

This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. This Accepted Manuscript will be replaced by the edited, formatted and paginated article as soon as this is available.

You can find more information about *Accepted Manuscripts* in the **Information for Authors**.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard <u>Terms & Conditions</u> and the <u>Ethical guidelines</u> still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.



www.rsc.org/advances

# Aggregate-based sub-CMC Solubilization of Hexadecane by Surfactants

Hua Zhong<sup>1,2,3\*</sup>, Lei Yang<sup>1,2</sup>, Guangming Zeng<sup>1,2</sup>, Mark L. Brusseau<sup>3</sup>, Yake Wang<sup>3</sup>,

Yang Li<sup>4</sup>, Zhifeng Liu<sup>1,2</sup>, Xingzhong Yuan<sup>1,2</sup>, Fei Tan<sup>1,2</sup>

<sup>1</sup> College of Environmental Science and Engineering, Hunan University, Changsha

410082, China;

<sup>2</sup> Key Laboratory of Environmental Biology and Pollution Control (Hunan

University), Ministry of Education, Changsha, 410082, China;

<sup>3</sup> Department of Soil, Water and Environmental Science, University of Arizona,

Tucson, Arizona 85721, U.S.A;

<sup>4</sup> Department of Chemistry, University of Science and Technology of China, Hefei,

230026, China.

Submitted to:

RSC Advances

26 June 2015

Email Addresses:

Hua Zhong:	zhonghua@email.arizona.edu
Lei Yang:	wlwyanglei@126.com
Guangming Zeng:	zgming@hnu.edu.cn
Mark L Brusseau:	brusseau@email.arizona.edu
Yake Wang:	yakew@email.arizona.edu
Yang Li:	ly2013fi@mail.ustc.edu.cn
Zhifeng Liu:	lzf18182002@163.com
Xingzhong Yuan:	yxz@hnu.edu.cn
Fei Tan:	tanfei_2013@163.com

Table of contents entry:



SDBS or Triton X-100 at sub-CMC concentrations enhances hexadecane solubilization due to aggregate formation mechanism. The sub-CMC aggregate size decreases with increasing surface excess of surfactant.

# 1 Abstract

2 Solubilization of hexadecane by two surfactants, SDBS and Triton X-100, at 3 concentrations near the critical micelle concentration (CMC) and the related aggregation behavior was investigated in this study. Solubilization was observed at 4 5 surfactant concentrations lower than CMC, and the apparent solubility of hexadecane increased linearly with surfactant concentration for both surfactants. The 6 7 capacity of SDBS to solubilize hexadecane is stronger at concentrations below CMC 8 than above CMC. In contrast, Triton X-100 shows no difference. The results of 9 dynamic light scattering (DLS) and cryogenic TEM analysis show aggregate 10 formation at surfactant concentrations lower than CMC. DLS-based size of the 11 aggregates (d) decreases with increasing surfactant concentration. Zeta potential of 12 the SDBS aggregates decreases with increasing SDBS concentration, whereas it 13 increases for Triton X-100. The surface excess ( $\Gamma$ ) of SDBS calculated based on 14 hexadecane solubility and aggregate size data increases rapidly with increasing bulk 15 concentration, and then asymptotically approaches the maximum surface excess 16  $(\Gamma_{\text{max}})$ . Conversely, there is only a minor increase in  $\Gamma$  for Triton X-100. Comparison 17 of  $\Gamma$  and d indicates that excess of surfactant molecules at aggregate surface has 18 great impact on surface curvature. The results of this study demonstrate formation of 19 aggregates at surfactant concentrations below CMC for hexadecane solubilization, 20 and indicate the potential of employing low-concentration strategy for surfactant 21 application such as remediation of HOC contaminated sites.

- 22 Keywords: surfactant, SDBS, Triton X-100, critical micelle concentration,
- 23 solubilization, aggregation.

# 24 **1. Introduction**

25 Today surfactants have been a chemical that is ubiquitously used in industries 26 and households. One well-known function of surfactants is to solubilize hydrophobic organic compounds (HOCs), which has been widely made use of, 27 ranging from oily dirt removal from textiles for housekeeping to enhanced 28 remediation of soil or aquifer contaminated by HOCs.<sup>1-3</sup> Solubilization enhancement 29 of HOCs by surfactants has been the subject of many experimental and theoretical 30 studies, especially at concentrations above CMCs.<sup>4-10</sup> Critical micelle concentration 31 32 (CMC) is generally considered to be the concentration at which surfactant molecules aggregate to form micelles. Micelles are considered to be of spherical shape, and the 33 34 size, shape, aggregation number, and stability of micelles vary according to temperature, surfactant concentration, and solution chemistry.<sup>11</sup> It is typically 35 assumed that surfactants solubilize low-solubility compounds only at concentrations 36 higher than CMC, through partitioning into the hydrophobic core of micelles.<sup>9, 12, 13</sup> 37 38 The results of some studies have shown, however, that solubilization 39 enhancement may also occur at surfactant concentration below the CMC. Zhang and Miller<sup>6</sup> investigated solubilization of octadecane by rhamnolipid biosurfactant. 40 Solubilization of octadecane was enhanced by rhamnolipid at concentrations below 41 42 CMC, and the enhancement was much more significant than above CMC. Similar results were observed for hexadecane solubilization in the presence of a 43 monorhamnolipid in our prior study.<sup>14</sup> Kile and Chlou investigated solubilization of 44

