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Stability of biodiesel, its improvement and the effect of antioxidant treated blends on engine performance and emission.

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Abstract

Biodiesel consists of long chain fatty acid esters derived from vegetable oils, animal fats, and used oils. Biodiesel contains different types, amounts, and configurations of unsaturated fatty acids, which are prone to oxidation. Biodiesel stability is affected by its interaction with atmospheric oxygen, light, temperature, storage condition, and factors causing sediment formation. It can be classified broadly into three types: oxidation stability, thermal stability, and storage stability. Oxidative degradation occurs in biodiesel upon aerobic contact during storage, as well as contact with metal contaminants. Thermal instability focuses on the oxidation rate at higher temperatures, which is characterized by the formation of insolubles and increase in the weight of oil and fat. Storage stability is concerned with interaction between the physical and chemical characteristics of biodiesel with environmental factors, such as light, metal contamination, color changes, and sediment formation. Antioxidant concentration greatly influences engine performance and emission. The BSFC of biodiesel fuel with antioxidant is less than that of fuel without antioxidant.

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Moreover, an antioxidant can significantly reduce NO_x formation during engine operation. Among the available synthetic antioxidants, only three antioxidants (TBHQ, PY, and PG) can significantly increase biodiesel stability. This article presents an overview of the stability of biodiesel, including the methods available for the prediction of its different stability properties. Feasible remedies to improve the stability of biodiesel and the effect of antioxidants in stabilized blends on engine performance and emission are also discussed.

Keywords: Biodiesel, Oxidation stability, Thermal stability, Storage stability, Performance, Emission, Antioxidant

Nomenclature

ASTM	American standard test method
AV	Acid value
AOM	Active oxygen method
APE	Allylic position equivalent
AH	Antioxidant
AACC	American association of central
	chemists
BHA	Butylated hydroxyanisole
BHT	Butylated hydroxytoluene
BAPE	Bis-allylic position equivalent
BP	Break power
BSFC	Break fuel specific fuel consumption
CO	Carbone monoxide
CA	Citric acid and caffeic acid
DI	Direct injection engine
DPF	Diesel particulate filter
D	Density
DSC	Differential scanning calorimetry
EDTA	Ethylenediamine tetraacetic acid
EHN	Ethylhexyl nitrate
FAME	Fatty acid methyl ester
FFA	Free fatty acid
HC	Hydro carbon
IV	Iodine value
IP	Induction period
NO _x	Nitrogen oxides
OT	Oxidation temperature
OX	oxidizability

OSI	Oil stability index
PDSC	Pressure differential scanning
	calorimetry
PAO	polyalpholefins
PY	Pyrogallol
PG	Propyl gallate
PV	Peroxide value
RIP	Rancimat induction period
TAN	Total acid value
TGA	Thermogravity analysis
TBHQ	Tert-butylhydroquinone
TDI	Terbocharged direct injection
THC	Total hydro carbon
V	viscosity

1. Introduction

Biodiesel is defined as a vegetable oil- or animal fat-based diesel fuel consisting of long chain alkyl esters. Biodiesel is produced by chemically reacting lipids (e.g., vegetable oil, animal fat) with an alcohol to produced fatty acid esters ^{1, 2}. The fatty acid profile of biodiesel corresponds to that of parent oil or fat, which is a key factor that influences its fuel characteristics. The stability of fuel refers to its resistance to the degradation processes that can change its fuel properties and make it inapplicable as a fuel ^{2, 3}. A fuel is considered unstable when it undergoes changes, such as oxidation or autoxidation in the presence of oxygen in ambient air, thermal or thermal-oxidative decomposition because of heat, hydrolysis when in contact with water or moisture in tanks and fuel lines, microbial contamination from water droplets containing bacteria or fungi, or migration of dust particles into the fuel ^{4, 5}.

The stability of biodiesel includes the aspects of oxidation, thermal, and storage stability. Oxidation stability is the tendency of fuels to react with oxygen at ambient temperature ^{6, 7}. Biodiesel degradation prior to combustion in diesel engine is affected by different factors, such as nature of the original lipid feedstock, biodiesel production process, storage and handling

conditions, fuel additives and impurities, conditions within the fuel tank, and fuel distribution system ⁸⁻¹¹. Thermal stability involves the measurement of the tendency of a fuel to produce asphaltenes when exposed to high temperature conditions; asphaltenes are tar-like resinous substances generated in the fuel, and these substances plug the fuel filters of engines when used as fuel ^{12, 13}. The temperature has a significant effect on oxidative degradation because it enhances the rate of degradation. Unstable oxidation products can attack elastomers ¹⁴. The oxidation of biodiesel prompts the development of hydroperoxides, which can assault elastomers or polymerize to form insoluble gums. Oxidation products, such as hydroperoxides and carboxylic acids, can function as plasticizers of elastomers¹⁵.

Storage stability describes the general stability of the fuel under long-term storage. Oxidative degradation is perhaps one of the initial concerns of storage stability, but microbial growth and water contamination are definite issues of storage stability in the long run ¹⁶.

Several previous studies have already investigated the oxidation, thermal, and storage stability of biodiesel ¹⁷⁻¹⁹. Few review articles have analyzed different aspects of biodiesel stability together with the effects of oxidation inhibitors on engine performance and emission^{1, 20-23}. Several test methods have been devised to measure the stability of biodiesel; these methods involve the treatment of fatty oil or ester under elevated temperature, time, and oxygen exposure while measuring one or more oxidation-sensitive properties, such as peroxide value, insolubles, evolution of volatile short chain fatty acids, or heat of reaction ^{20, 24 25}. However, no simple stability test or single stability parameter currently exists to sufficiently indicate all the stability features of biodiesel fuel. A single new test that can completely define biodiesel stability is highly improbable because different tests have various functions. The present paper attempts to review the work conducted on the oxidation, thermal, and storage stability of biodiesel, various test methods, and

improvement of biodiesel stability. This article focuses on a comprehensive study of three different aspects of biodiesel oxidation stability, the methods applied to improve it, effect of oxidation inhibitors (i.e., antioxidants) on stability, and influence of antioxidant-treated blend on diesel engine performance and emission characteristics.

2. Different aspects of biodiesel stability

Biodiesel stability is affected by interactions with atmospheric oxygen, light, temperature, storage conditions, and factors causing sediment formation²⁶. Biodiesel produced from vegetable oils and other feedstocks possess lower stability compared with petroleum-based diesel because of the unsaturated fatty acid content, such as linoleic and linolenic acids, on the fatty acid profile of the parent feedstock²⁷. Biodiesel stability depends on different fatty acid compositions. Most plant-derived fatty oils contain poly-unsaturated fatty acids that are methylene-interrupted rather than conjugated. This structural property is essential to the understanding of the stability. Thus, the instability of biodiesel can be divided into three aspects, namely, oxidative, thermal, and storage instability. The instability of biodiesel is dependent on the quantity and configuration of the olefinic unsaturation in the fatty acid chains.

2.1. Oxidation stability

The oxidation of fatty acid chain is a complex method because of its various applications ²⁸. The oxidation of biodiesel is caused by unsaturation in fatty acid chain and existence of double bonds in the fatty acid molecule, which exhibits high levels of reactivity with O₂, particularly when exposed to air or water. Unsaturated fatty compounds are used to mitigate oxidation stability, because low amounts of more highly unsaturated fatty compounds have a disproportionately strong effect in reducing oxidation stability²⁹. Hence, the oxidation mechanism can be explained by two

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categories, namely, primary oxidation and secondary oxidation. Numerous researchers have investigated the chemistry of primary and secondary oxidation ^{2, 9, 10, 14, 30-48}. Several studies have reported that vinyl polymerization involves higher molecular weight oligomers of fatty oils or ester formation ^{16, 34}. Primary oxidation occurs through a set of reactions categorized as initiation, propagation, and termination ²⁰. As shown in **Fig. 1**, the first set includes the elimination of hydrogen from a carbon atom to make a carbon free radical. If diatomic oxygen is present, the consequent reaction to form a peroxy radical becomes enormously fast, even not allowing substantial alternatives for the carbon-based free radical ^{35, 36}. Carbon free radicals are more active than peroxy free radicals. However, peroxy free radical is adequately reactive to fast abstract hydrogen atom to form another carbon radical and hydroperoxide (ROOH). The newly formed free carbon radical can react with diatomic oxygen and continue the propagation cycle.

Initiation: $RH+I \rightarrow R \cdot + IH$

Propagation: $R \cdot + O_2 \rightarrow ROO \cdot$

 $ROO \cdot + RH \rightarrow ROOH + R \cdot$

Termination: $R \cdot + R \cdot \rightarrow R \cdot R$

 $ROO \cdot + ROO \cdot \rightarrow Stable products$

Fig: 1. Basic oxidation reaction

During the induction period, the ROOH residue concentrations remains low until a certain time interval, and the oxidation stability of fatty acid or biodiesel can be determined under stress conditions ⁵.

For the whole oxidation system, the ROOH level increases very quickly until the initial period is reached ². During the initial period, ROOH can directly or indirectly change the properties of fatty oils and biodiesels ³². The maximum level of ROOH forms at 300–400 meq O₂/kg at any ROOH concentration profile peak, although the level of higher ROOH has been investigated ⁴⁹. The fatty acid reacts with the molecular oxygen and produces unstable peroxide radical (ROO_•), which further reacts with the original substrate RH. The transfer of a hydrogen atom from fatty acids to a peroxide radical will result in the formation of a fatty acid hydroperoxide (ROOH). The radical chain reaction is shown in Eq. (1), in which the reaction with oxygen results in the formation of a new fatty acid radical (R•), because of the addition of fatty acid hydroperoxide (ROOH) and self-sustaining chain reaction.

 $R \cdot + O_2 \longrightarrow ROO \cdot$

$$ROO \bullet + RH \longrightarrow ROOH + R \bullet$$
 (1)

The termination step is achieved when two free radicals react and form stable products, as shown in the following equations.

 $\mathbf{R}^{\bullet} + \mathbf{R}^{\bullet} \longrightarrow \mathbf{R} - \mathbf{R} \tag{2}$

$$ROO \bullet + ROO \bullet \rightarrow stable \text{ products} \tag{3}$$

When an adequate concentration of radical species is available, the probability of two radicals colliding is very high ¹¹. Peroxyl radicals (ROO•) can produce peroxyl-linked molecules(R–OO–R) and liberating oxygen as follows in reaction (4)

$$ROO+ROO \rightarrow R-OO-R+O_2 \tag{4}$$

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The ROOH concentration remains very low during the primary period of oxidation until a certain time interval, and this time period is often referred to as the induction period (IP), The presence of temperature and oxygen pressure during IP is identified by the comparative exposure to oxidation of TAG or alkyl ester, thereby signaling the onset of rapid oxidation; the ROOH level rapidly increases when the IP has elapsed ^{11.} The hydroperoxide (ROOH) levels can either peak and then decrease or increase and plateau at a steady state as oxidation progresses. Although issues, such as extent of earlier oxidation, temperature, oxygen availability, and incidence of metal catalysts, are likely involved in these phenomena, the explanations for the two different activities remain unclear. ROOH disintegration continues because of a peak in ROOH concentration. Insufficient levels of oxygen can slow or even stop ROOH formation. Similarly, different factors, such as higher temperature and presence of hydroperoxide decomposing metal catalysts (e.g., copper and iron), which increase the ROOH decomposition rate, can influence ROOH concentration. At 300-400 meq O₂/kg, maximum ROOH levels typically form ^{2, 11} although higher ROOH levels have been observed 11 Numerous secondary oxidation products, including short chain carboxylic acids, alcohols, high

molecular weight oligomers, and aldehydes, form even at ambient temperature during the secondary oxidation stages, whereas hydroperoxides (ROOH) continue to decompose and interact ⁵⁰. The secondary products are produced in different ways. Several studies reported various secondary oxidation products observed from different experiments using biodiesel, such as 25 different aldehyde compounds during vegetable oil oxidation, including hexenals, heptenals, propane, pentane, and 2,4-heptadienal.^{24,51}. Polymeric species form with the involvement of fatty acid chains. Trimmers or tetramers are smaller than polymeric spices ¹¹, although the open literature does not explain the reason for this difference. Polymer formation increases viscosity.

C–O–C and C–C linkages produce fatty acids, esters, and aliphatic alcohols. Hasenhuettle ¹¹ explained the decomposition mechanism of hydroperoxides to shorter chain fatty acids, such as formic acid. **Table 1.** demonstrates the oxidation stability or IP and unsaturated fatty acid composition for methyl esters of distinctive oils. These data were collected from the literature, and the details of oxidation of a specific biodiesel (ethyl linolate ester) are illustrated in **Fig 2**. Step 1: Hydrogen abstraction from the allyl group. Step 2: Oxygen attack at either end of the radical center, producing intermediate peroxy radicals. Step 3: Monohydroperoxide formation. Step 4: Partial decomposition of the initially formed monohydroperoxides into oxo-products and water.



Fig. 2. Scheme of radical oxidation of ethyl linoleate ester ^{52, 53}

Table 1. Fatty acid composition for different biodiesel and their stabilities.

