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1 Fast preparation of a hydrophobic monolith by redox initiation and
2 its application in the separation of small molecules

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6 **Abstract:** A novel skeleton hydrophobic polymeric monolith was prepared by redox
7 initiation in this paper. At ambient temperature, benzoyl peroxide (BPO) and N,
8 N-dimethyl aniline (DMA) were used as initiators; 1-Dodecene (C12) as the monomer
9 and ethyleneglycol dimethacrylate as the crosslinking agent. The polymerization
10 conditions were optimized in order to use for chromatographic separations. The
11 characters of the monolith were investigated by scanning electron microscopy (SEM),
12 fourier transform infrared spectroscopy, mercury porosimeter and nitrogen
13 adsorption-desorption mercury porosimetry. Moreover, the prepared monolith was
14 used as the stationary phase of high performance liquid chromatography to separate
15 the mixture of benzenes in hydrophobic chromatography mode. Baseline separations
16 and high column efficiencies in excess of 11,000 theoretical plates per meter were

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17 obtained.

18 Keywords: Hydrophobic monolith; Redox initiation (BPO/DMA); 1-Dodecene (C12);

19 Skeleton structure; High performance liquid chromatography

20 1. Introduction:

21 In recent years, monolithic stationary phase, has attracted increasing attention
22 because of its excellent mass transfer properties and versatile surface modification
23 compared to conventional columns packed with particles [1-2]. Basically, monolithic
24 column are divided into two groups: rigid organic polymer-based monoliths and
25 silica-based monoliths. The two kinds of monoliths have been used in high
26 performance liquid chromatography (HPLC) [3-4], solid phase extraction (SPE) [5-6],
27 and capillary electrophoresis (CE) [7-8]. The drawback of the silica-based monolith is
28 that it is subject to an insufficient hydrolytic of the Si - O - C linkage, especially
29 under moderately acidic or slightly alkaline conditions. Moreover, preparation of
30 silica-based monolithic columns is not only time-consuming but also difficult to
31 control the entire process, which leads to the problems with reproducibility. As an
32 alternate, the organic polymeric monolith shows stability within the entire range of pH
33 and exhibited excellent biocompatibility. However, it suffers from shrinking or
34 swelling under the influence of temperature or organic solvents. Besides, it is difficult
35 to prepare polymeric monoliths possessing both large through pores and multiple
36 small pores in one step [9-12]. An alternative approach is carried out in this paper.

37 Hydrophobic polymeric monolithic column is an important liquid chromatography
38 solid phase for analyzing small molecules. There are many approaches to prepare

39 hydrophobic columns such as single electron transfer-living radical polymerization
40 (SET-LRP) and atom transfer radical polymerization (ATRP) [13-14]. In situ radical
41 polymerization has the disadvantages of slow initiation, fast increase, easy chain
42 transfer and quick chain termination which lead a non-uniform structure [15-17], and
43 resulting in low column efficiency, low permeability and low resolution.

44 The redox initiator which can reduce the activation energy of organic peroxides
45 decomposition, is mostly used in the resin curing process. The reaction can fast occur
46 under contact pressure and ambient temperature condition [18]. The system generally
47 consists of peroxide in combination with reducing agent. The usually used reducing
48 agents are N, N-dimethyl toluidine, N, N-dimethyl aniline (DMA) [19-21] and
49 N-phenyl diethanol amine (PDEA). The benzoyl peroxide (BPO) can initiate the
50 polymerization of vinyl monomers at ambient temperature [22]. The complex
51 decomposes and gives free radicals or cation radicals which can then initiate radical
52 polymerization. This curing process is mostly used in the preparation of unsaturated
53 polyester resin, in which the linear polyester molecules are crosslinked into
54 three-dimensional network structure. This approach has several advantages:
55 effective control of the reaction rate, complete curing reaction, and good mechanical
56 stability of the products. Besides, a proper accelerator can meet various process
57 requirements. Compared to the reported references, the advantages of this method are
58 that not time-consuming preparation and process occurring at room temperature.

59 In this work, a hydrophobic monolith was prepared by one-step redox initiation
60 process. Moreover, the prepared monolith was used as HPLC hydrophobic stationary

61 phase to separate benzenes small molecules successfully.

62 2. Experimental:

63 2.1 Materials and instrumentation

64 1-Dodecene (C12) was purchased from Aladdin Co. Ltd. (Shanghai, China).
65 Ethyleneglycol dimethacrylate (EDMA) was produced by New Jersey (USA). Cetyl
66 alcohol, benzoyl peroxide (BPO), N, N-Dimethylaniline (DMA) and phenol,
67 1-naphthol, biphenyl, anthracene, triphenylamine, benzotriazole, 1-naphthylamine,
68 2,4-dinitrophenylhydrazine, for separated were obtained from Kermel Co. Ltd.
69 (Tianjin, China). Potassium bromide (KBr) was bought from Skylight Optical
70 Instrument Co. Ltd. (Tianjin, China). All of these chemicals and samples were
71 analytical reagent grade. Triple distilled water was used for all experiments.

72 An Agilent Technologies (Agilent, USA) with a 1100 system which was consist of
73 a quaternary pump with an online vacuum degasser, an autosampler with variable
74 injection capacity ranged from 0.1 to 100 μL , and a UV detector; Agilent liquid
75 chromatography system chemical software was used and operated under Windows XP
76 for data acquisition and integration. Microscopic analysis was carried out using a
77 Hitachi (Hitachi High Technologies, Tokyo, Japan) S-4300 SEM instrument. The
78 FT-IR spectra were recorded on an FTIR-8400S IR apparatus in the region of
79 400-4000 cm^{-1} (SHIMADZU, Kyoto, Japan). Pore size distribution was achieved by
80 mercury intrusion porosimetry (AutoPore II 9220 V 3.04, Micromeritics Instrument
81 Co., Atlanta, GA). Nitrogen adsorption-desorption isotherms were measured using
82 specific surface area analyzer (BUILDER, Beijing, China) SSA-4300 instrument.

