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Adsorptions of Cd(II) and Methylene Blue from Aqueous Solution by Silica Hybrid Hollow Spheres

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ABSTRACT: Silica hybrid hollow spheres were successfully synthesized by co-hydrolysis and condensation reactions of TEOS and vinyltrimethoxysilane (VTMS) under the catalysis of ammonia. The as-obtained silica hybrid hollow spheres were used as adsorbents for the removal of Cd (II) and methylene blue (MB) from aqueous solutions. The isotherm adsorption data of the silica hybrid hollow spheres for Cd(II) and MB followed the Langmuir isotherm model. The silica hybrid hollow spheres exhibited the adsorption capacities 10 as high as 54.702 and 25.242 mg g-1 for Cd(II) and MB, respectively. The adsorption kinetics of Cd(II) and MB onto the silica hybrid hollow spheres can be well fitted to the pseudo-second-order model. The adsorption processes of Cd(II) and MB onto the silica hybrid hollow spheres at 298, 318 and 338 K could be carried out spontaneously.

Introduction

- ¹⁵ It has been known that heavy metals ions and organic dyes are main two kinds of water contaminations. For example, Cd(II) as one of the most common heavy metal ions, has become a great threat to human health.¹ Exposure to even low concentration of Cd(II), has potential to cause neurological, reproductive, ²⁰ cardiovascular and developmental disorder for human beings.²
- Higher level of Cd(II) exposure could increase risks of cancer mortality, and damage to liver, kidneys and bones.^{3, 4} Their nonbiodegradability and biological accumulation make Cd(II) a long presence in environment and ecological chains. In addition,
- ²⁵ synthetic dyes containing difficultly decomposed aromatic structures or azo groups would be carcinogenic and mutagenic for aquatic organisms. Their discharge into water would further increase the chemical oxygen demand and decrease light penetration and visibility.^{5, 6} Although MB as a thiazine dye is not ³⁰ recognized as acutely hazardous, it has various harmful impacts
- such as nausea, vomiting and gastritis.⁷⁻⁹

Adsorption has been regarded as an effective and economic method for removal of pollutants in the past decades due to its easy operation process, high efficiency and low cost.¹⁰

- ³⁵ Conventional adsorbents come from nature or industrial waste such as peanut hulls,^{7,11} rice husks,¹² ash,¹³ etc.^{14, 15} However, they still exhibit many disadvantages including low adsorption capacity, fluctuant adsorption performance and limited resource. Nowadays, new types of silica based adsorbents have attracted a
- ⁴⁰ great deal of interest for their large specific area, controllable surface structure, and good adsorption capacity and separation.¹⁶⁻¹⁹
 ¹⁹ For example, Ho *et al.*²⁰ fabricated ordered mesoporous adsorbents by grafting amino- and carboxylic-containing

functional groups onto MCM-41 for the removal of MB from 45 wastewater. Pérez-Quintanilla et al.21 prepared SBA-15 chemically modified with 2-mercaptopyrimidine using a homogeneous method and this solid was employed as Cd(II) adsorbent. Machida *et al.*²² introduced mono-amino and mercapto-groups through grafting or co-condensation method 50 onto the mesoporous silica. The functionalized mesoporous silica was proved to be an efficient adsorbent for Cd(II) (28.11 mg g^{-1}). Alothman et al.23 grafted mesoporous silica with di-, tri- and penta-amine functional groups and these absorbents exhibited excellent potential for separation and preconcentration of Cu(II), 55 Zn(II) and Cd(II). Further, Wang et al.²⁴ successfully SBA-15 with N-[3functionalized (trimethoxysilyl)propyl]ethylene-diamine and used for removal of heavy metal ions in aqueous solution. Other silica materials with different structures such as silica nanofibers, gel and 60 nanocomposites can also be used as adsorbents to remove metal ions and dyes.^{25, 26} Hollow structured silica has been also used to remove organic and inorganic pollutants owing to its large capacity, low density, thermal stability, low toxic, mild synthetic condition and easily controllable morphology.²⁷⁻³³ Najafi et al.³⁴ 65 prepared silica nano hollow spheres with rather monodisperse size through the conventional soft method. The maximum adsorption capacity of the synthesized nano particles for Cd(II) was 49.5mg g⁻¹. Zhang et al.³⁵ synthesized magnetic Fe₃O₄@hierarchical silica hollow spheres by microemulsification 70 method. The spheres exhibited an excellent ability to adsorb MB from aqueous solutions with maximum adsorption capacity of 71.4 mg g⁻¹. Recently, Zhao and Xu³⁶ fabricated 0.8 - 4 µm hollow amino-functionalized organosilica microspheres with an open hole on the shell based on the hydrolysis and condensation 75 of 3-aminopropyltriethoxysilane and TEOS in an aqueous system without an additional template and catalyst. The adsorption capacity of this organosilica microspheres for Cd(II) was 47.4 mg g^{-1} due to the binding between Cd(II) and the amino groups.

