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## COMMUNICATION

# Improved Low Temperature NH<sub>3</sub>-SCR Performance of FeMnTiO<sub>x</sub> Mixed Oxide with CTAB-assisted Synthesis

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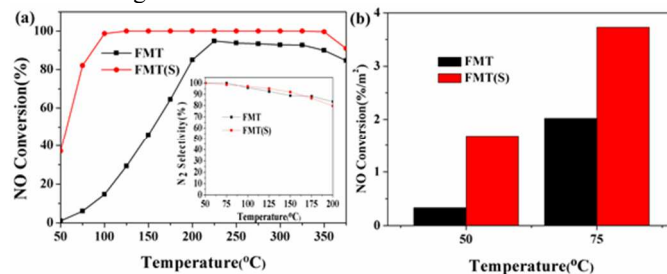
**FeMnTiO<sub>x</sub> mixed oxide is prepared by CTAB-assisted co-precipitation method, and the transformation of anatase to rutile is inhibited by CTAB to some extent. The catalyst obtained in present work shows nearly 100% NO conversion at 100–350 °C, more than 80% N<sub>2</sub> selectivity at 75–200 °C, and excellent H<sub>2</sub>O durability for the selective catalytic reduction of NO by NH<sub>3</sub> with a space velocity of 30000 mL·g<sup>-1</sup>·h<sup>-1</sup>.**

Nitrogen oxides (NO<sub>x</sub>) are one of the major pollutants in atmospheric environment, which can lead to photochemical smog, acid rain, ozone depletion and greenhouse effect, *etc.*<sup>1</sup>. Mitigation of NO<sub>x</sub> from the stationary and mobile sources, such as coal-burning power plants and automotive exhaust emissions, *etc.*, has been one of the key subjects in environmental protection<sup>2</sup>. In recent years, many methods have been used to reduce the emission of NO<sub>x</sub>. Among them, The selective catalytic reduction of NO by NH<sub>3</sub> (NH<sub>3</sub>-SCR) is a very effective technology for denitration (*deNO<sub>x</sub>*) in flue gas from stationary sources. The industrial operations are carried out on V<sub>2</sub>O<sub>5</sub>-WO<sub>3</sub> (MoO<sub>3</sub>)/TiO<sub>2</sub> catalysts during the NH<sub>3</sub>-SCR process<sup>3</sup>. Furthermore, the *deNO<sub>x</sub>* device is placed in the upstream of electrostatic precipitator and desulfurizer, because the high-activity temperature range of the above-mentioned catalysts is 300–400 °C. However, this arrangement causes many disadvantages, such as low N<sub>2</sub> selectivity in the high-temperature range, and deactivation of catalysts caused by sulfur containing compounds and dusts<sup>4</sup>. Therefore, it is of great significance to develop low-temperature (<200 °C) NH<sub>3</sub>-SCR catalysts, so that *deNO<sub>x</sub>* unit can be placed in the downstream of electrostatic precipitator and desulfurizer where SO<sub>2</sub> and dusts have been removed.

Many investigations have been carried out on low-temperature NH<sub>3</sub>-SCR catalysts. Manganese species have been demonstrated to be high NO<sub>x</sub> conversion but low N<sub>2</sub> selectivity, poor H<sub>2</sub>O durability and narrow operating temperature window<sup>3,5,6</sup>. Therefore, many researches have been focused on the modification of the manganese species. For instance, the performance of (Fe<sub>3-x</sub>Mn<sub>x</sub>)<sub>1-a</sub>O<sub>4</sub>, Mn-Ce and Fe<sub>0.5</sub>Mn<sub>0.5</sub>TiO<sub>x</sub> mixed oxide catalysts in selectivity, activity and water resistance are improved respectively<sup>3,7,8</sup>. However, it is still a challenge to develop the low-temperature NH<sub>3</sub>-SCR catalysts which has not only remarkable low-temperature activity, but also wide operating temperature window and excellent water resistance at low temperature. FeMnTiO<sub>x</sub> catalyst is considered to be a potential candidate for industrial application<sup>3</sup>. Anatase is considered to be

more beneficial for NH<sub>3</sub>-SCR than rutile<sup>9</sup>. However, whether supported catalysts prepared by impregnation method or mixed oxide prepared by co-precipitation method of FeMnTiO<sub>x</sub>, the transformation of anatase to rutile will happen, which is not beneficial to improve catalytic activity in low temperature<sup>9</sup>.

