*)-3-substituted glutaric acid monoesters, including chemical  
58 synthesis,<sup>12</sup> enzymatic methods<sup>13</sup> and chiral resolution.<sup>14</sup> Industrial production of  
59 (*R*)-3-substituted glutaric acid monoesters is mostly by chemical synthesis.<sup>12, 15, 16</sup> Green  
60 synthetic routes involving renewable raw materials and the replacement of environmentally  
61 “unfriendly” syntheses are receiving increasing attention. However, chemical syntheses of  
62 3-substituted glutarates require extreme conditions, such as low temperature ( $-78\text{ }^{\circ}\text{C}$ )<sup>12</sup> and  
63 expensive reagents (benzyl (*R*)-(-)-mandelate and  $\text{Pd}(\text{OH})_2\text{-C}$ )<sup>15, 17</sup> containing heavy-metals.  
64 , which affects the quality of the chiral end-product, and high energy consumption; And the

65 poor extraction and expensive additional purification steps made the whole process  
66 costly, which made the method unsuitable for large-scale *R*-J<sub>6</sub> preparation.

67 With high catalytic efficiency, mild reaction conditions, fewer side reactions, and  
68 environmental friendliness, biological catalysts have been widely applied to industrial  
69 production.<sup>18-21</sup> Enzymatic methods provide an alternative to traditional complex chemical  
70 synthesis.<sup>22</sup> Kinetic resolution by biological catalysts can remove one enantiomer from the  
71 racemate selectively and mildly, and the unwanted enantiomer can be separated. However,  
72 since the maximum theoretical yield is only 50%,<sup>23</sup> application of kinetic resolution on a  
73 large scale has been hampered. Hydrolysis of 3-substituted glutaric acid diesters using  
74 hydrolases or esterases has been applied to the preparation of (*R*)-3-substituted glutaric acid  
75 monoesters,<sup>24</sup> but, because the substrates are poorly soluble in water, the reaction is slow. To  
76 achieve higher yields, the hydrolysis has been conducted in a two-phase aqueous-organic  
77 system,<sup>25</sup> but yields are still limited because the reaction only occurs at the solvent interface.

78 The use of organic solvents in biocatalytic reactions has addressed the problem of low  
79 aqueous solubility of the substrate. A possible alternative for green production of  
80 (*R*)-3-substituted glutaric acid monoesters is acylation of alcohols with 3-substituted glutaric  
81 anhydride using biocatalysts (Scheme 1), which has a theoretical yield of 100%. Since  
82 suitable organic solvents<sup>26</sup> can enhance the “rigid” conformation of lipases,<sup>27-29</sup> improve heat  
83 resistance<sup>18,30</sup> and maintain high catalytic activity,<sup>27</sup> mono-esterification using lipases is more  
84 promising for industrial application. Unfortunately, a lot of work on preparation of  
85 3-substituted glutaric acid monoesters has revealed that natural lipases favor the product with  
86 *S*-configuration (*Supplementary data Table S1*)<sup>22,23</sup>. The yield of *R*-J<sub>6</sub> was low and could not  
87 meet industrial demand, therefore enzymatic synthesis of (*R*)-3-substituted glutaric acid  
88 monoesters (*R*-monoester) by lipases has rarely been reported.

89 In this study, we have extended the scope of the synthesis of (*R*)-3-TBDMSO glutaric  
90 acid methyl monoester (*R*-J<sub>6</sub>) using organic solvent by alcoholysis of 3-substituted glutaric  
91 anhydride with an *S*-selective lipase. The lipase from *Candida antarctica* (CALB) has been  
92 screened and employed for *R*-J<sub>6</sub> production with high catalytic efficiency.<sup>31</sup> Following  
93 selection of the best performing enzyme, the co-substrate (alcohol) that would be favored for  
94 synthesis of the *R*-monoester was selected as the acyl acceptor by molecular docking. The

95 final objective was to optimize the reaction conditions. An efficient process for large-scale  
96 production of (*R*)-3-substituted glutaric acid monoesters by reaction of 3-substituted glutaric  
97 anhydride with alcohols has been developed.

## 98 **2. Materials and methods**

### 99 **2.1. Materials**

100 Novozym 435 (CALB, lipase from *C. antarctica* immobilized on a macroporous anionic  
101 resin) was purchased from Novozymes (Beijing, China). 3-TBDMSO glutaric anhydride  
102 (TBDMSO: t-butyl-dimethyl-silyloxy) was purchased from Yuchen Fine Co., Ltd (Henan,  
103 China).  $\alpha$ -Chymotrypsin was purchased from Sangon Biological Engineering Technology &  
104 Services Co., Ltd (Shanghai, China). Isopropanol and *n*-hexane (HPLC grade) were  
105 purchased from Sigma (St Louis, USA). Other chemicals and solvents (analytical grade)  
106 were from local suppliers (Wuxi, China). Standards of (*R*)-3-TBDMSO glutaric acid methyl  
107 monoester and racemic 3-TBDMSO glutaric acid methyl monoester were obtained as a gift  
108 from Chanyoo Pharmatech Co., Ltd (Nantong, China). The Chiralpak AD-H column (4.6  $\times$   
109 250 mm) was purchased from Daicel Chiral Technologies (Shanghai, China).

### 110 **2.2. Analytical procedure**

111 Methyl esters in the reaction mixture were analyzed by high performance liquid  
112 chromatography (HPLC) using a Daicel Chiralpak AD-H column (4.6  $\times$  250 mm) and an  
113 ultraviolet detector supplied by Agilent. The mobile phase consisted of 96% hexane and 4%  
114 isopropanol with 0.02% (*v/v*) acetic acid, which was filtered through a 0.45  $\mu$ m membrane. A  
115 10  $\mu$ L sample was injected into the column with a detection temperature of 25  $^{\circ}$ C and a flow  
116 rate of 1 mL/min. The run time was 15 min.

117 *R*-J<sub>6</sub> and racemic 3-TBDMSO glutaric acid methyl monoester (racemic J<sub>6</sub>) were the  
118 internal standards. Under these conditions the retention times were as follows: *R*-J<sub>6</sub>, 7.7 min;  
119 (*S*)-3-TBDMSO glutaric acid methyl monoester (*S*-J<sub>6</sub>), 8.3 min. Aliquots (50  $\mu$ L) of the  
120 reaction mixture were taken and solvent removed in an oven at 70  $^{\circ}$ C. Each sample was  
121 diluted with 1 mL of mobile phase then filtered through a 0.22  $\mu$ m membrane.

