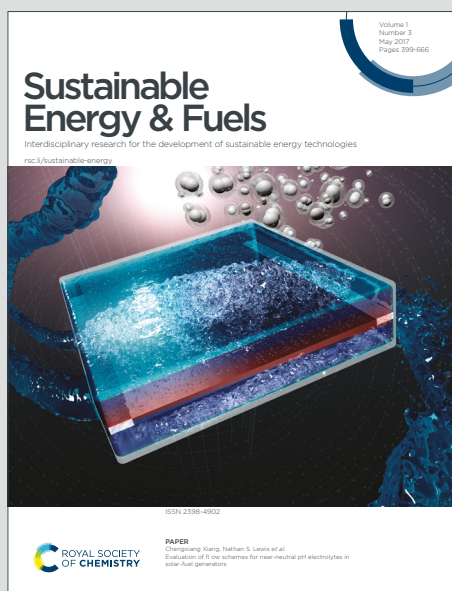


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Synergistic Plasmonic-Semiconductor Heterointerfaces Enabling Efficient CO₂ Hydrogenation to Methanol under Visible-Light Irradiation

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Abstract

The photocatalytic conversion of carbon-dioxide (CO₂) to methanol (CH₃OH) under mild conditions has been regarded as a promising, cost-effective, and environmentally sustainable approach for carbon utilization and renewable fuel generation. However, the process has been hindered by limited charge separation efficiency and insufficient CO₂ activation. In this study, a heterostructured Ag–Si/MgO/ZnO photocatalyst was rationally designed and synthesized via a solid-phase reaction method. A CH₃OH production rate of 357.53 μmol g_{cat}^{−1} h^{−1} was achieved over the optimized 10% Ag–Si/MgO/ZnO composite catalyst at 250 °C, representing a substantial enhancement compared to the Si/ZnO and Si/MgO/ZnO photocatalysts. The CH₃OH production performance was found to be higher in the photocatalyst/gas-phase system than that reported in comparable studies. The theoretical activation energy for Ag–Si/MgO/ZnO was found to be 158.14 kJ mol^{−1}, which is lower than that of Si/MgO/ZnO (167.79 kJ mol^{−1}) and Si/ZnO (177.97 kJ mol^{−1}), indicating enhanced CO₂ activation and



higher CO₂ conversion. More importantly, after more than 72 h of irradiation, the system still exhibited a high CH₃OH production rate, demonstrating its potential for practical application.

Keywords: Photocatalyst, hydrogenation, synergistic effect, carbon-dioxide photoreduction.

1. Introduction

The average concentration of CO₂ has jumped to 427.48 ppm in the atmosphere currently.¹ Although the concentration level of CO₂ in the atmosphere shouldn't be higher than 350 ppm. The sharp rise of concentration of CO₂ into the atmosphere is the main driver of greenhouse effect which causes global warming and climate change, gravely affecting human beings ability to live normally. Therefore, limiting the release of CO₂ is a significant task for humankind in an attempt to mitigate global warming. The production of liquid fuels and value-added chemicals via CO₂ hydrogenation has recently gained significant attention due to its promising economic potential and environmental advantages.²⁻⁴ Various value-added chemicals including CH₃OH, CH₄, CH₃CH₂OH, olefins, DME etc. are obtained from hydrogenation of CO₂.^{5,6} Among different products, CH₃OH has extensive applications as a vital organic solvent. It is an essential organic feedstock for organic synthesis, including the production of HCHO, C₃H₆O₃, C₂H₄, CH₃COOH, and other substances. It is also utilized as a hydrogen transporter, and as an energy source for fuel cells and gasoline.^{7,8} Consequently, the process of hydrogenation of CO₂ into CH₃OH utilizing green H₂ has garnered a lot of interest recently.^{9,10}

