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ARTICLE TYPE

Nitrogen-modified activated carbon supported bimetallic Gold-Cesium(I) as highly active and stable catalyst in the hydrochlorination of acetylene

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Abstract: In the challenging acetylene hydrochlorination to vinyl chloride over Au-base catalysts, Au-Cs¹ catalysts are substantially more active and stable than their monometallic counterparts. Here we describe a novel nitrogen-modified activated carbon supported Au-Cs¹ catalyst (1Au4Cs¹/NAC) delivers stable ¹⁰ performance with acetylene conversion reaching 90.1% and there was only 1.5% C₂H₂ conversion loss after 50 h under the reaction conditions of C₂H₂ hourly space velocity 1480 h⁻¹. After a careful characterization of all the catalysts, we concluded that the nitrogen atoms influence on the stability of the Au-Cs¹ catalysts correlate with the strengthening the adsorption of hydrogen chloride to the catalyst and consequently inhibiting Au³⁺ reduction under reaction conditions.

15 Introduction

Acetylene hydrochlorination is an important coal-based technology for the industrial production of vinyl chloride.¹ Supported mercury chloride (HgCl₂) catalysts are currently the most convenient and the most practical catalysts for ²⁰ hydrochlorination of acetylene, but HgCl₂ is susceptible to reduction by acetylene and sublimation, which severely limits the production capacity and causes severe environmental problems.² The catalysts free from toxic mercury are thus desired.

Since Hutchings et al. carried out pioneering work to ²⁵ investigate the use of non-mercury catalysts for acetylene hydrochlorination,³⁻⁵ a significant number of supported-metal chlorides catalysts, including Bi^{3+,6} Cu^{2+,7} Pt^{2+,8} and Pd²⁺ chlorides,⁹ displaying considerable activity toward catalyzing the acetylene hydrochlorination, and the most widely used are based

³⁰ on supported AuCl₃ often in combination with other metals chlorides owing to its high intrinsic activity toward the formation of the desired vinyl chloride.¹⁰⁻¹² However, the deactivation rate of the AuCl₃ catalyst is still very high when the reaction used is a real commercial condition with lifetimes in the range of few rehears.⁵ The production of Au actalysts for

³⁵ hours.⁵ The practical application of Au catalysts for hydrochlorination reaction is attractive but, at present, it is still desired that the stability should be improved.

Recently, Nitrogen-doped carbon materials have attracted considerable attention as new promising materials.¹³ The ⁴⁰ presence of nitrogen atoms in the carbonaceous material tailors their surface properties accordingly, supporting a new idea to employ it as one active catalyst for mercury-free hydrochlorination.¹⁴⁻¹⁷ In addition, recently Dai et al. reported that AuCl₃/PPy-MWCNTs catalyst showed the benefits of the ⁴⁵ nitrogen promotion of Au³⁺ catalysts.¹⁸ The enhanced catalytic

performance was attributed to electron transfer from PPy to the Au³⁺ center, which increased the adsorption of hydrogen chloride. We have recently contributed to the field of Au-catalyzed acetylene hydrochlorination by discovering that the use of Cs^I as 50 a promoter can facilitate more efficient Au³⁺ active species stabilization under much harsher conditions.¹⁹These findings are useful for the design of highly active and stable acetylene hydrochlorination catalysts and have prompted us to consider whether the nitrogen-promoting effect can be applied to 55 bimetallic catalysts, to give further improved performance in the acetylene hydrochlorination reaction. In this work the effect of modification of nitrogen to activated carbon supported Au-Cs¹ catalysts has been investigated by synthesizing a 1Au4Cs¹/NAC catalyst and evaluating the material properties by several 60 characterization techniques (XPS, STEM, TPD, TPR) comparing it to 1Au4Cs¹/AC catalysts as reference.

Experimental

Materials

Activated carbon (marked as AC, NORIT ROX 0.8, pellets of 0.8 ⁶⁵ mm diameter and 5 mm length); HAuCl₄ • 4H₂O (the content of Au assay 49.7%); urea (99 wt.%); CsCl (99.9 wt.%); H₂O₂ (10 wt.%); glacial acetic acid (10 wt.%); C₂H₂ (gas, 98%); HCl (gas, 99.999%).