Cationic surfactant cetyltrimethyl ammonium bromide (CTAB) can release cations in aqueous solution. FeMnTiO<sub>x</sub> mixed oxide catalyst is synthesised by CTAB-assisted method (denoted as FMT(S)) in the present work. For comparison, FeMnTiO<sub>x</sub> mixed oxide catalyst is also synthesized without CTAB (denoted as FMT). The detail of preparation process is described in the supporting information. The NH<sub>3</sub>-SCR activity and selectivity measurements over FMT and FMT(S) were performed in a fixed-bed quartz reactor, and the results are shown in Fig. 1.



**Fig. 1.** (a) NO conversion and N<sub>2</sub> selectivity (inserted) of FMT and FMT(S) in NH<sub>3</sub>-SCR reaction. (b) NO conversion per unit area of FMT and FMT(S) in NH<sub>3</sub>-SCR reaction at 50 °C and 75 °C.

Fig. 1 shows that NO conversion is about 82% at 75 °C, and reaches almost 100% in the range of 100–350 °C on FMT(S). While the NO conversion is only about 6% at 75 °C, and about 93% in the range of 225–350 °C on FMT. In other words, the activity of FMT(S) is much better than that of FMT in low temperature range (below 200 °C). Furthermore, the N<sub>2</sub> selectivity of the two catalysts is almost the same and above 80% from 75 to 200 °C. Apparently, the addition of CTAB is beneficial to improve the low-temperature catalytic activity of FMT(S), and in order to clarify the effect of CTAB-assisted in preparation process, the physicochemical properties of these catalysts are further characterized.

The XRD patterns in Fig. 2 show that the mixed crystal configurations of anatase and rutile were detected on FMT(S), and only diffraction lines attribute to rutile were detected on FMT. There are no other diffraction lines attribute to iron or manganese species were detected on both samples. Moreover, it can be seen that the rutile diffraction peaks of the two samples are slightly shifted to high angle direction when comparing with pure rutile (inserted in Fig. 2), which suggests that the metal cations with smaller radii replace  $\text{Ti}^{4+}$  in the rutile crystal lattice. It is well known that the ionic radius of  $\text{Mn}^{4+}$  (0.53 Å) is smaller than that of  $\text{Ti}^{4+}$  (0.605 Å), while the ionic radii of  $\text{Mn}^{3+}$  (0.645 Å),  $\text{Mn}^{2+}$  (0.67 Å),  $\text{Fe}^{3+}$  (0.645 Å) and  $\text{Fe}^{2+}$  (0.78 Å) are larger than that of  $\text{Ti}^{4+}$ . It indicates that some of  $\text{Ti}^{4+}$  ions have been replaced by  $\text{Mn}^{4+}$  in the lattice of rutile.

Comparing with pure anatase (inserted in Fig. 2), the anatase diffraction peaks of FMT(S) are not shifted, which suggests that no foreign cations are incorporated into the lattice of anatase. In addition, comparing with FMT, the proportion of rutile is so small on FMT(S) that less  $\text{Mn}^{4+}$  ions are introduced into the lattice of FMT(S). It is reported that tetravalent manganese species has good low-temperature activity in  $\text{NH}_3$ -SCR reaction<sup>10</sup>, thus more of that exposed on the surface of the catalyst, which will be beneficial to  $\text{NH}_3$ -SCR reaction.