Sl. no.	Type of Biodiesel	Stabilit y(h)	Saturate d fatty acid	Unsaturate d fatty acid	Ref.
1	Palm	4.0	44.7	55.3	54
2	Olive	3.3	15.7	84.4	54
3	Peanut	2.0	15.6	88.4	40
4	Rape	2.0	6.5	93.6	40
5	Soyben	1.3	15.3	84.7	40
6	Sunflower	0.8	11.1	88.9	40

7	GRAPE	0.5	11.3	88.5	40
8	H.O. Sunflower	1.2	9.3	90.5	40
9	Almond	3.0	13.9	86.4	40
10	Corn	1.2	8	91.7	40
11	Crude palm	25.7	50.6	43.4	55
12	Distilled Palm	3.52	48.73	51.27	41
13	Used frying	3.42	20.1	79.9	56
14	Spent bleaching earths	14.59	41.4	58.6	42
15	Palm	23.33	83.8	9.9	42
16	Croton	4.04	9.6	90.3	57
17	Moringa	5.05	21.6	78.3	43
18	Jatropha	10.43	22.4	77.6	43
19	Undistilled Rapseed	9.1	9.69	90.32	58
20	Distilled rapseed	3.4	6.23	93.64	44
21	Sunflower	3.4	11.7	87.92	44
22	Distilled Sunflower	1.2	11.42	88.58	44
23	Undistilled used frying	5.9	20.25	77.6	44
24	Distilled used	3.5	17.17	80.94	44
25	Beef tallow	1.2	41.11	55.76	44
26	Distilled Tallow	0.4	50.4	45.01	44
27	Safflower	0.86	10.9	89.1	59
28	Jatropha	3.23	21.1	78.9	48
29	Pomngamia	2.35	16	84	48
30	Safflower	1.73	11.6	88.4	48
31	Soyabean	3.8	15.5	84.5	48
32	Soyabean	4.87	23.3	76.7	60
33	Palm	13.37	43.4	56.6	49
34	Crude palm	25.70	50.6	49.22	49
35	Palm	15.4	83.8	9.9	61
36	Soy	1.3	15.3	84.7	50
37	Rapseed	7.8	64.5	29.7	62
38	Ground nut	2.0	15.6	84.4	51
39	Corn	1.2	8.0	91.7	51
40	Pongamia	2.54	16.0	84	51
41	Castor	3.18	3.49	94.58	51

2.1.1. Characterization of oxidation stability

A number of different matrices are characterized for oxidation stability. Different test processes have been developed to determine oxidation stability. Such test methods are categorized based on their application. A single method for identifying the stability of biodiesel is currently unavailable. Some methods can determine the tendency to oxidize materials, and others can specify the level of oxidation products ². The relative resistance to oxidation of a fuel can be assessed over a measured time by monitoring oxidation product levels. Additional elaborate tests to accelerate fuel, such as oxidation, are usually conducted to control oxygen exposure at higher temperatures⁶³. For example, acid levels may be continuously monitored and quantities of filterable insoluble materials may be measured in such tests. Moreover, the rate of the progression of oxidation can be determined.

Different techniques can be used for the characterization of oxidation stability depending on the parameter being measured, such as physical properties, initial fatty oil composition, other parameters indicative of relative stability, primary oxidation products, and secondary oxidation products ². To characterize the oxidation stability of biodiesel, the following techniques can be used ² compositional analysis (gas or liquid chromatography), free and total glycerol content, FFA, various structural indices (such as APE, OX, iodine value, BAPE, and electromagnetic spectroscopy), product levels of primary oxidation (peroxide value), product levels of secondary oxidation (anisidine value, aldehyde content, attendance of quantities of filterable insoluble materials, total acid number and polymer levels), physical properties (density and viscosity), and accelerated oxidation (Rancimat IP or oil stability index and pressurized differential scanning calorimetry). To monitor oxidation progression, few measurements are suitable because the peroxide value initially increases but decreases upon further oxidation as the peroxide reacts to

form secondary products. In most cases, the peroxide value increases with time ³⁹.No perfect test method can identify the characteristics of biodiesel, and the likelihood that any one new test will be able to completely define biodiesel stability is very low ^{11.} Therefore, several measurement test methods are used to adequately characterize oxidation stability, and these methods are discussed below.

(a) Analysis of the IR spectra

The usual determination methods of oxidation stability are slow, tedious, and time consuming, as evident from the aforementioned discussions. Comparatively, IR is an easy, simple, and fast technique for sample analysis. Furlan et al. ⁶⁴ investigated biodiesel oxidation using IR spectroscopy ⁵². In their report, the IR spectra were highly affected by degradation because hydroxyperoxides, alcohol, acids, aldehydes, and ketones formed during oxidation. Given the additional formation of carbonyl groups upon oxidation, monitoring of the band associated with the second harmonic of the carbonyl in the region between 3500 and 3400 per centimeter is helpful to evaluate biodiesel stability. The oxidation of soybean and crambe biodiesel has been analyzed by FTIR measurements, and more carbonyls are formed in soybean biodiesel to thermal stress ⁹.

Conceio et al. ⁶⁵ investigated the thermal and oxidative degradation of castor oil biodiesel ⁵³ based on thermogravimetric and calorimetric profiles. Their group also analyzed spectroscopic data. Castor oil and biodiesel contain ricinoleic acid as the major component, which contains a hydroxyl group and displays additional IR bands at 3440, 850, and 1000 per centimeter. The IR spectrum of degraded samples at 210 °C indicates oxidation by displaying a decrease in the intensity of the bands at 3007 and 724 per centimeter because of the decrease in unsaturation, representing

oxidative polymerization. Both near IR (NIR) and middle IR (MIR) spectroscopy are successful in monitoring the quality and stability of biodiesel and its blends with diesel fuel ^{66-69, 70}. In connection with multivariate calibration, MIR and NIR are employed in analyzing the quality of pure biodiesel (B100) and the transesterification reaction ^{71-74, 75}. Multivariate NIR spectroscopy has been used to evaluate biodiesel stability by analyzing various fuel properties, such as the IV, water content, CFPP, kinematic viscosity, methanol content, density, and AV. ^{47, 51.}

(b) The Active Oxygen Method

AOM is widely used in measuring the oxidation stability parameters. It is most suitable method to measure the peroxide value (PV). In this method, the sample is heated at a certain temperature and continuously bubbled at a particular flow rate. The specific PV is measured at a suitable time when oxidation is initiated and exposed to air. AOM ⁷⁶ is one of the oldest methods to determine the stability of biodiesel. It has been used for 60 years with various modifications⁷⁷⁻⁸². AOM uses a very simple system, in which the oil specimen is heated at an arranged temperature while bubbling waterless air at a fixed rate. The trend in PV varies with time because the peroxides undergo rapid degradation. Thus, PV measurement is not a suitable method for monitoring the oxidation stability. However, AOM is very labor intensive, requires chlorinated solvents, and provides inconsistent findings.

(c) Rancimat method (EN 14112)

The Rancimat method is one of the most effective methods for determining the oxidation stability of biodiesel. For the Rancimat method, FAMEs of the samples are initially oxidized to peroxides as the primary oxidation products. To form the secondary oxidation products, the peroxides are completely decomposed. The decomposition products are mainly composed of formic acid, acetic

acid, volatile organic compounds, and low molecular weight organic acids. Based on the American Oil Chemists' Society (AOCS), the Rancimat method is also the usual and official method for determining the oxidative stability of oils and fats. In this method, the temperature range is usually limited to a maximum of 130 °C ⁸³. In a brief experiment, the sample is first heated at 110 °C. In this process, the oxidation of the sample occurs because the air is bubbled in the sample, thereby releasing some gases with the air. Subsequently, deionized water is passed in the flask. The flask is connected to an electrode to measure the conductivity of the solution. The IP is measured in this process. In this case, the IP is noted as the time at which the conductivity starts to increase very quickly. The continuous measurement of conductivity results in an oxidation curve. The point of inflection in this curve is known as the IP. Volatile acidic gases, such as formic acid, acetic acid, and other acids, are produced by oxidation and absorbed in water, which is the main reason for the increment in conductivity and IP measurement ^{17, 82, 84}. A modified Rancimat test can also be used for the determination of the storage stability of samples ⁸⁵.

Several writers have investigated the work conducted on oxidation stability using the Rancimat test. The BIOSTAB ⁸⁶ project compared ASTM 2274 and Rancimat test, as show in **Fig. 3**



Fig. 3. Comparison between ASTM 2274 and Rancimat induction period⁸²

This project demonstrated the relationship between the filterable adherent and total insolubles with the IP. **Fig. 3** indicates that the total and filterable insolubles exhibit good agreement with the Rancimat IP. For this reason, both methods can be used effectively and interchangeably.

(d) Petro OXY method (ASTM D 7545)

Oxidation stability was determined using Petro OXY equipment from Petro test Instruments GmbH & Co. The experimental conditions were the same as those specified by the ASTM D7545 method (temperature, 140 °C; initial oxygen pressure, 700 kPa; and sample volume, 5 mL). In this method, the oxidation stability of the fuel is directly measured by the time needed to achieve a fixed pressure drop ⁸.

(e) Low pressurized differential scanning calorimetry

The oxidative induction time of biodiesel blends with antioxidants was measured using a pressure differential scanning calorimeter (PDSC; model P-20 Q-DSC from TA Instruments) that was previously calibrated using indium metal as standard ⁸. PDSC analyses were conducted using an open 1101 L platinum pan for sample and reference. Approximately 3.0 mg of sample was employed in each analysis, with static air at 80 psi (551 kPa). The samples were heated from ambient temperature to 110 °C at a heating rate of 10 °C min⁻¹. An isotherm was applied at this temperature until a significant oxidation step of the material occurred ⁴⁹. This step was indicated by a significant exothermic DSC peak, whose respective onset time is called the oxidation induction time ⁵⁹.

2.2. Thermal stability

Thermal stability refers to the stability of a molecule at high temperatures; a highly stable molecule has more resistance to decomposition or oxidation at high temperatures^{3, 8, 14, 26, 87, 88}. At significantly high temperatures, the methylene-separated polyunsaturated olefin structure will begin to isomerize to a more static conjugated structure. Isomerization forms a cyclohexene ring, in which a linked diene group from one fatty acid chain can react with a single olefinic group from another fatty acid chain ^{89, 90}. The Diels Alder reaction is a reaction between a conjugated di-olefin and mono-olefin group **Fig. 4** that becomes significant at 250–300 °C or higher, and the reaction products formed are called dimmers ^{2, 91, 92}.



Fig.4. Diels Alder reaction⁹³

Hence, the Diels Alder reaction also forms trimmers by thermal polymerization with the reaction of an isolated double bond in a dimer side chain with a conjugated diene from another fatty oil⁶⁹. However, a recent study found evidence supporting the non-Diels Alder coupling of two side-chain olefin groups from a dimer and fatty oil molecule ^{32, 68}. Thermal polymerization is characterized by rapid reduction in total unsaturation as all the three olefin groups become one. At 300 °C, initial polymerization resulted in the dramatic reduction in total unsaturation as measured by IV when linseed oil was thermally polymerized.

However, no increase in molecular weight was observed because of an intramolecular Diels Alder reaction between two fatty acid chains in the same triacylglyceride molecule. At temperatures higher than 300 °C, biodiesel produced from used cooking oils when recycled in high-pressure cookers may lead to transesterification to methyl esters and retained linkages. Under such thermal stress, intermolecular dimers also form. Moreover, a di-ester with a molecular weight about twice that of a normal biodiesel ester molecule will be produced. If such biodiesels (i.e., yellow greases) are not purified, these dimers would be present in the final fuel. Nevertheless, no work has reported the incidence of such dimers in recycled cooking oils and if so, their results are mainly on fuel properties of similar non-purified biodiesel fuels. The published literature pertaining to U.S. biodiesel production does not contain the impending existence of such dimeric types in non-purified yellow grease biodiesel ⁶⁹. Thermal polymerization may be of limited importance in biodiesel, which is heated continuously by the engine in the fuel tank before definite combustion. The storage stability of biodiesel is not influenced by thermal polymerization ¹².

2.2.1. Characterization of thermal stability

Different methods from various industries, most notably the fuel and lubricant industries, have been used to assess the oxidative and thermal instability of fatty oils. To determine the thermal stability of biodiesel, the following methods are commonly used: ASTM D 6468, which is the standard test method for high temperature stability of middle distillate fuels ⁹⁴, Rancimat test, which is the procedure specially modified for evaluating thermal stability ⁹⁵ and thermogravimetric analysis/thermal differential analysis (TGA/DTA), which is precise, sensitive, fast, and requires small amounts of samples to measure the thermal stability parameters ⁹⁶. The following test methods are widely used to characterize the thermal stability of oils.

(a) ASTM D 6468-08

ASTM D6468-08 is a method that is highly prominent for the high temperature stability determination of middle distillate fuels (including biodiesel). In this method, the sample is aged at 150 °C in open tubes with air contact for approximately 90 or 180 min. After the aging process, the sample is cooled. The insoluble sediments are then filtered and estimated by the light reflectance method of filter paper. For comparison purposes, a blank is prepared without the sample using an unused filter pad^{82,97}. The filter paper used for this method has a nominal porosity of 11 µm, so it cannot capture all the sediments formed during aging. However, it allows differentiation over a broad range of particle sizes for the sediments. Reflectance measurements can be affected by the color of the filterable insoluble, and they may not be successfully correlated with the mass of the material that is filtered. Thus, the accuracy of this method is not 100%. This method can provide an estimate of the stability of fuel when exposed to high temperatures in certain situations, including a recirculating engine or burner fuel delivery system, and under other high temperature conditions with limited exposure to air. In addition, the test method is also helpful in the study of operational problems related to fuel thermal stability. This method is not suitable for fuels with a flash point less than 38 °C. This test method is also not suitable for fuels containing residual oil, so it is only suitable in estimating the high temperature stability of biodiesel with a very high FAME content. This method can be useful for the observation of operational problems linked to fuel thermal stability. Reflectance decreases with increasing amounts of elements. Thus, the increased quantities of biodiesel polymers result in little or no variation in reflectance because the shapes of particles and polymers have almost no observable color with biodiesel. The test provides correct results when the biodiesel particles/polymers are measured gravimetrically^{70, 73}.

(b) Rancimat method

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The Rancimat method is one of the most effective methods in measuring the thermal stability of biodiesel. In this method, the sample is heated at 200 °C; after 6 h, an 8 g sample is obtained to measure the polymer elements without an airflow ^{62, 71}. ASTM D6468 is one of the most familiar tests for thermal stability, in which the sample is heated at 150 °C for either 90 or 180 min. The sample is then cooled and clarified via a mode similar to ASTM D227490 to determine the filterable via a total reflectance meter or gravimetrically. This method is easy to handle and suitable for use in terms of repeatability ⁶². This process also requires less time. Given that it is modified from D6468-08, it results in comparatively less errors and results in better repeatability. Polymers are used as stability parameters, but no national or international standards are available ^{62, 71}. Chemical structures determine the thermal stability of oils. Saturated oils are more stable than unsaturated fatty acids at high proportion ⁷². Recently, the chemical reaction and thermal stability have been successfully utilized to study the physical properties of oils ⁷².

