Accepted Manuscript



This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. We will replace this Accepted Manuscript with the edited and formatted Advance Article as soon as it is available.

You can find more information about *Accepted Manuscripts* in the **Information for Authors**.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard <u>Terms & Conditions</u> and the <u>Ethical guidelines</u> still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.



www.rsc.org/materialsA

Preparation of Single-Phase Three-Component Alkaline Earth Oxide of (BaSrMg)O: High Capacity and Thermally Stable Chemisorbent for Oxygen Separation

Xuncai Chen,^a Taesung Jung,^b Jongho Park,^{*b} Woo-Sik Kim^{*a}

^a Department of Chemical Engineering, ILRI, Kyung Hee University, Yoing Kiheung-ku Seochundong, Kyungki-do 449-701, Republic of Korea

^bKorea Institute of Energy Research, 71-2, Jangdong, Yuseong-gu, Daejeon, Republic of Korea

Abstract:

This study presents a preparation method for a single-phase three-component alkaline earth oxide of (BaSrMg)O that is a high capacity and thermally stable chemisorbent for oxygen separation based on the redox reaction cycle of BaO+1/2O₂ \leftrightarrow BaO₂. First, single-phase (BaSr)CO₃ is co-precipitated based on the reaction of Ba²⁺ and Sr²⁺ with CO₃²⁻ in a solution, and then transformed to single-phase (BaSrMg)CO₃ with the addition of an Mg²⁺ solution. When varying the reaction conditions, such as the reactant concentrations of Ba²⁺, Sr²⁺, Mg²⁺, and CO₃²⁻ and the reaction temperature, (Ba_{0.52}Sr_{0.06}Mg_{0.42})CO₃ crystals are identified as the most stable phase.

The single-phase (BaSrMg)CO₃ is then converted into single-phase (BaSrMg)O by thermal decomposition under an H₂ atmosphere at 750 °C. According to a TGA analysis, the chemisorption and desorption of oxygen in (BaSrMg)O are very fast at t_{80} =3.9 min and t_{80} =14 min, respectively. In addition, the chemisorption capacity of (BaSrMg)O is higher at 2.02 mmol/g at 700 °C when compared with the chemisorption capacity of BaO/MgO at 1.75 mmol/g⁻¹. The (BaSrMg)O is also thermally stable due to the inclusion of Mg. Thus, the chemisorption capacity of (BaSrMg)O is unchanged, even over 10 redox reaction cycles. Additionally, the transient oxygen pressure required for the redox reaction of (BaO-BaO₂) is shifted from 76 mmHg to 148 mmHg due to the inclusion of Sr in (BaSrMg)O. Consequently, the three component alkaline earth oxide (BaSrMg)O can be a highly effective sorbent for industrial application to oxygen separation in terms of the process design and operation.

1. INTRODUCTION

Currently, almost 100 million tonnes of oxygen are consumed for industrial processes yearly.² Additionally, this demand will only increase due to the involvement of oxygen in so many industrial processes, including glass melting, semiconductor manufacturing, food processing, metallurgical manufacturing (e.g., copper and steel production), cutting and welding, fuel combustion, GTL conversion, and wastewater treatment.³⁻⁴ Therefore, the development of a new approach for easy and cost-effective oxygen separation is an important challenge.

Cryogenic distillation and physisorption are the two main methods presently applied to air separation.⁵ While cryogenic distillation is suitable for large-scale air separation, it requires high energy consumption and high capital and operating costs.⁶ Meantime, although physisorption is advantageous for processification, it has a poor selectivity for air separation as the physisorption enthalpies of oxygen and nitrogen are very similar.⁷⁻⁹ Thus, several recent studies have been focused on exploiting various oxygen-selective materials for air separation, such as perovskite, alkaline earth oxides, and metal-organic frameworks.^{7,10-13} Among these oxygen-selective materials, perovskite and alkaline earth oxides have been investigated for potential practical applications, as they can store oxygen in a lattice by sorption and then reversibly release the oxygen by desorption 1^{14-15} . As a result, a new method using alkaline earth oxide has been commercialized for air separation based on the BaO-BaO₂ redox reaction cycle: BaO+1/2O₂↔BaO₂.^{1,10} In this method, BaO exhibits a high oxygen selectivity and sorption capacity. However, since BaO is very reactive, it reacts easily with its surroundings and is also sintered at an elevated temperature in the BaO-BaO₂ redox reaction, resulting in a poor thermal stability and poor productivity for a multi-cyclic operation.¹ Furthermore, the transition of the $BaO-BaO_2$ redox reaction occurs at a low oxygen pressure, which requires a high operating cost. Thus, various attempts have already been made to overcome these drawbacks using additives as a promoter or stabilizer for the BaO-BaO₂ redox reaction.¹⁶⁻¹⁸ For example, Jin et al.¹

used MgO powders to improve the thermal stability of the BaO-BaO₂ redox reaction, while Park et al.¹⁰ showed that the reaction rate and thermal stability of the BaO-BaO₂ redox reaction were both enhanced by coating the BaO particles with MgO. Notwithstanding, the requirement of a low transition oxygen pressure for the BaO-BaO₂ redox reaction remains an issue. Additionally, local sintering still occurs due to the non-uniform mixture of the MgO powders in the BaO particles.

There have been many recent attempts to develop single-phase multi-component alkaline earth oxides that are suitable for practical application to air separation with a high sorption capacity, high thermal stability, high selectivity, and high transition oxygen pressure. In general, the preparation of an alkaline earth oxide begins from the synthesis of an alkaline earth carbonate, as the alkaline earth carbonate is simply converted into an alkaline earth oxide, additionally, its composition and phase can be accurately controlled in an aqueous reaction. Therefore, various two-component alkaline earth carbonates have already been synthesized using a co-precipitation reaction, ¹⁹⁻²⁴ However, their methods have hardly produced single-phase alkaline earth carbonate (BaMg)CO₃, but multi-phase ones, such as (BaMg)CO₃+MgCO₃, (BaMg)CO₃+BaCO₃, BaCO₃+LiCO₃ etc., frustrating their practical application. Furthermore, no studies have yet reported on the synthesis of a three-component alkaline earth carbonate in a solution due to the complicated reaction, difficulty in controlling the reaction, and easy phase separation leading to multi-phase particles.

