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## COMMUNICATION

Microwave selective effect: a new approach towards oxygen inhibition removal for highly-effective NO decomposition by microwave catalysis over  $BaMn_xMg_{1-x}O_3$  mixed oxides at low temperature under excess oxygen

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A significant microwave selective effect to oxygen inhibition removal was found for NO decomposition through microwave catalysis over  $BaMn_xMg_{1-x}O_3$  catalysts. Especially, the NO

<sup>10</sup> conversion and N<sub>2</sub> selectivity were respectively up to 99.8% and 99.9% for  $BaMn_{0.9}Mg_{0.1}O_3$  catalyst even at coexistence of 10% oxygen and low temperature of 250 °C.

Nitrogen oxides (NO<sub>x</sub>), emitted from various of stationary and mobile sources, are recognized to be one of the most dangerous <sup>15</sup> atmospheric pollutants.<sup>1</sup> It has been developed several practical

- NO<sub>x</sub> emission control technologies, including three-way catalysts, NO<sub>x</sub> storage-reduction catalysts, and selective catalytic reduction (SCR) processes.<sup>2</sup> Among the various deNO<sub>x</sub> strategies, the direct decomposition of NO into N<sub>2</sub> and O<sub>2</sub> (2NO $\rightarrow$ N<sub>2</sub>+O<sub>2</sub>) is the most
- <sup>20</sup> desirable one with respect to both environmental and economic considerations, because it does not involve the addition of toxic reducing agent and the products are nontoxic.<sup>3,4</sup> Several catalysts, such as the noble metals,<sup>5-7</sup> oxides,<sup>8-12</sup> and metal ion-exchanged zeolites,<sup>13-15</sup> have been extensively investigated for the direct
- <sup>25</sup> decomposition of NO in the conventional reaction mode (CRM). Among these catalysts, perovskites are considered to be the most promising catalysts for the direct decomposition of NO in view that they are low-cost materials and sustainable for the long-term operation.<sup>2,3,9,16</sup> However, the NO decomposition over perovskites
- <sup>30</sup> is strongly inhibited by the coexistence of oxygen in the gaseous mixtures and also the produced O<sub>2</sub>, leading to the NO conversion drastically decrease.<sup>2,3,9,16-19</sup>. Iwakuni *et al.*<sup>18</sup> studied the catalytic performance of BaM nO<sub>3</sub>-based perovskites for the decomposition of NO, and N<sub>2</sub> yield over Ba<sub>0.8</sub>La<sub>0.2</sub>M n<sub>0.8</sub>M g<sub>0.2</sub>O<sub>3</sub> decreased from <sup>35</sup> 75% to 40% by the coexistence of 5% oxygen at 850 °C.

To avoid oxygen inhibition effect by the adsorbed oxygen over perovskites, two methods have been reported until to date. The one is that noble metal-doped perovskites  $(Ag/La_{0.6}Ce_{0.4}CoO_3)$ showed some degree of activity in the narrow temperature range

- <sup>40</sup> and the presence of oxygen.<sup>20</sup> The other one is that the group of Caro<sup>3,21</sup> reported the decomposition of NO and N<sub>2</sub>O over a novel perovskite (BaCo<sub>x</sub>Fe<sub>y</sub>Zr1-x-yO<sub>3, $\delta$ </sub>) hollow fiber membrane reactor, and the complete NO conversion with around 95% N<sub>2</sub> yield was achieved at 875 °C, which was considered to be a breakthrough in
- <sup>45</sup> this field. However, an additional reducing agent (such as CH<sub>4</sub>) must be adopted to remove the surface oxygen in this membrane reactor. Therefore, it is still great challenge to develop novel and efficient strategies for the highly-effective direct decomposition

of NO in the presence of excess oxy gen.

- <sup>50</sup> Of late, the microwave-accelerated heterogeneous catalytic reactions have attracted tremendous attentions by providing dramatic enhancement of reaction rate under mild conditions.<sup>22,23</sup> Furthermore, microwave irradiation has been well demonstrated to enhance reaction selectivity that differing from conventional
- <sup>55</sup> methods<sup>22-26</sup>. Although using microwave irradiation to accelerate chemical reactions is rapidly growing, it is still not elucidated for the nature of microwave irradiation on chemical reactions. Moreover, there is no literature report on the direct decomposition of NO by microwave catalysis over mixed oxides, in particular <sup>60</sup> the perovskites. Therefore, we attempt to investigate the catalytic performance of perovskites for the microwave direct catalytic decomposition of NO in this work.