(c) Thermo gravity analytical methods (TGA or DTA)

TGA or DTA refers to a set of methods in which the thermal activities or thermal properties of a material are measured as a function of temperature. Temperature plays a significant role in the stability of biodiesel, particularly for oxidation stability. In the TGA measurements, the change in value of any parameter is measured with temperature at different conditions. TGA can be performed either in the presence or absence of oxygen. TGA analysis is used for the determination of some of the properties of triglycerides and their derivatives, such as thermo-oxidative behavior, stability, specific heat, degree of unsaturation from melting, crystallization oil profile curves, and high pressure oxidation–IP measurements. The onset temperatures measured from TGA analysis provide the resistance of the sample to thermal oxidative degradation, and a direct correlation

exists between the onset temperature and oxidizability of the sample. The sample becomes easily oxidized with the onset temperature ⁹⁸⁻¹⁰¹. The equipment continuously observes a loss in model weight when the sample is heated in isothermal or energetic situations. To identify different properties, such as specific heat, thermal degeneration stimulation energy, thermo-oxidative activities, and stability, thermal analysis systems have been used for the classification of edible oils and fats ¹⁰²⁻¹⁰⁶, temperature and enthalpy of illustration ¹⁰⁷⁻¹⁰⁹, effects of antioxidants on thermal stability of oils ^{106, 110} analysis of period of unsaturation from melting and end-product of oil ¹¹¹ and high-pressure oxidation phase measurements ¹¹². Based on the high precision and sensitivity of the method, TGA/DTA is widely employed for determining the thermal stability and thermo-oxidation behavior of oil and biodiesel. Thermal stability is directly correlated with the chemical structure of the sample, and the samples with highly unsaturated fatty acids are less stable than the saturated molecules.

2.2.2. Thermal degradation reaction of biodiesel

Oxidation and thermal instability can result in the degradation of biodiesel fuel properties and harm engine performance. Instability is a fundamental consequence of fatty acid chain unsaturation (carbon double bonds C=C). Many polyunsaturated fatty acid chains in vegetable oil are methylene interrupted rather than conjugated. The twofold obligation of unsaturated fats limits the revolution of the hydrogen molecules joined to them. In this way, an unsaturated fatty acid with a twofold bond can exist in two forms, namely, the *cis* structure, in which the two hydrogen atoms are on the same "side," and the *trans* structure, in which the hydrogen atoms are on the inverse sides. *Trans* unsaturated fatty acid, or trans fats, are robust fats produced unintentionally by warming fluid vegetable oils in the presence of metal catalysts and hydrogen. This methodology is termed halfway hydrogenation because carbon particles bond in a straight aspect and stay in a strong state

at room temperature ¹¹³. Physical properties that are sensitive to the effects of fatty oil oxidation include viscosity, refractive index, and dielectric constant. **Fig. 5** indicates the mechanism of peroxy radical formation on a methylene group. In oxidative instability, the methylene group (- CH₂-) carbons between the olefinic carbons are initially attacked ¹¹⁴. The formation of hydroperoxide follows a noted peroxidation chain system. Oxidative lipid adjustments occur through lipid peroxidation systems, in which free radicals and responsive oxygen species produce a methylene hydrogen atom from polyunsaturated unsaturated fatty acids, creating a carbon-focused lipid radical.



Viscosity is one of the crucial properties of biodiesel. The effects of viscosity can be observed in the nature of atomization, ignition, and engine wear. The nature of fuel atomization is fundamentally influenced by viscosity ^{115, 116}. During thermal degradation, the viscosity of biodiesel increases because of the *trans*-isomer arrangement on twofold bonds. Decomposition of biodiesel and its related fatty acids smoothly increase from 293 K to 625 K. The densities of biodiesel fuels diminish linearly from 293 K to 575 K ¹¹⁵. Heat from biodiesel combustion increases when the degree of thermal degradation increases ¹¹⁶. Thermal polymerization of fatty acids is not crucial up to 525 K. Two fatty acid chains are connected by a cyclohexene ring, and thermal polymerization occurs via the Diels Alder reaction. Thus, thermal polymerization of biodiesel can increase its viscosity.

2.3. Storage stability

Storage stability can be defined as the ability of liquid fuel to resist shifts in its physical and chemical properties because of its interactions with its environment ¹¹⁷. Given that oxidation reactions give rise to substances, the stability of biodiesel in storage is critical because it can degrade different parts and materials used in biofuel storage systems. Several writers have observed the activities of biodiesel stored for long time periods in contact with various materials, when exposed and not exposed to light and air. Generally, changes have been reported regarding the IVs, PVs, and AVs, as well as the viscosity, methyl ester content, oxidative stability, and content of insoluble material. The main features for presenting biodiesel and its blends into the market and storage stabilities are characteristic assurance, customer receiving, and standardization. Common diesel fuels are less stable than biodiesel during storage. Feasibility, sustainability, and acceptance are vital issues during storage to protect biodiesel from oxidative degradation. The fuel

quality and engine performance deteriorate during long-term storage, interaction with atmospheric air, and other pro-oxidizing situations because of long-term storage oxidation of unsaturated esters in biodiesel⁸⁹. Upon interacting with variations in color, light, factors caused by residue formation, waste product, and other changes, storage stability may be affected, thereby decreasing the transparency of the fuel ¹². Different writers have studied the effect of biodiesel on the physical properties of the fuel with respect to time, as well as the effects of long-term storage on biodiesel quality ¹¹⁷⁻¹²³. When stored for two years, the heat from combustion decreases but the PV, viscosity, density, and AV of biodiesel increases ^{25,117, 119, 120, 124}. After a year, the viscosity and AV dramatically transforms with changes in the Rancimat IP on the feedstock. Significant growths in the viscosity, PV, free fatty acid, anisidine value, and UV absorption were observed during 90days storage tests ^{27, 30, 89,125}. Moreover, the oxidizability of fatty oils increases with the presence of certain metals, such as Fe, Sn, Ni, Cu, and brass ¹²⁶. Knothe and Dunn ⁹⁸ identified that rapeseed oil (even in 70 ppm) greatly increases the oxidizability of the fuel containing Cu. However, Fe or Ni does not greatly reduce the oxidation stability index (OSI) of methyl oleate compared with Cu. Bondioli et al.²⁵ found that Fe at 40 °C than Fe at 20 °C is a very effective hydroperoxide decomposer, and its effect on methyl esters in rapeseed oil is highly pronounced. Bessee et al.¹²⁷ specified that copper does not increase the total acid number (TAN) of soya methyl ester as much

as Fe.

2.3.1. Test methods to characterize storage stability

(a) ASTM D 4625

Standard test method ASTM D4625 is the most broadly accepted test method for determining the storage stability of central distillate petroleum fuels. The fuel is stored at 43 °C for periods up to 24 weeks. One week of storage in this test is generally accepted as equivalent to one month of storage at 17 °C (65 °F). Normally, a sample is filtered weekly to determine the total insolubles. Whatman GF/F filters (47 mm diameter) are used to test biodiesel. After filtering the aged sample, the filtrate is analyzed for the TAN (ASTM D664) and kinematic viscosity at 40 °C (ASTM D445) ^{2, 89}.

To estimate the long-term storage stability of central distillate petroleum fuels, ASTM D4625 is a very effective method. One week of storage at 43 °C is widely accepted as equivalent to four weeks at 15 °C (underground, ambient storage). When the same relationship has to be confirmed for B100, most investigators are inclined to accept that the relationship holds. Thus, D4625 is an excellent inquiry method, but it is not acceptable as a specification test.

(b) Modifying Rancimat test for storage stability

The Rancimat test may also be used for testing the storage stability of biodiesel. To assess storage stability, the test is amended by the BIOSTAB project ^{128, 129}. In this test, samples of 3 g (neat biodiesel) and 7.5 g (biodiesel blends) are held at 110 °C with a constant air flow of 10 L/h passing through the fuel and into a vessel containing distilled water. The formation of volatile organic acids (mainly formic and acetic acids) in the sample is indicated by an increase in conductivity in the measuring vessel. The time that elapses until the secondary oxidation products are detected is known as the IP. In the modified Rancimat method, several parameters change mainly because of the higher volatility of diesel fuels compared with that of methyl esters, which leads to higher

sample evaporation. The modified Rancimat test is suitable for use in terms of repeatability, significance, and feasibility.

2 (decrease)):

Name of biodiesel	Time of stora	Measured parametres (PV,IV,AV,V,D	Storage limit (month	Method	Remarks	Ref.
	ge, mont h	IP, purity, FAME))			
RME	14	PV↑,AV↑,V↑,D↑	11	EN 14112	RME biofuel in the course	130
SCME	8	$PV\uparrow,AV\uparrow,V\uparrow,D\uparrow$	11	EN 14112	of storage less worse than the properties of fuel	102
WCME	19	PV↑,AV↑,V↑,D↑	11	EN 14112	containing C.satia oil methyl	102
Karanja oil	6	IP \downarrow other constant	4	-	Significant effect in IP	131
Rice brain oil	24	PV↑,IV↓,AV↑,V↑	1	Rancimat	when the test temperature increases a drastic decrease in the induction period	132
POME	3	$AV\uparrow,IP\downarrow,V\uparrow$	1	DSC	Thermal & oxidation	133
JOME	3	AV↑,IP↓,V↑	1	DSC	stability higher.	
Coconut biodiesel	3	AV↑,IP↓,V↑	1			
SOME	12	IP↓ other constant	6	AACC 58- 15	Both V and AV shown the greatest potential in terms of timely and relative ease of measurement.	134
SOEE	1.3mo nth (40 days)	IP↓ other constant	-	EN 14112	low oxidation stability have shown a contamination by some metal ions	135
MOME	12	PV↑, V↑, other constant	-	-	PV &V has significant effect.	136
Canola oil	6.4	FAME concentration↓ other remain same	0.5	-		137
Hiolec sunflowe r oil	30	PV↑, AV↑, IV↓ ,V↑	12	-	friction and wear increase with increasing temperature	138
High erucic brassica oil						
Low erucic brassica oil						

Linseed	2	IP↓	1.4	PDSC	The oxidation stability of biodiesel are deeply impacted by several extrinsic factors and others residual contaminants from the synthesis and storage process.	139
Neat edible rapeseed oil	12	Purity of biodiesel↓	5	TGA	The lowest thermal stability in synthetic air.	140
Tallow oil	2	IP↓	1	supercritica 1	after the exposure for biodiesel initially oxidation	141
lard	2	IP↓	1		in peroxide value	
SBME	6	IP↓	1	EN14112	oxidation stability increase	10
HOSME	6				additives	
RME	6					
JCB	6	IP↑	-	EN14112	To maintain the IP of 6 h for predefined period of time conforming to biodiesel standard specifications Concentration of antioxidants required to be added to biodiesel.	142
Soybean	6	IP↓	6	Rancimat		143

3

JCB: *Jatropha curcus* biodiesel, RME: Rapseed oil methyl ester, SBME: Soybean oil methyl
ester, HOSME: High oleic sunflower methyl ester MOME: Mahua oil methyl ester, SOEE:
Sunflower oilmethyl ester, SOME: Sunflower oil methyl ester, JOME: Jatropha oil methyl
ester, POME: pulm oil methyl ester, WCME: Winter varity C. savita oil methyl ester, SCME:
Spring varity C. savita oil methyl ester.

9 Table 2 shows that the increase in storage time will increase the PV, AV, density, and viscosity,
10 whereas IP decreases in most cases. Therefore, for long-term storage, newly generated
11 biodiesel components upon degradation should be acidic in nature. Such components will
12 always have higher density and viscosity. The optimal storage time of different biodiesels
13 generally varies from one month to 12 months. Further studies should be conducted to clarify
14 the proper storage time that can stabilize various biodiesel properties.

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3. Review of different stabilities of biodiesel

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3.1. Oxidation stability studies of biodiesel

18 Sarin et al. ²⁵ observed the oxidation stability of biodiesel in the presence of metal 19 contamination in *Jatropha* biodiesel, and described a similar influence on the oxidation 20 stability in the presence of small or large metal contamination concentrations, but copper 21 showed the strongest detrimental and catalytic effect on the oxidation stability

Xin et al. ⁵⁹ reported the oxidation stability of rapeseed biodiesel using the supercritical 22 23 methanol method. Their group utilized rapeseed biodiesel as a representative biodiesel to 24 observe the effect of temperature on the tocopherel content in biodiesel. At 270 °C/17 MPa, 300 °C/20 MPa, 330 °C/37 MPa, and 360 °C/47 MPa for 30 min, rapeseed biodiesel was 25 exposed to supercritical methanol, and the remaining tocopherol content of rapeseed biodiesel 26 27 was measured. Their results demonstrated that the remaining tocopherol decreased with the increase in temperature above 300 °C. The increase in temperature significantly reduced the 28 29 tocopherol content. They concluded that tocopherol is not stable at temperatures above 300 °C. Biodiesel has lower stability in supercritical method compared with other methods, such as 30 transesterification^{12, 26, 117, 144}. 31

Knothe and Dunn ¹²⁶ investigated the effect of Cu, Fe, and Ni on the biodiesel stability via IP
measurement of methyl oleate at 90 °C, in which copper resulted in the smallest IP compared

with the other metal-contaminated methyl oleate samples ¹¹⁴. Many researchers have studied 34 the effect of metal contamination on the stability of biodiesel at different conditions and various 35 biodiesels. Jain and Sharma¹⁴⁵ recently investigated the metal contamination effect of *Jatropha* 36 biodiesel with and without antioxidant. Their group used different metals, such as Fe, Ni, Mn, 37 Co, and Cu, in varying concentrations. These different metal concentrations were mixed with 38 biodiesel, and their storage stability was analyzed. The concentration of antioxidants that 39 effectively increases the stability of samples containing different metal contaminants differs. 40 In this study, pyrogallol (PY) was used because it is one of the best antioxidants for stabilizing 41 42 biodiesel without metal contaminants.

