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1	Synthesis of Ni(II) ion imprinted polymer based on macro-mesoporous silica
2	with enhanced dynamic adsorption capacity: Optimization by response surface
3	methodology
4	Yan Liu ^{a,*} , Fangfang Liu ^a , Minjia Meng ^a , Zhanchao Liu ^b , Liang Ni ^{a,*} , Guoxing
5	Zhong ^c
6	^a School of Chemistry and Chemical Engineering, Jiangsu University, Zhenjiang
7	212013, China
8	^b School of Materials Science and Engineering, Jiangsu University of Science and
9	Technology, Zhenjiang 212003, China
10	^c School of Environmental and Chemical Engineering, Jiangsu University of Science
11	and Technology, Zhenjiang 212003, China
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29	* Corresponding author. Tel.: +8615751011770.
30	E-mail address: ly19821212@163.com

32 Abstract

In this study, Ni(II) ion imprinted polymer (Ni(II)-IIP) based on macroporous-33 34 mesoporous silica (MMS) was optimally synthesized using a response surface methodology (RSM) approach for enhanced dynamic adsorption capacity. MMS was 35 36 prepared via dual-templating routes employing liquid crystalline surfactants and polystyrene beads to improve mass transfer and reduce transport limitations. With 37 dynamic adsorption capacity for Ni(II) as the response, the effects of four variables, 38 39 i.e. amount of S,S'-bis(α,α' -dimethyl- α'' -acetic acid)trithiocarbonate (BDAAT), 40 consumption of acrylamide (AM), reaction time and dosage of 41 2,2'-azobisisobutyronitrile (AIBN), were investigated to solve complex synthesis process. The predicted appropriate preparation conditions were BDAAT dose 0.07 g, 42 43 AM dose 0.029 g, reaction time 6.3 h, and AIBN dose 4.54 mg, under which Ni(II)-IIP was prepared and used as adsorbent to remove Ni(II), obtaining the 44 45 maximum dynamic adsorption capacity (12.96 mg/g). The significance of independent variables and their interactions was studied to explain the specific 46 47 adsorption question. In addition, the resulting Ni(II)-IIP performed without obvious deterioration after five repeated cycles. 48

Keywords: response surface methodology, macro-mesoporous silica, ion imprinted,
synthesis optimization, Ni(II).

52 **1. Introductionc**

53 Mesoporous silica materials have been investigated by many researchers from both fundamental and practical viewpoints [1-2]. Unique characteristics based on their 54 pore structure, pore size uniformity, unusual surface topology and large surface area 55 56 have opened up a new possibility in the research fields of adsorbents [3-4]. Numerous 57 efforts have been attempted to improve the adsorption properties of mesoporous silica from morphology and composition control. By using different strategies, researchers 58 59 synthesize various kinds of mesoporous silica materials with controllable 60 morphologies, framework compositions, pore structures and pore sizes [5-7]. But it is 61 worth noting that they usually exhibit considerable resistance of diffusion especially in the case of long transportation distance due to pore size limitation [8]. 62

Through the templating approach based on polymer latexes as templates, 63 macroporous materials with pore size ranging from tens of nanometers to several 64 micrometers can be readily synthesized [9-12]. Because of their large interconnected 65 pores, these macroporous materials can provide excellent performance of mass 66 67 transport and offer easier accessibility for targets, but their surface area is relatively 68 lower which is disadvantageous for efficient adsorption [13-15]. The incorporation of macropores in mesoporous materials can combine the benefits of mesoporous and 69 macroporous structures. In these materials, the macropores act as channels and 70 71 facilitate the transport of targets that have to be adsorbed in the mesopores [16-18]. The addition of macropores can improve the efficiency of mesoporous materials as 72 they enhance mass transport and reduce diffusion limitations. Although the 73 74 macroporous-mesoporous materials mentioned above are effective to adsorption, the 75 selectivity of the metal ion from the complex system is not good enough. In order to 76 solve the problem, a method aimed to improve the selectivity of the ion is necessary.

Ion-imprinted polymers (IIPs) derived from molecular imprinted polymers (MIPs) are synthetic recognition materials that display predetermined selectivity towards a chosen template ion [19-20]. Furthermore, surface ion-imprinted polymers (SIIPs) were employed to overcome the drawbacks of IIPs prepared by conventional technique [21]. The main fields of imprinting include separation processes 82 (chromatography, solid-phase extraction, and membrane separations), artificial 83 antibodies, and sensors recognition elements [22-24]. However, the challenge of designing and synthesizing IIPs can be a daunting prospect to the uninitiated 84 practitioner. During free radical polymerization, there is a complex formation between 85 86 template and functional monomer, and the matrix is surrounded by complex and 87 cross-linking monomer, yielding a three-dimensional polymer network where template ions are trapped after completion of polymerization [25-26]. The nature of 88 89 the resulting material and its binding properties are influenced not only by the 90 composition of prepolymerization mixture but also by the experimental conditions 91 employed, such as the variety and dosage of radical initiator used, polymerization 92 temperature, the type and amount of solvent, and so forth. In addition, lots of researches have employed reversible addition-fragmentation chain transfer (RAFT) 93 reagents to synthesize polymers with well-defined structures [27]. That would make it 94 95 more difficult to synthesize an excellent SIIPs. Based on the above considerations, the optimization of appropriate polymerization conditions are crucial for the improvement 96 97 of SIIPs performance.

Response surface methodology (RSM) is a collection of statistical and 98 mathematical techniques useful for developing, improving, and optimizing processes 99 100 in which a response of interest is influenced by several variables and the objective is 101 to optimize this response. It defines the effect of the independent variables, alone or in 102 combination, on the processes [28-30]. Nowadays, it is clearly seen that RSM has 103 been widely applicable in a wide variety of chemical processes, such as the 104 production of microporous palm shell based activated carbon [31], nano-crystalline 105 TiO₂ thin films coated on hollow glass microspheres (HGMs) [32], hydrogel [33], and 106 so on. A critical appraisal of these reported references show how various process 107 variables through RSM could improve the properties of the product. Central 108 composite design (CCD), one type of RSM, is the most commonly used second-order 109 design [34]. It is more efficient and easier to arrange and interpret the optimization 110 experiments compared with other methods.

