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Liquid marbles as a micro-reactor for efficient radical alternating copolymerization of diene monomer and oxygen

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Liquid marbles have been shown to be a novel micro-reactor to synthesize polyperoxides by the radical alternating copolymerization of the 1,3-diene monomer with oxygen in a good yield. Oxygen gas is effectively absorbed as a comonomer by the large and permeable gas-liquid interface of the liquid marbles.

Alternating copolymerization is a practical and efficient method to use non-homopolymerizable compounds as a comonomer. Epoxy derivatives and olefins including dienes undergo an alternating copolymerization with gases such as carbon dioxide,¹ carbon monoxide,² oxygen,^{3,4} and sulfur dioxide.⁵ The resulting alternating copolymers are intriguing materials not only from the view point of using non-petroleum resources and the consumption of greenhouse gases, but also from the view point of the formation of main-chain functional polymers by chain polymerization. For instance, the alternating copolymers from oxygen and olefins, so-called polyperoxides, contain peroxy linkages as the main-chain repeating unit and undergo radical chain degradation by various stimuli including heat, UV irradiation, and redox reactions with amines. The functional polyperoxides with well-defined structures, such as the cross-linked polymers,⁶⁻⁸ the graft polymers,⁹ and the block copolymers,¹⁰ were successfully synthesized for application as functional materials, e.g., dismantlable (de-bondable) adhesives^{10, 11} biocompatible polymers,^{12, 13} thermoresponsive polymers,^{14, 15} and surface modifier.^{10, 16} In the case of diene monomers, an interesting regiospecificity was also reported, i.e., 2,4-hexadienoates (sorbic esters) undergo a regiospecific 5,4-addition to yield alternating copolymers (polyperoxides) in the presence of excess oxygen and only 5,2-addition to yield non-degradable homopolymers in the absence of oxygen.¹⁷⁻²⁰ In order to exclusively synthesize polyperoxides from the homopolymerizable diene monomers, a polymerization was performed with oxygen bubbling and vigorous stirring, which are energy consuming processes. An increase in the oxygen-liquid interfacial area is supposed to be an effective and smart solution for the efficient synthesis of polyperoxides.

It is well known that a liquid droplet with high surface energy can be stabilized by solid particles with a low surface energy adsorbed on the gas-liquid interface, and the resulting core-shell type particles are called liquid marbles.²¹⁻²⁶ Recently, liquid marbles 1 attracted significant attention in view of their potential applications in cosmetics,^{27, 28} transport & microfluidics,^{29, 30} miniature reactors.^{31, 32} personal & health care products,³³ sensors,³⁴⁻³⁸ accelerometers, and gas storage.⁴⁰ The liquid marbles possess a large specif. interfacial area, which leads to easy contact of the liquid droplet to external gases and thus the liquid marbles have been used for g sensing. heterogeneous hydrogenation reactions,⁴ and the interfacial polymerization of a gaseous monomer using an exterliquid as a catalyst.⁴² In this study, we described the use of a liquir⁴ marble as a novel micro-reactor for the effective synthesis (f polyperoxides (Fig. 1(a)). To the best of our knowledge, this is the first demonstration of a polymerization in the liquid marbles. The polymerization in the liquid marbles is expected to genera. polyperoxides in a good yield with neither stirring the liquid nor oxygen bubbling during the reaction, and has the potential to save manufacturing energy.

To fabricate the liquid marbles, 2-hydroxyethyl sorbate (HES) ar lycopodium (Fig. 1(b)) were used as a hydrophilic liquid and hydrophobic solid particle, respectively. As shown in Fig. 1(c), the



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Electronic Supplementary Information (ESI) available: experimental details, ¹H NMR, time-conversion plot, GPC data, and reaction scheme. See DOI: 10.1039/x0xx00000x



Fig. 2. ¹H NMR spectrum of the products obtained by radical alternating copolymerization in a liquid marble at 40 °C for 48 h measured in acetone- d_6 .

stable and near-spherical liquid marble with a diameter of a few mm was formed by just rolling the 15- μ L HES droplet on the lycopodium powder. A stable liquid marble was also formed on lycopodium using the HES droplet containing up to 1.1 wt% 2,2'-azobis(4-methoxy-2,4-dimethylvaleronitrile) (AMVN) as a radical initiator, and later studies were carried out using the HES containing 1.1 wt% AMVN.