45	DDT by surfactant Triton and Brij, and enhancement of apparent DDT solubility
46	was also observed below the nominal CMC. <sup>5</sup> To our knowledge, the mechanisms for
47	these sub-CMC solubilization behaviors, for example the potential for aggregate
48	formation below CMC, have not been systematically investigated in prior studies.
49	Moreover, concerns about the ecotoxicology of surfactants, e.g. alkylphenol
50	ethoxylates (APEs) <sup>15, 16</sup> , has caused the implementation of strict emission controls
51	for APEs in various industrial and consumer applications. <sup>17-20</sup> Thus, the ability for
52	surfactants to achieve solubilization enhancement of HOCs at sub-CMC
53	concentrations is of importance for cost and ecotoxicology considerations.
54	In this study, solubilization of <i>n</i> -hexadecane in the presence of SDBS or Triton
55	X-100 surfactant was investigated, with a special focus on such behavior at
56	surfactant concentrations below CMC. SDBS and Trion X-100 were selected to
57	represent anionic and nonionic surfactant, respectively. In addition to hexadecane
58	solubility, characterizations of the potential aggregation of the surfactants, such as
59	aggregate particle size and zeta potential measurements and cryo-TEM-based
60	aggregate observation, were implemented. Finally, based on surfactant interface
61	adsorption theory, spherical aggregate assumption and surfactant mass balance, the
62	aggregation formation and surfactant partitioning mechanism was raised to interpret
63	the sub-CMC hydrocarbon solubilization.

64

# 65 **2. Theoretical**

At a given temperature, adsorption of surfactant to the hexadecane/aqueous solution interface is related to interfacial tension and surfactant bulk activity as expressed by the Gibbs adsorption equation.<sup>21</sup> In this study, the adsorption of ionic and nonionic surfactant at the interface in the presence of swamping counterion (electrolyte solution) can be described by equation (1):

71 
$$\Gamma = -\frac{a}{RT} \left(\frac{d\gamma}{da}\right) \times 10^{-3}$$
(1)

where *a* is the surfactant bulk activity (mol/L); *R* is the universal gas constant (8.314 J/(mol K)), *T* (K) is the absolute temperature;  $\Gamma$  (mol/m<sup>2</sup>) is the interface excess of the surfactant;  $\gamma$  (mN/m) is the interfacial tension.

Surfactant adsorption at fluid-fluid interfaces is described by the Langmuir
 equation at concentrations below the critical micelle concentration (CMC)<sup>8, 22</sup>:

$$\Gamma = \Gamma_{\max} \frac{Ka}{1+Ka}$$
(2)

78 where  $\Gamma_{\text{max}}$  (mol/m<sup>2</sup>) is the maximum interface excess of surfactant and *K* (L/mol) 79 is the Langmuir constant.

Resolving equation (1) and combining it with equation (2) give the
Szyszkowski equation, which describes interfacial tension as a function of surfactant
bulk activity at concentrations below CMC:

83 
$$\gamma_0 - \gamma = RT\Gamma_{\max} \ln(1 + Ka) \times 10^3$$
(3)

84 where  $\gamma_0$  (mN/m) is the interfacial tension of the solution in the absence of surfactant. 85 The relation between *a* and the freely-dissolved surfactant monomer concentration, 86  $C_{\rm w}$  (mol/L), is:

$$a = fC_w \tag{4}$$

88 where *f* is the activity coefficient of surfactant. The concentration of surfactants in 89 bulk solution is relatively low (<0.01 mol/L) in this study, thus *f* is very close to 1 90 and  $a \approx C_w$ .<sup>22</sup>

Based on the classical model regarding the structure of alkane-surfactant aggregates formed in solution for alkane solubilization, the aggregates are assumed to be spherical with a layer of surfactant molecules on the surface. Thus, when solubilization reaches equilibrium, equation (5) and (6) can be obtained based on mass balance of surfactant:

$$\frac{\Gamma A_{\rm i} C_{\rm hex} M_{\rm hex}}{\rho_{\rm hex}} \times 10^{-3} + C_{\rm w} = C_0 \tag{5}$$

97 
$$A_{\rm i} = \frac{6}{d} \times 10^{-9}$$
 (6)

where  $A_i$  (m<sup>2</sup>/m<sup>3</sup>) is the hexadecane-water specific interfacial area;  $C_0$  (mol/L) is the 98 99 total concentration of surfactant initially added;  $C_{hex}$  (mol/L) is the concentration of 100 hexadecane solubilized in aqueous phase;  $M_{\text{hex}}$  (g/mol) is molecular weight of the hexadecane; and  $\rho_{\text{hex}}$  (g/cm<sup>3</sup>) is the density of the hexadecane at given temperature 101 102 T(K); d(nm) is the measured diameter of the aggregates. From equation (3), (4), (5) and (6), the surfactant excess,  $\Gamma$ , of surfactant on the aggregate surface and the  $C_{\rm w}$ 103 for a given  $C_0$  can be obtained. The area per surfactant molecule at the 104 hexadecane-aqueous interface (namely the aggregate surface), A ( $m^2$ ), is obtained by 105 106 equation (7):

$$A = \frac{1}{\Gamma N_{\rm A}} \tag{7}$$

**RSC Advances Accepted Manuscrip** 

108 where  $N_{\rm A}(6.022 \times 10^{23} \text{ mol}^{-1})$  is the Avogadro constant.