CO₂ hydrogenation to CH₃OH had been extensively studied. For instance, new active sites were introduced through nitrogen doping by Yang et al.,¹¹ which resulted in significant enhancement of reaction activity and catalytic stability of In₂O₃. Using an In₂O₃ nano-catalyst, a CH₃OH selectivity of 62.3% was achieved at 300 °C and 5 MPa. The ZrO₂/Cu photocatalyst was reported to have exhibited strong activity for CH₃OH formation. The hydrogenation of surface oxygenate intermediates and the activation of CO₂ were found to have been significantly enhanced over these configurations. In Cu-based catalysts, the promotion of CH₃OH synthesis was observed when Zn species were incorporated. The presence of Zn species was found to have increased the dispersion of Cu particles and prevented their agglomeration. As a result, a high copper surface area was maintained on the catalyst, which was considered to have improved its performance in CH₃OH synthesis. Moreover, the incorporation of ZnO was observed to have strengthened the resistance of Cu particles to



poisoning, improved CO₂ adsorption on the catalyst surface, and provided a higher density of catalytically active sites for the reactants.

Single-component photocatalysts had typically been limited by poor visible-light utilization, fast electron–hole recombination, and unfavorable adsorption energetics for key CO₂-reduction intermediates, whereas complementary metals had been shown to adjust charge-transfer pathways and intermediate binding in a controllable manner.¹² In bimetallic systems, plasmonic nanoparticles had been expected to generate localized surface plasmon resonance under visible light. As a result, hot-carrier generation and near-field enhancement had been exploited to strengthen light excitation and accelerate electron injection into nearby semiconductor or oxide domains, as widely reported for plasmon-assisted CO₂ photoreduction.¹³ Meanwhile, semiconductor domains had been introduced to tune the interfacial electronic structure and adsorption behavior. This approach had allowed early oxygenated intermediates to be stabilized on oxide sites, while hydrogenation-favored steps had been promoted on plasmonic metal sites, in agreement with the principle that bimetallic interfaces enabled spatial separation of adsorption/activation and hydrogenation functions.¹⁴ This mechanism had been expected to enhance both activity and selectivity by increasing the supply of reactive electrons from plasmonic components and by optimizing intermediate binding while suppressing unproductive pathways through interfacial site differentiation.¹⁵

Elemental Si, a visible-light-responsive semiconductor with a narrow indirect bandgap of ~1.1 eV, enables broad solar absorption and efficient generation of charge carriers under light irradiation, making it highly suitable for solar-driven catalytic applications.¹⁶ When coupled with plasmonic components, Si primarily functions as an electron reservoir and transport medium, facilitating the directional migration of photogenerated or plasmon-induced hot electrons toward catalytically active surface sites. This process promotes interfacial charge separation and effectively suppresses electron–hole recombination through plasmonic–semiconductor coupling and Schottky junction formation.¹⁷ Similar Si-based photocatalytic architectures have been reported to enhance visible-light utilization, charge separation efficiency, and CO₂ reduction performance through plasmonic–semiconductor coupling effects.^{18,19} Plasmonic–semiconductor photocatalysts can utilize up to ~45% of the solar spectrum, significantly improving photon-to-chemical conversion efficiency and reducing external heating energy input.²⁰ By coupling localized surface plasmon resonance (LSPR)–induced hot-electron generation with semiconductor charge transport, the system drives CO₂ reduction under mild conditions, thus lowering operational energy requirements per unit



methanol produced. From a techno-economic perspective, visible-light-assisted pathways may become cost-competitive as renewable H₂ prices continue to decline and scalable synthesis routes for plasmonic materials (e.g., Ag, Cu) are further optimized.²¹ Recent analyses suggest that photocatalytic methanol production can be economically favorable when solar-to-fuel efficiencies exceed 5–8% and catalyst stability surpasses several thousand hours.²² Although further development is needed, the combination of low-temperature operation, reduced energy intensity, and the prospect of using abundant, sunlight-driven excitation underscores the long-term economic viability of plasmonic–semiconductor photocatalysts for sustainable CO₂ valorization.