83 2.2 Preparation of the monolith

84 The monolithic column was prepared with the optimized condition by redox
85 initiator in stainless-steel tubes (50 mm× 4.6 mm i.d.). Functional monomer C12 (0.60
86 mL) and cross linking agent EDMA (0.80 mL) and initiator DMA (0.03 mL) BPO
87 (3.0 mg) were dissolved in 0.2 g melted cetyl alcohol. The mixture was surged
88 ultrasonically and then poured into the stainless steel tube, which was sealed at both
89 ends with close column heads. The mixture was bubbled with nitrogen for 5 min to
90 remove gases. Then the polymerization was allowed to proceed at ambient
91 temperature for less than 10 min. The monolith with the steel-tube was connected to
92 the HPLC system and was washed by methanol online for 2h at a flow rate of 1.0 mL
93 min⁻¹ to remove all of cetyl alcohol and other soluble compounds present from the
94 polymer rod. The polymerization scheme was given in Fig. 1.

95 2.3 Characterization of the monolithic column

96 The monoliths in the columns were pumped out and cut into small pieces followed
97 by drying under vacuum at 60 °C overnight. Chemical groups of the monolith were
98 detected by infrared spectra method, 1-2 mg of the dried monolith and 200 mg of
99 dried KBr were mixed and grinded to less than 2 μm i.d., and then the powder was
100 pressed into transparent sheet by the hydraulic press. Microstructures of the dried
101 monolith samples were observed by scanning electron microscopy (SEM), the pieces
102 of monoliths were snapped apart and placed on sticky copper foils, which were
103 attached to a standard aluminum specimen stub. Then the attached monoliths were
104 coated with about 20 nm of gold by an Eiko IB-3 sputter coating instrument (Eiko,

105 Tokyo, Japan). The pore size distribution was determined by mercury intrusion
106 porosimetry and nitrogen adsorption-desorption isotherm.

107 The permeability of monoliths was assessed by the pressure drop of the monolithic
108 column at different flow rates by using water and methanol as mobile phase,
109 respectively. The values of the system pressure were measured at each flow rate
110 without or with the monolith being connected, and the difference between the two
111 values was calculated as the pressure drop across the monolith. According to the
112 Darcy's law permeability of the monolith was calculated [23].

113 **2.4 HPLC measurements**

114 2.4.1 Selection of the mobile phase

115 In order to select a suitable mobile phase for the separation of the analytes, isocratic
116 elution with methanol and water being used as mobile phase was tested.

117 2.4.2 Chromatographic separation of small molecules

118 Chromatographic separation of small molecules was obtained by a monolithic
119 column (50 mm × 4.6 mm i.d.). The flow rate was 1.0 mL min⁻¹, UV wavelength was
120 set at 254 nm and the temperature was 25 °C. The injection volume of the sample was
121 1.0 µL. All sample solutions injected in the chromatographic system were filtered
122 through a millipore membrane (0.22 µm) to remove particles and large aggregates.
123 Methanol/water (75/25, v/v) was used as mobile phase.

124 **3. Results and discussions**

125 **3.1 Optimization of polymeric conditions**

126 In order to obtain materials with porous and uniform structure, the conditions of the

127 polymerization were optimized. Different compositions of polymerization mixtures
128 were tested. The resulting polymers were qualitatively evaluated for consistency,
129 rigidity and optical aspects. The results were summarized in Table 1.

130 Monomer and cross linking agent both play important roles in the preparation of the
131 monolith. They have significant effects on not only the rigidity and porosity, but also
132 the selectivity and column efficiency of the monolith. Three monolithic columns
133 (column A - C in Table.1) were prepared with different volume of C12 to investigate
134 the influence of C12 amount. Column B, D and E in Table.1 were prepared to
135 investigate the effects of EDMA on the monolith. According to the preliminary
136 experiments listed in Table.1, when the ratio of monomer and cross linking agent was
137 0.6/0.8 (v/v), material with good mechanical property was obtained. SEM was used to
138 investigate the morphology of the monoliths.

139 **3.2 Effect of the porogen on the structure**

140 The choice of pore-forming solvent or porogen is a tool that may be used for the
141 control of porous properties without changing the chemical composition of the final
142 polymer. Fig. 2 showed the effects of the content of cetyl alcohol in the
143 polymerization mixture on pore size distribution. In general, larger pores would be
144 obtained by using more macroporogen because of the earlier onset of phase separation.
145 According to the visualized results, the monolithic column using 0.2 g cetyl alcohol as
146 porogen had well-distributed pore size and submicron skeleton structure which led to
147 high permeability and high efficiency. Based on these results the composition of the
148 polymerization mixture chosen for further experiments was 0.60 mL of C12, 0.80 mL

149 of EDMA, and 0.2 g of cetyl alcohol.