The polymerization of HES in the liquid marbles was carried out under atmospheric oxygen in a sealed vessel at 40 °C (Fig. S1, ESI). As shown in Fig. 1(d), the shape of the liquid marbles was maintained after the polymerization for 48 h. The ¹H NMR spectrum of the products after the 48-h polymerization is shown in Fig. 2. The characteristic peaks assignable to the polyperoxide of HES (PP-HES), the homopolymer of HES (PHES), unreacted HES, and a trace amount of fumaraldehyde 2-hydroxyethyl ester (FA-2HE) as one of the degradation products of PP-HES,⁸ were detected (Fig. S2, ESI). Acetaldehyde (boiling point = 21 °C) as the other degradation product of PP-HES was not detected due to its evaporation during the polymerization.⁸ The consumption ratio of HES and the conversion to PP-HES and PHES are plotted versus the polymerization time in Fig. 3. PP-HES was the main product for any polymerization time and the conversion to PP-HES reached ca. 50 % after the 48-h polymerization. The conversion to FA-2HE was less than 5% throughout the polymerization showing that the degradation of PP-HES is a minor reaction (Fig. S3, ESI). In contrast, when the polymerization in the liquid marbles was carried out under an argon atmosphere instead of oxygen for 48 h, PP-HES was not formed and only PHES was generated with a 23.3 % conversion (Table 1). These results clearly show that the monomer



Fig. 3. Consumption ratio of HES (•) and conversion vs time plots for radical polymerization of HES and O_2 in a liquid marble (1 μ L) at 40 °C: Conversions to PP-HES (•) and PHES (▲).

within the liquid marbles absorbed the external gas during polymerization. Interestingly, the consumption ratio of HES under the oxygen atmosphere was 72.6 % and much higher than that in argon atmosphere, i.e., 23.3%. It is expected that under the oxygen atmosphere, the polymerization was not only initiated by the primary radical from AMVN but also by the oxygen-centered radical from PP-HES (Scheme S1, ESI). This consideration is substantiated b, the fact that the decomposition product of PP-HES, i.e., FA-2HF was detected by the ¹H NMR. The result that the consumption ratio of HES continuously increased even after 5 half-life times of AMVN (= ca. 15 h, calculated by the decomposition rate constant of AM , at 40 °C = 6.6×10^{-5} s⁻¹; k_d [s⁻¹] = 1.36×10^{16} exp(-117 [kJ/mol]/RT)⁴³ is also explained by the initiation from PP-HES (Fi. 3).

The GPC curves of the products obtained under an oxyge atmosphere were bimodal and the relative intensities of the peaks 1. the higher molecular weight region increased with the increasing polymerization time (Fig. 4). PHES obtained under the argo atmosphere resulted in a unimodal GPC curve and the M_n value was 1.64×10^4 with the peak top at log M = 4.3 (Fig. S4, ESI). It is the expected that in Fig. 4, the peaks above $\log M = 4.0$ come from PHES, and the main peaks with the peak tops at around $\log M = 3.5$ correspond to PP-HES. The molecular weights of PP-HES are an the order of 10³ and are similar to those for PP-HES obtained by the solution polymerization of HES with oxygen bubbling and stirring, and the polyperoxides from other olefins under different conditions.^{17, 20, 44} During the copolymerization of olefins including the 1,3-diene monomer with oxygen, frequent chain transfer of the oxygen-centered radical as one of the propagating radicals results the formation of polyperoxides with a relatively low molecular weight. The same phenomenon is expected for the polymerization the liquid marble. The shift in the main peak to the lower molecul. weight region with the increasing polymerization time is attribute to the moderate decomposition of PP-HES during the polymerization PP-HES obtained in the liquid marble underwent therm 1 degradation by heating at 100 °C in the same manner as the the polyperoxides obtained by conventional solution polymerization.¹⁸

reactor	interfacial area (mm ² /mL)	atmosphere	polymerization time (h)	consumption ratio of HES $(\%)^b$	Conversion $(\%)^b$			
reactor					PP-HES	PHES	FA-2HE	
liquid marble	2000	O ₂	48	72.6	47.7	19.6	5.2	7 1
liquid marble	2000	Ar	48	23.3	0	23.3	0	Y
glass tube	13	O ₂	6	7.4	1.5	5.8	0.12	
glass tube	13	$\overline{O_2}$	48	20.5	1.8	18.6	0.15	

^aHES with 1.1 wt% AMVN was polymerized at 40 °C. ^bDetermined by ¹H NMR.

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Fig. 4. GPC curves of the reaction mixture obtained by the copolymerization of HES and O_2 in the liquid marble at 40 °C for 6 (...), 36 (...), and 72 h (---).

