ChemComm

Accepted Manuscript



This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. We will replace this Accepted Manuscript with the edited and formatted Advance Article as soon as it is available.

You can find more information about *Accepted Manuscripts* in the **Information for Authors**.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard <u>Terms & Conditions</u> and the <u>Ethical guidelines</u> still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.



www.rsc.org/chemcomm

ChemComm

Journal Name

COMMUNICATION

Cite this: DOI: 10.1039/x0xx00000x

One-step synthesis of bismuth molybdate catalysts via flame spray pyrolysis for the selective oxidation of propylene to acrolein

K. Schuh,^a W. Kleist,^{a,b} M. Høj,^c V. Trouillet,^d A. D. Jensen^c and J.-D. Grunwaldt^{a,b}

Received ooth January 2014, Accepted ooth January 2014

DOI: 10.1039/x0xx00000x

www.rsc.org/

Flame spray pyrolysis (FSP) of Bi(III)- and Mo(VI)-2-ethylhexanoate dissolved in xylene resulted in various nanocrystalline bismuth molybdate phases depending on the Bi/Mo ratio. Besides α -Bi₂Mo₃O₁₂ and γ -Bi₂MoO₆, FSP gave direct access to the metastable β -Bi₂Mo₂O₉ phase with high surface area (19 m²/g). This phase is normally only obtained at high calcination temperatures (> 560 °C) resulting in lower surface areas. The β -phase was stable up to 400 °C and showed superior catalytic performance compared to α - and γ phases in selective oxidation of propylene to acrolein at temperatures relevant for industrial applications (360 °C).

Multicomponent mixed oxides (MMO) based on bismuth and molybdenum with addition of iron and cobalt are industrially used as catalysts for selective oxidation of propylene to acrolein for methionine production ¹ and as intermediate to acrylic acid ². It is generally accepted that bismuth molybdates are located at the catalyst surface providing the key active sites, whereas iron and cobalt molybdates are situated in the bulk.^{3,4} The specific surface area of bulk bismuth molybdates is often rather low $(1 - 4 \text{ m}^2/\text{g})$. ⁵⁻¹⁰ Addition of other transition metals increases the specific surface area but the surface related activity of these MMOs is only higher in the presence of iron. ¹¹ In order to improve the overall reaction rate it would be beneficial to increase the surface area of bulk bismuth molybdates and compare the catalytic performance of the different crystalline phases, i.e. α - $Bi_2Mo_3O_{12}$, β - $Bi_2Mo_2O_9$ and γ - Bi_2MoO_6 . Beale and Sankar prepared bismuth molybdates by hydrothermal synthesis at different pH values resulting in surface areas of $8 - 10 \text{ m}^2/\text{g}$ for the asprepared materials. Calcination at 400 °C did not decrease the surface area significantly, whereas calcination at 560 °C resulted in extensive sintering. Le et al. used spray drying ^{7, 13} and complexation 13 for the preparation of α -, β - and γ -bismuth molybdate. Addition of citric acid during spray drying increased the surface area to a maximum of 12 m^2/g for α -Bi₂Mo₃O₁₂ and supplementary variation of the pH value resulted in a surface area up to 17 m²/g for γ -Bi₂MoO₆. This increase in surface area also improved the rate of

acrolein formation. Nell et al. 14 applied a templating approach for the synthesis of high surface area bismuth molybdates and bismuth vanadates for selective propylene oxidation. They used mesoporous silica and carbons as templates for the preparation of $\rm Bi_2Mo_3O_{12}.$