109

# 110 **3. Materials and methods**

# 111 **3.1 Materials**

112 SDBS (Sodium dodecylbenzenesulfonate, technical grade, purity > 97.0%), 113 Triton X-100 (polyoxyethylene (10) isooctylphenyl ether, laboratory grade, purity > 98.0%), and hexadecane (purity > 99.0%) were purchased from Sigma-Aldrich (St. 114 115 Louis, Mo., U.S.). Selected properties and molecular structures of SDBS and Triton 116 X-100 are presented in Table 1 and Fig. 1, respectively. *n*-Octane (purity > 95.0%) 117 and HPLC grade ethanol were purchased from Damao Chemical (Tianjin, China). All other chemicals were of analytical grade and used as received. Ultra-pure water 118 with an initial resistivity of 18.2 M $\Omega$ ·cm produced by UPT-II-40 (Ulupure, 119 Chengdu, China) was used throughout the experiment. Phosphate buffer solution 120 121 (PBS, 1.24 g/L KH<sub>2</sub>PO<sub>4</sub> and 1.35 g/L K<sub>2</sub>HPO<sub>4</sub> 3H<sub>2</sub>O, pH 6.8) was used as the 122 background electrolyte solution to provide a stable concentration of counterions, which is important for application of the Gibbs adsorption equation for surfactant 123 124 surface excess calculation.

125

126 **3.2 Interfacial tension measurement** 

127 In order to obtain the CMCs of the surfactants and  $\Gamma_{\text{max}}$  and *K* in equation (3), 128 interfacial tension between hexadecane and surfactant solution with designated

surfactant concentrations was measured at 30 °C with a tensiometer (JZ-200A, 129 Chengde, China) using the Du Noüy Ring method.<sup>23</sup> In brief, 15 mL of surfactant 130 131 PBS solution was prepared in a 50 mL glass beaker. 15 mL of hexadecane was then 132 carefully added to the top of the surfactant solutions without disturbing the bulk 133 volumes. Before the interfacial tension was measured, the beaker was kept at  $30 \, {\rm C}$ 134 for half an hour to allow partition of surfactant to water-hexadecane interface to reach equilibrium. The measurements were reproducible, with the difference of 135 136 duplicate measurements within  $\pm 0.2$  mN/m.

137

# 138 **3.3 Solubilization of hexadecane by surfactants**

Solutions of SDBS and Triton X-100 with hexadecane were prepared in 139 140 triplicates using the following procedures. 50 µL of hexadecane was pipetted to a 141 25-mL glass flask, and the flask was rotated to spread the hexadecane on the bottom 142 of the flask. 10 mL of PBS solution of SDBS or Triton X-100 was then added to the 143 flask and incubated on a reciprocal shaker at 30 °C, 120 rpm for 72 h to allow the 144 solubilization to reach equilibrium (result of a preliminary test showed that hexadecane solubility does not change after 72 h). Then the flasks were held 145 146 stationary for 2 h to allow establishment of stable phase distributions. 4 ml of the 147 aqueous solution was separated and collected using the method described by Zhong et al.<sup>14</sup>. 1 mL of the collected samples was removed for hexadecane concentration 148 149 measurement, and another 2 mL was used for measurement on size and zeta

150 potential of the aggregate particles. The hexadecane concentration was measured using gas chromatography (Agilent GC 6890N) following the procedures described 151 by Zhong et al.<sup>14</sup>. Samples with 8000 µM SDBS or with 1000 µM Triton X-100 152 153 were centrifugally filtered using 30KD ultrafiltration membrane (Millipore, Darmstadt, Germany) followed by hexadecane concentration measurement in the 154 155 filtrate to check the partition of hexadecane. A control containing 10 mL surfactant 156 solution and no hexadecane was used to quantify loss of surfactant due to adsorption 157 to inner wall of the flasks. To examine the stability of solubilized hexadecane, 4 mL 158 of the solubilized hexadecane solution obtained with 50 µM SDBS or 25 µM Triton 159 X-100 were sealed and allowed to stand still for 48 hours. Then 3 mL of the solution were again centrifugally separated using the method described by Zhong et al.<sup>14</sup> and 160 161 hexadecane concentration was measured.

