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# **PAPER**

# **Low temperature sintering of binder-containing TiO2/metal peroxide pastes for dye-sensitized solar cells**

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<sup>5</sup>*Received (in XXX, XXX) Xth XXXXXXXXX 20XX, Accepted Xth XXXXXXXXX 20XX*  **DOI: 10.1039/b000000x** 

Nano-structured metal oxide films are a key component of dye-sensitized (DSC) solar cells. Scaling such devices requires lower temperature processing to enable cheaper substrates to be used. In this context, we report a new and scaleable method to sinter binder-containing metal oxide pastes to make DSC photo-

- 10 electrodes at lower temperatures. Metal peroxide powders  $(CaO<sub>2</sub>, MgO<sub>2</sub>, or ZnO<sub>2</sub>)$  have been added to terpineol–based P25 pastes containing ethyl cellulose binder or to commercial  $TiO<sub>2</sub>$  paste (DSL18NR-T). Thermal analysis shows binder decomposition occurring at 300 °C instead of the standard 450 °C for a TiO<sub>2</sub>-only paste and suggests that the metal peroxides act as combustion promoters releasing heat and oxygen within the film at temperatures. The data show that this heat and oxygen release coincide best
- 15 with binder combustion for  $ZnO_2$  and DSC device tests show that adding  $ZnO_2$  to TiO<sub>2</sub> pastes produces the best performances affording  $\eta = 7.5\%$  for small devices (0.26 cm<sup>2</sup>) and  $\eta = 5.7\%$  at 300 °C or 450 °C for DSL18NR-T/ $ZnO_2$  for larger (1 cm<sup>2</sup>) devices. To the best of our knowledge, the performance of the  $(0.26 \text{ cm}^2)$  cells is comparable to the highest efficiency devices reported for DSC fabricated using low temperature methods. Device efficiency was most strongly linked with J<sub>sc</sub>, BET and dye sorption

 $_{20}$  measurements suggesting that  $J_{\rm sc}$  was linked with metal oxide surface area and dye loading. The latter was linked to the availability of surface sorption sites for dye molecules which was strongly negatively affected by any residual organic binder which resulted from incomplete combustion.

O'Regan and Grätzel's breakthrough in dye-sensitised solar cell (DSC) technology<sup>1</sup> showed that sintering pre-made  $TiO<sub>2</sub>$  nano-25 crystals<sup>2-4</sup> at 450-600 °C significantly increases the photo-anode surface area, dye loading and short circuit current. This has led to considerable interest in DSC devices as promising candidates for large scale, low cost PV because they should be manufacturable using printing and roll-to-roll processing using abundant and non-30 toxic raw materials<sup>5,6</sup>.

 In DSC devices, the mechanical and electrical connectivity between the  $TiO<sub>2</sub>$  particles are key to long-term device function as charge must travel through the photo-electrode to the current collecting working electrode<sup>7</sup>. Typically this is achieved by

- $_{35}$  printing a colloidal suspension of well-dispersed, crystalline TiO<sub>2</sub> nanoparticles where the paste rheology is controlled by the addition of a long-chain organic polymer (the binder). The binder enables crack-free films to be printed with variable but controlled films thicknesses at a range of scales. Without the binder present,
- <sup>40</sup>it is impossible to print large enough photo-electrodes to scale the technology. This means that currently printed films must be sintered at  $> 450$  °C to completely combust the organic binder to free up dye sorption sites on the surface of the  $TiO<sub>2</sub>$  particles and to enable robust inter-particle connections to form but low
- $45$  enough to minimise any reduction in TiO<sub>2</sub> surface area. However, this limits the working electrode substrate to FTO-coated glass or Ti foil<sup>8</sup> which are inflexible and heavy or expensive<sup>9</sup>, respectively. By comparison cheaper, more lightweight and flexible substrates which are suitable for large-scale roll-to-roll <sup>50</sup>manufacture (e.g. metal foils, TCO-coated plastic) require lower processing temperatures; typically 300 °C for metal foils and 150 <sup>°</sup>C for plastics<sup>10</sup>. However, there are no reports in the literature to date of methods to sinter binder-containing pastes at low temperature.
- Instead, although low temperature sintering of photo-anodes for DSC has been widely studied, reports have centred on using binder-free pastes. However, as discussed previously, binder-free pastes are significantly limited for larger scale applications because of the difficulties in controlling printability and film 60 consistency over wider areas (e.g. film thickness, and interparticle adhesion which can lead to cracking and substrate adhesion which can lead to delamination). Binder-free approaches have included spin coating<sup>11</sup>, sol gel<sup>12</sup>, hydrothermal treatment<sup>13-15</sup> chemical sintering<sup>16-17</sup>, pressure sintering<sup>18-20</sup>, 65 electrophoretic deposition of TiO<sub>2</sub> nanoparticles<sup>21</sup>, varying TiO<sub>2</sub> particles<sup>22</sup> and the use of electron beam showers<sup>23</sup>. Variations on

radiant heating have also been studied including laser treatment $24$ , microwave irradiation<sup>25</sup> and post-sintering  $O_2$  plasma<sup>26</sup> aimed at removing residual organic matter from the metal oxide surface. Whilst these approaches have shown promise at the laboratory <sup>5</sup>scale, producing consistent, large-scale meso-porous films

- required for DSC device manufacturing will require the presence of a binder in the  $TiO<sub>2</sub>$  colloid. Hence, the study of low temperature approaches to sintering binder-containing metal oxide pastes remains a key challenge for DSC manufacturing.
- <sup>10</sup> In this context, this paper reports a new approach to lower sintering temperatures of binder-containing metal oxide pastes to manufacture photo-electrodes for DSC. We believe this is the first report using solid peroxides as combustion promoters. This approach enables accurate control of paste rheology by retaining
- <sup>15</sup>an organic polymer binder in the metal oxide pastes which is essential to produce coherent, large scale films with consistent thickness. Our combined experimental approach has been to screen larger films (3 x 2 cm) to examine film coherence and colour, to understand the fundamental thermal chemistry of
- <sup>20</sup>screen printing pastes and how this influences sintering and then to make larger DSC devices than are typically reported  $(1 \text{ cm}^2)$  to test the effects of sintering on performance. Finally, we have studied metal oxide area and dye loading to investigate the links between short circuit current and sintering treatment.
- 25

## **Experimental**

#### **Paste and device manufacture**

P25 pastes were prepared by thoroughly mixing P25 (16 g, Degussa) with terpineol (64.9 g, Fluka) and ethyl cellulose (8 g,

<sup>30</sup>Fluka Product# 46070). Peroxide containing pastes were prepared by adding calcium peroxide, magnesium peroxide or zinc peroxide (10% w/w *versus* TiO<sub>2</sub>, all Aldrich) and thoroughly mixing for 1 h. Commercial DSL18NR-T paste (Dyesol) was either used as purchased or metal peroxide was added as 35 described above.