Our previous work studied the microwave selective catalytic reduction of NO over  $Mn_2O_3/AC$  with 98.7% NO conversion and

- <sup>65</sup> 99.8% N<sub>2</sub> selectivity at the environment of excess oxygen and temperature as low as 300 °C.<sup>27</sup> Herein, we report the highlyeffective direct NO decomposition by microwave catalysis over  $BaMn_xMg_{1-x}O_3$  mixed oxides at low temperature under excess oxygen. We found a significant microwave selective effect for the 70 oxygen inhibition removal during the direct decomposition of NO. A complete NO decomposition with the NO conversion and N<sub>2</sub>
- selectivity respectively up to 99.8% and 99.9% was achieved over the BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> catalyst at temperature as low as 250 °C under excess oxygen in the microwave catalytic reaction mode 75 (MCRM). To the best of our knowledge, this is the first report on the direct decomposition of NO with such hick efficiency through
- the direct decomposition of NO with such high efficiency through microwave catalysis at low temperature under excess oxygen. Our work attempts to build a new approach to oxygen inhibition removal for the direct decomposition of NO.
- Fig. 1 displays the NO conversion as a function of temperature over these BaMn<sub>1-x</sub>Mg<sub>x</sub>O<sub>3</sub> catalysts in the MCRM. Surprisingly, even at 100 °C (an extremely low temperature for the direct decomposition of NO), the NO conversion can reach 49.7% for BaMnO<sub>3</sub>, 52.1% for BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub>, 52.7% for BaMn<sub>0.8</sub>Mg<sub>0.2</sub>O<sub>3</sub>, s5 56.8% for BaMn<sub>0.7</sub>Mg<sub>0.3</sub>O<sub>3</sub>, and 49.8% for BaMn<sub>0.6</sub>Mg<sub>0.4</sub>O<sub>3</sub> in the MCRM. NO conversion over these five catalysts firstly increases and then decreases with an increase of temperature (100-400 °C). Importantly, the best conversion in each reaction is up to 99.5% for BaMnO<sub>3</sub> at 250 °C, 99.8% for BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> at 250 °C, 98.2% for BaMn<sub>0.8</sub>Mg<sub>0.2</sub>O<sub>3</sub> at 300 °C, 99.1% for BaMn<sub>0.7</sub>Mg<sub>0.3</sub>O<sub>3</sub> at 250 °C, which are



Fig. 1 The influence of reaction temperatures on the NO conversion over  $BaMn_{1-x}Mg_xO_3$  catalysts and 5% water vapor over  $BaMn_{0.9}Mg_{0.1}O_3$  in the MCRM (Reaction conditions: molar fraction of O<sub>2</sub>, 5%; molar fraction of 5 NO, 0.1%; W/F = 1 g s cm<sup>3</sup>; and N<sub>2</sub> as the balance)

close to complete NO conversion. Tang *et al.*<sup>28</sup> used Fe/ZSM-5 as a catalyst for NO decomposition in the microwave heating mode, whereas the highest NO conversion was only 70% in their report.