162 The size and zeta potential of aggregate particles were measured using a 163 ZEN3600 Zetasizer Nano (Malvern Instruments, U.K.). The particle size was 164 determined through dynamic light scattering (DLS) at 633 nm with He-Ne laser, 165 which worked on 4.0 mV power. 1 mL of sample was loaded to the DTS-0012 cell and kept at 30 °C. The scattered light was collected by receptor at angle of 173 ° from 166 light path. The size of the aggregates was expressed in terms of hydrodynamic 167 168 diameter, which was calculated by using the software associated with the instrument. 169 To obtain the zeta potential of the aggregates, approximately 1 mL of sample was 170 loaded to the DTS1060 folded capillary cell and the electrophoretic mobility of the 171 aggregate particles was measured at 30 °C under automatic voltage using laser Doppler velocimetry with M3-PALS technique to avoid electrossmosis. The 172 measured data was converted into corresponding zeta potential applying the 173 Helmholtz-Smoluchowski equation.<sup>24</sup> 174 175 3.4 Cryo-Transmission Electron Microscopy (cryo-TEM) observation of 176 177 aggregates A 4 µL drop of sample was placed on the copper grid, and then sent to a FEI 178 179 Vitrobot sample plunger. The excess sample was removed with filter paper. The grid was then immediately plunged into a bath of liquid ethane and transferred to a bath 180 of liquid nitrogen. The samples were stored in a GATAN model cryo-transfer unit in 181 182 liquid nitrogen. The morphology of surfactant-hexadecane aggregates was viewed 183 with a Tecnai F20 cryo-transmission electron microscope (FEI, Hillsboro, Oregon)

185

184

# 186 **4. Results and discussion**

## 187 **4.1** $\Gamma_{max}$ and *K*

at 120 kV.

The dependence of interfacial tension on the surfactant concentration is presented in Fig. 2a. The interfacial tension of hexadecane/PBS solution in the absence of surfactants is 41.3 mN/m. For SDBS, hexadecane/PBS interfacial tension decreases rapidly from 41.2 to 2.3 mN/m with increase of the SDBS concentration

to approximately 600  $\mu$ M. Further increase in SDBS concentration has minimal effect on the interfacial tension. For Triton X-100, the interfacial tension decreases from 41.3 to 4.2 mN/m with increase in the Triton X-100 concentration to approximately 500  $\mu$ M. Further increase in Triton X-100 concentration slowly

reduces the interfacial tension from 4.2 to 1.4 mN/m.

197 CMCs of the surfactants were obtained using the method described by Zhong et 198 al.<sup>25</sup>. The CMC of SDBS is 612  $\mu$ M, which is lower than in pure water (e.g. 2764 199  $\mu$ M reported by Yang et al.<sup>26</sup>) due to the presence of counterions (i.e., K<sup>+</sup>) in PBS in 200 this study. The CMC of Triton X-100 is 672  $\mu$ M, which is in the range of 200-900 201  $\mu$ M reported by Sigma-Aldrich.<sup>27</sup> The significantly different CMCs for PBS versus 202 water obtained for SDBS compared to the similar values obtained for Triton is 203 consistent with the anionic and nonionic natures of the two, respectively.

The interfacial tension data at surfactant concentrations below CMC were well fitted by the logarithmic function described by Equation (3) (Fig. 2b), and the maximum interface excess of surfactant ( $\Gamma_{max}$ ) and the Langmuir constant (*K*) were thus obtained. Minimal surfactant molecule area at interface ( $A_m$ ) was calculated using equation (7). The results are summarized in Table 1.

209

210 **4.2 Solubilization of hexadecane by surfactants** 

As shown in Table S1, concentration of hexadecane solubilized by 50 μM
SDBS or 25 μM Triton X-100 after standing for 48 hours is essentially identical to

**RSC Advances Accepted Manuscript** 

#### **RSC Advances**

213	the initial concentration. 50 $\mu M$ and 25 $\mu M$ are lower end concentrations,
214	respectively, for SDBS and Triton X-100 used in this study. The results demonstrate
215	good stability of the solubilized hexadecane. Results of hexadecane solubilization by
216	SDBS and Triton X-100 are presented in Fig. 3. Both surfactants increase the
217	solubility of hexadecane at surfactant concentrations lower than CMC. The apparent
218	solubility of hexadecane increased linearly with surfactant concentration for both
219	surfactants, with different slopes below and above CMC. Solubilization capacity of a
220	surfactant for an HOC is characterized by the molar solubilization ratio (MSR),
221	which is defined as increase of solubilized hydrophobic compound concentration
222	(mol/L) per unit increase of surfactant concentration (mol/L) in the solution. <sup>12, 28</sup> As
223	shown from Fig. 3a, the MSR for SDBS is significantly higher below CMC than
224	above CMC (i.e. 0.84 and 0.16, respectively). Similar results were observed for an
225	ionic rhamnolipid biosurfactant in the solubilization of hexadecane <sup>14</sup> and
226	octadecane <sup>6</sup> . In contrast, MSRs for Triton X-100 are not significantly different
227	below and above CMC (1.9 and 1.5, Fig. 3b), indicating the influence of surfactant
228	molecule structure on solubilization behavior.

- 229
- 230 4.3 Size and zeta potential of aggregates

231 Formation of aggregates at surfactant concentrations both below and above CMC is demonstrated by the results of aggregate size measurement using DLS 232 233 method (Fig.4) and by direct view of the aggregates with cryo-TEM for Triton

234 X-100 at concentrations of 25 and 1500 µM (Fig. S1, Supplementary Information). 235 Also, the spherical aggregate assumption was confirmed by the sphere morphology of the aggregates. Although three groups of particles with different size range (three 236 237 peaks in the intensity and volume of particles distributions (%) plots, Fig. S2) were 238 detected by DLS particle size measurement, almost 100% of the particles in 239 numbers are in the group of the smallest size (Figs. S2 and S3). This is consistent 240 with the results of the cryo-TEM measurements, in which only one group of particles with similar size was observed (Fig. S1). For both surfactants, the particle 241 242 size decreases rapidly with increase of  $C_0$  to approximately 200  $\mu$ M, and then 243 stabilizes as  $C_0$  continues to increase to above CMC (Fig.4).

