# RSC Advances



This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

*Accepted Manuscripts* are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. This *Accepted Manuscript* will be replaced by the edited, formatted and paginated article as soon as this is available.

You can find more information about *Accepted Manuscripts* in the Information for Authors.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard Terms & Conditions and the Ethical quidelines still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.



www.rsc.org/advances

Cite this: DOI: 10.1039/c0xx00000x

www.rsc.org/xxxxxx

## **ARTICLE TYPE**

### **Functionalized phosphonium based ionic liquids: properties and application in metal extraction**

**Alessandra Caterina Barsanti, Cinzia Chiappe,\* Tiziana Ghilardi and Christian Silvio Pomelli** 

*Received (in XXX, XXX) Xth XXXXXXXXX 20XX, Accepted Xth XXXXXXXXX 20XX*  <sup>5</sup>**DOI: 10.1039/b000000x** 

The extraction of Cu(II), Zn(II), Co(II), Ni(II) and Pb(II) from model aqueous solutions using phosphonium based ionic liquids as sole extraction agents has been explored. The hydrophobic trioctyl(4-vinylbenzyl) phosphonium chloride,  $[P_{888(4-VB)}]C$ , allows almost complete removal of Pb(II), Cu(II), Zn(II) without addition of HCl, while the extraction of Co(II) and Ni(II) was almost null. An efficient extraction (*ca.*100%) of Pb(II), Cu(II) and Zn(II) was 10 obtained using  $[P_{888(4-VB)}][NO_2]$ .

#### **Introduction**

Phosphonium salts constitute an important sub-class of ionic liquids (ILs) which are known to have important properties, 15 sometimes superior in comparison with those of the widely

- investigated nitrogen-based ILs, in particular-dialkylimidazolium salts. Tetraalkylphosphonium ILs generally present greater inertness under basic conditions<sup>1</sup> and increased thermal and electrochemical stabilities.<sup>2</sup> Their potential applications include
- <sup>20</sup>the use as electrolytes for batteries and dye-sensitized solar cells, as corrosion inhibitors, lubricants, reaction media and extraction agents. However, this class of ILs has been less systematically studied than nitrogen-based ILs and some detailed studies about the physicochemical and thermal properties of <sup>25</sup>tetralkylphosphonium chlorides have been only recently
- published.<sup>3</sup> The principal drawbacks limiting their use are the high viscosity and the physical state (solid) at room temperature. However, analogously with nitrogen based ILs, a careful selection of anion
- <sup>30</sup>and substituents on cation can minimize these problems. For example, it has been shown<sup>4</sup> that trialkyl benzyl phosphonium cations combined with bis(trifluoromethanesulfonyl)imide anion can effort low-melting salts with high thermal stability and conductivity. On the other hand, hydrophobic and polar ILs,
- 35 exhibiting stable phase separation and high hydrogen bonding ability after mixing with water, have been obtained coupling tetraalkylphosphonium cations (in particular, tetra-*n*hexylphosphonium and tri-*n*-hexyl-*n*-octylphosphonium) with ethylphosphonate anion.<sup>5</sup> It is noteworthy that phosphonium
- <sup>40</sup>cations can give hydrophobic ILs also when two hydroxyl groups are introduced on the alkyl chains: trioctyl(2,3 dihydroxypropyl)phosphonium chloride is only partially soluble in water and the analogous bis(trifluoromethanesulfonyl)imide salt is completely insoluble.<sup>6</sup>
- $45$  It has been previously suggested<sup>6</sup> that the ability of these hydrophobic dihydroxyl functionalized ILs to complex metals

might be exploited not only in catalysis but also for other peculiar applications, such as extraction of metals and water remediation from industrial wastes and effluents. Liquid-liquid extraction is <sup>50</sup>one of the most important techniques employed for metal ion separation. The possibility to operate in continuous mode, using relatively simple equipment and employing only small amounts of the reagents are surely some of the advantages.<sup>7</sup> The principal drawback of classical liquid-liquid extraction<sup>8</sup> is however the use <sup>55</sup>of flammable, volatile or toxic water-immiscible solvents. The employ of ILs as water-immiscible extractants has been considered as an important alternative approach to improve the sustainability of the process.<sup>9</sup> However, as stated by Binnemans *et al.*,<sup>7</sup> the application of ILs as solvents for the extraction of <sup>60</sup>metal ions has only partially met the high expectations. Due to the high hydrophilicity of hydrated metal ions often other extractants have to be added. Moreover, extraction of metal ions from water solution to IL generally occur *via* an ion exchange mechanism: thus, IL cations are lost during extraction of a metal <sup>65</sup>ion with a neutral extractant, whereas ILs anions are lost when anionic metal complexes are extracted.<sup>10</sup> Finally, problems can arise for the application of ILs in water recovery if a significant dissolution of the IL in the aqueous phase occurs during the extraction process. Although these losses can be reduced 70 modifying the IL's structure through the introduction of long alkyl or fluorinated chains, thus increasing IL hydrophobicity, the same structural alterations often have negative effects on extraction efficiency. Unfortunately, hydrophobic ILs generally contain fluorinated anions which can release HF after prolonged 75 contact with water (in particular,  $[BF_4]$  and  $[PF_6]$ ) or are quite expensive. Phosphonium salts are actually an exception: they give hydrophobic salts also with the hydrophilic, not expensive and ecofriendly chloride as counteranion. Tetralkylphosphonium chlorides in toluene or kerosene have been used in extraction of

so metal ions (from aqueous solutions).<sup>11</sup> More recently, they are been used as undiluted solvents for separation of nickel by cobalt from 8M HCl aqueous solutions.<sup>7</sup>

Considering the potential binding ability of the *vic*-diol moiety towards metal cations, we decided to investigate the possibility to apply trioctyl(2,3-dihydroxypropyl)phosphonium salts with chloride, hexafluorophosphate,

<sup>5</sup>bis(trifluoromethanesulfonyl)imide and nitrite counteranion (**1**) in the extraction of several common heavy metal pollutants (Cu(II),  $Zn(II)$ ,  $Ni(II)$  and  $Pb(II)$ ) and  $Co(II)$  from water, avoiding the addition of HCl to the aqueous phase.