### 122 **2.3. Molecular docking of alcohols**

123 The crystal structure of CALB<sup>32</sup> [PDB: 1TCA] was taken from the Protein Data Bank  
124 (<http://www.rcsb.org/pdb/explore/explore.do?structureId=1TCA>). In the molecular docking,  
125 a series of alcohols were used as acyl acceptors. Three-dimensional structures of the ester  
126 products were obtained from Chemoffice Ultra 11.0 then minimized using CHARMM. The  
127 compounds were docked into the CALB binding site to determine docking energies and  
128 hydrogen bonding. Only the ligand molecules were considered flexible during the docking  
129 simulation, and only the free energy of the best pose was taken for comparison.

#### 130 **2.4. Esterification reaction**

131 A typical esterification reaction was conducted in 10 mL capped flasks using methyl  
132 *tert*-butyl ether (MTBE) as solvent, 3-TBDMSO glutaric anhydride as substrate, and  
133 Novozym 435 as catalyst (Scheme 1). Crushed 3 Å molecular sieves were activated by  
134 heating in an oven at 100 °C for at least 3 days. The organic solvent was dried over 3 Å  
135 molecular sieves for 72 h before use. The activated molecular sieves (2.5 g, Aldrich, 15–20  
136 wt % based on substrate) were added to the reaction mixture to absorb water generated  
137 during the esterification. The mixture was incubated for 24 h on an orbital shaker (200 rpm)  
138 at 35 °C.

#### 139 **2.5. Statistical analysis**

140 Three different factors (molar ratio of methanol to substrate, Novozym 435 concentration  
141 and 3-TBDMSO glutaric anhydride concentration) were explored using an L<sub>9</sub>-orthogonal  
142 array design. The design was developed and analyzed using Design-Expert 8.0 software. All  
143 measurements were taken in triplicate and experiments were repeated three times to evaluate  
144 the standard deviation.

145

### 146 **3. Results and Discussion**

#### 147 **3.1. Screening of the catalysts for *R*-J<sub>6</sub> production**

148 According to the literature<sup>33, 34</sup> there are four lipases (Lipozyme TLIM from *Thermomyces*  
149 *lanuginosus*, porcine trypsin, Novozym 435 from *C. antarctica*, and  $\alpha$ -chymotrypsin) that can  
150 be used as biocatalysts for asymmetric alcoholysis of 3-substituted glutaric anhydride. The  
151 performance of the four lipases in the synthesis of *R*-J<sub>6</sub> was investigated and the results are

152 shown in Table 1. Trypsin and  $\alpha$ -chymotrypsin performed poorly, giving product titers below  
153 10 g/L. Novozym 435 gave the best results, with the titer of  $R$ -J<sub>6</sub> reaching 12 g/L and  
154 productivity increased to 0.49 g/L/h. Based on these results, Novozym 435 was selected as the  
155 catalyst for  $R$ -J<sub>6</sub> production.

156 The effect of Novozym 435 concentration on  $R$ -J<sub>6</sub> production is shown in Fig. 1. As the  
157 concentration of Novozym 435 increased from 0 to 60 g/L, the titer of  $R$ -J<sub>6</sub> increased. The  
158  $R$ -J<sub>6</sub> titer reached 15.7 g/L when the concentration of Novozym 435 was 60 g/L, with a yield  
159 of 26.13 % and productivity of 0.65 g/L/h. The  $R$ -J<sub>6</sub> titer increased 11-fold compared with that  
160 obtained when 10 g/L Novozym 435 was used. CALB crystal structures suggest a catalytic  
161 mechanism somewhat similar to the serine proteases, with the Ser<sup>105</sup>-His<sup>224</sup>-Asp<sup>187</sup> triad as  
162 the catalytic centre.<sup>32,35, 36</sup> The mechanism of ( $R$ )-3-TBDMSO glutaric acid methyl monoester  
163 production by Novozym 435 has been studied by Molecular Dynamics Simulation (*more*  
164 *information showing in supplemental material Scheme S4*).

165

### 166 3.2. Effect of the acyl acceptor on $R$ -monoester production

167 The ester bond between the alcohol and 3-hydroxy glutaric acid is hydrolyzed in the final  
168 step of rosuvastatin synthesis (Scheme S2). However, alcohols can affect the interactions  
169 between product enantiomers and the enzyme. A series of alcohols were used as acyl  
170 acceptors in the molecular docking (Scheme 1), and the results are shown in Table 2. The  
171 larger the  $E_R/E_S$  ratio, the more stable the predicted transition state of the  $R$ -isomer. Of the  
172 alcohols studied, the best  $E_R/E_S$  ratios were for methanol (1.072) and *tert*-butanol (1.043).  
173 Therefore, methanol and *tert*-butanol were chosen as the acyl acceptors.

174 However, the shorter the carbon chain of the alcohol, the higher the rate of  
175 transesterification would be.<sup>37</sup> For the realization of large-scale production and reducing cost,  
176 methanol (the cheaper and the shortest carbon chain) was selected as the best acyl acceptor.  
177 To investigate the effect of the methanol concentration on  $R$ -J<sub>6</sub> production, the substrate was  
178 alcoholized at 30 °C for 24 h with various amounts of methanol by Novozym 435. The  
179 results (Fig. 2) show that when the molar ratio of methanol to substrate was 1:1, the  $R$ -J<sub>6</sub> titer  
180 was below 5.0 g/L. Of great interest, when the molar ratio of methanol to substrate reached  
181 2:1, the titer and yield of  $R$ -J<sub>6</sub> rose to 16.7 g/L and 33.4 %, respectively, while productivity



182 reached 0.695 g/L/h.

183

### 184 3.3. Effect of reaction conditions on *R*-J<sub>6</sub> production

185 The effect of reaction temperature on *R*-J<sub>6</sub> production was investigated (Fig. 3A). The  
186 titer of *R*-J<sub>6</sub> increased continually as the temperature increased from 22 to 35 °C, and the  
187 productivity of *R*-J<sub>6</sub> reached 0.71 g/L/h at 35 °C.

188 The effect of solvents with different logP values on *R*-J<sub>6</sub> production are shown in Fig. 3B.  
189 No *R*-J<sub>6</sub> was detected in the solvent-free reaction (only methanol, substrate and enzyme in  
190 the reaction system). The *R*-J<sub>6</sub> titer was 21.5 g/L when *iso*-octane was used as the solvent; the  
191 productivity and the yield were 0.895 g/L/h and 35.7 %, respectively.

192 The effect of substrate concentration is presented in Fig. 3C. The results show that the  
193 *R*-J<sub>6</sub> titer increased as the substrate concentration increased from 40 to 200 g/L. At a  
194 substrate concentration of 200 g/L, the *R*-J<sub>6</sub> titer was up to the maximum value, 67.1 g/L,  
195 3.7-fold higher than that at 40 g/L substrate. However, the yield of *R*-J<sub>6</sub> decreased as the  
196 substrate concentration increased (40–200 g/L). Excess substrate had a negative effect on the  
197 yield of *R*-J<sub>6</sub>. When the substrate concentration was above 200 g/L, the yield of *R*-J<sub>6</sub> dropped  
198 below 30%, therefore the optimal concentration was 200 g/L.