 Photo-electrodes were prepared prepared by doctor blading metal oxide paste on to FTO-coated glass (TEC15, NSG) and sintering in air at either 450 °C, 300 °C or 150 °C for 30min. Larger films were prepared  $(3 \times 2 \text{ cm})$  to study film coherence

 $40$  over a larger area. DSC devices were prepared using 1 cm<sup>2</sup> films (minimum 3 replicates per treatment) to study film coherence and reproducibility. Selected films were then immersed in 40 mM  $TiCl<sub>4</sub>:THF<sub>2(aq)</sub>$  at 70 °C for 30min before rinsing with water and air drying for 10min. The films were then re-sintered at the same

45 temperature used during the first sintering process so that no film experienced a temperature greater than its initial sintering temperature at any point during processing.

 Counter electrodes were prepared by spreading PT1 paste (Dyesol) on to TEC 8 glass (NSG) and heating to 400 ˚C in air

- 50 for 30min. The photo and counter electrodes were then sealed together using a Surlyn gasket at 120 ˚C followed by fast dyeing with 0.3 mM N719 (Dyesol) in acetonitrile:*tert.*-butanol (1:1 v/v) for 10min as described previously.<sup>27</sup> The electrolyte was  $0.8 M 1$ methyl-3-propyl imidazolium iodide, 0.05 M *tert.*-butyl
- $55$  ammonium iodide, 0.05 M  $I_2$ , 0.3 M benzimidazole and 0.05 M guanidinium thiocyanate in acetonitrile.

#### **Device Characterisation**

Current-voltage characteristics were measured using an ABET Solar Simulator with Xe arc lamp and a Keithley 2400 at 100 60 mW cm<sup>-2</sup> or 1 Sun between 0 and 1 V. Spectral response was measured from 300-800 nm on a QEX10 Quantum Efficiency Measurement System in DC mode at resolution of 10 nm. Lamps were calibrated to 1 Sun (100 mW  $\text{cm}^2$ ) using a certified (Oriel 91150V) mono-crystalline Si reference cell traceable to the <sup>65</sup>National Renewable Energy Laboratory (NREL).

 Photocurrent and photovoltage transients were measured as described in $^{28}$ . The white bias light was provided by a BRIDGELUX 9000 lumen LED array (Farnell) whilst the pulse light was provided by a bank of four OSLON PowerCluster green  $70$  LED arrays (RS). Pulse intensity was chosen to make sure  $\Delta V$  < 10 mV above  $V_{OC}$ . A pulse length of 250 µs was utilized and was generated *via* a fast MOSFET transistor controlled by a National Instruments USB-6251 data acquisition board (DAQ) and WaveMetrics IGOR Pro software. Voltages were measured <sup>75</sup>directly using the DAQ whilst currents were measured *via* a voltage drop against a 1 Ω resistor.

 XRD was carried out using a PANalytical diffractometer at 45 kV and 35 mA between 20 and 60 $^{\circ}$  20 using Ni-filtered Cu-K<sub> $01$ </sub> radiation  $(\lambda=1.5405^{\circ}A)$ . Thermal gravimetric analysis and <sup>80</sup>differential scanning calorimetry were performed using a SDTQ600 TGA/DSC (TA Instruments Ltd). The pastes were either run as prepared or were pre-dried at 100-110 ˚C for 2 h to evaporate the solvent to focus the analysis on binder combustion. The samples were ramped at  $10 \degree C$  min<sup>-1</sup> between room 85 temperature and 600 ˚C under flowing air. Surface area of presintered doctor-bladed films was determined using BET (Brunauer-Emmett-Teller) isotherms at -196 °C using a Micromeritics Gemini III 2375. Electron microscopy and energy dispersive X-ray elemental analyses were performed on a Field <sup>90</sup>Emission Gun-Scanning Electron Microscope (FEG-SEM) Hitachi S-4800 (12 keV, 10 µA) equipped with an Oxford instruments  $X-Max$  (50 mm<sup>2</sup> window) detector.

 N719 dye sorption was studied using sintered P25 and  $P25/ZnO<sub>2</sub>$  films either by directly immersing the film in N719 <sup>95</sup>dye solution for 24 h or by scraping sintered films off a glass substrate and immersing the collected powder into N719 dye solution for 24 h. N719 uptake was quantified by firstly desorbing the dye using 0.1 M NaOH(aq)<sup>/</sup> ethanol (1:1 v/v) followed by calculation of the concentration of the desorbed <sup>100</sup>solution using UV-visible spectroscopy at 512 nm in conjunction with a calibration graph (see ESI Fig. 1) obtained by using six N719 standards from 0 to 1.0 mM  $(11.82 \text{ mM}^{-1} \text{cm}^{-1})^{29}$ .

 Equilibrium N719 adsorption capacity of N719 was measured for freely-dispersed  $P25$ ,  $P25/ZnO<sub>2</sub>$  powder at seven N719 105 concentrations (25-500 mg/l) at 22, 40 and 50 °C. Adsorbed dye (q) (mg/g) was calculated according to Eqn.  $1^{30}$ 

$$
q = (C_0 - C_e) V/m
$$
 (Eq. 1)

 $_{110}$  where C<sub>0</sub> (mg/L) and C<sub>e</sub> (mg/L) are the initial and equilibrium N719 concentrations (mol  $L^{-1}$ ), respectively, V is the volume of dye solution  $(L)$ , and m is the mass  $TiO<sub>2</sub>$  (mg). Fits to the Langmuir (Eq. 2)<sup>31</sup> or Freundlich isotherms (Eq. 3 and  $4$ )<sup>31,32</sup>

were then calculated by plotting the data according to the relevant equations. For Langmuir,

$$
C_e/q=1/K_L q_m + C_e/q_m \qquad (Eq. 2)
$$

where  $C_e$  is the equilibrium N719 concentration (mg/l), q is the equilibrium adsorption capacity (mg/g),  $q_m$  is the maximum adsorption capacity (mg/g) and  $K<sub>L</sub>$  (L/mg) is the Langmuir constant. For Freundlich, Eq. 3 was converted to the linear form <sup>10</sup>(Eq. 4).

$$
q_e = K_f C_e^{1/n}
$$
 (Eq. 3)

 $(Eq. 4)$ 

 $\ln q_e = \ln K_f + 1/n \ln C_e^{1/n}$ 

15

5

where  $q_e$  is the equilibrium adsorbate concentration (mg/g),  $K_f$  is the Freundlich constant (mg/g),  $C_e$  is the equilibrium solution concentration (mg/l), and 1/n represents dimensionless heterogeneity factor.