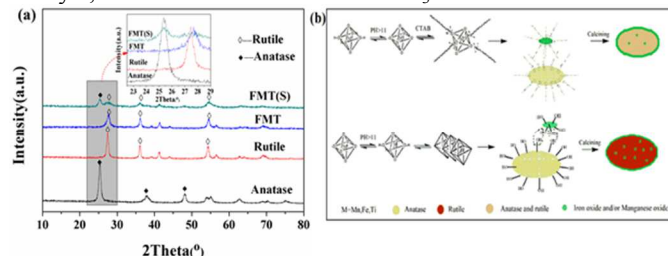


Fig. 2. (a) The XRD patterns of  $\text{TiO}_2$  (anatase and rutile) and mixed oxide catalysts (FMT and FMT(S)), (b) Schematic diagram of preparation process of FMT and FMT(S).

According to XRD results, iron and manganese species can induce anatase into rutile in the process of preparing FMT, which is consistent with many literatures<sup>9</sup>. However, the transformation of anatase to rutile can be restrained by CTAB in the present work. The possible mechanism is as follows: the isoelectric point of  $\text{TiO}_2$ ,  $\text{Fe}_2\text{O}_3$  and  $\text{MnO}_2$  are 3.9-8.2, 6.5-6.8 and 4-5, respectively, and the mixed oxides of them exhibit isoelectric point value among the corresponding pure oxides<sup>11</sup>; hence all metal oxides species are negative charged in condition of  $\text{pH}=11$ ; the cationic surfactant molecules provide  $\text{CTA}^+$  which combines with negative charged sites on metal oxide surface through electrostatic interaction, as shown in schematic diagram (Fig. 2);  $\text{MnO}_2$  is rutile crystal structure, and melting point of it is 535 °C that is far less than that of  $\text{TiO}_2$  (1830 °C), which is considered to promote the crystalline transition because of inducement effect<sup>12</sup>. While due to steric hindrance of the long chain alkane ends and no hydroxyl condensation, CTAB prevents the occurrence of this process to some extent. As we all know, this transformation of anatase to rutile will lead to a sharp decline of area.  $\text{N}_2$ -physisorption characterization is employed to determine specific surface area, and the results demonstrate that FMT(S) maintains large area (Table S1). Thus, the specific surface area may be one of the factors which leads to such a significant difference in reactivity. However, NO conversion per unit area of FMT(S) is still higher

than that of FMT, the corresponding results are presented in Fig. 1(b). This indicates that there are some other factors to affect the activity of catalysts in addition to specific surface area.

As we all known, redox property is an important factor to influence  $\text{NH}_3$ -SCR reaction, and TPR results are shown in Fig. 3(a). The profile of FMT(S) exhibits two main reduction peaks at around 346 °C and 438 °C, and the peaks of FMT are about 410 °C and 508 °C. On one hand, starting reduction peak temperature of FMT(S) is much lower than that of FMT, which suggests that the redox property of FMT(S) is stronger than that of FMT. The reason may be that the interaction between active components and anatase is stronger than that between active components and rutile<sup>13</sup>. On the other hand, peaks area of FMT(S) is larger than that of FMT, which may be related to two factors: firstly, FMT(S) possess more surface reducible species of  $\text{Mn}^{4+}$  ions, which has been demonstrated by XRD; secondly, there are more surface adsorbed oxygen species on FMT(S) (Fig. S4 (b)). In order to further verify this results, the activities of FMT(S) and FMT for NO oxidation are also measured in present work, and the results are shown in Fig. 3(b), and the NO conversion of FMT(S) is higher than that of FMT. Koebel *et al.* demonstrated that the partial conversion of NO into  $\text{NO}_2$  is helpful to “fast SCR”<sup>14</sup>. Therefore, it is reasonable that FMT(S) exhibits excellent reaction activity than FMT at low temperature in present work.