150 The choice of porogens for the preparation of porous polymer monoliths remains an
151 art rather than science. For example, Santora et al. carried out experiments with single
152 solvent porogens including tetrahydrofuran, acetonitrile, toluene, chlorobenzene,
153 hexane, methanol, dimethylformamide, and methyl-t-butyl ether, and prepared series
154 of poly(divinylbenzene), poly(styrene-co-divinylbenzene), poly(ethylene
155 dimethacrylate), and poly(methyl methacrylate-co-ethylene dimethacrylate) monoliths
156 [24]. Although some of these solvents afforded polymers with a surface area as 820
157 $\text{m}^2 \text{g}^{-1}$, it is unlikely that they would be permeable to flow since the pores were rather
158 small [25]. This is why not many porogens have been used and most often proven
159 porogen mixtures are applied. It is generally accepted that good solvents serve as
160 microporogens to provide high surface areas, while poor solvents act like
161 macroporogens to provide good bulk flow properties. For C12-based monoliths, cetyl
162 alcohol is a common solvent, which offered good solubility for C12 and EDTA.

163 Nitrogen adsorption is extensively used for determination of porous properties of
164 monoliths in their dry state. It allows a useful estimate of expected total surface areas
165 of porous polymeric materials and the existence of a permanent mesoporous pore
166 space at least qualitatively [26]. We had been ascertained that monolithic column with
167 no porogen having a surface area of $1.8 \text{ m}^2 \text{ g}^{-1}$ were not suitable for the efficient
168 separation of small molecules. When 0.2 g cetyl alcohol was used as porogen the
169 surface area increased to $279 \text{ m}^2 \text{ g}^{-1}$. Additionally, the nitrogen adsorption-desorption
170 isotherm exhibited typical type-IV hysteresis, indicative of the presence of mesopores

171 Fig. 3.

172 **3.3 Mechanical strength and permeability**

173 In order to characterize the mechanical performance and permeability of the
174 monoliths, the back pressures of the monolith at different flow rates were studied. Fig.
175 4 showed an excellent linear and the regression factors were 0.9997 and 0.9998, that
176 used methanol and water as mobile phase respectively, which indicated that the
177 internal structures of the monoliths were not damaged in the range of back pressure
178 from 13 to 90 bar. This superior flow-through property could be attributed to high
179 cross-linking homogeneity and large pore size. Moreover, the efficiency of
180 chromatographic separation was not affected after subjecting the high flow rates.
181 Besides, in order to evaluate its mass transfer property, the permeability behavior,
182 which is one of the most practical factors in designing a novel type of monolithic
183 column, was investigated. Column permeability (k) reflects through-pore size and
184 external porosity, or a domain size at a constant through-pore size/skeleton size ratio.
185 According to Darcy's law, the equation is as follow:

$$186 \quad Q = \frac{-kA}{\mu} \cdot \frac{P_b - P_a}{L}$$

187 Wherein, the total discharge, Q (units of volume per time, e.g., $\text{m}^3 \text{s}^{-1}$) is equal to the
188 product of the permeability of the medium, k (m^2), the cross-sectional area to flow, A
189 (units of area, e.g., m^2), and the pressure drop, all divided by the viscosity, μ ($\text{Pa}\cdot\text{s}$)
190 and the length over which the pressure drop is taking place [27]. The negative sign is
191 needed because fluid flows from high pressure to low pressure. The good permeability
192 value of $8.97 \times 10^{-14} \text{ m}^2$ was calculated based on the Darcy's law at ambient

193 temperature which supported the internal morphology information of Fig. 2(c). So the
194 skeleton structure not only had good permeability and fast mass transfer, but also had
195 higher surface which could benefit the chromatographic separation. And skeleton
196 structure had higher column efficiency and resolution than accumulated structure.
197 These results indicated that skeleton structure provided larger surface area and
198 excellent permeability.

199 **3.4 FT-IR spectra of the monolith**

200 The FT-IR spectra of the monolith were shown in Fig. 5, in which, typical and
201 expected bands were found. The peak at 3000 cm^{-1} was due to the stretching in C-H of
202 aliphatic or alkenes. The clear absorption peaks at 1510 cm^{-1} and 1100 cm^{-1} were
203 caused by the C-O-C group; The spectrum at 1725 cm^{-1} showed the presence of the
204 -C=O of esters.

205 **3.5 Pore size distribution of the monolith**

206 The measurement of pore size distribution for the monoliths was carried out by
207 mercury intrusion porosimetry. Pore size distribution determines the fraction of the
208 total pore volume accessible to molecules of a given size and shape, which is a very
209 important property of the monolith. The obtained result is depicted in Fig.6. Based on
210 Fig.6, the total intrusion volume, median pore diameter and the porosity were 2.37 mL
211 g^{-1} , $3.5\mu\text{m}$ and 70.5% , respectively.

212 **3.6 Chromatographic separation of small molecules**

213 The poly (C12-co-EDMA) monolith was used as the stationary phase of HPLC to
214 separate small molecules. Fig.7(a, b) showed the chromatograms, and in which two

215 groups of small molecular compounds distinct peaks could be observed. The retention
216 factors (k) of each sample of the first group small molecules on the poly
217 (C12-co-EDMA) monoliths were determined at various concentration of methanol in
218 the mobile phase and the results were shown in Fig.8. The elution capacity is
219 gradually increased with the increase of the amount of methanol, but the column
220 efficiency is not changed significantly which obtained from the calculation of
221 theoretical plate number. This indicates that the hydrophobic interaction between the
222 solutes and the stationary phase plays a dominating role in retaining the solutes on the
223 monoliths. The separations of basic compounds were always suffered from peak
224 tailing in previous reports due to non-specific adsorption on the stationary phases.
225 However, this phenomenon was not observed on the hydrophobic organic monolithic
226 column.