43

3.2. Thermal stability studies of biodiesel

Many studies have investigated the thermal stability of biodiesel, as well as the effects of 44 temperature on the stability of biodiesel. Dunn ¹² studied the effects of biodiesel temperature 45 on the OSI, and described that the oxidation reaction occurs rapidly by increasing the 46 temperature and decreasing the OSI of FAME. Monvem et al.²⁷ inspected the thermal stability 47 of biodiesel under different conditions, and reported an increase in the viscosity of the fuel 48 because the oxidation process accelerated with increasing temperature. Polavka et al. 146 49 50 studied the oxidation IP, which is dependent on temperature. Using the Arrhenius equation, they found that the IP of oxidation varies with temperature. Hiroaki et al. ⁶⁵ evaluated the 51 52 thermal stability, and found that only methyl linolenate undergoes a slight change in *cis-trans* 53 isomerization at 2708 C/17 MPa without affecting the biodiesel yield, and poly-unsaturated fatty acid methyl esters, such as methyl linoleate (18:2) and methyl linolenate (18:3), are 54 extensively decomposed at 3508 C/43 MPa, accompanied with isomerization of cis-type 55 double bonds into trans-type at 3508 C/43 MPa in supercritical methanol. Dunn ¹⁴⁷ observed 56 the effects of oxidation under accelerated conditions on the fuel properties of soyate, and found 57 that the increase in various biodiesel properties, such as viscosity, PV, and AV, is caused by 58

59 the increasing temperature. Hence, very little effect was observed for the cold flow properties at temperatures up to 150 °C on the specific gravity. As the reaction temperature increases, the 60 viscosity also increases linearly. The Diels Alder reaction results in the formation of polymers 61 62 at high temperatures, so the viscosity increases. Meanwhile, AV decreases linearly with increasing reaction temperature, and thermal degradation is responsible for the increase in AV 63 with increasing temperature. The PV decreases linearly, whereas the reaction temperature 64 increases, possibly because of the absence of oxygen or accelerated decomposition of 65 hydroperoxides with increasing temperature. 66

67

Dunn¹² studied the temperature effect on the stability of biodiesel, and described that 68 temperature significantly affects the OSI. By increasing the temperature, the oxidation reaction 69 70 occurs rapidly and OSI decreases. Dunn reported that the polymer formation rate increases, and the viscosity and AV increase, whereas the PV decreases at higher temperatures, resulting 71 in decreased OSI ¹²¹. Nzikou et al. ¹⁰⁵ evaluated the thermal stability of vegetable oils while 72 73 frying, and found that the content of linoleic acid decreased with the increase in time of frying oil, which occurred because of rapid oxidation. The formation of high molecular weight 74 polymers causes the viscosity of oil to increase with the increase in frying hour. A high 75 viscosity in frying oil results in a high degree of deterioration ¹⁰⁵ this result is in agreement 76 with the findings of Dunn 121 . 77

Xin et al. ¹⁴ observed the temperature effect on safflower oil during IP, and found that the IP decreases rising temperature. Bondioli et al.²⁶ analyzed the storage stability of biodiesel at different temperatures. During their experiment, samples were kept at two different temperatures (20 °C and 40 °C), and their results demonstrated that the PV was higher at lower temperatures at the same container.

- 83 Therefore, based on these lines of evidence, supercritical methanol treatment lower than 3008
- ^oC, preferably 2708 ^oC with a pressure higher than 8.09 MPa, was concluded to be appropriate
- 85 in maintaining the maximal yield and thermal stabilization of biodiesel.

86

3.3. Storage stability studies of biodiesel

Bondioli et al. ²⁶ and Thompson et al. ⁹⁷ have investigated the corrosion of methyl esters in 87 rapeseed oil, and found that AV, PV, and viscosity increase with time under various storage 88 conditions⁸⁹. Different authors⁹⁸ have studied natural antioxidants, such as tocopherol, and a 89 relationship between the oxidation stability and quantity of tocopherol was found. Bouaid et 90 al.⁸⁹ studied the long-term storage stability of biodiesel from high oleic sunflower oil using 91 frying oil, and found that the IV decreases with rising storage time, whereas the AV, PV, and 92 viscosity increase. Meanwhile, McCormick et al. ³⁸ found that polyunsaturated contents have 93 94 the longest effects on biodiesel stability because of the increased insoluble formation and reduction in the generation period. 95

Das et al.¹³ observed the oxidative stability of karanja oil ME (KOME) via storing the sample 96 inside a room at open air and exposing it to metal and air. They found that the viscosity and 97 PV decrease with increasing storage time, thereby decreasing the oxidative stability of KOME 98 and increasing oxidative degradation, despite the high PV and viscosity. Antioxidants 99 significantly affect KOME. By increasing the concentration of the antioxidant [propyl gallate 100 101 (PG), butylated hydroxyanisole (BHA), and butylated hydroxytoluene (BHT)] with changing load, the stability of KOME increases, and PG is the best antioxidant for KOME, followed by 102 BHA and BHT. Geller et al. ⁹² investigated the storage stability of poultry fat and diesel fuel, 103 which are liable for the corrosive effect of fuels on various metals, with respect to the 104 separation, dynamic viscosity, sedimentation accumulation, and specific gravity. At a storage 105 time of over one year, the viscosity and specific gravity slightly change, and the addition of 106 107 100% antioxidant minimizes the physical properties and sedimentation.

For perfect mixing followed by homogenization, mixing should be very fast and within the suggested time before the fuels are utilized. Regarding the corrosive properties, brass and copper were found to be susceptible to attack by biofuels, whereas 316 stainless steel and carbon steel were not attacked by biofuels. Sarin et al. ⁹¹ reported that the concentration of metal contamination (more or less) in *Jatropha* biodiesel has the same influence on oxidation stability; the oxidation stability of copper shows the strongest detrimental and catalytic effects.

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4. Techniques to improve the stability of biodiesel

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4.1. Purifying during production

117 To improve the biodiesel stability, some processes are necessary to meet the biodiesel's specification for stability under various conditions. Biodiesel consists of fatty acid monoalkyl 118 ester, which is normally produced by transesterification reaction ¹⁴⁸. Technology development 119 should be geared toward better process innovations and the processing of biodiesel ¹⁴⁹. Raw 120 materials and other elements first have to be managed to confirm the quality of biodiesel. Some 121 crude vegetable oils contain phospholipids, which are harmful to biodiesel, thus, such oils have 122 to be eliminated via hydration processes ⁷⁵. Deodorization is the most effective refining process 123 124 in removing unwanted odor and test forms in oil. Therefore, free fatty acids, ketones, aldehydes, and unsaturated hydrocarbons, all of which can cause undesirable smells and flavors 125 of the oil, can be removed via deodorization ¹⁵⁰. Iodine as a catalyst can reduce the high AV of 126 free fatty acids. Transesterification is catalyzed by either homogeneous reagent or 127 heterogeneous reagent. Homogeneous reagents include potassium hydroxide, hydrochloric 128 acid, sodium hydroxide, and sulfuric acid, whereas heterogeneous reagents are enzymes, 129 heterogenized on organic polymers, alkaline earth metal compounds, anion exchange resins 130 titanium silicates, and guanidine. During storage with air, the alkali homogeneous catalysts are 131

extremely hygroscopic ¹⁵¹. Thus, the alkali homogeneous catalysts should be appropriately 132 handled. The alcohol materials, such as methanol, amyl alcohol, ethanol, propanol, and butanol, 133 are used in the transesterification process. At the end of transesterification, alcohol and glycerol 134 are eliminated from the selected product esters by water washing^{124, 152}. The use of membrane 135 technology for the separation and refining of biodiesel eliminates water washing and results in 136 a realistic amount of time and energy depletion ¹⁵³. Cooke et al. ¹⁵⁴ observed that ion 137 interchange resin can eliminate impurities. Gabelman and Hwang¹⁵⁵ found that hollow fiber 138 membrane abstraction can be used effectively to eliminate contaminants. These methodologies 139 effectively avoid losses in the biodiesel yield, decrease the manufacturing steps, and increase 140 the properties of fuel. 141

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3 **4.2. Adding of different additives**

Several researchers ^{14,156-158} have studied biodiesel stability in the presence of additives. Two 144 types of antioxidants are generally used: chain breakers and hydroperoxide decomposers. 145 Phenol and amine are the two most familiar types of chain-breaking antioxidants ¹³². Generally, 146 antioxidants are highly effective for maintaining biodiesel stability under different conditions. 147 148 Antioxidants can prevent the oxidation process, and they are well recognized for maintaining the oxidation of biodiesel. For instance, antioxidant (AH) intercepts the peroxide radical 149 (RCOO.) to prevent it from generating another radical by the autoxidation appliance. The 150 associated mechanism is as follows ²: 151

154 Most studies on the stability of fatty oil and ester uses are restricted to the phenolic type of antioxidants. The necessity of phenolic antioxidants depends on the number of 155 hydroxyl/phenolic groups involved to its ortho and pera positions, i.e., 1 and 2 or 1 and 4 156 positions in an aromatic ring. For the suspension of the oxidation rate, protons, which are 157 delivered by an active hydroxyl group, can prevent the formation of free radicals or interject 158 the dissemination of free radicals. Antioxidants are described by their molecular structure. 159 Therefore, the effectiveness of tert-butylhydroxyquinone (TBHQ), PG, and PY can be 160 described based on their molecular structure. These additives possess two OH sets attached to 161 162 the aromatic ring, when both BHT and BHA possess one OH group on the aromatic ring. Thus, based on their electro negativities, TBHQ, PG, and PY offer more sites to form a complex 163 between the free radical and antioxidant radical for the stabilization of the ester chain ¹⁵⁹. 164

Antioxidants are reused for delaying oxidation. From the literature reviews, antioxidants 165 166 effectively improve the stability of biodiesel under various conditions. Different additives are used in various conditions for the improvement of biodiesel stability⁴. Many antioxidants can 167 markedly increase biodiesel stability. Among them, TBHQ is the most effective antioxidant for 168 soybean, Jatropha, palm, and sunflower biodiesel. BHT, PG, and BHA are also found to be 169 effective for most biodiesels ¹⁶⁰. The application of several antioxidants can enhance the fuel 170 171 stability up to the standard specification. The additive concentration may vary at different conditions because of the unsaturation concentration and composition of various biodiesel and 172 biodiesel blends ¹⁶¹. However, many possible scopes of study can be explored to understand 173 174 the effectiveness of different additives in enhancing corrosion resistance and stability, as well as the fuel properties of different biodiesels. 175

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4.2.1. Chemistry of Antioxidant

Antioxidants play a significant role in biodiesel degradation. As indicated by their mode of 178 activity, antioxidants can be classified as follows: primary antioxidants, such as free radical 179 180 terminators; oxygen scavengers that react with oxygen in closed frameworks; or metal particle chelators that catalyze lipid oxidation ¹⁶². To change them to more steady primary antioxidants, 181 they should react with highly vital lipid radicals. Hence, the group of free radical eliminators, 182 183 such as the phenolic antioxidant (AH), is the most utilized antioxidant. Secondary antioxidants function by retarding the rate of chain initiation by decomposing hydroperoxides. Bolland et 184 al. ¹⁶³ first investigated the activity of antioxidants, in which they hypothesized reactions 5 and 185 6 with the expectation of complimentary radical terminators. In oxidation process reactions 5 186 and 6, the free radical terminators have the most capable hydrogen atoms, which are very fast 187 compared with peroxyl ¹⁶⁴. The latter reactions, 7 and 8, compete with the chain propagation 188 reaction. Naturally, these reactions are exothermic. With the increase in separation vitality of 189 A-H and R-H, the initiation vitality of these reactions increases. As the bond quality of A-H 190 diminishes, the productivity of antioxidants increases¹⁶⁵. 191

192	ROO• + AH —	\rightarrow	ROOH + $A \bullet$	(5)

193

194	RO•	+ AH	\longrightarrow	$ROH + A \bullet$	(6)

195

197

196 $ROO \bullet + A \bullet \longrightarrow ROOA$ (7)

198 $RO \bullet + A \bullet \longrightarrow ROA$ (8)

Reaction 9 shows the valence bond of isomers, which is the stabilization of phenoxy radicaland occurs because of the delocalization of unpaired electrons around the aromatic ring.

Hydrogen substitution by alkyl assembles in ortho- and *para*- position, and expands the
electron density of the OH moiety by inductive impact ¹⁶⁵.



R = *tert*-butyl

TBHQ is economically accessible as a beige-hued powder, and it is a sufficient solvent in fats.
As a diphenolic antioxidant, TBHQ reacts with peroxyl radicals to structure a semiquinone
reverberation half and half. The semiquinone-organized radical intermediates may experience
distinct responses to structure more steady items. They can also react with each other to deliver
dimers, dismutate, and recover semiquinone. They can react with an alternate peroxyl radical,
as indicated in reactions 14, 15, and 16¹⁶⁵.

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Based on their labile hydrogen, the phenolic antioxidant can be positioned as $BHA \approx BHT < DTBHQ \approx TBHQ < PG \approx PY$, which is relevant to some edible oil-based biodiesels. An alternate crucial antioxidant is amine, which can be categorized as a free radical terminator.

