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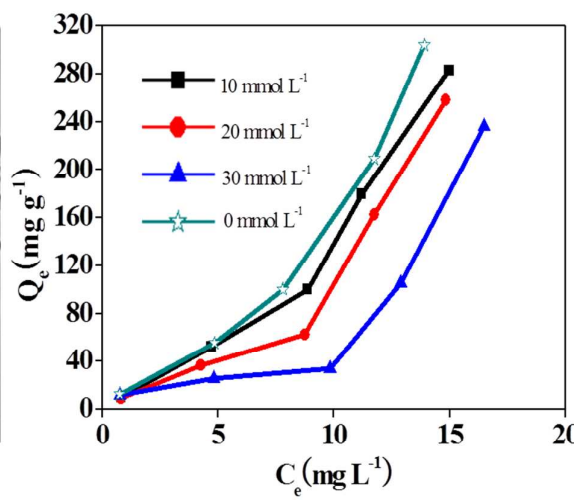
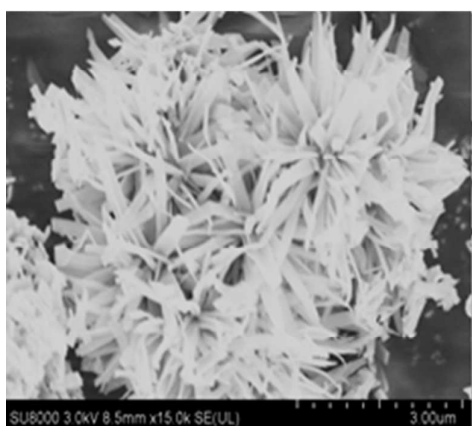
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A novel kind of nanoflakes zirconia-carbon ( $ZrO_2-C$ ) composites which exhibited much higher adsorption capacity to TCP



1           **Synthesis of flower-like ZrO<sub>2</sub>-C composites for adsorptive removal of**  
2                           **trichlorophenol from aqueous solution**

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20

## 21 ABSTRACT

22 In the current study, a novel kind of nanoflakes zirconia-carbon ( $\text{ZrO}_2\text{-C}$ )  
23 composites were synthesized through a simple method by using gallic acid and  $\text{ZrCl}_4$   
24 as precursor. The as-synthesized  $\text{ZrO}_2\text{-C}$  composites possessed high specific surface  
25 areas and chrysanthemum-like structure. High-resolution transmission electron  
26 microscope, X-ray photoelectron spectroscopy, infrared spectroscopy, X-ray  
27 diffraction, and Raman analysis revealed that  $\text{ZrO}_2\text{-C}$  composites were composed of  
28 graphitized carbon and numerous  $\text{ZrO}_2$  nanoparticles (3-4 nm in diameter).  $\text{ZrO}_2\text{-C}$   
29 composites were successfully used as adsorption materials to remove 2, 4, 6-  
30 trichlorophenol (TCP) from simulated water samples. The results showed that  $\text{ZrO}_2\text{-C}$   
31 exhibited much higher adsorption capacity to TCP than some reported carbon  
32 materials. The hydrophobic interaction and/or  $\pi\text{-}\pi$  stacking interaction between TCP  
33 and carbon phase, hydrogen bonding with functional groups of  $\text{ZrO}_2\text{-C}$ , and metal-  
34 anion binding with  $\text{ZrO}_2$  nanoparticles contributed to the high adsorption ability.  
35 Generally, TCP uptake was favorable at acidic environment and increased with the  
36 initial TCP concentration and temperature, the adsorption process obeyed the pseudo-  
37 second-order kinetics model and the adsorption isotherms could be better described  
38 by the Freundlich equation.

39 **Key Words:** Gallic acid, zirconia-carbon composites, Chrysanthemum-like structure,  
40 Adsorption, Trichlorophenol

41

## 42 Introduction

43 Chlorophenols are widespread used in petroleum refining, plastic, rubbers,  
44 pharmaceuticals, disinfectants, wood preserving, steel industries the pulp and paper  
45 industry. Due to their carcinogenic and mutagenic nature and high resistance to

46 biodegradation, chlorophenols pollutants are now receiving great concern<sup>1, 2</sup>. Many  
47 efforts have been made for the physicochemical (such as adsorption<sup>1-14</sup>, ozonation<sup>15-</sup>  
48 <sup>17</sup>, and electrochemical oxidation<sup>18</sup>) and biological treatment of chlorophenol-rich  
49 wastewater<sup>19, 20</sup>.

50 Over the last century, much research has occurred in the area of removal of  
51 chlorophenols by carbon materials, including activated carbon, carbon nanotubes,  
52 graphene, and mesoporous carbon, which demonstrates high removal efficiency to  
53 organic pollutants<sup>1-10</sup>. Soil, metal oxides and zeolite have been explored as  
54 adsorbents to remove chlorophenols from aqueous solutions as well<sup>11-14, 21-23</sup>. The  
55 sorption of chlorophenols on these inorganic adsorbents proceeded via different  
56 reaction mechanisms, including inner- or outer-sphere coordination, H-bonding,  
57 ligand exchange between the OH groups of phenolic compounds and the active sites  
58 (hydroxyl groups) of adsorbents, and complexation of phenolate anions with metal  
59 ions on the surface of adsorbents. Yousef et al. showed that the adsorption capacity of  
60 chlorophenols onto natural zeolites reached 0.32 mmol g<sup>-1</sup>, which was comparable  
61 with those obtained by some carbon materials<sup>11</sup>. Therefore, metal oxides, soil or  
62 zeolites can be regarded as potential adsorbents to remove chlorophenols from  
63 environmental waters.