227 Meanwhile, some chromatographic parameters such as retention time and
228 resolution, symmetry factor and theoretical plate number of each sample were
229 calculated and the results were shown in Table 2, in which the theoretical plate
230 number of biphenyl could be up to 10^4 . It could be seen that the poly (C12-co-EDMA)
231 monoliths are excellent stationary phase for separation of these analytes. Furthermore
232 these results strongly suggested further potential of this novel monolith for an
233 efficient downstream processing of benzenes small molecules.

234 **3.7 Advantages compared with other hydrophobic monoliths**

235 Organic polymeric monoliths, generally, are widely used as stationary phases for
236 bio-molecule separation because efficient separation of small molecules is not easily

237 realized in the normal columns (4.6 mm i.d.). However, achieving good column
238 efficiency for small molecules has been easy to obtain for capillary liquid
239 chromatography (cLC) and capillary electrochromatography (CEC). But compared
240 with the normal column in HPLC, both cLC and CEC methods can't achieve high
241 throughput separation.

242 A series of hydrophobic interaction monolithic columns have also been prepared in
243 a similar manner such as single electron transfer-living radical polymerization
244 (SET-LRP) and atom transfer radical polymerization (ATRP). Nevertheless, the
245 preparation processes of these monoliths are rather tedious and time-consuming. We
246 have used a simple one-set approach for preparing the organic polymeric monolith,
247 which represented a new way to prepare the organic polymeric monoliths with variety
248 of organic monomers. In this article the polymerization was allowed to proceed at
249 ambient temperature for less than 10 min. With the excellent hydrophobic of C12,
250 column efficiencies in excess of 11,000 theoretical plates per meter were obtained.
251 However, much less work has been performed with C12 as monomer in the field of
252 monolith.

253 **3.8 The effects of eluent linear flow velocity on the separation**

254 The plate height (H) of the first group small molecular on the poly (C12-co-EDMA)
255 monoliths were determined at various linear flow rate [28]. Fig. 9 shows that the van
256 Deemter plot demonstrating effect of velocity on efficiency of monolithic column for
257 small molecular. Fig.8 and Fig.9 were the average of seven cycle measurement results
258 derived from succedent section 3.8 where the experimental results demonstrate a good

259 repeatability process. Separately, benzene was employed as the mobile phase velocity
260 marker in this experiment according to the cited reference [29].

261 **3.9 Repeatability and stability**

262 A good column-to-column repeatability and monolith stability are important
263 measure of the process. An excellent repeatability characterized by relative standard
264 deviations (RSDs) for the retention times in the range of 1.3-2.6% was achieved on
265 poly (C12-co-EDMA) monoliths using the same process and conditions (n=7).
266 Furthermore, the chromatograms on the poly (C12-co-EDMA) monoliths were
267 obtained after numerous equilibrations and separation runs involving the small
268 molecular mixture. The results demonstrated that the preparation process had a good
269 repeatability and the monoliths were stable.

270 **4. Conclusion**

271 In order to obtain a hydrophobic monolithic column with uniform structure by a
272 simple approach, one-step redox initiation is used in the preparation of monolith in
273 this study. A monolithic structure with hydrophobic surface properties was obtained in
274 this study without post surface modification. The monolith had high performance in
275 the hydrophobic separation of benzenes small molecules which was high to 11,000
276 plates per meter (diphenyl). The results suggested that it's a simple, cheap and
277 effective method to prepare hydrophobic monolith. Hence the novel method presents
278 a promising alternative to commercially available monolithic supports.

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Caption for figures and tables

Fig. 1. Synthesis scheme of the poly (C12-co-EDMA) monolithic column.

Fig. 2. Effects of varying porogen on the morphology of poly (C12-co-EDMA) monolithic columns: (a) no porogen, (b) 0.1 g cetyl alcohol, (c) 0.2 g cetyl alcohol , (d) 0.3 g cetyl alcohol.

Fig.3. Nitrogen adsorption-desorption isotherm.

Fig. 4. Back pressures of the poly (C12-co-EDMA) monoliths at different linear flow rates. Mobile phase: 1 water, 2 methanol.

Fig. 5. The FT-IR spectrum of the poly (C12-co-EDMA) monolith.

Fig.6. The measurement of pore size distribution for the poly (C12-co-EDMA) monolith. Pore size distribution profile measured by mercury intrusion porosimetry.

Fig. 7. Elution profiles of small molecules on the poly (C12-co-EDMA) monoliths. HPLC conditions: the prepared hydrophobic monolith, 50 mm× 4.6 mm i.d.; flow rate 1.0 mL min⁻¹, UV detection at 254 nm .Samples a: the analytes are 1: phenol, 2: 1-naphthol, 3: biphenyl, 4: anthracene, 5: triphenylamine; Samples b: the analytes are 1: benzotriazole, 2:1-naphthylamine, 3: 2,4-dinitrophénylhydrazine, 4: biphenyl; Mobile phase: methanol/water (75/25, v/v), b methanol/water (65/35, v/v).

Fig.8. Relationship between k and methanol concentration on the poly (C12-co-EDMA) monolith. The retention factors (k) was defined as $(t_r - t_0)/t_0$, where t_r and t_0 represent the retention times of an analytes and an unretained compound, respectively.

Fig.9. Plate height curves obtained from separations on a monolithic poly

(C12-co-EDMA) column (1 phenol, 2 1-naphthol, 3 biphenyl, 4 anthracene, 5 triphenylamine). Mobile phase: 75% (v/v) methanol in water. In general the plate heights were fitted to the van Deemter equation $H = A + B/\mu + C\mu$.

Table 1. Qualitative comparison of polymer compositions.

Table 2. Chromatographic parameters of separation of the small molecules.