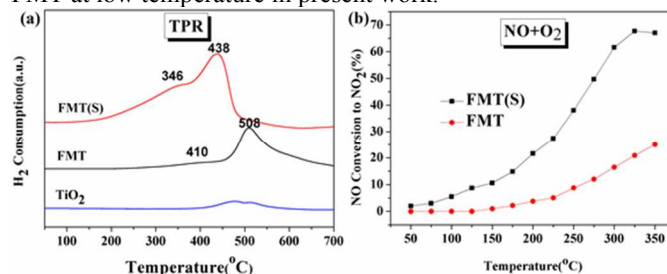


Fig. 3. (a)  $\text{H}_2$ -TPR profiles of FMT and FMT(S). (b) Oxidation activity of NO to  $\text{NO}_2$  by  $\text{O}_2$  on FMT and FMT(S).

Surface acid properties of catalysts plays an important role in  $\text{NH}_3$ -SCR reaction<sup>15</sup>. *In situ* diffuse reflectance infrared Fourier transform spectra (*In situ* DRIFTS) of  $\text{NH}_3$  adsorption are performed at various temperatures to determine the type and quantity of acid sites, and the corresponding results are exhibited in Fig. 4. It is widely reported that the bands at about 1600  $\text{cm}^{-1}$  and 1170  $\text{cm}^{-1}$  are attributed to Lewis acid sites, and the bands at 1460  $\text{cm}^{-1}$  and 1680  $\text{cm}^{-1}$  are attributed to Brønsted acid sites<sup>16</sup>. The results show that FMT(S) has more Lewis acid sites and less Brønsted acid sites, while FMT is in opposite, which might be related to the more  $\text{CTA}^+$  on FMT(S) and the more hydroxyl on FMT in the process of preparation. In addition, TPD results (Fig. S2) show that the quantity of Lewis acid sites of FMT(S) is far more than that of FMT. It is reported that  $\text{NH}_3$  preferentially adsorbed on manganese species for  $\text{MnO}_x/\text{TiO}_2$  catalyst<sup>17</sup>, therefore, more surface manganese species lead to the more Lewis acid sites, which is agreement with BET and XRD results. In order to investigate the effect of Lewis acid sites on  $\text{NH}_3$ -SCR reaction at low temperature, The reaction of *in situ* DRIFTS between NO and pre-saturated  $\text{NH}_3+\text{O}_2$  is conducted on FMT(S), and the results are exhibited in Fig. S3 (a). After the introduction of NO for 3 min, Lewis acid sites disappeared, which implies that the coordinate  $\text{NH}_3$  on Lewis acid sites is very important to activity of  $\text{NH}_3$ -SCR reaction at low temperature, coincidentally, many literatures have also reported similar results<sup>9,18</sup>. For  $\text{NH}_3$  and



O<sub>2</sub> co-adsorption, compared with only NH<sub>3</sub> adsorption in Fig. 4(a), the amount of Lewis acid increased obviously, which may be related to the oxidative abstraction of hydrogen from adsorbed ammonia<sup>19</sup>.

Nitrites are able to react with -NH<sub>2</sub> at temperature below 200 °C, and the reaction rate is very quick<sup>20</sup>, which indicates that nitrite species play an important role in NH<sub>3</sub>-SCR reaction at low-temperature. Thus, *in situ* DRIFTS of NH<sub>3</sub> adsorption are carried out on FMT(S) and FMT pre-saturated with NO+O<sub>2</sub>, the results are respectively shown in Fig. S3 (b) and Fig. S3(c). The bands at 1235 cm<sup>-1</sup>, 1550 cm<sup>-1</sup>, and 1610 cm<sup>-1</sup> are attributed to nitrite, and 1276 cm<sup>-1</sup>, 1543 cm<sup>-1</sup> and 1581 cm<sup>-1</sup> are attributed to nitrate<sup>3,7</sup>. The peak intensity of nitrite on FMT(S) is stronger than that on FMT, and nitrite disappeared quickly and part of nitrate species still existed when NH<sub>3</sub> was introduced into sample cell. It may be concerned that ammonium nitrite decomposes quickly into N<sub>2</sub> and H<sub>2</sub>O below 100 °C<sup>21</sup>, hence, the results demonstrate that nitrite species are more easily formed on FMT(S) than on FMT.