Accordingly, the present study presents a novel synthesis method for a single-phase threecomponent alkaline earth carbonate of (BaSrMg)CO₃ as a precursor for the preparation of a singlephase three-component alkaline earth oxide of (BaSrMg)O. In addition, the formation mechanism of (BaSrMg)CO₃ is also investigated. Here, it should be noted that the Mg and Sr in the alkaline earth components are considered as additives for thermal stabilization and a high transient oxygen pressure for the redox reaction of the sorbent. The effects of the reaction conditions, such as the Ba²⁺, Sr²⁺, Mg²⁺, and CO₃²⁻ reactant concentrations and reaction temperature, on the synthesis of (BaSrMg)CO₃

are also studied. Additionally, the redox reaction (chemisorption-desorption of oxygen) of (BaSrMg)O is characterized. Finally, the influence of Sr on the O₂ chemisorption-desorption of (BaSrMg)O is investigated based on Raman characterization using ¹⁸O-labeling.

2. EXPERIMENTAL SECTION

2.1 Preparation of (BaSrMg)O

The reagents of Ba(NO₃)₂, Sr(NO₃)₂, Mg(NO₃)₂•6H₂O, and (NH₄)₂CO₃ were all purchased from Sigma-Aldrich (ACS grade). 100 ml of a Ba(NO₃)₂ aqueous solution (84.8 g/l) was mixed with an equal volume of a Sr(NO₃)₂ aqueous solution (17.1 g/l) in a round-bottom flask equipped with a reflux condenser, and heated to 90 °C using a heating mantle. Next, 100 ml of a (NH₄)₂CO₃ aqueous solution (40 g/l) was added to the above mixture of Ba(NO₃)₂ and Sr(NO₃)₂ for the co-precipitation of (BaSr)CO₃. After 2 hours, 100 ml of a Mg(NO₃) aqueous solution (104.0 g/l) was slowly fed into the above (BaSr)CO₃ suspension at a flow rate of 1.67 ml/min for the re-coprecipitation of (BaSrMg)CO₃. After finishing the feeding, the suspension was continuously stirred for 7 hours. Here, all the reactions were carried out at 90 °C. The (BaMgSr)CO₃ crystals in the final suspension were filtered out using a filter paper and washed with distilled water. The filtered crystals were calcinated in a tube furnace at 750 °C under a H₂ environment (H₂ flow rate = 100 ml/min) for 4 hours to obtain (BaMgSr)O crystals.

2.2 Analysis of (BaSrMg)CO₃ and (BaSrMg)O

The size and shape of the (BaSrMg)CO₃ and (BaSrMg)O crystals were examined using an FE-SEM (LEO SUPRA 55 microscope, Carl Zeiss, Germany). Their structure was analyzed

using powder X-ray diffraction (M18XHF-SRA, Mac Science, Japan) with Cu K α radiation (λ =1.54056 Å). A (BaSrMg)CO₃ particle was cut using a Cryo Ultra microtome (RMC PTPC ultramicrotome& photographic, Boeckeler, USA), and the chemical composition at the cross-section was analyzed using FE-SEM/EDS. During the synthesis, the cation concentrations in the solution (Ba²⁺, Mg²⁺, Sr²⁺) were measured using an ICP (Direct Reading Echelle ICP, Leeman, USA). The chemical compositions of (BaMgSr)CO₃ and (BaMgSr)O were analyzed using EDS element mapping (Oxford INCA Resolution 30 mm² 136eV at Mn K α 5 B to 92 U) and ICP.

2.3 O₂ Sorption/Desorption of (BaSrMg)O

A thermogravimetric analyser (SDTQ600, TA, USA) was used to determine the sorption capacity of the (BaSrMg)O chemisorbent. About 50 mg of the (BaSrMg)O sample was placed in the TGA chamber and heated up to 700 °C at 5 K/min. After stabilizing the temperature at 700 °C, a (1 atm) gas mixture (O_2 and N_2 gas) was injected into the TGA chamber. Here, the oxygen partial pressure was controlled from 80~760 mmHg using mass flow controllers (5850E, Brooks, Japan). The pressures of N_2 and O_2 were monitored using a Flow & pressure controller (GMC 1200, ISVT, Korea). Every 1h, the oxygen and nitrogen partial pressure was changed for the sorption/desorption isotherm. Here, the total gas pressure was always fixed at 760 mmHg.

2.4 Analysis using isotope of ¹⁸O

The chemisorption mechanism was studied using an oxygen isotope (${}^{18}O_2$). The (BaSrMg)O sample was placed on a hot stage (700 °C) under vacuum conditions, and ${}^{18}O_2$ gas slowly injected onto the hot stage (Linkam TS 1500, Linkam Scientific Instrument, UK) up to 1 atm. After 3 h, the sample was cooled to room temperature and analyzed as regards the chemisorption of ${}^{18}O_2$ in the sample

using a FT-Raman spectrometer and laser wavelength of 785 nm (Renishaw Micro Raman, Renishaw, UK).