- In fact, industrial off-gases often contain oxygen. To further demonstrate the impressively high activity of  $BaMn_{1-x}Mg_xO_3$  catalysts in the MCRM, the direct decomposition of NO over  $BaMn_{1-x}Mg_xO_3$  were performed under excess oxygen, and the results are presented in Fig. 2. It is surprised that oxygen
- <sup>15</sup> concentrations (0-10%) do not inhibit the catalytic NO decomposition reaction in the MCRM. Moreover, N<sub>2</sub> selectivities are more than 99.9% in the MCRM (Fig. 2b). The dramatically high selectivity indicated that the undesired consecutive reactions for converting NO to N<sub>2</sub>O or NO<sub>2</sub> almost did not take place in the
- <sup>20</sup> MCRM, and all the NO molecules almost directly converted into N<sub>2</sub> and O<sub>2</sub>. Apparently, BaMn<sub>1-x</sub>Mg<sub>x</sub>O<sub>3</sub> catalysts exhibit excellent endurance to excess oxygen in the MCRM. Comparatively, Tang *et al.*<sup>28</sup> studied the direct decomposition of NO over Fe/ZSM-5 catalyst in the microwave heating mode, and they also
- <sup>25</sup> demonstrated good endurance performance to excess oxygen concentration ranging from 2% to 10%. However, the NO conversion will sharply decrease from 55% to 40% as the oxygen concentration gradually increased from 0% to only 2%.<sup>28</sup> On the other hand, Jiang *et al.*<sup>3</sup> reported the decomposition of NO over a
- <sup>30</sup> BaCo<sub>x</sub>Fe<sub>y</sub>Zr1-x-yO<sub>3- $\delta$ </sub> perovskite membrane, and a complete NO conversion was achieved at 875 °C as the oxygen concentrations less than 3%. Unfortunately, NO conversion will decrease to 87% as the oxygen concentration above 5%.<sup>3</sup>

The above results indicated oxygen inhibition removal for the <sup>35</sup> direct decomposition of NO over  $BaMn_{1-x}Mg_xO_3$  catalysts in the MCRM. The results can probably be attributed to the microwave selective effect under microwave irradiation. It is well-known that the microwave electromagnetic field is beneficial to activate polar molecules.<sup>23,29</sup> Therefore, it is speculated that the NO adsorbed on

<sup>40</sup> the surface of catalysts rather than the oxygen in the gas phase, can be activated effectively by the microwave electromagnetic field. The similar explanation was also reported by previous researches from our group<sup>27,30</sup> and others.<sup>31,32</sup> The NO molecules and O<sub>2</sub> molecules can all be physically adsorbed on the active <sup>45</sup> sites. However, only the physical adsorption of NO molecules can



Fig. 2 The influence of oxygen concentrations on the NO conversion (a) and N<sub>2</sub> selectivity (b) over  $BaMn_{1*}Mg_xO_3$  catalysts in the MCRM 50 (Reaction conditions: reaction temperature, 250 °C; molar fraction of NO, 0.1%; W/F = 1 g s cm<sup>-3</sup>; and N<sub>2</sub> as the balance)

become chemical adsorption on the active sites and further convert to N<sub>2</sub> in the MCRM. Meanwhile, the physical adsorption <sup>55</sup> of O<sub>2</sub> molecules is not enough to activate at low temperature under microwave selective effect and then they lose reactivity with NO to generate NO<sub>2</sub>. Therefore, BaM n<sub>1-x</sub>M g<sub>x</sub>O<sub>3</sub> catalyst can still exhibit excellent endurance to excess oxygen in the MCRM. This significant microwave selective effect can provide a new <sup>60</sup> route to address the problem of strong oxygen inhibition in NO decomposition.

The effect of water vapor on NO conversion in the MCRM over BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> was studied (Fig. 1). Although the NO conversation decreases slightly in the presence of water vapor, the <sup>65</sup> BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> catalyst still displays a high catalytic activity after the introduction of water vapor.

A durability test over BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> was performed in the MCRM. As shown in Fig. 3, BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> can still display a high stability in the MCRM. Surprisingly, NO conversion and N<sub>2</sub> ro selectivity are respectively higher than 97.7% and 99.9% in dry conditions and 94.6% and 99.8% under water vapor conditions within 20 h at 300 °C. Furthermore, XRD patterns (Fig. S3c, ESI†) for BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> suggest that the mixed oxide structure of BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> does not differ significantly before and after <sup>75</sup> microwave irradiation. Apparently, BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> catalyst exhibits excellent endurance to water vapor in the MCRM.

