# Green Chemistry

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# ARTICLE TYPE

# LiCoO<sub>2</sub>: Recycling from spent batteries and regeneration with solid state synthesis

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A green recycling process was designed and used to recycle spent  $LiCoO_2$  batteries, and the recycled  $LiCoO_2$  was regenerated after the solid state synthesis with  $Li_2CO_3$ . XRD results showed that the layered structure of  $LiCoO_2$  was repaired after regeneration. The physical and chemical

<sup>10</sup> properties (XRD, morphology, tap density, average particle size, specific surface areas and pH value) and electrochemical properties (discharge capacity, attenuation rate of capacity, plateau retention at 3.6V and attenuation rate of plateau) of LiCoO<sub>2</sub> after regeneration were tested in detail and compared with commercial LiCoO<sub>2</sub>.The test datas show that the regenerated LiCoO<sub>2</sub> at 900 °C can meet the commercial requirements for reuse.

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#### Introduction

The lithium-ion batteries (LIBs) are widely used in mobile electronic devices, electric vehicles and other fields, due to their high voltage, high energy density, low self-discharge, long cycle

<sup>20</sup> life, no memory effect, etc.<sup>1-3</sup> But along with the extensive use of LIBs, it must be noted that an increasing number of spent LIBs are generated. In these spent LIBs, there are many valuable chemicals, but many of them are harmful if they are released into the environment.<sup>4-6</sup> So these spent LIBs must be disposed safely <sup>25</sup> and properly recycled to avoid polluting the environment.

Because of their high energy density, high operating voltage and good electrochemical properties,  $LiCoO_2$  batteries represent a very large proportion of the LIBs market. Therefore, the recycling process of  $LiCoO_2$  batteries is an important focus area

- <sup>30</sup> for spent LIBs recycling. Currently, the conventional recycling processes of LiCoO<sub>2</sub> batteries include extraction process, chemical precipitation process and electrolytic process, etc.<sup>7-21</sup> The specific steps in these recycling processes are not identical, but the acid leaching step is common to all of them. After acid
- <sup>35</sup> leaching, the cathode powders are dissolved with acid to form a solution containing Co<sup>2+</sup>, Li<sup>+</sup>, etc., and then the extraction process, chemical precipitation process or electrolysis process is used to recycle cobalt and lithium in the form of CoSO<sub>4</sub>, CoC<sub>2</sub>O<sub>4</sub>, Co(OH)<sub>2</sub>, Co, Li<sub>2</sub>CO<sub>3</sub>, etc. A large amount of acid solution or
- <sup>40</sup> organic solvent is used in these recycling processes, which will create additional waste streams that need to be disposed of or recycled without causing harm to the environment. In addition, these recycling processes are complicated, difficult to operate and costly. Therefore, developing a novel, simple, comprehensive,
- 45 environmental friendly and low-cost recycling process has obvious economic and social value.

In this paper, a green and efficient recycling process is developed to recycle spent LiCoO<sub>2</sub> batteries. Different from the conventional recycling processes, the structure of recycled <sup>50</sup> LiCoO<sub>2</sub> is not destroyed and only the binder (PVDF) and conductive carbon (acetylene black) are removed during this recycling process. After recycling processes, the obtained LiCoO<sub>2</sub> is regenerated by solid state synthesis with Li<sub>2</sub>CO<sub>3</sub>. The properties of regenerated LiCoO<sub>2</sub> are tested and compared with <sup>55</sup> commercial LiCoO<sub>2</sub> in detail.

#### **Experimental**

#### **Recycling and regeneration**

The spent LiCoO<sub>2</sub> batteries were recycled and regenerated as the process flow diagram shown in Fig. 1. The spent batteries were <sup>60</sup> soaked in Na<sub>2</sub>SO<sub>4</sub> saturated solution with iron powders for 24 h and completely discharged by electrolyzing water and short circuit, and then dismantled in a sealed glove box. The electrolyte waste gas in sealed box was released to air after three-stage spray purification with DMF, dilute alkaline solution and water in turn, <sup>65</sup> and the electrolyte liquid remaining in the dismantled batteries was extracted and collected by centrifuging. After manual separation, washing and drying, the clean diaphragms and batteries outer shells were directly recycled, the clean cathodes and anodes needed to be further smashed.