3. RESULTS and DISCUSSION

Typical three-component (BaSrMg)CO₃ crystals synthesized using the present method are shown in Fig.1. According to the FE-SEM images, the crystals had an elongated hexagon shape and were uniform in size at around 28 µm (Fig. 1a). The EDS spectrum revealed that a single crystal was uniformly composed of Ba, Sr, and Mg, at 51.49%, 6.58%, and 41.93%, respectively (Fig. 1b), which matched well with the average crystal composition analyzed using ICP (Ba=51.42%; Sr=6.57; Mg=42.01%). Thus, the EDS and ICP analyses suggested that the (BaSrMg)CO₃ crystals were uniformly single phase. The phase uniformity of the crystals was also confirmed by the EDS element mapping (Fig. 1), which showed that the three elements of Ba, Mg, and Sr were uniformly distributed across the whole domain of a single crystal. In addition, the EDS spectrum demonstrated that the composition inside the crystal was equal to that at the crystal surface (Supporting Information Fig. S1 and Table S1). Thus, from the above results, it was concluded that the (BaSrMg)CO₃ synthesized using the proposed method were uniformly single-phase crystals.

Fig. 1c shows the X-ray diffraction (XRD) patterns of (BaSrMg)CO₃ with a main plane of (104). Although there are no reported references for (BaSrMg)CO₃ crystals, the XRD patterns for the (BaSrMg)CO₃ crystals were highly similar to those for the (BaMg)CO₃ crystals, where both crystals were based on a main plane of (104) and all their characteristic peaks were well matched with each other. This result is also reasonable when considering that only a small quantity of Sr (6 wt %) was incorporated in the crystals based on (BaMg)CO₃. Therefore, the lattice parameters of the (BaSrMg)CO₃ crystals, calculated based on a least-square analysis of the X-ray diffraction data as a=5.0189 Å and c= 16.731 Å, were highly comparable to the parameters of the (BaMg)CO₃ crystals (a=5.02 Å and c= 16.75). It is also interesting to note that the characteristic peak positions of the (BaSrMg)CO₃ crystals were slightly shifted to a higher angle when compared to those of the (BaMg)CO₃ crystals. This was due to the replacement of Ba²⁺ with Sr²⁺ in the crystal lattice. Since Ba²⁺ has a larger radius (1.6 Å) than Sr²⁺ (1.44 Å), ²⁵ when the Ba²⁺ in the crystal structure was replaced with Sr²⁺, the distance between the planes became smaller. Thus, according to Bragg's Law (2dsin θ = n λ), this shifted the peak position to a higher angle. Additionally, it should be mentioned that the XRD patterns of the BaCO₃, MgCO₃, and SrCO₃ crystals were significantly different from those of the (BaSrMg)CO₃ crystals (Supporting Information Fig.S2).

The synthetic mechanism of (BaSrMg)CO₃ was investigated, as shown in Figs. 2 and 3. During the solid-liquid reaction between (BaSr)CO₃-(s) and Mg(NO₃)₂-(l), the crystal shape and structure of the suspension solids were analysed using SEM and powder pattern XRD (Fig. 2 and Fig.3a), while the solution composition of Ba, Sr and Mg in the suspension solution was analyzed using ICP (Fig. 3b). Here, the compositions of Ba and Sr in the reactant (BaSr)CO₃ were around 80% and 20%, respectively (table S2 and Fig. S3). Initially, the typical rod-shape (BaSr)CO₃ crystals were dominant until bulky hexagonal crystals of (BaSrMg)CO₃ started to appear after about 1h (Fig. 2a-2c). After 2h, there were more hexagonal crystals than rod-shape crystals (Fig. 2d), and after 4h, there were no more rod-shape crystals and only bulky hexagonal crystals of about 30 μ m (Fig. 2e-2f). This change of (BaSr)CO₃ crystals to (BaSrMg)CO₃ crystals can be explained in terms of re-coprecipitation. That is, the (BaSr)CO₃ crystals were dissolved out in the solution as their solubility was enhanced with the feeding of the Mg(NO₃)₂ solution. This in turn increased the cation concentration (Ba²⁺, Sr²⁺, Mg²⁺) in the solution, which induced the three-component re-coprecipitation of (BaSrMg)CO₃. As the (BaSrMg)CO₃ crystals grew, the (BaSr)CO₃ crystals were continuously dissolved out and eventually disappeared.

Using the XRD patterns, the transformation of the (BaSr)CO₃ crystals into (BaSrMg)CO₃ crystals was confirmed (Fig. 3a). For the first 30 min, the XRD patterns of the crystals matched the reference diffraction data for (Ba_{0.8}Sr_{0.2})CO₃ (JCPDS: 47-0223), even though the characteristic peak intensity gradually decreased due to the dissolution of the crystals. After 1h, while the diffraction peaks of the (BaSr)CO₃ crystals were almost disappeared, new diffraction peaks for the (BaSrMg)CO₃ crystals were completely disappeared and those of the new (BaSrMg)CO₃ crystals were fully developed.