#### 20 **Results and Discussion**

To emphasise the importance of the binder within the pastes, two P25/terpineol pastes were prepared; one with ethyl cellulose binder and one without. These were doctor bladed onto glass

25 microscope slides and oven sintered at 450 °C for 30min. Fig. 1 initially suggests that the resultant films appear similar. However, closer inspection of the binder-free film reveals fine cracks and a simple adhesion test of applying Scotch tape to the film and removing it shows that the  $TiO<sub>2</sub>$  arising from the binder-free paste <sup>30</sup>delaminates easily (as denoted by the dashed red box on Fig. 1)

whilst the film from the binder-containing paste remains strongly adhered to the glass substrate.



**Fig. 1** Photographs of films produced by sintering either binder-free or binder-containing P25 pastes at 450 ˚C for 30min; (a) as produced films and (b) after adhesion test using Scotch tape. Binder = ethyl cellulose



**Fig. 2** TGA/DSC data for (a) P25 paste, (b)  $ZnO<sub>2</sub>$  powder and (c) P25/ZnO<sub>2</sub> paste heated from RT to 600 °C at 10°C min<sup>-1</sup>. TGA = solid lines and DSC = dashed lines. Exotherm = up

#### **Thermal chemistry**

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The approach taken in this paper is to lower the sintering temperature of binder-containing pastes by including metal peroxide powders which decompose to produce metal oxide 70 particles and release oxygen and heat within the photo-electrode film during the sintering process.

 Detailed thermal analyses of selected pastes used in this study are shown in Fig. 2 (all the data are shown in the ESI Fig. 2). These TGA/DSC data can be used to explain the principle of the <sup>75</sup>metal peroxide combustion effect. In addition, the challenge of lowering the sintering temperature of metal oxide pastes can be seen by looking at the detailed thermal analysis of a P25 paste (Fig. 2a). The data show a three-stage weight loss for P25-only

pastes with an initial loss of terpineol solvent (*ca.* 70%) between 60 ˚C and 214 ˚C which is associated with an endothermic peak which reaches its minimum at *ca*. 190 °C in line with this being an evaporative rather than a combustion process. The second <sup>5</sup>weight loss (*ca.* 10%, 210-320 ˚C) is associated with a broad, multi-feature exotherm with a shoulder at *ca.* 240 ˚C (labelled **Ia**  on Fig 2a) and two maxima *ca.* 290 and 320 ˚C. These features are associated with the combustion of ethyl cellulose to  $CO<sub>2(e)</sub>$ 

- and  $H_2O_{(g)}$ . Although the final weight loss is small (3%, 320-450) <sup>10</sup>˚C), it is associated with a strong exothermic peaks (maximum at
- *ca.* 410 ˚C) which continues up to 450 ˚C (labelled **IIIa** in Fig. 2a). This is ascribed to the combustion of residual carbonaceous material from the ethyl cellulose binder which, if not combusted, is believed to reduce dye uptake by blocking surface sorption <sup>15</sup>sites. This residual organic matter gives rise to the brown
- colouration in under-sintered films (see Fig. 3). It is key to remove this material to prepare suitable metal oxide surfaces for dyeing. The reason for adding the metal peroxides to the paste is to introduce an oxygen source and heat during binder combustion <sup>20</sup>to accelerate the removal of this residual organic matter.



<sup>25</sup>**Fig. 3** Photograph of films (*ca.* 3x2 cm) prepared from P25 and P25/peroxides (5-15% w/w) binder-containing pastes after sintering for 30min at 300 ˚C

 As such, an initial screening of P25 pastes containing metal 30 peroxides involved mixing either calcium, magnesium or zinc peroxide into a P25/terpineol paste containing ethyl cellulose binder at a loading of 5, 10 or 15% by wt *versus* P25. After casting onto glass slides, the films were sintered up to 250-300 °C for 30-120min. Fig. 3 shows that, after 30 min at 300 °C, the P25 35 control film changes from yellow to brown. Further tests show that the P25-only film becomes white only after heating to 450 °C; this colour change was deemed a suitable visual indicator of complete binder combustion which would prepare the metal

paler than the other films after 30 min but increasing the sintering time up to 120min did not change this. However, sintering these <sup>45</sup>films at 300 ˚C for 30min produces white films for all the P25/peroxide films whilst the P25-only control remains brown (Fig. 3). Hence, 300 ˚C was considered to be the threshold temperature to initiate both metal peroxide decomposition  $(MO<sub>2</sub>)$ becoming MO and  $\frac{1}{2}O_2$  and binder combustion. <sup>50</sup>To explore the reasons for the beneficial effects of metal

peroxide in detail, further TGA/DSC data have been recorded. All the data are presented in the ESI Fig. 2 whilst only the selected data for  $ZnO<sub>2</sub>$  are presented here as these data are representative of all the different metal peroxides tested. Thus,  $55$  TGA/DSC data for powdered  $ZnO<sub>2</sub>(Fig. 2b)$  show a small weight loss (*ca.* 2%) for up to 190 °C and then a very rapid weight loss of *ca.* 16% centred around 200 °C which corresponds to the decomposition of  $ZnO<sub>2</sub>$  into  $ZnO$  (Eq. 5). This is accompanied by a sharp exotherm which is labelled **Ib** in Fig. 2b. This is  $\omega$  important because the  $ZnO<sub>2</sub>$  decomposition occurs at a slightly lower temperature than the temperature at which binder combustion commences (see **IIa** in Fig. 2a). This means that the heat or oxygen released from  $ZnO<sub>2</sub>$  decomposition will be available to enhance binder combustion at lower temperatures. In <sup>65</sup>addition, because the metal peroxide particles are mixed into the pastes, they are subsequently distributed through the printed and sintering films. Hence, as the metal peroxides decompose, they release oxygen and heat to their local environment where the binder residues exist. This reduces any mass transfer issues which <sup>70</sup>further helps to explain the enhanced binder combustion at lower temperatures.