The extraction efficiency of these ILs was furthermore compared

10 with that of another class of hydrophobic phosphonium salts based on trioctyl(4-vinylbenzyl) phosphonium cation (**2**). The polymerizable nature of the vinyl group might be useful to develop immobilized ILs for metal separation from water.



$$
X = CI, PF_6, BF_4, NO_2, Tf_2N
$$

15

The main physicochemical (viscosity, conductivity and polarity) properties of these phosphonium salts were determined. The effect of IL structure on metal extraction was evaluated <sup>20</sup>determining extraction percentages by ICP-MS.

#### **Experimental**

NMR spectra were recorded at room temperature using a Bruker instrument at 250 MHz ( ${}^{1}H$ ) and 75.7 MHz ( ${}^{13}C$ ), in DMSO- $d_6$ ,  $_{25}$  CDCl<sub>3</sub> or D<sub>2</sub>O. ICP-MS analyses were carried out using Agilent

7500 ce instrument.

Trioctyl(2,3-dihydroxypropyl)phosphonium chloride,  $[P_{8,8,8(gly)}]$ Cl, hexafluorophosphate,  $[P_{8,8,8(gly)}]$ [PF<sub>6</sub>] and bis(trifluromethanesulfonyl)imide,  $[P_{8,8,8(gly)}][Tf_2N]$  were

30 prepared as previously reported.<sup>6</sup> CuCl<sub>2</sub>  $2H_2O$  (>99.0%), ZnCl<sub>2</sub> (>98%), NiCl<sub>2</sub>·6H<sub>2</sub>O (> 99.9 %), CoCl<sub>2</sub>·6H<sub>2</sub>O (>98%), ZnCl<sub>2</sub> (>98%) were purchased from Aldrich.

#### **Trioctyl(2,3-dihydroxypropyl)phosphonium nitrite,**

**[P8,8,8(gly)][NO<sup>2</sup>** <sup>35</sup>**]** 

To a solution of trioctyl(2,3-dihydroxypropyl)phosphonium chloride,  $[P_{8,8,8(glv)}]$ Cl, (16 g, 33 mmol) in acetonitrile (10 ml) an equimolar amount of  $AgNO<sub>2</sub>$  (yellow solid, freshly prepared from  $AgNO<sub>3</sub>$  and  $NaNO<sub>2</sub>$  in water) was added. The mixture was stirred

<sup>40</sup>at room temperature for 24h, then the precipitate was filtered off and the resulting aqueous solution was evaporated at reduced pressure. The residue liquid was dissolved in anhydrous acetone and the solution was cooled at -40°C for 48 h. After filtration on glass septa (porosity 4) containing two different powdered layers

<sup>45</sup>of 1 cm each of celite (lower layer) and decolorizing carbon

(upper layer), the solvent was removed at reduced pressure. The isolated IL was dried under vacuum  $(2x10^{-3} \text{ mm Hg}, 80^{\circ}\text{C}, 6h)$ and analyzed by NMR.

<sup>1</sup>H NMR (DMSO-d<sub>6</sub>,  $\delta$  ppm): 6.00 (s, 1H, OH), 5.23 (s, 1H, OH), 50 3.90 (m, 1H, CHOH), 3.38 (m, 2H, CH<sub>2</sub>OH), 2.41 (m, 8H,  $P^+CH_2$ ), 1.25 (m, 36H, CH<sub>2</sub>), 0.86 (m, 9H, CH<sub>3</sub>); <sup>13</sup>C NMR (DMSO-d<sub>6</sub>, δ ppm): 66.6 (m, CH<sub>2</sub>OH, CHOH), 31.3, 30.2 (d, *J* = 15 Hz), 28.4, 28.2, 23.3 (d,  $J = 47$  Hz,  $P^+CH_2CH(OH)CH_2OH$ ), 22.5, 21.2 (d,  $J = 4.5$  Hz), 19.1 (d, 47Hz P<sup>+</sup>CH<sub>2</sub>CH<sub>2</sub>CH<sub>2</sub>CH<sub>2</sub><sup>-</sup>), <sup>55</sup>14.2.