In addition, the cation composition in the solution was traced to confirm the mechanism of $(BaSrMg)CO_3$ formation. As shown in Fig. 3b, when feeding the Mg(NO₃)₂ solution into the reactor, the cation concentrations of Ba^{2+} and Sr^{2+} in the solution monotonically increased and then levelled off after 4 h, as the Mg ions in the solution increased the solubility of the (BaSr)CO₃, as previously reported by Davis et al,²⁶Voronkov et al,²⁷ Berner et al²⁸, and Van Enckevort et al ²⁹. Meanwhile, the Mg²⁺ concentration in the solution initially increased during 1 h, and then was followed by the sudden spontaneous nucleation of (BaSrMg)CO₃, which resulted in a rapid reduction of the Mg concentration in the solution after 2h. Thereafter, the Mg²⁺ concentration was slightly reduced until 4h whereas there were significant changes in Ba^{2+} and Sr^{2+} concentrations. After 4h, all ion concentrations levelled off, indicating the completion of the re-coprecipitation of (BaSrMg)CO₃. It is interesting to note that the cation composition of the (BaSrMg)CO₃ crystals was always about Ba²⁺=52%, Sr²⁺=6%, and Mg²⁺=42%, regardless of the initial reactant concentrations of (BaSr)CO₃ and Mg(NO₃)₂, as shown in Table.S3. Thus, when changing the reactant molar ratio of $Mg(NO_3)_2$ to $(BaSr)CO_3$, the solid-liquid reaction produced a significant variety of crystals. Here, (Ba_{0.8}Sr_{0.2})CO₃ crystals were used for the solid-liquid reaction. When the reactant ratio of $[Mg(NO_3)_2]/[(BaSr)CO_3] < 0.7$, multiphase crystals of (BaSr)CO₃ and (BaSrMg)CO₃ were obtained (Figs. 4a and 4b). This result was due to an incomplete conversion of (BaSr)CO₃ crystals to (BaSrMg)CO₃. When using EDS, it was confirmed that the (BaSr)CO₃ in the multi-phase crystal product had a composition of Ba=80% and Sr=20%, the same as the reactant solid (($Ba_{0.8}Sr_{0.2}$)CO₃), however, the cation composition of (BaSrMg)CO₃ in the product was almost the same as that of the above stable (BaSrMg)CO₃ in Fig. 1 (Supporting Information Fig. S4). Yet, when [Mg(NO₃)₂]/[(BaSr)CO₃] \geq 0.7, the (BaSr)CO₃ crystals were completely converted to stable (BaSrMg)CO₃ crystals (Fig. 4c-4e). The multi-phase crystals produced when varying the reactant molar ratio was also confirmed using XRD (Fig.4f). At a reactant ratio of [Mg(NO₃)₂]/[(BaSr)CO₃]<0.7, the diffraction peaks for both (BaSr)CO₃ and (BaSrMg)CO₃ were present, however, the characteristic peaks for (BaSr)CO₃ diminished when increasing the reactant ratio and completely disappeared with the reactant ratio above 0.7.

The influence of the cation ratio of Ba to Sr in the reactant (BaSr)CO₃ on the synthesis of (BaSrMg)CO₃ is investigated in Fig. 5. Here, the reactant ratio $[Mg(NO_3)_2]/[$ (BaSr)CO₃] was always fixed at 1.0. When the cation ratio of Ba to Sr (Ba/Sr) in the reactant (BaSr)CO₃ was below 4.0, multi-phase crystals of (BaSrMg)CO₃ and SrCO₃ were coprecipitated (Fig 5a and 5b). However, when increasing the Ba/Sr ratio above 4.0, single-phase crystals of (BaSrMg)CO₃ were synthesized (Fig. 5c and 5d), as confirmed by an XRD analysis (Fig.5e). The phase separation at a low Ba/Sr ratio was due to the excess Sr ions dissolved in the solution. That is, at a low Ba/Sr ratio, the relative amount of Sr to Ba and Mg was more than enough for the formation of (BaSrMg)CO₃, resulting in the simultaneous precipitation of SrCO₃. When compared with the carbonate compounds of BaCO₃ and MgCO₃, the low solubility of SrCO₃ may also have contributed to its easy precipitation.³⁰ It should also be mentioned that the crystal structure and shape of (BaSr)CO₃ did not vary with the Ba/Sr ratio across the whole range of 1/9 ~9.0, as summarized in the Supporting Information Fig.S5 and S6.

The influence of the reaction temperature on the preparation of the (BaSrMg)CO₃ crystals was examined, as shown in Fig. S7. According to the SEM images and XRD analysis, single-phase crystals of (BaSrMg)CO₃ were produced at a reaction temperature above 70 °C, whereas below this

temperature, multi-phase crystals of (BaSrMg)CO₃ and (BaSr)CO₃ were produced (Figs. S7a and S7b) due to the dissolution of (BaSr)CO₃ depending on the temperature. Thus, at a low temperature, since not enough (BaSr)CO₃ was dissolved out in the solution due to its low solubility, the (BaSr)CO₃ remained in the product suspension. In addition, the influence of the carbonate concentration $[CO_3^{2^-}]$ on the synthesis of (BaSrMg)CO₃ is summarized in Fig. S8 of the Supporting Information. Actually, the anion had no effect on the multi-component co-precipitation. Thus, the crystal shape, structure, and composition of the (BaSrMg)CO₃ remained unchanged across the whole range of carbonate concentrations from 0.04 g/mL to 0.12 g/mL, yet the crystal size became smaller when increasing the carbonate concentration due to the promotion of (BaSrMg)CO₃ crystal nucleation.

As shown in Fig. 6, the single-phase three-component alkaline earth carbonate (BaSrMg)CO₃ was converted to single-phase three-component alkaline earth oxide (BaSrMg)O for use as a chemisorbent for oxygen separation based on the redox reaction cycle of BaO + $1/2O_2 \leftrightarrow BaO_2$. While the (BaSrMg)O crystals were similar in shape and size to the (BaSrMg)CO₃ crystals, they were covered with nanosize needles that were normally oriented to the crystal surface (Figs.6a and 6b). These nanoneedles on the crystal surface increased the specific reaction surface with O₂ for chemisorption. Based on the EDS element mapping (Fig. 6b) and XRD pattern (Fig. 6c), the phase uniformity of the (BaSrMg)O crystals was confirmed.