In this study, we successfully synthesize silica hybrid hollow so spheres without any open holes via one simple hydrolysis and condensation of vinyltrimethoxysilane (VTMS) and

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tetraethoxysilane (TEOS) with ammonia as catalyst at room temperature. The as-obtained silica hybrid hollow spheres can be used as adsorbent to remove Cd(II) and MB in aqueous solution as shown in **Scheme 1**. Furthermore, the adsorption isotherm, s kinetics and thermodynamic properties of the silica hybrid hollow spheres for Cd(II) and MB have been measured and discussed in details



10 Scheme 1. Schematic diagram of the silica hybrid hollow spheres via one step and their adsorption for Cd(II) and MB

Experimental procedure

Materials

- ¹⁵ Vinyl trimethoxysilane (VTMS, CH₂CHSi(OCH₃)₃, \geq 97%) was obtained from Evonik Specialty Chemical (Shanghai) Co., Ltd. Cadmium chloride (CdCl₂, >99%), methylene blue (MB, \geq 94%), tetraethoxysilane (TEOS, Si(OCH₂CH₃)₄, 99%) and ammonia (25wt% NH₃ in water) were obtained from Sinopharm
- ²⁰ Chemical Reagent Corp. All chemicals were used as received without further purification. Deionized water was used throughout the experiment.

Synthesis of silica hybrid hollow spheres

- Typically, VTMS (0.2 g) and H_2O (50 g) were charged into a 100 mL two neck round flask equipped with a mechanical stirrer, a thermometer with a temperature controller and a Graham condenser and then mechanically stirred at 40 °C by 500 rpm for 1 h to hydrolyze VTMS. Then TEOS (1 g) and ammonia (20 μ L)
- ³⁰ were added and stirred at the same temperature for another 3 h to produce the silica hybrid hollow spheres. The as-obtained silica hybrid hollow spheres were centrifuged and washed with absolute ethanol two times. For comparison, the silica hybrid solid spheres were also prepared with VTMS (1g) and TEOS (0.2g) according ³⁵ to the above process.

Characterization

Transmission electron microscopy (TEM) images were observed with a Hitachi H-800 transmission electron microscope 40 at 75KV. Scanning electron microscopy (SEM) images was recorded on a Philips XL 30 field emission microscope at an accelerating voltage of 10 kV. Fourier transform infrared spectra (FTIR) were obtained using a Nicolet Nexus 470 FTIR with powder-pressed KBr pellets. Raman results were determined

45 using a LABRAM-EB raman spectroscopy. Nitrogen adsorptiondesorption isotherm analysis was performed using Micromeritics ASAP 2010. The specific surface area was characterized with the Brunauer–Emmett–Teller (BET) method. The pore size distribution was calculated from the analysis of the isotherm ⁵⁰ desorption curves using the Brunauer–Joyner–Halenda (BJH) method.