111

In this study, we first synthesized macroporous-mesoporous silica (MMS) via a

112 dual-template approach. Then, conduct process optimization using the RSM approach 113 was carried out for the development of Ni(II) ion imprinted polymer (Ni(II)-IIP) 114 based on MMS with enhanced adsorption capacity. There is very little information in 115 the literature using macro-mesoporous silica as the substrate material to synthesize 116 IIPs, and novelty in the present study lies in the use of RSM approach for synthesis 117 process optimization. Different preparation variables on the characteristics of 118 Ni(II)-IIP were studied to find the optimum conditions. In addition, dynamic 119 selectivity and regeneration were also discussed.

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121 **2. Experimental**

122 2.1. Materials

123 Pluronic P123, triblock poly-(ethylene oxide)-poly (propylene oxide)-poly (ethylene oxide), (EO₂₀PO₇₀EO₂₀, molecular weight 5800) was purchased from Sigma 124 (USA). Styrene (St), 3-(methacryloxyl) propyltrimethoxysilane (MPS), Ethylene 125 126 glycol dimethacrylate (EGDMA), Acrylamide (AM) and 2,2'-azobisisobutyronitrile 127 (AIBN) were purchased from the Aladdin Reagent Co., Ltd. (Shanghai, China). Polyvinylpyrrolidone (PVP), tetraethyl orthosilicate (TEOS), and $Ni(NO_3)_2$ were 128 129 obtained from Sinopharm Chemical Reagents Co. Ltd. (Shanghai, China). The chain 130 transfer agent of S,S'-bis(α,α' -dimethyl- α'' -acetic acid)trithiocarbonate (BDAAT) was synthesized according to the reported literatures [35]. 131

132 2.2. Preparation of Ni(II)-IIP

The dispersion polymerization approach of Sen and coworkers was adopted to 133 134 generate monodisperse polystyrene (PS) beads [36]. For a typical preparation, 2 g of styrene, 1.6 g of PVP, 0.5 g of MPS and 0.04 g of AIBN were dissolved in a mixture 135 of ethanol (28 mL) and H₂O (2 mL). The obtained solution was then added into a 100 136 137 mL three-neck round bottom flask equipped with a mechanical stirrer, a refluxing 138 condenser, and a nitrogen inlet. After sealing in a nitrogen atmosphere, the reactor was submerged in a water bath and polymerization was carried out with a stirring 139 140 speed of 300 rpm at 70 °C for 24 h. The resulting polymer microspheres were 141 repeatedly washed with an ethanolwater mixture (1:1, v:v) by centrifugation.

142 Macroporous–mesoporous silicas were synthesized following the approach of 143 Zhao et al. [37], with the addition of polystyrene beads during the synthesis to create 144 macropores. Typically, 2.0 g of P123 was dissolved in 15 mL of water and 50 mL of 2 M HCl solution while stirring at 35 °C. 1.0 g of polystyrene beads were then added to 145 the solution and stirred for an hour. 4.6 mL of TEOS were added to the solution, 146 which was maintained at 35 °C for 24 h while stirring. The mixture was then aged at 147 80 °C for 24 h and the solid product filtered, washed 3 times with deionised water, 148 149 and calcined statically in air at 550 °C (ramp rate of 1 °C/min) for 6 h. The final solids 150 abbreviated as MMS. A pure mesoporous SBA-15 silica for comparison was also

151 synthesised for comparison in the absence of polystyrene.

0.3 g of MMS was dispersed in 40 mL of ethanol and the mixture was sonicated
for 10 min. Then 2 mL of MPS was added. The reaction was kept at 40 °C for 12 h.
The product was separated by centrifuge and washed with ethanol. Finally, the
resulting material (MMS@MPS) was dried under vacuum at 50 °C overnight. Using
the same method, SBA-15@MPS was prepared by modified SBA-15.

157 Typically, 0.1 mmol (29.1 mg) of Ni(NO₃)₂, an appropriate amount of AM, 1 158 mmol (0.19 mL) of EGDMA, a know amount of BDAAT, and 50 mg of MMS@MPS 159 were dispersed into a 15.0 mL methanol/distilled water solutions (1:1, v:v). After 160 sealing, shaking, and purging the mixture with nitrogen, a 5.0 mL methanol/distilled 161 water solutions (1:1, v:v) with an appropriate amount of AIBN was added into the suspension. The resultant mixture was stirred at 65 °C for a know time under nitrogen 162 163 protection. The products extensively washed with methanol/distilled water (1:1, v:v) 164 for several times. Then, the solid was treated with 2 mol/L HCl until no Ni(II) ion was 165 detected in the wash solutions. At last, the polymer was centrifuged with distilled 166 water to neutralization, dried at 50 °C under vacuum. Nonimprinted control polymers 167 (NIP) were synthesized under identical conditions in the absence of Ni(II) ion. For 168 comparison, Ni(II)-IIP-S was prepared in the same manner except using SBA-15 169 substitute MMS.

170 2.3. Characterization

VISTA-MPX Inductive Coupled Plasma-Atomic Emission Spectrometer 171 (ICP-AES, Varian, USA) was used to determine the concentrations of Ni(II) and other 172 173 mental ions. Fourier transmission infrared spectra were separately recorded in a FT-IR spectrophotometer (NEXUS 470 FT-IR apparatus, Nicolet, USA) over the range of 174 4000–400 cm⁻¹. The crystal phases of the samples were determined by XRD with Cu 175 Ka radiation (model D8 diffractometer, Bruker, Germany). The morphologies of 176 177 Ni(II)-IIP and support were observed by a scanning electron microscope (SEM, JEOL, 178 JSM-6480) and a transmission electron microscope (TEM, JEOL, JEM-2100). 179 Thermogravimetric analysis (TGA) was carried out using a DSC/DTA-TG (STA 449C Jupiter Netzsch, Germany). 180

Brunauer–Emmett–Teller (BET) surface area of dried samples was analyzed by nitrogen adsorption in a Micromeritics ASAP 2000 nitrogen adsorption apparatus using the adsorption data in the relative pressure (p/p_0) range of 0.05–0.3. The nitrogen adsorption volume at the relative pressure (p/p_0) of 0.98 was used to determine the pore volume. The desorption isotherm was used to determine the pore size distribution via the Barret–Joyner–Halender (BJH) method. All samples were degassed before nitrogen adsorption measurements.