**Trioctyl(4-vinylbenzyl)phosphonium chloride, [P8,8,8(4-VB)]Cl** 

Under an argon atmosphere, trioctylphosphine (16,7 g, 45 mmol) was added to a solution of 1-(chloromethyl)-4-vinylbenzene (6,87

- <sup>60</sup>g, 45 mmol) in toluene (20 ml), previously accurately deareated and containing a small amount of 2,6-di-*tert*-butyl-4 methylphenol as radical inhibitor. The resulting mixture was stirred for 48 h at room temperature, then the solvent was removed at reduced pressure and the resulting white solid (99%
- <sup>65</sup>yield) was washed with ethyl acetate, dried under vacuum and analyzed by NMR. The  ${}^{1}H$  NMR spectrum exactly matched literature data.<sup>12</sup>

<sup>1</sup>H NMR (CDCl<sub>3</sub>,  $\delta$  ppm): 7.32 (m, 2H, aromatic CH), 7.18 (m, 2H, aromatic CH),  $6.65$  (dd, J = 17, 11 Hz, 1H, CH=), 5.70 (d, J =

 $\pi$  17 Hz, 1H, =CH<sub>2</sub>), 5.25 (d, J = 11 Hz, 1H, =CH<sub>2</sub>), 4.30 (d, J = 15 Hz, 2H, P<sup>+</sup>CH<sub>2</sub>Ph), 2.33 (m, 6H, P<sup>+</sup>CH<sub>2</sub>Ph), 1.18 (m, 36H, CH<sub>2</sub>), 0.83 (m, 9H, CH<sub>3</sub>). <sup>13</sup>C NMR (CDCl<sub>3</sub>,  $\delta$  ppm): 137.6, 135.9, 130.4, 129.0, 128.2, 127.1, 114.9, 31.7, 30.9 (d, *J* = 15 Hz), 28.4, 28.2, 26.5 (d,  $J = 47.5$  Hz,  $P^+CH_2Ph$ ), 22.6, (d,  $J = 4.5$  Hz), 19.1 75 (d, 47 Hz,  $P^+CH_2CH_2CH_2CH_2, 14.2$ .

#### **Trioctyl(4-vinylbenzyl)phosphonium hexafluorophosphate,**   $[P_{8,8,8(4-VB)}][PF_6]$

To a solution of  $[P_{8,8,8(4-VB)}]$ Cl (12 g, 23 mmol) in water-ethanol  $\text{so (2:1, 20 ml)}$  HPF<sub>6</sub> (2.23 ml, 25 mmol) was added and the resulting reaction mixture was stirred at room temperature for 24 h. The resulting biphasic system was separated and the nonaqueous phase was diluted with dichloromethane and repeatedly washed with water (3 x 10 ml). The organic phase was dried

(MgSO<sup>4</sup> <sup>85</sup>) and concentrated at reduced pressure to give 13.8 g of  $[P_{8,8,8(4-VB)}][PF_6]$  as a colourless liquid.

<sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm): 7.38 (m, 2H, aromatic CH), 7.26 (m, 2H, aromatic CH), 6.65 (dd, J = 17, 11 Hz, 1H, CH=), 5.70 (d, J = 17 Hz, 1H,  $=CH_2$ ), 5.30 (d, J = 11 Hz, 1H,  $=CH_2$ ), 3.80 (d, J = 15

90 Hz, 2H, P<sup>+</sup>CH<sub>2</sub>Ph), 2.13 (m, 6H, P<sup>+</sup>CH<sub>2</sub>Ph), 1.23 (m, 36H, CH<sub>2</sub>), 0.87 (m, 9H, CH<sub>3</sub>). <sup>13</sup>C NMR (CDCl<sub>3</sub>, δ ppm): 137.6, 135.9, 130.4, 129.0, 128.2, 127.1, 114.9, 31.7, 30.9 (d, *J* = 15 Hz), 28.4, 28.2, 26.5 (d,  $J = 47.5$  Hz,  $P^+CH_2Ph$ ), 22.6, (d,  $J = 4.5$  Hz), 19.1  $(d, 47 \text{ Hz}, \text{ P}^+ \text{CH}_2\text{CH}_2\text{CH}_2\text{CH}_2), 14.2.$ 

#### **Trioctyl(4-vinylbenzyl)phosphonium bis(trifluoromethane)sulfonimide, [P8,8,8(4-VB)][Tf2N]**

95

A round bottom flask was charged with  $[P_{8,8,8(4\text{-}VB)}]Cl$  (12.00 g, 23 mmol) and a mixture of ethanol and water (2 : 1) (20.0 mL)  $_{100}$  then Li(Tf<sub>2</sub>N) (7.1 g, 25.2 mmol) was added in one portion under stirring. The resulting reaction mixture was stirred at 60 °C

for 18h and diluted with  $CH_2Cl_2$  and water. The organic phase was repeatedly washed with water (3 x10 ml), concentrated at reduced pressure and dried at 70 °C for 18 h under high vacuum to give 16.7 g (95%) of  $[P_{8,8,8(4-VB)}][Tf_2N]$  as a colorless liquid. The <sup>1</sup>H  $5$  NMR spectrum exactly matched literature data.<sup>11</sup>

<sup>1</sup>H NMR (CDCl<sub>3</sub>, δ ppm): 7.41 (m, 2H, aromatic CH), 7.21 (m, 2H, aromatic CH),  $6.65$  (dd, J = 17, 12 Hz, 1H, CH=), 5.70 (d, J = 17 Hz, 1H,  $=CH_2$ ), 5.30 (d, J = 12 Hz, 1H,  $=CH_2$ ), 3.60 (d, J = 14 Hz, 2H, P<sup>+</sup>CH<sub>2</sub>Ph), 2.06 (m, 6H, P<sup>+</sup>CH<sub>2</sub>Ph), 1.23 (m, 36H, CH<sub>2</sub>),

