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# Hyperbranched polyethers with tunable glass transition temperature: controlled synthesis and mixing rules

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Received (in XXX, XXX) XthXXXXXXX 20XX, Accepted Xth XXXXXXXX 20XX 5 DOI: 10.1039/b000000x

By taking advantage of competing side reactions, controlled synthesis of a series of homo- and copolymerized hyperbranched polyethers (HBPEs) is demonstrated using a series of AB<sub>2</sub> monomers of different spacer lengths. This reacting system shows good controllability and scalability. More importantly, the degree of branching is found to be insensitive to molecular weight and the spacer length

<sup>10</sup> in monomers. Thus, the value and width of  $T_g$  can be tuned by varying monomer spacer length, terminal groups, molecular weight, as well as by copolymerization and physical blending. The dependence of  $T_g$  in binary homopolymers blends on composition and the dependence of  $T_g$  in copolymers on monomer ratio are established and compared for the first time.  $T_g$  of copolymers obeys Fox equation, whereas  $T_g$  in binary blends only follows Kwei equation. Copolymerization does not increase the width of  $T_g$ . In

<sup>15</sup> contrast, the width of  $T_g$  in binary blends is much broader than that of copolymers, even though the broadening in  $T_g$  can be reduce by increasing the polarity of terminal groups.

#### Introduction

Hyperbranched polymers (HBPs) have been a hot research area<sup>1</sup> <sup>20</sup> for two decades due to their unique structures, such as highly branched structure, compacted shape, ample and modifiable terminal groups. The special structure imparts unique properties and leads to wide applications in various fields.<sup>2</sup> Properties of HBPs depend on many factors, including backbone structure,

- <sup>25</sup> terminal group, molecular weight (MW), and degree of branching (DB).<sup>3</sup> However, the random growth nature in one-pot synthesis often lead to poor controllability, which is a big issue not only for industrial applications but also for in-depth scientific studies.<sup>4</sup> Progress has been made to target that issue; however, most efforts
- <sup>30</sup> have been focused on controlling molecular weight distribution (or polydispersity, PDI) and degree of branching (DB).<sup>8</sup> On one hand, addition of polyfunctional core and slow monomer addition are found to be effective in lowering PDI to as low as 1.3.<sup>5</sup> For certain reacting systems in which the reactivity of formed
- <sup>35</sup> oligomers is much higher than that of monomers, PDI can be further lowered to 1.13.<sup>6</sup> On the other hand, progress has also been made in controlling DB. High DB values (>90%) have been achieved using Suzuki-Miyaura coupling reaction<sup>7</sup> and click chemistry<sup>8</sup>. Recently, HBP with tunable DB (from 0 to 100%) has
- <sup>40</sup> been achieved by adjusting catalyst dosage.<sup>9</sup> Min and Cao<sup>10</sup> also showed that the micro-emulsion polymerization technique is beneficial in obtaining HPBs with high DB and low PDI.

The glass transition temperature  $(T_g)$  is the most important parameter for polymers and is closely related to mechanical, <sup>45</sup> thermal, and other properties.<sup>11</sup> However, due in large part to the poor controllability, controlled synthesis of HBPs with tunable  $T_g$ has not been reported, especially for HBPs with polar terminal groups.  $T_{\rm g}$  of linear polymers depends on the chemical structure of backbone and MW.<sup>12</sup>  $T_{\rm g}$  of HBPs, however, depends on more <sup>50</sup> factors<sup>4</sup>, including backbone structure, terminal groups, DB, and MW and thus is more difficult to control. In HBPs, changes in

MW are often accompanied by changes in DB, which is also an important factor in determining  $T_{g}$ , making the control of  $T_{g}$  more challenging. In one-pot synthesis of HBPs, the control of MW 55 without changing DB is notoriously difficult. In addition, reproducibility and scalability are also difficult to achieve when the reactor size changes. This paper is organized into three parts. First, one-pot controlled synthesis of a series of hyperbranched polyethers (HBPEs) with almost invariant DB, controllable MW, 60 and good scalability is presented using a series of AB2 monomers with different spacer lengths. Second, the tuning of  $T_g$  was demonstrated using several ways, including varying monomer spacer length, terminal group, and MW, as well as physical blending and copolymerization. Third, the relationship between 65 the  $T_g$  of copolymers and monomer ratio and that between  $T_g$  of binary homopolymer blends and composition are compared in detail for the first time. Effects of terminal group on miscibility of binary blends were also discussed.