The bismuth molybdate phases relevant for selective oxidation of propylene to acrolein are α -Bi₂Mo₃O₁₂, metastable β -Bi₂Mo₂O₉ and γ -Bi₂MoO₆ but despite intensive research, there is still a debate in the literature about the relative activity of these bismuth molybdate phases. As outlined above, a number of preparation methods such as co-precipitation ^{5, 6, 15}, solid state reaction ¹⁶ and spray drying ^{7, 13} have been applied under different preparation conditions. In all cases only higher calcination temperatures led to the formation of β-bismuth molybdate, which is in line with the phase diagram established by Egashira et al. ¹⁷ showing that β -Bi₂Mo₂O₉ only forms above 540 °C. In fact, Beale and Sankar¹² treated their samples at 400 °C to obtain α - and γ -bismuth molybdate, but required 560 °C to produce the β -phase. Le et al. ¹³ calcined the as-prepared materials at 500 °C, 550 °C and 600 °C resulting in α -, γ - and β -bismuth molybdate, respectively. However, the higher calcination temperatures led to a lower surface area, which we also found in a previous study.¹⁸

Hence, a method is required that provides temperatures > 540 °C and at the same time does not result in particle sintering. Potentially, flame spray pyrolysis (FSP) is suited for this purpose. This novel synthesis method uses high preparation temperatures (up to 3000 K)¹⁹ but very short residence time (~1 ms).^{20, 21} We report in this communication that this one-step method allows the preparation of α -, β - and γ -bismuth molybdate under similar synthesis conditions by just varying the initial Bi/Mo ratio. The three materials were then tested in the selective oxidation of propylene to acrolein.

For the flame synthesis, Bi(III)- and Mo(VI)-2-ethylhexanoate were dissolved in xylene to a total metal concentration of 0.15 mol/l at Bi/Mo ratios of 2:1, 1:1 and 2:3 resulting in the corresponding bismuth molybdate phase (γ -Bi₂MoO₆, β -Bi₂Mo₂O₉, α -Bi₂Mo₃O₁₂). The solutions were sprayed using oxygen as dispersion gas and ignited by a methane/oxygen flame with a recently established set-up at KIT based on previous designs by Mädler and Pratsinis ²²⁻²⁴. A detailed description of the preparation is given in the Electronic Supporting Information (ESI †). The obtained bismuth molybdate samples were characterized by powder X-ray diffraction (PXRD), nitrogen physisorption, X-ray absorption spectroscopy (XAS), optical emission spectrometry with inductively coupled plasma (ICP-OES), transmission electron microscopy (TEM) and X-ray photoelectron spectroscopy (XPS); the results are given in Fig. 1 and Table 1 (additional data cf. ESI †).

The diffraction patterns of the samples synthesized with Bi/Mo = 2:1 and Bi/Mo = 1:1 (cf. Fig. 1) show well-defined reflections of high intensity at $2\theta = 28.2^{\circ}$ and 27.8° which is in good agreement with the diffraction patterns of γ -Bi₂MoO₆ and β -Bi₂Mo₂O₉, respectively. The flame made material synthesized with Bi/Mo = 2:3was highly amorphous and only exhibited one small reflection at 20 = 27.9 ° matching the main reflection of α -Bi₂Mo₃O₁₂. The ratio of bismuth to molybdenum in the bulk determined by ICP-OES corresponded to the applied ratio for the sample synthesized with Bi/Mo = 2:1 (see Table 1) indicating that the precursors were completely transformed. For γ -Bi₂MoO₆ synthesized with Bi/Mo = 2:1 an excess of bismuth was detected at the surface by XPS (cf. Table 1). The surface composition of the catalysts was calculated using the peak areas of Mo $3d_{5/2} = 232.7$ eV and Bi $4f_{7/2} = 159.4$ eV in the XPS indicating the presence of Bi³⁺ and Mo⁶⁺. ²⁵ High Bi/Mo surface ratios were also reported in the literature for γ -Bi₂MoO₆ prepared by different methods (spray dried: 2.4⁷, co-precipitated: 2.6⁶). The sample synthesized with Bi/Mo = 1:1 composed of β -Bi₂Mo₂O₉ resulted in a Bi/Mo ratio on the surface of 1.1 which agrees well with the results reported for β -Bi₂Mo₂O₉ by Matsuura et al.⁹ and Soares et al.²⁶.

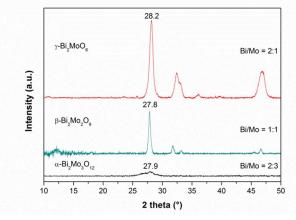


Fig. 1 X-ray diffraction patterns of samples synthesized by flame spray pyrolysis with three different Bi/Mo ratios resulting in three different phases.