Catalyst preparation

- ⁷⁰ A commercially activated carbon NORIT ROX 0.8 was selected for the preparation of support. The activated carbon was first pretreated with HNO₃ (65 wt.%) at room temperature for 1 h. Subsequently, it was filtered, washed and then dried at 110 °C for 12 h (sample AC).
- 5 N-doped AC was prepared based on the process described

below.²⁰A mixture of AC (5 g), glacial acetic acid (3 mL) and distilled water (50 mL) was stirred for 30 min to obtain carbon slurry. Urea (3 g), H_2O_2 (10 mL) and deionized water (30 mL) were added, and the solution was stirred for 24 h at room s temperature in the dark. Finally, the solution was filtered and

calcined at 500 °C under a nitrogen atmosphere for 1 h. The obtained sample was labeled as NAC.

Supported bimetallic Au-Cs¹ catalysts were prepared using an incipient wetness impregnation technique. A $HAuCl_4 \cdot 4H_2O$ and

- ¹⁰ CsCl solution in *aqua regia* was added dropwise to the NAC or AC support with agitated stirring. After the solution was homogeneously mixed with the support, the system was aged at 40 °C for 4 h, followed by drying at 110 °C for 12 h for use. The obtained catalysts were labeled as 1Au4Cs^I/NAC and ¹⁵ 1Au4Cs^I/AC, respectively. Au loading in all the catalysts was
- fixed at 1.0 wt.%.

Catalyst characterization

The sizes of particles on samples were also observed by a transmission electron microscope (TEM, Tecnai G2 F30 S-Twin,

- ²⁰ 300 kV). The solid samples were finely ground. The resultant fine powders were dispersed ultrasonically in the ethanol and were then loaded on a copper grid (Beijing Zhongjingkeyi Technology Co., Ltd.).
- The elemental surface composition of the catalysts was ²⁵ controlled by XPS acquired with a Kratos AXIS Ultra DLD spectrometer. XPS analysis was performed with the monochromatized aluminum X-ray source and pass energy of the electron analyzer of 40 eV. The pressure in the sample analysis chamber was lower than 6×10^{-9} Torr during data acquisition. ³⁰ Binding energies were referred to the C1s line at 284.8 eV.

Temperature-programmed desorption (TPD) experiments were performed in a tubular quartz reactor. The samples (about 75 mg) were first treated in situ at 180 °C for 0.5 h using pure HCl and then cooled to room temperature in the same atmosphere. The

³⁵ sample was swept with pure Ar at a flow rate of 30 ml/min for 1 h to remove physisorbed and/or weakly bound species. TPD was performed by heating the sample from room temperature to 500 °C at a ramp rate of 10 °C min⁻¹ in pure Ar, and the TPD spectra were recorded by a quadrupole mass spectrometer (QMS ⁴⁰ 200 Omnistar).

Temperature-programmed reduction (TPR) experiments were carried out on a micro-flow reactor fed with a flow of hydrogen (5% in Ar) at a rate of 40 ml min⁻¹. The weight of the tested samples was (about) 75 mg. The temperature was increased from

⁴⁵ 30 to 850 °C at a rate of 10 °C min⁻¹. The hydrogen consumption was measured using a thermal conductivity detector (TCD).

Catalytic test

Catalysts were tested for acetylene hydrochlorination in a fixedbed glass microreactor (i.d. 10 mm). Acetylene (10 mL min⁻¹, 1 ⁵⁰ bar) and hydrogen chloride (12 mL min⁻¹, 1 bar) were fed though

- a mixing vessel via calibrated mass flow controllers to a heated glass reactor containing catalyst (200 mg), with a total GHSV (C_2H_2) of 1480 h⁻¹. A reaction temperature of 180 °C was chosen, blank tests using an empty reactor filled with quartz wool did not
- ss reveal any catalytic activity, and quartz sand was used to extend the bed length, above and below the catalyst itself, separated by quartz wool. The gas phase products were passed through an

absorption bottle containing NaOH solution to remove excess HCl first and then analysed on-line by GC equipped with a flame 60 ionisation detector (FID). Chromatographic separation and identification of the products was carried out using a Porapak N packed column.