# **Experimental section**

## 70 Materials

All chemicals were analytical pure and used as received unless otherwise stated. Phenol and p-toluenesulfonic acid (PTSA) were purchased from Tianjin Fuguang reagent Co., China. 1,2dibromoethane (98%), 1,4-dibromobutane (98%), and 1,6-75 dibromohexane (98%) were purchased from Beijing Ouhe Technology Co., China. 2-Phenoxyethylbromide (98%), 4hydroxylbenzaldehyde (PHBA, 98%), and benzyl bromide (98%) were obtained from Zhongsheng Huateng Reagent Co., China. 4bromo-1-butene (98%) was obtained from Energy Chemical Co.,

<sup>5</sup> China. All other solvents and reagents were purchased from Beijing reagent Co., China. N,N-dimethyl formamide (DMF) were dried before use.

# Characterization

Nuclear magnetic resonance (NMR) spectra were collected on a <sup>10</sup> Bruker AV-600 spectrometer (600 MHz), and chemical shifts are reported in ppm. Fourier transform infrared spectroscopy (FTIR) spectra were collected on a Bruker Tensor 37 spectrophotometer

- using the potassium bromide (KBr) disc technique. Molecular weights of the hyperbranched molecules were determined using a <sup>15</sup> Waters 515-2410 gel permeation chromatography (GPC) system
- waters 515-2410 gel permeation chromatography (GPC) system which was calibrated using linear polystyrene calibration standards and with tetrahydrofuran (THF) as the eluent.  $T_g$  values of HBPEs were determined on second heating runs (typically 10 K/min) under a dry nitrogen atmosphere (40 ml/min) using a
- <sup>20</sup> DSC-1 (Mettler-Toledo, Switzerland) differential scanning calorimeter, which is equipped with an intra-cooler. All measurements were performed at 25±3 °C.

#### Synthesis of AB<sub>2</sub> monomers

All three monomers were synthesized in a two-step procedure

- $_{25}$  (Scheme 1). As an example, the procedure for synthesizing 2C-AB<sub>2</sub> (n=2) is given below. 4C-AB<sub>2</sub> (n=4) and 6C-AB<sub>2</sub> (n=6) were synthesized using similar procedures but with different reactants, and the characterization results are supplied in the supporting information (SI).
- <sup>30</sup> The first step is the synthesis of 4-(2-bromine-oxethyl)benzaldehyde. Under mechanical stirring, PHBA (12.2 g, 0.1 mol), 1, 2-dibromoethane (75.2 g, 0.4 mol),  $K_2CO_3$  (27.6 g, 0.2 mol), and 500 mL ethanol were added into a three-necked flask and refluxed for 10 h. After cooling to room temperature, the
- <sup>35</sup> mixture was filtered, and ethanol was removed using a rotary evaporator. The crude product was purified using silica gel column chromatography (GPC) with CH<sub>2</sub>Cl<sub>2</sub>/petroleum ether (1:1) as the eluent. The obtained product is a light green crystallike solid. Yield: 19.01 g, 83%. Please note that the crude product
- <sup>40</sup> can be directly used in the next step without purifying, because byproducts can be automatically removed the next step. <sup>1</sup>H-NMR (600 MHz, CDCl<sub>3</sub>,  $\delta$ ): 3.65 (t, 2H, OCH<sub>2</sub>CH<sub>2</sub>Br), 4.35 (t, 2H, OCH<sub>2</sub>CH<sub>2</sub>Br), 6.99 (d, 2H, C<sub>6</sub>H<sub>4</sub>O), 7.81 (d, 2H, C<sub>6</sub>H<sub>4</sub>O), 9.87 (s, 1H, PhCHO). <sup>13</sup>C-NMR (600 MHz, CDCl<sub>3</sub>,  $\delta$ ): 28.56, 67.95, 114.90, 120.45 (122.04) 120.70

45 114.89, 130.45, 132.01, 163.00, 190.70.

In the second step, 4-(2-bromine-oxethyl)-benzaldehyde (11.5 g, 0.05 mol), phenol (0.25 mol, 23.5 g), ZnCl<sub>2</sub> (0.7 g, 5 mmol), and PTSA (0.95 g, 5mmol) were added into a three-necked flask under mechanical stirring. After stirring for 1 h, reactants were

