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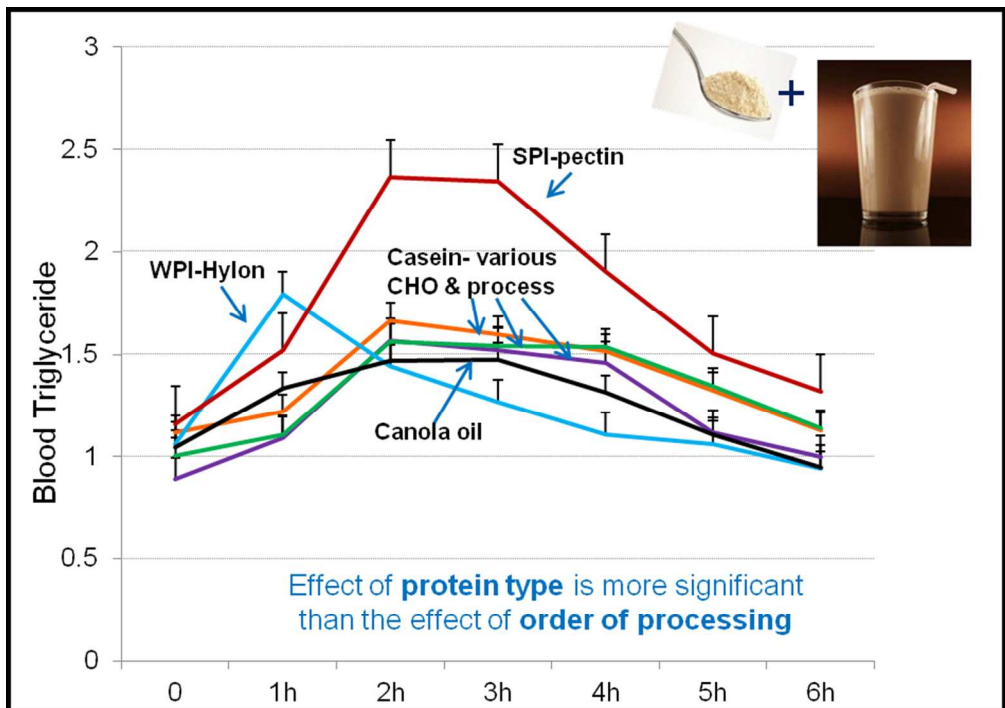


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1 **Digestion of microencapsulated oil powders: *In vitro* lipolysis and *In vivo***  
2 **absorption from a food matrix**

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12

13 **ABSTRACT**

14 Microencapsulation provides a vehicle for the incorporation of fats and oils into powders that  
15 can be used as dry ingredients in an expanded variety of food products. Microencapsulated  
16 omega-3 oils in particular are commonly incorporated into a variety of foods and numerous *in*  
17 *vitro* studies have examined the impact of individual microencapsulation technologies on the  
18 simulated digestibility of the oil core. We have exposed twelve microencapsulated canola oil-  
19 in-water emulsions, formulated with different proteins (milk or soy) or mixtures of protein  
20 and carbohydrates (sugars, oligosaccharides, resistant starch) and processed into powders by  
21 spray drying, to simulated gastric and intestinal fluids *in vitro*. The extent of lipolysis of the  
22 canola oil in these products varied between 12-68 % suggesting that the *in vitro* digestibility  
23 of the oil within the powders was dependent on both the formulation and the processing steps  
24 used in their manufacture. Five microencapsulated powders with differing extents of *in vitro*  
25 lipolysis were then incorporated into a dairy beverage for an *in vivo* human trial with neat oil  
26 incorporation in the beverage used as the control. Measurement of triglyceride levels in blood  
27 revealed both enhanced peak height and area under the curve (AUC) *in vivo* for the  
28 microencapsulated oil groups when compared to the neat oil control. The range of lipolysis  
29 efficiencies observed with the different formulations *in vitro* was not reflected *in vivo*. These  
30 observations suggest that care needs to be taken when extrapolating data from *in vitro*  
31 lipolysis to bioavailability in humans.

32

33 Keywords: omega-3 oil, microencapsulation, *in-vitro*, *in-vivo*, food matrix

34

## 35 **Introduction**

36 Emulsions stabilised by low molecular weight emulsifiers, gums or proteins or combinations  
37 of these have been used for the delivery of oils into foods.<sup>1-3</sup> Emulsions may be converted  
38 into powdered ingredients to enable them to be delivered in a convenient format for food  
39 manufacturing applications. Proteins alone or in combination with carbohydrates have been  
40 typically used in the formulations for spray dried oil powders.<sup>4</sup> To improve the resistance of  
41 unsaturated oil powders to oxidation, proteins and carbohydrates used for encapsulation have  
42 been heat treated to form Maillard reaction products.<sup>5</sup> The heat treatment can be carried out  
43 on the aqueous protein-carbohydrate mixture prior to emulsion formation or the oil may be  
44 emulsified with a physical blend of protein and carbohydrate prior to heat treatment of the  
45 whole emulsion.<sup>6</sup>

46 Many studies using different *in vitro* models have been used to evaluate the  
47 bioaccessibility of oils and food bioactive components delivered in emulsions.<sup>7</sup> Factors  
48 affecting the *in vitro* digestion of the emulsions include *in vitro* test conditions (e.g. shear,  
49 temperature, pH, concentration and type of digestive enzymes, bile salts) and the physico-  
50 chemical properties of the emulsion formulation (e.g. the size of the oil droplets, their  
51 interfacial composition and structure, the degree of crystallisation of the fat phase) which  
52 affect the lipolysis of the oil.<sup>8-11</sup> The interfacial composition is altered after each digestion  
53 stage (i.e. mouth, stomach, small intestine) under simulated *in vitro* conditions as well as *in*  
54 *vivo*, and this has a significant effect on the digestibility of lipids. In addition, structuring of  
55 emulsions take place at each stage of the digestion process which influences the subsequent  
56 rate and extent of lipolysis as the emulsion transits through to other parts of the  
57 gastrointestinal tract.<sup>12,13</sup>

58 The extent to which *in vitro* test results can be used to predict the fate of the oil in the  
59 body needs to be further understood. The comparability of *in vitro* and *in vivo* results is