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4.2.2. Antioxidants effect on stability of biodiesel

Several methods are available to prevent oxidation or decelerate its rate. By avoiding contact with oxidizing conditions, as well as decreasing air contact, storage in a dark room in stable containers and low temperatures at inert conditions are highly effective for the prevention of

biodiesel oxidation ¹⁶⁹. However, the above conditions are difficult to achieve, and the use of 251 chemicals is of considerable concern. The use of antioxidants is the most active and commercial 252 method available to effectively increase the oxidative stability of biodiesel and its blends. 253 254 Through the extension of the IP, antioxidants have an enhanced role in delaying oxidation. The most common antioxidants are chain breakers (peroxide radical quenchers) and hydroperoxide 255 decomposers (reducing agents) ¹³⁵. Hydroperoxides react with the antioxidants of 256 hydroperoxide decomposers and then convert them to alcohols. Hence, harmless oxidation 257 forms from the antioxidant. Metal chelating agents and acid neutralizers are other categories of 258 antioxidants ¹⁷⁰. The synthetic antioxidants provide higher effectiveness compared with 259 tocopherols when they are added to biodiesel. Another effective natural antioxidant is cardanol 260 oil, which is extracted from cashew nut shell liquid ¹⁷¹ citric acid and caffeic acid are other 261 naturally derived antioxidants that are used as biodiesel stabilizers ¹⁷². Photo-oxidation is 262 influenced by quenchers of singlet oxygen, such as β -carotene. The major synthetic 263 antioxidants are BHT, BHA, TBHQ, PY (i.e., 1, 2, 3-trihydroxybenzene), and PG (i.e., propyl 264 3, 4, 5-trihydroxybenzoate) ¹⁶⁶. Baynoxs is a commercially available synthetic antioxidant 265 widely used for the storage of biodiesel ¹⁷³ BHA, BHT, PG, and vitamin E are chain breakers, 266 whereas sulfides and phosphides are peroxide destroyers ¹⁷⁴. 267



Propyl gallate (PG) tert-butylhydroxyquinone (TBHQ) tert-butylhydroxy toluene (BHT
 Fig: 4 Chemical structures of different antioxidants ¹⁷⁵

Antioxidant occurs naturally, such as vitamin E (i.e., tocopherols and tocotrienols). The four species in each α , β , γ , and δ exist or the synthetic antioxidant materials are deliberately added, such as PG, BHT, TBHQ, PY, and BHA. The refining process influences the level of natural antioxidants in vegetable oil. Early reports stated that the most effective synthetic antioxidants are pyrimidinols, which have strong electron-donating dialkylamino groups ¹⁷⁶. To interrupt the chain reaction, the phenol and amine antioxidants donate the hydrogen atom; phynols go to

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276 quinones and react with a radical in an additive fashion. For proper solubility and utility, the levels of synthetic antioxidant that are normally used are in the range of 100–200 ppm, and the 277 antioxidant with the lowest solubility is PG. Different factors, such as storage, amount of 278 279 naturally occurring antioxidant, oil fatty acid profile, and other conditions, influence the utility of antioxidants. Primary and secondary antioxidants are used in the system; they can influence 280 their effectiveness via synergistic effects between the antioxidant. Meanwhile, amino acid, 281 citric acid, ethylenediamine tetraacetic acid, and phosphoric acid function as secondary 282 antioxidants and help in removing metal ions with different materials, including chelating 283 284 agents. Oxygen scavengers or reducing agents, such as ascorbic acid, which can regenerate spent antioxidants, and singlet oxygen quenchers, such as β -carotene, are also used as oxidation 285 inhibitors. The activity of each antioxidant on biodiesel is different with various feedstocks, 286 FAME composition, and oxidative stability ^{177,178}. Biodiesel stability increases with the 287 addition of antioxidants and varies with the antioxidant concentration. Metal contamination 288 also influences stability. Hence, various metal containers are used for biodiesel storage. To 289 290 increase the oxidation stability of biodiesel, various techniques have been used, such as fractional crystallization or hydrogenation, for reducing the unsaturated fatty acid content in 291 oil. With the variations in the molecular weight structure, BHA and BHT are less effective 292 compared with PY, TBHQ, and GA. The effects of the antioxidants on the oxidative stability 293 of biodiesel mainly depend on the group; maximum antioxidant has two hydroxyl groups, but 294 295 BHT and BHA have only one group with an aromatic ring. Thus, BHT and BHT are less effective on biodiesel stability ¹⁷⁹. Meanwhile, TBHQ and PY are strongly effective on the 296 biodiesel stability, and they are more active in the development of a complex between the free 297 radical of the sample antioxidant ^{180, 181}. Methyl ester stabilization in biodiesel is responsible 298 for its complexity. Antioxidants also influence the viscosity of biodiesel. During storage of 299 oxidized compounds, viscosity increases because of the addition of antioxidants in biodiesel; 300

301 thus, for long-term storage, viscosity in biodiesel affects stability. However, the addition of proper concentrations of antioxidants, such as PG, BHT, and BHA (1000 ppm), causes the 302 viscosity of biodiesel to remain under the ASTM limit (1.9–6 cSt)¹⁸². Table 3 lists the selected 303 studies on the evaluation of biodiesel oxidation stability upon antioxidant addition. It also 304 shows that the most effective synthetic antioxidant is TBHQ, followed by PY and PG. In the 305 306 literature, BHA and BHT are found to be less effective. However, based on the table, synthetic antioxidants are more significantly effective than natural antioxidants, such as different 307 tocopherols and vitamin E. Much work has been conducted on the mechanism of oil and fat 308 309 degradation based on the above literature review.

Biodiesel	Antioxidant order	Stability effect	Concent ration (ppm)	Remarks	Ref.
Karanja oil	PY>PG>BHA>BHT>TBHQ	Oxidation stability ↑with ↑of antioxidant	300,500, 700,1000	PY retain for all concentration	145
Neat jatropha	TBHQ>BHT>TBP>OBPA>α-T	Oxidative stability ↑with ↑of antioxidant	1000	600ppm of natural AO α-T is needed for improve IP	116
Jatropha curcus	PY>PG>TBHQ>BHT>BHA	Thermal stability ↑with ↑of antioxidant	1000	To meet EN 14112 spcification 100ppm of PY is required minimum concentration	73
Jatropha oil	PG>TBHQ>BHA	PG is suitable for Long term oxidation		For 150 ppm PG decrease the IP	183
(Rapseedoil, sunflower oil, frying oil, beef tallow oil) (undistilled	TBHQ>PG>PY>BHA>BHT PY>PG>BHA>TBHQ>BHT PY>PG>TBHQ>BHA>BHT PY>PG>TBHQ>BHA>BHT PY>PG>TBHQ>BHA>BHT TBHQ>PG>BHA>PY>BHT PY>TBHQ>PG>BHA>BHT PG>PY>TBHQ>BHT>BHA	BHT has no effect except Tallow ME (distilled)	1000	Antioxidant concentration were varied from 100 to 1000 mg/kg	184
& distilled) Rapseed oil & tallow	BHA~ BHT&BHT>BHA	IP↑ with ↑of antioxidant concentrati	400	Rate of deactivitation increase with unsaturation in the oil	185
Mahua oil	PG>BHA>BHT	The use of antioxidant s improved the stability significantl	1000	PV & Viscosity increase over the time	186
Soyaben oil Soyaben oil	BHT>BHA>TBHQ TBHQ>BHT>BHA	TBHQ displayed a greater stabilizing potential when used in higher concentrati	1000 7000	From 200 to 7000 ppm BHT displayed the greatest efficacy in concentrations ranging	187
Distilled &crude Palm oil	TBH>BHT>α-tocopherol.	ons. BHT and TBHQ are found to be more effective than	-	At the same dosage TBHQ is more effective compared to BHT	188

310 Table 3: Impact of the use of antioxidant for the oxidation stability of biodiesel

		natural antioxidant			
Waste cooking oil	BPH>BHT	Oxidation stability ↑ with ↑of antioxidant concentrati	600	BPH was more effective than BHT and could be used as a antioxidant	189
Terminalia oil	PG>PY>TBHQ>BHT>BHA>α- tocopherols	Storage stability depends mainly on the antioxidant type and concentrati on	1500	Stability can be upgraded up to 12 times by 1000 ppm PG	190
Croton oil	PY> PG>BHT	 ↑ in dosage of antioxidant s ↑oxidation stability 	1000	To improve the oxidation stability of COME synthetic antioxidants was required.	191
Cotton seed oil	ТВНQ	Oxidative stability increases linearly with the amount of antioxidant	1000	The addition of 300 mg kg^{-1} TBH Q was sufficient to attend the oxidation stability parameter	192

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4.3. Modification of storage conditions

The stability of biodiesel can be increased by modifying storage conditions. Biodiesel can be 314 stored in different ways, and different factors influence biodiesel stability during storage, such 315 as oxidative stability, solvency of fuel, and compatibility of materials ^{193, 156, 194, 157}. Lee et al. 316 ^{195, 158} studied the storage condition of biodiesel in different ways, and concluded that the 317 storage temperature should be between 7 °C and 10 °C to protect pure biodiesel from oxidation. 318 By contrast, the extreme cold weather underground storage of pure biodiesel needs an 319 optimized storage temperature to avoid crystal formation ^{196, 159}. Biodiesel should be stored 320 appropriately because the environment affects the different elements that can degrade biodiesel 321 and reduce its stability. For more than six months of storage, pure biodiesel and its blends 322 require appropriate antioxidants because antioxidants have different characteristics that can 323 increase biodiesel stability. Contamination from water may lead to biological progress in the 324 fuel, so biocides that can prevent water contamination in the fuel should be used. Aluminum, 325 326 steel, polypropylene or fluorinated polyethylene, and Teflon are the main containers for biodiesel storage ¹⁹⁷. Aluminum is the most suitable container for biodiesel storage because it 327 has no catalytic effect on biodiesel. In summary, biodiesel degradation can be affected by 328 temperature and air coverage, which are major important features affecting degradation. The 329 degradation rate increases significantly when biodiesel is stored in environments with high 330 temperature and ambient air exposure. However, the temperature or air exposure alone has 331 minimal effects on biodiesel degradation. The water content in biodiesel will increase biodiesel 332 degradation because of hydrolysis, but its consequence is much less than that of the other 333 334 factors. The aforementioned factors should be studied in detail, particularly for long-term biodiesel storage ^{157.} The tanks should minimize the presence of water impurities, and should 335 be thoroughly cleaned prior to use for biodiesel storage 23 . 336

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5. Effect of stabilized biends of engine performance & emission	338	5.	Effect of stabilized	l blends on	engine	performance	& emission
-----------------------------------------------------------------	-----	----	----------------------	-------------	--------	-------------	------------

Numerous studies on the performance and emission analyses of biodiesel or mixed biodiesel-339 fueled diesel engine are accessible ^{198-201,160-163}. However, reports on the management of the 340 performance and emission of antioxidant prevention agent in biodiesel-fueled engines are 341 limited. Antioxidants demonstrate slight (either expand or abatement) effects on the engine 342 performance and fuel properties. Biodiesel is attracting interest as an eco-accommodating fuel, 343 so elements influencing its ignition and emission are essential. Investigations on the part of 344 antioxidants in compound contamination of biodiesel-fueled engines demonstrated that the 345 346 determination of the antioxidant additive substance to biodiesel is imperative in evaluating pollutants. In the report of Suyin Gan and Hoon Kiat Ng, the effect of antioxidant addition to 347 biodiesel on engine emission was examined in the mixtures of palm oil biodiesel with diesel 348 (B10 and B20)^{164,202}. Among the examined antioxidants (i.e., BHT, BHA, and TBHQ), 349 decreased NO emission has been shown by BHA and TBHQ; however, their high concentration 350 in the fuel blends expands the NO levels. Additionally, BHA can even decrease CO emission, 351 but the two other antioxidants are unable to do so. Kivevele et al. observed that the addition of 352 1000 ppm PY antioxidants to croton oil methyl ester exerts a negligible influence on engine 353 exhaust emissions ^{165,203}. The emission of CO, NO_x, total hydrocarbons, and smoke decreases 354 or expands based on the applied load. The effect of antioxidants BHA, BHT, TBHQ, and 2-355 ethylhexyl nitrate (EHN) on the engine performance and fume gas outflow of canola oil methyl 356 ester mix (B20) was researched by Erol Ileri and Gunnur Kocar ^{166,204}. NO_X emission was 357 observed to decrease upon antioxidant addition, whereas the CO level expanded. EHN was the 358 most effective in decreasing NOx, and TBHQ showed minimal evolution of CO. Jain and 359 Sharma ^{167, 205} analyzed the emission of *Jatropha* biodiesel-fueled diesel engine, and found that 360 the additive PY has minimal effects on the emission. The exhaust of CO and THC slightly 361 decreases, whereas NOx formation slightly increases or decreases with engine load ¹⁶⁷. 362

363 Analysis on the emission of soybean biodiesel-fueled engine showed that the antioxidants have no effects on the engine exhaust ^{168,206}. The use of antioxidant additives is one of the most cost-364 effective ways to lessen the emission of NOx from biodiesel-fueled engines ^{169,207}. However, 365 in their study, the formation of CO and THC increased. The antioxidants selected for their 366 study were EDA, p-PDA, BHT, α-tocopherol, and L-ascorbic acid; p-PDA showed the best 367 activity in reducing NOx emission. In most studies on antioxidant added biodiesel emission 368 analysis, a reduction in NOx and slight increase in CO and THC are observed. The amounts of 369 CO and THC are lower than that emitted by diesel fuel ^{170,5, 208} Compared with the emission 370 371 from diesel fuel ignition, NO_X formation is the main imperfection of biodiesel fuel. Based on the aforementioned studies, antioxidants can assume a real part in decreasing NO_X $^{209, 210}$. The 372 establishment of NO_X is caused by the presence of free radicals in fuel, as effectively specified 373 374 in this article. The fuel radicals react with nitrogen from the air to form NOx. The presence of 375 antioxidants can end the radical reaction and decrease NOx formation.