Table 1 Phase composition, specific surface area and ratio of bismuth to molybdenum on the surface as well as maximum acrolein yield obtained in catalytic activity measurements.

Applied Bi/Mo	Phase according to	Specific surface area (BET)	Surface Bi/Mo ratio ^a	Max. acrolein yield at 360 °C °
ratio	PXRD	(m²/g)	(at.%/at.%)	(%)
2:1	γ-Bi ₂ MoO ₆	45	2.3 ^b	11.2
1:1	β-Bi ₂ Mo ₂ O ₉	19	1.1	18.8
2:3	α -Bi ₂ Mo ₃ O ₁₂	18	-	3.4

^a Average of two XPS measurements at different spots. ^b Bi/Mo ratio in the bulk determined by ICP-OES equals 1.9. ^c Test conditions: $C_3H_6/O_2/N_2 = 5/25/70$, total flow of 50 Nml/min, 500 mg catalyst.

The samples synthesized with Bi/Mo = 1:1 and Bi/Mo = 2:3 exhibited similar surface areas (19 m²/g and 18 m²/g respectively, cf. Table 1). The sample synthesized with an excess of bismuth (Bi/Mo = 2:1) exhibited the highest surface area (45 m²/g). Whereas the spherical particles of this sample were approximately 25 nm in size

Page 2 of 3

(see TEM images in Fig. S3 a-b, ESI \dagger), the samples with initial Bi/Mo ratio of 1:1 and 2:3 yielded larger particles with smaller spherical particles with a diameter < 10 nm on top (Fig. S3 d-f, ESI \dagger). In line with the objective of the work, the surface areas were higher compared to other unsupported bismuth molybdates previously tested in the selective oxidation of propylene

The β -phase is only considered stable at temperatures between 540 and 665 °C ¹⁷ and, thus, FSP represents a valuable technique to prepare this metastable high-temperature phase with high surface area for catalysis. In a similar way, Kemmler et al. ²⁷ recently used this approach for the synthesis of the high temperature phase In₄Sn₃O₄, which showed excellent performance in sensor applications and long-term stability at the operation conditions.

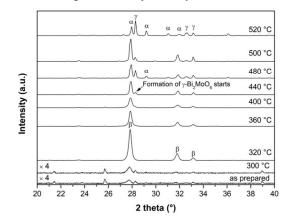


Fig. 2 PXRD analysis of the stability of flame made β -Bi₂Mo₂O₉ after calcination at different temperatures. The formation of γ -Bi₂MoO₆ from β -Bi₂Mo₂O₉ sets in at 440 °C. At 480 °C and 500 °C α -, β - and γ -phase were present, whereas at 520 °C β -Bi₂Mo₂O₉ was below the detection limit.

As the β -phase is a metastable phase, another proof of its existence is the instability below 540 °C. For this purpose, fresh samples were calcined at various temperatures for 4 h and analyzed by PXRD (Fig. 2). The formation of γ -Bi₂MoO₆ set in at 440 °C, as indicated by its characteristic reflection at 28.3° (see also patterns of the phase mixtures in ref. 28). The decomposition into α -Bi₂Mo₃O₁₂ and γ -Bi₂MoO₆ was completed at 520 °C, when no more β -bismuth molybdate could be detected by X-ray diffraction. Consequently, this also proves indirectly the existence of the β -phase. At the same time, the results demonstrate that the β -phase is stable at least during calcination under industrially relevant conditions.³