64 Herein a kind of combination of carbon materials and metal oxides has been put  
65 forward, which can provide multiple adsorptive sites and different interaction  
66 mechanisms to chlorophenols. Gallic acid (GA), a phenolic compound belonging to  
67 the hydroxybenzoic acids, is highly present in legums (onions, black radish, hops),  
68 fruits (grapes, some red fruits), nuts (gallnuts) and beverages (team wine, beer). GA  
69 can form a complex with Fe(II), Fe(III), Cu(II), Al(III), Zr(IV), and Mo(VI), et al<sup>24-</sup>  
70 <sup>28</sup>. GA has been used in the green synthesis of AgNPs and AuNPs as well<sup>29</sup>.  
71 However, to the best of our knowledge, GA has not been utilized as organic ligands

72 to synthesize hierarchical structured nanoparticles. In the current study, we use GA as  
73 both organic ligands and carbon precursor to prepare carbon and metal oxides  
74 composites. Zirconium oxides are used as metal precursors due to the excellent  
75 chemical stability of Zr-based inorganic or organic materials<sup>30</sup>. The synthesis method  
76 of ZrO<sub>2</sub>-C composites is very simple with high yields. The as-prepared ZrO<sub>2</sub>-C  
77 composites possess chrysanthemum-like structure and are used as adsorbents to  
78 remove 2, 4, 6-trichlorophenol from water.

79

## 80 **2. Experimental section**

### 81 **2.1. Chemicals and materials**

82 Zirconium tetrachloride, hydrochloric acid (HCl, 36%~38%), ethanol, and N,N-  
83 dimethylformamide (DMF, 99.5%) were purchased from Sinopharm Chemistry  
84 Reagent Co., Ltd. (Beijing, China). 2, 4, 6-trichlorophenol (TCP) and gallic acid  
85 were obtained from J&K Chemical Ltd. (Beijing, China). TCP (100 mg L<sup>-1</sup>) was  
86 prepared and diluted to certain concentration when it was necessary. Ultrapure water  
87 used in all of the experiments was prepared by using Milli-Q SP reagent water  
88 system (Millipore, Bedford, MA, USA).

### 89 **2.2 Synthesis and structure of ZrO<sub>2</sub>-C**

90 Firstly, ZrCl<sub>4</sub> (0.933g) was dissolved in 5 mL of ethanol, and then mixed with 65  
91 mL of DMF; after that 0.753g of gallic acid were added to the mixture under stirring.  
92 The reaction solution was transferred in Teflon-lined stainless-steel autoclave, sealed  
93 to heat at 403 K for 24 h. The white products were washed with DMF three times  
94 and soaked in ethanol for three days (change ethanol each day) and dried at 323 K  
95 under vacuum environment for 12h. Finally, the product (1.348g) was removed to a  
96 quartz tube to carbonize under the protection of nitrogen at 1073 K for 4h.

### 97 **2.3 Characterization of the material**

98 The size and morphology of the synthesized materials were surveyed using a  
99 Hitachi S-5500 field-emission scanning electron microscope (FE-SEM, Tokyo, Japan)  
100 equipped with an energy dispersive X-ray spectrometer (SEMEDX, Tokyo, Japan), a  
101 JEOL JEM-2010 high-resolution transmission electron microscope (HRTEM, Kyoto,  
102 Japan), and a Hitachi H-7500 transmission electron microscope (TEM, Tokyo,  
103 Japan). The crystalline phase of products were analyzed using X-ray powder  
104 diffraction (XRD, Almelo, Netherlands) by using a Cu K $\alpha$  radiation ranging from 5  
105 to 90° with a resolution of 0.02°. BET methods were adopted to measure the surface  
106 area, pore size and volume (ASAP2000 V3.01A; Micromeritics, Norcross, GA).  
107 FTIR spectra were recorded in the range of 4000-400 cm<sup>-1</sup> by a NEXUS 670 Infrared  
108 Fourier Transform Spectrometer (Nicolet Thermo, Waltham, MA) after pelletizing  
109 with KBr. Thermogravimetry and differential thermal analysis (TG-DTA) for freeze-  
110 dried samples were carried out on a Mettler Toledo Star TGA/SDTA 851 apparatus,  
111 and the temperature ranged from room temperature to 1173 K with rising rate of 10  
112 K min<sup>-1</sup>. The sample chamber was purged with dry nitrogen. To detect the  
113 composition and chemical state of elements on the surface of materials, the products  
114 were analyzed using X-Ray photoelectron spectroscopy (XPS) collected on an  
115 ESCA-Lab-200i-XL spectrometer (Thermo Scientific, Waltham, MA) with  
116 monochromatic Al K $\alpha$  radiation (1486.6 eV).

### 117 **2.4 Absorptive removal of pollutants**

118 Absorption experiments were conducted in the simulated polluted water (10mL) in  
119 batch experiment. The concentration of adsorbent was 0.02g L<sup>-1</sup>. The solution pH  
120 was adjusted with HCl and NaOH to desired values, and the ionic strength was  
121 adjusted with 1 M NaCl. The effect of initial pH on the sorption of TCP was studied

122 in the pH range of 3.0-10.0. Dynamic experiments were operated under the condition  
123 of temperature 303K and TCP 20 mg L<sup>-1</sup>. The influence of ionic strength was tested  
124 by adding NaCl (10, 20, and 30 mM) in solution. To investigate the thermodynamic  
125 properties, adsorption isotherms were recorded in 10 mL of TCP solution with  
126 concentrations of TCP varying from 0.5 to 20 mg L<sup>-1</sup> at 303K, 313K, and 323K,  
127 respectively. All experiments were conducted in triplicate, and average results were  
128 reported.

129 We calculated the maximum and equilibrium adsorption quantity by measuring the  
130 concentration of the original TCP and equilibrium TCP in the whole process. The  
131 formula of adsorption as follows:

$$132 \quad q_e = \frac{(C_0 - C_e) V}{m} \quad (1)$$

133 where  $q_e$  (mg g<sup>-1</sup>) is on behalf of the equilibrium adsorption quantity;  $C_0$  (mg L<sup>-1</sup>)  
134 and  $C_e$  (mg L<sup>-1</sup>) is the original and equilibrium concentration of TCP;  $m$  (g) is the the  
135 quality of adsorbent; and  $V$  (L) is the volume of the solution which is original.