- 10 0.87 (m, 9H, CH<sub>3</sub>). <sup>13</sup>C NMR (CDCl<sub>3</sub>, δ ppm): 137.6, 135.9, 129.2, 129.0, 128.2, 127.1, 114.9, 31.7, 30.9 (d, *J* = 15 Hz), 28.9, 28.7, 26.5 (d,  $J = 47.5$  Hz,  $P^+CH_2Ph$ ), 22.6, (d,  $J = 4.5$  Hz), 19.1  $(d, 47 \text{ Hz}, \text{ P}^+ \text{CH}_2\text{CH}_2\text{CH}_2\text{CH}_2), 14.2.$
- **Trioctyl(4-vinylbenzyl)phosphonium nitrite, [P8,8,8(4-VB)][NO<sup>2</sup>** <sup>15</sup>**]**  To a solution of trioctyl(4-vinylbenzyl)phosphonium chloride,  $[P_{8,8,8(4-VB)}]$ Cl, (16 g, 30.6 mmol) in acetonitrile (10 ml) an equimolar amount of  $AgNO<sub>2</sub>$  (yellow solid, freshly prepared from  $AgNO<sub>3</sub>$  and  $NaNO<sub>2</sub>$  in water) was added. The mixture was stirred
- <sup>20</sup>at room temperature for 24h, then the precipitate was filtered off and the resulting aqueous solution was evaporated at reduced pressure. The residue liquid was dissolved in anhydrous acetone and the solution was cooled at -40°C for 48 h. After filtration on glass septa (porosity 4) containing two different powdered layers
- <sup>25</sup>of 1 cm each of celite (lower layer) and decolorizing carbon (upper layer), the solvent was removed at reduced pressure. The isolated IL was dried under vacuum  $(2x10^{-3}$  mm Hg, 80°C, 6h) and analyzed by NMR.

<sup>1</sup>H NMR (CDCl<sub>3</sub>,  $\delta$  ppm): 7.35 (m, 2H, aromatic CH), 7.26 (m,

<sup>30</sup>2H, aromatic CH), 6.65 (dd, J = 17, 11 Hz, 1H, CH=), 5.74 (d, J = 17 Hz, 1H,  $=CH_2$ ), 5.27 (d, J = 11 Hz, 1H,  $=CH_2$ ), 4.07 (d, J = 15 Hz, 2H, P<sup>+</sup>CH<sub>2</sub>Ph), 2.27 (m, 6H, P<sup>+</sup>CH<sub>2</sub>Ph), 1.21 (m, 36H, CH<sub>2</sub>), 0.85 (m, 9H, CH<sub>3</sub>). <sup>13</sup>C NMR (CDCl<sub>3</sub>, δ ppm): 137.6, 135.9, 129.2, 129.0, 128.2, 127.1, 114.9, 31.7, 30.9 (d, *J* = 15 Hz), 28.4, 35 28.2, 26.5 (d,  $J = 47.5$  Hz,  $P^+ \underline{C} H_2P$ h); 22.6, (d,  $J = 4.5$ ), 19.1 (d, 47 Hz,  $P^+CH_2CH_2CH_2CH_2$ , 14.2.

#### **Measurements of Physical Properties**

The viscosity of each liquid compound was measured using Brookfield  $DV-II + Pro$  instrument equipped with a Brookfield <sup>40</sup>TC-502 water bath. The viscometer was calibrated over the

- temperature range  $20 100$  °C using reference oils and ionic liquids. Conductance measurements were performed using a CON 510 bench meter supplied with conductivity/TDS electrode. This electrode has a stainless steel ring and a cell constant of
- <sup>45</sup>K=1.0. It also has an inbuilt temperature sensor for automatic temperature compensation. UV−vis absorption spectra of solvatochromic dyes (Reichardt's betaine dye, *N*,*N*-diethyl-4 nitroaniline and 4-nitroaniline) dissolved in ILs recorded with a Cary 2200 spectrophotometer employing 1 mm path length quartz
- 50 cell. Individual stock solutions of Reichardt's betaine dye, *N*,*N*diethyl-4-nitroaniline and 4-nitroaniline were prepared in dichloromethane. In order to prepare a given dye/IL solution, the appropriate amount of the dye stock solution was transferred into a quartz cuvette. Residual dichloromethane was evaporated under
- <sup>55</sup>gentle stream of argon gas in dry box. The IL was then added to the cuvette. The cuvette was sealed and the sample was hand

mixed for several times before the measurements. To prevent dye aggregation, the dye concentration was chosen low enough but sufficient to allow an absorbance value of about 0.2.

#### <sup>60</sup>**Extraction experiments**

Extraction of metal ions from water was performed as follows. Aqueous stock solutions of metal salts were prepared by addition of the proper metal chloride to 1 L of highly purified water (Milli-Q). Each solution was diluted 1:10 to obtain a <sup>65</sup>concentration of metal ions of 100 ppm.

*Procedure 1*: 0.5 g of dried IL were added to 1.5 g of the proper aqueous metal stock solution (metal concentration 100 ppm). The resulting two phases were mixed using an ultra high vibration shaker (Vortex 3) for 10 min, then the mixture was centrifuged at

<sup>70</sup>3000 rpm for 10 min to favour phases separation. After that, the metal concentration in the aqueous phase was determined by ICP-MS.