60 dependent on the *in vitro* model used, the nature of the carrier systems for the emulsified  
61 lipids and the animal model used for the *in vivo* studies. When different types of emulsion-  
62 based delivery systems (conventional emulsions, small microcluster emulsions, large  
63 microcluster emulsions and filled hydrogel beads) were compared, the data from *in vitro*  
64 digestion and *in vivo* rat trials had similar qualitative trends although there were quantitative  
65 differences.<sup>14</sup> However, a lack of correlation between some *in vitro* evaluations and *in vivo*  
66 data has also been observed. For example, although *in vitro* studies of emulsified lipid  
67 droplets coated by lecithin or lecithin-chitosan suggested that the additional chitosan layer  
68 produced using a layer-by-layer deposition technique inhibited the digestibility of the  
69 emulsified droplet, studies on mice showed that *in vivo* lipid digestibility of chitosan-  
70 encapsulated oil droplets was not inhibited.<sup>15</sup> *In vitro* studies showed that there was  
71 incomplete lipolysis of microencapsulated fish oil stabilised by heated protein-carbohydrate  
72 mixtures incorporated into foods after exposure to simulated gastric and intestinal fluids, with  
73 lipolysis of the oil in the cereal bar being lower than that in orange juice or yoghurt.<sup>16</sup>  
74 However, an ileostomy trial with the same formulations suggested higher levels of lipid  
75 digestion and absorption in humans (>98%) although there was some evidence of altered  
76 transit time with different food matrices.<sup>17</sup>

77 In this work, a direct comparison of a large number of formulations tested *in vitro*, from  
78 which formulations with very different extents of *in vitro* lipolysis were chosen to be tested in  
79 human trials. We determined the *in vitro* lipolysis of twelve microencapsulated canola oil  
80 powders stabilised with different proteins (milk or soy) or mixtures of protein and  
81 carbohydrates (sugars, oligosaccharides, resistant starch) and processed in different ways.  
82 We also compared the triglycerides in the blood of healthy humans who consumed dairy  
83 beverages enriched with either neat canola oil or selected microencapsulated oil powders.  
84 The aim was to determine whether microencapsulation altered the lipolysis of the oils *in vitro*

85 and the uptake of oil on digestion, and to determine if there is a relationship between *in vitro*  
86 lipolysis and the timing of the peak in triglycerides *in vivo*.

87

## 88 **Materials and methods**

### 89 **Materials**

90 Commercially available food grade ingredients were purchased from suppliers or from a local  
91 supermarket. Sodium caseinate (NaCas; Alanate 180<sup>®</sup>) and whey protein isolate (WPI;  
92 Alacen 895<sup>®</sup>) were from New Zealand Milk Products, Fonterra (Rowville, Victoria,  
93 Australia). Hydrolysed whey protein (HWP) was from Myopure (Petersham, New South  
94 Wales, Australia). Soy protein isolate (SPI; Supro<sup>®</sup> 760 IP) was from Solae Australia Pty Ltd  
95 (Chatswood, New South Wales, Australia). Dried glucose syrup (DGS, Fieldose 30<sup>®</sup> with  
96 dextrose equivalent of 30) was from Penford Australia Ltd (Lane Cove, New South Wales,  
97 Australia) and oligofructose (Oligo, Beneo P95<sup>®</sup>) was from Mandurah Australia Pty Ltd  
98 (Matraville, New South Wales, Australia). High amylose resistant starch (Hylon VII<sup>®</sup>) was  
99 from National Starch (Seven Hills, New South Wales, Australia). Pectin (Grinsted pectin  
100 SS200) was from Danisco Australia Pty Ltd (Botany, New South Wales, Australia). Canola  
101 oil (Crisco<sup>®</sup>) was from Goodman Fielder (Port Melbourne, Victoria, Australia). Powder  
102 drinking chocolate (Weight Watchers) and UHT fat free skim milk (Devondale) was  
103 purchased from Coles Supermarket (Werribee, Victoria, Australia).

104

### 105 **Formulation and processing of microencapsulated oil powders**

106 Twelve microencapsulated oil powder formulations containing 50% canola oil (dry basis),  
107 with protein alone (WPI) or protein (NaCas, WPI, HWP, SPI) in combination with one or  
108 more carbohydrates (processed Hylon VII (Hylon), oligofructose (Oligo), dried glucose syrup  
109 (DGS) or pectin) were manufactured on a pilot scale (Table 1). The processing of the Hylon

110 VII<sup>®</sup> involved heating a 20% total solids (TS) starch dispersion at 121°C for 60 min (FMC  
111 Surdry, Spain), cooling to room temperature, mashing the starch gel formed, diluting with  
112 deionised water to 10% TS and homogenising at 35MPa (Rannie Pilot Homogenizer,  
113 Denmark) prior to its use as an encapsulant.

114 The outline of the processes used for the manufacture of the microencapsulated oil  
115 powders is given in Fig 1. Briefly the protein was dispersed in water (60°C) using a high  
116 shear mixer with stirring for 30 min. For Processes A and B (Fig 1), carbohydrates were  
117 added to the protein solution and stirred for a further 5-10 min and the pH of the protein-  
118 carbohydrate mixtures was then adjusted to 7.5. This aqueous protein-carbohydrate mixture is  
119 referred to as the aqueous phase. For formulations where heating of the aqueous phase was  
120 carried out (Fig 1, Process A), the aqueous phase was heat-treated in a retort at 100°C for 50  
121 mins (FMC Surdry, Spain). Canola oil preheated to 60°C, was then added into the aqueous  
122 phase whilst stirring using a high shear mixer. This pre-emulsion was then homogenised  
123 using two-stage homogenization pressures at 350/100 bar. The emulsions were spray dried at  
124 180°C and 80°C inlet and outlet temperature, respectively. For formulations where the  
125 emulsion was heated (Fig 1, Process B), canola oil, preheated to 70°C for 30 min, was added  
126 into the aqueous phase using a high shear mixer and the pre-emulsion was homogenised  
127 using two-stage homogenization pressures at 350/100 bar. The homogenised emulsions were  
128 heated in a retort at 100°C for 50 mins (FMC Surdry, Spain), cooled down to 60°C and spray  
129 dried (Niro Production Minor, GEA process Engineering A/S, Sørborg, Denmark) at 180°C  
130 and 80°C inlet and outlet temperature, respectively.

131 For the heat-denatured WPI stabilised emulsion (Fig 1, Process C), the WPI powder was  
132 initially dispersed in water at 60°C, pH adjusted to 7.0 and heated at 90°C for 30 mins prior  
133 to oil emulsification (350/100 bar) and spray drying. For the SPI-pectin stabilised emulsion  
134 (Fig 1, Process D), an aqueous dispersions of SPI solution prepared at 60°C was mixed with a



135 pectin dispersion prepared separately at 80°C, then canola oil was added and the combined  
136 mixture then emulsified (350/100 bar) and spray dried. Spray drying was carried out as  
137 outlined above.

138

### 139 **Characterisation of microencapsulated oil powders**

140 The total oil content of powders was determined using an acid extraction method.<sup>18</sup> The total oil  
141 content was expressed as g oil/100 g powder (dry basis). The estimation of ‘free oil’ in powder  
142 was based on the method by Pisecky<sup>18</sup> except that petroleum ether was used in place of  
143 carbon tetrachloride.<sup>5</sup> The results were expressed as g/100g powder (dry basis).