136 The dosage of TCP was detected by HPLC system equipped with a DIONEX HPLC  
137 pump (P680), a thermostatted column compartment (TCC-100) and a photodiode  
138 array detector (PDA-100). Separations were conducted on a Dikma C18 column (250  
139 ×4.6 mm; 5 μm). The mobile phase for TCP was acetonitrile: 2% HAc (80:20 V/V)  
140 at a flow rate of 1 mL min<sup>-1</sup>. The wavelength was set at 290 nm.

### 141 **3. Results and discussion**

#### 142 **3.1 Characterization and properties of adsorbents**

143 **Fig 1** shows the TEM and SEM images of the as-prepared materials. The Zr-GA  
144 particles shape like chrysanthemum with the size of about 4μm (Fig. 1A and 1B).  
145 High resolution TEM image of Zr-GA indicates that this material is composed of



146 nanoflakes (Fig. 1C) with  $\sim 350$  nm in width. After carbonization, the  
147 chrysanthemum-like shape remains, the particle size of  $\text{ZrO}_2\text{-C}$  composites decreases  
148 to about  $2\mu\text{m}$  (Fig. 1D and E). Fig. 1F and 1G demonstrate that the nanoflakes of Zr-  
149 GA have reduced to about 100-300 nm in width and contain numerous tiny  
150 nanoparticles (3-4 nm in diameter) which should be  $\text{ZrO}_2$ .

151 The crystal phases of the samples are investigated by XRD analysis. **Fig. 2**  
152 displays that the XRD pattern of Zr-GA is totally different with that of  $\text{ZrO}_2$  and GA  
153 powder. The peaks occurring at  $7.2^\circ$ ,  $9.0^\circ$ ,  $11.3^\circ$ ,  $16.8^\circ$ ,  $17.3^\circ$ ,  $21.3^\circ$ ,  $23.5^\circ$ ,  $26.3^\circ$ ,  
154  $28.5^\circ$ ,  $31.1^\circ$ ,  $36.6^\circ$  were basically conformed to Zr-MOF which are synthesized by  
155 zirconium metal salts and organic compounds with carboxyl group in other studies<sup>31-</sup>  
156 <sup>34</sup>. Since the organic ligands (gallic acid) in our study are different with the traditional  
157 organic ligands used to synthesize MOF, a little deviation of the some peaks may occur. The  
158 characteristic peaks suggest the chelation of Zr atoms with GA in Zr-GA. In the XRD  
159 pattern of  $\text{ZrO}_2\text{-C}$ , the distinguishing characteristic peaks appear at  $2\theta=30.1^\circ$ ,  $35.4^\circ$ ,  
160  $50.2^\circ$ , and  $60.2^\circ$ , which can be attributed to the (101), (002), (112), and (211)  
161 diffraction planes of the tetragonal zirconia<sup>35,36</sup>.

162 **Fig. 3A** shows the IR spectra of GA, Zr-GA and  $\text{ZrO}_2\text{-C}$ . In the spectrum of GA,  
163 the broad peaks at  $3368\text{ cm}^{-1}$  and  $3287\text{ cm}^{-1}$  are corresponding to the phenolic groups.  
164 The peaks ranged in  $3200\text{-}2500\text{ cm}^{-1}$  are associated with the bending or stretching  
165 vibration of carboxylic acid O-H and C-H in aromatic groups. The sharp peak at  
166  $1701\text{ cm}^{-1}$  is due to the C=O stretching vibration from carboxylic groups. The peaks  
167 in the region of  $1500\text{-}1000\text{ cm}^{-1}$  are assigned to the stretching vibration of C-O,  
168 binding adsorption of O-H of carboxylic and phenolic groups and C-H of aromatic  
169 rings (Fig 3B). After interaction with Zr (IV), the O-H stretching band in the region  
170 of  $3400\text{-}2500\text{ cm}^{-1}$ , Zr-O-H bending peaks at  $1332\text{ cm}^{-1}$ , and O-H of carboxylic  
171 groups bending band at  $1029\text{ cm}^{-1}$  disappear, indicating that all the phenolic groups

172 and carboxylic groups in GA chelate with Zr. Correspondingly, C=O stretching bend  
173 in the spectrum of Zr-GA shift to low frequency, and two characteristic bands of the  
174 carboxylate groups (COO<sup>-</sup>) between 1300 and 1600 cm<sup>-1</sup> appear. Asymmetrical  
175 stretching of carboxylate groups occurs at 1500 cm<sup>-1</sup> with stretching at 1426 cm<sup>-1</sup>.  
176 These results indicate that all the carboxylic and phenolic groups in the molecules  
177 interact with Zr. Actually, the carboxylic groups are vital for the formation of  
178 chrysanthemum-like structure of materials. If tannic acid is adopted as linker, the  
179 hierarchical morphology of the as-prepared products could not be observed. In the  
180 spectrum of ZrO<sub>2</sub>-C, the characteristic peaks for carboxylic groups, phenolic groups  
181 and benzene rings generally disappear, suggesting the successful carbonization of  
182 GA; the broad peaks in the region of 3600-3300 cm<sup>-1</sup>, and 1670-1550 cm<sup>-1</sup> are  
183 corresponding to the surface-sorbed water and hydroxyl groups of carbon materials.