The smashed cathodes were calcined in air at 400 °C for 1 h (to remove PVDF), and then most of the powders were separated from Al foils after sieving with 50 mesh screen. The Al foils were recyled after further washing. The cathode powders needed to be further calcined in air at 800 °C for 2 h (to remove 75 acetylene black) after ball-milling and sieving with 400 mesh screen. The C, Li and Co mass contents of the cathode powders 45

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were respectively 0.3 %, 6.4 % and 59.2 % (ICP), and the molar ratio of Li/Co was 0.92 after calculating. According to the data, 100 g cathode powders were mixed with the supplementary  $Li_2CO_3$  powders (molar ratio of Li/Co in the mixtures was 1.05), s calcined in air at 850-950 °C for 12 h, ball-milled, and sieved with 400 mesh screen. Finally, the regenerated LiCoO<sub>2</sub> was obtained.

The smashed anodes were further processed as the process flow diagram shown in Fig. 1. At last, clean Cu foils and the <sup>10</sup> mixture of graphite and conductive additive were recycled.



Fig. 1 Recycling and regeneration process flow diagram of spent  $LiCoO_2$  batteries.

#### 15 Physical and chemical properties measurements

The thermal gravimetric analysis was measured with Thermo Gravimetric Analyzer (TGA, EXSTAR6000, SEIKO). The total chemical composition was analyzed by an inductively coupled plasmas spectrometer (ICP, SPS 7800, Seiko Instruments, Japan).

- <sup>20</sup> The crystal structure and surface configuration were characterized by X-ray diffraction (XRD, Rigaku D/MAX-2500), scanning electron microscope (SEM, JMS-6700F, JEOL). The tap density was measured by ZS tap density meter (ZS-201) and the particle size distribution was measured with a particle size analyzer
- 25 (OMEC, LS-POP (6)). The specific surface areas were measured with nitrogen adsorption/desorption isotherms (NOVA 2200e, Quantachrome Instruments).

After regeneration, the amount of the residual  $Li_2O$  and other alkaline compounds on the surface of particle, which was highly

 $_{30}$  related to processability in a lithium battery system, was measured by the following method. Firstly, 1.000 g LiCoO<sub>2</sub> was added into 1000 mL redistilled water with continually stirring 0.5 h under a nitrogen atmosphere. Then, pH value of solution was measured by Mettler PE20.

#### 35 Electrochemical properties measurements

For fabrication of cathodes consisted of 80 wt.% active materials, 10 wt.% acetylene black, and 10 wt.% PVDF, 3.2 g LiCoO<sub>2</sub> was mixed with 0.4 g acetylene black and 0.4 g PVDF in N-methyl-2-pyrrolidone (NMP). The electrochemical characterization of

<sup>40</sup> electrodes was performed using CR2032 coin-type test cells with lithium foil as the anode and 1 M LiPF<sub>6</sub> in ethylene carbonate and diethyl carbonate (1:1 in volume) as the electrolyte. The cells were charged and discharged between 3.0 V and 4.3 V versus Li<sup>+</sup>/Li by applying a current density of 30 mA g<sup>-1</sup> at 25 °C.

#### **Results and discussion**



Fig. 2 (a) TG-DTG curves of electrode powders scraped directly from clean cathodes (b) TG-DTG curves of PVDF.

Fig. 2 (a) shows the TG-DTG curves of cathode powders scraped directly from clean cathodes. There are two weight loss steps observed at 400-500 °C and 500-620 °C in the curves. Combining the TG-DTG curves of PVDF in Fig. 2(b), the first rapid weight loss step is attributed to the decomposition of the PVDF, while the second weight loss step is attributed to the oxidization of the acetylene black. Therefore, 400 °C is selected to remove PVDF (calcination at over 400 °C is more efficient but will accelerate the oxidization of Al foils) and 800 °C is selected to remove the acetylene black (calcination at 800 °C is more efficient than that at 620 °C). After calcination at 400 °C, the PVDF in recycled cathode powders can be removed completely, which is beneficial for the separation of powders and Al foils. After calcination at 800 °C, the acetylene black can be removed scompletely, which is beneficial for the further regeneration.