Results and discussion



Fig.1 XPS spectra of (a) fresh 1Au4Cs¹/AC and 1Au4Cs¹/NAC samples normalized at 284.8 eV of C1s, (b) N1s spectrum for the fresh 1Au4Cs¹/NAC catalyst.

The XPS results shown in Fig. 1a confirm the elemental ⁷⁰ compositions of 1Au4Cs¹/AC and 1Au4Cs¹/NAC samples. The peaks at about 86.1, 200.6, 284.8, 399.5, and 725.6eV can be assigned to the binding energy of Au4f, Cl2p, C1s, N1s, O1s and Cs3d, respectively. The XPS spectrum of AC indicates that as the annealing temperature increases to 500 °C with doping carbon 75 with nitrogen atoms, the nitrogen signal can be clearly detected. Fig. 1b demonstrates the high-resolution XPS spectra based on the deconvoluted N1s spectra. The peak at 398.6, 400.4, 402.7 eV corresponds to pyridinic N. pyrrolic N and quaternary N. respectively.¹⁵ XPS analysis (Fig. 1b) reveals that three types of ⁸⁰ nitrogen species coexist in the 1Au4Cs¹/NAC catalyst. Recent observations suggest that carbon-based catalyst support materials can be systematically doped with nitrogen to create strong, beneficial catalyst-support interactions by increased support/catalyst chemical binding (or anchoring) which 85 substantially enhances catalyst activity and stability.²¹

The gold content by mass of the catalysts as determined by ICP-MS was 0.94 +/- 0.07 wt% for 1Au4Cs^I/AC and 0.95 +/-

15

60

0.05 wt% for 1Au4Cs¹/NAC. Fig. 1 shows two typical TEM micrographs. The small bright dots represent the metal particles; particles below 5 nm are dominant in 1Au4Cs¹/AC, though some are found up to 6 nm in diameter (Fig. 2a). In contrast, particles

- ⁵ below 3 nm are dominant in 1Au4Cs¹/NAC (Fig. 2b). Especially 1Au4Cs¹/AC showed a large particle size distribution. Most of the particles in 1Au4Cs¹/AC had particle sizes below 4 nm, with a small fraction between 4 and 6 nm. For 1Au4Cs¹/NAC, hardly any particles larger than 4 nm were observed. The average
- ¹⁰ particle size for 1Au4Cs¹/AC was 3.7 nm and for 1Au4Cs¹/NAC 2.3 nm. This indicates that adding nitrogen atoms had caused a decrease in Au NPs particle size.



Fig.2 Representative STEM figures of fresh 1Au4Cs¹/AC (a) and 1Au4Cs¹/NAC (b) and corresponding particle size distributions.

The catalytic performance of Au-base catalysts for acetylene hydrochlorination is shown in Fig.3. To accelerate the deactivate process of Au-based catalysts, higher GHSV (1480 h⁻¹) was carried out than that reported in the literature. NAC catalysts ²⁰ display very poor catalytic activity (5% conversion) for acetylene hydrochlorination reaction (not shown), while no conversion was detected in AC. In fact, experimental studies and theoretical simulations revealed that the carbon atoms bonded with pyrrolic nitrogen atoms as active sites can deliver limited activity have ²⁵ been reported by Bao's group before.¹⁵

The catalyst evaluation data in Fig. 3b shows that 1Au4Cs^I/AC had good performance with the acetylene conversion of 1Au4Cs^I/AC catalyst decreases from 89.2% down to 80.1% after running for 50 h, indicating that 1Au4Cs^I/AC is slightly ³⁰ deactivated under this reaction conditions. As a comparison, the 1Au4Cs^I/NAC catalyst exhibits a similar initial performance with 1Au4Cs^I/AC, and its C₂H₂ conversion reaches 90.1% at 4 h (Fig. 3a). At the same time, 1Au4Cs^I/NAC had stable conversion without significant decline in activity is observed in the reaction