Heavy metal ion and organic dye adsorption experiment

In order to study the adsorption capacity of the obtained silica 55 hybrid hollow spheres, the organic and inorganic materials such as Cd(II) ions and MB were utilized. Batch adsorption experiment was performed in 100 mL-conical flasks containing 25mg adsorbents and 25mL Cd(II) ion or MB solution, shaken at 150 rpm for 12h at (25±1 °C). The pH of the aqueous solution 60 was adjusted by using either 0.1 M HCl or 0.1 M NaOH. A sample of silica hybrid hollow spheres (25 mg) was suspended in 25 mL of 100 mg L^{-1} Cd (II) ions solution at several pH values (2, 3, 4, 5, 6, 7). This is because that Cd (II) would precipitate from the solution when pH is >7. But pH of MB solution was chosen 65 from 2 to 10 at the concentration of 30 mg L⁻¹ MB. Adsorption isotherms were carried out with the varying initial concentrations of Cd(II) ions (10, 20, 40, 60, 80, 100, 150, 200, 300, 400, 500 $mg \cdot L^{-1}$) at pH 4 and those of MB (5, 10, 15, 20, 25, 30, 35, 40, 60, 80, 100 mg·L⁻¹) at pH 8. To study the effect of time, the 70 adsorption time of Cd(II) ions was controlled from 0 to 300 min at the initial concentrations of 100 mg L⁻¹ and pH 4. That of MB was chosen from 0 to 420 min at the initial concentrations of 30 mg L^{-1} and pH 8. These kinetic experiments were performed by using the batch technique. After an aliquot of Cd(II)/MB solution 75 at the predetermined time intervals was removed, the remain

solution didn't continue to use. Then, the next determination should be obtained by using a new solution with the same concentration. Adsorption thermodynamics was conducted at the temperatures ranging from 298K to 338 K with varying initial so concentration of Cd(II) (100, 150, 200, 300, 400, 500mg·L⁻¹) and

MB (10, 15, 20, 25, 30, 35mg·L⁻¹) for 12h.

After a desired adsorption period, the silica hybrid hollow spheres were separated from the solution, and then the concentration of Cd(II) ions was measured by the atomic ⁸⁵ absorption spectrophotometry using a AA 240 DUO instrument. That of MB was determined by UV/Vis Spectrometer (UV 2100). The adsorption capacity of the adsorbates (Cd(II) ion and MB) at equilibrium was calculated according to the following equation:³⁷

$$q_e = \frac{\left(c_0 - c_e\right)v}{m} \tag{1}$$

⁹⁰ where q_e is the equilibrium adsorption capacity of adsorbent (mg of metal g⁻¹ adsorbent), C_0 is the initial concentration of adsorbate in mg L⁻¹, C_e is the equilibrium concentration of adsorbate in mg L⁻¹, v is the volume of the adsorption medium in L, and *m* is the weight of the adsorbent in g. All the experiments were carried out ⁹⁵ in triplicate and their mean value was reported.

Results and discussions

Preparation of silica hybrid hollow spheres

Fig. 1 displays the typical TEM and SEM images of silica hybrid hollow spheres and solid spheres. Monodisperse silica ¹⁰⁰ hybrid hollow spheres have the average size of 390 nm with a shell thickness of 50 nm as shown in Fig.1a, and their surfaces are little bit rough (Fig. 1 b). When more VTMS was used, solid spheres with the mean size of $1.2\mu m$ are obtained (Fig.1c and 1d).



Fig. 1 Typical TEM and SEM images of silica hybrid hollow spheres (a, b) and s silica hybrid solid spheres(c, d)

The FTIR spectra of silica hybrid hollow spheres, silica hybrid solid spheres and SiO₂ particles are illustrated in **Fig. 2**. The strong absorption bands at 1100 cm⁻¹ and 470 cm⁻¹ are assigned to the stretching vibration of Si-O-Si groups. The broad and strong ¹⁰ peak at 3420 cm⁻¹ is attributed to Si-OH stretching vibration.

- Except these characteristic peaks of SiO₂ particles, the spectra of the silica hybrid hollow spheres and solid spheres exhibit the absorption bands at 3062cm⁻¹, 2961cm⁻¹ attributing to the vibration absorptions of -CH and CH₂= groups, respectively. The ¹⁵ strong peak at 1602cm⁻¹ is related to the vibration of C=C groups,
- while the bands at 1407cm⁻¹ and 1278 cm⁻¹ are for the bending banding deformations of Si-CH=CH₂ groups and the rocking vibrations of -CH₂=. This identifies the existence of vinyl groups in these hybrid spheres. Furthermore, in the spectrum of the silica
- ²⁰ hybrid solid spheres, the peaks associated with C=C, CH₂= and CH₂= groups are enhanced with increasing the amount of VTMS obviously. This demonstrates that the organic vinyl groups have been linked on Si-O-Si chains of these hollow spheres.