C12 (mL)	EDMA (mL)	Cetyl alcohol (g)	Permeability ($\times 10^{-14} \text{ m}^2$)	Plate numbers (plates m^{-1})	Resolution	Symmetry factor	Optical properties	Mechanical/ physical properties
A 0.3	0.8	0.2	--	--	--	--	White	Soft, granulous
B 0.6	0.8	0.2	≤ 8.97	≤ 11884	≤ 4.61	≤ 0.90	White	Quite, hard
C 1.0	0.8	0.2	≤ 0.81	≤ 1385	≤ 1.07	≤ 0.52	White	Hard, brittle
D 0.6	0.5	0.2	--	--	--	--	White	Soft, fluffy
E 0.6	1.0	0.2	≤ 1.78	≤ 1874	≤ 1.43	≤ 0.61	White	Hard
F 0.3	0.5	0.2	--	--	--	--	Translucid	Gel like

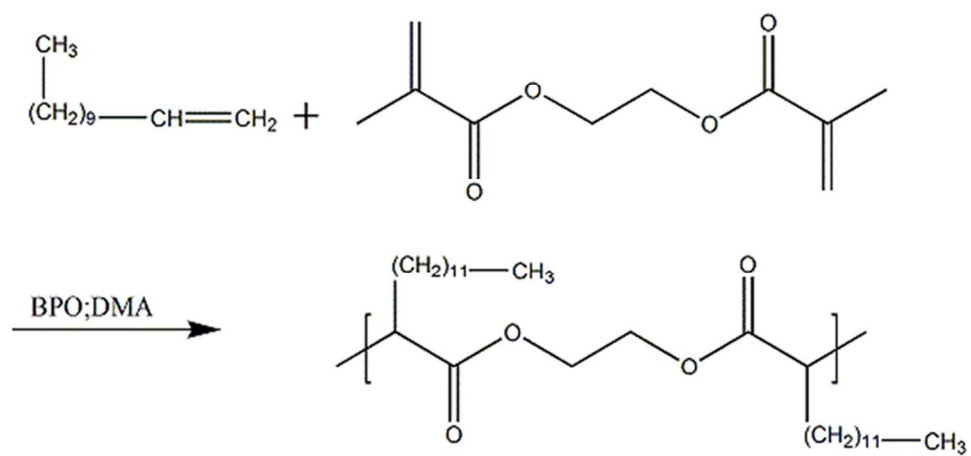
	Retention time (min)	Resolution	Symmetry factor	Plate numbers (plates m ⁻¹)
Phenol	1.170	2.84	0.62	9540
1-Naphthol	2.032	3.37	0.70	8626
Biphenyl	3.735	2.69	0.78	11686
Anthracene	6.058	1.54	0.73	9632
Triphenylamine	8.442	—	0.62	5830

	Retention time (min)	Resolution	Symmetry factor	Plate number (plates m ⁻¹)
Benzotriazole	1.394	4.61	0.67	8943
1-Naphthylamine	3.676	3.19	0.79	8222
2,4-Dinitrophényl hydrazine	6.921	1.92	0.82	8707
Biphenyl	9.742	—	0.90	11884

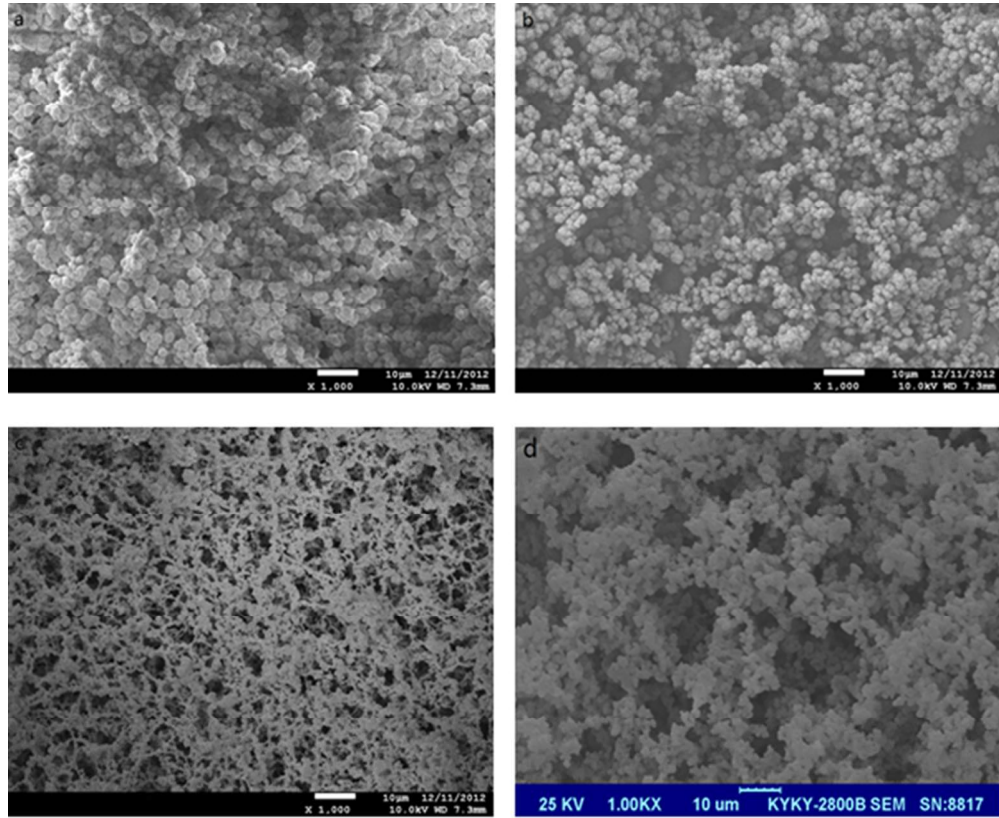
One equation has been used to calculate the plate number:

$$N = \frac{5.55(T_r / W_{0.5})^2}{L}$$

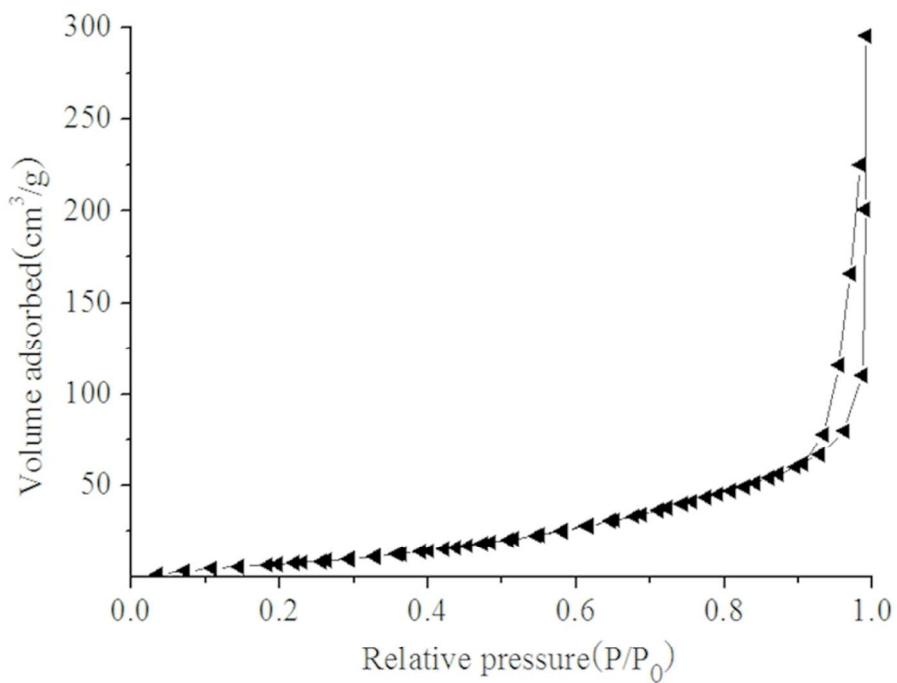
N is the theoretical plate number per m and Tr is the retention time of the analyte in min and W_{0.5} is the peak width at half height in min and L is the length of the column.



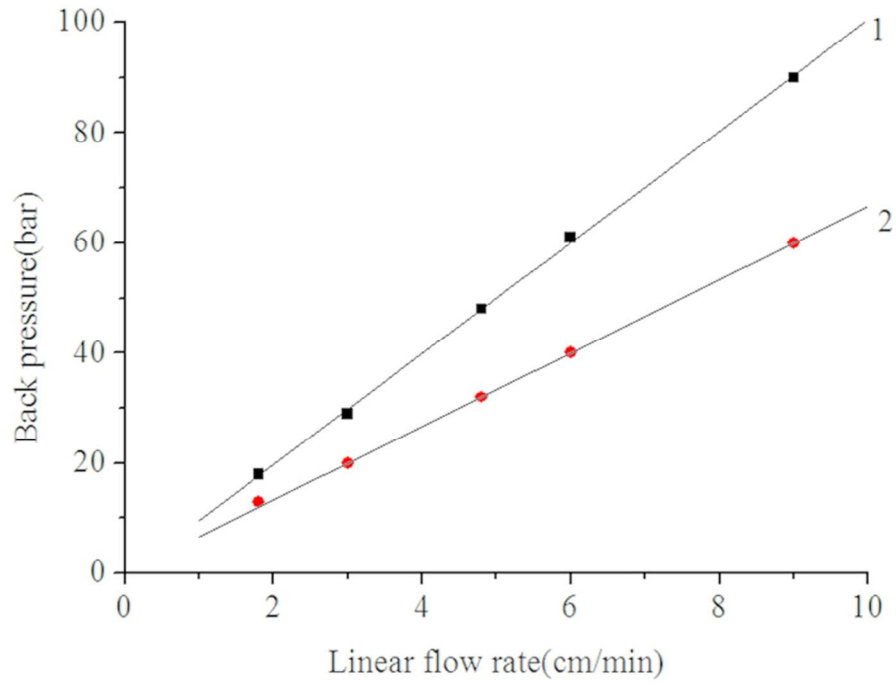
80x45mm (300 x 300 DPI)



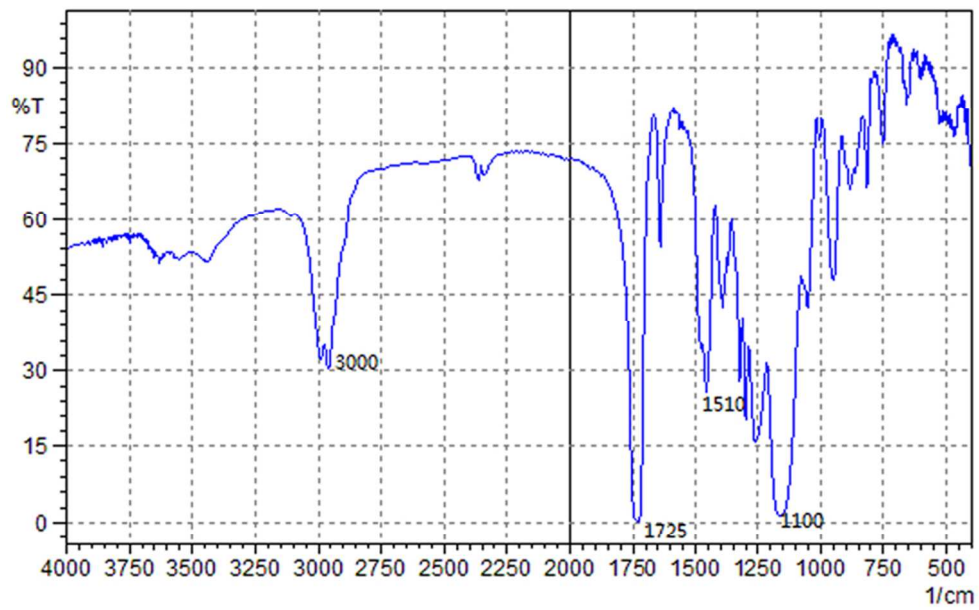
80x65mm (300 x 300 DPI)