35 time (89.6% at 50 h). Thus, the results suggest that the nitrogendoped catalysts (1Au4Cs^I/NAC) exhibited improved catalytic stability as well as a slightly increased catalytic activity. This indicates the effectiveness of nitrogen doping in tuning the reactivity. Dai and coworkers ¹⁸ have indicated an improved 40 activity and stability upon the addition of nitrogen atoms to Aubased acetylene hydrochlorination catalysts (AuCl₃/PPy-MWCNT). On the one hand, it has been reported that the incorporation of nitrogen atoms increased the electron density of the Au³⁺ center via the transfer of lone pair electrons on the ⁴⁵ nitrogen atom to the Au³⁺ center. On the other hand, Au³⁺ species is the electron donor in the adsorption process of hydrogen chloride. Thus, it is most likely that this promoting effect of 1Au4Cs^I/NAC bimetallic catalysts during acetylene hydrochlorination is related to the increased electron-donating ⁵⁰ capability of Au³⁺ for hydrogen chloride adsorption, which is due to the increased electron density of Au³⁺ as a result of electron transfer from nitrogen atom. This will be discussed in the HCl-TPD analysis. It should be highlighted that for all the tests carried out and reported in the current study, the selectivity to vinyl ss chloride was virtually 100% with trace amounts (< 0.1%) of 1,2dichlorethane and chlorinated oligomers only throughout the entire run period according to the spectrum of TCD.



Fig.3 Conversion of acetylene to VCM in acetylene hydrochlorination over (a) 1Au4Cs¹/NAC and (b) 1Au4Cs¹/AC catalysts, respectively.



Fig.4 TPR intensities for the reduction of Au^{3+} species for fresh and used $1Au4Cs^{I}/AC$ (a) and $1Au4Cs^{I}/NAC$ (b) catalysts.

Fig. 4 shows the TPR profiles for the fresh and used Au-base ⁶⁵ catalysts. For all the catalysts, a distinguishable hydrogen

consumption peak in the range of 400-800 °C can be observed,



Fig.5 XPS spectrum and simulation for the samples: (a) fresh 1Au4Cs¹/AC catalyst, (b) used 1Au4Cs¹/AC catalyst, (c) fresh 1Au4Cs¹/NAC catalyst, (d) used 1Au4Cs¹/NAC catalyst.

which can be attributed to the reduction of the surface groups of ${}^{\scriptscriptstyle 10}$ activated carbon at the carbon surface, which releases CO and CO_2 with concomitant reduction of oxygenated groups by ${\rm H_2}$ in

the TPR stream. More specifically, the profile can befitted with two contributions. The reduction bands in the range of 400-650 °C can be assigned to the decarboxylation reactions of carboxylic 15 acids and carboxylic anhydrides groups,²² while above 650 °C, these are likely due to the reduction of lactones and phenols.²³ As mentioned before, this phenomenon on the carbon matrix should be considered a consequence of using HNO₃ in the washing step, which induced modifications on the carbon surface inducing 20 oxygenated functional groups, as well as changes in the textural properties of the carbon support. In addition, the analysis of 1Au4Cs^I/AC sample led to assign the reduction band around 322 °C to Au³⁺ to Au⁰ (Fig. 4a). Besides, a straightforward decrease of temperature in the reduction band of Au³⁺ to 309 °C was 25 observed (Fig. 4b) for 1Au4Cs¹/NAC, this shifts indicate strong interactions between Au species and nitrogen atoms exists in 1Au4Cs^I/NAC catalysts. Through comparing the TCD signals with a standard, the fractions of different Au species in these fresh catalysts can be estimated. This allows an estimation of 30 ca.46.8, and 38.8% for the 1Au4Cs^I/AC and 1Au4Cs^I/NAC catalysts, respectively. As in the case of used 1Au4Cs^I/AC, the reduction peak of Au³⁺ to Au⁰ is evidently decreased comparing with the fresh one, which shows a degree of Au^{3+} reduction to Au⁰ during acetylene hydrochlorination. In contrast, the reduction 35 peak of Au³⁺ to Au⁰ is negatively observed for 1Au4Cs^I/NAC comparing with the fresh one. Also through comparing the TCD signals with a standard, this allows an estimation of ca. 27.8 and 36.2% for the used 1Au4Cs¹/AC and 1Au4Cs¹/NAC catalysts, respectively. This result showed that the presence of nitrogen ⁴⁰ atoms in the 1Au4Cs¹/NAC catalyst partly inhibited the reduction of Au³⁺, which can further stabilize the catalytic active Au³⁺ species in the reaction process of AuCl₃ catalysts. This result is consistent with the excellent catalytic activity and stability of the 1Au4Cs^I/NAC catalyst. It is worth noting that the result revealed ⁴⁵ in this study, i.e., that the 1Au4Cs^I/AC presents higher amount of Au³⁺ compared with the 1Au4Cs^I/NAC, however, the activity of 1Au4Cs^I/AC is no more than 1Au4Cs^I/NAC. In fact, according to