oxide surface area for dyeing. The films from the metal peroxide <sup>40</sup>pastes all show some residual pale brown colour at combustion temperatures up to 250 °C regardless of the metal peroxide loading (see ESI Fig. 3). At 250 °C, the  $P25/CaO<sub>2</sub>$  film appeared

$$
ZnO_{2(s)} \to ZnO_{(s)} + \frac{1}{2}O_{2(g)} \qquad (Eq. 5)
$$

 $75$  These effects are illustrated by the data for a  $P25/ZnO<sub>2</sub>$  paste (Fig. 2c). As expected, the data show a very similar pattern to the P25 paste because the paste only contains  $10\%$   $ZnO<sub>2</sub>$ . However, there is a much more clearly defined and more intense exothermic peak in the DSC signal (labelled **Ic** on Fig. 2c). This reflects the 80 exotherm associated with ZnO<sub>2</sub> decomposition. As predicted, this is believed to have two main effects; firstly additional and localized heat is released within the film and secondly the peroxide decomposing releases oxygen into the film which can help to oxidize the organic binder. This results in a greater loss of 85 residual organic matter from the film at temperatures lower than 450 °C (labelled **IIIc** in Fig. 2c). By comparison, the TGA/DSC data for  $CaO<sub>2</sub>$  and  $MgO<sub>2</sub>$  (see ESI Fig. 2) show that, while they do decompose to produce CaO and MgO, respectively and to release oxygen, the main weight loss takes place at higher temperature  $\mathcal{L}_{90}$  (*ca.* 400 °C). Also, for both CaO<sub>2</sub> and MgO<sub>2</sub>, their decomposition is an endothermic process which will remove energy from the surrounding paste during sintering. Thus, for these peroxides, the localized addition of oxygen should still occur at similar temperatures to binder combustion and therefore should still help <sup>95</sup>this process. However, during any sintering process, the paste

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must be heated from room temperature to the sintering dwell temperature. Hence, the higher decomposition temperatures for  $CaO<sub>2</sub>$  and  $MgO<sub>2</sub>$  means that the oxygen will be released slightly later in the process. Overall, both the higher temperature and  $5$  endothermic nature of the decomposition mean that  $CaO<sub>2</sub>$  and  $MgO<sub>2</sub>$  should be less effective combustion additives compared to

 $ZnO<sub>2</sub>$ .

 Having established that the addition of metal peroxides can reduce the sintering temperature of  $TiO<sub>2</sub>$ -ethyl cellulose pastes, 10 selected films were sintered at different temperatures and sensitized with N719 before being manufactured into dyesensitized solar cell devices as described in the next section.

#### **DSC device data**

- 15 In this paper, we are studying sintering so we have made larger photo-electrodes  $(1 \text{ cm}^2)$  than are typically reported for DSC devices to test film cohesion in devices. $33$  To study reproducibility, we have also made replicate devices and reported the average  $\eta \pm$  the error. Whilst this suppresses device <sup>20</sup>efficiencies relative to the highest efficiencies reported in the literature (e.g. for ball-milled P25 pastes<sup>34,35</sup>), this approach is necessary to accurately test the effectiveness of the different sintering treatments.
- Table 1 shows IV data for replicate devices made using one <sup>25</sup>layer of metal oxide paste (*ca.* 7 µm thickness) after sintering at 300 or 450 °C. The approach taken was to keep photo-electrode thickness constant and vary the type of  $TiO<sub>2</sub>$  particles used in the paste. This was because DSC devices are tending towards thinner electrodes as the molar extinction coefficient (ε) of dyes increase
- <sup>30</sup>and because solid state devices require thinner electrodes. Thus, two different pastes have been studied in these devices; in house prepared P25-ethyl cellulose-terpineol paste which is denoted P25 in Table 1 and a commercial  $TiO<sub>2</sub>$  paste (DSL18NR-T from Dyesol Ltd) which is denoted NRT in Table 1. The data for the
- $35$  TiO<sub>2</sub>-only films P25 sintered at 450 °C can be used as a baseline for the other devices. Thus, Device A for P25-only shows η of 4.4% with  $J_{\rm sc}$  of 9.01 mA cm<sup>-2</sup> and  $V_{\rm oc}$  of 0.71 V. By comparison, Device B gives a better performance  $(\eta = 5.0\%)$  mainly due to an improvement in  $J_{\rm sc}$  up to 9.80 mA.cm<sup>-2</sup>. This is ascribed to the
- <sup>40</sup>DSL18NR-T paste containing smaller, nanoparticulate anatase  $TiO<sub>2</sub>$  particles leading to higher dye loading (see ESI Fig. 4). In addition the DSL18NR-T paste contains no rutile phase whilst P25 does which is known to produce less efficient DSC devices<sup>36</sup>. The DSL18NR-T paste has also been optimized for DSC devices.
- $45$  For the P25/peroxide films sintered at 450 °C, the highest efficiencies are observed for the  $ZnO<sub>2</sub>$  treated pastes. Thus, for P25/ZnO<sub>2</sub> (Device E)  $\eta = 4.4\%$  which is comparable to the P25only device (Device A). By comparison, the  $NRT/ZnO<sub>2</sub>$  data (Device F) again shows a significant improvement over the P25
- <sup>50</sup> and P25/ZnO<sub>2</sub> data with  $η = 5.7%$  which is again mainly due to improved  $J_{sc}$ . However, the NRT/ZnO<sub>2</sub> device also shows a significant improvement compared to Device B which contains only DSL18NR-T with improved efficiency again related to improved  $J_{sc}$ . This is in line with the P25 data which suggests the
- $55$  ZnO<sub>2</sub> provides an additional benefit to the device performance. This may be because the larger  $ZnO<sub>2</sub>$  particles may increase light scattering during device operation and/or that the  $ZnO<sub>2</sub>$  particles

provide an additional benefit during sintering leading to improved surface area and dye loading. Having established the influence of  $\omega$  peroxide on larger devices, some smaller (0.26 cm<sup>2</sup>) devices were

- prepared and ultra-fast dyed with  $N719/SQ1$  cocktail solution<sup>27</sup> to study the effect of increased  $J_{\rm sc}$  on the peroxide photo-electrodes. This showed that device efficiencies of up to  $\eta = 7.5\%$  can be achieved from binder-containing paste sintered at 300 °C (Table
- <sup>65</sup>1) which is comparable with previous reports for this dye system $2^7$ . To the best of our knowledge, the performance of these devices is comparable to the highest efficiency devices reported for DSC fabricated using low temperature methods except that the previous reports used binder-free  $TiO<sub>2</sub>$  pastes and pressure  $70$  rather than thermal sintering<sup>18, 19</sup>.
- Sintering the photo-electrodes at 300 °C shows the importance of the metal peroxide additions. For example, sintering P25-only devices at 300 °C gives very low η regardless of whether TiCl<sup>4</sup> treatment is used ( $\eta$  < 0.3%, Devices F and G); essentially

Table 1 IV data for (1 cm<sup>2</sup>) N719-dyed DSC devices prepared using P25 or P25/peroxide pastes (10% wt/wt). Efficiencies are reported as mean of 3 devices for each condition  $\pm$  error.