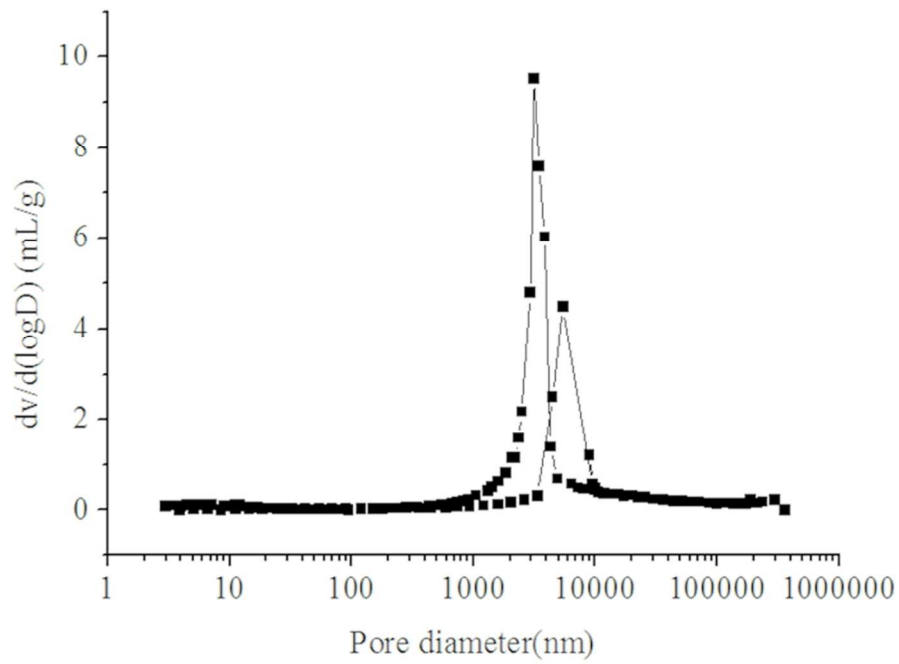
80x63mm (300 x 300 DPI)



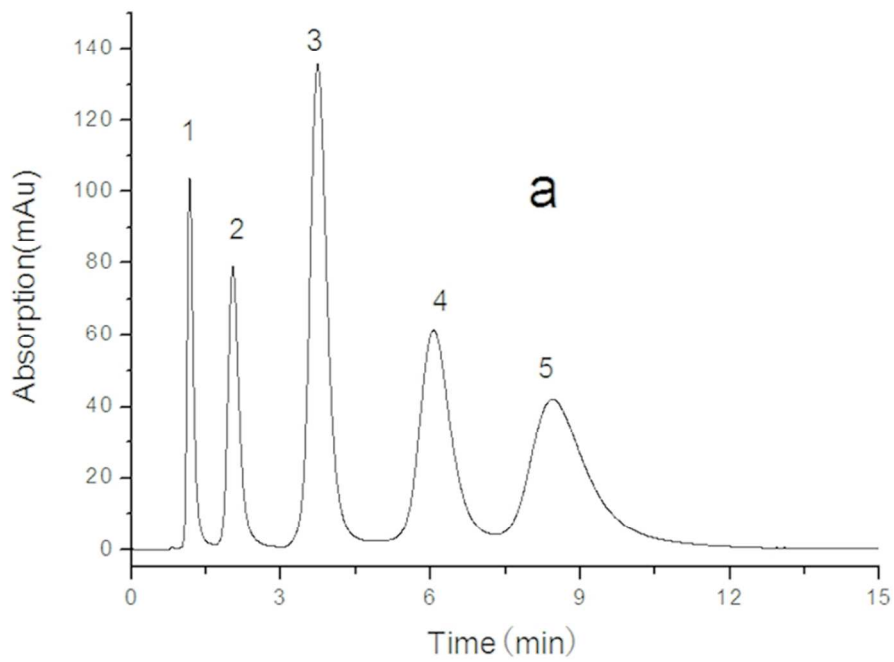
80x63mm (300 x 300 DPI)