needed for the reaction, exceeding a given threshold will not ⁵⁰ further increase the activity.²⁴ By using TPR determinations, the optimal Au³⁺ amount would be about ca. 30 %, with excess amounts not affecting the reactivity of the catalyst, which is consistent with the catalytic performance of 1Au4Cs¹/AC and 1Au4Cs¹/NAC catalysts (see Fig. 3).

Hutchings et al., the increasing amount of Au³⁺, being clearly

Since previous literature studies ascribed the activity of the 55 Au-base catalyst to the presence of Au³⁺ species postulating them as active sites. In order to obtain a correlation on the activity of VCM production with the amount of Au³⁺ species clusters made on the catalyst surface and the valence state changes of the 60 catalyst structure before and after the reaction, samples tested for the acetylene hydrochlorination at different composition were then carefully analysed by XPS. It should be noted that where more than one Au species was evident, curve fitting was employed to determine the ratio of each species (Fig. 5). The 65 XPS spectra of Au 4f level for all samples were deconvoluted into three pairs of peaks for Au⁰, Au³⁺ and Au⁰-s species, respectively.²⁴⁻²⁵ Table 1 lists the binding energy and the relative content of each Au species in the fresh and used catalysts. The full-width-half-maximum (FWHM) values of Au peaks were also

summarized in Table 1. It is worth mentioning that the FWHM of Au³⁺ peaks obtained for both fresh and used bimetallic catalysts are very close. Due to the reduction property of carbon towards Au^{3+} , there is a large number of Au^{0} in fresh Au-base catalysts 5 (Table 1).⁴ It should also be stressed that some small metallic gold clusters (Au⁰-s) are also formed in the fresh 1Au4Cs^I/AC and 1Au4Cs^I/NAC catalyst, which coincided well with the previous publications.²⁴⁻²⁵ However, the Au⁰-s species are inactive and not involving in the reaction, since the reduced 10 catalysts also contain these Au⁰-s clusters and they displayed negligible catalytic activity (< 5% conversion) for acetylene hydrochlorination under the same conditions (not shown), illustrating that the presence of Au³⁺ was indispensable for high catalytic activity and the Au⁰-s species are inactive and not 15 involving in the reaction. It has also been confirmed by other researchers ²⁴⁻²⁵ that reduced Au-base catalysts containing only Au⁰-s and Au⁰ clusters can not activate acetylene directly. In fresh 1Au4Cs^I/AC and 1Au4Cs^I/NAC samples, the relative content of Au³⁺ is 32.6% and 31.4%, respectively (Table 1). The 20 higher content of Au3+ in 1Au4CsI/AC can be observed. Under the reaction conditions, Au³⁺ is reduced into Au⁰, contributing to the deactivation of the Au catalyst. In the case of 1Au4Cs¹/AC

catalysts after reaction, only 20.5% Au³⁺ species presents (Table 1), demonstrating that a reduction and/or agglomeration of Au^{3+} 25 species occurs in the reaction process. In contrary, in the used 1Au4Cs¹/NAC catalyst, there are still large amounts of Au³⁺ (30.6%), indicating that the incorporation of the nitrogen atoms helps to keep the active Au³⁺ species stable at high temperature under reducing atmosphere. The Au3+ amount obtained by XPS 30 are lower than those obtained by H2-TPR can be ascribed to that XPS is known to cause chemical and structural changes within several investigated molecules. For example, Karadas published an overview of the HAuCl₄ photoreduction process from Au³⁺ to Au⁰ when exposed to 1253.6 eV Mg K α (nonmonochromatized) 35 radiation.²⁵ Together with further contributions from Ozkaraoglu et al., Karadas and co-workers showed that the disappearance of Au³⁺ peaks in the XPS spectra occur via first-order kinetics but at differing rates.²⁷⁻²⁸ In view of this, the content of Au³⁺ obtained by XPS always lower than those obtained by TPR is reasonable. ⁴⁰ In combination with the catalytic performances of these catalysts (Fig. 3), it is reasonable to conclude that a high content of Au^{3+} leads to the best catalytic performance, as displayed by the 1Au4Cs^I/NAC.