*Procedure 2*: 0.5 g of dried IL were added to 1.5 g of the proper aqueous metal stock solution (metal concentration 100 ppm). The <sup>75</sup>resulting two phases were mixed using an ultra high vibration shaker (Vortex 3) for 10 min, then the resulting mixture was centrifuged at 3000 rpm for 10 min. After that, the organic phase was reused and another extraction was performed, as described in procedure 1 (see above). Subsequently, the metal concentration in  $80$  the two aqueous phases were determined by ICP-MS.

- *Procedure 3*: 0.5 g of dried IL were added to 1.5 g of the proper aqueous metal stock solution (metal concentration 100 ppm). The resulting two phases were mixed using an ultra high vibration shaker (Vortex 3) for 10 min, then the resulting mixture was
- 85 centrifuged at 3000 rpm for 10 min. After that, the aqueous phase was re-extracted with fresh IL. The procedure was repeated two times. Finally, after three subsequent extractions, the metal concentration in the aqueous phase was determined by ICP-MS. Experimental results, collected at least in duplicate, agree within <sup>90</sup>5%.

Extraction percentage is calculated as follows:

$$
E\% = \left(\frac{[M]_{aq,l} - [M]_{aq}}{[M]_{aq,i}}\right) \times 100
$$

95 Where  $[M]_{aq,i}$  is the initial metal concentration in the aqueous phase before extraction,  $[M]_{aq}$  is the metal concentration in the aqueous phase after extraction.

#### **Results and Discussion**

The synthesis of phosphonium salts was performed by reacting 100 commercial trioctylphosphine with 3-chloropropane-1,2-diol or 1-(chloromethyl)-4-vinylbenzene under an inert atmosphere (see experimental) to prevent oxidation of trialkylphosphine. Phosphonium chlorides were then converted into the corresponding hexafluorophosphates, tetrafluoroborates, <sup>105</sup>bis(trifluoromethane)sulfonylamides and nitrites through metathesis reactions. As expected, ILs **1-2** appeared as viscous liquids and although the factors that determine ILs viscosity are still not fully understood, a dependence on ionic structure could be immediately evidenced. Table 1 reports some fundamental 110 properties (viscosity, conductivity) of ILs 1 and 2 at 20 °C. 50

55

Viscosities and conductivities were measured at several temperatures between 20 and 80 °C.





<sup>5</sup><sup>a</sup>Measured at 40 °C

For these salts, a striking decrease of viscosity on increasing temperature was generally observed and, in agreement with the behaviour characterizing most ILs, the temperature dependency only approximately follows the Arrhenius equation 1, where  $E_n$  is 10 the activation energy for viscous flows, and lnn<sub>∞</sub> is the viscosity

at infinite temperature, over the examined temperature range (20- 80 °C).

$$
ln \eta = ln \eta_{\infty} + E_{\eta} / RT \qquad (1)
$$

The Arrhenius plots (here not reported) show indeed a slight <sup>15</sup>upward curvature. In contrast, the Vogel-Fulcher-Tammann (VFT) equation 2 (where  $\eta_0$  (cP), B (K), and T<sub>0</sub> (K) are fitting parameters) with few exceptions is able to model the temperature effect:

$$
\eta = \eta_0 \, e^{B/(T-T_0)} \tag{2}
$$

The optimized parameters and related correlation coefficients are reported in Table 2 together with the Arrhenius parameters. The calculated viscosities of the investigated ILs display a good <sup>25</sup>agreement with the corresponding experimental viscosity.

- It is quite surprising that glyceryl substituted phosphonium salts **1** are generally characterized by a lower viscosity and higher conductivity than the corresponding styryl substituted salts **2**, despite the presence of two hydroxyl groups.
- <sup>30</sup>As expected, the anion chemical structure exerts a significant effect also on conductivity and the less viscous ILs, with  $[Tf_2N]$ <sup>-</sup> as anion, show the highest conductivities. Conductivity increases on increasing temperature but, in agreement with viscosity, the temperature dependence follows only "approximately" the <sup>35</sup>Arrhenius equation 3:

$$
ln\sigma = ln\sigma_{\infty} - E_{\sigma} / RT \qquad (3)
$$

where  $E\sigma$  is the activation energy for conductivity.



Data have been therefore fitted using the more appropriate VTF equation 4, where A ( $\mu$ S cm<sup>-1</sup>), B (K) and T<sub>0</sub> (K) are fitting parameters.

$$
\sigma = A e^{-B/(T-T_0)}
$$
 (4)

The optimized parameters and related correlation coefficients are reported in Table 3, together with the Arrhenius parameters.

Table 3. Arrhenius and VFT conductivity parameters

				J 1			
Anion	$E\sigma$ KJ $mol-1$	lnσ∞ $(\mu s/cm)$	R	A $(\mu s/cm)$	B K	T <sub>0</sub> (K)	$R^2$
$[P_{888(gly)}]Cl$	34.2	13.5	0.997	1701	429	218	0.999
$[P_{888(gly)}][PF_6]$	42.8	17.0	0.998	3981	548	213	0.999
$[P_{888(gly)}][BF_4]$	35.6	15.8	0.998	101278	1544	123	0.999
$[P_{888(gly)}][Tf_2N]$	35.2	15.2	0.989	4033	360	221	0.999
$[P_{888(gly)}][NO_2]$	31.7	13.3	0.988	6138	678	182	0.998
$[P_{888(4-VB)}][PF_6]$	51.5	18.2	0.996	1016	352	243	0.995
$[P_{888(4-VB)}][BF_4]$	47.1	17.8	0.998	6098	680	206	0.999
$[P_{888(4-VB)}]$ [Tf <sub>2</sub> N]	38.2	15.8	0.989	2913	332	230	0.996
$[P_{888(4-VB)}]$ [NO <sub>2</sub> ]	34.1	15.9	0.999	1291	1018	169	0.999