184 XPS was adopted to investigate the elemental composition on the surface of Zr-  
185 GA before and after carbonization. Curve-fitting of the O1s and Zr3d lines for both  
186 materials employed Gaussian (20%)-Lorentzian (80%) peak-shapes, respectively  
187 (defined in Casa XPS as GL (80)). The O1s core levels for Zr-GA present three main  
188 components related to C-OH, COO<sup>-</sup> and H<sub>2</sub>O species. (Fig. 4A). The Zr3d spectra of  
189 Zr-GA are characterized by doublet terms of Zr3d<sub>3/2</sub> and Zr3d<sub>5/2</sub> due to spin-orbit  
190 coupling, and the positions of Zr3d<sub>5/2</sub> and Zr3d<sub>3/2</sub> peaks locate at 182.5 and 185.0  
191 eV (Fig. 4B), respectively, which is consistent with the zirconium (IV) cations  
192 coordinated carboxylic oxygens of organic ligands in zirconium metal-organic  
193 framework and amine-functionalized zirconium metal-organic framework<sup>38</sup>. After  
194 carbonization, the O1s core-level shifts to lower binding energies with the  
195 disappearance of H<sub>2</sub>O species and significant decrease of the contents of C-OH and  
196 COO<sup>-</sup> species, meanwhile, the Zr-O bond appears. The Zr3d spectra intensity of  
197 ZrO<sub>2</sub>-C increases obviously, and the positions of Zr3d peaks are observed to shift to

198 lower binding energies (182.4 and 184.8 eV, respectively). Generally, the Zr 3d  
199 spectra of Zr-GA and ZrO<sub>2</sub>-C are in good agreement with the reported values for  
200 Zr(IV) cations. Wang<sup>39</sup> and co-workers found that the binding energy of the Zr3d in  
201 hybrid ZrO<sub>2</sub>/polymer nanoparticles was higher than that in ZrO<sub>2</sub>, suggesting the  
202 formation of chemical bonds between the Zr(IV) and the organic components.  
203 Similar with the case of zirconium metal-organic framework, we deduce that the Zr  
204 atoms coordinate the oxygen atoms from gallic acids in the chrysanthemum-like Zr-  
205 GA structure; while zirconium transforms to ZrO<sub>2</sub> in the process of carbonization. In  
206 Raman spectrum of ZrO<sub>2</sub>-C (**Fig. 4C**), two peaks centered at 1580 (G-line) and 1350  
207 cm<sup>-1</sup> (D-line), attributing to in-plane vibrations of crystalline graphite and disordered  
208 amorphous carbon, respectively, suggesting that the GA linkers are successfully  
209 graphitized. The above-mentioned results imply that ZrO<sub>2</sub>-C is composed of ZrO<sub>2</sub>  
210 and graphitized carbon.

211 The TGA curve of ZrO<sub>2</sub> (**Fig. 4D**) shows slight weight decreases below 473 K due  
212 to the initial loss of water. When the heat temperature is above 623 K, carbon phase  
213 in the ZrO<sub>2</sub>-C decomposes promptly suggesting the oxidation of carbon. The percent  
214 remaining after 713 K can be regarded as absolutely ZrO<sub>2</sub>. According to the TGA  
215 result of ZrO<sub>2</sub>-C, the mass percentage of carbon is estimated to be 40 %. The N<sub>2</sub>  
216 adsorption/desorption isotherm and calculated pore size distribution of ZrO<sub>2</sub>-C (**Fig.**  
217 **4E**) suggests that the adsorption process conform to the IV-type with a H3-type  
218 hysteresis loops, indicating that the pore belongs to mesoporous. The total pore  
219 volume of ZrO<sub>2</sub>-C was determined to be 0.25 cm<sup>3</sup> g<sup>-1</sup>. The average pore size  
220 calculated from desorption branch of the N<sub>2</sub> isotherm by Barrett-Joyner-Halenda  
221 (BJH) method was 3.8 nm, and the Brunauer-Emmett-Teller (BET) surface area of  
222 the obtained ZrO<sub>2</sub>-C composite was 79.4 m<sup>2</sup> g<sup>-1</sup>.

### 223 3.2 Adsorption kinetics

224 The kinetics of TCP adsorption onto ZrO<sub>2</sub>-C was analyzed using both the pseudo-  
225 first-order and pseudo-second order kinetic models. The pseudo-first-order kinetic  
226 model is defined as follows:

$$227 \quad \ln(q_e - q_t) = \ln q_e - k_1 t \quad (2)$$

228 where  $q_e$  (mg g<sup>-1</sup>) and  $q_t$  (mg g<sup>-1</sup>) are the amounts of TCP adsorbed at equilibrium  
229 and any time  $t$  (h), respectively, and  $k_1$  (h<sup>-1</sup>) is the adsorption rate constant.

230 The pseudo-second-order constants were calculated according to equation (3):

$$231 \quad \frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{1}{q_e} t \quad (3)$$

232 where  $k_2$  (g mg<sup>-1</sup>·h<sup>-1</sup>) is the pseudo-second-order rate constant.

233 As shown in **Fig. 5A**, TCP adsorption increased rapidly with time and reached a  
234 constant value in 10 h. The kinetic parameters and correlation coefficient ( $R^2$ )  
235 obtained for the plots are given in **Table 1**. As a result, the  $R^2$  value of pseudo-  
236 second-order kinetic model is 0.994 and the calculated  $q_{e,cal}$  is very close to the  
237 experimental  $q_{e,exp}$ , demonstrating that the kinetics data fits well with the pseudo-  
238 second-order kinetic model.

### 239 3.3 Effect of pH

240 The pH of solution is one of the main factors affecting the adsorption capacity of  
241 compounds that can be ionized. The surface chemistry of carbon adsorbents may  
242 change with solution pHs. These effects may result in significant alterations in the  
243 removal efficiency of TCP depending on the pHs. **Fig. 5B** shows that the uptake of  
244 TCP on ZrO<sub>2</sub>-C is superior in acid solution to those in neutral and alkali solutions,  
245 which is resemble with the optimum pH range observed on other carbonaceous  
246 materials<sup>37, 40, 41</sup>. In the current study, the adsorption capacity of TCP on ZrO<sub>2</sub>-C is  
247 the highest at pH 4.0, and then declines with rising of solution pH. Since the pK<sub>a</sub> of  
248 TCP is pH 5.99<sup>42</sup>, the majority of TCP exists in the neutral and unionized forms in