Visible-light-driven CH₃OH synthesis over plasmonic Cu/ZnO catalysts, achieving a CH₃OH production rate of 127.8 μmol g⁻¹ h⁻¹, was reported by Wang and co-workers.²³ It was found that, despite these advancements, copper-based catalysts were still prone to favor the reverse water–gas shift (RWGS) reaction. This undesired pathway was identified as a major limitation to the selective hydrogenation of CO₂ into CH₃OH and other value-added products when thermal heterogeneous catalysts were employed. To mitigate sintering and enhance catalyst stability, various promoters such as Al₂O₃, MgO, SiO₂, CeO₂, and ZrO₂ were commonly incorporated.²⁴ Among these, MgO was recognized as a promising promoter owing to its unique physicochemical properties. MgO was reported to inhibit the RWGS reaction and function as an adsorbent carrier with desirable features such as large surface area, high density of adsorption sites, tunable surface properties, and high chemical reactivity. Mg-based catalysts were reported to exhibit excellent performance for CO₂ hydrogenation to hydrocarbons. The incorporation of MgO as a catalyst component led to enhanced CO₂ adsorption due to its basic nature and improved metal dispersion by increasing surface area as a result of its low density. Few studies had been conducted on MgO-based catalysts for CO₂ hydrogenation to CH₃OH, and MgO was generally combined with other catalytic components to improve overall performance. For example, the influence of Cu/MgO/Al₂O₃ catalysts was investigated by Dasireddy et al.,²⁵ and the Cu/MgO/Al₂O₃ sample was reported to display the highest activity, which was attributed to the increased number of active sites for CO₂ and H₂ adsorption provided by MgO. Using a Cu–ZnO/MgO catalyst, Guo et al. achieved a CO₂ conversion of 7.6% and a CH₃OH selectivity of 91% at 200 °C and 5 MPa.²⁶ These findings demonstrated that high CH₃OH selectivity could be achieved through conventional heterogeneous catalysis. Nevertheless, because of the inherent thermodynamic stability of CO₂, its hydrogenation to CH₃OH was typically carried out under relatively harsh conditions, requiring elevated temperatures (>200 °C) and high pressures (>4 MPa).



Doping was adopted as a standard modification strategy and was increasingly focused upon by researchers. Among the various modification approaches applied to ZnO or MgO carriers, the incorporation of metals was predominantly employed. Noble metals were considered effective cocatalysts for charge carrier separation, as they were believed to act as electron sinks and solid-state mediators. Catalysts based on noble metals such as Pd, Pt, and Au were reported to exhibit excellent hydrogen spillover capacity, high stability, and strong anti-sintering ability in the CO₂-to-CH₃OH reaction.²⁷ For instance, oxygen vacancies were introduced on the surface of Pd/In₂O₃ catalysts by Men et al.,²⁸ resulting in a CH₃OH yield of 8.9% with a CO₂ conversion of 24.5%. Similarly, a 2 wt.% Pd/CeO₂ catalyst was reported by Pothu et al. to have achieved a CO₂ conversion of 49.6% and a CH₃OH selectivity of 69.5%.²⁹ In another study, CO₂ hydrogenation with H₂ over a Pt/film/In₂O₃ catalyst was reported by Men and co-workers, achieving a CO₂ conversion of 37.0% and a CH₃OH selectivity of 62.6%. Sun et al. confirmed,³⁰ both theoretically and experimentally, the feasibility of selective CO₂ hydrogenation to CH₃OH over Ag/In₂O₃. Under reaction conditions of 300 °C and 5 MPa, CH₃OH selectivity of 58.2% was maintained with a CO₂ conversion of 13.6% and a space–time yield (STY) of 0.453 g_e□□□_a□□□ g⁻¹h⁻¹. The appropriate selection of dopant metal into the metal oxide catalyst was reported to enhance interfacial charge transfer, thereby significantly improving CO₂ adsorption. Although plasmonic–semiconductor hybrid systems have been investigated under photothermal conditions, where thermal effects predominantly govern the catalytic activity,^{31–34} studies focusing on photocatalytic CO₂ conversion driven by plasmon-induced charge separation particularly in silicon-based, cost-effective semiconductor platforms remain limited.