144

### 145 ***In-vitro* digestion and analysis of microencapsulated oil powders**

146 The simulated gastric fluid (SGF) and simulated intestinal fluid (SIF) with bile extract were  
147 prepared as described by Oliver et al.<sup>19</sup> Sequential digestion in SGF and SIF, hereafter termed  
148 SGF-SIF, were carried out as follows: 1 g of microencapsulated oil powder or 1 g oil was  
149 dispersed in SGF (10 g). The mixture was incubated in a shaker water-bath (100 rpm) at 37°C  
150 for 2 h. After exposure to SGF, the pH of the sample was adjusted to pH 6.8. Then SIF (8 g)  
151 was added and the mixture was incubated at 37°C/100 rpm for 20 min. After this time, 2 ml  
152 of 50 mM CaCl<sub>2</sub> solution was added and the resulting mixture was further incubated at  
153 37°C/100 rpm for 160 min. The final concentration of bile salt and calcium chloride in the  
154 mixture was 12 mM and 10 mM, respectively.

155

156 **Extraction of oil after *in vitro* digestion in SGF-SIF.** Oil was extracted from the samples  
157 after *in vitro* digestion using the ammonia extraction method specified in AS 2300.1.3.<sup>20</sup> The  
158 solvent was evaporated from the extracts using a rotary evaporator (60°C) then further dried  
159 in a vacuum oven at 48°C overnight. The amount of the oil extracted after SGF-SIF was

160 expressed as g/100 g powder (dry basis). The oil recovered (as % of the total oil) was  
161 calculated from the amount of oil extracted after SGF-SIF divided by the total oil content of  
162 powders or the neat oil added. The extracted oil was used for analysis of fatty acids by GC.

163 **Quantification of total free fatty acids.** The major individual fatty acids both in free  
164 and glycerol bound forms (namely palmitic (C16:0), stearic (C18:0), oleic (C18:1), linoleic  
165 (C18:2) and linolenic (18:3)) were determined after acid methylation. The fatty acids in  
166 glycerol bound forms were quantified after alkaline methylation. The levels of individual free  
167 fatty acids, which indicate the extent of lipolysis, were obtained by difference. The total free  
168 fatty acids were the sum of the individual free fatty acids.

169 For the acid methylation, 50 ( $\pm 0.01$ ) mg of the extracted oil, 3 ml aliquot of internal  
170 standard solution (1.83 mg/ml C23:0 methyl ester /ml isooctane), 2 ml tetrahydrofuran and 2  
171 ml 2M sulphuric acid in methanol were added into a culture tube. The mixture solutions were  
172 blanketed with argon, capped tightly and agitated (200 rpm) at 70°C for 2.5 h in a water bath  
173 shaker. Every 30 min, the tubes were taken out from the shaker water bath and vortexed for  
174 one minute. Water (5 ml) containing sodium chloride (5% w/v) was added to stop the  
175 methylation and the methyl esters were extracted with 3 ml hexane. The top organic phase  
176 was washed with water (4 ml) containing potassium bicarbonate (5% w/v) and dried over  
177 anhydrous sodium sulphate. The methyl ester solution was subjected to GC injection without  
178 further concentration.

179 For the alkaline methylation, 50 ( $\pm 0.01$ ) mg of extracted oil, 3 ml aliquot of internal  
180 standard solution (1.83 mg C23:0 methyl ester /ml isooctane), 3 ml of hexane and 300  $\mu$ l of  
181 2M KOH/methanol solution were added into a culture tube. The mixture solutions were  
182 blanketed with argon, capped tightly and vortexed (2000 rpm) at room temperature for 10  
183 min. The methyl ester solution was neutralized by 300  $\mu$ l of 2M HCL-methyl orange water.  
184 After 30 min settling, the top layer was injected into GC without further concentration.

185 Total free fatty acids were calculated using the following formula:

$$186 \text{ Individual FA (X) (mg/g oil) = } \frac{\text{GC area for X} \times \text{IS (mg)} \times \text{CF}}{\text{GC area for IS} \times \text{oil mass (g)}} \quad (1)$$

$$187 \text{ Individual FFA = (free + glycerol bound) FA - glycerol bound FA} \quad (2)$$

$$188 \text{ Total FFA = Sum of individual free fatty acids} \quad (3)$$

189 Where: FA = fatty acid; FFA = free fatty acid; X = individual fatty acid; IS = internal

190 standard added; CF = ratio of theoretical flame ionization detector correction factor of X/IS

191 The above method was validated with fresh canola oil and the less than 0.01% total free  
192 fatty acids was obtained.<sup>16</sup>

193

#### 194 **Clinical Trial**

195 For the clinical trial, 6 healthy normotriglyceridemic volunteers (three men and three women)

196 aged 20-65 years with BMI 25-30 kg/m<sup>2</sup> were recruited. The inclusion criteria were no recent

197 history (past 3 months) of weight loss or changes to diet or physical activity routine. The

198 exclusion criteria were persons with one or more of the following conditions: Type 1 or 2

199 Diabetes, active liver and kidney disease, current gastrointestinal disease, past history of

200 gastrointestinal surgery which may affect study outcomes, intolerance to fat or on

201 medications which affect gastrointestinal tract motility or hunger /appetite. The volunteers

202 fasted from midnight, the night prior to attending the clinic in the morning. All experimental

203 procedures were approved by Human Ethics Committees of the Commonwealth Scientific

204 and Industrial Research Organization and participants provided written informed consent.

205 All research was conducted following institutional guidelines.

206 **Preparation of test samples for consumption.** The dairy-based beverages containing

207 either neat canola oil or microencapsulated canola oil powder were prepared. Five

208 microencapsulated canola oil powders, displaying different extents of lipolysis *in vitro*, were

209 chosen after completion of the *in vitro* trials and incorporated into beverages for the human

210 trial. The dairy based beverages were made up with water (78 g), skim milk (200 g) and  
211 drinking chocolate powder (Weight Watchers) (12 g) using a hand-held mixer for 45 s. Either  
212 a microencapsulated oil powder (60 g powder containing 30 g oil) or neat oil (30 g oil plus 30  
213 g water) was added and mixed for a further 30 s. Each volunteer consumed the entire 350 g  
214 chilled beverage formulation on 6 different occasions and at least three days apart to assess  
215 the time line of fat digestion from the pre-load (dairy based beverage).

216 **Conduct of clinical study.** Six healthy normotriglyceridemic volunteers (three men and  
217 three women) attended the clinic on 6 separate occasions with a minimum 3 days apart for  
218 each visit. On each occasion the volunteers consumed 350 g of an isocaloric chilled beverage  
219 containing 30 g canola oil added as neat oil (control) or oil encapsulated in selected protein or  
220 protein-carbohydrate powdered formulations. They were allowed to sit or stand but not to lie  
221 down during their time in the clinic. Finger prick samples were taken after fasting and then  
222 every hour (over 6 h) for whole blood triglyceride levels.