249 acid solution; and ionizes gradually and becomes negatively charged as solution pH  
250 is higher than 5.99. To interpret the effect of solution pH on TCP adsorption, we also  
251 measured  $\zeta$ -potentials of ZrO<sub>2</sub>-C in aqueous solutions. The isoelectric point (IEP) of  
252 ZrO<sub>2</sub>-C is found at about pH 3.5 (**Fig. 5C**). At pH 3.5-4.0, both TCP and ZrO<sub>2</sub>-C  
253 surface are neutral, which favors the hydrophobic interaction and/or  $\pi$ - $\pi$  stacking  
254 interaction between TCP and ZrO<sub>2</sub>-C. When the solution pH is lower than 3.5, the  
255 surface of the material is positively charged and the hydrophobic interaction between  
256 TCP and ZrO<sub>2</sub>-C is weakened. So the adsorption capacity will decline under the  
257 condition of strong acid (pH<3.5). On the other hand, the neutral formed TCP also  
258 can form H-bonds with the oxygen-containing groups of carbon phase and ZrO<sub>2</sub>  
259 nanoparticles of the adsorbents.

260 In neutral and alkaline solution, electrostatic repulsions between the negative  
261 surface of ZrO<sub>2</sub>-C and anionic TCP are expected, leading to decreased adsorption of  
262 TCP on ZrO<sub>2</sub>-C. However, the downshift of TCP sorption in the pH range 6-10 is  
263 fairly slow, and the sorption capacity is still considerable at pH 12. This trend is  
264 obviously different with that obtained on most carbon materials such as graphene and  
265 graphene oxide<sup>6</sup>, multi-walled carbon nanotubes<sup>7</sup>, and surfactant-modified bentonite<sup>6</sup>.  
266 It was reported that the phenolate anions can complex with metal ions on the metal  
267 oxides, and zeolite surface, which proceeds via a kind of charge transfer from  
268 phenolate anions to empty d-orbitals of metal (such as Si, Al, Fe, Ti, Mn) on the  
269 surface of metal oxides<sup>11-13, 21-23</sup>. Okolo et al. suggested that the benzene ring ( $\pi$   
270 electron) rather than the hydroxyl substituent of phenols interacts with synthetic  
271 zeolite surface<sup>23</sup>. Karunakaran and co-workers<sup>43</sup> assumed that the acidic sites on the  
272 surface of ZrO<sub>2</sub> may coordinate to the phenolic oxygen and/or the basic O<sup>-</sup> group  
273 may be involved in hydrogen bonding with the -OH group of phenol. Since the  
274 electron density of phenol rings increases with solution pH, we believe that the

275 considerate adsorption of TCP on ZrO<sub>2</sub>-C composites at higher solution pH result  
276 from complexation of TCP anions with Zr ions on the surface of large number of  
277 inlaid ZrO<sub>2</sub> NPs. On the other hand, in our previous work, we used magnetic  
278 mesoporous carbon which is composed of graphitic carbon and Fe<sub>3</sub>C/ $\alpha$ -Fe, as  
279 adsorbents to remove TCP as well. The specific surface area and carbon content of  
280 this material (220 m<sup>2</sup>g<sup>-1</sup> and 54.5%, respectively) are larger than those of ZrO<sub>2</sub>-C  
281 synthesized in this study. However, the adsorption capacity of the magnetic  
282 mesoporous carbon to TCP at 303 K was much lower than that achieved on ZrO<sub>2</sub>-C  
283 at pH 4. We deduce that the adsorption of TCP onto ZrO<sub>2</sub>-C proceeds via  
284 hydrophobic interaction and/or  $\pi$ - $\pi$  stacking interaction with carbon phase, hydrogen  
285 bonding with functional groups of ZrO<sub>2</sub>-C, and/or complexation with Zr(IV) cations  
286 (especially at high solution pH).

### 287 **3.4 Adsorption isotherm**

288 The effect of solution temperature on TCP adsorption was investigated by varying  
289 the temperature at 303, 313 and 323 K, respectively. As a result, the adsorption  
290 capacity of TCP on ZrO<sub>2</sub>-C enhances slightly with temperature, indicating the  
291 endothermic nature of the sorption process. Langmuir and Freundlich isotherm  
292 models were used to study the relationship between the adsorption quantity of TCP  
293 onto ZrO<sub>2</sub>-C and its equilibrium concentration in water solution. The Langmuir  
294 model is widely used for the adsorption assuming that takes place specific  
295 homogeneous; while the Freundlich model assumes that the binding takes place on a  
296 heterogeneous adsorption surface with multilayer adsorption.

297 The linear form of the Langmuir isotherm equation is expressed as:

$$298 \quad \frac{C_e}{q_e} = \frac{1}{K_L Q_0} + \frac{1}{Q_0} C_e \quad (4)$$

299 where  $C_e$  (mg L<sup>-1</sup>),  $q_e$  (mg g<sup>-1</sup>) and  $Q_0$  (mg g<sup>-1</sup>) are equilibrium concentration,

300 equilibrium adsorption quantity and single largest adsorption quantity, respectively.

301  $K_L$  is a constant related to the free energy of the adsorption ( $L\text{ mg}^{-1}$ ).

302 The logarithmic form of the Freundlich equation is described as following:

$$303 \quad \ln q_e = \ln K + \frac{1}{n} \ln C_e \quad (5)$$

304 where  $K_F$  ( $(\text{mg g}^{-1})(L\text{ mg}^{-1})^{1/n}$ ) and  $n$  are the Freundlich constants that point to  
305 the sorption capacity and adsorption intensity of the adsorbent, respectively.

306 Table 2 lists the constants and correlation coefficients gained from the two isotherm  
307 models. The Freundlich model yields better fit with higher  $R^2$  values (higher than  
308 0.986), indicating that the Freundlich isotherm is more suitable in describing the  
309 adsorption of TCP on  $ZrO_2$ -C. The  $1/n$  value obtained from the Freundlich model is  
310 below 1 representing that adsorption of TCP on the  $ZrO_2$ -C is favorable. This result  
311 is consistent with TCP sorption on other carbon materials such as Loosestrife-based  
312 activated carbon<sup>8</sup>, activated clay<sup>12</sup> and commercial grade coconut shell-based  
313 activated carbon<sup>4</sup>.