Hence, these flame-derived bismuth molybdates were applied in the selective oxidation of propylene using three different flows (50, 80 and 120 Nml/min) resulting in three different contact times (details see ESI [†]). In Fig. 3 the activity and selectivity of the different phases are depicted at 360 °C, which is close to the temperature used in industrial applications. Interestingly, β -Bi₂Mo₂O₉ showed the highest propylene conversion (15-28%), whereas α -Bi₂Mo₃O₁₂ exhibited the lowest propylene conversion (2-5%). γ -Bi₂MoO₆, which featured the highest specific surface area (45 m^2/g), did not lead to the highest propylene conversion (9-15%). Acrolein selectivity remained stable around 70-80% with increasing propylene conversion (c.f. Fig. **3**b). The higher surface area of γ -Bi₂MoO₆ did not increase the amount of CO_x. Temperature-dependent catalytic activity measurements showed that the β -phase was also more active at 400 and still at 440 °C (cf. Fig. S4, ESI †), where its decomposition started. The used samples were characterized by PXRD (Fig. S5, ESI [†]) and XAS (Fig. S6, ESI \dagger). Both analysis methods revealed that the β phase decomposed, while the samples synthesized with Bi/Mo = 2:1 $(\gamma$ -Bi₂MoO₆) and 2:3 (α -Bi₂Mo₃O₁₂) did not change phase during the tests at higher temperatures.

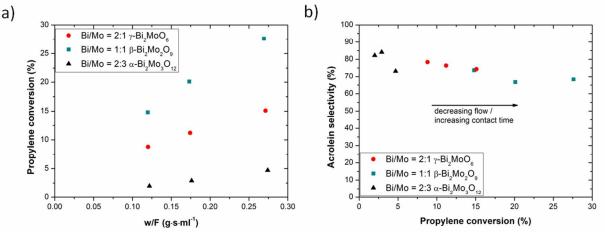


Fig. 3 Performance of the flame made materials in selective oxidation of propylene to acrolein at 360 °C (total flows: 50, 80 and 120 Nml/min; $C_3H_6/O_2/N_2 = 5/25/70$; 500 mg catalyst). a) Propylene conversion as a function of contact time (w/F; at measured reactor temperature and pressure) b) Acrolein selectivity as a function of propylene conversion.

Conclusions

In summary, flame spray pyrolysis gave access to three different bismuth molybdate phases (a-Bi2Mo3O12, β-Bi2Mo2O9 and γ -Bi₂MoO₆) with high surface area by variation of the Bi/Mo ratio. In particular, the method gave direct access to the high temperature metastable phase β -Bi₂Mo₂O₉. The activity of the different bismuth molybdate phases prepared by flame spray pyrolysis decreased in the following order: $\beta > \gamma > \alpha$. In general, this selective one-step synthetic access to the Bi-Mo- O_x system nicely illustrates the great potential of flame spray pyrolysis for catalyst synthesis, in particular if high temperature phases such as the metastable β -Bi₂Mo₂O₉ need to be prepared. This work was funded by the Danish Council of Strategic Research in the framework of the DSF proposal "Nanoparticle synthesis for catalysis". The European Synchrotron Radiation Facility (ESRF) in Grenoble is acknowledged for providing XAS beamtime at the beamline BM01B.

Notes and references

^{*a*} Karlsruhe Institute of Technology (KIT), Institute of Chemical Technology and Polymer Chemistry (ITCP), Engesserstr. 20, 76131 Karlsruhe (Germany). E-Mail: grunwaldt@kit.edu

^b Institute of Catalysis Research and Technology (IKFT), Hermann-von-Helmholtz-Platz 1, Building 725, 76344 Eggenstein-Leopoldshafen (Germany).

^c Technical University of Denmark (DTU), Department of Chemical Engineering & Biochemical Engineering, Søltofts Plads Building 229, DK-2800 Kgs. Lyngby (Denmark).

^d Karlsruhe Institute of Technology (KIT), Institute of Applied Materials (IAM) and Karlsruhe Nano Micro Facility (KNMF), Hermann-von-Helmholtz-Platz 1, 76344 Eggenstein-Leopoldshafen (Germany).

† Electronic Supplementary Information (ESI) available: Materials and methods; supplementary text; Fig. S1 – S6. See DOI: 10.1039/c000000x/

- 1 E. Pierson, M. Giella and M. Tishler, J. Am. Chem. Soc., 1948, 70, 1450.
- 2 Y. Oda, K. Uchida and T. Morimoto, U.S. Patent 3,865,873, 1975.