223 **Measurement of triglycerides.** Fingerprick triglycerides (TG) was measured using the  
224 Cardiochek Triglyceride system (Polymer Technology, Systems Indianapolis, Indiana, USA).

225 **Power calculation.** With 6 people there was 84% power,  $p < 0.05$  to see a 0.35 mmol/L  
226 difference in peak TG values and a 79% power,  $p < 0.05$  to see a 1.1 mmol/l/h difference in  
227 AUC above baseline. Plasma values are obviously a summary of absorption and clearance  
228 rates. We know nothing of the latter but given the fact that the fat is the same in all  
229 preparations there should no differences. Absorption rates will be dictated primarily by  
230 lipolysis rates with no contribution likely from differences in intestinal cell metabolism.

231 **Data analysis.** Data was analysed using SPSS v19 (IBM, Australia). The primary  
232 analysis was repeated measures ANOVA with 6 treatments repeated across 7 time points.  
233 Post hoc contrast were performed if  $p$  was  $< 0.05$  for time by treatment. No adjustments were

234 made for the number of post hoc contrasts and  $p < 0.05$  was deemed to be significant. Time by  
235 treatment reflects both a change in peak height as well as a change in peak timing.

236

## 237 **Results and Discussion**

### 238 **Total oil content and ‘free oil’ of microencapsulated oil powders**

239 The total oil and ‘free oil’ of the microencapsulated oil powders are given in Table 2. The  
240 total oil content of most microencapsulated oil powders was 46-54 % (dry basis). This  
241 compares well with the formulated amount of 50 % (dry basis) in most cases.

242 The ‘free oil’ of the powders was variable and dependent on the formulation and process  
243 conditions (Table 2). The protein only (WPI Process C), protein-pectin (SPI-pectin Process  
244 D) and NaCas or WPI formulations containing Hylon (both Process A and Process B) had  
245 high ‘free oil’ (13-25 % of the powder) (Table 2). The addition of Oligo and further  
246 replacement of Hylon with DGS to the NaCas-Hylon formulation resulted in a decrease in  
247 ‘free oil’ from 21.6 % (NaCas-Hylon Process A) to 13.4 % (NaCas-Oligo-Hylon Process A)  
248 and 0.5 % (NaCas-Oligo-DGS Process A) (Table 2). The presence of small sugars is known  
249 to aid the efficiency of the encapsulation process during drying<sup>4</sup>. The presence of low  
250 molecular weight sugars in powdered oil-containing formulations reduces the accessibility by  
251 the extracting solvent.<sup>21</sup> However, the exception was observed with the addition of sugars to  
252 the WPI-Hylon formulations which had little effect on the ‘free oil’ (Compare WPI-Oligo-  
253 Hylon with WPI-Hylon where the same process was used) (Table 2). This is possibly because  
254 the globular whey proteins by themselves form a more robust interfacial layer than the  
255 caseins. Studies on the adsorption of milk proteins at interfaces have suggested that globular  
256 whey proteins such as  $\beta$ -lactoglobulin form a more cohesive gel-like layer at the interface  
257 than the more randomly ordered caseins.<sup>22</sup>

258 The heat treatment of emulsion resulted in a marked reduction in solvent extractable  
259 ‘free oil’ when WPI was used as an encapsulant but not when NaCas or HWP was used as the  
260 protein source. This was evident when formulations with the same gross formulation made  
261 using Process A, were compared to those made using Process B (Table 2). It may have been  
262 expected that the interface of the droplets formed would be different depending on whether  
263 the aqueous protein-carbohydrate mixture was heated prior to emulsification (Process A) or  
264 whether the emulsion was formed prior to heating (Process B). This is because in systems  
265 where the unheated mixtures of proteins and carbohydrates are emulsified with the oil, only  
266 the proteinaceous species in the aqueous phase will accumulate at the interface as  
267 carbohydrates are not surface active. When these emulsions are heated, the proteins at the  
268 interface may be decorated by carbohydrates which conjugate with available sites on the  
269 protein. In systems where the oil is emulsified after heating the protein carbohydrate mixture  
270 (Process A), the composition of the interface is dependent on the type of protein encapsulant  
271 or hydrolysed protein and protein-carbohydrate conjugate formed by heating of the aqueous  
272 mixture of protein and carbohydrate and that are present at the time of emulsification.<sup>23</sup> The  
273 observation that the encapsulation efficiency was only different for heat-treatment of WPI-  
274 based formulations but not when NaCas or HWP was used as the protein source maybe  
275 related to the greater ability of WPI (a globular protein which is also prone to denaturation),  
276 to unfold at the interface compared to the caseins and hydrolysed whey protein which are less  
277 structured.<sup>22</sup>

278

### 279 ***In vitro* digestibility**

280 The *in vitro* digestibility of the microencapsulated oil powders was examined by measuring  
281 the free fatty acid released after exposure to SGF-SIF. The amount of oil that was extractable  
282 from the sample after SGF-SIF, the calculated oil extraction efficiency, the extent of lipolysis

283 measured from extracted oil and the calculated extent of lipolysis after SGF-SIF are given in  
284 Table 2.

285 Although the total oil extractable from the powders before SGF-SIF (Table 2) was close  
286 to the formulated oil content of the powders (Table 1), not all the oil could be recovered by  
287 extraction after SGF-SIF for some formulations (Table 2). The oil recovered after exposure to  
288 SGF-SIF (expressed as % of the total oil) was 53 – 115 % (Table 2). Most of the samples had  
289 >80 % of total oil recovered by solvent extraction. The exceptions were formulations  
290 containing NaCas-Hylon made using Process B (52.6 % of total oil) and HWP-Oligo-Pectin  
291 made using Process B (54.4 % of total oil) (Table 2).

292 The calculated extent of lipolysis assumes the amount of oil that is not extracted from the  
293 samples after *in vitro* digestion, is undigested oil in triglyceride form (Table 2). This  
294 calculated extent of lipolysis was taken as the % of the total oil that is bioaccessible.  
295 Quantitation of the measured amounts of free fatty acids by gas chromatography combined  
296 with the data on oil recovered suggested that 45 % - 68 % of oil was bioaccessible after SGF-  
297 SIF except for powders made from NaCas-Hylon Process B (12.1 %) and HWP-Oligo-Pectin  
298 process B (12.5 %) (Table 2). These latter two microencapsulated oil powders with the lowest  
299 amounts of (calculated) lipolysed oil (~12 % of total oil) also had the lowest amounts of  
300 recoverable extractable oil after SGF-SIF exposure (~50 %). In comparison, when neat  
301 canola oil is subject to *in vitro* digestion, there was an extremely low extent of lipolysis  
302 ( $1.08 \pm 0.42\%$ ) as under the conditions of the *in vitro* system the oil is not in the form of fine  
303 emulsion droplets. This is in contrast to when microencapsulated formulations are used and  
304 the emulsions are homogenised prior to drying. The particle size (volume median diameter)  
305 of all formulated emulsions (measured by laser light scattering) used was  $d(0.5) 0.30 - 11.46$   
306  $\mu\text{m}$  depending on the formulation and order of processing (data not shown).