314 Because TCP sorption on  $ZrO_2$ -C does not fit well to Langmuir equation, we can  
315 make a coarse estimate of the adsorptive ability of  $ZrO_2$ -C to organic pollutants by  
316 comparing the adsorption capacity calculated at a certain concentration with those  
317 obtained by other adsorbents reported in literature. The results are listed in Table 3.  
318 In despite of its relatively low specific surface areas and small porous volume, the  
319 sorption ability of  $ZrO_2$ -C to TCP is much higher than those obtained on many kinds  
320 of carbon-based materials reported previously. This may result from the joint  
321 contribution of  $ZrO_2$  NPs and carbon phase of  $ZrO_2$ -C adsorbents to TCP sorption.

### 322 **3.5 Adsorption thermodynamics**

323 The thermodynamic equation is as following:

$$\ln K_d = \frac{\Delta S^0}{R} - \frac{\Delta H^0}{RT} \quad (6)$$

$$\Delta G^0 = \Delta H^0 - T \Delta S^0 \quad (7)$$

326 In the formula 6  $K_d$  is the distribution coefficient of adsorbent, equal to  $q_e/c_e$ ,  $R$   
327 (8.314 J mol<sup>-1</sup> K<sup>-1</sup>) is the universal gas constant,  $T$  (K) is the temperature.  $\Delta G^0$  can  
328 figure up by  $\Delta H^0$  and  $\Delta S^0$ .

329 The values of the thermodynamic parameters for the adsorption of TCP on  
330 mesoporous carbon materials are listed in Table 4. The value of  $\Delta H^0$  is positive  
331 suggesting that the reaction is endothermic, which is consistent with the result that  
332 TCP uptake increases with temperature. If  $\Delta H^0$  is higher than 40 kJ mol<sup>-1</sup>, the  
333 adsorption process is supposed to proceed via chemisorption; while for values less  
334 than 40 kJ mol<sup>-1</sup>, the adsorption process is of physical nature. The value of  $\Delta H^0$  is  
335 8.7 kJ mol<sup>-1</sup>, indicating that the main interaction between TCP and mesoporous  
336 carbon materials is of physical nature. The positive value of  $\Delta S^0$  suggests that the  
337 adsorption is irreversible. The negative value of  $\Delta G^0$  shows the spontaneous nature  
338 of the adsorption process.

### 339 3.6 Effect of ionic strength

340 The effect of ionic strength on TCP adsorption was investigated by conducting  
341 adsorption equilibrium experiments with different concentrations of NaCl at pH 4.  
342 As shown in **Fig. 5D**, the adsorption capacity of ZrO<sub>2</sub>-C to TCP decreases by 7, 15  
343 and 23% as the NaCl concentration is 10, 20, and 30 mM, respectively. This result  
344 indicates that the hydrophobic interaction and/or  $\pi$ - $\pi$  stacking interaction between  
345 TCP and ZrO<sub>2</sub>-C are stronger than non-specific electrostatic interactions, since the  
346 electrostatic interactions can be weakened by increased ionic strength of the solution.

### 347 4. Conclusion



348 We have synthesized ZrO<sub>2</sub>-C composites with chrysanthemum-like morphology  
349 using a simple method with high yield. The ZrO<sub>2</sub>-C composites exhibit excellent  
350 water stability and remarkable adsorption capacity to chlorophenols. The  
351 hydrophobic interaction and/or  $\pi$ - $\pi$  stacking interaction and hydrogen-bonds between  
352 TCP and ZrO<sub>2</sub>-C contribute to the fantastic adsorption of TCP on the material.  
353 Besides, ZrO<sub>2</sub> nanoparticles embedded in the carbon phase can form metal-anion  
354 bonds with TCP, which is responsible for the reasonable adsorption ability of ZrO<sub>2</sub>-C  
355 to TCP even in weak alkali solution. The adsorption of TCP on ZrO<sub>2</sub>-C is slightly  
356 influenced by temperature and ionic strength. These results provide effective method  
357 and reference for the removal of TCP in wastewater.

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452 **Table 1** The pseudo-first-order and pseudo-second rate constants for the adsorption  
 453 of TCP on ZrO<sub>2</sub>-C

	$q_{e,exp}$ (mg g <sup>-1</sup> )	Pseudo-first-order			Pseudo-second-order		
		$q_{e,cal}$ (mg g <sup>-1</sup> )	$k_1$ (h <sup>-1</sup> )	$R^2$	$q_{e,cal}$ (mg g <sup>-1</sup> )	$K_2$ (h <sup>-1</sup> )	$R^2$
TCP	306	158	0.2524	0.9146	312.5	0.0039	0.9974

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489 **Table.2** Langmuir and Freundlich parameters for the adsorption of TCP on ZrO<sub>2</sub>-C at  
490 different temperature

Solution temperature(K)	Langmuir isotherm model			Freundlich isotherm model		
	Q <sub>0</sub> (mg g <sup>-1</sup> )	K <sub>L</sub> (L mg <sup>-1</sup> )	R <sup>2</sup>	K (mg g <sup>-1</sup> (L mg <sup>-1</sup> ) <sup>1/n</sup> )	1/n	R <sup>2</sup>
303	454.5	0.090	0.7489	32.422	0.749	0.9863
313	476.2	0.095	0.8139	34.655	0.743	0.9906
323	476.2	0.117	0.9401	38.303	0.748	0.9941

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493 **Table 3** summarizes the comparison of TCP adsorption capacity on various  
 494 adsorbents

Adsorbent	T(K)	$Q_e$ (mg g <sup>-1</sup> ) ( $C_0=20$ mg L <sup>-1</sup> )	Reference
Zirconium dioxide-carbon	303	306	This study
Graphene oxide	303	190	6
Coconut husk-based activated carbon	303	122	5
Graphene	298	50	7
CFAC	293	192	9
Coconut shell-based activated carbon	303	112	4
MMC	303	210	10
Commercial activated carbon	303	20	4
Activated clay	303	123	12

