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Selective electrochemical reduction of $CO₂$ to CO with **a cobalt chlorin complex adsorbed on multi-walled carbon nanotubes in water†**

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Electrocatalytic reduction of CO₂ occurred efficiently **using a glassy carbon electrode modified with a cobalt(II) chlorin complex adsorbed on multi-walled carbon nanotubes at an applied potential of –1.1 V** *vs***. NHE to yield CO with a Faradaic efficiency of 89% with hydrogen production accounting for the remaining 11% at pH 4.6.**

Electrocatalytic two-electron reduction of $CO₂$ to CO has merited significant interest, because CO can be converted to liquid hydrocarbon fuels with H_2 by Fischer-Tropsch processes.1-3 There have been extensive studies on electrocatalytic reduction of $CO₂$ with cobalt and nickel macrocycles.⁴⁻⁶ The selective electrocatalytic reduction of $CO₂$ to CO has been achieved using nickel macrocycles in water without formation of H_2 .⁷⁻⁹ Cobalt macrocycles can also act as good electrocatalysts for selective $CO₂$ reduction to CO in organic solvents.10-13 In water, however, cobalt macrocycles have lacked selectivity for $CO₁₃₋₁₅$ because cobalt complexes act as good catalysts for H_2 evolution.¹⁶⁻²¹

We report herein selective electrocatalytic reduction of $CO₂$ to CO using a glassy carbon electrode modified with a cobalt(II) chlorin complex $(Co^{II}(Ch))$: a chemical structure shown in Scheme 1) adsorbed on carbon nanotubes in water.

The $Co^H(Ch)$ -modified electrode was prepared by drop casting a sonicated acetonitirile (MeCN) solution containing $Co^H(Ch)$ (1.0 mM), multi-walled carbon nanotubes (MWCNTs: 1.3 mg) as a support material and 5% Nafion (12 µL) as a proton exchange membrane and stabilization agent of $CO^H(Ch)$ on MWCNTs to an glassy carbon electrode (Experimental details are shown in the electronic supplementary information (ESI)). Similarly the $Co^H(OEP)$ -modified electrode ($OEP²⁻$) octaethylporhyrin dianion) was prepared by sonication in an MeCN solution containing $Co^H(OEP)$ (1.0 mM), MWCNT and Nafion. The $Co^H(Ch)$ -modified electrode exhibited a catalytic current at an applied potential at ≤ -1.0 V *vs*. NHE in a CO₂-

Fig. 1 Cyclic voltammograms (CV) of (a) a $Co^H(Ch)$ -modified and (b) a $Co^H(OEP)$ -modifi electrode in CO₂- and N₂-saturated aqueous solutions containing Na₂SO₄ (5.0 mM, pH²) 4.6). Sweep rate: 10 mV s⁻¹; a working electrodes were modified Co complexes (0.01 umol) and MWCNTs (13 ug) on a glassy carbon disk electrode.

saturated aqueous solution at pH 4.6 as shown in Fig. 1 (red line). When $Co^H(Ch)$ was replaced by $Co^H(OEP)$ under otherwise the same experimental conditions, decrease of the catalytic current from 60 µA (red line) to 30 µA (green line) at –1.1 V *vs*. NHE was observed as shown in Fig. 1.

To assess the catalytic activity of $Co^H(Ch)$, controlledpotential electrolysis of a $CO₂$ -saturated aqueous solution with Na₂SO₄ (5.0 mM) as an electrolyte was performed and formation of CO and H_2 was quantitated by the gas chromatography analyses. No formation of the reduced products such as formaldehyde, methane, methanol and oxalate was observed in the present experimental conditions, however small amount of formic acid was detected by the formate dehydrogenase assay (Fig. S1 in the electronic supplementary information (ESI) †). We examined various experimental conditions such as pH of a $CO₂$ -saturated aqueous solution, an applied potential and various amount of $Co^H(Ch)$ adsorbed on MWCNTs in a sonicated MeCN solution as summarized in Table 1. The time courses of formation of CO and H_2 in electrolysis of a CO_2 -saturated aqueous solution with Na_2SO_4 at various pH were shown in Fig S2 in ESI \dagger . The maximum turnover number (TON) was 1200 with a TOF of 100 h^{-1} at pH 4.6. When the pH value is smaller than 4.6, proton reduction to evolve H_2 occurred preferentially rather than CO_2 reduction. The reason why small TON at pH 6.8 is slow proton-coupled electron-transfer reduction of $CO₂$ to CO in the high pH

Table 1 pH dependence of CO production and selectivities in electrocatalytic reduction in a $CO₂$ -saturated aqueous solution on the $Co^H(Ch)$ -modified electrode at -1.1 V *vs*. NHE.

pH	TON ^a	TOF a (h ⁻¹)	CO:H ₂
2.0	140	87	1:32
2.8	350	87	11:17
3.6	540	100	4.2:1
4.6	1100	140	4.3:1
6.8	240	79	4.9:1
^a Experimental errors are within 5%			

Experimental errors are within 5%.

Fig. 2 Time courses of evolution of CO and H_2 in the electrocatalytic reduction of CO₂ on the glassy carbon electrode modified with Co^{II}(Ch) (0.01 µmol) adsorbed on MWCNTs (13 µg) in a CO₂-saturated aqueous solution containing Na_2SO_4 (5.0) mM) at an applied potential of -1.1 V vs. NHE. CO₂ was bubbled every 2 h.