307 Where the same emulsion composition was used with different processing steps, there  
308 was a consistent trend in the relative extents of bioaccessibility of the oils. Systems where  
309 microencapsulated oil powders were made from heat treated emulsions (Process B) were less  
310 bioaccessible than corresponding powders made from emulsions stabilised by heat treated  
311 aqueous mixtures of protein and carbohydrate (Process A) (Table 2). The cross-linking of  
312 interfaces of heated emulsions may have contributed to the lower bioaccessibility of oil in  
313 powders made from heat treated emulsions (Process B).

314

### 315 **Selection of microencapsulated oil powders for *in vivo* human trials**

316 The *in vitro* analysis of the microencapsulated oil powders exposed to SGF-SIF indicated  
317 differences in the extent of lipolysis (Table 2). Based on the *in vitro* analyses, five samples  
318 with different levels of *in vitro* lipolysis were chosen for a human study in which the  
319 bioavailability of microencapsulated oil powders and neat oil (control) when incorporated  
320 into a dairy based average were compared. The powders chosen were NaCas-Hylon Process  
321 B, NaCas-Hylon Process A, NaCas-Oligo-DGS Process A, WPI-Hylon Process A and SPI-  
322 Pectin process D. NaCas-Hylon Process B (12.1 % lipolysed) was one of the least digested  
323 microcapsules based on *in vitro* analysis. NaCas-Hylon Process A (53.4 % lipolysed) and  
324 SPI-Pectin Process D (54.6 % lipolysed) were in the middle range for extents of lipolysis.  
325 WPI-Hylon Process A (64.2 % lipolysed) and NaCas-Oligo-DGS Process A (67.6 %  
326 lipolysed) were two of the most extensively lipolysed samples *in vitro* amongst the powders  
327 screened (Table 2). Although HWP-Oligo-Pectin Process B (12.5 % lipolysed) had a very  
328 low extent of digestion comparable to NaCas-Hylon Process B (12.1 %), this system was not  
329 used in the clinical trial due to its unacceptable flavour profile, which was attributed to the  
330 hydrolysed protein component.

331



**332 Clinical trial**

333 There was an enhanced peak height and area under curve (AUC) for most subjects (individual  
334 results not shown) when the dairy beverage with microencapsulated oil powders were  
335 consumed, compared to that for the dairy beverage made by incorporation of the neat oil (Fig  
336 2). As the fat used was the same in all preparations no differences in the handling of the  
337 triglyceride after digestion and absorption should occur. Therefore the enhanced peak and  
338 AUC may be attributed in part to smaller oil droplet size of all the microencapsulated  
339 formulations compared to neat oil. Others have shown that decreasing particle size of oil  
340 droplets increases the rate of lipolysis<sup>24</sup> and  $\beta$ -carotene bioaccessibility in emulsions<sup>25</sup>. This  
341 was considered to be due to the increase in lipid surface area exposed to pancreatic lipase.

342 There were only small differences in the AUC for plasma triglyceride level between  
343 the canola oil mixed with the dairy beverage and four of the microencapsulated formulations  
344 (Cas-Hylon Process B, Casein-Hylon Process A, Casein-oligo-DGS Process A and WPI-  
345 Hylon Process A) in dairy beverages (Fig. 2). This suggests the accessibility of lipase to the  
346 interface of microencapsulated particles and the canola oil mixed with the dairy beverage was  
347 largely similar. Even if neat canola oil was added into beverage and was consumed, it will be  
348 emulsified when blended into the beverage because it is mixed with other components in the  
349 dairy beverage (e.g. dairy protein) that have emulsifying properties. After consumption there  
350 is the further combined action of the mixing in the stomach and the presence of other  
351 emulsifying food components that are residual in the stomach. Others have shown the  
352 bioequivalence of microencapsulated powders made by a coacervation process and the same  
353 oil delivered in gelatin capsules<sup>1</sup>.

354 The highest peak and area under curve is most marked with SPI pectin Process D (e)  
355 compared to all other treatments. SPI pectin Process D (e) is significantly different ( $p < 0.05$ )  
356 from neat canola oil (f), WPI-Hylon Process A (d) and Cas-Hylon Process B (a). In 3 out of 6

357 subjects, Cas-Oligo-DGS Process A (c) produced some prolongation or delay in the curves  
358 (individual results not shown) and is in fact significantly different ( $p < 0.05$ ) from WPI-Hylon  
359 Process A (d), SPI-pectin Process D (e) and neat canola oil (f) on time by treatment analysis.

360 The most noticeable difference was the shifting forward of the release of the WPI-  
361 Hylon Process A formulation compared to all other formulations. It was also noted that when  
362 the protein in the WPI-Hylon Process A formulation was substituted with casein to make the  
363 Cas-Hylon Process A formulation, a delayed release was obtained (Fig 2). This shows the  
364 important influence of the protein on the lipolysis *in vivo*, with a casein based interface being  
365 more resistant to early lipolysis.

366 A significant observation is the marked enhancement in the AUC for the SPI-pectin  
367 Process D formulation compared to all other formulations tested. Given that the same fat and  
368 the same amount of fat were used in all preparations any differences seen in postprandial  
369 triglyceride will reflect differences in the gut only i.e. gastric and intestinal emptying rates as  
370 well as differences in digestion. After digestion absorption of the free fatty acids and  
371 monoglycerides will be the same in all preparations. There are many factors that influence the  
372 lipolysis of oils. In encapsulated or emulsified systems, it is envisaged that lipolysis will  
373 depend on the access of the lipase to the encapsulated oil and the particle size of the oil  
374 droplet. These include the digestibility of the interface and the ease of displacement of  
375 protein from the interface and the subsequent attachment of lipase which then enables the  
376 lipase to act on the emulsified oil. It is well known that different proteins adopt different  
377 conformations at the interface and in addition the digestibility of different proteins is also  
378 different, whether this is *in vitro* or *in vivo*. A study which compared WPI and SPI based oil-  
379 in-water emulsions (10% w/w soybean oil, 1.5% w/w protein, homogenised at 40 MPa using  
380 a microfluidizer) suggested that there was more lipolysis of the SPI emulsions and also that  
381 the particle size of SPI emulsions were smaller than those of WPI emulsions<sup>26</sup>. In our work,

382 the % lipolysis in the WPI emulsions (45.2 – 64.9 % lipolysis, Table 2) depended on the  
383 formulation and process used and there was not a consistent trend in extent of lipolysis when  
384 compared to that of the SPI-pectin emulsion (54.6 lipolysis, % Table 2). Taken together, this  
385 highlights the sensitivity of the extent of lipolysis to the different interfacial structures formed  
386 with changed formulations and processes even *in vitro*. Although the particle size of the  
387 emulsions *in vivo* have not been measured, it is tempting to speculate that the increased  
388 digestibility of the SPI-pectin systems may be because the emulsified oil in this system *in*  
389 *vivo* remain more stable to coalescence compared to dairy protein stabilised emulsions and/or  
390 that the ease of displacement of the SPI pectin interface was greater, providing easier access  
391 to lipase and consequently a higher degree of lipolysis.