Fig. 2 FTIR spectrum of silica hybrid hollow spheres (a), silica hybrid solid spheres (b) and SiO_2 particles (c)

The existence of vinyl groups on the silica hybrid spheres can ³⁰ be further verified by Raman (**Fig. 3**). For silica hybrid hollow and solid spheres, the stretching modes of C=C groups are observed at 1604cm⁻¹, while the scissoring and rocking vibration of CH_2 = and $-CH_2$ = groups occur at 1415 and 1276 cm⁻¹, respectively. For silica hybrid solid spheres, the stronger peaks associated with C=C, CH_2 = and $-CH_2$ = groups are observed, indicating higher grafting density with the increasing amount of VTMS.



Fig. 3 Raman spectrum of silica hybrid hollow spheres (a), silica hybrid solid ⁴⁰ spheres (b) and SiO₂ particles (c)

Fig.4 shows the typical nitrogen adsorption/desorption isotherms and pore size distribution of silica hybrid hollow spheres and solid spheres. The N₂ adsorption–desorption⁴⁵ isotherms of the silica hybrid hollow spheres exhibit the representative type-IV curves. The BET surface area, pore volume and mean pore size of the silica hybrid hollow spheres are 259.9 m² g⁻¹, 0.36 cm³ g⁻¹ and 4.25 nm due to their special hollow structures, which are significantly larger than those of the ⁵⁰ solid hybrid spheres (52.4 m² g⁻¹, 0.23 cm³ g⁻¹ and 1.60 nm, respectively).



Fig. 4 Nitrogen adsorption/desorption isotherms of silica hybrid hollow ⁵⁵ spheres (1) and silica hybrid solid sphere (2). Inset: distribution of pore size.

Adsorption properties Effect of pH

pH is one of the most important parameters governing the 60 remove of metal ions and dye from the aqueous solution by adsorption.



$$=\frac{q_m b C_e}{1+bC_e} \tag{2}$$

Where C_e and q_e are equilibrium adsorbate concentration (mg L⁻¹) ⁴⁵ and equilibrium adsorption capacity (mg g⁻¹). q_m (mg g⁻¹) is the maximum uptake capacity corresponding to complete monolayer coverage and b (L g⁻¹) is Langmuir constant that represents the affinity between solute and adsorbent.

A Freundlich isotherm is based on the assumption of the 50 heterogeneous adsorption due to the diversity of the adsorption sites or the diverse nature of the metal ions adsorbed. The Freundlich equation is expressed as Eq.(3):³⁹

$$q_e = k c_e^{\frac{1}{n}} \tag{3}$$

Where k and n are the Freundlich constants, related to the 55 adsorption capacity of adsorbent and adsorption intensity, respectively.

Fig. 6 illustrates the typical adsorption isotherms of silica hybrid hollow spheres and solid spheres as a function of different adsorbates (Cd(II) and MB) concentrations. The fitting results 60 for the adsorption of Cd(II) and MB on silica hybrid hollow spheres and solid spheres are calculated and listed in Table 1. The Langmuir model is much better than the Freundlich model, suggesting that the adsorption of Cd(II) and MB by silica hybrid hollow spheres and solid spheres is homogenous. The values of $_{65}$ q_m are found to be 54.702 and 48.401 mg g⁻¹ for Cd(II), and 25.242 and 5.811 mg g⁻¹ for MB on the silica hybrid hollow spheres and solid spheres, respectively. Obviously, the silica hybrid hollow spheres exhibit the superior adsorption property due to their special hollow structures and more -OH groups. The 70 BET surface area, pore volume and mean pore size of the silica hybrid hollow spheres (259.9 m² g⁻¹, 0.36 cm³ g⁻¹ and 4.25 nm) are larger than those of the solid hybrid spheres (52.4 m² g⁻¹, 0.23 $cm^3 g^{-1}$ and 1.60 nm). The capillary force between the inside and outside of the silica hybrid hollow spheres is a primary one 75 causing migrations of Cd(II) and MB. Meanwhile, the MB adsorption capacity of the solid spheres is lowest due to its only surface adsorption. The average pore size calculated form BJH method for the solid spheres is 1.60 nm, which is too small to stop the MB molecules with 1.43 nm length \times 0.61 nm width \times

 $_{80}$ 0.4 nm height penetrating inside the spheres⁴⁰. While the average diameter of Cd (II) is 0.095 nm[Taken from Ionic radius table], which allow itself to migrate towards the inside of the spheres.