188 Porous structures of the samples were analyzed by using a mercury porosimeter 189 (Micromeritics Autopore 9500). In order to perform analysis, samples were weighed 190 and loaded onto a penetrometer which consists of a sample cup integrated with a 191 metal-clad and glass capillary stem, followed by outgassing from sample in a vacuum. 192 Then the penetrometer was automatically filled with mercury. Pore size distribution 193 (PSD) curve was determined from the mercury intrusion data. Under the assumption 194 that all pores are cylindrical, the pore diameter d_p was calculated from the value of p using a well-known capillary law [38]: 195

$$d_{\rm p} = \frac{4\gamma\cos\theta}{p} \tag{1}$$

197 where γ and θ denote the surface tension of mercury and the contact angle of mercury 198 with the sample, respectively.

199 2.4. Experimental design

200 Central composite design (CCD) was used to optimize preparation parameters 201 with adsorption capacity of resulting Ni(II)-IIP for Ni(II) as the response. The four 202 significant independent variables considered in this study were dosage of BDAAT 203 (X_1) , dosage of AM (X_2) , reaction time (X_3) , and dosage of AIBN (X_4) . CCD was characterized by three operations namely: 2n axial runs, 2^n factorial runs and six 204 205 center runs (n is the number of factors). For this case, it translated to 8 axial points, 16 206 factorial points and 6 replicates at the center which gives a total of 30 experiments 207 [28].

The usual code of ± 1 was used to represent the sixteen factorial points, $\pm \alpha$ represented the eight axial points, and the six replicates located at the center (0, 0, 0)

- 210 were run. Alpha (α) is the distance of the axial point from center had its value fixed at
- 211 α =2.0. The coded points and their corresponding values were presented in Table 1.

212	(See an	example	of table	presentation	in	Table	1)	١.
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Factors	Symbol		Actual val	ues of codeo	d levels	
Factors	Symbol -	- α *	-1	0	1	$+\alpha$
RAFT dose (g)	X_1	0.01	0.03	0.05	0.07	0.09
AM dose (g)	X_2	0.006	0.017	0.029	0.040	0.052
Reaction time (T)	X_3	2	4	6	8	10
AIBN dose (mg)	X_4	2	4	6	8	10

Table 1 Experimental ranges and levels of the independent variables.

214 Note: $\alpha = 2$.

The response variable was fitted by a second-order model in the form of quadratic polynomial equation:

$$Y = b_0 + \sum_{i=1}^n b_{ii} x_i + \sum_{i=1}^n b_{ii} x_i^2 + \sum_{i=1}^{n-1} \sum_{j=i+1}^n b_{ij} x_i x_j + \varepsilon$$
(2)

where *Y* is predicted response (predicted adsorption capacity), x_i , x_j are independent variables in coded levels, b_i , b_{ij} , b_{ij} are coefficients for linear, quadratic and interaction effect, respectively, b_0 is model coefficient, *n* is the number of factors (independent variables), and ε is model error. The quality of fit of polynomial model was expressed by value of correlation coefficient (R^2). The main indicators demonstrating the significance and adequacy of used model include model *F*-value (Fisher variation ratio), probability value (prob>*F*), and adequate precision [39].

225 2.5. Adsorption studies

226 Fixed-bed adsorption tests were performed using a glass column with 20 cm 227 height and 1 cm internal diameter at 25 °C. A known quantity 0.1 g of Ni(II)-IIP was measured into column to give the desired 0.5 cm bed height. To avoid nonuniform 228 229 flow (axial dispersion) of the solution and fluidization, some quantity of glass wool were placed in column. Feeding solution with 30 mg/L initial Ni(II) concentration was 230 231 transported using peristaltic pump from the top of column down to the bottom with 232 flow rate of 1 mL/min. The effluents were collected at a fixed time interval, until the 233 effluent Ni(II) concentration was nearly equal to influent concentration. The

concentration of Ni(II) was tested by ICP-AES.

The breakthrough curves were usually expressed by the plot of C_t/C_0 versus reaction time under various conditions. C_t and C_0 are concentration of metal ions (mg/L) in the effluent and influent, respectively.

For a given flow rate and influent concentration, maximum adsorption capacity of column, q_{total} (mg), is obtained using Eq. (3):

240
$$q_{total} = \frac{QA_c}{1000} = \frac{Q}{1000} \int_{t=0}^{t=t_{total}} C_{ad} dt$$
(3)

where Q is volumetric flow rate (mL/min) and t_{total} is total flow time (min). Meanwhile, equilibrium uptake column capacity (q_{eq}) is derived as the quantity adsorbed (q_{total}) per weight of adsorbent:

244
$$q_{eq} = \frac{q_{total}}{m} \tag{4}$$

where m is dry weight of adsorbent in column (g).

Batch experiments were carried out to obtain static adsorption capacity. The adsorption capacity $Q_e (mg g^{-1})$ at equilibrium is calculated as follows:

248
$$Q_{\rm e} = \frac{(C_0 - C_{\rm e})V}{W}$$
 (5)

where $C_0 \text{ (mg L}^{-1)}$ and $C_e \text{ (mg L}^{-1)}$ are concentrations of Ni(II) at initial and equilibrium, respectively. V (mL) and W (g) are the volume of solution and the mass of adsorbent, respectively.