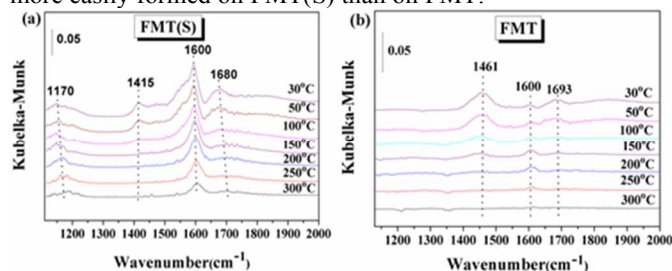


Fig. 4. *In situ* DRIFTS of NH<sub>3</sub> adsorption on catalysts: (a) FMT(S), (b) FMT.

X-ray photoelectron spectra (XPS) of Ti 2p and O 1s for the two catalysts are collected (Fig. S4), the value of Ti 2p<sub>3/2</sub> XPS peak at 457.9 eV on FMT(S) is lower than 458.0 eV on FMT. Literature suggests that the shift of peaks toward lower binding energy is due to the stronger interaction of titanium with manganese<sup>22</sup>. Hence the interaction on FMT(S) is stronger than that on FMT, which is consistent with conclusion of TPR. The O 1s spectra after deconvolution are shown in Fig. S4 (b). The sub-bands at 529.3-529.5 eV correspond to the lattice oxygen O<sup>2-</sup> (denoted as O<sub>α</sub>), and the sub-bands at 531.4 eV correspond to the surface adsorbed oxygen (denoted as O<sub>β</sub>), such as O<sub>2</sub><sup>-</sup>, O<sub>2</sub><sup>2-</sup>, O<sup>-</sup> belonging to defect-oxide<sup>23</sup>. Generally, O<sub>β</sub> is more reactive in oxidation reactions due to its higher mobility than O<sub>α</sub><sup>24</sup>. The ratios of O<sub>β</sub>/(O<sub>α</sub>+O<sub>β</sub>) on the two samples are calculated and listed in Table S3, and the ratio is 38.4% on FMT(S) which is larger than that 28.8% on FMT. Combining with TPR results, it indicates that the FMT(S) is easier to adsorb oxygen than FMT. Kapteijn *et al.* pointed out that NO easily adsorbed on the active center which was oxidized by O<sub>2</sub><sup>25</sup>. Therefore, it is beneficial to further adsorption of NO and formation of nitrite and nitrate on FMT(S), which may be related to the crystal structure of anatase and rutile in TiO<sub>6</sub> octahedron. In rutile, the octahedron shows a slight orthorhombic distortion; in anatase, the octahedron is significantly distorted and its symmetry is lower than rutile<sup>26</sup>. Accordingly, anatase is easier to produce defects and dislocations, and easier to interact with manganese or iron species. Hence, it is helpful to adsorb oxygen and form nitrite on the surface of catalysts.

Since the flue gas still contain steam after electrostatic precipitation and desulfurization under practical condition, we further investigated the effect of H<sub>2</sub>O on performance over the FMT(S). The process and results are shown in Fig. S5, and FMT(S) still exhibits excellent activity and selectivity when the water is introduced in NH<sub>3</sub>-SCR reaction at low temperature.

In summary, CTAB can suppress the transformation of anatase to rutile during the preparation of FMT(S). According to BET specific surface area, XRD, TPR, *in situ* DRIFTS and XPS results, due to the presence of anatase, FMT(S) exhibits greater specific surface area, stronger redox property, more Lewis acid sites and more nitrite species. All of them greatly enhanced the activity of NH<sub>3</sub>-SCR reaction at low temperature, and further research need to be done on the mechanism of CTAB action during the preparation of FMT(S).

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## Notes and references

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