- <sup>50</sup> heated to 45 °C for 24 h and then washed at least twice with hot water (>70 °C) to remove residual salts. After evaporation at 140 °C, most phenol was removed, and the crude product was then purified by silica column chromatography with 1:5 ethyl acetate/petroleum ether as the eluent, and the obtained 2C-AB<sub>2</sub> is
- <sup>55</sup> a yellow solid. Yield: 8.78 g, 44%. <sup>1</sup>H-NMR (600 MHz, acetone-d6, δ): 3.76 (t, 2H, OCH<sub>2</sub>CH<sub>2</sub>Br), 4.33 (t, 2H, OCH<sub>2</sub>CH<sub>2</sub>Br), 5.38 (s, 1H, CHPh<sub>3</sub>), 6.76 (d, 4H, C<sub>6</sub>H<sub>4</sub>O), 6.89 (d, 2H, C<sub>6</sub>H<sub>4</sub>O), 6.94

(d, 4H, C<sub>6</sub>H<sub>4</sub>O), 7.06 (d, 2H, C<sub>6</sub>H<sub>4</sub>O), 8.15 (s, 2H, PhOH). <sup>13</sup>C-NMR (600 MHz, acetone-d6, δ): 30.29, 54.30, 67.99, 114.29, 60 114.87, 130.05, 130.17, 135.64, 138.03, 155.64, 156.65.

## Typical polymerization procedure

Procedures for homo- and co-polymerizing different monomers are the same (Scheme 2), when describing the detailed procedure,  $2C-AB_2$  is used as an example.  $2C-AB_2$  (0.8 g, 2 mmol),  $K_2CO_3$ 

- 65 (0.55 g, 4 mmol), and 20 mL DMF were added into a two-necked flask. Under magnetic stirring, reactants were heated to 80 °C for 24 h under a dry nitrogen atmosphere. After cooling to room temperature, the mixture was acidified with hydrochloric acid and filtered. The filtrate was precipitated into water to remove DMF
- <sup>70</sup> and residual salts. The crude product was dissolved in THF and added drop wise into 2:1 ethanol/water solution under strong agitation. The precipitate was collected, washed with ethanol, and dried under vacuum at 90 °C to give a brick red solid product. Yield: 0.49 g, 77%.

# 75 Typical procedure for terminal group modification

The procedure for terminal group modification is shown in Scheme 4. 1 g HBPE-2C or HBPE-6C, 5.2 g benzyl bromide, and 1.8 g K<sub>2</sub>CO<sub>3</sub> were added into 20 mL DMF. Under magnetic stirring, reactants were heated to 80 °C for 24 h under dry <sup>80</sup> nitrogen atmosphere. After cooling to room temperature, the mixture was filtered and precipitated into petroleum ether twice. After the precipitate was dried under vacuum at 90 °C, the obtained benzyl-terminated HBPE-2C (BHBPE-2C) is a light red solid. Yield: 0.90 g, 70%. <sup>1</sup>H-NMR (600 MHz, CDCl<sub>3</sub>, δ): 4.22-<sup>85</sup> 4.30 (br, O-CH<sub>2</sub>CH<sub>2</sub>-O), 5.00-5.05 (br, Ph<sub>3</sub>CH<sub>2</sub>-O), 5.36-5.42 (br, Ph<sub>3</sub>CH), 6.80-7.44 (br, C<sub>6</sub>H<sub>4</sub>O).

# Physical blending

Binary blends were prepared by dissolving two homopolymers in THF according to different designed weight ratios. After <sup>90</sup> transparent solution was obtained, THF was removed completely in a vacuum oven at 90 °C.

# **Results and discussion**

# Synthesis of AB<sub>2</sub> monomers and HBPEs

The synthesis route for three AB<sub>2</sub> monomers of different spacer <sup>95</sup> lengths (*i.e.*, n=2, 4, and 6) is shown in Scheme 1. In the second step, although both ortho- and para-substituted products are obtained.<sup>13</sup> The para-substituted products are the main products and will be used as monomers in later polymerization processes.

Using the three AB<sub>2</sub> monomers, which have different space 100 length, a variety of homo- and co-polymerized HBPEs were prepared using one-pot polymerization. The synthesis route for homopolymerized HBPEs is shown in Scheme 2. Homopolymerized HBPEs synthesized from monomers of different spacer lengths, (*i.e.*, n=2, 4, and 6 in Scheme 1) are 105 labelled as HBPE-2C, HBPE-4C, and HBPE-6C, respectively; suffixes "-1, -2, and -3" after "HBPE-nC" denotes different MWs. Polymerization reactions were carried out under nitrogen protection using water-free solvents. Two types of terminal groups were found in HBPEs: the double bond and the bromine

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 $R = + CH_2 + n, n = 2, 4, 6$ 

Scheme 1 The synthesis route of AB<sub>2</sub> monomer and its byproduct.



Scheme 2 Typical synthesis route for synthesizing homopolymerized HBPEs.