As shown in Fig. 5, for anionic surfactant SDBS, the zeta potential of 244 245 aggregates decreases approximately from -20 mV to -35 mV with increase of  $C_0$ from 25  $\mu$ M to 200  $\mu$ M, and stabilizes at ~ -35 mV with further increasing C<sub>0</sub> to 800 246  $\mu$ M. Similar trend was observed by Ivanov et al.<sup>29</sup> for zeta potential of hexadecane 247 248 emulsion drops versus concentration of ionic surfactant SDS at significantly low SDS concentrations. When  $C_0$  is even further increased to 1200  $\mu$ M, a secondary 249 decrease of zeta potential to ~-70 mV is observed. In contrast, the zeta potential of 250 251 hexadecane-Triton X-100 aggregates increased from -20 mV to -5 mV with increasing  $C_0$  from 50 µM to 1000 µM and stabilized at ~-5 mV when  $C_0$  was above 252 253 1000 µM. Zeta potential is the potential difference between the bulk solution of the 254 dispersion medium and the slippery layer of fluid attached to the dispersed

255	particle. <sup>24, 30</sup> Due to the anionic hydrophilic heads of SDBS, the aggregates have
256	negatively charged surface. <sup>31</sup> The negatively charged surface of aggregates for
257	non-ionic Triton X-100 probably results from association of anions in PBS (i.e. OH <sup>-</sup> ,
258	$HPO_4^{2-}$ , $H_2PO_4^{-}$ , $PO_4^{3-}$ ) with the polyoxyethylene chain of Triton on the aggregate
259	surface.

260

# 261 **4.4 Partitioning of surfactants and its relation with aggregation**

262 In the experiments no emulsion of hexadecane in the presence of surfactants 263 was observed. Adsorption of the surfactants to the inner wall of the flask was also minimal (data not shown). Because very limited volume of hexadecane (50 µL) was 264 used, partition of surfactants to the hexadecane phase, or to the interface between the 265 floating mass of hexadecane and the aqueous phase (less than  $1 \text{ cm}^2$  in contrast to 266 the magnitude of  $10^2 \sim 10^4$  cm<sup>2</sup> for the total surface area of the aggregates according 267 268 to calculation below), was minimal. Therefore, the surfactants reside either in bulk aqueous solution or in the aggregate. The hexadecane concentration in the filtrate 269 270 after ultrafiltration was under the detection limit (data not shown), showing that the amount of freely-dissolved hexadecane in bulk aqueous phase is minimal and all the 271 272 solubilized hexadecane is associated with aggregate. This is consistent with the fact 273 that hexadecane has extremely low water solubility (0.09  $\mu$ g/L, 25 °C) and high octanol-water partition coefficient (10<sup>8.3</sup>, 25 °C) of hexadecane.<sup>32</sup> Hence, based on 274 275 the spherical aggregate assumption, the aggregate surface excess  $\Gamma$  and the bulk

276 concentration  $C_w$  of surfactants were calculated by applying equation (2) and (5) 277 using  $\Gamma_{\text{max}}$  and *K* previously obtained.

For both SDBS and Triton X-100, a linear relationship between the apparent 278 279 solubility of hexadecane,  $C_{\text{hex}}$ , and the freely-dissolved surfactant monomer 280 concentration,  $C_w$ , is observed with increase of  $C_w$  to CMC (Fig. 6a). This is similar 281 to the relationship between  $C_{\text{hex}}$  and the total surfactant concentration,  $C_0$  (Fig. 3). By comparing the slopes of  $C_{\text{hex}}$ - $C_0$  profile at  $C_0$  below CMC and  $C_{\text{hex}}$ - $C_w$  profile 282 (0.84 versus 1.0 for SDBS, and 1.9 versus 2.5 for Triton X-100), the relative 283 284 distribution of the surfactant between the freely-dissolved and aggregate-associated is calculated. The percentage of the aggregate-associated surfactant is approximately 285 286 16% and 23% of the total for SDBS and Triton X-100, respectively.

287 Changes of surfactant surface excess ( $\Gamma$ ) and molecule area (A) versus  $C_{\rm w}$  are 288 presented in Fig. 6b. For SDBS, a rapid increase of  $\Gamma$  and decrease of A are observed when  $C_w$  increases from ~25  $\mu$ M to ~150  $\mu$ M. Further increase of  $C_w$  causes 289 asymptotic approach of  $\Gamma$  and A to  $\Gamma_{max}$  and  $A_m$ , respectively. Conversely, there is 290 only a minor increase in  $\Gamma$  for Triton X-100. Only very slight increase of  $\Gamma$  and 291 decrease of of A are observed when  $C_w$  was below ~80  $\mu$ M.  $\Gamma$  and A are more 292 293 sensitive to change of  $C_w$  with a smaller K according to equation (2) and (7). The K value for Triton X-100 is much larger than for SDBS  $(4.33 \times 10^3 \text{ and } 0.2 \times 10^3 \text{ m}^3/\text{mol})$ , 294 295 respectively (Table 1)). Thus, a more significant change of  $\Gamma$  and A over a broader range of  $C_{\rm w}$  occurred for SDBS. 296