In this study, a plasmonic Ag–Si/MgO/ZnO composite photocatalyst was synthesized via a solid-phase reaction method, and its photocatalytic performance was evaluated for CO₂ conversion under visible-light irradiation. Bimetallic Ag and Si species were introduced as cocatalysts supported on an MgO promoter to enhance charge separation efficiency and overall catalytic activity of the Ag–Si/MgO/ZnO system. The photocatalytic performance was systematically investigated in terms of product yield and apparent quantum yield (AQY). Furthermore, surface activation, structural evolution, and catalyst stability under extended illumination were analyzed using a suite of advanced characterization techniques. The findings reveal that the engineered heterostructure exhibits excellent stability, high photocatalytic efficiency, and strong scalability potential, offering valuable insights into the rational design of next-generation plasmonic–semiconductor systems for solar-driven CO₂ reduction.



2. Materials and Methods

2.1 Materials

Mg powder (99%), Zn powder (99%), and Silver Nitrate (AgNO_3), tri-Sodium citrate dehydrate ($\text{C}_6\text{H}_5\text{Na}_3\text{O}_7 \cdot 2\text{H}_2\text{O}$), Sodium Borohydride (NaBH_4) were purchased from Sigma-Aldrich (USA). Ultra-pure water was supplied through distillation of water. CO_2 (99.99%) and N_2 (99.99%) were collected from Spectra International Limited, Bangladesh. Water is electrolyzed to deliver renewable H_2 (99.99%). The electrolyte, Na_2SO_4 (99.99%) utilized to electrolyze water, was purchased from Sigma-Aldrich (USA). All chemicals used in this work were employed without any additional treatment.

2.2 Synthesis of SiO_2

Through the calcination procedure, waste rice husk was converted into a precursor silica (SiO_2) nanopowder. The wasted rice husk was first acid purified by immersing it in a 1000 ml aqueous solution of 20% HCl in a beaker and heating it to 100 °C for six hours. After being cleaned three times with pure water, the deep yellow rice husk was taken out from the beaker. The cleaned rice husk was then dried in an oven for 12 hours at 90 °C. To calcine the sample, the dried rice husk was placed in a tube furnace with the aid of a ceramic crucible and heated to 800 °C for two hours at a ramping rate of 10 °C min^{-1} . The bright white SiO_2 powder was collected when it had attained room temperature.

2.3 Synthesis of Si/MgO/ZnO

To develop a semiconductor-based photocatalyst, solid combustion approach was utilized in a specifically developed sealed stainless steel reactor. Employing a single-step magneto-thermic reduction technique, a Si/MgO/ZnO composite was developed in an enclosed reactor. Initially, 1 g of the obtained SiO_2 nanopowder was finely grounded with 0.65g of Zn powder and 0.65g of Mg powder by following the proportions of SiO_2 , Zn, and Mg being 1: 0.65: 0.65. Then, the sealed stainless steel reactor was filled with the grounded mixture of SiO_2 , Zn, and Mg powders. To execute the magneto-thermic conversion, the enclosed stainless steel reactor was placed within a muffle furnace and heated to 800 °C for 6 h, raising the temperature by 5 °C per minute. The reactor was removed from the furnace once it reached room temperature. The built Si/MgO/ZnO material was removed from the reactor and finely powdered.



