

Environmental Science Water Research & Technology

Accepted Manuscript



This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. We will replace this *Accepted Manuscript* with the edited and formatted *Advance Article* as soon as it is available.

You can find more information about *Accepted Manuscripts* in the [Information for Authors](#).

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard [Terms & Conditions](#) and the [Ethical guidelines](#) still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.

1 Bacterial production of transparent exopolymer particles during static and 2 laboratory-based cross-flow experiments

3

4 Tamar Jamieson¹, Amanda V. Ellis², Dmitriy A. Khodakov², Sergio Balzano¹, Deevesh A. Hemraj¹, Sophie C. Leterme^{1*}

5

6 ¹School of Biological Sciences, Flinders University, GPO BOX 2100, Adelaide SA 5001, Australia7 ²Flinders Centre for Nanoscale Science and Technology, School of Chemistry and Physical Sciences, Flinders

8 University, GPO BOX 2100, Adelaide SA 5001, Australia

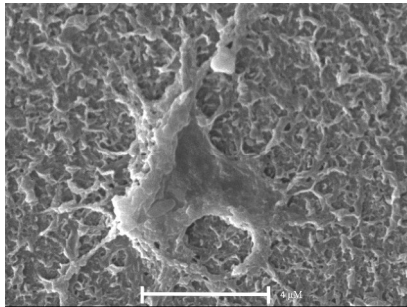
9

10 * Corresponding author: Sophie C. Leterme, sophie.leterme@flinders.edu.au, Tel: +61 8 8201 3774

11

12

13 Table of Contents entry

15 The aim of this paper was to provide novel insights into the biofouling mechanism of transparent exopolymer particles (TEP)
16 production through the use of static and laboratory-based cross flow experiments.

17

18 Abstract

19 Biofouling of seawater reverse osmosis (SWRO) membranes represents one of the leading causes of performance deterioration in the
20 desalination industry. This work investigates the biofouling potential of microbial communities present in a reverse osmosis (RO) feed tank. As
21 an example, water from the RO feed tank of the Penneshaw desalination plant (Kangaroo Island, South Australia) was used in a static biofilm

22 formation experiment. Cultures of the indigenous biofilms formed during the static experiment showed that α -Proteobacteria and γ -
23 Proteobacteria accounted for nearly 80% of the classes of bacteria present in the RO feed tank. *Pseudomonas* sp. was identified as the major
24 species and isolated for testing in static and laboratory-based cross flow biofilm formation experiments. Results showed that the volume of TEPs
25 generated by *Pseudomonas* sp. during the laboratory-based cross-flow experiment was 10 fold higher to that produced during the static
26 experiment for the same time period, while both experiments were inoculated with cell concentrations of the same order of magnitude. The
27 availability of nutrients was also shown to be a key driver in TEP production, particularly for the static experiments. This study provides insights
28 into the phenomenon of biofouling by assessing the production of biofouling precursors from one of the main genera of biofilm-forming
29 bacteria, namely *Pseudomonas* sp..

30

31 **Water Impact Statement**

32 Seawater reverse osmosis (SWRO) desalination is considered one of the most effective methods to combat world water
33 shortages. However, loss of productivity and costs in SWRO are associated with biofouling issues. This paper provides new
34 insights on the precursors of biofilm formation on RO membranes. Results show that nutrient availability has a significant
35 impact on the production of biofouling precursors.

36

37 **Introduction**

38 Throughout the world, the desalination of seawater is expanding in response to climate change and associated increases in
39 temperature, desertification and drought.¹ Water shortages are further exacerbated due to the stress of an increasing
40 population, uneven water distribution and stringent water quality regulations.¹

41 Desalination plants are extensively recognized as an effective treatment of seawater and/or brackish water to produce
42 fresh water, especially with the advances made in membrane materials and components.² Seawater reverse osmosis (SWRO) is
43 considered the simplest and most cost effective method of freshwater production in comparison to other separation methods
44 such as distillation, solvent extraction, ion-exchange and adsorption.³ However, SWRO systems are prone to clogging and biofilm
45 formation on the RO membrane. Membrane fouling still occurs even after seawater pre-treatment and cross-flowing within the
46 RO system.⁴ This results in a negative impact on the performance of the system through a decline in the water flux as well as an
47 increase in the amount of seawater rejected, energy requirement and system pressure.^{2, 5-6}

48 The control of biofilm formation is a complicated and controversial process involving the reduction of microorganisms
49 within the RO water, monitoring strategies and controlling factors such as nutrient concentrations and physico-chemical

50 interactions between microorganism and membrane surface.⁷ In particular, bacteria are highly abundant organisms in aquatic
51 habitats and can take part in the biofouling process.⁸

52 The inflow of live biofilm forming bacteria, organics and nutrients onto the RO membrane allows for growth and
53 proliferation of the bacteria leading to biofouling.⁹ The accumulation of nutrients from the water and metabolites produced by
54 bacteria such as extracellular polymeric substances (EPS), proteins, and lipids further allow microorganisms to adhere and grow
55 on the membrane surface.⁶

56 Biofilms consist of sessile microbial cells contained within a heterogeneous matrix of EPS, which attach irreversibly to a
57 solid surface.¹⁰ These cells differ from free-living cells of the same species in terms of growth rate and gene expression as they
58 have an altered phenotype.¹⁰ The physical and chemical processes that are involved in the early formation of a biofilm are not
59 well understood. However, a sequence of processes is thought to lead to the formation of a biofilm such as a) the adsorption of
60 organic and inorganic particles on the surface, b) attachment of pioneer microorganisms, c) growth and reproduction of primary
61 colonisers and d) maturation of the biofilm matrix.¹¹

62 Transparent exopolymer particles (TEPs) are often found in the marine environment and play a crucial role in the formation
63 and development of marine biofilms.¹² They are deformable, gel like transparent particles that appear in many forms, such as
64 amorphous blobs, clouds, sheets, filaments or clumps.¹³ TEPs can be formed spontaneously from the aggregation of dissolved
65 precursor substances, which is controlled by environmental parameters such as turbulence, ion density and concentration of
66 inorganic colloids as well as the type and concentration of precursors present in water.¹⁴ In the marine environment, TEPs serve
67 as “hot spots” of intense microbial and chemical activity within the water column facilitating the attachment of planktonic TEPs
68 to surfaces.¹⁵ Within the desalination process, high levels of potential biofilm forming TEPs have been found to reach the RO
69 membrane.¹²