### 199 3.4. Statistical analysis

200 The optimum values of the molar ratio of methanol to substrate (molar ratio), Novozym  
201 435 concentration (catalyst), and 3-TBDMSO glutaric anhydride concentration (substrate)  
202 were examined using an orthogonal array design (Table 3). The order of the effect of the  
203 factors on *R*-J<sub>6</sub> production was molar ratio > substrate > catalyst. The molar ratio of  
204 methanol to substrate was the main factor for *R*-J<sub>6</sub> production. In this study, the optimal  
205 conditions for synthesis of *R*-J<sub>6</sub> were as follows: 50 g/L catalyst, 3:1 molar ratio, and 200 g/L  
206 substrate. The *R*-J<sub>6</sub> titer was 117.2 g/L, and the yield was 58.6 %. Under the optimal  
207 conditions, production of *R*-J<sub>6</sub> with time is shown in Fig. 4, indicating a maximum at 24 h.  
208 The biocatalytic process described in this study achieved a highest synthesis rate of 4.84  
209 g/L/h, and thus has great potential for large-scale production of (*R*)-3-TBDMSO glutaric acid  
210 methyl ester, the purity of the desire product was up to 98 %. The *R*-J<sub>6</sub> titer can be  
211 maintained at 90 g/L, therefore, the biocatalyst (Novozym 435) can be reused at least four  
212 times (Fig. 5).

213 *R*-J<sub>6</sub> has been prepared by using the lithium salt of benzyl (*R*)-(-)-mandelate,<sup>12,17</sup> three  
214 additional steps were required to generate *R*-J<sub>6</sub> (see supplementary data Scheme S1), the  
215 yield was only 42.3 % from 3-TBDMSO glutaric anhydride, isolation and purification and  
216 waste treatment were difficult.  $\alpha$ -Chymotrypsin with *R*-selective has been used to prepare  
217 *R*-isomers by hydrolysis of diethyl-3-hydroxyglutarate, however, the maximum *R*-isomer  
218 titer was 32.5 g/L, and the productivity was only 0.68 g/L/h.<sup>38</sup> The 3- substituents group of  
219 the substrate significantly affect the enzyme activity and selectivity, the  $\alpha$ -Chymotrypsin  
220 performed a low catalytic efficiency on the substrate whose 3-substituent was TBDMSO.<sup>39</sup>  
221 The *R*-isomer productivity was only 0.33 g/L/h by  $\alpha$ -Chymotrypsin while the 3-substituent  
222 was TBDMSO in our study.

223 Typical enzymatic process goals are a substrate loading >100 g/L, reaction time < 24 h,  
224 conversion > 98%, and *ee* > 99%.<sup>40</sup> In our study, the synthesis of *R*-J<sub>6</sub> in non-aqueous media  
225 requires only a single step, and the titer of *R*-J<sub>6</sub> was up to gram scale. The desired products  
226 can be isolated, purified, and dried easily, and the organic solvents can be recycled by  
227 vacuum distillation with no wastewater discharge. Substrate concentration was up to 200 g/L  
228 and the reaction time was 24 h, but the yield of *R*-J<sub>6</sub> was only 58.6% and the *ee* value was  
229 low. The *S*-isomer (*S*-J<sub>6</sub>) that was also produced can be used to assemble other statins and  
230 their derivative products<sup>33</sup> such as hapalosin,<sup>41</sup> iostatine<sup>33</sup> and dolastatin.<sup>42</sup> In order to obtain  
231 the statin skeleton of *R*-J<sub>6</sub> in high optical purity, further studies could explore isolation of  
232 *R*-J<sub>6</sub> from the enzymatic conversion solution containing racemic J<sub>6</sub> by dynamic kinetic  
233 resolution<sup>43-46</sup> using vinyl acetate as acyl donor<sup>47</sup> (Scheme S3). Novozym 435 can be reused  
234 directly for dynamic kinetic resolution by filtering without any pretreatment, making the  
235 whole process green. To enhance the yield and further reduce costs of *R*-J<sub>6</sub> production and  
236 simplify the process, we are doing our best to change the enantioselectivity of CALB, and  
237 wanna to obtain a catalyst with high *R*-selectivity on *R*-J<sub>6</sub> preparation by directed evolution.

#### 238 4. Conclusions

239 In summary, different acyl acceptors have been screened based on molecular  
240 docking,<sup>48</sup> and methanol was chosen as the best acyl acceptor. Our experiments  
241 suggest that several lipases, especially lipase from *C. antarctica*, catalyze

242 (*R*)-3-TBDMSO glutaric acid methyl ester (*R*-J<sub>6</sub>) production via esterification in high  
243 yields. A method for enzymatic synthesis of *R*-J<sub>6</sub> in non-aqueous media has been  
244 described. The desired product, *R*-J<sub>6</sub>, was afforded with a titer up to 117.2 g/L and a  
245 yield of 58.6 %; the productivity of *R*-J<sub>6</sub> was improved tenfold from 0.49 g/L/h to  
246 4.88 g/L/h. The biocatalyst (CALB) with high efficiency<sup>49, 50</sup> and selectivity<sup>51-53</sup> can  
247 be reused at least four times (Fig. 5). Besides the advantages of this method, the  
248 highest enantiomeric excess (ee = 22 %) is still moderate and ongoing studies are  
249 underway to circumvent this limitation. Compared with chemical syntheses and  
250 enzymatic hydrolysis, this method is a green chemical process with significant  
251 potential for industrial application.

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## Figure legends

Fig. 1. Effect of Novozym 435 concentration on  $R\text{-}J_6$  production. (■)  $R\text{-}J_6$  titer, (□)  $S\text{-}J_6$  titer, (—■—) yield of  $R\text{-}J_6$ .

Fig. 2. Effect of methanol:substrate molar ratio on  $R\text{-}J_6$  production. (■)  $R\text{-}J_6$  titer, (□)  $S\text{-}J_6$  titer, (—■—) the yield of  $R\text{-}J_6$ . Reaction conditions: 3-TBDMSO glutaric anhydride (50 g/L), the solvent was MTBE, 60 g/L Novozym 435. Methanol was added in one portion at the beginning of the reaction.