392 The data suggests that the SPI-pectin Process D formulation, which provided the  
393 highest concentration of triglycerides in the blood, is one that has the potential to be the most  
394 bioavailable and may provide an exceptional system for the delivery of fatty acids, when  
395 incorporated into a dairy beverage. It would be important to determine if this enhancement is  
396 also obtained with a range of other oils (e.g. omega- 3 fish oils) and extends to the transit of  
397 lipophilic bioactives (e.g. carotenes) and also when the SPI-pectin Process D formulation is  
398 delivered in different food matrices.

399 There is no direct correlation between lipolysis *in vitro* (12.2 – 67.6% lipolysis  
400 amongst formulations (a) – (e), Table 2) and the AUC *in vivo* for the formulations compared  
401 (Fig 2). A plot of AUC and the extent of lipolysis *in vitro* showed a poor correlation between  
402 these two parameters ( $n=5$ ,  $r^2=0.011$ ) (Figure not shown). One of the reasons for lack of  
403 correlation between the *in vitro* and *in vivo* data is likely to be the higher shear forces *in vivo*  
404 relative to that *in vitro*.

405

## 406 **Conclusions**

407 *In vitro* studies are useful to the extent that they give insights into how the structure of the  
408 interface around the oil droplets affects the accessibility of the oil within an oil droplet to  
409 digestive enzymes. In this work, there was no direct correlation between *in vitro* and *in vivo*  
410 digestibility for corresponding microencapsulated formulations. *In vivo* lipolysis is highly  
411 efficient in systems where oil is delivered in emulsions formulated with food proteins and  
412 carbohydrates.<sup>17</sup> When oil was delivered as microencapsulated oil powders incorporated into  
413 a dairy based beverage, there was enhanced peak height and AUC *in vivo* for the  
414 microencapsulated oil groups when compared to the neat oil control. *In vivo* human trials are  
415 essential to understand the bioequivalence of oil delivered in different food structures.

416

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420

#### 421 **References**

- 422 1. C.J. Barrow, C. Nolan and Y. Jin, Stabilization of highly unsaturated fatty acids and  
423 delivery into foods, *Lipid Tech.*, 2007, 19(5), 108-111.
- 424 2. M.A. Augustin and Y. Hemar, Nano- and micro-structured assemblies for encapsulation  
425 of food ingredients, *Chem. Soc. Rev.* 2009, 38(4), 902-912.
- 426 3. S. Drusch and S. Mannino, Patent-based review on industrial approaches for the  
427 microencapsulation of oils rich in polyunsaturated fatty acids, *Trends Food Sci. Technol.*,  
428 2009, 20(6-7), 237-244.
- 429 4. S.A. Hogan, B.F. McNamee, E.D. O’Riordan and M. O’Sullivan, Emulsification and  
430 microencapsulation properties of sodium caseinate/carbohydrate blends, *Int. Dairy J.*,  
431 2001, 11(3), 137-144.

- 432 5. M.A. Augustin, L. Sanguansri and O. Bode, Maillard reaction products as encapsulants  
433 for fish oil powders, *J. Food Sci.*, 2006, 71(2), E25-E32.
- 434 6. L. Sanguansri and M.A. Augustin, Encapsulation of Food Ingredients. *WO200174175*,  
435 2001.
- 436 7. F. Leal-Calderon and M. Cansell, The design of emulsions and their fate in the body  
437 following enteral and parenteral routes, *Soft Matter*, 2012, 8, 10213-10225.
- 438 8. A.M. Nik, A.J. Wright and M. Corredig, Impact of interfacial composition on emulsion  
439 digestion and rate of lipid hydrolysis using different *in vitro* digestion models, *Colloids  
440 and Surfaces B: Biointerfaces*, 2011, 83, 321-330.
- 441 9. H. Singh and A. Ye, Structural and biochemical factors affecting the digestion of protein-  
442 stabilized emulsions, *Current Opin. Colloid & Interface Science*, 2013, 18, 360-370.
- 443 10. D.J. McClements and H. Xiao, Potential biological fate of ingested nanoemulsions:  
444 influence of particle characteristics, *Food and Funct.*, 2012, 3, 202-220.
- 445 11. D.J. McClements, Crystals and crystallization in oil-in-water emulsions: Implications for  
446 emulsion-based delivery systems, *Adv. Colloid and Interfacial Sci.*, 2012, 174, 1-30
- 447 12. M. Golding, T.J. Wooster, L. Day, M. Xu, L. Lundin, J. Keogh and P. Clifton, Impact of  
448 gastric structuring on lipolysis of emulsified lipids, *Soft Matter*, 2011, 7, 3513-3523.
- 449 13. J. Maldonado-Valderrama, J.A. Holgado Terriza, A. Torcello-Gómez and M.A.  
450 Cabrerizo-Vilchez, *In vitro* digestion of interfacial structures, *Soft Matter*, 2013, 9, 1043-  
451 1053.
- 452 14. Y. Li, J. Kim, Y. Park and D.J. McClements, Modulation of lipid digestibility using  
453 structured delivery systems: Comparison of *in vivo* and *in vitro* measurements, *Food  
454 Funct.*, 2012, 3, 528-536.