252 2.6. Dynamic desorption experiments

An amiable quality of an adsorbent is its predisposition for reuse. This was investigated through desorption and regeneration studies which were valuable attributes in adsorption processes. The dynamic desorption experiment was carried out by using pre-adsorbed Ni(II)-IIP as the sample and 2 M HCl solution as an eluent.

- 257 3. Results and discussion
- 258 3.1. Preparation of Ni(II)-IIP

The synthesis of Ni(II)-IIP could be simply divided into four steps as follows: (1) Preparation of PS beads. Monodisperse PS beads can be synthesized by dispersion polymerization approach. (2) Preparation of macro-mesoporous silica. In this step, PS beads and P123 were as dual-templating to form macro and mesopores. macroporous–

mesoporous silica combined the benefits of mesoporous and macroporous structures.
(3) Surface Modification of MMS. In this step, MPS was reacted with the MMS. The
C=C was introduced onto the surface of MMS. (4) Preparation of Ni(II)-IIP.
Imprinting was conducted in this step, yielding a three-dimensional polymer network
where template Ni(II) was trapped. Then, chelated Ni(II) was eluted by 2 mol/L HCl.
Finally, a novel Ni(II)-IIP based on macroporous–mesoporous silica was obtained.

269 3.2. Characterization

270 3.2.1. FT-IR spectra

271 FT-IR spectra of (a) polystyrene; (b) MMS; (c) Ni(II)-IIP were given in Fig. 1. For PS (**Fig. 1a**), the band around 3060 cm⁻¹ and 3027 cm⁻¹ was attributed to aliphatic 272 C-H stretching vibration. The bands at 2924 cm⁻¹ and 2846 cm⁻¹ were the 273 characteristic adsorption peaks of -CH₃ and -CH₂-, respectively. The adsorption peaks 274 at 1945, 1872, 1801 and 1601 cm⁻¹ assigned to benzene rigid vibration. The sharp 275 band at 540 cm⁻¹ corresponded to twist vibration of C=C of vinyl compound. After 276 277 the calcination, the obtained MMS showed adsorption bands of silica at 1090 $\rm cm^{-1}$, adsorbed water at 1640 cm⁻¹, and hydroxyl group at around 3500 cm⁻¹, and no band 278 279 associated with organic species was detected, suggesting the full decomposition of 280 polymer microsphere templates and surfactant templates. These results demonstrated 281 the successful synthesis of macro-/mesoporous silica materials by using the polystyrene and block copolymer P123 as dual templates. Ni(II)-IIP (Fig. 1c) 282 exhibited obvious adsorption bands around 1733 cm⁻¹, which was due to the C=O 283 stretching vibration. The adsorption peaks at 1635 and 1458 cm⁻¹ assigned to amide I 284 and -CH2- deformation characteristic adsorption, respectively. These results 285 suggested that Ni(II)-IIP was successfully synthesized. (See an example of artwork 286 287 presentation in Figure 1).



2	8	8
2	8	9

Fig. 1 FT-IR spectra of (a) PS; (b) MMS; (c) Ni(II)-IIP.

290 3.2.2. Surface morphology

The surface morphology of a) polystyrene, b) SBA-15 and c) MMS were studied by scanning electron microscopy. The as-prepared PS microspheres had a mean diameter of $\sim 1.2 \,\mu$ m with a standard size deviation of less than 5% (**Fig. 2a**). SEM of the undoped SBA-15 revealed a rod-like morphology characteristic of this class of material [40]. The addition of PS beads modified the SBA-15-like organization, creating a new macroporous network. It was interesting to note that the macropores were open and thus well-suited to promote rapid transfer through particle diffusion.

298 TEM images of the obtained MMS showed macropores of ca. 1.1 μ m (Fig. 3a). 299 Mesopore character showed that the typical mesoporous structure of SBA-15 was 300 retained in MMS (Fig. 3b). The pore sizes of MMS were observed to be ca. 5-6 nm, 301 with a wall thickness of ca. 6-7 nm. After polymerization, thin polymer layers were 302 formed onto the surface of the MMS (Fig. 3c). The polymer layer had a thickness of 303 about 20 nm and appeared to be uniform, which could be attributable to the intrinsic 304 characteristics of the controlled/living polymerization mechanism of the RAFT polymerization process [41]. (See an example of artwork presentation in Figure 2). 305 306 (See an example of artwork presentation in Figure 3).



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Fig. 2 SEM images of: a) PS beads; b) SBA-15 and c) MMS.



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Fig. 3 TEM images of: a) macropore structures in MMS; mesopore structures in b)

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MMS and c) Ni(II)-IIP.

312 3.2.3. Characterization of pores

313 Nitrogen adsorption-desorption isotherms showed all materials exhibit Type IV adsorption isotherms with type-H1 hysteresis loops characteristic of bottlenecked pore 314 openings evident in Fig. 4A, which was a characteristic of mesoporous materials. 315 316 Pure mesoporous SBA-15 had the largest BET specific surface area, pore size and pore volume. Compared with pure SBA-15, the addition of PS beads created new 317 318 macropores morphology. However, the introduction of macropores didn't affect its 319 mesoporous characteristics, the BET specific surface area, pore size and pore volume 320 of MMS were all similar to SBA-15. After polymerization, the BET specific surface area had a different degree of reduction for different synthesis conditions. Fig. 4A c-e 321 were Ni(II)-IIP prepared with a AM loading of 0.006 g, 0.029 g, 0.052 g, respectively 322