70 EPS, a main component of TEPs, is produced by phytoplankton and bacteria.¹⁶ EPS production has been found to be species
71 specific and dependent on surrounding growth conditions.¹⁷ When attached to surfaces such as biofilms, bacteria produce EPS
72 in large amounts.¹⁸ In contrast, when in a planktonic state within the water column, bacteria produce TEP.¹⁹ However, the role
73 of bacteria in the production of TEPs is not yet known due to the close association between phytoplankton and bacteria when
74 experiments are conducted *in situ*.¹⁷

75 Biofilms have been strongly implicated in the biofouling of the SWRO membranes present in desalination plants. However,
76 only very small portions of biofouling microbes have been identified thus far. As the microbial community composition changes
77 seasonally, so do the conditions that influence biofouling. Therefore, the present study aims to fill this gap in knowledge by
78 identifying the composition, diversity and biofouling potential of the cultivable microbial communities present after seawater

79 pre-treatments but before the RO process (i.e., RO feed tank water) within a desalination plant. This study thus identifies the
80 bacteria likely to be involved in biofilm formation on the SWRO membranes. In particular, the bacteria *Pseudomonas* sp., which
81 was isolated from RO feed tank water and tested.

82

83 **Experimental methods**

84 **Study site**

85 The Penneshaw SWRO desalination plant has a capacity of 3×10^5 L day⁻¹ and has been described in detail in previous
86 studies^{20,21}. Seawater from a depth of 6 m is pumped from the coastal waters north of Kangaroo Island at a site located 190 m
87 from the Penneshaw desalination plant and enters the system through two pre-filtration screens (10 cm and 0.5 mm pore sizes,
88 respectively). This is then followed by the pre-treatment system which includes an MP-UV disinfection unit, four parallel MMF
89 (gravel, garnet, sand and coal with grain size ranging from 0.3 to 10 mm), and two consecutive sets of three CFs each with a pore
90 size of 15 µm and 5 µm, respectively. The flow rate through the system is typically 8.4 L sec⁻¹ after which the seawater enters
91 the RO feed tank. For the study, the fully operational Penneshaw SWRO plant was selected due to its small size and simple
92 configuration along with the lack of biocide and coagulant applications in its pre-treatment.

93 Seawater samples used in this study were obtained from the RO feed tank of the desalination plant at Penneshaw. Samples
94 from the RO feed tank were collected in 20 L white opaque carboys and kept on ice during transportation to the laboratory
95 where they were stored at 4 °C in the dark to minimize changes in the water properties (i.e., nutrients and microbial content).

96

97 **Biofilm formation from RO feed tank water**

98 **Static experimental setup.** Flat sheets of polyamide thin-film composite (TFC) seawater reverse osmosis membranes FILMTEC™
99 SW30HR (DOW, California, USA) similar to those used in the RO unit at Penneshaw were used for this experiment. TFC
100 membranes were sterilized with 80% v/v isopropanol and then washed with sterile Milli-Q water (18.2 Ω cm). To investigate the
101 sequential formation of biofilm over time the TFC membranes were incubated in RO feed tank water under static conditions.
102 Five 1 L containers were filled with RO feed tank water in which six TFC membranes were placed. Four containers were
103 incubated in the dark, one of which contained sterile RO feed tank water (i.e., autoclaved for 15 min at 121 °C). The remaining

104 container was under a 12:12 hour light/dark cycle as a control to emulate the natural day/night cycle conditions of seawater.

105 The RO feed tank water in each container was replaced every three days and assessed for microbial abundance.

106 The six membranes placed in the containers were dedicated to a specific incubation period (i.e., 14, 28 or 56 days) (see
107 Supplementary Information Table S1). At the end of the incubation periods of 14, 28 and 56 days, one membrane was removed
108 from each container for bacteria isolation and a second membrane was removed to analyze the amount of TEP accumulated in
109 the biofilm formed on the membrane. Those membranes were then replaced by a clean membrane (see Supplementary
110 Information Table S1).

111 **Isolation of biofouling microbial communities.** Upon the removal of the membrane from the incubation container, the
112 biofilm was removed via scraping with a scalpel and resuspended in 1 mL of autoclaved raw seawater (15 min at 121 °C).
113 Dilutions of 1:10, 1:50 and 1:100 in sterile seawater were spread plated onto either Luria-Bertani (LB) agar or nutrient agar and
114 incubated in the dark at 20 °C in a temperature cycling chamber (Labec, Australia).

115 Single colonies were patched on LB agar, or nutrient agar, and incubated in the dark at 20 °C in the temperature cycling
116 chamber. Individual colonies were subsequently inoculated into 5 mL of the sterile liquid phase of the same medium and
117 incubated as previously described.

118 **Identification of biofouling microbial communities.** Genomic DNA was extracted from single colonies using a modified
119 protocol from Real Genomics HiYield™ DNA extraction kit (Real Biotech Corporation, Taiwan). Amplification of the 16S rRNA
120 regions from the genomic DNA was undertaken with one pair of universal primers for bacteria: CC
121 (5'CAGACTCTACGGGAGGCAGC3') and CD (5'CTTGTGCGGGCCCCGTCAATTC3').²² For the PCR, a 25 µL volume, containing
122 approximately 1 ng/µL of genomic DNA, 2.5 µL 2.5 mM of deoxynucleotide triphosphates (dNTP) (Promega), 1 µL of
123 complementary primer to the 3' and 5' ends of the 16S region to be amplified, 0.25 µL of Hot Start Q5 polymerase and 5 µL of
124 10X Q5 reaction buffer. PCR conditions were as follows: initial denaturing step of 1 min at 98 °C, 30 cycles of a denaturing step
125 of 30 sec at 98 °C, annealing step of 35 s at 53 °C, and an extension step of 35 s at 72 °C, followed by a final extension step of 72
126 °C for 3 min. The PCR products were subsequently purified using a Wizard SV Gel and PCR clean-up system (Promega). The
127 taxonomic identification of the sequences was then inferred using Basic Local Alignment Search Tool (BLAST) available from the
128 National Centre for Biotechnology Information (NCBI). ClustalW application within Bioedit software (Ibis Biosciences) was used
129 to align the sequences. NJ and Maximum Likelihood (ML) phylogenetic trees were constructed using Mega5 software.²³

130 **TEP analysis.** At the end of each incubation period, a membrane was removed and placed into 50 mL tubes containing 40
131 mL of 0.2 µm bonnet syringe Minisart filter (Sartorius Stedim, Dandenong, Australia) filtered seawater and stored at -20 °C until
132 analysis. Determination of TEP was carried out following previously published methods.²⁴⁻²⁵ A FLUOstar Omega (BMG Labtech)

133 was used to measure adsorption at 787 nm. TEP values of relative fluorescence were converted in μg equivalent of Xanthan gum
134 L^{-1} (see Supplementary Information Figure S2).