- 455 15. G.Y. Park, S. Mun, Y. Park, S. Rhee, E.A. Decker, J. Weiss, D.J. McClements and Y.  
456 Park, Influence of encapsulation of emulsified lipids with chitosan on their in vivo  
457 digestibility, *Food Chemistry*, 2007, 104(2), 761-767.
- 458 16. Z. Shen, A. Apriani, R. Weerakkody, L. Sanguansri and M.A. Augustin, Food matrix  
459 effects on in vitro digestion of microencapsulated tuna oil powder, *J. Agric Food Chem.*,  
460 2011, 59, 8442-8449.
- 461 17. L. Sanguansri, Z.P. Shen, R. Weerakkody, M. Barnes, T. Lockett and M.A. Augustin,  
462 Omega-3 fatty acids in ileal effluent after consuming different foods containing  
463 microencapsulated fish oil powder - an ileostomy study, *Food Funct.*, 2013, 4(1), 74-82.
- 464 18. J. Pisecky, Handbook of milk powder manufacture, *Copenhagen, Niro A/S*, 1997, p 206.
- 465 19. C.M. Oliver, M.A. Augustin and L Sanguansri, Maillard-based casein-carbohydrate  
466 microcapsules for the delivery of fish oil: emulsion stability during *in vitro* digestion,  
467 *Aust J Dairy Technol.*, 2009, 64, 80-83.
- 468 20. AS 2300.1.3. General methods and principles - Determination of fat - Gravimetric  
469 method Methods, *Standards Assoc. of Aust.*, 2008, 1-8.
- 470 21. S.L. Young, X. Sarda and M. Rosenberg, Microencapsulating properties of whey  
471 proteins, 1. Microencapsulation of anhydrous milk-fat, *J Dairy Sci.*, 1993, 10, 2868-2877.
- 472 22. E. Dickinson, Milk protein interfacial layers and the relationship to emulsion stability and  
473 rheology, *Colloids and Surfaces B: Biointerfaces* 2001, 20, 197-210.
- 474 23. C. Chung, L. Sanguansri and M.A. Augustin. *In vitro* lipolysis of fish oil microcapsules  
475 containing protein and resistant starch, *Food Chem.*, 2011, 124, 1480-1489.
- 476 24. M. Armand, B. Pasquier, M. Andre, P. Borel, M. Senft, J. Peyrot, et al. Digestion and  
477 absorption of 2 fat emulsions with different droplet sizes in the human digestive tract, *Am*  
478 *J Clin Nutr*, 1999, 70, 1096-106.

- 479 25. S. Salvia-Trujillo, C. Qian, O. Martin-Belloso, D.J. McClements. Influence of particle  
480 size on lipid digestion and  $\beta$ -carotene bioaccessibility in emulsions and nanoemulsions,  
481 *Food Chem.*, 2013, 1472-1480.
- 482 26. A.M. Nik, A.J. Wright, M. Corredig. Impact of interfacial composition on emulsion  
483 digestion and rate of lipid hydrolysis using different in vitro digestion models, *Colloids*  
484 *and Surfaces B: Biointerfaces*, 2011, 321-330.

**Table 1** Formulated compositions of the aqueous phase, emulsions and microencapsulated oil powders

Aqueous phase components <sup>a</sup>	ID Process	Heat-treatment		Aqueous phase composition (% wet basis)		Emulsion composition (% wet basis)			Powder composition (% dry basis)		
		Aqueous	Emulsion	Protein	CHO <sup>b</sup>	Protein	CHO <sup>b</sup>	Oil	Protein	CHO <sup>b</sup>	Oil
NaCas-Hylon	B	No	Yes	6.0	6.0	5.4	5.4	10.7	25.0	25.0	50.0
NaCas-Hylon	A	Yes	No	6.0	6.0	5.4	5.4	10.7	25.0	25.0	50.0
NaCas-Oligo-Hylon	A	Yes	No	5.7	11.4	4.8	9.7	14.5	16.7	33.3	50.0
NaCas-Oligo-DGS	A	Yes	No	5.7	11.4	8.6	17.1	25.7	16.7	33.3	50.0
WPI-Hylon	A	Yes	No	5.0	5.0	4.6	4.6	9.1	25.0	25.0	50.0
WPI-Hylon	B	No	Yes	5.0	5.0	4.6	4.6	9.1	25.0	25.0	50.0
WPI-Oligo-Hylon	A	Yes	No	4.8	9.6	4.2	8.3	12.5	16.7	33.3	50.0
WPI-Oligo-Hylon	B	No	Yes	4.8	9.6	4.2	8.3	12.5	16.7	16.7	50.0
HWP-Oligo-Pectin	A	Yes	No	7.2	14.4	5.9	11.8	17.8	16.7	33.3	50.0
HWP-Oligo-Pectin	B	No	Yes	7.2	14.4	5.9	11.8	17.8	16.7	33.3	50.0
WPI	C	Yes	No	10.0	0	9.1	0	9.1	50.0	0	50.0
SPI-Pectin	D	No	No	9.0	0.5	8.3	0.4	8.7	47.6	2.4	50.0

<sup>a</sup>Hylon = Hylon where pre-processing involved homogenisation of a heated aqueous dispersion of the starch prior its use as an encapsulant