Fig. 3 EPR spectra of (a) $Co^H(Ch)$ (1.0 mM) in deaerated MeCN measured at 4.2 K and (b) $Co^{\prime\prime}$ (Ch) (1.0 mM) adsorbed on MWCNTs (0.30 mg) and Nafion (3.0 μ L) in deaerated MeCN (250 µL) measured at 4.2 K.

conditions. The largest CO formation was observed when ϵ applied potential was -1.1 V *vs*. NHE and concentration ϵ f $Co^H(Ch)$ was 1.0 mM (Figs. S3-S4 in ESI \dagger). Fig. 2 shows the time courses of formation of CO and H_2 in electrolysis of μ CO_2 -saturated aqueous solution with Na₂SO₄ under optimise. conditions (*i.e.* pH 4.6, -1.1 V *vs.* NHE, $[Co^H(Ch)] = 1.0$ mMⁿ, indicating that the CO yield is significantly higher than the H_2 yield with the maximum turnover number (TON) of 1500 and TOF of 100 h^{-1} . The time course of formation of CO and H_2 $N₂$ -saturated aqueous solution is shown in Fig. S5 in ESI \dagger . GC data are shown in Fig S6 in ESI \dagger . The CVs and time courses of evolution of H₂ under N₂ and CO₂ in the absence of Co^{II}(Ch) or MWCNTs are shown in Figs S7 and S8 in ESI†as control experiments. No catalytic current for the $CO₂$ reduction and formation of CO in the electrolysis were observed without MWCNTs or $Co^H(Ch)$. The current efficiency for CO production for the initial 2 h was determined to be as high α . 89%, whereas that for H₂ production was $11\%^{23}$ In the case of the $Co^H(OEP)$ -modified electrode, the selectivity for CO production decreased to 50% and TON for CO production at 2 h electrolysis was only 20 (Fig. S9 in ESI \dagger). Thus, the $Co^H(Ch)$ -modified electrode exhibits much higher electrocatalytic reactivity and selectivity for CO production than the $Co^H(OEP)$ -modified electrode. **Chemcommanus**
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EPR spectra of $Co^H(Ch)$ in solution and $Co^H(Ch)$ on MWCNTs are shown in Fig. 3 to observe the $\pi-\pi$ interaction between $Co^H(Ch)$ and MWCNTs. An EPR spectrum of a froz MeCN solution containing $Co^H(Ch)$ at 4.2 K exhibited a wellresolved signals at $g = 2.293$ (Fig. 3a), which is a typical lowspin five-coordinated cobalt(II) complex.^{24,25} On the other han¹ an EPR spectrum of $Co^H(Ch)$ on MWCNTs showed a new signal at $g = 4.203$ in addition of signal at $g = 2.293$ to the low-

Fig. 4 Time courses of formation of CO and H_2 in the electrocatalytic reduction of CO₂ on the glassy carbon electrode modified with Co^{II}(Ch) (0.01 µmol) adsorbed on rGO (13 µg) in a CO₂-saturated aqueous solution containing Na₂IO₄ (5.0 mM) on rGO (13 μ g) in a CO₂-saturated aqueous solution containing Na₂ at an applied potential of -1.1 V *vs*. NHF

spin Co(II). The $g = 4.203$ signal is a triplet marker due to two molecules of cobalt(II) complexes $(S = 1/2)$ located in close to each other. This indicates that the selective reduction of $CO₂$ to CO results from involvement of two cobalt(I) complexes for two-electron transfer reduction of CO_2 .²⁶

We also examined the XPS measurements to confirm the situation of cobalt complex on MWCNTs after electrolysis. The XPS signal of the binding energy at 781 eV due to the $Co(2p_{3/2})$ was shifted to at 779 eV after electrolysis (Fig. S1⁰ in ESI). The lower energy shift may be attributed to the reduction of $Co(II)$ to form the low valent cobalt species.²⁷ Thus, the deactivation of $Co^H(Ch)$ on MWCNTs may be attributed to the formation of unreactive monomer cobalt(I) species after the electrolysis.

When MWCNTs were replaced by reduced graphene oxide (rGO), which is planar, as a support material of $\overline{Co}^{\Pi}(Ch)$ (Preparation procedures are shown in the experimental section in ESI), the CO and $H₂$ yields became much smaller (TON = 300 for CO and 200 for H_2) (Fig. 4). Thus, the three dimensional assembly of MWCNTs with $Co^H(Ch)$ (Scheme 1b) on the electrode surface may play an important role for the selective electrocatalytic reduction of CO₂ to CO. The π - π interaction between MWCNT and $Co^H(Ch)$ also provides a suitable hydrophobic environment for binding of CO₂ instead of proton, because the binding of $CO₂$ to the Co(I) complex is required for formation of CO.²² Because another Co($\frac{1}{2}$ complex is also required for the two-electron reduction of C D_2 ^{22a} two $Co^I(Ch)$ molecules located in close to each other on MWCNTs facilitate $CO₂$ reduction to CO (Scheme 1). Such situations may not be attained by a large two-dimensional π-system such as rGO, which afforded inefficient electrocatalytic reactivity for $CO₂$ reduction with $Co^H(Ch)$.

In conclusion, a cobalt(II) chlorin complex adsorbed on MWCNTs acts as an efficient catalyst for selective electrocatalytic reduction of $CO₂$ to CO in H₂O (pH = applied potential of -1.1 V *vs*. NHE with a h efficiency of 89%. The present study provides a unique strategy for selective electrocatalytic reduction of $CO₂$ to CO over proton reduction to $H₂$.

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† Electronic Supplementary Information (ESI) available: UV- Δ bsorption spectra for detection of formic acid (Fig. S1) and time courses of evolution of CO and $H₂$ in various conditions (Figs. S2- S9). XPS of working electrode (Fig. S10) See L_{\sim} 10.1039/c000000x/

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