135

136 **TEP production by *Pseudomonas* sp. under static conditions**

137 **Static experimental setup.** *Pseudomonas* sp. was identified in the bacterial strains isolated during the static experiment
138 described previously. A *Pseudomonas* sp. culture was prepared in LB broth before being washed with tangential flow filtered
139 (TFF) RO feed tank water (see Supplementary Information for protocol) and inoculated in the dark into 3 replicates of TFF
140 filtered RO feed tank water (Nalgene carboy; 5 L) ($2.68 \times 10^6 \pm 3.45 \times 10^5 \text{ Cell.mL}^{-1}$). The controls for the experiment were (i)
141 another inoculation of 1000 mL of culture into a 5 L carboy containing TFF filtered RO feed tank water and incubated in the light
142 and (ii) a sterile control of a 5L carboy containing only TFF filtered RO feed tank water incubated in the dark.

143 **Growth monitoring of *Pseudomonas* sp..** Samples (1 mL) were collected daily in triplicates from each carboy and analyzed
144 via flow cytometry to monitor the growth of *Pseudomonas* sp..²⁶

145 **TEP analysis.** Samples (10 mL) were collected daily in triplicate from each carboy and analyzed for TEPs, following
146 previously described methods.²⁴⁻²⁵

147 **Nutrient analysis.** Daily samples (10 mL) for nutrient analysis were taken in triplicate from each carboy and filtered through
148 $0.45 \mu\text{m}$ bonnet syringe Minisart filters (Sartorius Stedim, Australia). Filtrates were then stored at $-20 \text{ }^\circ\text{C}$ until analysis. Analyses
149 of all chemical concentrations were measured simultaneously and carried out following published methods,²⁷ using a Lachat
150 Quickchem Flow Injection Analyser (FIA). Samples were thawed on ice and approximately 7 mL from each replicate were
151 injected in the FIA, in duplicate, for a total of 6 replicates per sample. The detection limits were 40 nM for dissolved silica
152 species, 70 nM for ammonia, 30 nM for orthophosphate and 70 nM for nitrate/nitrite; the method was calibrated using
153 standard solutions prepared in 0.6 M sodium chloride, corresponding to a seawater salinity of 35 practical salinity units (PSU).

154

155 **TEP production by *Pseudomonas* sp. under cross-flow conditions**

156 *Pseudomonas* sp. was used as an inoculum for an overnight culture grown in 250 mL of autoclaved raw seawater (15 min at 121
157 $^\circ\text{C}$). This overnight culture was diluted in 5 L of TFF filtered raw seawater to be used as the inoculum for the laboratory-based
158 cross-flow experiment.

159 **Laboratory-based cross-flow system.** A laboratory scale SWRO test unit comprising of six membrane cells (Sterlitech
160 CF042, Sterlitech), a high pressure pump (Hydra-Cell, Wanner Engineering), a feed water reservoir and a data acquisition system
161 (PC interfaced) was used to conduct the experiment (see Supplementary Information for cleaning protocol). The feed tank water
162 was circulated at a pressure of 500 psi and a flow of 1.5 L.min⁻¹. Flat sheets of polyamide TFC SWRO FILMTEC™ SW30HR (DOW,
163 California, USA) were used in the system.

164 **Biofouling protocol using a laboratory-based cross-flow system.** Six TFC SWRO membranes were incubated for 1 h in
165 100% isopropanol followed by sterilization in 80% isopropanol for 1 h before being washed with sterile Milli-Q water for 1 h.
166 Sterile TFC SWRO membranes were then placed in each of the 6 cells of the laboratory-based cross-flow system. *Pseudomonas*
167 sp. (5L) was added to TFF filtered raw seawater (35 L) in the reservoir tank of the laboratory-based cross-flow system to mimic
168 cell concentrations ($4.76 \times 10^6 \pm 1.44 \times 10^5$ Cell.mL⁻¹) observed in the natural environment. The bacteria were circulated within
169 the system at a pressure of 500 psi for 8 h at approximately 20 °C (kept at this temperature over the duration of the
170 experiment). Samples (10 mL) were taken daily for monitoring microbial communities, temperature, pH and salinity.

171 **TEP analysis.** Samples (10 mL) were collected from the reservoir tank of the laboratory-based cross-flow system hourly and
172 analyzed following previously described methods.²⁴⁻²⁵

173

174 **Statistical Analysis**

175 All environmental and bacterial abundance data were tested for normality using Shapiro-Wilks tests computed with the R
176 statistical package. However, due to the data not being of normal distribution, non-parametric tests were applied to determine
177 correlations (Spearman's rank correlation coefficient) and for the comparison for mean (Kruskal-Wallis / Wilcoxon rank sum
178 test).

179

180 **Results**

181 **Biofilm formation from RO feed tank water**

182 **Diversity of cultivable bacteria.** Biofilms formed on SWRO membranes submerged in RO feed tank water and incubated under
183 static conditions were analyzed for biofouling microorganisms. Phylogenetic analysis based on the 16S region from bacteria
184 isolated from the biofilm sample revealed that the majority of the isolated strains belonged to the α -Proteobacteria (39%), γ -
185 Proteobacteria (38%) and Actinobacteria (22%) classes. Moreover, 1% of the strains belonged to Flavobacteria (*Muricauda* sp.)
186 or to Bacilli (*Staphylococcus* sp.) lineages (see Supplementary Information Figure. S1). α -Proteobacteria included 13 strains,
187 which could not be identified at the genus level and *Celeribacter* sp. (9 strains) whereas *Alteromonas* spp., *Pseudoalteromonas*
188 sp., *Marinomonas* sp. and *Pseudomonas* sp. were the main genera found in the γ -Proteobacteria class. Finally, Actinobacteria
189 comprised of 8 genera including *Microbacterium* sp. and *Micrococcus* sp.