6 pH

(mg/g)

Cd(II)

MB

Cd(II) (b) and MB(c) onto silica hybrid hollow spheres and solid spheres

Fig. 5 demonstrates the effect of pH on Cd(II) and MB adsorption by silica hybrid hollow spheres and solid spheres. For both Cd(II) and MB, the silica hybrid hollow spheres still have obviously much higher adsorption capacity than the solid spheres. because the former has larger BET surface area and more -OH

- ¹⁰ groups. The isoelectric points (pI) of silica hybrid hollow spheres and solid spheres are 3.8 and 4.7, respectively (Fig. 5a). The adsorption of Cd(II) by the silica hybrid spheres increases with pH increasing from 2.0 to 4.0, and reaches the equilibrium with pH from 4.0 to 6.0, then decreased with pH increasing from 6.0 to
- 15 7.0. This is due to the fact that both the spheres exhibit positive charges and would reject with Cd (II) at pH<pI. When pH>5, both the spheres remain negatively charged. The adsorption capacity decreases sharply with increasing of pH from 4.0 to 7.0, this is likely attributed to that the pores of spheres are filled up
- 20 with Cd(OH)₂ precipitation from the hydroxylated complexes of the Cd(II). Therefore, the optimum pH 4.0 for Cd (II) is chosen throughout the subsequent experiment. Fig.5 c demonstrates that the MB adsorption capacity of both silica hybrid hollow spheres and solid spheres is growing slowly at pH < pI due to the
- 25 electrostatic repulsion between MB and the excessive H⁺ ions on their surface. Then the adsorption of MB by the silica hybrid hollow spheres increases quickly at pH > pI and get the equilibrium with pH from 8 to 10. The negatively charged Si-OH groups on the surfaces of the silica hybrid spheres favor the
- 30 adsorption of cationic dye molecules. However, the solid spheres exhibit little adsorption capacity for MB as shown in Fig. 5c $(0.395 \text{ mg g}^{-1} - 5.211 \text{ mg g}^{-1})$. This implies that MB is only absorbed on the surface of the solid spheres via electrostatic interaction due to their small BET surface area, pore volume and $_{35}$ pore size (52.4 m² g⁻¹, 0.23 cm³ g⁻¹ and 1.60 nm).

Adsorption isotherms

Langmuir and Freundlich mathematic models were used to

Table 1 Langmuir and Freundlich isotherm	constants for Cd(II) and MB onto	o silica hybrid hollow spheres	and solid spheres
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		La	ngmuir model		Freundlich model			
Adsorbate	Sorbent	q_m (mg/g)	b	R^2	k	п	R^2	
	Hollow spheres	54.702 ± 2.174	0.037 ± 0.006	0.9692	11.726 ± 2.074	3.889 ± 0.053	0.9256	
Cd(II)	Solid spheres	48.401 ± 5.090	0.013 ± 0.004	0.9865	3.798 ± 1.716	2.496 ± 0.053	0.8259	
	Hollow spheres	25.242 ± 0.875	0.679 ± 0.117	0.9817	12.937 ± 1.666	5.865 ± 0.143	0.8944	
MB	Solid spheres	5.811 ± 0.246	$0.342\!\pm\!0.095$	0.9875	2.981 ± 0.338	6.379 ± 0.132	0.9126	

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Fig. 6 The adsorption isotherms with Langmuir (a and b) and Freundlich (c and d) on silica hybrid hollow spheres and solid spheres.