297	As shown in Fig. 7, for both surfactants, aggregate size, $d$ , decreases with the
298	increase of surfactant surface excess on the aggregates, $\Gamma$ , in a way that d approaches
299	the stabilized minimum aggregate size $(d_{\min})$ as $\Gamma$ approaches $\Gamma_{\max}$ . This result
300	indicates that the curvature of the aggregate surface increases with increasing
301	surface density of surfactant molecules. For SDBS, which has charged hydrophilic
302	head, as SDBS molecules approach each other ( $\Gamma$ increases and A decreases) on the
303	aggregate surface, the electrostatic repulsion between charged heads of SDBS
304	becomes stronger. Such enhancement in electrostatic repulsion induces unequal rate
305	of approach for polar and hydrophobic moieties between molecules, and therefore
306	increase in aggregate surface curvature (Fig. 8). Thus, the aggregate size, $d$ ,
307	decreases with increasing $\Gamma$ . Similarly, as the polar head of Triton X-100 molecule,
308	the polyoxyethylene chain, usually twists and curls, causing large actual molecule
309	radius <sup>33</sup> , the spatial steric repulsion between Triton X-100 polar heads may act in a
310	way similar to electrostatic repulsion between charged heads in SDBS molecules,
311	thus also causing an increase in surface curvature of aggregates (Fig. 8).

312 Zeta potential is a function of particle size and surface charge density.<sup>24, 34, 35</sup> 313 Because SDBS is an anionic surfactant with a polar head that fully dissociates in 314 solution, surface charge density is determined by surface molecule density, or  $\Gamma$ . 315 Also, as discussed above, particle size is also a function of  $\Gamma$ . For SDBS, therefore, 316 zeta potential is essentially a dependent of  $\Gamma$  and its change also exhibits an 317 asymptotic pattern at concentrations lower than CMC. For Triton X-100, binding of

anions, i.e.  $H_2PO_4^{-}$ ,  $HPO_4^{2-}$  and  $OH^{-}$ , to the polyoxyethylene group through hydrogen bond may be responsible for the negative zeta potential of the aggregates. As  $\Gamma$  increases, the Triton X-100 molecules become more compacted on the aggregate surface, leaving less space for the anions to partition. Consequently zeta potential increases.

323 For the standard surfactant solubilization conceptualization, enhancement of HOC solubility requires surfactant concentrations higher than CMC.<sup>28, 36-38</sup> In 324 325 contrast, results in this study show that significant hexadecane solubility 326 enhancement takes place at surfactant concentrations lower than CMC and such enhancement is related to formation of aggregates. In fact, the CMC measurement 327 using the general methods, e.g. the interfacial tension and conductometric methods, 328 329 is based on a pure-surfactant micelle formation mechanism. We speculate that the presence of hexadecane has some influence on surfactant monomers activity through 330 331 the hydrophobic interaction between surfactant and hexadecane molecules, which may be more significant than between surfactant molecules themselves. Thus, the 332 333 interaction between surfactant and hexadecane molecules may favor formation of aggregates in priority to formation of pure-surfactant micelles, leading to 334 335 hexadecane solubilization enhancement below CMC.

When surfactant concentration in the aqueous phase is higher than CMC, the surfactant molecules form micelles. Co-existence of hexadecane-SDBS aggregates and SDBS micelles is observed with Cryo-TEM at high magnification (Fig. S4). The

339	decreases in MSR and aggregate zeta potential for SDBS as $C_w$ goes above CMC are
340	probably a result of micelle formation. At surfactant concentrations higher than
341	CMC, a new partitioning equilibrium of surfactant between the bulk solution,
342	hexadecane/water interface, and micelles is established. In this case, $C_w$ remains at
343	CMC and is insensitive to the change of $C_0$ , and so are $\Gamma$ and $d$ . Hence, the regime of
344	HOCs solubilization by surfactants at concentrations above CMC differs from that
345	below CMC.

346

# 347 **5. Conclusion**

In contrast to the conceptualized micelle-based mechanism for solubilization of 348 349 HOCs starting at surfactant concentration higher than CMC, the results of this study demonstrated that SDBS and Triton X-100 at sub-CMC concentrations can enhance 350 351 hexadecane solubilization employing an aggregate formation mechanism. 352 Observation of sub-CMC aggregates by both DLS and cryo-TEM methods suggests 353 that HOC-surfactant interaction contributes to sub-CMC aggregate formation, which 354 is in contrast to pure-surfactant micelles formation above CMC. This is for the first time the sub-CMC solubilization of HOCs by surfactants is comprehensively 355 356 explored. The study is of importance for better understanding the solubilization behavior of HOCs by surfactants and for economical application of surfactants. 357 358 Future studies should aim at testing such sub-CMC solubilization behavior for a 359 variety of surfactants and HOCs.