<sup>b</sup>CHO = carbohydrate



**Table 2** Analyses of microencapsulated oil powders before and after sequential exposure to SGF and SIF<sup>a</sup>

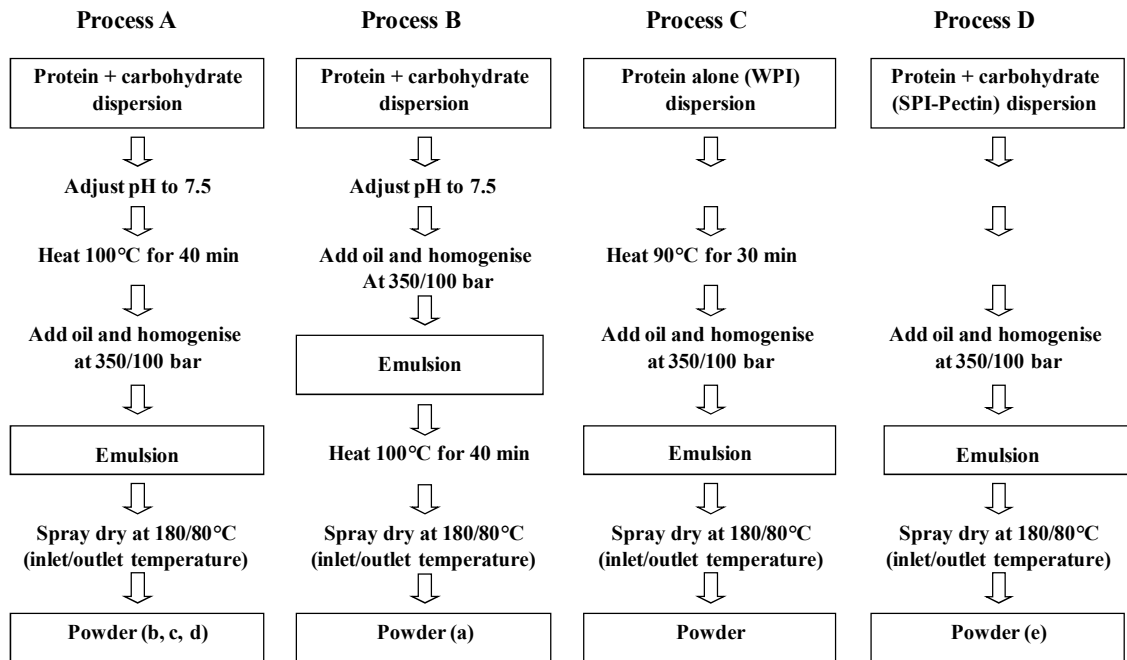
Aqueous phase components <sup>b</sup>	ID	ID	Neat Powder (Before SGF-SIF)		Oil extractable (After SGF-SIF)		Extent of Lipolysis (After SGF-SIF)	
	Process	Clinical study sample	Total oil <sup>c</sup> (g/100g solids)	'Free oil' (g/100g solids)	Oil extracted (Measured) (g/100 g solids)	Oil recovered (Calculated) (% of total oil)	Lipolysis (Measured) (% in extracted oil)	Lipolysis (Calculated) <sup>d</sup> (% of total oil)
NaCas-Hylon	B	a	46.4±0.1	21.3±0.3	24.4±1.0	52.6	23.0±0.5	12.1±0.2
NaCas-Hylon	A	b	49.1±0.2	21.6±0.7	44.4±0.1	90.4	59.0±0.2	53.4±0.2
NaCas-Oligo-Hylon	A	-	51.4±0.3	13.4±0.1	52.4±1.1	101.9	61.0±0.3	62.2±0.3
NaCas-Oligo-DGS	A	c	50.3±0.5	0.5±0.0	57.6±0.7	114.5	59.0±0.2	67.6±0.2
WPI-Hylon	A	d	51.4±0.1	24.5±0.1	52.4±1.2	101.9	63.0±1.2	64.2±1.2
WPI-Hylon	B	-	47.2±0.2	14.2±0.3	44.9±0.4	95.1	59.0±0.8	56.1±0.7
WPI-Oligo-Hylon	A	-	52.6±0.5	25.2±0.1	56.9±0.8	108.2	60.0±1.1	64.9±1.1
WPI-Oligo-Hylon	B	-	53.9±0.2	14.5±0.3	43.5±0.6	80.7	56.0±0.5	45.2±0.4
HWP-Oligo-Pectin	A	-	51.3±0.5	0.6±0.0	51.2±0.2	99.8	63.0±0.1	62.9±0.1
HWP-Oligo-Pectin	B	-	52.9±0.1	0.7±0.0	28.8±0.8	54.4	23.0±0.3	12.5±0.2
WPI	C	-	52.9±0.3	19.4±0.3	50.9±1.4	96.2	56.0±0.8	53.9±0.8
SPI-Pectin	D	e	53.6±0.5	24.1±0.5	53.2±0.4	99.3	55.0±0.4	54.6±0.4

<sup>a</sup> Data is the mean±s.d. where oil extractions were carried out in duplicate and each oil extract was analysed by GC for fatty acids.

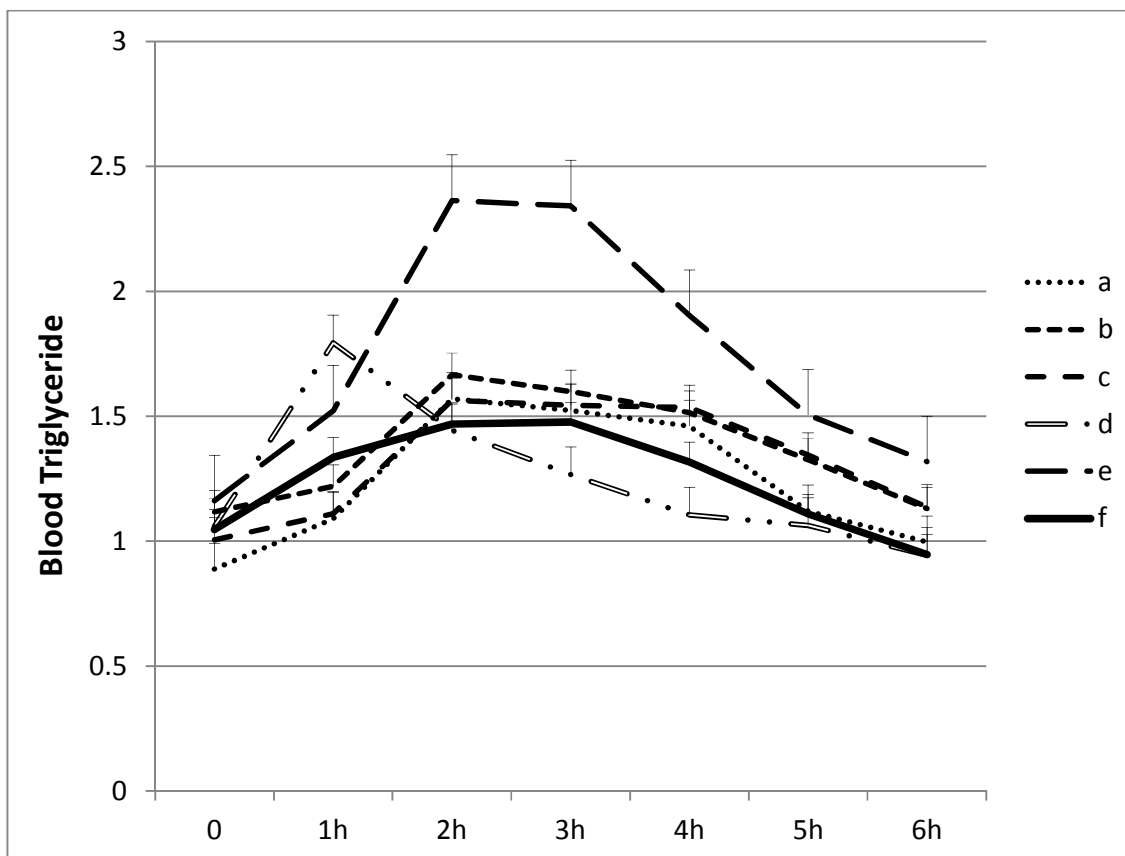
<sup>b</sup>Hylon = Pre-processed Hylon where pre-processing involved homogenisation of a heated aqueous dispersion of the starch.

<sup>c</sup>Total oil, Free oil, and oil extractable after SGF-SIF are calculated as % powder dry basis.

<sup>d</sup>The calculated extent of lipolysis assumes the amount of oil that is not recoverable after SGF-SIF is undigested oil in triglyceride form.



**Fig 1** Process flow diagram for the manufacture of microencapsulated oil powders



**Fig 2** Average blood triglyceride values for 6 normotriglyceridemic subjects (3 Male, 3 Female) over 6 h after consumption of beverage. (a) Cas-Hylon Process B; (b) Cas-Hylon Process A; (c) Cas-oligo-DGS Process A; (d) WPI-Hylon Process A; (e) SPI-pectin Process D; (f) canola oil. Processes used are given in Fig 1. By repeated measures and using ANOVA, sample (e) is significantly different from all others ( $p < 0.05$ ). Sample (c) was significantly different from (d), (e) and (f) ( $p < 0.05$ ).