Code <sup><i>a</i></sup>	Concentration	M <sub>n</sub>	$M_{ m w}$	PDI	$T_{\rm g}$	$\mathrm{DB}^b$
	(mol/L)	(kDa)	(kDa)		(°C)	
HBPE-2C-1	0.10	3.8	6.8	1.8	127	0.53
HBPE-2C-2	0.20	6.0	12.6	2.1	129	0.51
HBPE-2C-3	0.40	7.3	18.3	2.5	131	0.50
HBPE-4C-1	0.10	3.5	6.0	1.7	101	0.51
HBPE-4C-2	0.20	4.1	7.8	1.9	109	0.51
HBPE-6C-1	0.10	4.2	8.4	2.0	93	0.53
HBPE-6C-2	0.20	8.9	22.3	2.5	97	0.53
HBPE-6C-3	0.40	10.0	27.0	2.7	99	0.50

Table1 Characterization results of phenol-terminated HBPEs obtained at 80 °C.

<sup>*a*</sup> The first number in the code represents the number of carbon atoms in alkyl spacer, i.e., n in each structural unit. The second number in the code distinguish HBPEs of different MWs.

<sup>b</sup> Degree of branching is calculated according to Hawker's definition using <sup>1</sup>H NMR.

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group. As shown in the <sup>1</sup>H NMR results (Fig. 1), Ph<sub>3</sub>CH protons at ~5.3 ppm split into three peaks. For HBPE-2C, three peaks are well separated. As the spacer length increases, three peaks are closer to each other. Chemical shifts of Ph<sub>3</sub>CH proton are <sup>15</sup> affected differently by the dendritic (D), linear (L), and terminal

(T) units and thus spilt into different peaks, which can be used to determine  $DB^{14}$ .

#### **MW control in HBPEs**

Effects of reaction condition, including temperature, monomer <sup>20</sup> concentration, and reaction time, on MW were studied. Characterization results of homopolymerized HBPEs, which were all obtained at 80 °C, are summarized in Table 1. The MW was determined using GPC which was calibrated using linear polystyrene standards in the corresponding MW range. We note <sup>25</sup> that the MW of HBP obtained from GPC may be smaller than actual values. However, studies also show that for the MW of HBP is close to its actual value when MW is not very high (ca. 10000 g/mol).<sup>13</sup> HPBs show notable deviations only when the MW is high and the backbone structure is stiff. In our HBPEs, the <sup>5</sup> MW is not very high, and the backbone structure is not that stiff. Thus, no notable deviations from actual values are expected.

For easy comparison, normalized GPC curves corresponding to different reaction times (from 4 h to 72 h) are shown in Fig. 2.

At 60, 80, and 100 °C, GPC results corresponding to 4 h and 6 h <sup>10</sup> almost overlap, indicating that MW and its distribution stabilize in 6 h. When temperature increases from 40 to 100 °C, numberaverage molecular weight ( $M_n$ ) of HBPE-2C goes through a maximum at 80 °C (Fig. 3). The fast stabilization and temperature-dependence in  $M_n$  are somewhat unexpected, and <sup>15</sup> explanations are offered in the following paragraph.



**Fig. 1** <sup>1</sup>H NMR spectra of HBPEs obtained from monomers with different spacer length (*i.e.*, n = 2, 4, and 6).

- <sup>20</sup> Two assumptions were made in Flory's classic treatment of AB<sub>2</sub> polymerization<sup>15</sup>: the reactivity between A and B groups remain unchanged during polymerization; side reactions, such as intermolecular cyclization, are absent. Based on those assumptions, MW only stabilizes after long times when steric
- <sup>25</sup> hindrance become dominate, making MW sensitive to local reaction conditions, such as mixing and heat transfer. We realize that violation of any of the two assumptions can lead to some degree of controllability. Similar fast stabilization has been ascribed to intermolecular cyclization.<sup>16</sup> However, cyclization
- <sup>30</sup> cannot occur in our system due to the short spacer length in monomers, which has been confirmed by NMR. Rather, the elimination reaction<sup>17</sup>, which competes with the main substitution (or propagation) reaction, is responsible. Comparing the corresponding peak areas in <sup>1</sup>H NMR spectra of HBPE-4C-2 (Fig.
- <sup>35</sup> 4) to that of a model molecule, 4-bromo-1-butene (see Fig. S9 in SI) reveals that more than 70% Br group was converted to C=C after reacting at 80 °C for 24 h, which essentially terminates the substitution reaction and leads to a fast stabilization in MW. Thus, the relative speed of the elimination to substitution
- <sup>40</sup> reactions changes with temperature and lead to temperaturedependent MW. We note that fast stabilization is not achieved at 60 °C (Fig. 2A). This can be explained by the low reaction speeds of both elimination and substitution reactions at 60 °C, which lead to incomplete termination even after 4 h reaction. Thus, MW
- <sup>45</sup> continues to increase with time. In contrast, at the highest temperature of 100 °C, the elimination reaction is favored and leads to a decrease in MW (Fig. 3).