The oxygen chemisorption of (BaSrMg)O was characterized using a thermogravimetric analyser (TGA), as shown in Fig. 7. According to the sorption isotherm of O_2 at 700°C (Fig. 7a), the oxygen chemisorption began to occur above an oxygen partial pressure of 148 mmHg, which is called the transient oxygen pressure and means the oxygen pressure required for the equilibrium of the redox reaction in (BaSrMg)O. Thus, the oxidation reaction (chemisorption) proceeds at an oxygen pressure above the equilibrium pressure, while reduction (desorption) prevails at an oxygen pressure below the equilibrium pressure. The transient oxygen pressure (148 mmHg) for (BaSrMg)O is much higher

than transient oxygen pressure for BaO at 76 mmHg ³¹, indicating that the three-component chemisorbent of (BaSrMg)O would be much more economical for industrial application than the single component chemisorbent of BaO. In addition, the sorption isotherm also revealed that the sorption capacity (2.02 mmol-O₂/g) of (BaSrMg)O was much higher than that (1.75 mmol-O₂/g) of (BaMg)O, as previously reported by Jin et al and his co-workers^{1,32}. The chemisorption and desorption cycle is shown in Fig. 7b. Under the oxygen flow, the weight of the sorbent rapidly increased due to the fast oxidation reaction. Thus, the relaxation time, t₈₀, was measured as 3.9 min for (BaSrMg)O, representing a much faster adsorption rate than that for (BaO₂/MgO) prepared using hydrothermal (t₈₀= 4 min)and sol–gel (t₈₀= 6~9 min) methods, as reported by Park et al.¹⁰ The desorption was also much faster, where the desorption time, t₈₀, was measure as 14 min under a N₂ environment. Here, the relaxation time, t₈₀, was defined as the time required for the fractional approach to reach 80% of the reaction from an equilibrium state to a new one, as reported by Lin et al.³² Figure 7c shows the multi-cycle chemisorption and desorption of the sorbent at 700°C. No significant change in the chemisorption and desorption profiles was observed over 10 cycles, demonstrating the high thermal stability of the sorbent due to the incorporation of Mg in the crystals.

As mentioned above, the high transient oxygen pressure for the redox reaction (BaO + $1/2O_2 \leftrightarrow$ BaO₂) of the sorbent was due to the incorporation of Sr in the crystal lattice ((BaSrMg)O). Since Sr belongs to the same family of alkaline earth metals as Ba, it easily replaced Ba in the crystal lattice (Ba-O-Sr). However, since the ionic radius of Sr²⁺ is smaller than that of Ba²⁺, Sr²⁺formed a shorter and stronger bondage with oxygen (Sr-O) than Ba²⁺ (Ba-O). According to a report by de La Croixet et al,³³ the lattice energy of Sr-O (-3240 KJ/mol) is higher than that of Ba-O (-3021 KJ/mol). In addition, due to the stronger electron attraction of Sr, the Ba-O bondage in Ba-O-Sr is slightly looser and longer when compared with that in Ba-O-Ba. Thus, it can be assumed that during the oxygen chemisorption, the Ba-O bondage in Ba-O-Sr was more easily broken for oxidation to Ba-O-O-Sr when compared with the oxidation of Ba-O-Ba to Ba-O-O-Ba. Inversely, during the oxygen

desorption, Ba-O-O-Sr was more easily reduced to Ba-O-Sr when compared with the reduction of Ba-O-O-Ba to Ba-O-Ba. As a result, Ba-O-Sr and Ba-O-O-Sr could be in equilibrium at an even higher oxygen partial pressure than the Ba-O-Ba and Ba-O-O-Ba system. Consequently, the transient oxygen pressure for the redox reaction of (BaMgSr)O was much higher than that of BaO.

To confirm the above explanation, the (BaSrMg)O₂ crystals were analysed using Raman spectroscopy. As shown in Fig. 8a, the O-O frequency of (BaSrMg)O₂ occurring at 844 cm⁻¹ was lower than the O-O frequency of BaO₂(847 cm⁻¹)³¹, indicating that the O-O bonding in Ba-O-O-Sr was weaker than that in Ba-O-O-Ba. Using an isotope of oxygen (¹⁸O₂), it was also found that all three absorption peaks of the three kinds of O-O bonding in (BaSrMg)O₂, including ¹⁸O-¹⁸O, ¹⁸O-¹⁶O, and ¹⁶O-¹⁶O, appeared at 795, 820, and 844 cm⁻¹ respectively, which were red-shifted from the corresponding absorption peaks at 799, 824, and 847 cm⁻¹, respectively, in BaO₂³¹ (Fig. 8b). This was due to the replacement of Ba with Sr that has a smaller radius, thereby allowing strong Sr-O bonding and reducing the O-O vibration energy in Ba-O-O-Sr. Thus, the small amount of Sr incorporated in the (BaSrMg)O crystals had a significant influence on the increment of the transient oxygen pressure required for the redox reaction cycle.

4. CONCLUSION

This study presented a method for preparing a highly capable and thermally stable chemisorbent of (BaSrMg)O. In addition, the formation mechanism was also discussed at length. First, the (BaSr)CO₃ crystals are synthesized by co-precipitation and then transformed into (BaSrMg)CO₃ crystals in the solution by the addition of an Mg²⁺ solution. Thus, when adding the Mg²⁺, the Ba²⁺ and Sr²⁺ concentrations in the solution are increased due to the dissolution of (BaSr)CO₃ in the solution, inducing three-component co-precipitation for the formation of single-phase (BaSrMg)CO₃. The reactant concentrations of Ba²⁺, Sr²⁺, Mg²⁺, and CO₃²⁻, and the reaction temperature were found to

have a significant influence on the formation of the $(BaSrMg)CO_3$ crystals. However, the singlephase $(BaSrMg)CO_3$ was always formed with a composition of 52 % (Ba), 6% (Sr), and 42 % (Mg), which was the most stable, regardless of the reaction conditions.