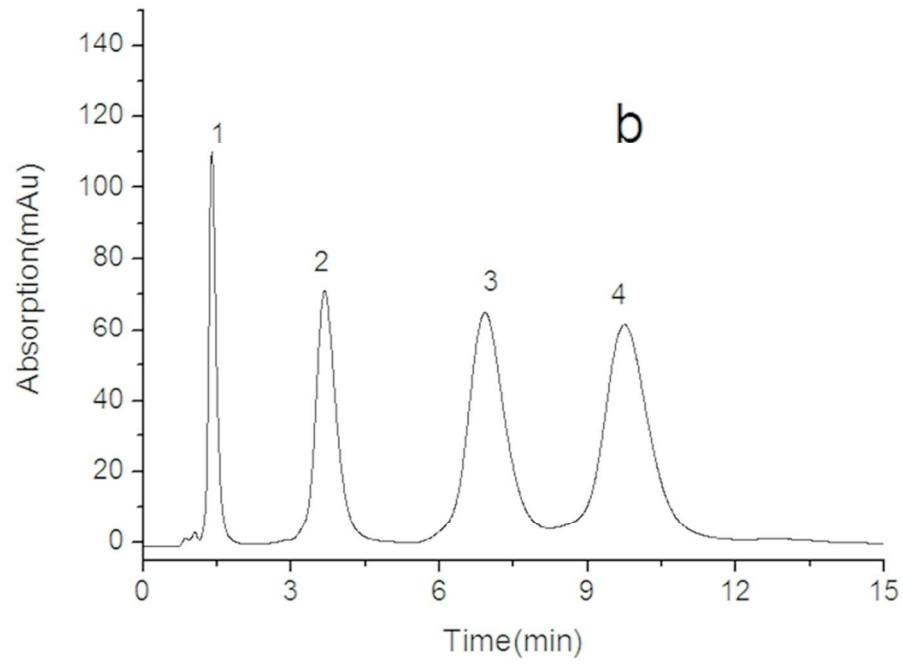
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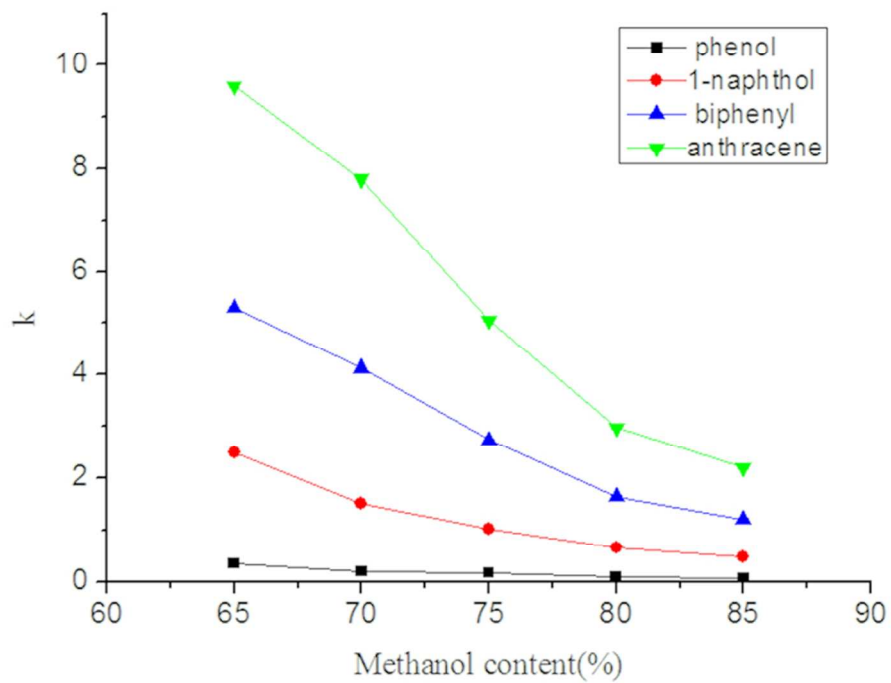
80x60mm (300 x 300 DPI)



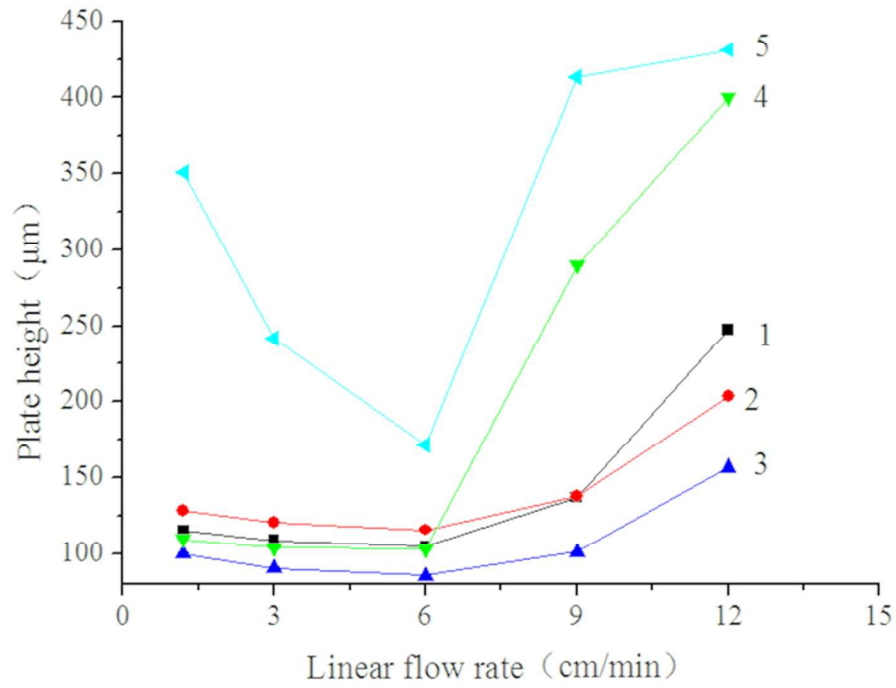
80x60mm (300 x 300 DPI)



80x60mm (300 x 300 DPI)



80x62mm (300 x 300 DPI)



80x63mm (300 x 300 DPI)