Fig. 3. Effect of reaction conditions on  $R\text{-}J_6$  production. (■)  $R\text{-}J_6$  titer, (□)  $S\text{-}J_6$  titer, (—■—) the yield of  $R\text{-}J_6$ . A, effect of temperature. Reaction conditions: the solvent was MTBE, 3-TBDMSO glutaric anhydride (60 g/L), 60 g/L Novozym 435, 2:1 molar ratio of methanol to substrate. B, effect of different organic solvents: MTBE ( $\log P = 0.96$ ), n-hexane ( $\log P = 2.50$ ), cyclohexane ( $\log P = 3.00$ ), *iso*-octane ( $\log P = 3.72$ ), *n*-octane ( $\log P = 3.84$ ); Reaction conditions: 3-TBDMSO glutaric anhydride (60 g/L), 60 g/L Novozym 435, 2:1 molar ratio of methanol to substrate, at 35 °C with a shaking speed of 200 rpm. C, effect of substrate concentration. Reaction conditions: the solvent was *iso*-octane, 60 g/L Novozym 435, 2:1 molar ratio of methanol to substrate, at 35 °C with a shaking speed of 200 rpm. Methanol was added in one portion at the beginning of the reaction.

Fig. 4. Time course of  $R\text{-}J_6$  production under optimized reaction conditions. (■)  $R\text{-}J_6$  titer, (□)  $S\text{-}J_6$  titer, (—■—) the yield of  $R\text{-}J_6$ . Reaction conditions: 3-TBDMSO glutaric anhydride (200 g/L), the solvent was *iso*-octane, 50 g/L Novozym 435, 3:1 molar ratio of methanol to substrate, at 35 °C with a shaking speed of 200 rpm. Methanol was added in one portion at the beginning of the reaction.

Fig. 5. Operation stability of *Novozym* 435 on  $R\text{-}J_6$  production.

Scheme 1. Enzymatic preparation of rosuvastatin side-chain intermediate ( $R\text{-}J_R$ ) from 3-TBDMSO glutaric anhydride using *Novozym* 435. When R is  $\text{CH}_3$ -,  $R\text{-}J_R = R\text{-}J_6$ ; alcohol can be methanol, ethanol, *n*-propanol, *n*-butanol, *iso*-butanol, *tert*-butanol, hexanol, benzyl alcohol, 1-Phenylethanol or 2-phenylethanol.

Scheme S1. Preparation of  $R\text{-}J_6$  by chemical synthesis.

Scheme S2. Preparation of rosuvastatin calcium by chemical synthesis.

Scheme S3. The follow-up process from racemic  $J_6$  to rosuvastatin calcium by *Novozym* 435. The optical purification of  $R\text{-}J_6$  by enzymatic kinetic resolution is shown in the blue dashed box.

Scheme S4. The proposed mechanism for enzymatic synthesis of  $R\text{-}J_6$  by CALB based on molecular docking and molecular dynamics. 3-TBDMSO glutaric acid is generated from 3-TBDMSO glutaric anhydride in the presence of trace water before participating at the active centre of CALB (Scheme 2a). Firstly, one of the carboxylic acids (I) coordinates with the lipase while the other (II), away from the catalytic center, is coordinated by Asp<sup>134</sup> and Gln<sup>157</sup>, providing a stable molecular conformation of the substrate in the catalytic site (Scheme 2b). Ser<sup>105</sup> then attacks the carboxylic acid (I) to form a tetrahedral intermediate from which a water molecule is eliminated (Scheme 2b), leaving a positive charge at (I). After binding of methanol to the catalytic site, the hydroxyl (–OH) is deprotonated by His<sup>224</sup> to generate a negatively charged methoxy group (CH<sub>3</sub>–O<sup>–</sup>) (Scheme 2d). A C–O bond is then formed between the positively charged carbon of the carboxylic acid (I) and the negatively charged oxygen of the methoxy group (Scheme 2e). After the ester-bond formation, the free-energy of the transition state is at its minimum, the carboxylic acid group (II) is fixed by the Ser<sup>105</sup> residue and the TBDMS substituent points out of the active site. Collapse of this intermediate releases  $R\text{-}J_6$  (Scheme 2h).

Table 1. Performance of different lipases in the synthesis of  $R\text{-}J_6$ <sup>a</sup>

Entry	Enzyme	Time (h)	$R\text{-}J_6$ titer (g/L)	Productivity (g/L/h)
1	Novozym 435	24	11.72	0.49
2	Lipozyme TLIM	24	10.56	0.44
3	$\alpha$ -Chymotrypsin	24	7.92	0.33
4	Trypsin	24	6.64	0.28

a. Reaction conditions: 100 g/L 3-TBDMSO glutaric anhydride, 3:1 molar ratio of methanol to substrate, 30 g/L enzyme, MTBE as solvent at 30 °C with a shaking speed of 200 rpm.

Table 2. Results of molecular docking

Entry	R-OH	Energy of <i>R</i> -isomer (kcal/mol)	Energy of <i>S</i> -isomer (kcal/mol)	$E_R/E_S$
1	Methanol	-97.74	-91.187	1.072
2	Ethanol	-96.00	-109.65	0.876
3	<i>n</i> -Propanol	-100.70	-101.06	0.996
4	<i>n</i> -butanol	-99.896	-107.47	0.930
5	<i>iso</i> -butanol	-84.362	-87.93	0.959
6	<i>tert</i> -butanol	-107.84	-103.37	1.043
7	hexanol	-85.98	-113.09	0.760
8	benzyl alcohol	-96.55	-102.17	0.945
9	1-Phenylethanol	-113.46	-115.89	0.979
10	2-Phenylethanol	-107.87	-115.27	0.936

Table 3. Orthogonal array design to improve  $R\text{-}J_6$  production

Run	Factor			A Substrate (g/L)	B Molar ratio	C Catalyst (g/L)	<i>R</i> -J <sub>6</sub> titer (g/L)
	A	B	C				
1	1	1	1	150	1	50	23.12±1.2
2	1	2	2	150	2	60	50.83±1.5
3	1	3	3	150	3	70	87.44±2.4
4	2	1	2	200	1	60	37.44±2.0
5	2	2	3	200	2	70	73.99±2.4
6	2	3	1	200	3	50	117.19±2.9
7	3	1	3	250	1	70	36.79±1.8
8	3	2	1	250	2	50	73.11±1.7
9	3	3	2	250	3	60	108.24±2.7
Range				22.41	71.84	5.64	
Rank				2	1	3	
Optimization				200	3	50	