**Fig. 2** Normalized GPC results of HBPE-2C as a function of <sup>50</sup> reaction time for polymerization carried out at (A) 60 °C, (B) 80 °C, and (C) 100 °C.



**Fig. 3** The variation of number-average molecular weight  $(M_n)$  of HBPE-2C with reaction temperature when polymerized for 24 h <sup>55</sup> and at a monomer concentration of 0.1 mol/L.



**Fig. 4** The <sup>1</sup>H NMR spectrum of HBPE-4C-1 (80 °C, 24 h). Insets show the enlarged views of boxed parts.

<sup>60</sup> In the synthesis of HBPs, side reactions can lower MW and are thus often undesirable. In the absence of side reactions, MW and DB are mainly determined by reaction kinetics, making them sensitive to changes in local variations in temperature, mixing, concentrations of reactants and catalysts. As aforementioned, violation of two assumptions (*i.e.*, constant reactivity or/and absence of side reactions) can lead to better controllability. <sup>5</sup> Yokozawa<sup>7</sup> showed that, for reacting systems with increasing reactivity, HBPs with narrow polydispersity (PDI) can be obtained. In our systems which violate the second assumption, good controllability and reproducibility can also be achieved. As

aforementioned, at the right temperature range, the competing <sup>10</sup> side reaction can lead to fast stabilization and allows us to control MW simply by controlling temperature and monomer concentration.



**Fig. 5** (A) <sup>1</sup>H NMR spectra of three model molecules with well-<sup>15</sup> defined D, L, and T units. Isolated peaks of HBPE-2C-1 at corresponding locations are also shown. (B) The typical curvefitting result for HBPE-4C-2 showing the deconvolution of each type of structural unit.



<sup>20</sup> Scheme 3 The synthesis route of three model molecules which have well-defined <sup>1</sup>H NMR peaks of dendritic (D), linear (L), and terminal (T) units, respectively.

#### Insensitivity of DB to MW and monomer spacer length

<sup>25</sup> It is well know that DB in HBPs plays crucial roles in determining physical properties, such as  $T_g$  and viscosity.<sup>6</sup> One of the most used definitions of DB is that proposed by Hawker and Fréchet<sup>14</sup>:

#### DB = (D+T)/(D+T+L)

- <sup>30</sup> where D, T, and L represent numbers of dendritic, terminal, and linear units, respectively. In order to assign corresponding chemical shifts to the dendritic, terminal, and linear units, three model compounds that have well defined NMR peaks for D, L, and T units are synthesized (see Scheme 3 and Fig. 5A). For
- <sup>35</sup> HBPE-2C, three peaks corresponding to Ph<sub>3</sub>H protons are well defined and isolated (Fig. 1). However, for HBPE-4C and HBPE-

6C, the three peaks are not well separated and but can be deconvoluted by assuming a Gaussian distribution.<sup>18</sup> A typical convolution result of HBPE-4C-2 is given in Fig. 5B. DB values <sup>40</sup> of other HBPEs (prepared at 80 °C) are summarized in Table 1. It is clear that although HBPEs samples are prepared from different monomers and monomer concentrations, they all have a DB of ~0.51. The insensitivity of DB to monomer type could be explained by the fact that the reactivity between A and B group is <sup>45</sup> insensitive to spacer length. This important finding implies that DB of copolymerized HBPEs is similar to that of homopolymers.

#### Tg-Tuning in HBPEs

 $T_{\rm g}$  of HBPs depend on many factors, including MW, DB, and structures of backbone and terminal group.<sup>19</sup> One complication in <sup>50</sup> HBPs is that changes in MW are often accompanied by changes in DB, which also has notable effects on  $T_{\rm g}$ . Thus, the control and tuning of  $T_{\rm g}$  in HBPs is often challenging. For our HBPE systems, the fast stabilization in MW and the insensitivity of DB make them a good model system for making HPBEs with tunable <sup>55</sup>  $T_{\rm g}$ , which is also very useful for other scientific investigations. Several ways of preparing  $T_{\rm g}$  tunable HBPEs are demonstrated below. The reported  $T_{\rm g}$  values were obtained from second heating runs in DSC at 10 K/min unless otherwise stated.