 Table 1 Quantification and identification from XPS of Au species over Au-base catalysts

Catalysts	Au species (%)			(Binding energy) +/- (FWHM) (eV)		
	Au ³⁺	Au ⁰	Au ⁰ -s	Au ³⁺	Au^0	Au ⁰ -s
1Au4Cs ^I /AC fresh	32.6	59.2	8.2	(86.7) +/- (1.4)	(84.3) +/- (1.3)	(85.4) +/- (1.7)
1Au4Cs ^I /AC used	20.5	66.5	13.0	(86.7) +/- (1.5)	(84.3) +/- (1.4)	(85.5) +/- (1.4)
1Au4Cs ^I /NAC fresh	31.4	41.2	27.4	(87.0) +/- (1.4)	(84.3) +/- (1.2)	(85.1) +/- (1.3)
1Au4Cs ^I /NAC used	30.6	55.1	14.3	(87.3) +/- (1.5)	(84.8) +/- (1.1)	(85.8) +/- (1.2)



Fig.6 TPD profiles of hydrogen chloride on different samples: (a) $1Au4Cs^{I}/AC$ and (b) $1Au4Cs^{I}/NAC$.

HCl-TPD is also used to characterize the active sites for the hydrogen chloride adsorption. As shown in Fig. 6, the ⁵⁰ 1Au4Cs^I/AC and 1Au4Cs^I/NAC catalysts presented a band between 50 and 400 °C, which was characteristic of hydrogen chloride desorption. However, the areas of the HCl-TPD peaks for the 1Au4Cs^I/NAC catalyst were much larger than for 1Au4Cs^I/AC catalyst. This suggested that the increase in ⁵⁵ chemisorbed hydrogen chloride on 1Au4Cs^I/NAC compared with

1Au4Cs^I/AC. The observed adsorption was caused by the interaction between nitrogen and Au³⁺, which changed the nature of the catalyst itself. The favorable adsorption of hydrogen chloride on 1Au4Cs^I/NAC can be explained by the transfer of ⁶⁰ nitrogen π electrons to the empty orbital of gold, which enhanced the electron-donating ability of gold and allowed the catalyst to combine with more hydrogen chloride.¹⁸ It is reported in the literature that when hydrogen chloride and acetylene coadsorbed on the AuCl₃, the acetylene was co-catalyzed by hydrogen 65 chloride and the AuCl₃ to produce vinyl chloride. In contrast, if the hydrogen chloride in the gas phase could not adsorb on the Au sites, the intermediate chlorovinvl was difficult to desorb from the AuCl₃ catalyst that resulted in the side reaction and the rapid deactivation of the AuCl₃ due to the loss of Cl atoms and 70 consequently loses its activity.²⁹ Based on the above understanding, the adsorption of hydrogen chloride is very important for the stability of AuCl₃ catalyst, for one thing, is beneficial for improving the catalytic activity, for another, hydrogen chloride can remain Au in its oxidative state and inhibit ⁷⁵ the active Au^{3+} species reduced by C_2H_2 . Thus, it is clearly that doping of carbon materials with nitrogen atoms can enhance the adsorption of hydrogen chloride and activate acetylene, and hence the hydrochlorination of acetylene.

Conclusions

In summary, we have successfully demonstrated that the doping of nitrogen can efficiently further enhance the catalytic performance of Au-Cs^I bimetallic catalysts. The doped 1Au4Cs^I/NAC catalysts with a total nitrogen content of 2.9 wt.% are quite stable and more active for the hydrochlorination of acetylene. The enhanced catalytic performance may due to that ⁵ nitrogen atoms strongly interacted with Au species and

- strengthened the ability of the resultant catalysts to adsorb hydrogen chloride and inhibit the reduction of Au^{3+} to Au^{0} during acetylene hydrochlorination and hence improve the catalytic stability. The excellent catalytic performance of the
- ¹⁰ 1Au4Cs¹/NAC catalyst demonstrated its potential as an alternative to mercury chloride catalysts for acetylene hydrochlorination.

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