The single-phase (BaSrMg)CO₃ crystals were converted into single-phase(BaSrMg)O crystals by thermal decomposition under an H₂ atmosphere at 750°C. The (BaSrMg)O crystals showed a high chemisorption capacity of oxygen (2.02 mmol/g) at 700 °C owing to the high fraction of Ba and a high thermal stability based on the inclusion of Mg in the crystals. Furthermore, the (BaSrMg)O crystals exhibited a high chemisorption rate ($t_{80} = 3.9$ min) and desorption rate ($t_{80}=14$ min). In particular, the transient oxygen pressure for the redox reaction in (BaSrMg)O significantly increased from 76 mmHg to 148 mmHg at 700 °C, implying a high-strength chemisorbent for practical application to oxygen separation. This was because the replacement of Ba with Sr in the crystal lattice shifted the equilibrium state of the BaO-BaO₂ redox reaction cycle to a high oxygen partial pressure. Therefore, the proposed method for the preparation of (BaSrMg)O is a promising platform for the elaboration of multi-component metal oxide materials. In addition, due to their high capacity, thermal stability, and high transient pressure, such materials represent a significant improvement in oxygen separation for industrial application.

ACKNOWLEDGMENT

This work was conducted under the framework of the Research and Development Program of the Korea Institute of Energy Research (KIER) (B4-2442-02).

ASSOCIATED CONTENT

Supporting Information.

Supplementary Table S1-S3, and Figures S1-S8 (Section S 2) (PDF)

AUTHOR INFORMATION

Corresponding Author

* E-mail: <u>wskim@khu.ac.kr</u> (W.S. Kim), <u>jongho@kier.re.kr</u> (H.J.Park)

Notes and references

- 1. Jin, C.; Hirose, T.; Koto, M. Ind. Eng. Chem. Res. 2005, 44, 2942.
- 2. Wall, T. F. Combustion processes for carbon capture. Proce Combust Institute. 2007, 31, 31.
- 3. Badwal, S. P. S; Ciacchi, F. T. Adv.mater. 2001.13.12.
- 4. Watson, C. F.; Whitley, R. D.; Meyer, M. L. U.S. Patten5529610. 1996.
- 5. Gaffney, T.R. Curr. Opin.Solid State Mater.Sci. 1996,1,69.
- 6.Cengel, Y; Boles, M. Thermodynamics: an engineering approach. 5th ed. New York: McGraw-Hill; 2006.
- 7. Southon, P. D.; Price, D. J.; Nielsen, P. K.; McKenzie, C. J.; Kepert, C. J. J. Am. Chem. Soc. 2011,133,10885-10891.
- 8.Sircar, S.; Rao, M. B.; Golden, T. CElsevier Science Publ B V: Amsterdam, 1999; 120, 395.
- 9. Ismail, A. F.; David, L. I. B. J. Membr. Sci. 2001,193,1.
- 10. Park, J. H.; Cho, Y. S.; Yi, K. B.; Han, S. S.; Cho, S. H. Appl. Surf. Sci. 2010,256, 5528-5532.
- 11.Kharton, V. V.; Yaremchenko, A. A. Memb Sci. 1999, 163, 307-317.
- 12. Wang, E. A.; Oxygen-Selective Adsorbents. USA Patent. Patent No.: US 6436171 B1.
- 13. Tiné, M. R. Coord. Chem. Rev. 2012, 256, 316-327.
- 14. Yang, Q.; Lin, Y. S.; Bülow, M. AIChE J.2006, 52, 574-581.
- 15. Lin, Y. S.; Maclean, D. L.; Zeng, Y.; USA patent. Patent No,6059858.
- 16. Moriaty, J. L. J. Iowa Acad. Sci. 1970, 77, 360.
- 17. Massey, L. G.; Tarman, P. B.; Ranwani, D. U. S. Patent 3903010, 1975.
- 18. Fahim, M. A.; Ford, J. D. Chem. Eng. J. 1983, 27, 21.
- 19. Moriaty, J. L. J. Iowa Acad. Sci. 1970, 77, 360.
- 20. Hood, W. C.; Steidl, P. F. American Mineralogist. 1973, 58, 342-347.
- 21. Terada, J.. Phys. Soc. Japan. 1953, 8, 2.
- 22. Pasierb, P.; Komornicki, S.; Rokita, M.; Rekas, M..Molec.Struc. 2001, 596, 151-156.
- 23. Weinbruch, S.; Buttner, H.; Rosenhauer, M. Phys. Chem. Minerals. 1992, 19, 289-297.
- 24. Hood, W. C.; Steidl, P. F.; Tschopp, D. G. 1974, 59, 471-474.
- 25 Chen, Y. H.; Yu, S. C.; Huang, E.; Lee, P. L. Phys. B. 2010, 405, 4386-4388.
- 26. Davis, K.J.; Dove, P. M.; De yoreo, J, J. Sci. 2000, 290, 1134.
- 27. Voronkov, V. V.; Rashkovich, L. N. Sov. Phys. Crystal-logr. 1992,37, 289.
- 28. Berner, R. A. Geochim. Cosmochim. Acta. 1975, 39, 489.
- 29. Van Enckevort, W. J. P.; Van den Berg, A. C. J. F., J. Cryst. Growth, 1998, 183, 441.

- 30. Harris, D.; Porter, L. K.; Paul, E. A. Commun Soil Sci Plant Anal. 1997, 28,747.
- 31. Mestl, G.; Rosynek, M. P.; Lunsford, J. H. J. Phys. Chem. B. 1998, 102,154.
- 32. Jin, C.; Suehiro, T.; Kodama, A.; Goto, M.; Hirose, T. J. Chem. Eng. Jpn. 2001, 34,279.
- 33. De La Croix, A.; English, R. B.; Brow, M. E. J. Solid State Chem. 1998, 137, 346.