(1)  $T_{g}$ -tuning by varying MW, monomer spacer length, and 60 terminal group. At 0.1 mol/L and 80 °C, the one-pot approach yields a  $M_{n}$  of ~4000 g/mol in the case of HBPE-2C-1. By increasing monomer concentration,  $M_{n}$  can be further increased to ~7000 g/mol. Alternatively, by adding additional batches of monomers into the already stabilized systems, the propagation 65 reaction can be reinitiated and yield HBPEs with a  $M_{n}$  of more than 10000 g/mol. However, increasing  $M_{n}$  from 4000 to 10000 g/mol only increase  $T_{g}$  by 10 °C, suggesting changing  $T_{g}$  by varying MW is not very effective for our system. Thus, in later studies concerning the binary blends and copolymerization, 70 effects of  $M_{n}$  on  $T_{g}$  are not shown.

 $T_{\rm g}$  of HBPEs can also be varied by changing backbone structure. As shown in Table 1, at comparable  $M_{\rm n}$ ,  $T_{\rm g}$  of HBPE-2C is approximately 30 °C higher than that of HBPE-6C. Terminal groups in HBPs also have notable effects on  $T_{\rm g}$ . After 75 converting the phenolic terminal groups in HBPE-2C-1 into benzyl groups (Scheme 4),  $T_{\rm g}$  decreases approximately 50 °C due to the weaker interactions between terminal groups. Thus, changing backbone structure and terminal group are more effective ways of tuning  $T_{\rm g}$ .





Scheme 4 The reaction route for terminal group modification.

(2)  $T_{\rm g}$ -tuning by varying copolymerization and binary blending. Copolymerization and physical blending have been <sup>85</sup> used to change  $T_{\rm g}$ s of linear polymer systems, and prediction of  $T_{\rm g}$  with composition in those systems ( $T_{\rm g}$  mixing laws) has been well documented. However, mixing laws for hyperbranched systems have not been systematically studied. Based on our HBPEs, the variation of  $T_g$  in binary homopolymerized blends with composition and variation of  $T_g$  in copolymers with monomer ratio are demonstrated. Furthermore, the difference in s two mixing laws is investigated in detail for the first time.

Random copolymerized HBPEs were obtained using two monomers (*i.e.*, n=2 and 6) at different monomer mole ratios, and the synthetic route is shown in Scheme 5.  $M_n$  of copolymerized HBPEs is in the range of 3800~4300 g/mol. Please note that DB

- <sup>10</sup> of copolymerized HBPEs (80 °C, 0.1 mol/L) cannot be accurately determined due to the stronger overlaps in <sup>1</sup>H NMR peaks. However, as explained before, DBs of copolymers are expected to be close to those of homopolymers. As shown in Fig. 6, both copolymers and binary blends of HBPE-2C and HBPE-6C show
- <sup>15</sup> only one  $T_g$ . In copolymers,  $T_g$  increases systematically when the molar fraction of 6C-AB<sub>2</sub> monomer (X) decreases; in binary blends,  $T_g$  also increases systematically with the weight fraction of HBPE-6C (w).



<sup>20</sup> Scheme 5 The route of copolymerized HBPEs using 2C-AB<sub>2</sub> and 6C-AB<sub>2</sub>. X denotes the mole fraction of 6C-AB<sub>2</sub>.



**Fig. 6** DSC traces of copolymers and binary blends. (A)  $T_{\rm g}$ s of copolymerized HBPEs (2C-AB<sub>2</sub> and 6C-AB<sub>2</sub>) as a function of <sup>25</sup> molar fraction of 6C monomer (*X*); (B)  $T_{\rm g}$ s of binary homopolymers of HBPE-2C and HBPE-6C as a function of the weight fraction of HBPE6C (*w*)

For miscible blends and copolymers without interactions, the variation of  $T_g$  with composition can be described by Couchman

<sup>30</sup> equation based on entropy continuity<sup>20</sup> or a simplified version of Couchman equation, *i.e.*, the Gordon-Taylor equation that can be derived from volume additivity.<sup>21</sup> Due to its simplicity, Gordon-Taylor equation is often used to predict the compositiondependent  $T_g$  of binary blends of linear polymers:

$$=\frac{w_{1}T_{g1}+kw_{2}T_{g2}}{w_{1}+kw_{2}}$$
(1)

<sup>35</sup> where  $T_{\rm g}$ ,  $T_{\rm g1}$  and  $T_{\rm g2}$ , are  $T_{\rm g}$  values of the binary blend (or copolymer), homopolymers 1 and 2, respectively;  $w_1$  and  $w_2$  are weight fractions of homopolymers 1 and 2; k is a fitting parameter. Further simplifications ( $\rho_1/\rho_2=1$ ;  $\Delta \alpha_1 T_{\rm g1} = \Delta \alpha_2 T_{\rm g2}$ ) lead to the Fox equation<sup>12, 22</sup>:

 $T_{g}$ 

$$\frac{1}{T_{\rm g}} = \frac{w_{\rm l}}{T_{\rm g1}} + \frac{w_{\rm 2}}{T_{\rm g2}} \tag{2}$$

<sup>40</sup> Theoretically, for systems with strong interactions such as our phenol-terminated HBPEs (BHBPEs), both Gordon-Taylor equation and Fox equation are not adequately; instead, Kwei<sup>23</sup> equation which takes into the strong interactions between different components has to be used:

$$T_{\rm g} = \frac{w_{\rm l} T_{\rm g1} + k w_{\rm 2} T_{\rm g2}}{w_{\rm 1} + k w_{\rm 2}} + q w_{\rm 1} w_{\rm 2} \tag{3}$$

<sup>45</sup> where *q* quantifies the degree of interactions, including effects of both steric hindrance and hydrogen bonding. Generally, hydrogen bonding leads a positive *q*, and the steric effects lead a negative *q*.



Fig. 7 (A) Variations of  $T_g$  in copolymers with weight fraction of  $_{50}$  6C-AB<sub>2</sub> monomer HBPEs; (B) variation of  $T_g$  in binary blends with weight fraction of HBPE-6C. Data are shown in symbols; predictions from Kwei and Fox equations are shown as dashed and solid curves, respectively.

<sup>55</sup> Variations of  $T_g$  in both copolymers and binary blends along with fittings from Kwei (dashed curve) and Fox Eq. (solid curve) are shown in Fig. 7. Notable differences between copolymers and blends are clearly shown:  $T_g$  values of copolymers follow Fox Eq., whereas  $T_g$  values in binary blends show negative deviations <sup>60</sup> from Fox Eq. In both cases, Kwei Eq. can fit data well, with k=1

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and q=0.6 for copolymers, and k=1 and q=-10.6 for binary blends. Interestingly, for  $T_g$  of copolymers, Fox Eq. which does not take into account of the effects of interactions can also fit data well. Satisfactory fitting using Fox Eq. has also reported for

- s hyperbranched copolymers with nonpolar terminal groups.  $^{24, 25}$  In our case, the unexpected good fit from Fox Eq. could be explained by two competing effects: on one hand, phenolic terminal groups can form hydrogen bonding and lead to an increase in q; on the other hand, ample terminal groups and the
- highly branched structure can also lead to steric hindrance and thus decrease q. The two competing factors result in a small q(0.6) and negligible  $qw_1w_2$  term in Kwei Eq., and thus lead to a satisfactory fitting with Fox Eq. In contrast, in binary blends, the steric hindrance effects dominate and lead to a large negative q (-
- <sup>15</sup> 10.6), thus Fox Eq. does not apply. The effects of heating rate on  $T_g$  is demonstrated by reducing the DSC heating rate from 10 K/min to 2 K/min. Results show that the T<sub>g</sub>s in blends and copolymers obtained at 2 K/min are all *ca.* 2.3 °C lower than those obtained at 10 K/min. However, the new sets of data can <sup>20</sup> still be fitted by Fox or Kwei Eqs.



**Fig. 8** (A)  $T_g$  of benzyl-terminated binary blends as a function of weight fraction of HBPE-6C, and predictions from Kwei equation (solid curve) and Fox equation (dashed curve). (B) DSC traces of <sup>25</sup> binary blends (*w*:*w*= 50:50) of benzyl-terminated BHBPE-2C-1 and phenol-terminated HBPE-2C-1.

In order to investigate the effects of terminal group on the glass transition phenomena in binary blends, HBPE-2C and 30 HBPE-6C, which have phenolic terminal groups, were converted to BHBPE-2C and BHBPE-6C, which have less-polar benzyl terminal groups. For binary blends of BHBPE-2C and BHBPE-6C, dependence of  $T_g$  on the weight fraction of BHBPE-6C along with fitting results from Kwei Eq. is shown in Fig. 8A. Again, in 35 the benzyl-terminated binary blends, only one  $T_g$  is observed for mixtures at all compositions. Kwei Eq. can fit data well with k=1 and q=-12.5. Compared with the phenol-terminated blend, the more negative q value in benzyl-terminated blends suggests that