190

191 **Assessment of TEP production by the indigenous bacteria community and nutrient concentrations.** The concentration of TEP
192 present on the SWRO membranes was assessed over three static incubation periods (14, 21 and 56 days; Figure 1). The TEP
193 production significantly increased between the 14-day to 28-day incubations (Kruskal-Wallis, $p < 0.05$) (T_{14d} : 2.12 ± 0.10 Xg.mg.L⁻¹
194 and T_{28d} : 2.95 ± 1.69 Xg.mg.L⁻¹) and then remained consistent between the 28-days and 56-days incubation (T_{28d} : 2.95 ± 0.17
195 Xg.mg.L⁻¹ and T_{56d} : 2.63 ± 0.42 Xg.mg.L⁻¹).

196

197 **TEP production by *Pseudomonas* sp. under static conditions**

198 Exponential growth of *Pseudomonas* sp. was evident as well as daily variations in TEP production (Figure 2). An inverse
199 correlation was apparent between population growth and the production of TEP (population $\rho = -0.371$, $p < 0.05$). However,
200 nutrients were negatively correlated to TEP (phosphate $\rho = -0.466$, $p < 0.05$, nitrate $\rho = -0.364$, $p < 0.05$; Figure 3) suggesting that
201 the production of TEP is influenced by the nutrients that were available in solution.

202

203 TEP production by *Pseudomonas* sp. under cross-flow conditions

204 Laboratory-based cross-flow experiments are the closest mimicry of what happens to the water circulated within a desalination
205 plant system. Here, a mono-culture of *Pseudomonas* sp. isolated from RO feed tank water was circulated within a laboratory-
206 based cross-flow system at a pressure of 500 psi for 8 h at approximately 20 °C. A significant correlation between *Pseudomonas*
207 sp. and the TEP in the reservoir water of the laboratory-based cross-flow system was apparent ($\rho = -0.595$, $p < 0.05$) (Figure 4).
208 Here no variation was observed in nutrients.

209

210 Discussion

211 As a result of the recognition of biofouling as a leading cause of system inefficiency within SWRO desalination plants,
212 considerable efforts have been made to elucidate details about the mechanisms involved and the significance of TEP in
213 biofouling.^{5-6,13,28-31} Here, biofilms were formed on SWRO membranes using RO feed tank water and showed that the prevailing
214 cultivable phylum was Proteobacteria (>70%) and that the α -Proteobacteria class dominated the samples (see Supplementary
215 Information Figure S1). These results are in agreement with Ayache *et al.*,³² Zhang *et al.*,³³ and Chen *et al.*,³⁴ although the ratio
216 of α - and γ -Proteobacteria varied between the studies. It has been suggested that the α -Proteobacteria class are present in
217 larger quantities in mature biofilms and replace β -Proteobacteria, which are generally thought to be instrumental in initial
218 biofilm development.³⁵

219 TEPs also play an important role in biofilm formation within aquatic environments,^{13-14,17} facilitating and accelerating biofilm
220 development.^{13,36} In particular, TEPs have a role in the conditioning of surfaces by creating a more favourable environment for
221 the attachment of planktonic cells and the proceeding biofilm that is developed.^{14,17,37} It has been suggested that TEP
222 precursors, through the formation of a conditioning film, could reduce the diffusion of ions (Na^+ , Ca^{2+} , Mg^{2+} , Cl^- , SO_4^{2-}) and
223 organics from the membrane surface to the bulk flow, enhancing the concentration polarization on the membrane surface³⁶.

224 Here, the concentration of TEPs produced by the biofilm suggests that production reflects the growth stages of the biofilm from
225 the initial adherence of bacteria to the membrane, resulting in low levels of TEPs which increase over time as the biofilm
226 expands. This increase in TEP production, due to an increase in the abundance of bacteria, has been seen *in situ*^{38,39} as well as
227 under laboratory conditions³⁶. While these studies were conducted on planktonic bacteria the assumption could still stand as a
228 reduction in organic matter results in the increased production of TEPs.³⁹

229 Here, the volume of TEPs generated by *Pseudomonas* sp. under static conditions was of the same order of magnitude of
230 that presented by Sheng *et al.*³⁶ for static experiments on *Pseudoalteromonas atlantica*. However, the volume of TEPs generated

231 by *Pseudomonas* sp. during the laboratory-based cross-flow experiment was 10 fold higher to that produced during the static
232 experiment for the same time period, while both experiments were inoculated with cell concentrations of the same order of
233 magnitude. Our study corroborates findings by Passow⁴⁰ who showed that indigenous bacteria under shear conditions produced
234 a significant amount of TEPs in comparison to that produced under static conditions. In particular, they showed that shear and
235 turbulent conditions impacted on the TEP production. Others have shown that shear can impact the structure and
236 polysaccharides composition of biofilms^{41,42}. While bacteria are known to generate large amounts of polysaccharide, through
237 the renewal of capsules and films as well as free exopolymers,⁴⁰ an increase in TEP production in such a short period of time (8
238 hours) could be due to the shear conditions resulting in abiotic formation of TEP particles as opposed to spontaneously.⁴⁰ As
239 shear conditions have been found to enhance the growth rate of bacteria⁴⁰, an increase in shear could also possibly result in an
240 higher production of polysaccharides which form into TEP particles.