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**Table 4** Thermodynamic parameters calculated

$\Delta H^0$ (KJ mol <sup>-1</sup> )	$\Delta S^0$ (J mol <sup>-1</sup> K <sup>-1</sup> )	$\Delta G^0$ (KJ mol <sup>-1</sup> K <sup>-1</sup> )		
		303K	313K	323K
4.105	38.49	-7.56	-7.94	-8.33

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499 **Figures Captions**500 **Fig.1.** SEM images of Zr-GA (A) and ZrO<sub>2</sub>-C (D), TEM images of Zr-GA(B, C), Zr-501 GA-C(E, F) , HRTEM image of ZrO<sub>2</sub>-C(G).502 **Fig.2.** XRD spectra of GA, Zr-GA and ZrO<sub>2</sub>-C from 2 $\theta$ =5 to 80°503 **Fig.3.** FTIR spectra of GA, Zr-GA and ZrO<sub>2</sub>-C (A) and FTIR spectra of GA and Zr-504 GA in the region of 400-1800 cm<sup>-1</sup> (B).505 **Fig.4.** The fitted XPS O1s spectra (A) and Zr3d core level lines (B) of Zr-GA and506 ZrO<sub>2</sub>-C, Raman spectra (C), TGA curves (D) and N<sub>2</sub> adsorption/desorption isotherm507 (E) of ZrO<sub>2</sub>-C. Inset D describes the calculated pore size distribution of ZrO<sub>2</sub>-C.508 **Fig.5.** Effect of time (A) and solution pH (B) and ionic strength (D) on TCP509 adsorption to ZrO<sub>2</sub>-C;  $\zeta$ -potential of ZrO<sub>2</sub>-C at different solution pHs (C).

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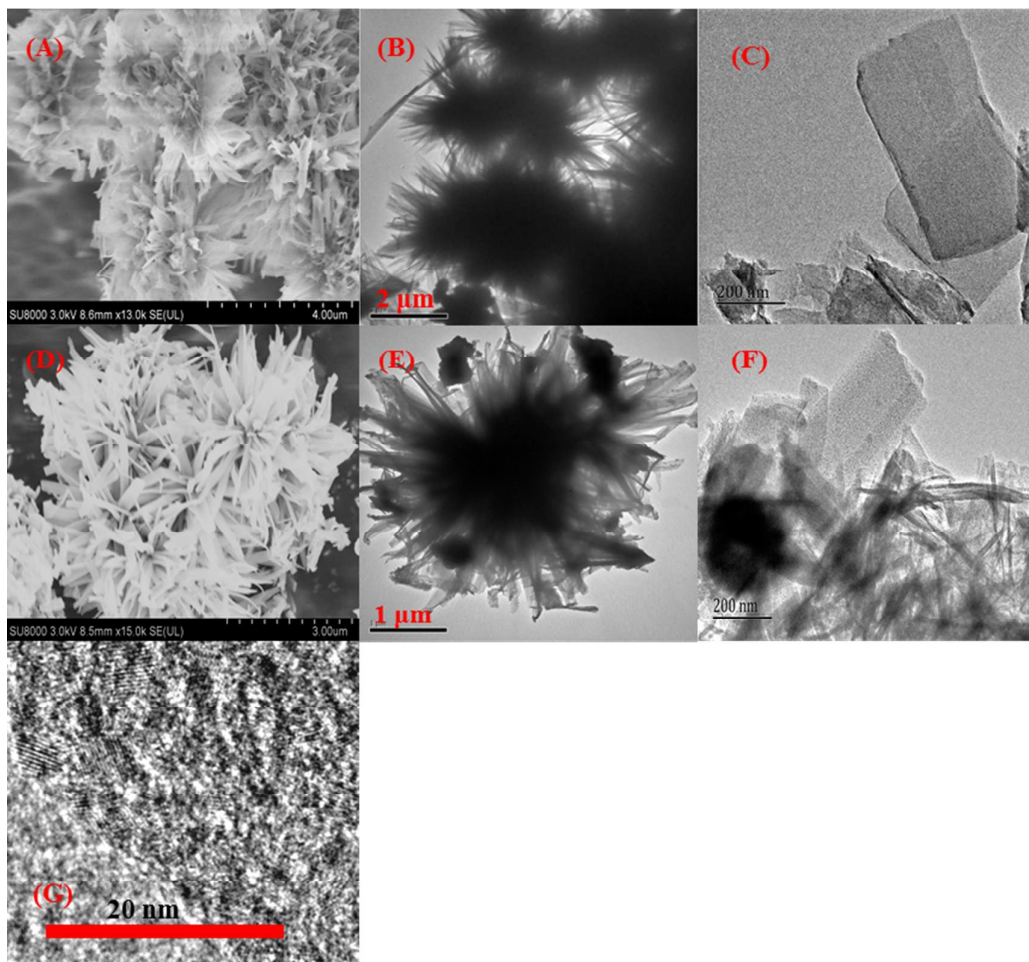
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Fig. 1

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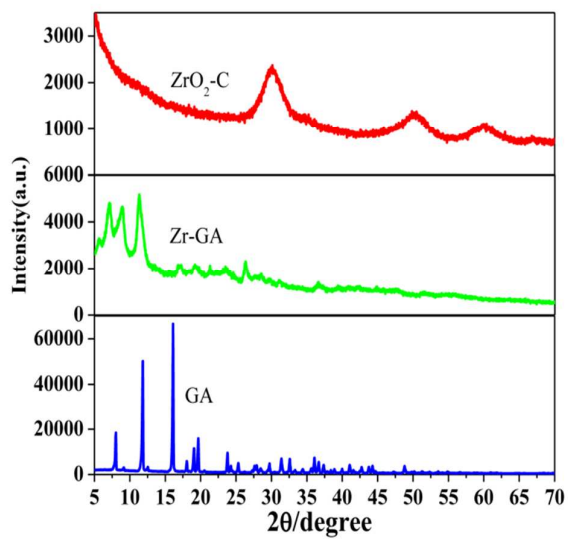
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Fig. 2