360

# 361 Acknowledgments

362	The authors thank the Center for Integrative Imaging (CII) at University of
363	Science and Technology of China for cryo-TEM analysis. This study was funded by
364	the National Student Innovation Training Program (SIT) of China (521611246), the
365	National Natural Science Foundation of China (51378192, 51378190, 51308200 and
366	51108166), the Program for Changjiang Scholars and Innovative Research Team in
367	University (IRT-13R17). Additional support was provided by the NIEHS Superfund
368	Research Program (ES04940).

369

# 370 **References**

- 1 L. M. Abriola, C. D. Drummond, E. J. Hahn, K. F. Hayes, T. C. G. Kibbey, L. D.
- 372 Lemke, K. D. Pennell, E. A. Petrovskis, C. A. Ramsburg and K. M. Rathfelder,
- 373 Environ. Sci. Technol., 2005, **39**, 1778-1790.
- 2 J. Childs, E. Acosta, M. D. Annable, M. C. Brooks, C. G. Enfield, J. H. Harwell,
- 375 M. Hasegawa, R. C. Knox, P. S. Rao, D. A. Sabatini, B. Shiau, E. Szekeres and
- 376 A. L. Wood, J. Contam. Hydrol., 2006, 82, 1-22.
- 377 3 R. Masrat, M. Maswal and A. A. Dar, J. Hazard. Mater., 2013, 244, 662-670.
- 4 K. D. Pennell, L. M. Abriola and W. J. Weber Jr, Environ. Sci. Technol., 1993, 27,
- 379 2332-2340.
- 380 5 D. E. Kile and C. T. Chiou, *Environ. Sci. Technol.*, 1989, 23, 832-838.

381	6	Y. Zhang and R. M. Miller, Appl. Environ. Microb., 1992, 58, 3276-3282.
382	7	J. E. McCray, G. Bai, R. M. Maier and M. L. Brusseau, J. Contam. Hydrol.,
383		2001, <b>48</b> , 45-68.
384	8	S. Peng and M. L. Brusseau, Water Resour. Res., 2005, 41, 6874-6880.
385	9	J. S. Clifford, M. A. Ioannidis and R. L. Legge, J. Colloid Interface Sci., 2007,
386		<b>305</b> , 361-365.
387	10	J. D. Albino and I. M. Nambi, J. Environ. Sci. Heal. A, 2009, 44, 1565-1573.
388	11	A. Patist, J. R. Kanicky, P. K. Shukla and D. O. Shah, J. Colloid Interface Sci.,
389		2002, <b>245</b> , 1-15.
390	12	M. A. Mir, O. A. Chat, M. H. Najar, M. Younis, A. A. Dar and G. M. Rather, J.
391		Colloid Interface Sci., 2011, 364, 163-169.
392	13	A. R. Tehrani-Bagha and K. Holmberg, Materials, 2013, 6, 580-608.
393	14	H. Zhong, Y. Liu, Z. F. Liu, Y. B. Jiang, F. Tan, G. M. Zeng, X. Z. Yuan, M. Yan,
394		Q. Y. Niu and Y. S. Liang, Int. Biodeter. Biodegr., 2014, 94, 152-159.
395	15	U. Zoller, Environ. Int., 2006, <b>32</b> , 269-272.
396	16	S. S. Talmage, Environmental and human safety of major surfactants: alcohol
397		ethoxylates and alkylphenol ethoxylates, CRC Press, 1994.
398	17	S. Rebello, A. K. Asok, S. Mundayoor and M. Jisha, Environmental chemistry
399		<i>letters</i> , 2014, <b>12</b> , 275-287.
400	18	K. Hill and C. LeHen-Ferrenbach, in Sugar-based surfactants fundamentals and
401		Applications, ed. C. C. Ruiz, CRC Press, Boca Raton, 2008.

- 402 19 R. Höfer and K. Hinrichs, in Polymers-Opportunities and Risks II: Sustainability,
- 403 *Product Design and Processing*, Springer, Berlin, Heidelberg, 2010, pp. 97-145.
- 404 20 K. Hill and R. Höfer, in Sustainable Solutions for Modern Economies, ed. R.
- 405 Höfer, RSC Publishing, Cambridge, 2009, pp. 167-237.
- 406 21 L. Chen and T. C. Kibbey, *Langmuir*, 2006, **22**, 6874-6880.
- 407 22 M. J. Rosen, *Surfactants and Interfacial Phenomena*, John Wiley & Sons,
  408 Hoboken, 3rd edn., 2004.
- 409 23 X. Z. Yuan, F. Y. Ren, G. M. Zeng, H. Zhong, H. Y. Fu, J. Liu and X. M. Xu,
- 410 *Appl. Microbiol. Biot.*, 2007, **76**, 1189-1198.
- 411 24 R. J. Zasoski, in Encyclopedia of Soil Science, ed. W. Chesworth, Springer
- 412 Netherlands, Dordrecht, 2008, pp. 841-845.
- 413 25 H. Zhong, G. M. Zeng, J. X. Liu, X. M. Xu, X. Z. Yuan, H. Y. Fu, G. H. Huang,
- 414 Z. F. Liu and Y. Ding, *Appl. Microbiol. Biot.*, 2008, **79**, 671-677.
- 415 26 K. Yang, L. Zhu and B. Xing, *Environ. Sci. Technol.*, 2006, **40**, 4274-4280.
- 416 27 Sigma-Aldrich, Selected properties of Triton X-100, http://www.sigmaaldric
- 417 <u>h.com/catalog/product/sial/x100?lang=zh&region=CN</u> [In Chinese], (accessed
- 418 April 8, 2015).
- 419 28 D. A. Edwards, R. G. Luthy and Z. Liu, Environ. Sci. Technol., 1991, 25,
- 420 127-133.
- 421 29 I. B. Ivanov, K. G. Marinova, K. D. Danov, D. Dimitrova, K. P.
  422 Ananthapadmanabhan and A. Lips, *Adv. Colloid Interface Sci.*, 2007, 134,