We investigated the catalytic activity and microwave heating profile of the BaM  $n_{0.9}Mg_{0.1}O_3$ -1000 sample (calcined at 1000 °C

75

85

100

110



Fig. 3 Time profile of NO conversion and N<sub>2</sub> selectivity over BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> catalyst in the MCRM (Reaction conditions: molar fraction of O<sub>2</sub>, 5%; molar fraction of NO, 0.1%; W/F = 1 g s cm<sup>3</sup>; N<sub>2</sub> as 5 the balance; and reaction temperature, 300 °C)

and possesses perovskite structure, Fig. S3b, ESI<sup>†</sup>). Surprisingly, the BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub>-1000 exhibits very poor microwaveabsorbing ability compared with the BaMn<sub>0.9</sub>Mg<sub>0.1</sub>O<sub>3</sub> (calcined at 10 700 °C) at the microwave power of 150W (Fig. S2, ESI<sup>†</sup>), and

the catalytic performance of  $BaMn_{0.9}Mg_{0.1}O_3$ -1000 is much worse than the  $BaMn_{0.9}Mg_{0.1}O_3$  in the MCRM (Fig. S4, ESI†).

We also studied the catalytic activity of  $BaMn_{0.9}Mg_{0.1}O_3$  under identical conditions in the CRM, and the results are shown in Fig. 25 (TSU).

<sup>15</sup> S5 (ESI<sup>†</sup>). Among the reaction temperature ranges of 450-650 °C, N<sub>2</sub> formation starts at 450 °C and the highest NO conversion and N<sub>2</sub> yield are respectively only 38.5% and 24.1% at 650 °C. However, BaMn<sub>1-x</sub>Mg<sub>x</sub>O<sub>3</sub> catalysts still display good catalytic activity at low temperature in the MCRM (Fig. 1). It is obvious

 $_{20}$  that microwave catalysis remarkably enhances the activity of  $BaMn_{1-x}Mg_xO_3$  for the decomposition of NO.

In addition, we calculated the apparent activation energies (Ea') of  $BaMn_{1-x}Mg_xO_3$  catalysts for the direct decomposition of NO (Table S1, ESI†). Surprisingly, Ea' of  $BaMn_{1-x}Mg_xO_3$  in the

- $_{25}$  MCRM are as low as 11.6-27.8 kJ/mol. Therefore, Ea' in the MCRM are much lower than the corresponding Ea' values of similar BaMn<sub>1-x</sub>Mg<sub>x</sub>O<sub>3</sub> in the CRM, and the direct decomposition of NO in the MCRM can operate at a lower temperature with a dramatically higher conversion than that in the CRM.
- <sup>30</sup> In conclusion, we believe the most significant aspect of this study is that it reports the microwave selective effect: a new approach to oxygen inhibition removal for a difficult (strong oxygen inhibition) and important catalytic decomposition reaction for the direct decomposition of NO under excess oxygen.
- <sup>35</sup> Importantly, the oxygen concentration has surprisingly no effect on the catalytic performance of decomposition of NO over  $BaMn_xMg_{1-x}O_3$  catalysts in the MCRM. A complete NO decomposition with NO conversion and N<sub>2</sub> selectivity respectively up to 99.8% and 99.9% was achieved over the
- $_{40}~BaM\,n_{0.9}M\,g_{0.1}O_3$  catalyst at the environment of excess oxygen and temperature as low as 250  $\,^\circ\!\!C$  in the MCRM.

Although only the catalysts of  $BaMn_{1-x}Mg_xO_3$  and the reaction of direct NO decomposition were used as a case study, we believe that this novel process can be extended to other catalysts and strong owner inhibition reactions, such as direct decomposition

45 strong oxygen inhibition reactions, such as direct decomposition

of NO over noble metals, oxides, and metal ion-exchanged zeolites catalysts, and also the situation for the direct catalytic decomposition of  $N_2O$ .