	Paste	TiCl <sub>4</sub>	η $(\%)$	FF	$V_{oc}$ / V	$J_{sc}$ $mA cm-2$			
	450 °C								
A	P <sub>25</sub>	Yes	$4.4 \pm 0.2$	0.69	0.71	9.01			
B	<b>NRT</b>	Yes	$5.0 \pm 0.2$	0.65	0.79	9.80			
C	P25/CaO <sub>2</sub>	Yes	$3.4 \pm 0.1$	0.61	0.78	6.85			
D	P25/MgO <sub>2</sub>	Yes	$3.5 \pm 0.1$	0.57	0.78	7.99			
Е	P25/ZnO <sub>2</sub>	Yes	$4.4 \pm 0.1$	0.73	0.78	7.73			
F	NRT/ZnO <sub>2</sub>	Yes	$5.7 \pm 0.2$	0.72	0.77	10.43			
	300 °C								
G	P <sub>25</sub>	Yes	0.3	0.61	0.58	0.82			
Н	P <sub>25</sub>	No	0.0	0.34	0.02	0.20			
I	P25/CaO <sub>2</sub>	Yes	$3.2 \pm 0.2$	0.55	0.79	7.32			
J	P25/MgO <sub>2</sub>	Yes	$3.5 + 0.1$	0.53	0.78	8.32			
K	P25/ZnO <sub>2</sub>	Yes	$4.1 \pm 0.2$	0.72	0.77	7.51			
L	P25/ZnO <sub>2</sub>	No	$1.1 + 0.0$	0.60	0.74	2.53			
М	NRT/ZnO <sub>2</sub>	Yes	$5.7 \pm 0.1$	0.71	0.76	10.62			
N	NRT/ZnO <sub>2</sub>	No	$0.0 + 0.0$	0.00	0.01	0.02			
Ο†	NRT/ZnO <sub>2</sub>	Yes	$7.5 \pm 0.3$	0.67	0.84	13.40			
<sup>†</sup> Cocktail dved (N719/SO1) 0.26 cm <sup>2</sup> device									

 $\mathrm{^{\dagger}Cocktail}$  dyed (N719/SQ1) 0.26 cm<sup>2</sup> device

resulting in non-functional devices. Sintering DSL18NR-T pastes which do not contain  $ZnO<sub>2</sub>$  at 300 °C produces similar device performances; i.e. no efficiency (data not shown). By comparison, sintering P25/metal peroxide films at 300 °C shows 85 similar device performance data to the respective 450 °C sintered films. The highest efficiency for these devices is again observed for P25/ZnO<sub>2</sub> compared to P25/CaO<sub>2</sub> or P25/MgO<sub>2</sub> (Device J *versus* Devices H and I).

The data also show the importance of  $TiCl<sub>4</sub>$  treatment for the  $\omega_9$  metal peroxide-containing films. For P25/ZnO<sub>2</sub> pastes, the addition of a TiCl<sub>4</sub> treatment increases  $\eta$  from 1.1% (Device L, no TiCl<sub>4</sub>) to  $4.1\%$  (Device K, with TiCl<sub>4</sub>). For DSL18NR-T/ZnO<sub>2</sub>

pastes, the effect is even more pronounced with zero η without TiCl<sub>4</sub> treatment (Device N) and  $\eta = 5.7\%$  with TiCl<sub>4</sub> (Device M). For DSL18NR-T, it is hard to compare the data as the absence of TiCl<sup>4</sup> produces a non-functional device. However, for the  $5 \text{ P25/ZnO}_2$  devices, the main reason is  $J_{\text{sc}}$ . This effect is ascribed to the  $TiCl<sub>4</sub>$  treatment hydrolyzing onto the photo-electrode surface

- producing a more coherent  $TiO<sub>2</sub>$  surface for dyeing. Indeed, it is known that  $TiCl<sub>4</sub>$  treatment has little influence on high temperature sintered devices where all organic matter has been
- 10 removed and the particles are thermally well sintered together. However, here the value of the  $TiCl<sub>4</sub>$  effectively repairing photoelectrode defects can be seen. The differences in performance between the P25 and DSL18NR-T pastes may reflect different paste additives which make it more difficult to remove all organic
- 15 matter from the commercial paste at 300 °C. To illustrate the importance of J<sub>sc</sub>, Fig. 4 shows EQE<sub>max</sub> for N719 at 530 nm for a P25 device sintered at 450 °C. By comparison for films sintered at 300 °C, the P25/ZnO<sub>2</sub> device shows EQE of 45% at 530 nm whilst the equivalent P25-only device shows  $EQE < 5\%$ . Finally,
- 20 the data for  $NRT/ZnO_2$  sintered at 300 °C (Device M) shows very similar data to the equivalent device sintered at 450 °C) with  $\eta$  = 5.7%; again an improvement over the NRT-only device sintered at 450 °C (Device B).



<sup>25</sup>**Fig. 4** EQE for P25 films sintered at 300 °C (dotted line), 450 °C (dashed line), and  $P25/ZnO<sub>2</sub>$  (solid line) sintered at 300°C for 30min. All films TiCl4 treated and dyed with N719.