423		105-124.	<b>S</b>
424	30	D. Q. Lin, L. N. Zhong and S. J. Yao, <i>Biotechnol. Bioeng.</i> , 2006, <b>95</b> , 185-191.	
425	31	W. Liu, J. Kumar, S. Tripathy and L. A. Samuelson, Langmuir, 2002, 18,	Ö
426		9696-9704.	S
427	32	NCBI, PubChem Compound Database; CID=11006, selected properties of	
428		n-Hexadecane, http://pubchem.ncbi.nlm.nih.gov/compound/11006, (accessed	
429		May 8, 2015).	2
430	33	J. Penfold, I. Tucker, R. Thomas, E. Staples and R. Schuermann, J. Phys. Chem.	Ő
431		<i>B</i> , 2005, <b>109</b> , 10760-10770.	ote
432	34	D. A. Dzombak and F. M. M. Morel, Surface Complex Modeling, Hydrous Ferric	<b>D</b>
433		Oxide, John Wiley & Sons, New York, 1990.	Ö
434	35	R. J. Hunter, Zeta Potential in Colloid Science. Principles and Applications,	
435		Academic Press, New York, 1981.	
436	36	G. Bai, M. L. Brusseau and R. M. Miller, J. Contam. Hydrol., 1998, 30,	ð
437		265-279.	S
438	37	C. L. Chun, JJ. Lee and JW. Park, Environ. Pollut., 2002, 118, 307-313.	a
439	38	S. Paria, Adv. Colloid Interface Sci., 2008, 138, 24-58.	
440			
			Ŕ

Table 1 Selected properties and the water-hexadecane interface coefficients of the

surfactants used in this study

Surfactant	Formula	Surfactant type	Molecular weight (g/mol)	<i>CMC</i> <sup>a</sup> (µM)	$\Gamma_{max}^{\ \ b}$ (mol/m <sup>2</sup> )	$A_m^c$ (nm <sup>2</sup> )	K <sup>d</sup> (m <sup>3</sup> /mol)
SDBS	$C_{12}H_{25}C_6H_4SO_3Na$	Anionic	348.48	612	3.3×10 <sup>-6</sup>	0.50	$0.2 \times 10^3$
Triton X-100	$C_8H_{17}C_6H_4O(CH_2CH_2O)_{10}H$	Non-ionic	648.86	672	1.9×10 <sup>-6</sup>	0.87	$4.3 \times 10^3$
<sup><i>a</i></sup> Critical micelle concentration (CMC) measured in PBS solution at 30 $^{\circ}$ C							

<sup>b</sup> Maximum interface excess of surfactant

 $^{c}$  Area per surfactant molecule at  $\Gamma_{\rm max.}$ 

<sup>d</sup> Langmuir equation constant

Figure 1 The molecular structure of SDBS and Triton X-100.

**Figure 2** (a) The hexadecane/PBS interfacial tension as a function of surfactant concentration. (b) Interfacial tension-concentration relation regression at surfactant concentrations below CMCs using Szyszkowski equation (Equation (3) in text).

**Figure 3** Apparent hexadecane solubility ( $C_{hex}$ ) versus total surfactant concentration ( $C_0$ ) of (a) SDBS and (b) Triton X-100. Two sets of regression represent data for below and above the CMCs.

**Figure 4** Aggregate size (*d*) versus the total surfactant concentration ( $C_0$ ) for hexadecane solubilization. (Insert) Zoom-in for  $C_0$  lower than CMC.

Figure 5 Zeta potential of aggregates versus the total surfactant concentration ( $C_0$ ) for the hexadecane solubilization.

**Figure 6** (a) Apparent solubility of hexadecane  $(C_{hex})$  versus the bulk surfactant concentration  $(C_w)$  at  $C_w$  below CMCs; (b) surface excess  $(\Gamma)$  and molecule area (A)of surfactants on the aggregates surface versus surfactant bulk concentration  $(C_w)$ . The dash lines and dash dot lines represent the maximum surface excess  $(\Gamma_{max})$  and the minimum area per surfactant molecular on the surface  $(A_m)$ , respectively.

**RSC Advances Accepted Manuscript** 

**Figure 7** Aggregates diameter (*d*) and surface excess of surfactants ( $\Gamma$ ) versus the bulk surfactant concentration ( $C_w$ ) blow CMCs.

**Figure 8** Schematic diagram of aggregate formation at surfactant concentration below CMCs and the change of curvature of aggregates surface with increasing surfactant bulk concentration for the hexadecane solubilization by surfactant.



Triton X-100

Figure 1



Figure 2



Figure 3



Figure 4



Figure 5



Figure 6

**RSC Advances Accepted Manus** 



Figure 7



Figure 8