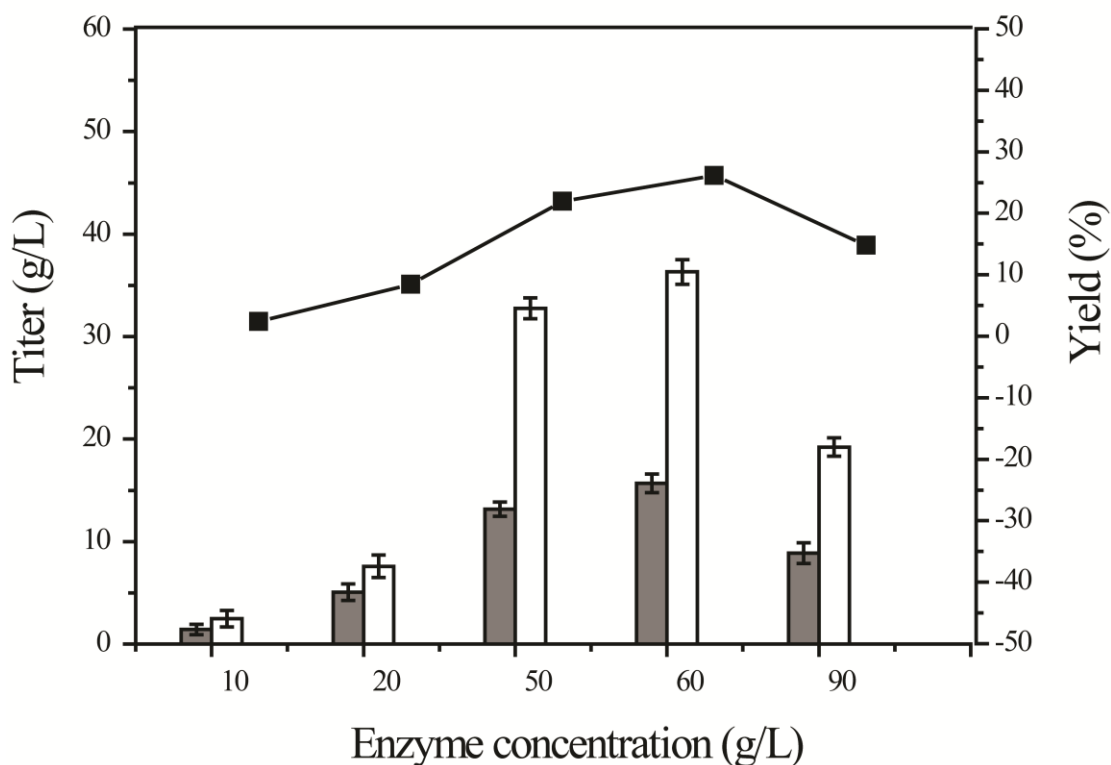


Fig. 1. Effect of Novozym 435 concentration on *R*-J<sub>6</sub> production. (■) *R*-J<sub>6</sub> titer, (□) *S*-J<sub>6</sub> titer, (—■—) yield of *R*-J<sub>6</sub>.



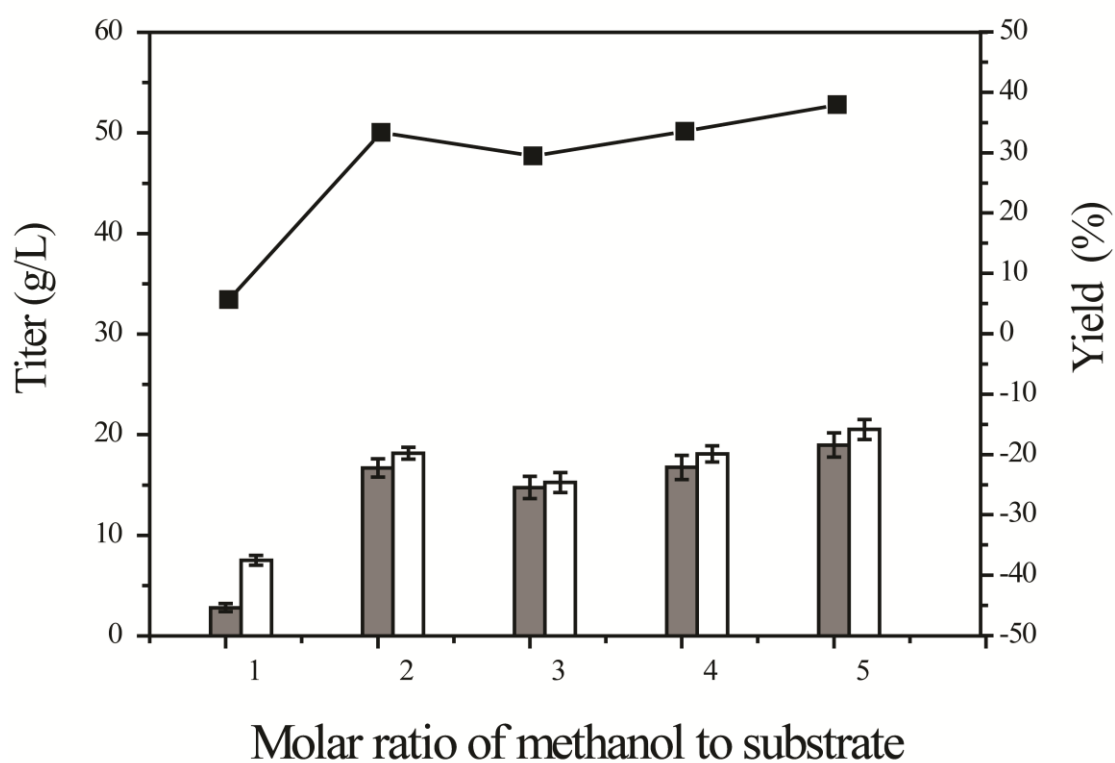


Fig. 2. Effect of methanol:substrate molar ratio on *R*-J<sub>6</sub> production. (■) *R*-J<sub>6</sub> titer, (□) *S*-J<sub>6</sub> titer, (—■—) the yield of *R*-J<sub>6</sub>. Reaction conditions: 3-TBDMSO glutaric anhydride (50 g/L), the solvent was MTBE, 60 g/L Novozym 435. Methanol was added in one portion at the beginning of the reaction.