Figure list:

- Figure 1. FE-SEM and XRD analysis of (BaSrMg)CO₃ crystals (a) FE-SEM images of (BaSrMg)CO₃ crystals, (b) Element analysis on an isolated (BaSrMg)CO₃ crystal using EDS-mapping (elements incuding Ba, Sr, and Mg), (c) XRD patterns of (BaSrMg)CO₃ crystals.
- Figure 2. Transient profile of (BaSr)CO₃+Mg(NO₃)₂ reaction at 90°C monitored by FE-SEM. (a) FE-SEM image of (BaSr)CO₃ crystals (b) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 30 min, (c) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 1 h, (d) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 2 h, (e) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 4 h, (f) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 6 h.
- Figure 3. (a) Transient solid profile of (BaSr)CO₃+Mg(NO₃)₂ reaction at 90°C monitored by XRD,
 (b) Cation concentration profiles of Ba²⁺, Mg²⁺, and Sr²⁺ in solution during (BaSr)CO₃+Mg(NO₃)₂ reaction at 90°C.
- Figure 4. Effect of reactant ratio $[Mg(NO_3)_2]/[(Ba_xSr_y)CO_3]$ on co-precipitation of $(BaSrMg)CO_3$. Here, the x : y ratio of $(Ba_xSr_y)CO_3$ was fixed at 0.8 : 0.2. (a) reactant ratio of 0.5, (b) reactant ratio of 0.6, (c) reactant ratio of 0.7, (d) reactant ratio of 0.8, (e) reactant ratio of 0.9 and (f) XRD patterns of product crystals.
- Figure 5. Effect of (Ba_xSr_y)CO₃ with various x : y ratio on co-precipitation of (BaSrMg)CO₃. Here, reactant concentration ratio [Mg(NO₃)₂]/[(BaSr)CO₃] was fixed at 1.0 ; (a) 0.6:0.4 (b) 0.7:0.3 (c) 0.8:0.2 (d) 0.9:0.1, and (d) XRD patterns of product crystals.
- Figure 6. FE-SEM and XRD analysis of (BaSrMg)O crystals (a) FE-SEM images of (BaSrMg)O crystals, (b) SEM image of single (BaSrMg)O crystal, and element analysis of Ba, Mg, Sr and O by EDS-mapping, (c) XRD patterns of (BaSrMg)O crystals. (BaO reference JCPDS 260177; MgO reference JCPDS 450946; SrO reference JCPDS 060520)
- Figure 7. (a) Sorption capacity of O_2 on (BaSrMg)O crystals, (b) One cycle of sorption and desorption, Relaxation time, t_{80} , was defined based on 80% weight change. (c) Multi sorption-desorption cycles of O_2 , All analyses were measured by TGA at 700°C.
- Figure 8. Raman spectra for (a) (BaSrMg)O₂ crystals and (b) (BaSrMg)O₂ crystals of the (BaSrMg)O crystals after chemisorption of ¹⁸O₂ gas for 3h.

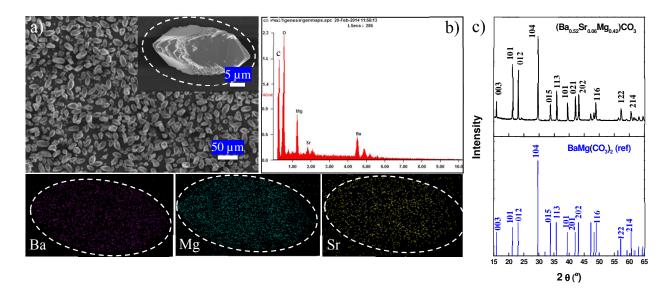


Figure 1. FE-SEM and XRD analysis of (BaSrMg)CO₃ crystals (a) FE-SEM images of (BaSrMg)CO₃ crystals, (b) Element analysis on an isolated (BaSrMg)CO₃ crystal using EDS-mapping (elements incuding Ba, Sr, and Mg), (c) XRD patterns of (BaSrMg)CO₃ crystals.

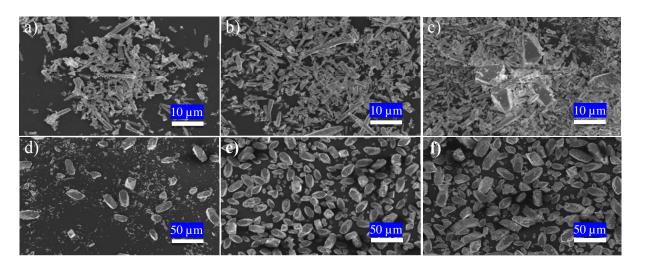


Figure 2. Transient profile of (BaSr)CO₃+Mg(NO₃)₂ reaction at 90°C monitored by FE-SEM. (a) FE-SEM image of (BaSr)CO₃ crystals (b) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 30 min, (c) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 1 h, (d) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 2 h, (e) product solids ((BaSr)CO₃ and (BaSrMg)CO₃ at 4 h, (f) product solids ((BaSr)CO₃ and (BaSrMg)CO₃) at 6 h.

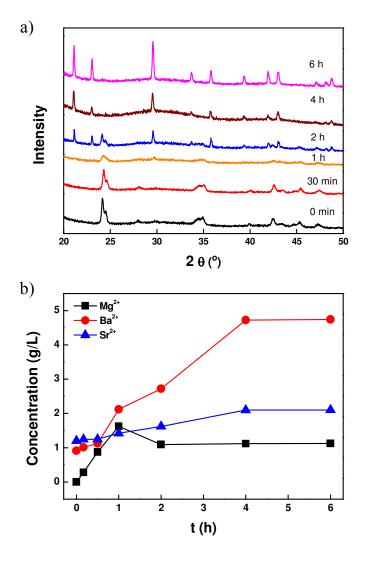


Figure 3. (a) Transient solid profile of (BaSr)CO₃+Mg(NO₃)₂ reaction at 90°C monitored by XRD,
(b) Cation concentration profiles of Ba²⁺, Mg²⁺, and Sr²⁺ in solution during (BaSr)CO₃+Mg(NO₃)₂ reaction at 90°C.