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Test fuel/Bl end	Engine specificati on	Operating condition	Comparison of Emission with and without antioxidantComparison of performance with and with and conce without antioxidant				Antioxid ant concentra tion	Ref.		
			NO _x	СО	HC	Smoke	BSFC	BP	_	
Soybea n (SB10 0)	4C,4S,CR :22RP:80 kw at 4000 rpm, IP= 150 bar	Constant speed and different load	Slightly higher than without AO	Lower than	lower than without AO	Lower than withou t AO	Ţ	-	500- 2000ppm	172
Canola (B100, B50, B20, B10)	2C,4S,DI, CR:16.5: 1,RP:11.2 kw at 1800rpm, IP= 22 bar	Constant speed & different load	↓up to 5% but slightly ↑ at low load and medium conditio n	max ↓ about 19%	max↓up to 65% at B ₁₀₀	-	<pre>↑6% with ↑blend ratio and AO</pre>	_	-	211
Kerose ne(B10 0, B50, B20, B10)	2C,4S,DI, CR:16.5: 1,RP:11.2 kw at 1800rpm, IP= 22 bar	Constant speed & different load	↓up to 5% but slightly ↑ at low and medium load conditio n	max ↓ about 19%	max↓up to 65% at B ₁₀₀	-	<pre>↑6% with ↑blend ratio and AO</pre>	-	-	173
Neem oil (B100)	1C,4S,DI, CR:12:1 to 18:1,RP:3 .5kw at 1500rpm.	Constant speed &differen t load	↓ up to 19.99% at full load conditio n	↑slightl y 4.3%	↑ slightl1. 62%y	↑ up to 2.02%	same	same	100- 400ppm	212
Cocon ut (B20) & jatroph a (B20)	4C, DI	Different speed & constant load	↓ 2.6 - 5.0%	↑4.9- 20.8%	↑23.2- 40.2%	-	↓ 0.55- 0.79%	Ţ	175.8- 184.9pp m	213
Canola (B20)	4C,4S,CR : 19.5:1,W C,TDI	Constant load & different speed	↓4.3%	Î	-	-	↓ 10.19%	-	1000ppm	214
Caloph yllum (B20)	DI,4C,RP : 55kw	Constant load & different speed	↓1.6- 3.6%	↑39.14 %	↑26.5%	-	↓up to 1.5%	Ţ	1000- 2000ppm	161

Table: 4. Comparison performance & emission with and without antioxidant

Palm (B20)	DI,4C,RP : 42kw	Constant load & different speed	↓ upto 9.8- 12.6%	↑8.6- 12.3%	↑9.1- 12.0%	-	↓ 0.18- 0.64%	Low er up to 0.68- 1.02 %	1000ppm	
Jatroph a (B5, B10, B15, B20)	4C,4S,DI, RP: 55kw	Full load & different speed	↓ up to 8.03- 16.54% for all blends	†signifi cantly	↓↑up to 9.33- 44% for all blends	-	↑ higher at 1000rp m	Ţ	-	170
Croton megalo carpus (B100)	4C,TDI,C R: 195.:1, RP: 66kw at 1900rpm	Different load & constant speed	Slightly higher at 1000pp m	Slightly higher at 1000pp m	Slightly higher at 1000pp m	Slightl y higher at full load conditi on	↓14.24 %	-	1000ppm	215
Soybea n (B20, B100)	1C,4S,DI, RP:4.4kw ,IP: 200bar	Constant speed	↓ up to 4.06- 9.35%	↑ over 9.09% for SB20 and 14.28% for SB100	↑ about 10.52- 16.92%	↑signif icantly	-	†slig htly	1000ppm	
Jatroph a (B100)	1C,4S,DI, RP:4.4kw ,IP: 200bar	Constant speed & different load	↓5.86- 43.44% for all AO	↑ for all AO	Î	Î	Slightly ↑ at BHT,α- tocophe rol	↑ for all load	0.025%- m	169

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1C: single cylinder, 4S: four stroke, IP: injected pressure, RP: Rated power, CR: compression
ratio, TDI: terbocharged direct injection, WC: water cooled, DI: direct injection

From Table 4 it can be concluded that addition of antioxidant in biodiesel significantly effect
on engine performance and emission hence decrease the NOx and most of the cases CO, HC,
increase but engine performance increase and good improve BSFC and BP compare that of
without antioxidant . Addition of BHA, BHT, TBHQ increase CO and HC due to the reduction
of oxidative free radicals.

387	6. Conclusion
388	Different parameters are affected by biodiesel stability, which can be categorized into
389	oxidation, thermal stability, and storage stability. The present review has covered the various
390	types of fuel stabilities, mechanisms of occurrence, effect of different parameters on the
391	stability of biodiesel, test methods, stability measurements, and improvement of biodiesel
392	stability. The following conclusions were drawn:
393	1. IP, PV, AV, IV, viscosity, and density are the main parameters related to the stability
394	of biodiesel; among these parameters, IP and BAPE are the major factors.
395	2. Various tests have been applied to determine the oxidation stability; among them, IR
396	analysis is an effective, fast, easy, and non-destructive method.
397	3. To determine thermal stability, the Rancimat test, D 5304-06, and TGA/DTA are
398	commonly used. Among these various tests, Rancimat is the most effective method to
399	investigate the thermal stability of oils, biodiesel fuels, and fats.
400	4. More effective and important research and development areas are needed to enhance
401	and improve the stability of biodiesel for future use in existing engines as a substitute
402	to petroleum diesel. Studies on the effect of antioxidants in improving the oxidation
403	stability revealed that the activity of each antioxidant differs depending on the type of
404	biodiesel feedstock used, antioxidant concentration, blending percentage with
405	petrodiesel, and storage conditions.
406	5. The effectiveness of these antioxidants can be written in the following order:
407	TBHQ > PY > PG. Among the different antioxidants, PG is the best antioxidant for
408	most biodiesel samples; an additional advantage is that, the decreased NOx emission
409	from the biodiesel-fueled diesel engines.
410	6. Aluminum is the best storage container for biodiesel because it does not exert any
411	catalytic effect on biodiesel oxidation.

7. Synthetic antioxidants are more effective on the engine performance and emission; the
addition of antioxidants in biodiesel significantly affects engine performance and
emission, thereby decreasing NOx and increasing CO and HC. However, engine
performance increases, indicating good improvement. BSFC and BP decrease without
antioxidants, and BHA, BHT, and TBHQ increase CO and HC because of the reduction
in oxidative free radicals.

Additional research is required to investigate the effect of biodiesel stability on engine
performance, as well as the effect on emissions. Further studies are required to
investigate and confirm that the use of antioxidants will ensure the long-term storage
stability of biodiesel fuel. More experimental research is required to clarify the effect
of antioxidant on biodiesel emission formation, as well as analyze the effectiveness of
other antioxidants under wider operating conditions

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431	1.	H. Rashedul, H. Masjuki, M. Kalam, A. Ashraful, S. A. Rahman and S. Shahir, <i>Energy</i>
432		Conversion and Management, 2014, 88, 348-364.

- 433 2. S. Jain and M. P. Sharma, *Renewable and Sustainable Energy Reviews*, 2010, 14, 667434 678.
- 435 3. I. Hiroaki, M. Eiji, H. Shusaku and S. Saka, *Fuel*, (2008), **87** (1), p. 1–6.
- 436 4. R. O. Dunn, *Biofuels, Bioproducts and Biorefining*, 2008, **2**, 304-318.
- 437 5. H. K. Rashedul, H. H. Masjuki, M. A. Kalam, A. M. Ashraful, M. M. Rashed, I.
 438 Sanchita and T. Shaon, *RSC Advances*, 2014, 4, 64791-64797.
- 439 6. J. Pullen and K. Saeed, *Renewable and Sustainable Energy Reviews*, 2012, 16, 5924440 5950.
- 441 7. B. R. Moser, G. Knothe and S. C. Cermak, *Energy & Environmental Science*, 2010, 3, 318-327.

⁴²⁹ **Reference**

443	8.	K. Yamane, K. Kawasaki, K. Sone, T. Hara and T. Prakoso, <i>International Journal of</i>
444	0	Engine Research, 2007, $\mathbf{\delta}$, 507-519.
445 446	9.	K. Arisoy, Energy Sources, Part A: Recovery, Utilization, and Environmental Effects, 2008, 30 , 1516-1522.
447 448	10.	W. E. Neff, M. A. El-Agaimy and T. L. Mounts, <i>Journal of the American Oil Chemists'</i>
440	11	A M Ashraful H H Masjuki M A Kalam H K Dashadul H Sajiad and M I
449 450	11.	Abedin, Energy Conversion and Management, 2014, 87 , 48-57.
451 452	12.	S. Schober and M. Mittelbach, <i>European journal of lipid science and technology</i> , 2005, 107 , 268-271.
453	13.	M. Mofijur, H. Masjuki, M. Kalam and M. Shahabuddin, <i>Energy Educ Sci Technol Part</i>
454		A: Energy Sci Res, 2012, 30 , 737e748.
455	14.	A. Monvem, M. Canakci and J. H. Van Gerpen, <i>Applied Engineering in Agriculture</i> .
456		2000. 16. 373-378.
457	15.	R. L. McCormick, DIANE Publishing, 2009, 1-85.
458	16	I V Gerpen B Pruszko R Clements and G D Knothe National Renewable Energy
459	10.	Laboratory (2004) NREL/SR-510-36244.
460	17.	M. L. M. Valle, R. S. Leonardo and J. Dweck, <i>Thermal Analysis and Calorimetry</i> , 2014,
461		116 , 113-118.
462	18.	W. T. Wazilewski, R. A. Bariccatti, G. I. Martins, D. Secco, S. N. M. D. Souza, H. A.
463		Rosa and L. I. Chaves, Industrial Crops and Products, 2013, 43, 207-212.
464	19.	M. Serrano, A. Bouaid, M. Martínez and J. Aracil, Fuel, 2013, 113, 50-58.
465	20.	M. Mofijur, H. H. Masjuki, M. A. Kalam and A. E. Atabani, <i>Energy</i> , 2013, 55, 879-
466		887.
467	21.	M. Mofijur, H. Masjuki, M. Kalam, M. Hazrat, A. Liaquat, M. Shahabuddin and M.
468		Varman, Renewable and Sustainable Energy Reviews, 2012, 16, 5007-5020.
469	22.	M. Mofijur, A. Atabani, H. Masjuki, M. Kalam and B. Masum, Renewable and
470		Sustainable Energy Reviews, 2013, 23, 391-404.
471	23.	I. Shancita, H. Masjuki, M. Kalam, I. R. Fattah, M. Rashed and H. Rashedul, <i>Energy</i>
472		Conversion and Management, 2014, 88, 794-807.
473	24.	W. JA. National Renewable Energy Laboratory, SwRI® Project No. 08-10721, 2005.
474	25.	A. Sarin, N. P. Singh, R. Sarin and R. K. Malhotra, <i>Energy</i> , 2010, 35 , 4645-4648.
475	26.	R. O. Dunn. Energy and Fuels. 2008. 22, 657-662.
476	27	L M Das D K Bora S Pradhan M K Naik and S N Naik <i>Fuel</i> 2009 88 2315-
477	27.	2318
178	28	I Xin H Imahara and S Saka <i>Fuel</i> (2009) 88 (2) n 282–286
470 179	20. 29	G Knothe Fuel Processing Technology 2005 86 (10) 1059–1070
475	2). 30	M W Formo F Jungermann F Noris and N O V Sonntag John Wiley and Sons
400	50.	$1070 \ 1 \ no \ 4 \ 608 \ 711$
401	21	D E Church and W A Dryor Environmental Health Derspectives 1085 VOI 64
402	51.	D. T. Church and W. A. Fryor, Environmental freatmer respectives, 1965, VOL. 04,
483	20	111-120. E.D. Curretone and T. D. Hilditch, Learner lof the Chamier L Seriety (Resumed) 1045
484	32.	F. D. Gunstone and T. P. Hildlich, <i>Journal of the Chemical Society</i> (<i>Resumed</i>), 1945,
485	22	
486	<i>33</i> .	G. Knothe, JAOCS, Journal of the American Oil Chemists' Society, 2002, 79, 847-854.
487	34.	W. E. Nett, I. L. Mounts, W. M. Rinsch and H. Konishi, <i>Journal of the American Oil</i>
488	95	Chemists' Society, 1993, 70, 163-168.
489	35.	A. A. Retaat, International Journal of Environmental Science and Technology, 2009,
490	_	6 , 677-694.
491	36.	M. Canakci, A. Monyem and J. Van Gerpen, <i>Transactions of the American Society of</i>
492		<i>Agricultural Engineers</i> , 1999, 42 , 1565-1572.