The effect of the specific interfacial areas on the conversion to PP-HES was investigated by employing the liquid marbles formed by 3, 5, and 15 µL of the HES with AMVN (specific interfacial area = 1600, 2000, and 2800 mm²/mL, respectively, assuming a sphere) (Fig. 5). As the control experiments, the polymerization was also carried out in glass tubes with different diameters, i.e., 4, 10, and 15 mm, using the 1-mL HES with AMVN (gas-monomer interfacial area = 13, 79, and 180 mm²/mL, respectively). In the liquid marbles, PP-HES was the main product regardless to the specific interfacial areas and the conversion to PP-HES increased with the increasing specific interfacial areas, whereas the conversion to PHES was almost constant. In stark contrast, in the glass tubes, PHES was the main product, although the conversion to PP-HES increased with an increase in the gas-monomer interfacial areas. To obtain PP-HES as the main product at the same level as in the liquid marbles, a glass tube having a diameter greater than at least 45 mm is required to polymerize 1 mL of HES based on the calculation of the gasmonomer interfacial area. Considering the surface tension and viscosity of the monomers, it appears difficult to spread the monomers all over the wide glass tube, and the liquid marbles are an excellent micro-reactor to achieve a significantly large specific interfacial area.

In order to obtain information about the diffusion of oxygen within the liquid marbles, the conversion to PP-HES in each section of the liquid marble, i.e., the surface layer, center part, and complete liquid marble, were separately investigated. The polymerized liquid marble (15 μ L) at 40 °C for 48 h was dipped in deuterated acetone for 10 s to dissolve the surface layer. The other polymerized liquid



Fig. 5. Consumption ratio of HES (•) and conversion vs gasliquid interfacial area plots for radical copolymerization of HES and O_2 in the glass tubes (diameter = 4, 10, and 15 mm, interfacial area < 200 mm²/mL) and in the liquid marbles (volume = 3, 5, and 15 μ L, interfacial area > 1500 mm²/mL) under oxygen atmosphere at 40 °C for 48 h: Conversion to PP-HES (□) and PHES (▲).

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Table 2. Conversion dependence on the sections in the liquid marble $(15 \text{ uL})^a$.

1	consumption ratio of HES	Con			
location	$(\%)^{b}$	PP-HES	PHES	FA-2H'E	-
surface ^c	81.7	67.3	0	14.4	
center ^d	67.9	41.1	21.7	5.1	
complete	71.4	46.1	18.7	6.5	
^a HES with	h 1 1 wt% AMVN was poly	merized a	at 40 °C	for 48 h	

^bDetermined by ¹H NMR. ^cA liquid marble was dipped in acetone- d_6 for 10 s. ^dA frozen liquid marble was cleaved and the center part was collected by a pick.

marble (15 µL) was frozen by liquid nitrogen and cleaved in half and the products at the center was collected. The results of the $\frac{1}{1}$ NMR analysis are summarized in Table 2. On the surface layer, the conversion to PP-HES reached 67.3% without the formation PHES. Whereas, at the center, the conversion to PP-HES (= 41.19) was much lower than that obtained on the surface layer and significant amount of PHES (= 21.7%) was formed. These results indicated that most of the oxygen absorbed from the gas-liquid interface was consumed in the surface layer because the addition carbon-centered radicals to oxygen is much faster than that to the 1,3-diene monomer, i.e., HES.¹⁸ This consideration is supported by the results obtained in the glass tube with the diameter of 4 mm (ga monomer interfacial area = $13 \text{ mm}^2/\text{mL}$) at different polymerization. times (Table 1). The conversion to PP-HES after 6-h and 48-1 polymerizations was almost the same, i.e., 1.5 and 1.89 respectively, whereas the conversion to PHES increased from 5.8 to 18.6% with the increasing polymerization time from 6 to 48 These results showed that PP-HES was formed during the early stag of the polymerization using the initially adsorbed oxygen, an¹ thereafter, only the homopolymerization of HES proceeded under limited oxygen. Although PP-HES is rubbery due to its low gla s transition temperature (= -4.2 °C), the oxygen permeability of PH HES is expected to be lower than that for liquid HES, $^{45, 46}$ and th may be one of the reasons for the suppression of oxygen diffusion the center part.

In summary, it was demonstrated that the liquid marbles can work as an efficient and convenient micro-reactor to synthesize polyperoxides by absorbing external oxygen as a comonomer through the large and permeable gas-liquid interface. We copolymerization in the liquid marbles resulted in polyperoxides in good yield without oxygen bubbling and stirring, and the technique has the potential to reduce manufacturing energy. The method described here is simple and applicable to the other alternating copolymerization systems with gases^{1, 2, 5} and the polymer reaction with gases such as the reversible trap-release system of carbo dioxide.^{47, 48} Polyperoxide derivatives are known as degradable functional materials and the application of the polymerized liqu. I marbles containing polyperoxide to functional adhesives a currently under investigation.

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