323 (the samples c, d, and e correspond to entries 13, 6, and 20 in **Table 3**, respectively), 324 which were abbreviated as Ni(II)-IIP-0.006, Ni(II)-IIP-0.029, Ni(II)-IIP-0.052, 325 respectively. The BET specific surface area decreased from 479.4 to 272.5 m^2/g as the amount of AM was increased from pristine MMS to Ni(II)-IIP-0.052. The similar 326 trend was observed for the total pore volume decreasing from 1.194 to 0.815 cm^3/g , 327 concomitant with the narrow pore size distribution ranging from 5.5 to 3.4 nm (Fig. 328 329 4B and **Table 2**). These results can be explained that the attachment of polymer layers 330 on the MMS surfaces decreased specific surface area and pore sizes and subsequently 331 limited the diffusion. NIP was synthesized using the same procedure as 332 Ni(II)-IIP-0.029, but in the absence of Ni(II) ion. Comparison of Ni(II)-IIP-0.029 and 333 NIP showed that the BET surface area, pore volume and pore size of the former were 334 slightly larger than those of the latter, probably owing to those cavities left after the 335 elution of Ni(II). (See an example of artwork presentation in Figure 4). (See an 336 example of table presentation in Table 2). (See an example of table presentation in Table 3). 337



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339

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Fig. 4 Nitrogen adsorption-desorption isotherms (A) and pore size distribution (B) of
a) SBA-15; b) MMS; Ni(II)-IIP prepared with a AM loading of 0.006 g (c), 0.029 g
(d), 0.052 g (e), respectively (the samples c, d, and e correspond to entries 13, 6, and

20 in Table 2, respectively) and (f) NIP.

344	Table 2 Physical parameters of SBA-15, MMS, Ni(II)-IIP prepared with a AM						
345	loading of 0.006 g, 0.029 g, 0.052 g, respectively measured by $N_{\rm 2}$						
346	adsorption-desorption isotherms and NIP.						
	Samples	BET surface area	Pore size (nm)	Pore volume (cm ³ /g)			
	SBA-15	490.6	5.7	1.212			
	MMS	479.4	5.5	1.194			
	Ni(II)-IIP-0.006	436.0	4.9	1.098			
	Ni(II)-IIP-0.029	374.7	4.2	1.024			
	Ni(II)-IIP-0.052	272.5	3.4	0.815			
_	NIP	352.7	4.0	0.975			

Table 3 CCD and results for the study of four experimental variables in actual units.

		Actual	lavals		Ni(II) adsorpt	ion capacity
Run		Actual			(mg/	/g)
	X ₁ (g)	$X_2(g)$	X ₃ (h)	X ₄ (mg)	Experimental	Predicted
1	0.05	0.029	10	6	11.2	10.96
2	0.03	0.040	8	8	10.2	10.16
3	0.07	0.017	4	8	8.2	8.33
4	0.07	0.017	4	4	8.6	8.56
5	0.05	0.029	6	6	12.1	12.32
6	0.05	0.029	6	6	12.3	12.32
7	0.03	0.040	8	4	10.4	10.63
8	0.07	0.040	4	4	12.2	12.35
9	0.05	0.029	2	6	10.4	10.36
10	0.07	0.040	8	4	12.1	12.08

I ugo Io ol ol

11	0.07	0.017	8	8	9.8	9.96
12	0.05	0.029	6	2	11.4	11.36
13	0.05	0.006	6	6	5	4.79
14	0.07	0.040	4	8	11.2	11.23
15	0.09	0.029	6	6	12.8	12.58
16	0.03	0.040	4	4	11.9	11.66
17	0.03	0.017	8	4	9.2	9.09
18	0.05	0.029	6	6	12.6	12.32
19	0.05	0.029	6	10	10.9	10.66
20	0.05	0.052	6	6	9.3	9.23
21	0.07	0.040	8	8	10.7	10.85
22	0.05	0.029	6	6	12.4	12.32
23	0.01	0.029	6	6	11.5	11.44
24	0.03	0.040	4	8	11.1	11.28
25	0.07	0.017	8	4	10.1	10.28
26	0.03	0.017	8	8	9.3	9.52
27	0.05	0.029	6	6	12.3	12.32
28	0.05	0.029	6	6	12.2	12.32
29	0.03	0.017	4	4	7.9	8.12
30	0.03	0.017	4	8	8.7	8.64

349 Mercury penetration was also used to characterize the pores, and the data were 350 shown in Fig. 5. The mesopore size distribution of MMS was centered at 5.5 nm, 351 which was consistent with the above nitrogen adsorption-desorption data. And another 352 important data were the second peak of MMS with an average diameter of 1096 nm, 353 the macropores were close to the parent PS beads dimensions. This contrasted with 354 previous reports [42]. Herein notable macropore shrinkage was observed after 355 calcination. After polymerization reaction, the mesopores and macropores of 356 Ni(II)-IIP were reduced to 4.2 nm and 988 nm, respectively. Although there was a slight decrease of macropores, but it can still act as channels and reduce mass transfer 357

resistance. (See an example of artwork presentation in Figure 5).





360

Fig. 5 Pore size distribution determined by mercury porosimetry.

361 3.2.4. XRD characterization

362 XRD patterns of MMS and Ni(II)-IIP were presented in **Fig. 6**. All the samples 363 exhibited well defined peaks at 1.01°, 1.70° and 1.96°, associated with the (100), (110) 364 and (200) planes of the P6mm space group for the hexagonal arrangement of 365 mesoporous channels, suggesting that pore structure is retained after polymerization. 366 However, there is a slight shift of the small-angle shift to higher angles, indicating the 367 decrease in d-spacing [43]. (See an example of artwork presentation in Figure 6).



368

Fig. 6 Low angle powder XRD patterns of: a) MMS; and b) Ni(II)-IIP.

370 3.2.5. Characteristic of TGA

The thermal behavior of polymers was evaluated by TGA (**Fig. 7**). The first mass loss steps, from about 25 to 100 °C, were due to the loss of physically adsorbed water on surface of MMS. The high rate of weight loss in temperature ranging from 200 to 800 °C may be due to the loss of polymer layer. Throughout the analysis, total mass loss of MMS and Ni(II)-IIP were calculated to be 4.78% and 27.16%, respectively. The remaining mass was attributed to the more thermally resistant silicon-based material. (See an example of artwork presentation in Figure 7).



Fig. 7 TGA profiles of MMS and Ni(II)-IIP.