493	37.	M. Mittelbach and S. Gangl, JAOCS, Journal of the American Oil Chemists' Society,
494	20	2001, 78, 573-577.
495 496	38.	<i>P.</i> Bondioli, A. Gasparoli, L. Della Bella and S. Tagliabue, <i>European Journal of Lipid</i> Science and Technology, 2002, 104 , 777-784.
497	39.	P. Bondioli, A. Gasparoli, L. Della Bella, S. Tagliabue and G. Toso, <i>European Journal</i>
498		of Lipid Science and Technology, 2003, 105, 735-741.
499	40.	P. Bondioli, A. Gasparoli, A. Lanzani, E. Fedeli, S. Veronese and M. Sala, JAOCS,
500		Journal of the American Oil Chemists' Society, 1995, 72, 699-702.
501	41.	T. Y. Miyata I, Tsurutani K, Okada M., SAE paper 2004-01-3031, 2004.
502	42.	K. Andersson and H. Lingnert, JAOCS, Journal of the American Oil Chemists' Society,
503		1998, 75 , 1041-1046.
504	43.	L. M. Du Plessis, J. B. M. De Villiers and W. H. Van Der Walt, <i>Journal of the American</i>
505		Oil Chemists' Society, 1985, 62, 748-752.
506	44.	C. Y. Lin, H. A. Lin and L. B. Hung, Fuel, 2006, 85, 1743-1749.
507	45.	Gülgün Yildiz, Randy L. Wehling and S. L. Cuppett, Journal of the American Oil
508		<i>Chemists Society</i> , 2003, 80 (2) .
509	46.	R.A. Korus, T.L. Mousetis and L. Lloyd, American Society of Agricultural Engineering
510		1982, 18–223.
511	47.	R. L. McCormick and S. R. Westbrook, <i>Energy & Fuels</i> , 2009, 24, 690-698.
512	48.	J. C. Cowan, Wiley Interscience, 1979, 8, 130–150.
513	49.	MI Gurr JL Harwood and K. Frayn, (5th ed.)Blackwell Science Ltd, 2002.
514	50.	R. L. McCormick, M. Ratcliff, L. Moens and R. Lawrence, Fuel Processing
515		Technology, 2007, 88, 651-657.
516	51.	H. Hasenhuettle, Chapman and Hall, New York 1997.
517	52.	J. N. Chacón, P. Gaggini, R. S. Sinclair and F. J. Smith, <i>Chemistry and physics of lipids</i> ,
518		2000, 107 , 107-120.
519	53.	V. M. L. dos Santos, J. A. B. da Silva, L. Stragevitch and R. L. Longo, <i>Fuel</i> , 2011, 90 ,
520		811-817.
521	54.	M. J. Ramos, C. M. Fernández, A. Casas, L. Rodríguez and A. Pérez, <i>Bioresource</i>
522		technology, 2009, 100 , 261-268.
523	55.	Y. C. Liang, C. Y. May, C. S. Foon, M. A. Ngan, C. C. Hock and B. Yusof, <i>Fuel</i> 2006,
524		85 , 867-870.
525	56.	SK. Loh, SM. Chew and YM. Choo, Journal of the American Oil Chemists Society,
526		(2006), 83 , 947–952.
527	57.	T. Kivevele, A. K. Agarwal, T. Gupta and M. Mbarawa, Oxidation Stability of Biodiesel
528		Produced from Non-Edible Oils of African Origin, SAE Technical Paper, 2011.
529	58.	M. Mittelbach and S. Schober, Journal of the American Oil Chemists Society, (2003),
530		80 , 817–823.
531	59.	J. Xin, H. Imahara and S. Saka, <i>Fuel</i> , 2009, 88 , 282-286.
532	60.	A. K. Domingos, E. B. Saad, W. W. Vechiatto, H. M. Wilhelm and L. P. Ramos,
533		Journal of the Brazilian Chemical Society, 2007, 18, 416-423.
534	61.	A. Fröhlich and S. Schober, Journal of the American Oil Chemists' Society, 2007, 84,
535		579-585.
536	62.	R. Sarin, M. Sharma, S. Sinharay and R. K. Malhotra, <i>Fuel</i> , 2007, 86 , 1365-1371.
537	63.	in Biodiesel: Production and Properties, The Royal Society of Chemistry, 2012, pp.
538		51-79.
539	64.	P. Y. Furlan, P. Wetzel, S. Johnson, J. Wedin and A. Och, <i>Spectroscopy Letters</i> , 2010,
540		43, 580-585.
541	65.	M. Conceicüa o, V. F. Jr, A. Arau'jo, M. Farias, I. Santos and A. Souza, <i>Energy Fuels</i> ,
542		(2007), 21 , 1522–1527.

543	66.	J. S. Oliveira, R. Montalvão, L. Daher, P. A. Z. Suarez and J. C. Rubim, <i>Talanta</i> , 2006,
544		69 , 1278-1284.
545	67.	G. Knothe, JAOCS, Journal of the American Oil Chemists' Society, 2001, 78, 1025-
546	_	1028.
547	68.	F. C. C. Oliveira, C. R. R. Brandão, H. F. Ramalho, L. A. F. da Costa, P. A. Z. Suarez
548		and J. C. Rubim, Analytica Chimica Acta, 2007, 587, 194-199.
549	69.	I. P. Soares, T. F. Rezende, R. C. Silva, E. V. R. Castro and I. C. P. Fortes, <i>Energy and</i>
550		<i>Fuels</i> , 2008, 22 , 2079-2083.
551	70.	P. Baptista, P. Felizardo, J. C. Menezes and M. J. N. Correia, Analytica Chimica Acta,
552		2008, 607 , 153-159.
553	71.	P. Felizardo, P. Baptista, J. C. Menezes and M. J. N. Correia, Analytica Chimica Acta,
554		2007, 595 , 107-113.
555	72.	P. Baptista, P. Felizardo, J. C. Menezes and M. J. Neiva Correia, Talanta, 2008, 77,
556		144-151.
557	73.	G. Knothe, JAOCS, Journal of the American Oil Chemists' Society, 1999, 76, 795-800.
558	74.	G. Knothe, JAOCS, Journal of the American Oil Chemists' Society, 2000, 77, 489-493.
559	75.	G. F. Zagonel, P. Peralta-Zamora and L. P. Ramos, <i>Talanta</i> , 2004, 63 , 1021-1025.
560	76.	AOCS Official and Tentative Methods: Cd 12-57, Fat stability-active oxygen method
561		(AOM) reapproved(1997).
562	77.	S. G. Morris, P. Magidman, F. E. Luddy and R. W. Riemenschneider, Journal of the
563		American Oil Chemists' Society, 1956, 33, 353-355.
564	78.	E. R. Sherwin, Journal of the American Oil Chemists' Society, (1971), 49 (8) 468–472.
565	79.	E. R. Sherwin and B. M. Luckadoo, Journal of the American Oil Chemists' Society,
566		1970, 47 , 19-23.
567	80.	M. W. Läubli and P. A. Bruttel, Journal of the American Oil Chemists' Society, 1986,
568		63 , 792-795.
569	81.	S. E. Hill and E. G. Perkins, JAOCS, Journal of the American Oil Chemists' Society,
570		1995, 72 , 741-743.
571	82.	S. Jain and M. Sharma, Renew Sustain Energy Rev. (2010), 14, 1937–1947.
572	83.	ASTM Standard D6468 2008 (2013), Standard test method for high temperature
573		stability of middle distillate fuels, ASTM International, West Conshohocken, PA;
574		2003.http://dx.doi.org/10.1520/D6468, www.astm.org (2014)
575	84.	Z. Yaakob, B. N. Narayanan, S. Padikkaparambil, S. Unni K and M. Akbar P.
576		Renewable and Sustainable Energy Reviews, 2014, 35, 136-153.
577	85.	Determining the oxidation stability of biodiesel, European standard EN 14112.
578	86.	D. Berthiaume and A. Tremblay, <i>Oleotek Inc.</i> , (November 2006).
579	87.	Prepared by System Lab Services Division of Williams Pipe Line Company, February
580		1997.
581	88.	K. YAMANE, K. KAWASAKI, K. SONE and T. PRAKOSO, INTERNATIONAL
582		JOURNAL OF ENGINE RESEARCH. 2007. 8.
583	89.	N. T. Joyner and J. E. McIntyre, <i>Oil Soap</i> , 1938, 15 , 184-186.
584	90.	M. Formo, E. Jungermann, F. Norris and N. Sonntag, John Wiley & Sons, Inc. Canada,
585	201	1979.
586	91.	O. C. Johnson and F. A. Kummerow, J Am Oil Chem Soc. 1957. 34, 407-409.
587	92.	H. Wexler. <i>Chemical Reviews</i> , 1964, 64 , 591-611.
588	93	S Jain and M P. Sharma Renewable and Sustainable Energy Reviews 2011 15 438-
589		448
590	94.	Standard test method for high temperature stability of middle distillate fuels ASTM
591		standard D 6468-08.

592	95.	Stability of biodiesel used as a fuel for diesel engines and heating systems, Presentation
593	0.6	of BIOSTAB project results, Graz, Austria. (July 3, 2003).
594	96.	W. B. Wan Nik, F. N. Ani and H. H. Masjuki, <i>Energy Conversion and Management</i> ,
595	07	2005, 40 , 2198-2215. S. Join and M. D. Sharma, <i>Excl.</i> 2012, 02 , 252, 257
596	97.	S. Jain and M. P. Sharma, Fuel, 2012 , 93, $252-257$.
597	98. 00	C. A. Wilkie, Polymer Degradation and Stability, (1999), 66 (3), p. $301-306$.
598	99. 100	T.D. Fornes, P.J. Yoon and D. R. Paul, <i>Polymer</i> , (2003), 44 (24), p. 7545–7556.
599	100.	1. FORNES, P. YOON and D. PAUL, <i>Polymer</i> , 2003, 44 , 7545-7556.
600	101.	X. H. Li, Y. Z. Meng, Q. Zhu and S. C. Ijong, <i>Polymer Degradation and Stability</i> ,
601	102	2003, 81, 157-105.
602	102.	I. Buz as, E. Kurucz and J. Hollo, <i>Journal of the American Oil Chemists Society</i> , 1979,
603	102	50 , 085-088.
604	103.	Y. H. Roos, Journal of Thermal Analysis and Calorimetry, 2003, 71, 197-203.
605	104.	J. Magoshi, M. A. Becker, Z. Han and S. Nakamura, <i>Journal of Thermal Analysis and</i>
606	105	Calorimetry, (2003), $70(3)$, 833–839.
607	105.	B. Kowalski, <i>Journal of Inermal Analysis</i> , 1988, 34 , 1321-1326.
608	100.	B. Kowalski, Inermochimica Acta, 1991, 184 , 49-57.
609	107.	H. Gloria and J. M. Aguilera, <i>Journal of Agricultural and Food Chemistry</i> , 1998, 46,
610	100	1303-1308. C. D. Tan and Y. D. Cha Man. Engl. Cha. 1400 (7, 177, 194
611	108.	C. P. Tan and Y. B. Che Man, <i>Food Chemistry</i> , 1999, 67 , 177-184.
612	109.	P. Reikin, S. Sourdet and P. Y. Fosseux, <i>Journal of Thermal Analysis and Calorimetry</i> ,
613	110	2005, 71, 187-195.
614	110.	M. L. Feisner and J. R. Matos, Anais and Associacao Brasileira ae Química, (1998), 47
615	111	(4), 508-512. C. D. Tan and Y. D. Cha Man. 14 OCE. Lawrent of the American Oil Chamistel' Seriety.
616	111.	C. P. Tan and Y. B. Che Man, JAOCS, Journal of the American Oil Chemists Society,
017	110	2000, 77, 143-155. E. Cimpowski, Thermochimics Acts, 1000, 170 , 07, 105
018	112.	E. GIIIZEWSKI, Intermochimica Acia, 1990, 170, 97-103. M. D. Koton, D. L. Zoelv and D. D. Monginik, Annual Pay, Nutr. 1005, 15, 472, 402
619	115.	M. D. Katali, P. L. Zock and K. P. Melisink, Annu. Rev. Nuir., 1995, 15, 475-495.
620	114.	D. E. Williard, T. L. Kaduce, S. D. Harmon and A. A. Specior, <i>Journal of lipia</i>
621	115	research, 1998, 39 , 978-980.
622	115.	K. E. Tale, K. C. Walls, C. A. W. Allen and K. L. Wilkle, <i>Fuel</i> , 2006, 65 , 1010-1015. T. Eviji D. Khuwijitian, V. Kimura and S. Adashi, <i>Easd shamistry</i> , 2006, 04 , 241, 247.
623	110.	A Devid M Mertingg and L Arabil Eval 2007 86 2506 2602
624	11/.	A. Bouald, M. Martinez and J. Arach, $Fuel, 2007, 60, 2390-2002$.
625	110.	P. DONDIOLI and A. GASPAROLI, 2003. A Saria D. Arara N. D. Singh M. Sharman and D. K. Malhatra, Example 2000, 24
626	119.	A. Sarin, K. Afora, N. P. Singii, M. Sharina and K. K. Mainoura, <i>Energy</i> , 2009, 34 , 1071–1075
627	120	12/1-12/3. D. D. Coller, T. T. Adama, I. W. Coodrum and I. Dandaramaa, Eucl. 2008, 97 , 02, 102
628	120.	L. Des D. K. Dere S. Dredhen M. K. Neils and S. Neils <i>Fuel</i> , 2000, 89 , 2215, 2219
629	121.	L. Das, D. K. Bora, S. Fraunani, M. K. Naik and S. Naik, Fuel, 2009, 66 , 2515-2518.
630	122.	E. O. Aluyor, K. O. Obamagbon and M. Ori-Jesu, <i>Scientific Research and Essays</i> , 2009,
631	102	4, 545-548. D. K. Sharman, D. A. Z. Swaran, I. M. Daran, and S. Z. Erkan, Eval Duranaina
632	123.	B. K. Snarma, P. A. Z. Suarez, J. M. Perez and S. Z. Ernan, <i>Fuel Processing</i>
633	124	Technology, (2009). E. D. Cunstone, The chemistry of fate and cilePlachwell Dublishing, CPC Press
634	124.	F. D. Gunstone, The chemistry of fats and outsblackwell Publishing, CRC Press,
635	105	Uxford, UK, (2004), 150–108.
030	125.	J. C. Thompson, C. L. Peterson, D. L. Reece and S. M. Beck, <i>Transactions of the</i>
۲ د ک	100	American Society of Agricultural Engineers, 1998, 41, 931-939.
038 630	120.	U. KIIOUIE allu K. U. Dullii, JAUUS, Journal of the American Uli Chemists Society, 2002 80 1021 1026
039 640	107	2003, 00 , $1021-1020$. P. C. P. and F. I. D. [SAF manor 0716001, 1007]
040	14/.	D. D. D allu F. J. F. $(SAL \mu \mu \mu e I P / 10 P 0), 17 P / 10 P 0$