 Transient photovoltage and photocurrent decay measurements have been used to further study the influence of sintering  $_{30}$  temperature, TiCl<sub>4</sub> treatment and  $ZnO<sub>2</sub>$  addition to devices (Fig. 5) and ESI Fig. 5). The data show significantly longer recombination lifetimes for all TiCl<sub>4</sub> treated photo-electrodes compared to their non-TiCl<sub>4</sub> treated analogues. For P25 devices, there is no difference in the transport kinetics which suggests that 35 any increase in  $J_{\rm sc}$  observed as a result of TiCl<sub>4</sub> treatment can be attributed to a downward shift in the conduction band as observed in<sup>37</sup>. For the 300 °C sintered devices however, an apparent decrease in transport kinetics, due to  $TiCl<sub>4</sub>$  treatment, may indicate a change in trap density additional to the negative CB  $40$  shift that is commonly observed as a result of TiCl<sub>4</sub> treatment.

made with  $ZnO<sub>2</sub>$  in the paste suggests that the  $ZnO<sub>2</sub>$  performs a different role to  $TiCl<sub>4</sub>$  in the devices and supports our assertion that the peroxide assists binder combustion and the removal of <sup>45</sup>residual organic material which otherwise acts as recombination sites. The data also show that the 450 °C sintered P25 device without  $ZnO_2$  or  $TiCl_4$  treatment, shows comparable recombination lifetimes to TiCl<sub>4</sub>-treated devices suggesting that TiCl<sup>4</sup> treatment does not significantly affect recombination  $50$  processes for well-sintered TiO<sub>2</sub>-only photo-electrodes which is in line with many literature reports. However, recombination lifetimes shorten for the 450  $^{\circ}$ C sintered ZnO<sub>2</sub>/P25 device without TiCl<sub>4</sub> treatment but are shortest for all the 300  $^{\circ}$ C sintered devices which have not been  $TiCl<sub>4</sub>$  treated. These data  $55$  confirm that both  $ZnO<sub>2</sub>$  and TiCl<sub>4</sub> treatment are required for low temperature sintering to achieve adequate recombination lifetimes for effective charge extraction. Overall, these data show that low temperature sintering of binder-containing  $TiO<sub>2</sub>$  pastes is possible and with careful control to minimize any over-sintering of the  $\omega$  TiO<sub>2</sub> surface can lead to enhanced short-circuit currents. The later materials characterisation work reported in this paper has sought to understand the reasons for these observations.

The large decrease in recombination rate observed in devices



**Fig. 5** Recombination lifetime  $\tau$  *versus*  $V_{\infty}$  for devices sintered at 450 °C - ■ P25 with TiCl4;▲P25 no TiCl4 or at 300 C - ○ P25 with TiCl4; ∆ P25 no TiCl<sub>4</sub>;  $\Box$  ZnO<sub>2</sub>/P25 with TiCl<sub>4</sub>;  $\bullet$  ZnO<sub>2</sub>/P25 no TiCl<sub>4</sub>.

 $\frac{70}{20}$  Studies of varying the paste  $\text{ZnO}_2$  loading from 5 to 25% shows that lower  $ZnO<sub>2</sub>$  loading (5-10%) gives the best device performance (see ESI Table 1). This is mainly due to reduced  $J_{\rm sc}$ as the metal peroxide loading increases which is ascribed to lower dye loadings arising from increased proportion of lower surface  $75$  area  $ZnO<sub>2</sub>$  particles. Studies of extending the sintering time at 300 °C from 30min to 120min (see ESI Table 2) also show a slight negative impact on device efficiency due to slight reductions in  $J_{\rm sc}$  and  $V_{\rm oc}$ . These changes probably reflect increased interactions

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between the zinc oxide and  $TiO<sub>2</sub>$  phases with time which may lead to a loss of surface area and potentially surface doping of each phase into the other.



**Fig. 6** X-ray diffraction pattern of P25/ZnO<sub>2</sub> film sintered at 300  $^{\circ}$ C showing  $\bullet$  anatase TiO<sub>2</sub>,  $\ddagger$  rutile TiO<sub>2</sub> and  $\dagger$  ZnO





Fig. 7 Scanning electron micrographs of ZnO<sub>2</sub>-contaning P25 films sintered at (top) 450 °C and (bottom) 300 °C

#### **Materials Characterisation**

The aim of this part of the work has been to try to understand how the addition of metal peroxides to  $TiO<sub>2</sub>$ -ethyl cellulose pastes affects the phases and morphology of the resulting metal <sup>20</sup>oxides. Their surface chemistry has also been studied using BET and dye loading isotherms because of the strong correlation between device performance and  $J_{\rm sc}$ . Thus, a key aim of this work has been to understand if the completion of sintering and any presence of residual organic matter is linked to surface area and <sup>25</sup>dye loading. Unless otherwise stated, the data for P25-ethyl cellulose pastes containing  $10\%$  ZnO<sub>2</sub> (by wt.) are presented these pastes gave rise to the most efficient DSC devices.

 Firstly, looking at the structural phases present, XRD data show that all the films contain anatase<sup>38</sup> and rutile<sup>39</sup>  $TiO<sub>2</sub>$  phases <sup>30</sup>in approximately 4:1 ratio as expected for P25. The data for a sintered P25/ZnO<sub>2</sub> film (Fig. 6) shows additional peaks at  $31.7^{\circ}$ and 34.4 $\degree$  20, which can be attributed to ZnO<sup>40</sup> resulting from the decomposition of  $ZnO_2$ . The data for P25/CaO<sub>2</sub> or P25/MgO<sub>2</sub> films were essentially identical to the P25-only film with no 35 evidence for the formation of a second metal oxide phase which suggests that the  $CaO<sub>2</sub>$  or  $MgO<sub>2</sub>$  form amorphous products on decomposition (see ESI Fig. 6). The P25-only XRD data also show slight narrowing of the diffraction lines (see ESI Figs. 6 and 7) for films sintered at 450  $^{\circ}$ C compared to 300  $^{\circ}$ C in line with <sup>40</sup>increased crystallinity and inter-particle necking. Interestingly, a similar but subtle effect is seen for the P25/peroxide films sintered at 300 °C. It is difficult to identify the reasons for this with absolute confidence because XRD measures an "average" across the whole sample. However, this might reflect the 45 generation of localized heat during peroxide decomposition as the TGA shows this is an exothermic process. In turn, this might increase  $TiO<sub>2</sub>$  crystallinity and /or might reflect increased interparticle interactions leading to increased crystallite size.