Subsequently, we examined the solvent properties of these ILs determining the solvatochromic Kamlet-Taft parameters, π\* <sup>60</sup>(dipolarity/polarizability), β (hydrogen bonding basicity), α (hydrogen bonding acidity) and the Reichardt parameter  $E_{T(30)}$ . The solvatochromic parameters have been determined exclusively for phosphonium salts **1**, since the salts **2** have an exceedingly high absorption in the UV region of interest. Table 4 reports the <sup>65</sup>Kamlet-Taft parameters of the investigated ILs. Values related to

two unfunctionalized tetraalkylphosphonium salts have been added for comparison.

As expected, ILs **1** are generally characterized by a significantly higher hydrogen bonding acidity when compared with the 70 unfunctionalized tetraalkylphosphonium salts: as previously observed<sup>13</sup> for other classes of ILs, the introduction of two hydroxyl groups on cation gives ILs with  $\alpha$  values comparable to that of water (1.13), with the exception of chloride salts.

75

40



 $a^2$ Determined at 50 °C.  $b^b$ From ref. 14. °From ref. 5.

 Furthermore, also for these ILs the hydrogen bonding basicity  $5(6)$  depends mainly on the anion although an inverse relationship between  $\alpha$  and  $\beta$  parameters can be envisaged: basic anions (such as chloride) reduce the cation hydrogen bond donor ability ( $\alpha$ decreases from 0.97 to 0.54 going from  $[Tf_2N]$  to Cl, Table 4). The strong proton accepting nature of chloride anion, probably

<sup>10</sup>through the formation of hydrogen bonds with the hydroxyl groups of the glyceryl moiety,<sup>6</sup> increases the networking inside the IL and reduces the ability of IL cation to interact with the probe dyes.

 $[P_{888(gly)}]$ Cl and  $[P_{888(gly)}]$  [BF<sub>4</sub>] have been not employed for 15 metal extraction. Preliminary experiments showed indeed a cleancut decrease in the volume of the organic phase, attributable to a partial dissolution in water, when exactly measured amounts of these ILs were added to water and the phases were vigorously mixed and subsequently separated by centrifugation. Moreover,

20 we avoided the use of  $[P_{888(4-VB)}][PF_6]$  owing to its surfactant properties that drastically reduced the phase separation efficiency after mixing of organic and aqueous phase.

The selected ILs **1** and **2** have been therefore tested as metal ions extractants from water in biphasic separations. The extraction of

25 the individual metal ions Cu(II),  $\text{Zn(II)}$ , Co(II), Ni(II) and Pb(II) was performed by mixing 0.5 g of IL with 1.5 g of water containing a metal ion concentration of 100 ppm. Chloride salts were used as Cu(II), Zn(II), Co(II), Ni(II) and Pb(II) sources.

Table 5. Extraction efficiency for metal extraction (procedure 3) 30 using  $[P_{888(gly)}]$ <sup>+</sup> based ILs.





Figure 1. Effect of IL anion on extraction percentage (E%) of metals cations from aqueous solutions (procedure 1 and 3) using  $[P_{888(gly)}]$ <sup>+</sup> based ILs.

<sup>35</sup>To be sure that the equilibrium conditions were reached, the extraction efficiencies obtained after 10 min stirring were compared with the efficiencies obtained after stirring for 30 min. Since the values were practically identical, a stirring time of 10 min was selected for all experiments. It is noteworthy that the <sup>40</sup>reuse of the organic phase for extraction of fresh metal ion solutions gave only a no-significative increase in extraction efficiency: for these ILs the pre-conditioning phase appears not important.

For each metal, the extraction efficiency was therefore evaluated  $45$  after one or three consecutive extractions using fresh IL (3 x 0.5) gr), values are depicted in Figure 1. As expected an increase in E (extraction efficiency) was always observed on increased the number of extractions (Figure 1): in particular, three extractions assured a practically complete recover of Pb(II) and Cu(II)**.** 

<sup>50</sup>Unfortunately, despite the well-known chelation ability of two vicinal hydroxyl groups, the association of the dihydroxyl functionalized phosphonium cation  $[P_{888(gly)}]^{+}$  to hydrophobic anions (such as  $[PF_6]$ <sup>-</sup> or  $[Tf_2N]$ <sup>-</sup>) gave ILs having only a moderate metal extraction ability. The high extraction efficiency 55 towards Pb(II) and Cu(II), observed in  $[P_{888(gly)}][NO_2]$ , is most likely attributable to the anion properties, *i.e.* its coordinating ability or reducing power. The formation of metallic particles in the organic phase was indeed detected in the samples containing Pb(II). The subsequent, ICP-MS analysis of the recovered  $\omega$  precipitate after dissolution in HNO<sub>3</sub> (65%) confirmed the formation of Pb(0) in nitrite based ILs.

Since the hydroxyl groups on cation appeared unable to affect significantly extraction efficiency we have decided to test four trioctyl(4-vinylbenzyl)phosphonium salts having as counteranion 65  $[Tf_2N]$ ,  $[NO_2]$  and Cl. It is noteworthy that the highly hydrophobic nature of this aryl substituted phosphonium cation makes it possible the association with the coordinating chloride anion: the corresponding IL is indeed water insoluble.