241 Microorganisms are constantly subject to the environment and their ability to sense and respond accordingly is therefore
242 essential to their survival.⁴³ In response to nutrient starvation, or limitation, bacteria adapt to the environment through a
243 number of different activities, and in an attempt to maintain viability they may adopt a more resistant state.⁴³⁻⁴⁵ Prior to
244 nutrient starvation bacteria are well dispersed; however, it has been observed that during nutrient limited conditions there is
245 increased adhesion and surface hydrophobicity.⁴⁵⁻⁴⁷ In addition, limitation of nutrients such as carbon, nitrogen and
246 phosphorous within aquatic ecosystems has been found to affect not only bacterial growth and EPS production but also
247 biomass.⁴⁷⁻⁴⁹ Moreover, phosphate deprivation can result in the production of larger quantities of EPS in comparison to
248 eutrophic environments.⁵⁰⁻⁵³ The production of large amounts of EPS has thus been suggested as a survival mechanism with the
249 matrix being an effective strategy to trap nutrients from the surrounding environment.⁵⁴ Under continuing starvation conditions
250 Myszka and Czaczyk⁵² found that *P. aeruginosa* had a high level of EPS output and produced the highest amount of EPS after an
251 incubation period of 120 h.

252

253 **Conclusion**

254 This study demonstrates the importance of TEP production by microorganisms in the biofouling process within desalination
255 plants. Our results indicate that in a planktonic state within the natural environment the production of TEP is relatively
256 controlled, in particular by the availability of nutrients, however, within the desalination system microbial composition and

257 turbulence determine the generation of TEP. Therefore, both direct and indirect approaches need to be undertaken in order to
258 reduce the biofouling capacity of the microorganisms present within the RO feed tank and make the system more economical.

259

260 Acknowledgements

261 The authors acknowledge the financial support of the National Centre of Excellence in Desalination Australia, which is funded by
262 the Australian Government through the National Urban Water and Desalination Plan. The authors are also grateful to T. Kirby, T.
263 Kildea, N. Nedelkov and G. Ralston for their assistance in sampling from the Penneshaw desalination plant and to C. Le Lan for
264 assistance with measuring TEP concentration.