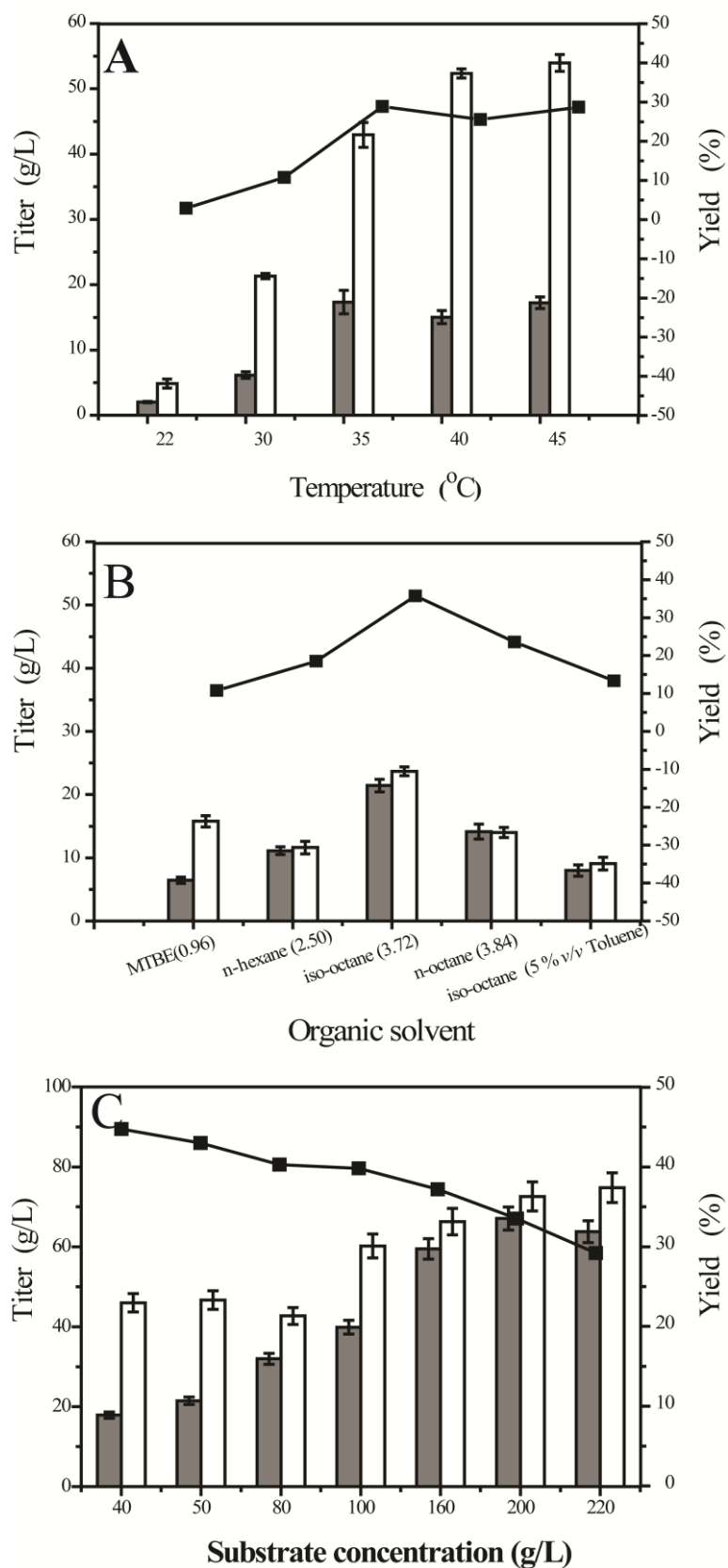


Fig. 3. Effect of reaction conditions on *R*-J<sub>6</sub> production. (■) *R*-J<sub>6</sub> titer, (□) *S*-J<sub>6</sub> titer, (—■—) the yield of *R*-J<sub>6</sub>. A, effect of temperature. Reaction conditions: the solvent was MTBE, 3-TBDMSO glutaric anhydride (60 g/L), 60 g/L Novozym 435, 2:1 molar ratio of methanol to

substrate. B, effect of different organic solvents: MTBE ( $\log P = 0.96$ ), n-hexane ( $\log P = 2.50$ ), cyclohexane ( $\log P = 3.00$ ), *iso*-octane ( $\log P = 3.72$ ), *n*-octane ( $\log P = 3.84$ ); Reaction conditions: 3-TBDMSO glutaric anhydride (60 g/L), 60 g/L Novozym 435, 2:1 molar ratio of methanol to substrate, at 35 °C with a shaking speed of 200 rpm. C, effect of substrate concentration. Reaction conditions: the solvent was *iso*-octane, 60 g/L *Novozym* 435, 2:1 molar ratio of methanol to substrate, at 35 °C with a shaking speed of 200 rpm. Methanol was added in one portion at the beginning of the reaction.

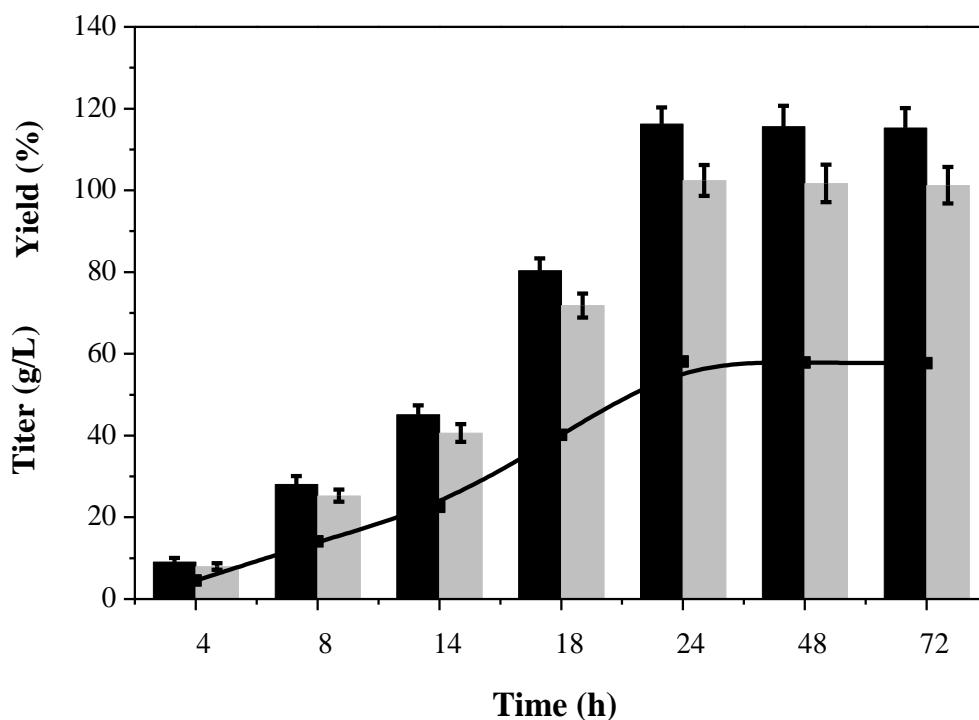


Fig. 4. Time course of *R*-J<sub>6</sub> production under optimized reaction conditions. (■) *R*-J<sub>6</sub> titer, (▒) *S*-J<sub>6</sub> titer, (—■—) the yield of *R*-J<sub>6</sub>. Reaction conditions: 3-TBDMSO glutaric anhydride (200 g/L), the solvent was *iso*-octane, 50 g/L *Novozym* 435, 3:1 molar ratio of methanol to substrate, at 35 °C with a shaking speed of 200 rpm. Methanol was added in one portion at the beginning of the reaction.