Fig. 3 shows XRD patterns of the recycled  $\text{LiCoO}_2$  after regeneration at different temperatures. Before regeneration, there are some small diffraction peaks of Co<sub>3</sub>O<sub>4</sub> observed at 32.2° and 36.8°, after regeneration at 800-950 °C, the diffraction peaks of 70 Co<sub>3</sub>O<sub>4</sub> disappear, and all the regenerated  $\text{LiCoO}_2$  has  $\alpha$ -NaFeO<sub>2</sub> layered structure. It is generally believed that the higher I<sub>003</sub>/I<sub>104</sub> is corresponding to the better layered structure of LiCoO<sub>2</sub>, which is of great advantage to the intercalation/deintercalation of Li<sup>+</sup> and the good electrochemical properties. It can be seen that  $I_{003}/I_{104}$  of LiCoO<sub>2</sub> before regeneration is 1.232, demonstrating 5 the poor layered structure. After regeneration,  $I_{003}/I_{104}$  of LiCoO<sub>2</sub> increases obviously as regeneration temperature rises from 800 °C to 900 °C, demonstrating the repaired layered structure.  $I_{003}/I_{104}$  reaches the maximum of 2.554 at 900 °C, but decreases when the regeneration temperature rises to 950 °C. It is

<sup>10</sup> known that too high temperature can result in some loss of lithium, thus can result in lattice defects and a decline of the crystallization degree. <sup>22</sup>



Fig. 3 (a)XRD patterns of LiCoO<sub>2</sub> after regeneration at different temperatures, and (b) the enlarged view of rectangle region.

SEM images of the recycled LiCoO<sub>2</sub> after regeneration are shown in Fig. 4. After regeneration, there are some small particles (residual Li<sub>2</sub>O) attached to the surface of LiCoO<sub>2</sub>, but as <sup>20</sup> regeneration temperature rises, these small particles decrease gradually until disappear completely. The similar phenomenon has been reported.<sup>23</sup> In addition, it can be observed that the particle size of regenerated LiCoO<sub>2</sub> is in the range of 5-20 um and increases a little as the regeneration temperature rises from  ${}_{25}$  800 °C to 900 °C. The morphology and particle size of the regenerated LiCoO<sub>2</sub> are similar to those of commercial LiCoO<sub>2</sub> (5-20 um).



Fig. 4 SEM images of LiCoO<sub>2</sub> after regeneration at different temperatures. (a) before regeneration, (b) 800 °C, (c) 850 °C, (d) 900 °C, (e) 950 °C

Generally, high tap density of LiCoO<sub>2</sub> is corresponding to excellent processing properties in the battery production. Table 1 lists the tap densities of LiCoO<sub>2</sub> after regeneration at different temperature. The tap density of LiCoO<sub>2</sub> before regeneration is far <sup>35</sup> from that of commercial LiCoO<sub>2</sub> (2.4-2.9 g ml<sup>-1</sup>). As the regeneration temperature rises from 800 °C to 900 °C, the tap densities of regenerated LiCoO<sub>2</sub> increase gradually and reach the maximum of 2.366 g ml<sup>-1</sup> at 900 °C, which is close to the level of commercial LiCoO<sub>2</sub>. However, when the regeneration <sup>40</sup> temperature rises to 950 °C, the tap density reduces. These changes may be caused by material agglomeration at 950 °C, which is often observed in industrialized production of LiCoO<sub>2</sub> at this temperature.

Table 1 The tap densities of LiCoO2 after regeneration at different45 temperatures.

Samples	Tap density (g ml <sup>-1</sup> )
Before regeneration	2.176
800 °C 12 h	2.311
850 °C 12 h	2.324
900 °C 12 h	2.366
950 °C 12 h	2.228



Fig. 5 Size distribution curves of LiCoO<sub>2</sub> after regeneration at different temperatures.

- Particle size is also one of the important parameters related to <sup>5</sup> processing properties. The size distribution curves of LiCoO<sub>2</sub> after regeneration at different temperature are shown in Fig. 5. The average particle size (D50) of LiCoO<sub>2</sub> is 13.45 um before regeneration, but decrease to 11.50 um after regeneration at 800 °C. As the regeneration temperature rises from 800 °C to <sup>10</sup> 900 °C, the average particle size (D50) of regenerated LiCoO<sub>2</sub>
- increases gradually. However, the average particle size (D50) of regenerated ElCoO<sub>2</sub> increases gradually. However, the average particle size (D50) increases sharply from 900 to 950 °C, which is due to the material agglomeration occurs at 950 °C. Except for LiCoO<sub>2</sub> regenerated at 950 °C, the average particle size (D50) of other <sup>15</sup> regenerated LiCoO<sub>2</sub> is within the scope of commercial LiCoO<sub>2</sub> (9-18 um).