380 3.3. Discussion of regression model

Table 3 represents the experimental planning matrix with the response variables obtained experimentally. The following equation is a regression model with experimental results:

$$Q_{e} = +12.32 + 0.28X_{1} + 1.11X_{2} + 0.15X_{3} - 0.18X_{4} + 0.063X_{1}X_{2} + 0.19X_{1}X_{3}$$
$$-0.19X_{1}X_{4} - 0.50X_{2}X_{3} - 0.22X_{2}X_{4} - 0.025X_{3}X_{4} - 0.077X_{1}^{2} - 1.33X_{2}^{2} \qquad (6)$$
$$-0.41X_{3}^{2} - 0.33X_{4}^{2}$$

where Q_e is predicted adsorption capacity of Ni(II); X_1 , X_2 , X_3 and X_4 are coded values of amount of BDAAT, consumption of AM, reaction time and dosage of AIBN, respectively.

Analysis of variance (ANOVA) was used for further justification of the adequacy 388 389 of model. The significance of each model was assessed from adjusted determination coefficient (R_{adj}^2) which was found to be 0.9838, implying that only 1.62% of 390 variation in Q_e response cannot be explained by this model. The *F*-value for a model 391 392 was the test for comparing variance associated with that term with residual variance. 393 As it can be seen in **Table 4**, model *F*-value of 127.19 implied that the model was 394 significant. There was only a 0.01% chance that a "Model F-value" this large could 395 occur due to noise. The significance of each term in this model was also evaluated by 396 *p*-value (prob>*F*). The smaller *p*-values, the bigger the significance of corresponding variable. p-values in this study less than 0.05 indicate model terms were significant. In 397 this case $X_1, X_2, X_3, X_4, X_1X_3, X_1X_4, X_2X_3, X_2X_4, X_2^2, X_3^2, X_4^2$ were significant model 398 terms. The coefficient of variation (CV) indicated the degree of precision with which 399 400 the treatments are compared. A lower CV meant a higher reliability of the experiment.

The lower value of CV (2.11%) demonstrated the performed experiments were highly reliable. The value of 0.2233 for "Lack of Fit *F*-value" implied that Lack of Fit was not significant relative to pure error. Non-significant lack of fit was good and showed that the above model was appropriate to predict the adsorption capacity of Ni(II) within the range of variables studied. (See an example of table presentation in Table 406 4).

Sources of variation	Sum of squares	Degree of freedom	Mean square	F value	Probability> <i>F</i>	7 Comment
Model	89.43	14	6.39	127.19	< 0.0001	significant
X_1	1.93	1	1.93	38.36	< 0.0001	significant
<i>X</i> ₂	29.48	1	29.48	587.02	< 0.0001	significant
<i>X</i> ₃	0.54	1	0.54	10.75	0.0051	significant
X_4	0.74	1	0.74	14.63	0.0017	significant
X_1X_2	0.06	1	0.06	1.24	0.2822	
<i>X</i> ₁ <i>X</i> ₃	0.56	1	0.56	11.20	0.0044	significant
X_1X_4	0.56	1	0.56	11.20	0.0044	significant
X ₂ X ₃	4.00	1	4.00	79.65	< 0.0001	significant
<i>X</i> ₂ <i>X</i> ₄	0.81	1	0.81	16.13	0.0011	significant
X ₃ X ₄	0.01	1	0.01	0.20	0.6618	
X_{1}^{2}	0.16	1	0.16	3.25	0.0918	
X_{2}^{2}	48.31	1	48.31	961.84	< 0.0001	significant
X_{3}^{2}	4.71	1	4.71	93.87	< 0.0001	significant
	Sources of variation Model X_1 X_2 X_3 X_4 X_1X_2 X_1X_2 X_1X_3 X_2X_3 X_2X_4 X_3X_4 X_1^2 X_2X_4 X_2X_4 X_1^2 X_2^2 X_2^2 X_3^2	Sources of variation Sum of squares Model 89.43 X_1 1.93 X_2 29.48 X_3 0.54 X_4 0.74 X_1X_2 0.06 X_1X_3 0.56 X_1X_3 0.56 X_1X_4 0.56 X_2X_3 4.00 X_2X_4 0.81 X_3X_4 0.01 X_1^2 0.16 X_2^2 48.31 X_3^2 4.71	Sources of variationSum of squaresDegree of freedomModel 89.43 14 X_1 1.93 1 X_2 29.48 1 X_3 0.54 1 X_4 0.74 1 X_1X_2 0.06 1 X_1X_3 0.56 1 X_1X_4 0.56 1 X_2X_3 4.00 1 X_2X_4 0.81 1 X_3X_4 0.01 1 X_1^2 0.16 1 X_2^2 48.31 1	Sources of variationSum of squaresDegree of freedomMean squareModel 89.43 14 6.39 X_1 1.93 1 1.93 X_2 29.48 1 29.48 X_3 0.54 1 0.54 X_4 0.74 1 0.74 X_1X_2 0.06 1 0.06 X_1X_3 0.56 1 0.56 X_1X_4 0.56 1 0.56 X_2X_4 0.81 1 0.81 X_3X_4 0.01 1 0.01 X_2^2 48.31 1 48.31 X_3^2 4.71 1 4.71	Sources of variationSum of squaresDegree of freedomMean squares F valueModel 89.43 14 6.39 127.19 X_1 1.93 1 1.93 38.36 X_2 29.48 1 29.48 587.02 X_3 0.54 1 0.54 10.75 X_4 0.74 1 0.74 14.63 X_1X_2 0.06 1 0.06 1.24 X_1X_3 0.56 1 0.56 11.20 X_2X_3 4.00 1 4.00 79.65 X_2X_4 0.81 1 0.61 3.25 X_2^2 48.31 1 0.16 3.25 X_2^2 48.31 1 4.71 93.87	Sources of variation Sum of squares Degree of freedom Mean squares F value Probability> F Model 89.43 14 6.39 127.19 < 0.0001

407 Table 4 Analysis of variance for the response of the adsorption capacity for Ni(II).

X_{4}^{2}	2.93	1	2.93	58.43	< 0.0001	significant
Residual	0.75	15	0.05			
Lack of fit	0.60	10	0.06	2.04	0.2233	not significant
Pure error	0.15	5	0.03			
Total	90.18	29				

Fig. 8 showed predicted values versus experimental values for Ni(II) adsorption capacity. The obtained experimental values were quite close to predicted values, indicating that the developed model was successful in capturing the correlation between Ni(II)-IIP preparation variables to Ni(II) adsorption capacity. (See an example of artwork presentation in Figure 8).