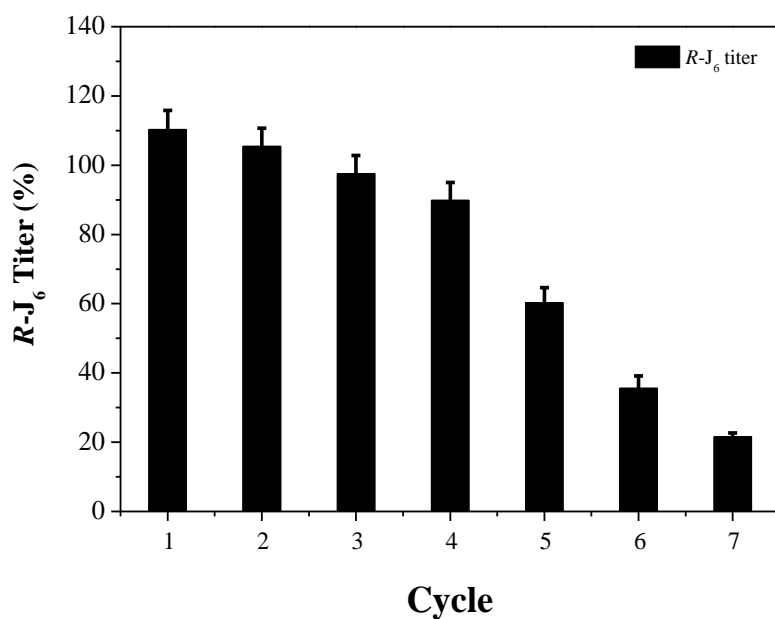
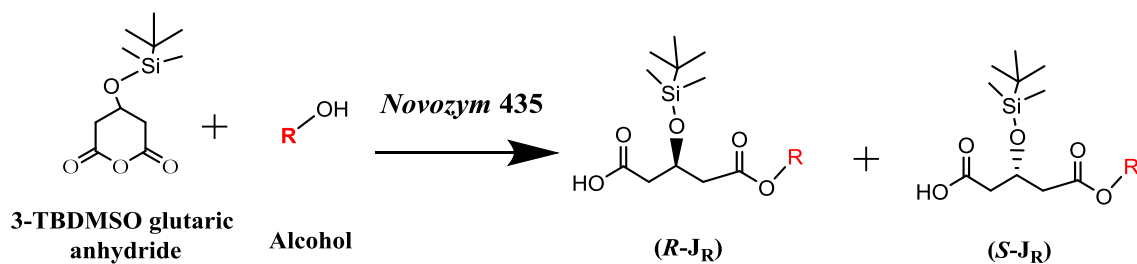
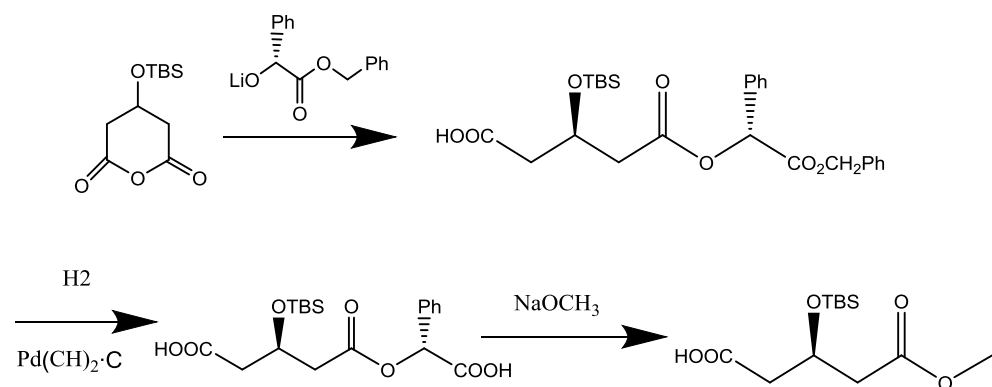
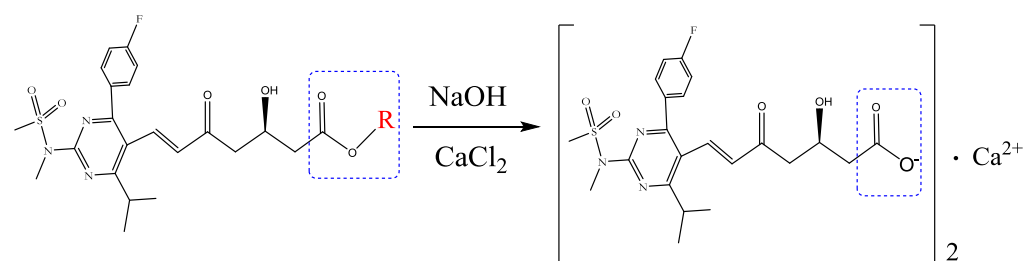


Fig. 5. Operation stability of *Novozym* 435 on  $R$ - $J_6$  production.