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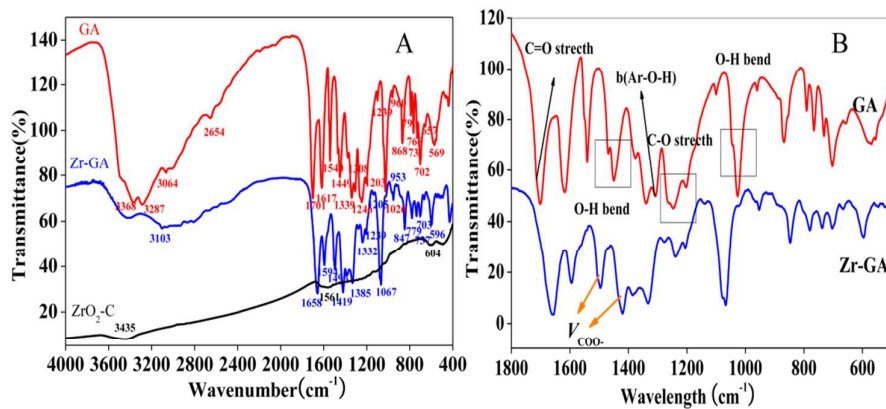
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Fig. 3



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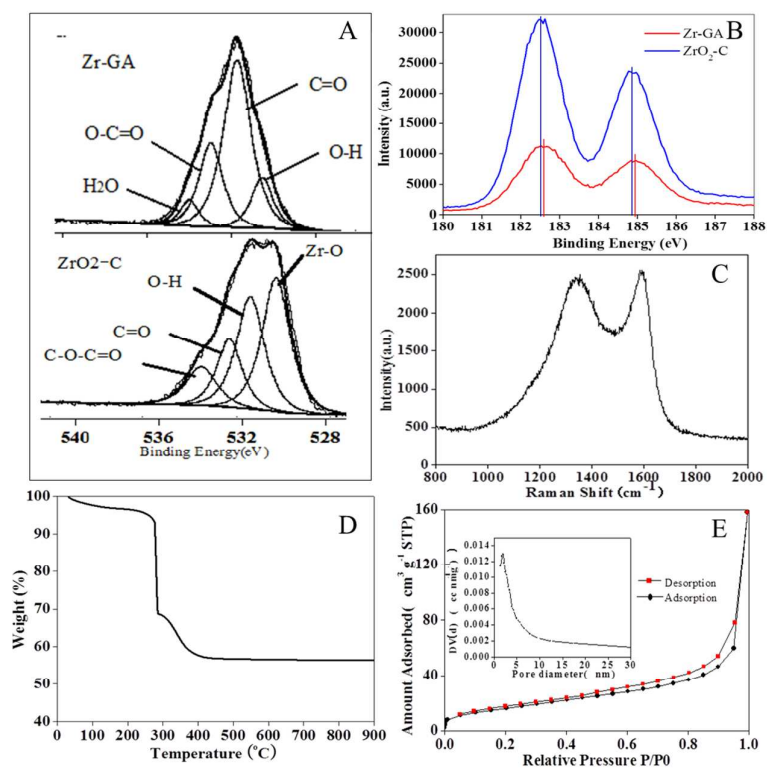
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Fig. 4



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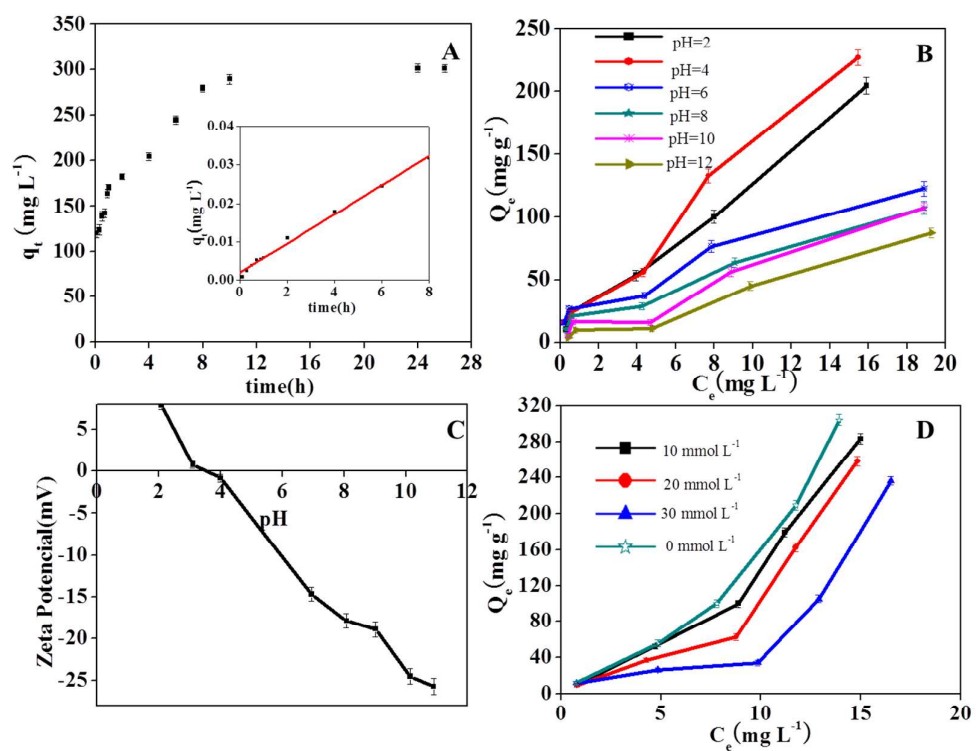
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Fig. 5



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