265

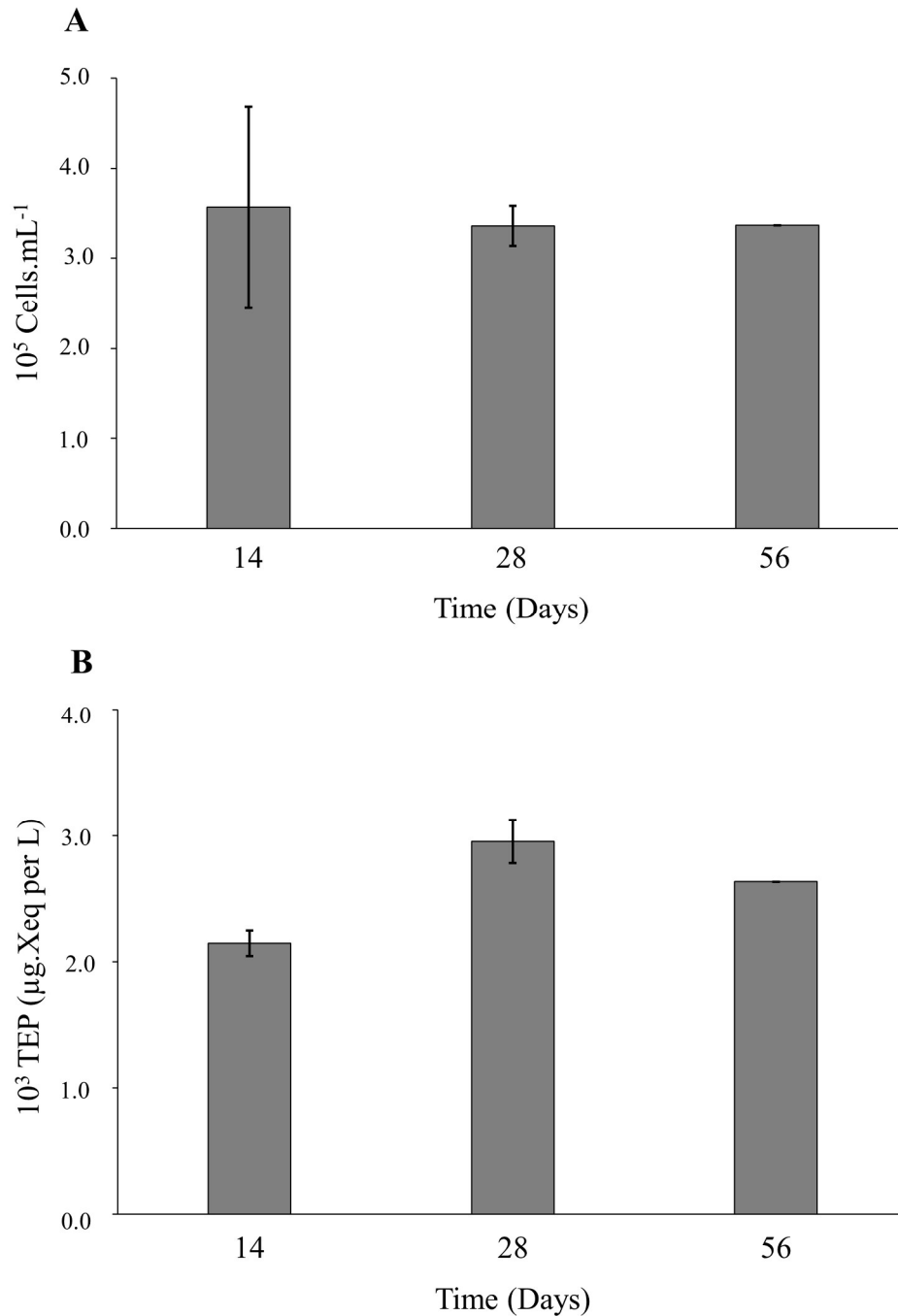
266

267 References

- 268 1. L. F. Greenlee, D. F. Lawler, B. D. Freeman, B. Marrot, and P. Moulin, *Water Res.*, 2009, **43**, 2317-2348.
- 269 2. T. Harif, H. Elifantz, E. Margalit, M. Herzberg, T. Lichi, and D. Minz, *Desalination Water Treat.*, 2011, **31**, 151-163.
- 270 3. A. Matin, Z. Khan, S. M. J. Zaidi, and M. C. Boyce, *Desalination*, 2011, **281**, 1-16.
- 271 4. R. Komlenic, *Filtr. Separat.*, 2010, **47**, 26-28.
- 272 5. J. Lee, and I. S. Kim, *Desalination*, 2011, **273**, 118-126.
- 273 6. L. Katebian, and S. C. Jiang, *J. Memb. Sci.*, 2013, **425**, 182-189.
- 274 7. R. A. Al-Juboori, T. Yusaf, and V. Aravinthan, *Desalination*, 2012, **286**, 349-357.
- 275 8. B. R. Borlee, A. D. Goldman, K. Murakami, R. Samudrala, D. J. Wozniak, and M. R. Parsek, *Mol. Microbiol.*, 2010, **75**, 827-
276 842.
- 277 9. C. L. D. Manes, N. West, S. Rapenne, and P. Lebaron, *Biofouling*, 2011, **27**, 47-58.
- 278 10. R. M. Donlan, and J. W. Costerton, *Clin. Microbiol. Rev.*, 2002, **15**, 167-193.
- 279 11. E. Bar-Zeev, I. Berman-Frank, O. Girshevitz, and T. Berman, *PNAS*, 2012, **109**, 9119-9124.
- 280 12. E. Bar-Zeev, I. Berman-Frank, B. Liberman, E. Rahav, U. Passow, and T. Berman, *Desalination Water. Treat.*, 2009, **3**, 136-
281 142.
- 282 13. R. V. Linares, V. Yangali-Quintanilla, Z. Y. Li, and G. Amy, *J. Memb. Sci.*, 2012, **421**, 217-224.
- 283 14. U. Passow, *Prog. Oceanogr.*, 2002, **55**, 287-333.

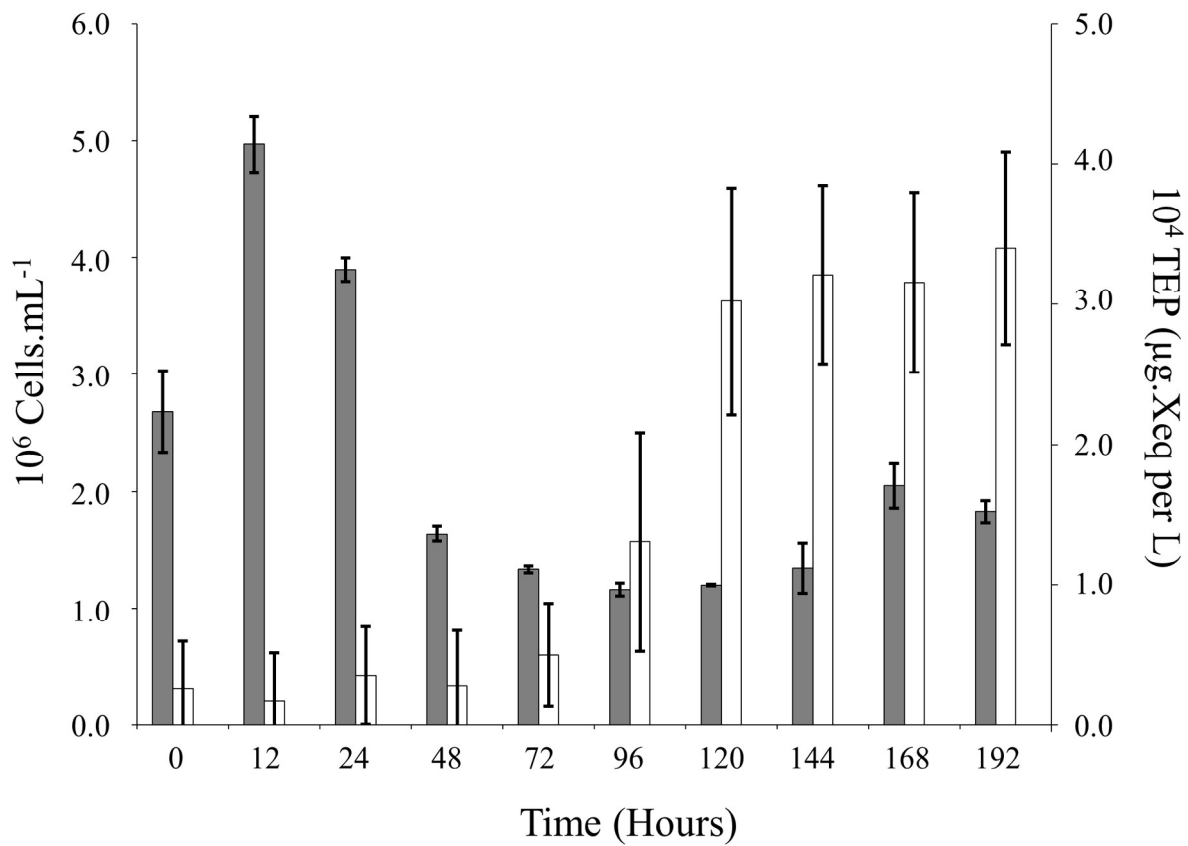
- 284 15. T. Berman, R. Mizrahi, and C. G. Dosoretz, *Desalination*, 2011, **276**, 184-190.
- 285 16. U. Passow, and A. L. Alldredge, *Mar. Ecol. Prog. Ser.*, 1994, **113**, 185-198.
- 286 17. M. Simon, H. P. Grossart, B. Schweitzer, and H. Ploug, *Aquat. Microb. Ecol.*, 2002, **28**, 175-211.
- 287 18. K. E. Stoderegger, and G. J. Herndl, *Limnol. Oceanogr.*, 1998, **43**, 877-884.
- 288 19. K. E. Stoderegger, and G. J. Herndl, *Mar. Ecol. Prog. Ser.*, 1999, **189**, 9-16.
- 289 20. C. Pelekani, S.A. Jewell, and G. Kilmore, *IDA World Congress-Maspalomas, Gran Canaria, Spain*, 2007.
- 290 21. M.B. Dixon, T. Qiu, M. Blaikie, and C. Pelekani, *Desalination*, 2012, **284**, 245-252.
- 291 22. K. Rudi, O. M. Skulberg, F. Larsen, and K. S. Jakobsen, *Appl. Environ. Microbiol.*, 1997, **63**, 2593-2599.
- 292 23. K. Tamura, D. Peterson, N. Peterson, G. Stecher, M. Nei, and S. Kumar, *Molecul. Biol. Evol.*, 2011, **28**, 2731-2739.
- 293 24. U. Passow, and A. L. Alldredge, *Limnol. Oceanogr.*, 1995, **40**, 1326-1335.
- 294 25. P. Claquin, I. Probert, S. Lefebvre, and B. Veron, *Aquat. Microb. Ecol.*, 2008, **51**, 1-11.
- 295 26. D. Marie, F. Partensky, D. Vaultot, and C. Brussaard, *Curr. Protoc. Cytom.*, 2007, **11**, 1-14.
- 296 27. H. P. Hansen, and F. Koroleff, *Determination of nutrients, in methods of seawater analysis*, Wiley, Weinheim, Germany,
297 2007.
- 298 28. M. Krivorot, A. Kushmaro, Y. Oren, and J. Gilron, *J. Memb. Sci.*, 2011, **376**, 15-24.
- 299 29. R. A. Al-Juboori, and T. Yusaf, *Desalination*, 2012, **302**, 1-23.
- 300 30. T. Nguyen, F. A. Roddick, and L. Fan, *Membranes*, 2012, **2**, 804-840.
- 301 31. S. Huang, N. Voutchkov, and S. C. Jiang, *Desalination*, 2013, **319**, 1-9.
- 302 32. C. Ayache, C. Manes, M. Pidou, J. P. Croue, and W. Gernjak, *Water Res.*, 2013, **47**, 3291-3299.
- 303 33. M. L. Zhang, S. Jiang, D. Tanuwidjaja, N. Voutchkov, E. M. V. Hoek, and B. L. Cia, *Appl. Environ. Microbiol.*, 2011, **77**, 4390-
304 4398.
- 305 34. C. L. Chen, W. T. Liu, M. L. Chong, M. T. Wong, S. L. Ong, H. Seah, and W. J. Ng, *Appl. Microbiol. Biotechnol.*, 2004, **63**, 466-
306 473.
- 307 35. L. A. Bereschenko, H. Prummel, G. J. W. Euverink, A. J. M. Stams, and M. C. M. van Loosdrecht, *Water Res.*, 2011, **45**, 405-
308 416.
- 309 36. S. Li, H. Winters, S. Jeaong, A-H. Emwas, S. Vigneswaran, and G.L. Amy, *Desalination*, 2016, **379**, 68-74.
- 310 37. T. Berman, and M. Hohenberg, *Filtration Sep.*, 2005, **42**, 30-32.
- 311 38. I. De Vicente, E. Ortega-Retuerta, I. P. Mazuecos, M. L. Pace, J. J. Cole and I. Reche, *Aquat. Sci.*, 2010, **72**, 443-453.
- 312 39. E. Ortega-Retuerta, C. M. Duarte, and I. Reche, *Microb. Ecol.*, 2010, **59**, 808-818.