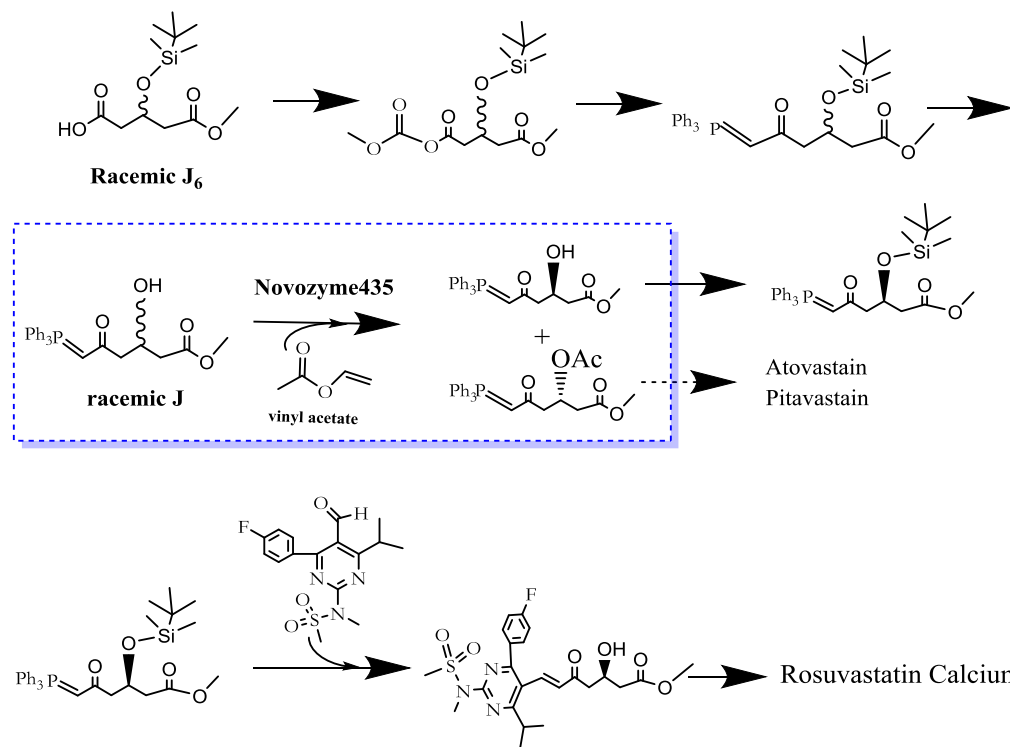


Scheme 1. Enzymatic preparation of rosuvastatin side-chain intermediate ( $R$ - $J_R$ ) from 3-TBDMSO glutaric anhydride using *Novozym* 435. When  $R$  is  $\text{CH}_3$ -,  $R$ - $J_R = R$ - $J_6$ ; alcohol can be methanol, ethanol, *n*-propanol, *n*-butanol, *iso*-butanol, *tert*-butanol, hexanol, benzyl alcohol, 1-Phenylethanol or 2-phenylethanol.

## SUPPLEMENTAL MATERIALS

Scheme S1. Preparation of *R*- $J_6$  by chemical synthesis.

Scheme S2. Preparation of rosuvastatin calcium by chemical synthesis.

Scheme S3. The follow-up process from racemic  $J_6$  to rosuvastatin calcium by Novozym 435. The optical purification of *R*- $J_6$  by enzymatic kinetic resolution is shown in the blue dashed box.

Scheme S4. The proposed mechanism for enzymatic synthesis of *R*-J<sub>6</sub> by CALB based on molecular docking and molecular dynamics. 3-TBDMSO glutaric acid is generated from 3-TBDMSO glutaric anhydride in the presence of trace water before participating at the active centre of CALB (Scheme 2a). Firstly, one of the carboxylic acids (I) coordinates with the lipase while the other (II), away from the catalytic center, is coordinated by Asp<sup>134</sup> and Gln<sup>157</sup>, providing a stable molecular conformation of the substrate in the catalytic site (Scheme 2b). Ser<sup>105</sup> then attacks the carboxylic acid (I) to form a tetrahedral intermediate from which a water molecule is eliminated (Scheme 2b), leaving a positive charge at (I). After binding of methanol to the catalytic site, the hydroxyl (–OH) is deprotonated by His<sup>224</sup> to generate a negatively charged methoxy group (CH<sub>3</sub>–O<sup>–</sup>) (Scheme 2d). A C–O bond is then formed between the positively charged carbon of the carboxylic acid (I) and the negatively charged oxygen of the methoxy group (Scheme 2e). After the ester-bond formation, the free-energy of the transition state is at its minimum, the carboxylic acid group (II) is fixed by the Ser<sup>105</sup> residue and the TBDMS substituent points out of the active site. Collapse of this intermediate releases *R*-J<sub>6</sub> (Scheme 2h).

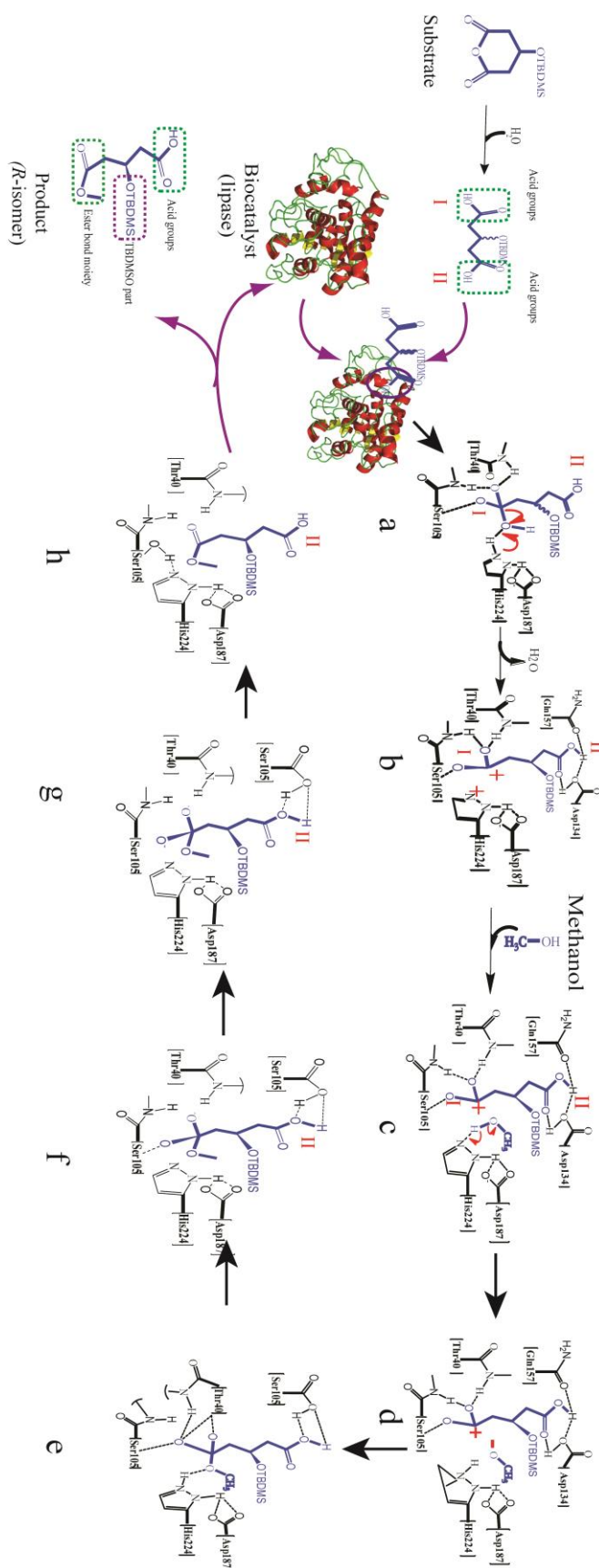


Table S1. Enzymatic desymmetrization by hydrolysis of diethyl 3-hydroxyglutarate (a) and dimethyl 3-hydroxyglutarate (b).

Substrate	Enzyme	Activity	$[\alpha]_D^{20}$	Configuration
a	CALB	7 PLU/mg	+ 1.8 (c 11.5, acetone)	S
a	CALA		+ 1.8 (c 11.5, acetone)	S
a	CLEC-CALB	17 U/mg		S
a	HLL			S
a	RML	60 U/g		S
a	PLE	15 U/mg	+ 0.2 (c 11.5, acetone)	S
a	<i>A. lwoffii</i>	(cell cult.)		S
a	$\alpha$ -Chymotrypsin	70 U/mg		R
b	PLE			S
b	MCL	cell prep.		S