## Notes and references

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- 1 J. Galloway, A. Townsend, J. Erisman, M. Bekunda, Z. Cai, J. Freney, L. Martinelli, S. Seitzinger and M. Sutton, *Science*, 2008, **320**, 889.
  2 N. Imanaka and T. Masui, *Appl Catal.*, A, 2012, **431**, 1.
  - H. Q. Jiang, L. Xing, O. Czuprat, H. Wang, S. Schirrmeister, T. Schiestel and J. Caro, *Chem. Commun.*, 2009, 44, 6738.
- 65 4 J. Zhu, Y. Wei, W. Chen, Z. Zhao and A. Thomas, *Chem. Commun.*, 2010, 46, 6965.
  - 5 A. Amirnazmi, J. E. Benson and M. Boudart, J. Catal., 1973, 30, 55.
  - 6 J. M. D. Cónsul, C. A. Peralta, E. V. Benvenutti, J. A. C. Ruiz, H. O. Pastore and I. M. Baibich, J. Mol. Catal, A, 2006, 246, 33.
  - 7 M. Haneda, Y. Kintaichi, I. Nakamura, T. Fujitani and H. Hamada, *Chem. Commun.*, 2002, **23**, 2816.
  - 8 E. R. S. Winter, J. Catal., 1971, 22, 158.
  - 9 N. Imanaka, T. Masui and H. Masaki, Adv. Mater. 2007, 19, 3660.
  - 10 J. J. Yu, X. P. Wang, L. D. Li, Z. P. Hao, Z. P. Xu and G. Q. Lu, *Adv. Funct. Mater.*, 2007, **17**, 3598.
  - 11 W. J. Hong, S. Iwamoto, S. Hosokawa, K. Wada, H. Kanai and M. Inoue, J. Catal., 2011, 277, 208.
  - 12 M. Haneda, Y. Kintaichi, N. Bion and H. Hamada, Appl. Catal., B, 2003, 46, 473.
- 80 13 M. Iwamoto, H. Furukawa, Y. Mine, F. Uemura, S. I. Mikuriya and S. Kagawa, J. Chem. Soc. Chem. Commun., 1986, 16, 1272.
  - 14 M. Y. Kustova, S. B. Rasmussen, A. L. Kustov and C. H. Christensen, *Appl. Catal.*, *B*, 2006, **67**, 60.
  - 15 C. Yun, and G. M. Jon, J. Catal., 1998, 178, 408.
  - 16 J. Zhu and A. Thomas, Appl. Catal., B, 2009, 92, 225.
    - 17 C. Tofan, D. Klvana and J. Kirchnerova, *Appl. Catal. A*, 2002, 226, 225.
      18 H. Iwakuni, Y. Shinmyou, H. Yano, H. Matsumoto and T. Ishihara,
  - 18 H. Iwakuni, Y. Shinmyou, H. Yano, H. Matsumoto and T. Ishihara, *Appl. Catal. B*, 2007, **74**, 299.
  - 19 T. Ishihara, M. Ando, K. Sada, K. Takiishi, K. Yamada, H. Nishiguchi and Y. Takita, J. Catal., 2003, 220, 104.
  - 20 Z. Liu, J. Hao, L. Fu and T. Zhu, Appl. Catal. B, 2003, 44, 355.
  - 21 H. Jiang, H. Wang, F. Liang, S. Werth, T. Schiestel and J. Caro, Angew. Chem. Int. Ed., 2009, 48, 2983.
  - 22 X. Zhang and D. Hayward, Inorg. Chim. Acta, 2006, 359, 3421.
  - 23 M. Crosswhite, J. Hunt, T. Southworth, K. Semiak, A. Ferrari and A. E. Stiegman, *ACS Catal*, 2013, **3**, 1318.
  - 24 J.A. Gerbec, D. Magana, A. Washington and G.F. Strouse, J. A. C. S., 2005, **127**, 15791.
  - 25 C. O. Kappe, B. Pieber and D. Dallinger, Angew. Chem. Int. Ed., 2013, 52, 1088.
  - 26 C. O. Kappe, Chem. Soc. Rev., 2008, 37, 1127.
  - 27 W. Xu, J. Zhou, H. Li, P. Yang, Z. You and Y. Luo, *Fuel Process. Technol.*, 2014, **127**, 1.
  - 28 J. Tang, T. Zhang, D. Liang, H. Yang, N. Li and L. Lin, *Appl. Catal.*, *B*, 2002, **36**, 1.
  - 29 W. C. Conner and G A. Tompsett, J. Phys. Chem. B, 2008, 112, 2110.
  - 30 W. Xu, J. Zhou, Z. You, Y. Luo and Y. Ou, *Chem CatChem.*, 2014, doi: 10.1002/cctc.201402852.
  - 31 J. Tang, T. Zhang, D. Liang, C. Xu, X. Sun and L. Lin, *Chem. Commun.*, 2000, **19**, 1861.
  - 32 X. Wang, T. Zhang, C. Xu, X. Sun, D. Liang and L. Lin, *Chem. Commun.*, 2000, **4**, 279.