 SEM data (Fig. 7) clearly show two different types of particle <sup>50</sup>interspersed within the film. The majority of particles are *ca.* 25 nm and EDX analysis (see ESI Fig. 8) shows the presence of Ti and O confirming these as  $P25 TiO<sub>2</sub>$  nanoparticles (Fig. 7 - top). The data also show larger irregularly-shaped agglomerations of particles which are 100-300 nm in size and which EDX data <sup>55</sup>show contain Zn and O confirming these to be the ZnO particles arising from the thermal decomposition of  $ZnO<sub>2</sub>$ . Interestingly, the surface morphology of particles appears different dependent on the sintering temperature. Thus, after sintering at 450 °C, the surface appears smooth and the particles singular whilst the 300 <sup>60</sup>°C sintered particles are larger (120-600 nm), have a much more irregular surface and appear to be made up of many smaller particles. This suggests that, whilst the TGA data show that the loss of  $O_2$  from the  $ZnO_2$  occurs rapidly at *ca*. 200 °C, the atomic rearrangement into a more ordered ZnO structure is not complete <sup>65</sup>after 30min at 300 °C.

Sorption data have been measured either using  $N_{2(g)}$  sorption data at -196 °C fitted to the BET model isotherm or using N719 dye solutions sorbed at 22, 40 or 50 °C which have been fitted to model Langmuir or Freundlich isotherms. The dye uptake data <sup>70</sup>have been measured using relatively low initial dye concentrations passively dyed and at equilibrium to study the effects of photo-electrode composition  $(\pm ZnO_2)$  and sintering

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conditions (300 *vs* 450 °C) rather than to optimise sensitization. Thus, fast dyeing<sup>27</sup> higher initial dye concentrations would be expected to show different responses but that is beyond the scope of this paper.  $P25/ZnO<sub>2</sub>$  films were chosen as these devices show <sup>5</sup>the best device responses compared to the P25 or other P25/peroxide films (Table 1).



**Fig. 8** (Top) adsorption isotherms for N719 dyed at 22 ˚C onto (solid line, diamonds) P25 sintered at 450 °C; (dotted line, squares) P25/ZnO<sub>2</sub> sintered at either 450 °C or (dashed line, triangles) at 300 °C and (bottom) the same data fitted to Langmuir isotherms.

The N<sub>2</sub> sorption BET data show a surface area of 54 m<sup>2</sup> g<sup>-1</sup> for P25 sintered a 300 °C which drops to 45  $m^2g^{-1}$  after sintering at 450 °C. This is expected because one aim of the raising the temperature to 450 °C is to sinter particles together and create  $_{20}$  inter-particle necking. This can only be achieved if the TiO<sub>2</sub> surface atoms become mobile. If this occurs, then surface tension will provide a driving force towards smoothing the surface to the

- lowest surface area. In this case, 450 °C is not sufficient to complete this process but is sufficient to sinter the particles  $25$  together. For the P25/ZnO<sub>2</sub> data, a similar trend is observed but with a surface area of 51 m<sup>2</sup>g<sup>-1</sup> at 300 °C and 42 m<sup>2</sup>g<sup>-1</sup> at 450 °C.
- The situation is complicated for these samples partly because they contain a mixture of  $TiO<sub>2</sub>$  particles along with a smaller number of ZnO particles which have resulted from the  $30$  decomposition of  $ZnO<sub>2</sub>$  but also because the surface area
- measurement is an average across the whole. Looking at neat ZnO<sub>2</sub> powder first, this has a surface area of 14  $m^2g^{-1}$  at RT which increases slightly to 18  $m^2g^{-1}$  after sintering at 300 °C but

drops to 7.8  $m^2g^{-1}$  at 450 °C. These trends are typical for a  $35$  material such as  $ZnO<sub>2</sub>$  which releases gas during decomposition as this effectively bursts out of the material creating increased surface area during the process<sup>41</sup>. However, the resultant  $ZnO$ particles sinter rapidly as the temperature is increased further to 450 °C resulting in a subsequent loss of surface area. Thus, whilst  $40$  the "average" surface area for  $P25/ZnO<sub>2</sub>$  might be expected to be slightly lower to reflect the addition of lower surface area  $ZnO<sub>2</sub>$ particles, it is not possible to separate out what is happening to the surface of the  $TiO<sub>2</sub>$  particles alone. In addition,  $N<sub>2</sub>$  will physisorb to residual organic matter and also include this surface <sup>45</sup>area in the data whilst N719 dye will only chemisorb to "free"

metal oxide surfaces. Finally,  $N_2$  is much smaller than N719 so their sorption characteristics will be different. Hence, although the BET data are useful in highlighting trends between organic matter containing under-sintered samples and over-sintered <sup>50</sup>samples (where surface area begins to be lost), dye loading data have been measured and analysed in some detail to provide the most accurate picture of metal oxide surface for dye binding.

 The dye sorption data show relatively higher dye sorption at low initial dye concentration. However, as the initial dye 55 concentration increases, dye sorption increases but to a relatively lesser extent until the data reach a plateau (Fig. 8 - top). This is expected as there are a fixed number of sorption sites in the metal oxide films and, as these become increasingly filled fewer free sites remain, and greater dye concentrations are required to <sup>60</sup>partition more dye onto the surface. However, in these measurements, the dye concentration decreases throughout the experiment as dye adsorbs until equilibrium is reached between the remaining free sites and the remaining dye concentration. Thus, if dye concentration is proportional to the driving force for <sup>65</sup>dye sorption and this drops throughout the sorption process, initial dye concentration should be predictive of final dye loading.

**Table 2** Parameters derived from Langmuir isotherms for N719 dyed at 22, 40 or 50 °C onto P25 sintered at 450 °C or onto P25/ZnO<sub>2</sub> films sintered at 300 or 450 ˚C

Paste	<b>Dyeing</b> temp. $(^{\circ}C)$	$q_m$ (mg/g)	$K_{L}$ (l/mg)	$\mathbf{R}_{\mathrm{L}}$	$\mathbf{R}^2$
	22	47.5	0.021	0.088	0.999
P <sub>25</sub> (450 °C)	40	76.6	0.022	0.082	0.998
	50	85.9	0.030	0.050	0.998
	22	62.1	0.023	0.081	0.999
P25/ZnO <sub>2</sub> (450 °C)	40	88.4	0.029	0.064	0.998
	50	106.3	0.038	0.050	0.997
	22	70.9	0.029	0.064	0.997
P25/ZnO <sub>2</sub> (300 °C)	40	94.8	0.040	0.048	0.997
	50	116.2	0.044	0.043	0.997

Comparing the two isotherm models, the  $R^2$  values are consistently higher when the data are fitted to the Langmuir isotherm ( $R^2 > 0.997$ ) compared to the Freundlich isotherm ( $R^2$ ) 0.962-0.983); see ESI Fig. 9-11 and ESI Tables 3-6. The

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Langmuir model assumes monolayer sorption of adsorbates onto identical sites in separate sorption events whilst the Freundlich model assumes that adsorption takes place on heterogeneous surfaces and is not restricted to monolayer sorption<sup>33</sup>. On the <sup>5</sup>basis of the higher correlations, the Langmuir data have been

used to analyse dye uptake using P25 films sintered at 450 °C as a control to compare to  $P25/ZnO<sub>2</sub>$  films sintered at either 450 or 300 °C.