413 414

Fig. 8 Predicted vs. experimental Ni(II) adsorption capacity of Ni(II)-IIP.

415 3.4. Effects of process parameters on optimization

Response surface plots and contour plots were shown in **Figs. 9-10**, which provided a method to visualize the relationship between response and experimental levels of each variable and the type of interactions between two test variables. The shapes of the contour plots, circular or elliptical, indicated whether the mutual interactions between variables were significant or not.

The combined effect of amounts of BDAAT (X_1) and AM (X_2) on Ni(II) dynamic adsorption was shown in **Figs. 9a-b**. Obviously, the amount of AM played an important role in controlling final adsorption capacity for Ni(II) during preparation process. It was observed that when the amount of AM was lower than 0.029 g (4 times molecular weight of template ion), adsorption capacity of Ni(II) on Ni(II)-IIP

426 increased with increasing AM content due to the increase in the number of recognition 427 sites. However, a slight decrease in the adsorption amount could be obtained as the 428 content of AM was above 0.029 g. This was because excessive functional monomers 429 would occur self-polymerization, which made the decrease of recognition sites and 430 specific surface area [44]. Meanwhile, adsorption capacity of Ni(II) increased with 431 increasing BDAAT content. BDAAT, a reversible chain transfer agent, can easily 432 introduce functional groups into the chain ends of polymers and control the chains of 433 polymers with appropriate molar mass and low polydispersity. The more dosage of 434 BDAAT, the more structured polymer layer and higher adsorption capacity. A 435 maximum Ni(II) adsorption (>12 mg/g) was determined at constant T (6 h) and AIBN 436 dose (6 mg).

The interaction relationships of BDAAT (X_1) with reaction time (X_3) on dynamic 437 adsorption of Ni(II) were shown in Figs. 9c-d. It was evident that at high value, 438 439 about >0.045 g, the positive influence of reaction time on Ni(II) adsorption was 440 significant. While in case of the BDAAT dose being below 0.045 g, adsorption 441 capacity of Ni(II) would fall below 12.2 mg/g no matter reaction time was. And for a 442 definite amount of BDAAT, an optimum reaction time existed around 6.3 h. Reaction 443 time was an important condition for synthesis process of imprinted polymers. If 444 reaction time was short, imprinted sites would be relatively poor. Whereas, molecular 445 weight of polymer will be great in the case a long time, causing the polymer layer too thick. A maximum Ni(II) adsorption (>12.4 mg/g) was observed at constant AM 446 dosage (0.029 g) and AIBN dose (6 mg). 447

In Figs. 9e-f, response curve and isogram were drawn as a function of BDAAT 448 449 (X_1) and AIBN (X_4) doses. It was observed that adsorption capacity increased with 450 increase in BDAAT and AIBN dose. However, up to a certain limit adsorption 451 capacity was decreased by increasing AIBN dose. AIBN was the most common kind 452 of azo initiators. The higher initiator agent content, the higher concentration of active 453 centers, so that polymerization rate was accelerated, thereby affecting the molecular 454 weight of polymer. Thus, the impact of the amount of initiator and reaction time on adsorption capacity had a similar effect. Meanwhile, with the increase of BDAAT, the 455

amount of AIBN had more and more impact on adsorption capacity. It can be seen
that RAFT agent played an important role in reaction. A maximum Ni(II) adsorption
(>12.6 mg/g) was observed at constant AM dosage (0.029 g) and T (6 h). (See an
example of artwork presentation in Figure 9). (See an example of artwork
presentation in Figure 10).



461

Fig. 9 (a) Three-dimensional response surface plot and (b) contour plot of interactions
of variables BDAAT and AM doses and its effect on Ni(II) adsorption. (c)
Three-dimensional response surface plot and (d) contour plot of interactions of
variables BDAAT dose and reaction time and its effect on Ni(II) adsorption. (e)
Three-dimensional response surface plot and (f) contour plot of interactions of
variables BDAAT and AIBN doses and its effect on Ni(II) adsorption.





Fig. 10 (a) Three-dimensional response surface plot and (b) contour plot of
interactions of variables AM dose and reaction time and its effect on Ni(II) adsorption.
(c) Three-dimensional response surface plot and (d) contour plot of interactions of
variables AM and AIBN doses and its effect on Ni(II) adsorption. (e)
Three-dimensional response surface plot and (f) contour plot of interactions effect of
AIBN dose and reaction time and its effect on Ni(II) adsorption.

475

476 The effect of AM dose (X_2) and reaction time (X_3) on Ni(II) dynamic adsorption 477 capacity was illustrated in Figs. 10a-b. When AM dose and reaction time increased 478 simultaneously, adsorption capacity increased and then decreased. This can be 479 explained by the above conclusion. The binding sites were increasing rapidly when 480 both were increased. But when AM dose and reaction time were extreme, 481 self-polymerization and excessive growth of chain occurred simultaneously, causing 482 the decrease of binding sites and specific surface area. A maximum Ni(II) adsorption 483 (>12 mg/g) was observed at constant BDAAT dosage (0.05 g) and AIBN dose (6 mg).

Figs. 10c-d gave a clear idea about the effect of AM (X_2) and AIBN (X_4) doses on Ni(II) dynamic adsorption. It can be seen that Fig. 10d and Fig. 10b showed similar pattern. Therefore, the above theory can also be used to explain these trends. A
maximum Ni(II) adsorption (>12 mg/g) was observed at constant BDAAT dosage
(0.05 g) and T (6 h).