Adsorption kinetics

- The kinetics of adsorption that describes the adsorbents uptake rate governing the contact time of the adsorption reaction is one ¹⁰ of the important characteristics that define the efficiency of adsorption. In this study, the kinetics of the adsorption process was studied by batch experiments at room temperature. A sample of 25 mg of the silica hybrid hollow spheres and solid spheres was used in each experiment, and the initial concentrations of ¹⁵ Cd(II) and MB were 100 mg·L⁻¹ and 30 mg·L⁻¹, respectively.
- **Fig.7a** shows the adsorption kinetic curves of the silica hybrid hollow spheres and solid spheres as the example to Cd(II) and MB. It can be seen that the MB adsorption by the silica hybrid hollow spheres reaches the equilibrium within initial 5 min
- ²⁰ quickly. However, this adsorption by the silica hybrid solid spheres is very rapid in the first 25min, and then slows down in the following time, and finally reaches the equilibrium after 60 min. On the contrary, the Cd(II) adsorption onto both the silica hybrid hollow spheres and solid spheres increases sharply in the ²⁵ first 50 min and then reaches the equilibrium (Fig. 7b).
- The adsorption kinetic data of Cd(II) and MB onto both the spheres are analyzed in terms of pseudosecond-order kinetic equations. This equation is based on the assumption that the determining rate step would be chemisorption promoted by

 $_{30}$ covalent forces through the electron exchange, or valency forces through electrons sharing between adsorbent and adsorbate. The liner form of the pseudo-second-order model is expressed as Eq.(4, 5): $^{41-43}$

$$\frac{t}{q_{t}} = \frac{t}{q_{e}} + \frac{1}{k_{2}q_{e}^{2}} \quad (4)$$
$$h_{0} = k_{2}q_{e}^{2} \quad (5)$$

Where q_t is the amount of adsorbate at any time (mg g⁻¹), q_e is the amount of adsorbate at equilibrium (mg g⁻¹); K_2 is the adsorption constant (min⁻¹), h_0 is the initial adsorption rate (g mg⁻¹ min⁻¹).

The fitting curve of pseudo-second-order kinetic model and the 40 corresponding kinetic parameters are illustrated in Fig.7(c, d) and **Table 2**. The determination coefficients (R^2) of the silica hybrid hollow spheres and solid spheres are 0.9927 and 0.9875 for Cd(II) adsorption, and 0.9991 and 0.9964 for MB, respectively. The theoretical q_e value (q_e , $_{cal}$) estimated from the pseudo-second-45 order kinetic model is close to the experimental values of q_e (q_e , $_{exp}$). These results suggest that the whole process controlling the rate may be a chemical adsorption.



⁵⁰ Fig. 7 Effect of adsorption time on the adsorption behavior (a, b) and Pseudo-second-order kinetic model fitting (c, d) of silica hybrid hollow spheres and solid spheres.

Table 2 Pseudo-second-order model constants for Cd(II) and MB adsorption on silica hybrid hollow spheres and solid spheres

Adsorbate	Sorbent	$q_{e,\exp} (\mathrm{mg/g})$	Pseudo-second-order					
			$q_{e, ext{cal}} \ (ext{mg/g})$	h_0 (g.mg ⁻¹ min ⁻¹)	$\frac{K_2}{(\min^{-1})}$	R^2		
Cd(II)	Hollow spheres	52.712 ± 1.267	55.788 ± 0.022	3.945 ± 0.027	$0.0013 \pm < 0.0001$	0.9927		
	Solid spheres	45.213 ± 2.885	45.589 ± 0.073	4.752 ± 0.029	$0.0023 \pm < 0.0001$	0.9875		
MB	Hollow spheres	25.203 ± 2.124	$27.333 \!\pm\! 0.016$	1.881 ± 0.023	$0.0025 \pm < 0.0001$	0.9991		
	Solid spheres	5.386 ± 0.038	5.523 ± 0.063	0.435 ± 0.012	0.014 ± 0.0007	0.9964		

Thermodynamic Studies

The thermodynamic parameters provide in-depth information about the energetic changes associated with adsorption process. ⁶⁰ Thermodynamic parameters, such as change in enthalpy (ΔH^{θ}) ,

entropy (ΔS^{θ}) and Gibbs free energy (ΔG^{θ}) can be determined by the following Eq.(6, 7):^{44,45}

$$\Delta G^{\theta} = -RT \ln K_c \qquad (6)$$

$$\ln K_c = \frac{\Delta S^{\theta}}{R} - \frac{\Delta H^{\theta}}{RT} \quad (7)$$

⁶⁵ where *R* is the universal gas constant (8.314 J mol⁻¹ K⁻¹), *T* (K) is the absolute temperature, K_c is the thermodynamic equilibrium constant. K_c is obtained by plotting $\ln(q_e/C_e)$ versus q_e and extrapolating to zero as shown in Fig. S1. Table 3 displays the values of $\ln K_c$. The values of ΔH^{θ} (KJ mol⁻¹) and ΔS^{θ} (J mol⁻¹ K⁻¹) ⁷⁰ can be further obtained from the slop and interception of the van't Hoff linear plots of $\ln K_c$ versus 1/T by using Eq.(7) (Fig.8). The change of adsorption Gibbs free energy (ΔG^{θ}) can be calculated from Eq. (6).