50

 Table 6. Extraction efficiency for metal extraction (procedure 3) using  $[P_{888(4-VB)}]$ <sup>+</sup> based ILs.

	$[P_{888(4-VB)}]Cla$		$[P_{888(4-VB)}]Cl$ $[P_{888(4-VB)}] [Tf_2N]$ $[P_{888(4-VB)}] [NO_2]$	
$M^{2+}$				
	E%	E%	E%	E%
$Pb^{2+}$	92.1	99.9	28.9	99.9
$Cu2+$	25.1	99.4	36.3	99.7
$Zn^{2+}$	84.2	99.9	75.6	97.8
$Co2+$	-	-	۰	39.3
$Ni2+$	$\overline{\phantom{0}}$	-	٠	36.5

a Procedure 1.



Figure 2. Effect of IL anion on extraction percentage (E%) of metals cations from aqueous solutions using  $[P_{888(4-VB)}]$ <sup>+</sup> based ILs.

- <sup>15</sup>Extraction efficiency values (Table 6 and Figure 2) show that  $[P_{888(4-VB)}][Tf_2N]$ , analogously to the corresponding IL of the other series, has no affinity for Co(II) and Ni(II). However, it shows a fairly good extraction ability towards  $Zn(II)$  (E% = 76). On the other hand,  $[P_{888(4-VB)}][NO_2]$  presents an excellent
- $20$  extraction ability for Pb(II), Cu(II) and Zn(II). These metal cations can be however efficiently extracted also by  $[P_{888(4-VB)}]Cl$ , which is able to remove 92% of Pb(II) and 84% Zn(II) after a single extraction.
- The coordination ability of the IL anion appears therefore <sup>25</sup>fundamental in metal extraction from water. The hydrophobic  $[P_{888(4-VB)}]$ Cl is indeed able to perform an efficient transfer of metal ions from water to organic phase. The formation of polychlorometallate anions, as key species able to positively affect the transfer process, could be hypothesized considering 30 their stability in ILs. Halometallate ILs have been widely applied
- as Lewis acids and solvents in synthesis or in electrochemistry, 15- <sup>16</sup> and their involvement for the cobalt/nickel separation from 8 M HCl solutions has been recently reported. $<sup>7</sup>$ </sup>

However, considering the different working conditions (in our 35 experiments the pH of the aqueous medium was in the range 4.5-

- 5) to verify their actual formation, UV-vis measurements have been carried out on the organic phase in the case of Cu(II). Extraction of a blue colored (*ca.* 0.1 M) aqueous solution of  $CuCl<sub>2</sub>$  (the blue color is indicative for the fully hydrated  $Cu(II)$ )
- 40 ion) with  $[P_{888(4-VB)}]$ Cl gave a yellow organic phase attributable to the formation of  $[CuCl<sub>4</sub>]<sup>2–</sup>$  ion. This species was identified by UV-vis spectroscopy, on the basis of its typical absorption around 408 nm the other two maxima (at 291 nm and 231 nm, respectively) being completely covered by the strong absorption  $45$  of the IL below 300 nm. $^{17}$

Therefore, taking into account the coordination number of the different anions, we propose the following pathway (eq 5) for extraction of Cu(II) and Zn(II),

$$
\underbrace{2[P_{888(4\text{VB})}]Cl}_{IL\text{-phase}} + M^{2+} + 2Cl \qquad \Longleftrightarrow \qquad \underbrace{[P_{888(4\text{VB})}]_2[MCl_4]}_{IL\text{-phase}} \quad (5)
$$

based on the formation of anionic tetrahedral metal chloride complexes, which become the "new" IL counteranions. A similar pathway can be hypothesized also for  $Pb(II)$ ,<sup>18</sup> even if the very <sup>55</sup>low concentration of the metal salt could favour the formation of an octahedral complex  $[PbCl_6]^4$  arising from an analogous process:

$$
\underbrace{4 [P_{888(4-VB)}]Cl}_{IL\text{-phase}} + Pb^{2+} + 2Cl^-\n \underbrace{[P_{888(4-VB)}]_4 [PbCl_6]}_{IL\text{-phase}}\n (6)
$$

- <sup>60</sup>Although the ionic nature of ILs can allow a variety of mechanisms, including solvent ion-pair extraction (eq 5 and 6), ion exchange (metal-IL cation) and simultaneous combination of them,<sup>19</sup> the inability to detect the IL cation ( $[P_{888(4-VB)}]$ <sup>+</sup>) in water phase after extraction of concentrated metal solutions (0.1M) by
- <sup>65</sup>NMR suggests a moderate (if any) involvement of the metal-IL cation exchange mechanism, with a very low IL leaching. It is noteworthy that only very small quantities of other tetralkylsubstituted phosphonium based ILs have been measured by Binnemans et al. in the aqueous phase after solvent extraction.<sup>7</sup> 70

Probably, an analogous mechanism can be hypothesized also for bis(trifluoromethane)sulfonylamide based ILs, although the chelating ability of this anion should give complexes of different speciation and geometry.

<sup>75</sup>Finally, it is to mention the chelating and reducing properties of nitrite anion which favour also in the case of the styryl functionalized cation,  $[P_{888(4-VB)}]^+$ , extraction and deposition of reducible metals, such as Pb(II).