Firstly comparing P25 and P25/ZnO<sub>2</sub> data sintered at 450 °C, 10 the values for adsorption capacity  $(q_m)$  are consistently higher for the P25/ZnO<sub>2</sub> films which is in line with higher  $J_{\rm sc}$  in these devices (Table 2). This is despite the slightly lower surface area for the  $P25/ZnO<sub>2</sub>$  films measured by N<sub>2</sub> sorption. As discussed previously, the  $N_2$  BET data measures an "average" surface area

- $15$  of the entire sample surface (TiO<sub>2</sub>, ZnO and any residual organic matter). However, we expect the dye sorption data to only measure a monolayer of N719 dye chemisorbed to any available metal oxide surfaces. Thus, we believe the increased dye loading in P25/ZnO<sub>2</sub> samples reflects improved removal of residual
- <sup>20</sup>organic matter from the metal oxide surfaces that improves the metal oxide surfaces for dye uptake. However, the device efficiency data (ESI Table 1) show that increasing the  $ZnO<sub>2</sub>$ loading within the films from 5 to 15 to 25% reduces device performance. This suggests that the increases in dye uptake are
- $25$  associated with improvements to the surface of  $TiO<sub>2</sub>$  particles. This is in line with earlier assertions that the main role of  $ZnO<sub>2</sub>$  is to release oxygen and heat to aid binder combustion which removes organic matter and increases  $TiO<sub>2</sub>$  surface area for dye binding.
- <sup>30</sup>The data in Table 2 also show that adsorption capacity is higher for  $P25/ZnO<sub>2</sub>$  films sintered at 300 °C than P25 or  $P25/ZnO<sub>2</sub>$  sintered at 450 °C. This is to be expected based on the higher BET surface area for  $P25/ZnO<sub>2</sub>$  sintered at 300 °C. However, as discussed previously, the situation is complicated
- <sup>35</sup>because the BET data is an average of all the material in the sample. The increased dye uptake for  $P25/ZnO<sub>2</sub>$  at 300 °C does suggest that the presence of  $ZnO<sub>2</sub>$  results in greater removal of residual organic matter from metal oxide surfaces (which in this sample must be dominated by the much more abundant  $TiO<sub>2</sub>$
- <sup>40</sup>particles). In addition, higher BET surface area and increased dye loading after 300 °C sintering suggests that, as long as residual binder can be removed at lower temperature, the metal oxide particles lose less surfaces area than if sintered at 450 °C. However, this benefit can only be realised in increased dye
- $45$  loading if combustion agent such as  $ZnO<sub>2</sub>$  is added to help combust the residual binder. This beneficial influence on dye loading has not been realised before because it has not been previously been possible to sinter binder-containing pastes at low temperature.
- <sup>50</sup>Table 2 also shows that the N719 adsorption capacity increases on all films with dyeing temperature which suggests an endothermic adsorption process. In practice, solvent volatility limits dyeing temperature and so these data have only been measured up to 50 °C. Low  $R_L$  values indicate favourable dye
- $555$  uptake<sup>30</sup>. The data show that  $R<sub>L</sub>$  values decrease with increasing dyeing temperature and also across the series P25 450 ˚C >  $P25/ZnO_2$  (450 °C) >  $P25/ZnO_2$  (300 °C). Thus,  $P25/ZnO_2$  films

sintered at 300 °C and dyed at 50 °C show the most favourable N719 uptake in line with the highest N719 adsorption capacity. 60 This is in line with the  $J_{sc}$  and η data which suggests that, as expected,  $J_{sc}$  is linked to dye loading (Table 1).

### **Conclusions**

The data show that, for the first time, binder-containing pastes <sup>65</sup>can be sintered at low temperature by using metal peroxide combustion promoters. This has the advantage that metal peroxides are low cost powders which are safe and easy to use within commonly used paste formulations. The most effective metal peroxide when using ethyl cellulose binder-containing  $70$  pastes is  $ZnO_2$  which is believed to be because  $ZnO_2$  decomposes at similar temperatures to ethyl cellulose combustion so that the oxygen released during this process enhances binder combustion and removal as  $CO<sub>2(g)</sub>$  at lower temperature. In addition, the byproducts of  $ZnO<sub>2</sub>$  decomposition are relatively large particles of <sup>75</sup>ZnO which may enhance light scattering within the device whilst not limiting the device because ZnO is used as a photo-anode material in DSC devices in its own right.

 The sorption data show the importance of considering BET surface area data arising from multi-layer  $N_2$  physi-sorption as an <sup>80</sup>average of the whole sample surface area whilst dye loading data relate to chemisorbed dye monolayers. Furthermore, dye loading data after sintering at lower temperatures show, for the first time, that this can actually give rise to higher dye loadings which is linked to the removal of residual binder al lower temperatures <sup>85</sup>along with a reduction in the loss of metal oxide surface area associated with 450 °C sintering. This suggests that sintering at 450 °C actually slightly over-sinters the  $TiO<sub>2</sub>$  resulting in a loss of surface area and lower dye loading. However, it remains important to remove the vast majority (and ideally all) of the <sup>90</sup>organic binder in order to maximize the number of dye binding sites and resulting  $J_{sc}$ . Thus, a general model of sintering would be to sinter at the lowest possible temperature to remove organic material, optimize dye loading and enable inter-particle connections to form to ensure the films are mechanically robust.

## **Acknowledgements**

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We gratefully acknowledge Iraqi Govt. support for DKM, ERDF-WG LCRI funding for SPARC (AC, EWJ, CC), EPSRC SPECIFIC funding (MLD) and Sêr Cymru funding (PJH), Drs <sup>100</sup>Graham Ormondroyd and Simon Curling in the Biocomposites Centre for BET measurements and NSG for supply of TEC™ glass to the SPARC consortium.

# **Notes and references**

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- <sup>110</sup>† Electronic Supplementary Information (ESI) available: [details of any supplementary information available should be included here]. See DOI: 10.1039/b0000000x/
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