- 3 Y. Morooka and W. Ueda, Adv. Catal., 1994, 40, 233.
- 4 D. H. He, W. Ueda and Y. Morooka, *Catal. Lett.*, 1992, 12, 35.
 5 D. Carson, G. Coudurier, M. Forissier, J. C. Védrine, A. Laarif and F.
- Theobald, J. Chem. Soc., Faraday Trans. 1, 1983, **79**, 1921.
- 6 Z. Bing, S. Pei, S. Shishan and G. Xiexian, J. Chem. Soc., Faraday Trans. , 1990, 86, 3145.
- 7 M. T. Le, J. Van Craenenbroeck, I. Van Driessche and S. Hoste, *Appl. Catal.*, A, 2003, 249, 355.
- 8 G. I. Aleshina, C. Joshi, D. V. Tarasova, G. N. Kustova and T. A. Nikoro, *React. Kinet. Catal. Lett.*, 1984, 26, 203.
- 9 I. Matsuura, R. Schut and K. Hirakawa, J. Catal., 1980, 63, 152.
- 10 C. Zhao and I. E. Wachs, J. Phys. Chem. C, 2008, 112, 11363.
- 11 W. Ueda, Y. Morooka, T. Ikawa and I. Matsuura, Chem. Lett., 1982, 1365.
- 12 A. M. Beale and G. Sankar, Chem. Mater., 2003, 15, 146.
- 13 M. T. Le, W. J. M. Van Well, I. Van Driessche and S. Hoste, *Appl. Catal.*, A, 2004, 267, 227.
- 14 A. Nell, A. B. Getsoian, S. Werner, L. Kiwi-Minsker and A. T. Bell, Langmuir, 2014, 30, 873.
- 15 L. D. Krenzke and G. W. Keulks, J. Catal., 1980, 64, 295.
- 16 R. P. Rastogi, A. K. Singh and C. S. Shukla, J. Solid State Chem., 1982, 42, 136.
- 17 M. Egashira, K. Matsuo, S. Kagawa and T. Seiyama, J. Catal., 1979, 58, 409.
- 18 K. Schuh, W. Kleist, M. Høj, V. Trouillet, P. Beato, A. D. Jensen, G. R. Patzke and J.-D. Grunwaldt, *Appl. Catal.*, A, 2014, 482, 145.
- 19 A. J. Gröhn, S. E. Pratsinis and K. Wegner, *Chem. Eng. J.*, 2012, 191, 491.
- 20 M. Høj, K. Linde, T. K. Hansen, M. Brorson, A. D. Jensen and J.-D. Grunwaldt, Appl. Catal., A, 2011, 397, 201.
- 21 W. Y. Teoh, R. Amal and L. Mädler, *Nanoscale*, 2010, **2**, 1324.
- 22 H. K. Kammler, L. Mädler and S. E. Pratsinis, *Chem. Eng. Technol.*, 2001. **24**, 583.
- 23 L. Mädler, H. K. Kammler, R. Müller and S. E. Pratsinis, J. Aerosol Sci., 2002, 33, 369.
- 24 W. J. Stark, S. E. Pratsinis and A. Baiker, Chimia, 2002, 56, 485.
- 25 J.-D. Grunwaldt, M. D. Wildberger, T. Mallat and A. Baiker, J. Catal., 1998, 177, 53.
- 26 A. P. V. Soares, L. D. Dimitrov, M. de Oliveira, L. Hilaire, M. F. Portela and R. K. Grasselli, *Appl. Catal.*, A, 2003, 253, 191.
- 27 J. A. Kemmler, S. Pokhrel, J. Birkenstock, M. Schowalter, A. Rosenauer, N. Barsan, U. Weimar and L. M\u00e4dler, Sens. Actuators, B, 2012, 161, 740.
- 28 L.M. Thang, L.H. Bac, I. Van Driessche, S. Hoste, W.J.M. Van Well, Catal. Today, 2008, **131** (2008) 566.