- 313 40. U. Passow, *Mar. Ecol. Prog. Ser.*, 2002, **236**, 1-12.
- 314 41. P. Stoodley, I. Dodds, J.D. Boyle, and H.M. Lappin-Scott, *J. Appl. Microbiol.*, 1999, **85**, 19–28.
- 315 42. P. Stoodley, R. Cargo, C.J. Rupp, S. Wilson, and L. Klapper, *Ind. Microbiol. Biotechnol.*, 2002, **29**, 361-367.
- 316 43. S. N. Wai, Y. Mizunoe, and S. Yoshida, *FEMS Microbiol. Lett.*, 1999, **180**, 123-131.
- 317 44. A. S. Seshasayee, P. Bertone, G. M. Fraser, and N. M. Luscombe, *Curr. Opin. Microbiol.*, 2006, **9**, 511-519.
- 318 45. S. Kjelleberg, and M. Hermansson, *Appl. Environ. Microbiol.*, 1984, **48**, 497-503.
- 319 46. S. L. Sanin, S. D. Sanin, and J. D. Bryers, *Prog. Biochem.*, 2003, **38**, 909-914.
- 320 47. V. F. Farjalla, F. A. Esteves, R. L. Bozelli, and F. Roland, *Hydrobiologia*, 2002, **489**, 197-205.
- 321 48. W. Graneli, S. Bertilsson, and A. Philibert, *Aquat. Sci.*, 2004, **66**, 430-439.
- 322 49. M. Jansson, A. K. Bergstrom, D. Lymer, K. Vrede, and J. Karlsson, *Microb. Ecol.*, 2006, **52**, 358-364.
- 323 50. I. W. Sutherland, In *Microbial Extracellular Polymeric Substances*, ed. J. Wingender, T. R. Neu, and H. C. Flemming, Springer-
324 Verlag, Berlin, first edition, 1999, 4, 73-89.
- 325 51. P. J. Looijesteijn, W. H. M. van Casteren, R. Tuinier, C. H. L. Doeswijk-Voragen, and J. Hugenholtz, *J. App. Microbiol.*, 2000,
326 **89**, 116-122.
- 327 52. K. Myszka, and K. Czaczyk, *Curr. Microbiol.*, 2009, **58**, 541-546.
- 328 53. C. M. Kim, S. J. Kim, L. H. Kim, M. S. Shin, H. W. Yu, and I. S. Kim, *Desalination*, 2014, **349**, 51-59.
- 329 54. W. M. Dunne, *Clin. Microbiol. Rev.*, 2002, **15**, 155-166.