Table 2 The specific surface areas of LiCoO<sub>2</sub> after regeneration at different temperatures.

Samples	Specific surface areas (m <sup>2</sup> g <sup>-1</sup> )
Before regeneration	0.747
800 °C 12 h	0.546
850 °C 12 h	0.506
900 °C 12 h	0.178
950 °C 12 h	0.191

- <sup>20</sup> Low specific surface areas is also conducive to good processing properties of LiCoO<sub>2</sub>. Table 2 lists the specific surface areas of LiCoO<sub>2</sub> after regeneration at different temperature. Brunauer-Emmett-Teller (BET) specific surface areas of LiCoO<sub>2</sub> before regeneration is as high as 0.747 g ml<sup>-1</sup>. As
- <sup>25</sup> the regeneration temperature rises 800 °C to 900 °C, the specific surface areas of LiCoO<sub>2</sub> decrease gradually and reach the minimum of 0.178 g ml<sup>-1</sup> at 900 °C, which is within the scope of commercial LiCoO<sub>2</sub> (0.2-0.6 g ml<sup>-1</sup>).

Table 3 The pH values of LiCoO <sub>2</sub> after regeneration at different temperatures.					
-	_			_	-

Samples	pH values
Before regeneration	10.00

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Low pH value is also conducive to good processing properties of LiCoO<sub>2</sub>. Table 3 lists the pH values of LiCoO<sub>2</sub> after regeneration at different temperature. It can be seen that the pH value of LiCoO<sub>2</sub> decreases as the regeneration temperature rises. <sup>35</sup> This phenomenon can be explained as follows, as the regeneration temperature rises, more added Li<sub>2</sub>CO<sub>3</sub> reacts with fine powers and the less Li<sub>2</sub>CO<sub>3</sub> is residual, so the pH value decreases. In addition, the pH values of the regenerated LiCoO<sub>2</sub> are all within the scope of commercial LiCoO<sub>2</sub> (9.5-11.5).

Based the above test datas, the physical and chemical properties properties (XRD, morphology, tap density, average particle size, specific surface area and pH value) of  $LiCoO_2$  after regeneration at 900 °C are all close to those of commercial  $LiCoO_2$  and meet the commercial requirements for reuse.



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0.0938

0.0313

0.0375

99.27

99.08

97.07

0.1300

0.0463

0.0225

850 °C 12 h

900 °C 12 h

950 °C 12 h

150.6

152.4

150.3

## Fig. 6 Electrochemical properties of LiCoO<sub>2</sub> after regeneration at different temperatures.

Fig. 6 displays the electrochemical properties of LiCoO<sub>2</sub> after regeneration at different temperature. It is obvious that the <sup>5</sup> electrochemical properties of LiCoO<sub>2</sub> before regeneration are poor and not suitable for reusing. By contrast, the electrochemical properties of regenerated LiCoO<sub>2</sub> are improved obviously. Especially after regeneration at 900 °C, the discharge capacity could reach about 152.4 mAh g<sup>-1</sup> and the attenuation rate of

- <sup>10</sup> capacity during every cycle is only 0.0313 mAh g<sup>-1</sup>. The improved electrochemical properties of the regenerated  $\text{LiCoO}_2$ are associated with the repaired layered structure, which is demonstrated by the increasing  $I_{003}/I_{104}$  (in Fig. 3). The electrochemical properties of regenerated  $\text{LiCoO}_2$  at 900 °C are
- <sup>15</sup> close to those of commercial LiCoO<sub>2</sub> (140-155 mAh g<sup>-1</sup>, coin cell) and meet the commercial requirements for reuse.

#### Conclusions

A green recycling process of spent  $LiCoO_2$  batteries is developed in this paper. In this process, the spent  $LiCoO_2$  batteries can be

- <sup>20</sup> dismantled, separated and recycled without secondary polution. After solid state synthesis with Li<sub>2</sub>CO<sub>3</sub>, the recycled LiCoO<sub>2</sub> is regenerated efficiently. The physical and chemical properties properties and electrochemical properties of LiCoO<sub>2</sub> after regeneration at 900 °C are all close to those of commercial
- <sup>25</sup> LiCoO<sub>2</sub>, and meet the commercial requirements for reuse. In general, the novel recycling and regeneration processes are simple, comprehensive, environmental friendly, low-cost and can be applied to a large scale in industrialization.

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