#### **Conclusions**

- <sup>80</sup>In this paper we report the successful use of phosphonium based ILs for the extraction of some common metal cations from water using two series of functionalized phosphonium based ILs. IL anion strongly affects the efficiency of the extraction process which is however affected also by cation functionalization.
- 85 Differences in extraction are observed between the ILs possessing diol-substituted (hydrogen bond donor) and styryl-substituted (non- hydrogen bond donor) cations. In this context,  $[P_{888(4-VB)}]Cl$ allows a nearly complete extraction of Pb(II), Cu(II), Zn(II), while the extraction of Co(II) and Ni(II) was negligible.
- <sup>90</sup>Reduction and possible chelation of metal ion species by nitrite-based ILs distinguish these solvents from the other investigated ILs. On the other hand, the chelation ability of chloride anion appears to be the driving force in the extraction of metal ion species able to give stable polychlorometallate anions.
- <sup>95</sup>Pb(II), Cu(II), Zn(II) can be extracted avoiding the addition of HCl (8 M) to the aqueous phase.

#### **Acknowledgements**

This research was partially supported by the Fondazione Cassa di Risparmio di Pisa (grant: POLOPTEL). The authors wish to thank Mr Franco Castellani (ARPAT, PISA) for his technical <sup>5</sup>assistance in ICP-MS analysis.

#### **Notes and references**

*Dipartimento di Farmacia, via Bonanno 33, 56126 Pisa, Italy. Fax: 39 050 2216990; Tel: 39 050 2216996; E-mail: cinziac@farm.unipi.it* 

- <sup>1</sup> T. Ramnial, D. D. Ino, J. A. Clyburne *Chem. Commun.* 2005, 325.
- <sup>2</sup> C. J. Bradaric, A. Downard, C. Kennedy, A. J. Robertson, Y. Zhou *Green Chem.* 2003, **5**, 143. K. Tsunashima, M. Sugiya *Electrochem. Commun.* 2007, **9**, 2353.
- 3 G. Adamová, R. L. Gardas, L. P. N. Rebelo, A. J. Robertson, K. R. Seddon *Dalton Trans.* 2011, **40**, 12750. G. Adamová, R. L. Gardas,M. Nieuwenhuyzen, A. V. Puga, L. P. N. Rebelo, A. J. Robertson, K. S. Seddon *Dalton Trans.* 2012, **41**, 8316.
- 4 K. Tsunashima, E. Niwa, S. Kodama, M. Sugiya, Y. Ohno *J. Phys. Chem. B* 2009, **113**, 15870.
- 5 Y. Fukaya, H. Ohno *Phys.Chem.Chem.Phys.* 2013, **15**, 4066.
- 6 F. Bellina, C. Chiappe, M. Lessi *Green Chem.* 2012, **14**, 148.
- 7 S. Wellens, B. Thijs, K. Binnemans *Green Chem*. 2012, **14**, 1657.
- 8 A. G. Chmielewski, T. S. Urbanski, W. Migdal *Hydrometallurgy* 1997, **45**(3), 333. N. B. Devi, K. C. Nathsarma. G. Chakravortty *Hydrometallurgy* 1998, **49** (1-2), 47.
- 9 J. G. Huddleston, H. D. Willauer, R. P. Swatloski, A. E. Visser, R. D. Rogers, *Chem. Comm.* 1998, 1765.
- <sup>10</sup> M. L. Dietz, J. A. Dzielawa *Chem. Commun*. 2001, 2124. M. P. Jensen, J. A Dzielawa, P. Rickert, M. L. Dietz *J. Am. Chem. Soc. 2002*, **124**, 10664.
- <sup>11</sup> A. Cieszynska, M. Wisniewski *Sep. Purif. Technol.* 2010, **73**, 202. F. D. M. Fabrega, M. B. Mansur *Hydrometallurgy* 2007, **87**, 83.
- <sup>12</sup> S. Cheng, M. Zhang, T. Wu, S. T. Hemp, B. D. Mather, R. B. Moore, T. E. Long *J. Polymer. Chem.* 2012, **50**, 166.
- <sup>13</sup> C. Chiappe, S. Ramajani, C. S. Pomelli *J. Phys. Chem. B* 2011, **115**, 9653.
- <sup>14</sup> M. A. Ab Rani, A. Brant, L. Crowhurst, A. Dolan, M. Lui, N. H. Hassan, J. P. Hallett, P. A. Hunt, H. Niedermeyer, J. M. Perez-Arlandis, M. Schrems, T. Welton, R. Wilding *Phys.Chem.Chem.Phys.* 2011, **13**, 16831.
- <sup>15</sup> T. Welton, *Coord. Chem. Rev.* 2004, **248**, 2459.
- <sup>16</sup> J. Estager, J. D. Holbrey, M. Swadzba-Kwasny, *Chem. Soc. Rev.* 2014, **43**, 847.
- <sup>17</sup> P. De Vreese, N. R. Brooks, K. Van Hecke, L. Van Meervelt, E. Matthijs, K. Binnemans, R. Van Deun Inorg. Chem. 2012, 51, 4972.
- <sup>18</sup> F. Coleman, G. Feng, R. W. Murphy, P. Nockemann,
- K. R. Seddon, M. Swadzba-Kwasny *Dalton Trans*., 2013, **42**, 5025.
- <sup>19</sup> E. A. Mowafy, H. F. Aly *J. Hazard. Mater.* 2007, **149**, 465.