330

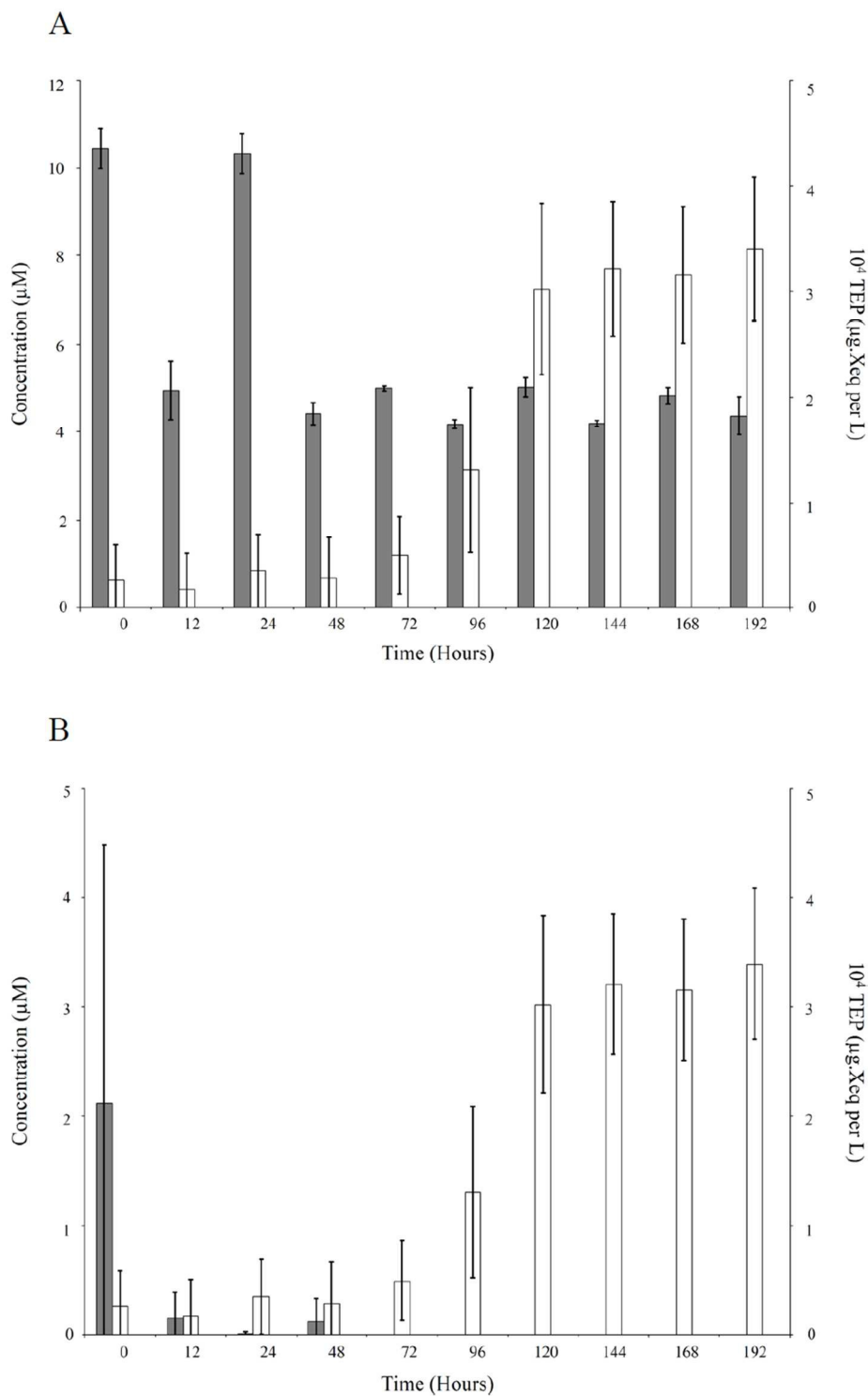
331 Figure 1: (A) Average indigenous bacterial abundance determined by flow cytometry during
332 incubation periods 14, 28 and 56 days under static conditions and (B) TEP concentrations
333 measured from the biofilms formed on the RO membranes after incubation periods of 14, 28
334 and 56 days under static conditions.



335

336 Figure 2: Fluctuations in *Pseudomonas* sp. population (black) and TEP production (white)

337 overtime during static conditions.

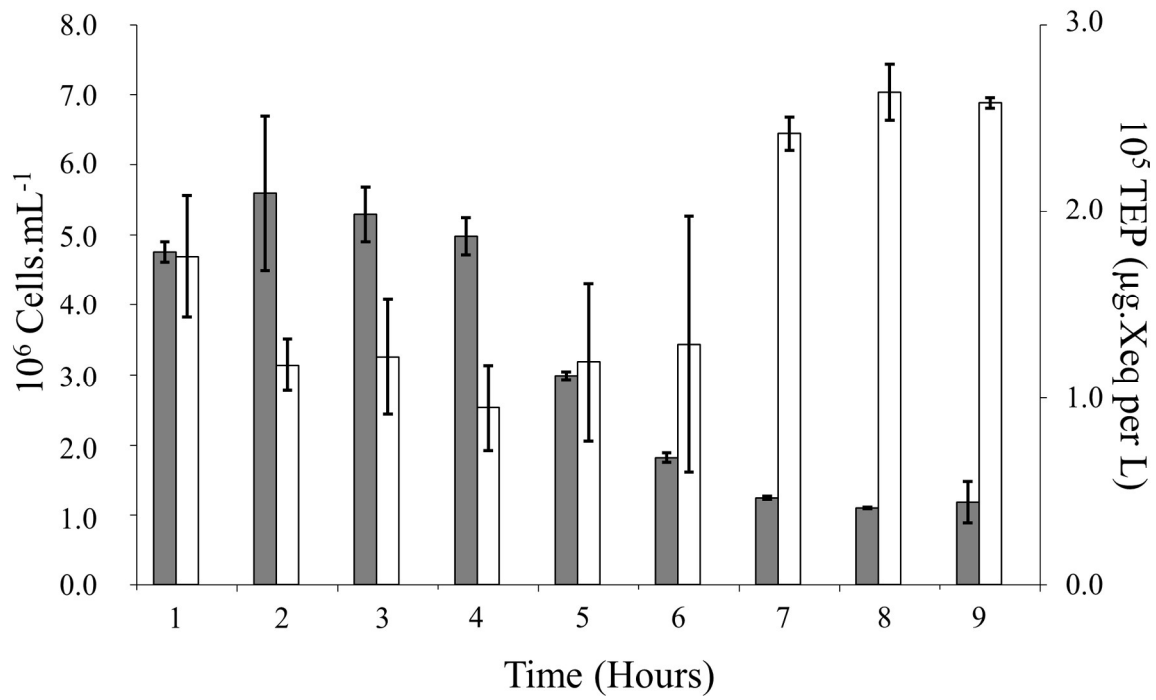


338

339 Figure 3: (A) Fluctuations in phosphate (black) and TEP production (white) overtime during

340 static conditions and (B) Fluctuations in nitrogen (black) and TEP production (white) overtime

341 during static conditions.



342

343 Figure 4: Fluctuations in *Pseudomonas* sp. population (black) and TEP production (white)

344 overtime during the laboratory-based cross-flow experiments.

345

346