steric hindrance is more pronounced in benzyl-terminated blends, 40 which is reasonable considering the lack of hydrogen bonding and the bigger size of benzyl groups. We note that only one  $T_{g}$  is observed in both the phenol-terminated blends and benzylterminated blends. In binary blends of linear polymers, stronger interactions, such as hydrogen bonding, are often necessary to 45 ensure misciblility.26 However, our results suggest that strong interactions are not necessary to ensure miscibility in binary blends of HBPEs. Thanks to the large numbers of contact sites in HBP blends, the same terminal groups (though not polar) in both components is enough to achieve adequate miscibility. This is 50 further confirmed by dual  $T_{\rm g}$  values found in binary blends of phenol-terminated HBPE-2C-1 and benzyl-terminated BHBPE-2C-1 (Fig. 8B). Please note that although two  $T_{gs}$  are observed, they do move closer to each other compared with  $T_{gs}$  of pure components.



**Fig. 9** The width of  $T_g (\Delta T_g)$  in copolymers (circles) as a function of the weight fraction of the 6C-AB<sub>2</sub> monomer,  $\Delta T_g$  in blends of HBPE-2C and HBPE-6C (squares) as a function of the weight fraction of HBPE-6C, and  $\Delta T_g$  in blends of BHBPE-2C-1 and 60 BHBPE-6C-1 (triangles) as a function of the weight fraction of BHBPE-6C-1.

Aside from the value of  $T_{\rm g}$ , the width of  $T_{\rm g}$  ( $\Delta T_{\rm g}$ ), which is reported as the difference between the extrapolated onset and 65 endset temperatures, can provide additional information on miscibility. Although only one  $T_g$  is observed in binary blends of both phenol-terminated and benzyl-terminated HBEPs,  $\Delta T_{g}$  does vary with composition (Fig. 9).  $\Delta T_{g}$  values of both phenolterminated blends of HBPE-2C-1 and HBPE-6C-1 (squares) and 70 benzyl-terminated blends of BHBPE-2C-1 and BHBPE-6C-1 (triangles) are bigger than that of copolymers (circles).  $\Delta T_{g}$ values of both blends go through maxima at intermediate compositions. However,  $\Delta T_g$  in benzyl-terminated blends is bigger than that in phenol-terminated blends, suggesting that 75 hydrogen bonding between polar terminal groups can enhance miscibility and lead to a narrower  $T_{g}$ . In contrast, for copolymers prepared from 2C-AB<sub>2</sub> and 6C-AB<sub>2</sub> monomers,  $\Delta T_g$  is always close to that of homopolymers despite the different monomer ratios. As a result,  $\Delta T_{\rm g}$  in copolymers is always smaller than 80 binary blends.

#### Conclusions

A series of homo- and co-polymers were synthesized via one-step polymerization using  $AB_2$  monomers of different spacer lengths. Thanks to the elimination side reaction, fast stabilization in  $M_n$ 

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can be achieved in 6 h with good controllability and scalability. More importantly, the degree of branching is found to be insensitive to molecular weight and monomer type, making it a good model system for producing HBPE with tunable  $T_g$  in large s scale.

 $T_{\rm g}$ -tuning in HBPEs was demonstrated using several methods, including terminal group modification, copolymerization, and physical blending. Moreover, the dependence of  $T_{\rm g}$  in binary blends on composition and the dependence of  $T_{\rm g}$  in copolymers

- <sup>10</sup> on monomer ratio are compared in detail for the first time. For copolymers, variation of  $T_g$  with monomer ratio can be fitted with both Kwei and Fox equations; and the width of  $T_g$  ( $\Delta T_g$ ) in copolymers is similar to that of homo-polymers. For both phenoland benzyl-terminated binary blends, the relationships between  $T_g$
- <sup>15</sup> and composition can be fitted with Kwei Eq.; however, they show negative deviations from Fox Eq. In addition, the *q* value in Kwei equation is found to depend on the nature of the terminal groups, including polarity and steric hindrance. For binary blends,  $\Delta T_g$ values are always bigger than those of homo-polymers. Unlike
- <sup>20</sup> linear polymer blends, hydrogen bonding is not necessary to ensure miscibility in blends of hyperbranched polymers as long as both components have the same terminal groups; however, hydrogen bonding can indeed improve miscibility and decreased the width of  $T_{\rm g}$ .

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#### Notes and references

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- <sup>35</sup> † Electronic Supplementary Information (ESI) available: Experimental details of synthetic procedures of model molecules, and NMR, GPC and DSC spectra which are not shown in the text. See DOI: 10.1039/b000000x/
- 40 ‡ Footnotes should appear here. These might include comments relevant to but not central to the matter under discussion, limited experimental and spectral data, and crystallographic data.
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