- **Table 3** summarizes all the thermodynamic parameters. The ⁵ positive values of ΔH^{θ} indicate that the adsorption process of Cd(II) and MB onto the silica hybrid hollow spheres and the solid spheres is endothermic. The positive ΔS^{θ} indicates an irregular increase of the randomness at the adsorbent/solution interface during the adsorption procedure. The negative values of ΔG^{θ} by
- ¹⁰ the silica hybrid hollow sphere obtained at all of the experimental temperatures display that the adsorption process could be carried out spontaneously. As the temperature increases, the value of ΔG^{θ} decreases. This indicates that the adsorption is more favorable in high temperature. However, the positive values of ΔG^{θ} for MB ¹⁵ onto the solid sphere indicate that the adsorption between solid

spheres and MB molecules is not spontaneous.



Fig. 8 Plots of $\ln K_c$ versus 1/T for adsorption of Cd(II) and MB on silica hybrid hollow spheres and solid spheres

Silica hybrid hollow spheres have been successfully synthesized via a sol-gel procedure involving the hydrolysis and condensation reactions of VTMS and TEOS. The silica hybrid hollow spheres with large –OH groups displayed the excellent ²⁵ adsorption capacity for Cd(II) and MB in aqueous solution. The maximum adsorption capacities of the silica hollow hybrid spheres for Cd(II) and MB are found to be 54.702 mg g⁻¹ and 25.242 mg g⁻¹ at room temperature. The adsorption of Cd(II) and MB on the silica hollow hybrid spheres shows the homogeneous ³⁰ characteristics. The adsorption kinetics of Cd(II) and MB onto silica hollow hybrid spheres can be fitted to the pseudo-second-order model well. The negative values of ΔG^{θ} and positive values of ΔH^{θ} suggest the spontaneous and endothermic process of the adsorption of Cd(II) and MB onto the silica hollow hybrid spheres.

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Electronic supplementary information (ESI) available: Plots of $ln(q_e/C_e)$ 45 as a function of q_e for Hollow spheres and Solid spheres at various temperature. See DOI:

20 Conclusion

⁵⁰ Table 3 Thermodynamic parameters for Cd(II) and MB adsorption on silica hybrid hollow spheres and solid spheres

Adsorbate	Sorbent	Temperature	1 17	ΔG^{θ}	ΔS^{θ}	ΔH^{θ}	R^2
		(K)	$\ln K_c$	$(J mol^{-1})$	$(J mol^{-1}k^{-1})$	$(kJ mol^{-1})$	
Cd(II)	Hollow spheres	298	1.295	-3208.393 ± 11.135			
		318	1.572	-4156.912±76.661	56.319 ± 1.087	12.665 ± 0.042	0.9665
		338	1.949	-5477.327±11.816			
	Solid spheres	298	0.522	-1292.507 ± 28.727			
		318	1.253	-3313.284±41.664	84.211 ± 1.063	23.812 ± 0.041	0.9594
		338	1.596	-4485.369 ± 94.601			
MB	Hollow spheres	298	1.297	-3213.731 ± 27.706			
		318	1.445	-3819.541 ± 19.342	40.769 ± 0.321	8.999 ± 0.012	0.9067
		338	1.730	-4862.796 ± 15.698			
	Solid spheres	298	-0.818	2027.846 ± 12.724			
		318	-0.755	1997.283 ± 12.424	3.626 ± 0.754 3.118	3.118 ± 0.021	0.9650
		338	-0.675	1898.099 ± 47.209			

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Silica hybrid hollow spheres prepared via one step method can be used as adsorbents for Cd (II) and methylene blue.