The effect of reaction time (X_3) and AIBN dose (X_4) on Ni(II) dynamic adsorption capacity was illustrated in **Figs. 10e-f**. It can be concluded that Ni(II) adsorption capacity increased with reaction time within 5.1-7.6 h range and AIBN dose within 4.1-6.8 mg range. At constant BDAAT (0.05 g) and AM (0.029 g) dose, a maximum Ni(II) removal of >12.2 mg/g was determined.

494 3.5. Validation of models

495 To confirm the goodness of the model for predicting maximal Ni(II) adsorption 496 capacity, additional experiments in triplicate using these optimized conditions were 497 carried out. According to the results of statistical design, the optimized preparation 498 conditions were as follows: BDAAT dose 0.07 g, AM dose 0.029 g, reaction time 6.3 499 h, and AIBN dose 4.54 mg, obtaining maximum dynamic adsorption capacity (12.96 500 mg/g) of Ni(II). To ensure the predicted result was not bias the practical value, 501 experiment rechecking was performed using modified optimal conditions: BDAAT 502 dose 0.07 g, AM dose 0.029 g, reaction time 6.3 h, and AIBN dose 4.5 mg. A mean value of 12.83 ± 0.23 mg/g (N=3) was gained, which was in agreement with the 503 504 predicted value significantly, demonstrated the validation of RSM model.

505 3.6. Comparison of different adsorbents

In order to verify the superiority of macro-mesoporous silica, dynamic 506 adsorption properties of Ni(II)-IIP, Ni(II)-IIP-S and NIP were studied. The results 507 were shown in Fig. 11. Compared with Ni(II)-IIP-S, Ni(II)-IIP exhibited higher 508 509 dynamic adsorption capacity. The adsorption capacity of Ni(II)-IIP was 12.16 mg/g, 510 more than that of Ni(II)-IIP-S (7.59 mg/g). The results proved that the introduction of 511 macropores may act as channels and facilitate the transport of Ni(II) to be adsorbed in 512 mesopores, thus favoring mass transfer and reducing transport limitations. And the 513 adsorption capacity of Ni(II)-IIP was also much higher than NIP, this result proved 514 excellent adsorption ability of Ni(II)-IIP due to the specific binding sites. (See an 515 example of artwork presentation in Figure 11).



516 517

Fig. 11 Adsorption study of different adsorbents.

Nowadays, there was few literatures investigating the dynamic adsorption on 518 519 Ni(II). In this study, dynamic adsorption is the main adsorption mode. But the fact 520 that the adsorption capacity of dynamic mode was much smaller than that of static has 521 been proved in lots of literatures [45]. Hence, Static adsorption studies were also 522 carried out to research the property of Ni(II)-IIP. A comparison of the maximum static capacity (Q_{max}) of Ni(II) onto Ni(II)-IIP with those of other adsorbents reported in the 523 literatures is given in Table 5. It was obviously seen that Ni(II)-IIP had the highest 524 adsorption capacity (92.48 mg g^{-1}) among these adsorbents. (See an example of table 525 526 presentation in Table 5).

Sorbent	Maximum adsorption capacity (mg/g)	Reference
Cashew nut shell	18.87	[46]
ECH crosslinked chitosan– clay beads	32.36	[47]
Fe3O4–TW	38.30	[48]
IIP	40.26	[49]
RAFT-IIP	81.73	[50]
Ni(II)-IIP	92.48	This study

527 Table 5 Comparison of maximum adsorption of Ni(II) ions onto various adsorbents.

528 3.7. Competitive adsorption of Ni(II)-IIP

The effect of interference of coexisting ions of Cd(II), Co(II),Cu(II) and Zn(II) (30 mg/L) with Ni(II) ion (30 mg/L) on the adsorption of Ni(II) was studied using the dynamic procedure. Adsorption capacities of the Ni(II)-IIP and NIP for metal ions under competitive conditions were given in **Fig. 12**. Ni(II)-IIP exhibited good adsorption selectivity for Ni(II) in the presence of competitive metal ions. And it was
obviously that adsorption capacity of Ni(II)-IIP was higher than that of NIP, which
were due to the presence of specific cavities on imprinted adsorbents. (See an
example of artwork presentation in Figure 12).



537



539 3.8. Reusability of Ni(II)-IIP

540 For economic reasons, the recyclability of spent adsorbent is a key evaluation 541 factor. Several eluents were tried in order to regenerate Ni(II)-IIP. The desorption of Ni(II) is 87.6%, 92.1%, and 97.8% for 2.0 mol/L HNO₃, 2.0 mol/L H₂SO₄, and 2.0 542 543 mol/L HCl, respectively. Among them 2.0 mol/L HCl was proved to be a relatively 544 effective eluent for desorption of Ni(II) ions from Ni(II)-IIP. Adsorption-desorption 545 results of repeated uses in Ni(II)-IIP were shown in **Fig. 13**. It is stable for up to five 546 adsorption cycles without obvious decrease in the removal efficiency for Ni(II). The 547 experimental results indicate that Ni(II)-IIP had excellent regeneration ability. (See an 548 example of artwork presentation in Figure 13).



549

550

Fig. 13 Stability and potential regeneration of Ni(II)-IIP.

552 **4.** Conclusion

553 Response surface methodology was applied for optimizing the preparation parameters to obtain Ni(II) ion imprinted polymer with excellent adsorption properties 554 555 for Ni(II). The use of macro-mesoporous silica matrix significantly improved the 556 adsorption capacity of imprinted polymer. The statistical analysis results showed that the 557 appropriate preparation conditions were follows: as 558 S,S'-bis(α, α' -dimethyl- α'' -acetic acid)trithiocarbonate dose 0.07 g, acrylamide dose 559 0.029 g, reaction time 6.3 h, and 2,2'-azobisisobutyronitrile dose 4.54 mg. Among 560 four parameters, the amount of acrylamide was the most important one in controlling 561 the final adsorption capacity. Moreover, the prepared Ni(II) ion imprinted polymer 562 exhibited a good selectivity of Ni(II) and eluting performance.

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