641	128.	Stability of biodiesel used as a fuel for diesel engines and heating systems, Presentation
642		of BIOSTAB project results (July 3, 2003): Graz, Austria.
643	129.	D. Berthiaume and A. Tremblay, <i>Oleotek Inc.</i> , 2006.
644	130.	V. Makarevičiene, S. Lebedevas, P. Rapalis, M. Gumbyte, V. Skorupskaite and J.
645		Žaglinskis, <i>Fuel</i> , 2014, 120 , 233-239.
646	131.	C. Haşimoğlu, M. Ciniviz, I. Özsert, Y. Içingür, A. Parlak and M. Sahir Salman,
647		Renewable Energy, 2008, 33 , 1709-1715.
648	132.	M. Lapuerta, J. Rodríguez-Fernández, A. Ramos and B. Álvarez, Fuel, 2012, 93, 391-
649		396.
650	133.	J. M. Nzikou, L. Matos, J. E. Moussounga, C. B. Ndangui, N. P. Pambou-Tobi, E. M.
651		Bandzouzi, A. Kimbonguila, M. Linder and S. Desobry, Research Journal of Applied
652		Sciences, 2009, 4, 94-100.
653	134.	R. O. Dunn, JAOCS, Journal of the American Oil Chemists' Society, 2002, 79, 915-920.
654	135.	S. Tagliabue, A. Gasparoli, L. Della Bella and P. Bondioli, Influenza della
655		contaminazione mettalica sulla stabilità térmico ossidativa del biodiesel. La Rivista
656		Italiana Delle Sostanze Grasse LXXXII (marzo/aprile 2005), 2005, 93-96.
657	136.	Y. F. Wang, K. L. Huang, C. T. Li, H. H. Mi, J. H. Luo and P. J. Tsai, Atmospheric
658		<i>Environment</i> , 2003, 37 , 4637-4643.
659	137.	N. O. V. Sonntag. <i>Composition and Characteristics of Individual Fats and Oils</i> , 1979.
660		289.
661	138.	A. S. M. A. Haseeb, S. Y. Sia, M. A. Fazal and H. H. Masjuki, <i>Energy</i> , 2010, 35, 1460-
662		1464.
663	139.	A. Dos Reis Albuquerque, J. Maul, J. Pereira Dos Santos, I. Maria Garcia Dos Santos
664		and A. Gouveia De Souza, <i>Fuel</i> , 2012, 102 , 585-591.
665	140.	C. C. Garcia, P. I. B. M. Franco, T. O. Zuppa, N. R. A. Filho and M. I. G. Leles, <i>Journal</i>
666		of Thermal Analysis and Calorimetry, 2007. 87 , 645-648.
667	141.	J. Xin. H. Imahara and S. Saka, <i>Fuel</i> , 2008, 87 , 1807-1813.
668	142.	S. Jain and M. P. Sharma, Fuel. 2013, 109, 379-383.
669	143.	A. Sarin, R. Arora, N. P. Singh, R. Sarin and R. K. Malhotra, <i>Energy</i> , 2010, 35 , 3449-
670	1.01	3453.
671	144.	L. M. J.M. Nzikou, J.E. Moussounga, C.B. Ndangui, N.P. Pambou-Tobi, E.M.
672		Bandzouzi et al., <i>Res J Appl Sci</i> , (2009), 4 (2) 94–100.
673	145.	R. O. Dunn. Transactions of the American Society of Agricultural Engineers, 2000, 43.
674		1203-1208.
675	146	I Polavka J Paligová J Cvengroš and P Šimon JAOCS Journal of the American Oil
676	1.00	Chemists' Society 2005, 82, 519-524
677	147.	R. O. Dunn. J Am Oil Chem Soc. (2009). 79 , 915–920.
678	148.	I. M. Atadashi, M. K. Aroua, A. R. Abdul Aziz and N. M. N. Sulaiman, <i>Renewable and</i>
679	1.01	Sustainable Energy Reviews 2012, 16 3456-3470
680	149	P P Oh H L N Lau I Chen M F Chong and Y M Choo <i>Renewable and</i>
681	11/1	Sustainable Energy Reviews 2012, 16 5131-5145
682	150	A Demirbas and H Kara Energy Sources Part A: Recovery Utilization and
683	100.	Environmental Effects 2006 28 619-626
684	151	D.Y. C. Leung and Y. Guo, Fuel Processing Technology, 2006, 87 , 883-890.
685	152	Y C Chen H E Si and I Cheng Journal of Yangtze University (Natural Science
686		Edition) Sci & Eng v. 2007. 1. 015.
687	153	I. M. Atadashi, M. K. Aroua and A. A. Aziz, <i>Renewable and Sustainable Energy</i>
688		Reviews, 2010, 14 , 1999-2008.
689	154.	A. C. Cooke BS. Bertram B. Purification of biodiesel with adsorbent materials. CA
690		Patent CA2,541,327; 2005.

691	155.	A. Gabelman and S. T. Hwang, <i>Journal of Membrane Science</i> , 1999, 159 , 61-106.
692	156.	R. McCormick, M. Ratcliff, L. Moens and R. Lawrence, <i>Fuel Processing Technology</i> ,
693		2007, 88.
694	157.	G. Knothe, Fuel Processing Technology, 2007, 88, 669-677.
695	158.	A. Sarin, R. Arora, N. Singh, R. Sarin and R. Malhotra, <i>Energy</i> , 2010, 35 , 3449-3453.
696	159.	G. Karavalakis and S. Stournas, <i>Energy and Fuels</i> , 2010, 24 , 3682-3686.
697	160.	I. M. Rizwanul Fattah, H. H. Masjuki, M. A. Kalam, M. Mofijur and M. J. Abedin,
698		Energy Conversion and Management, 2014, 79 , 265-272.
699	161.	I. M. Rizwanul Fattah, H. H. Masjuki, M. A. Kalam, M. A. Wakil, A. M. Ashraful and
700		S. A. Shahir, Energy Conversion and Management, 2014, 83, 232-240.
701	162.	F. Shahidi, P. Janitha and P. Wanasundara, <i>Critical reviews in food science & nutrition</i> ,
702		1992, 32 , 67-103.
703	163.	P. TenáHave, Transactions of the Faraday Society, 1947, 43, 201-210.
704	164.	Z. Yang, B. P. Hollebone, Z. Wang, C. Yang and M. Landriault, Fuel Processing
705		<i>Technology</i> , 2013, 106 , 366-375.
706	165.	I. M. Rizwanul Fattah, H. H. Masjuki, M. A. Kalam, M. A. Hazrat, B. M. Masum, S.
707		Imtenan and A. M. Ashraful, Renewable and Sustainable Energy Reviews, 2014, 30,
708		356-370.
709	166.	M. Gordon, in Food antioxidants, Springer, 1990, pp. 1-18.
710	167.	G. Miller and F. Quackenbush, Journal of the American Oil Chemists Society, 1957,
711		34 , 249-250.
712	168.	Jh. Lee, JI. Choe, Sw. Jung and SW. Ham, Bulletin of the Korean Chemical
713		Society, 2006, 27 , 33-34.
714	169.	J. Sheehan, V. Camobreco, J. Duffield, M. Graboski and H. Shapouri, National
715		Renewable Energy Laboratory, Golden, CO (1998), 206–261.
716	170.	A. Wojdyło, J. Oszmiański and R. Czemerys, Food Chemistry, 2007, 105, 940-949.
717	171.	D. Lomonaco, F. J. N. Maia, C. S. Clemente, J. P. F. Mota, A. E. Costa Jr and S. E.
718		Mazzetto, Fuel, 2012, 97, 552-559.
719	172.	V. C. Ramalho and N. Jorge, Antioxidantes utilizados em óleos, gorduras e alimentos
720		gordurosos, 2006, 29 , 755-760.
721	173.	<u>www.biofuelsystems.com/other/baynox.pdf</u> . (2014)
722	174.	www.istc.illinois.edu/research/092910symposium/0905.pdf. (2014)
723	175.	S. Schober and M. Mittelbach, European Journal of Lipid Science and Technology,
724		2004, 106 , 382-389.
725	176.	M. Wijtmans, D. A. Pratt, J. Brinkhorst, R. Serwa, L. Valgimigli, G. F. Pedulli and N.
726		A. Porter, Journal of Organic Chemistry, 2004, 69, 9215-9223.
727	177.	Y. H. Chen and Y. M. Luo, Fuel Processing Technology, 2011, 92, 1387-1393.
728	178.	C. D. Bannister, C. J. Chuck, M. Bounds and J. G. Hawley, Proceedings of the
729		Institution of Mechanical Engineers, Part D: Journal of Automobile Engineering, 2011,
730		225 , 99-114.
731	179.	L. Haya, A. M. Mainar, J. I. Pardo and J. S. Urieta, Physical Chemistry Chemical
732		Physics, 2014, 16, 1409-1414.
733	180.	G. Karavalakis, D. Hilari, L. Givalou, D. Karonis and S. Stournas, <i>Energy</i> , 2011, 36,
734		369-374.
735	181.	Z. Wang, F. Yang, H. Zheng, X. Qin, J. Luo, Y. Li and D. Xiao, Analyst, 2014, 139,
736		3622-3628.
737	182.	A. K. Agarwal and D. Khurana, <i>Fuel Processing Technology</i> , 2013, 106 , 447-452.
738	183.	D. Chaithongdee, J. Chutmanop and P. Srinophakun, Kasetsart Journal - Natural
739		Science, 2010, 44, 243-250.

740	184	M Mittelbach and S Schober IAOCS Journal of the American Oil Chemists' Society
741	101.	2003. 80 , 817-823
742	185	A Fröhlich and S. Schober, JAOCS, Journal of the American Oil Chemists' Society
743	1001	2007, 84 , 579-585.
744	186.	D. K. Bora, L. M. Das and M. K. G. Babu, <i>Journal of Scientific and Industrial Research</i> ,
745		2009, 68 , 149-152.
746	187.	A. K. Domingos, E. B. Saad, W. W. D. Vechiatto, H. M. Wilhelm and L. P. Ramos,
747		Journal of the Brazilian Chemical Society, (2007),, p. 18.
748	188.	Y. C. Liang, C. Y. May, C. S. Foon, M. A. Ngan, C. C. Hock and Y. Basiron, Fuel,
749		2006, 85 , 867-870.
750	189.	P. Udomsap, N. Chollacoop, S. Topaiboul and T. Hirotsu, Int J Renew Energy, 2009,
751		4 , 47-59.
752	190.	M. Chakraborty and D. C. Baruah, <i>Fuel Processing Technology</i> , 2012, 98 , 51-58.
753 754	191.	T. T. Kivevele, M. M. Mbarawa, A. Bereczky, T. Laza and J. Madarasz, <i>Fuel</i> Processing Technology 2011 92 1244-1248
755	192	D M Fernandes D S Sergueira F M Portela R M N Assunção R A A Munoz
756	172.	and M. G. H. Terrones, <i>Fuel</i> , 2012, 97 , 658-661.
757	193.	S. M. Mudge and G. Pereira, <i>Spill Science and Technology Bulletin</i> , 1999, 5 , 353-355.
758	194.	D. Y. C. Leung, B. C. P. Koo and Y. Guo, <i>Bioresource Technology</i> , 2006, 97, 250-256.
759	195.	I. Lee, L. A. Johnson and E. G. Hammond, JAOCS, Journal of the American Oil
760		<i>Chemists' Society</i> , 1995, 72 , 1155-1160.
761	196.	S. B. Van Gerpen J, Pruszko R, Clements D, Knothe G. Biodiesel production
762		technology. Report for the National Renewable Energy Laboratory USA: Department
763		of Energy. 2004;30:42.
764	197.	G. Knothe, Energy & Environmental Science, 2009, 2, 759-766.
765	198.	D. Laforgia and V. Ardito, <i>Bioresource Technology</i> , 1995, 51 , 53-59.
766	199.	A. Monyem, J. H. Van Gerpen and M. Canakci, <i>Transactions of the American Society</i>
767		of Agricultural Engineers, 2001, 44, 35-42.
768	200.	C. Peterson and D. Reece, Transactions of the American Society of Agricultural
769		Engineers, 1996, 39 , 805-816.
770	201.	K. McDonnell, S. Ward, J. J. Leahy and P. McNulty, <i>JAOCS, Journal of the American</i>
771		<i>Oil Chemists' Society</i> , 1999, 76 , 539-543.
772	202.	S. Gan and H. K. Ng, <i>Energy Conversion and Management</i> , 2010, 51 , 1536-1546.
773	203.	T. T. Kivevele, L. Kristóf, A. Bereczky and M. M. Mbarawa, Fuel, 2011, 90, 2782-
774		2789.
775	204.	E. Ileri and G. Koçar, <i>Energy Conversion and Management</i> , 2013, 76 , 145-154.
776	205.	S. Jain and M. P. Sharma, <i>Fuel</i> , 2013, 106 , 152-156.
777	206.	K. Ryu, <i>Bioresource Technology</i> , 2010, 101 , S78-S82.
778	207.	K. Varatharajan, M. Cheralathan and R. Velraj, <i>Fuel</i> , 2011, 90 , 2721-2725.
779	208.	S. M. Palash, M. A. Kalam, H. H. Masjuki, M. I. Arbab, B. M. Masum and A. Sanjid,
780		Energy Conversion and Management, 2014, 77, 577-585.
781	209.	K. Varatharajan and M. Cheralathan, <i>Fuel Processing Technology</i> , 2013, 106 , 526-532.
782	210.	K. Ryu, <i>Bioresource technology</i> , 2010, 101 , S78-82.
783	211.	M. M. Roy, W. Wang and M. Alawi, <i>Energy Conversion and Management</i> , 2014, 84 ,
784	010	
785	212.	G. Balaji and M. Cheralathan, Journal of the Energy Institute.
/86	213.	I. M. KIZWANUI Fattah, H. H. Masjuki, M. A. Kalam, M. A. Wakil, H. K. Rashedul and
/8/	214	M. J. Abedin, Industrial Crops and Products, 2014, 57, 152-140.
700	<i>∠</i> 14.	A. Aunanii, E. Heri and B. Yuksel, Energy Conversion and Management, 2014, 81,
109		512-521.

790 215. T. Kivevele, L. Kristof, A. Bereczky and M. Mbarawa, Fuel, 2	011, 90 , 2782-2789.
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- 791
- 792