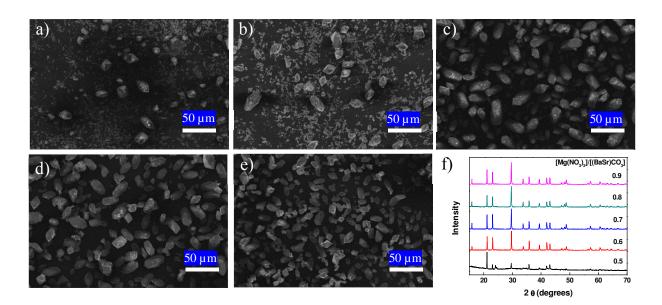


Figure 4. Effect of reactant ratio [Mg(NO₃)₂]/[(Ba_xSr_y)CO₃] on co-precipitation of (BaSrMg)CO₃. Here, the x : y ratio of (Ba_xSr_y)CO₃ was fixed at 0.8 : 0.2. (a) reactant ratio of 0.5, (b) reactant ratio of 0.6, (c) reactant ratio of 0.7, (d) reactant ratio of 0.8, (e) reactant ratio of 0.9 and (f) XRD patterns of product crystals.

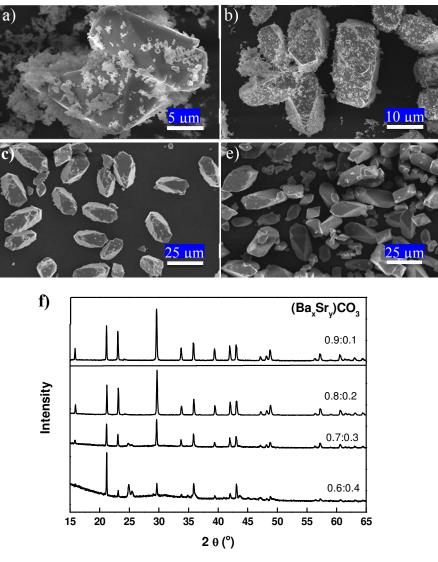


Figure 5. Effect of (Ba_xSr_y)CO₃ with various x : y ratio on co-precipitation of (BaSrMg)CO₃. Here, reactant concentration ratio [Mg(NO₃)₂]/[(BaSr)CO₃] was fixed at 1.0; (a) 0.6:0.4 (b) 0.7:0.3 (c) 0.8:0.2 (d) 0.9:0.1, and (d) XRD patterns of product crystals.

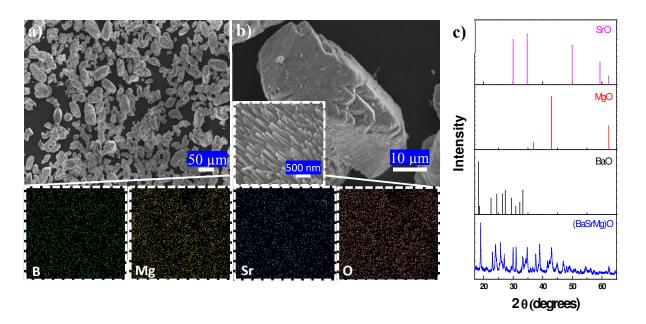


Figure 6. FE-SEM and XRD analysis of (BaSrMg)O crystals (a) FE-SEM images of (BaSrMg)O crystals, (b) SEM image of single (BaSrMg)O crystal, and element analysis of Ba, Mg, Sr and O by EDS-mapping, (c) XRD patterns of (BaSrMg)O crystals. (BaO reference JCPDS - 260177; MgO reference JCPDS - 450946; SrO reference JCPDS - 060520)

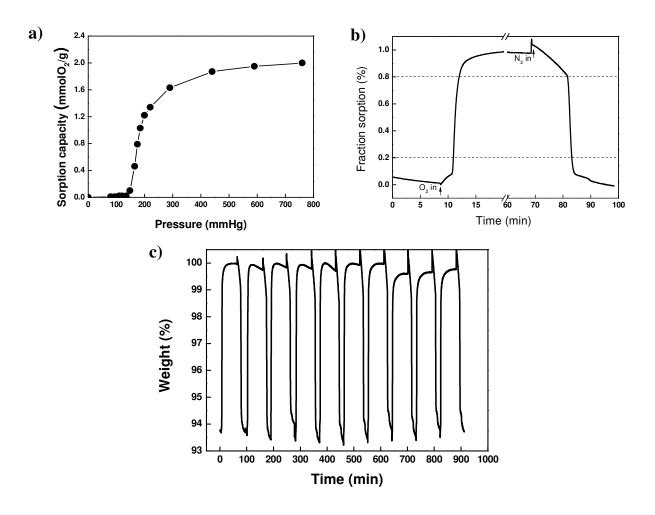


Figure 7. (a) Sorption capacity of O_2 on (BaSrMg)O crystals, (b) One cycle of sorption and desorption, Relaxation time, t_{80} , was defined based on 80% weight change. (c) Multi sorption-desorption cycles of O_2 , All analyses were measured by TGA at 700°C.

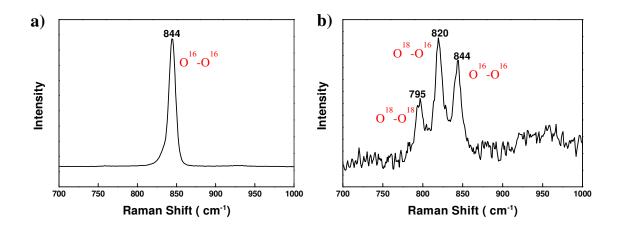
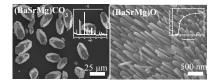


Figure 8. Raman spectra for (a) (BaSrMg)O₂ crystals and (b) (BaSrMg)O₂ crystals of the (BaSrMg)O crystals after chemisorption of ¹⁸O₂ gas for 3h.



Highlight: A single-phase three-component alkaline earth (BaSrMg)O crystals were prepared by a novel method, which show a high performance in oxygen chemisorption .