2.4 Synthesis of Ag nanoparticles (NPs)

Ag nanoparticles (Ag NPs) were synthesized via a chemical reduction method employing tri-sodium citrate ($C_6H_5Na_3O_7 \cdot 2H_2O$) and sodium borohydride ($NaBH_4$) as reducing agents. Silver nitrate ($AgNO_3$) and $Na_3C_6H_5O_7$ were used as precursors, and all solutions were freshly prepared using distilled water. In a typical procedure, 100 mL of 1 M $Na_3C_6H_5O_7$ solution was magnetically stirred, after which 100 mL of 0.25 mM $AgNO_3$ solution was added dropwise under continuous stirring until a clear and homogeneous solution was obtained. Subsequently, 250 mL of 148 mM $NaBH_4$ solution was introduced dropwise at a controlled rate of approximately one drop per second. The reaction mixture was stirred vigorously for 6 h, during which a gradual color transition from light yellow to dark yellow and finally to gray was observed, indicating nanoparticle formation and subsequent colloid destabilization. After completion of the reaction, stirring was stopped, and the solution was left undisturbed overnight to allow complete precipitation of the nanoparticles. The resulting Ag nanoparticles had been collected as a solid residue, repeatedly washed with distilled water to remove impurities, and subsequently subjected to high-temperature treatment (850 °C for 6 h) during photocatalyst preparation. Therefore, any residual species would have been expected to be removed through post calcination process.

2.5 Synthesis of Ag-Si/MgO/ZnO

With the aid of a hydraulic pressure machine, the fine Ag-Si/MgO/ZnO mixture powder were further sealed in a cylindrical stainless steel reactor under elevated pressures. Attempting to build a solid Ag-Si/MgO/ZnO structure, the reactor was then placed inside a muffle furnace and heated to 850 °C for 6 h, raising in temperature by 5 °C per minute. When the reactor reached room temperature, it was removed from the furnace. Employing a hydraulic pressure machine, the Ag-Si/MgO/ZnO specimen with a solid structure was removed from the reactor. After being cleaned the surface of the formed solid Ag-Si/MgO/ZnO specimen with series paper, it was heated in a Muffle furnace for two hours at a temperature of 5 °C per minute. The solid-structured Ag-Si/MgO/ZnO composite was subsequently removed from the furnace and split it into several pieces to be used as a photocatalyst in a continuous flow reactor once it had reached room temperature. For the purpose to assess the photocatalytic efficiency, additional Si/MgO/ZnO and Si/ZnO catalysts were developed without Ag or Ag/MgO, respectively. The overall synthesis process of Ag-Si/MgO/ZnO photocatalyst is presented in Fig. S1.



2.2 Characterization

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The microstructure and morphology of the prepared materials were characterized by scanning electron microscopy (SEM, Sigma-300, Germany), while elemental composition and mapping were determined by energy-dispersive spectroscopy (EDS). Transmission electron microscopy (TEM) and high-resolution TEM (HRTEM) images with elemental mapping were obtained using FEI Talos F200X and Tecnai F20 instruments. The crystalline phases were analyzed by X-ray diffraction (XRD, Bruker AXS, Germany) using Cu K α radiation ($\lambda = 1.5418 \text{ \AA}$). Optical absorbance and diffuse reflectance spectra were recorded using a Cary 5000 UV-vis spectrophotometer (Varian, USA) and a Thermo Scientific Evolution 220 UV-vis DRS instrument, respectively. Surface composition and chemical states were examined by X-ray photoelectron spectroscopy (XPS, ESCALAB 250Xi, Thermo Fisher, UK), and photoluminescence (PL) spectra of the solid powders were measured with a Hitachi F-7000 fluorescence spectrophotometer (Japan).

2.4 Photo-electrochemical tests

The CorrTest electrochemical workstation (Wuhan Corrtest Instruments Comp. Ltd., China) was utilized to measure the transient photocurrent response of all samples. The electrochemical impedance spectroscopy, and Mott-Schottky plots of catalyst specimens were performed on the Autolab workstation (Netherlands). A platinum wire served as the counter electrode. An Ag/AgCl electrode was used as the reference electrode. A conventional quartz cell with three-electrode was employed in both the electrochemical system. The solution of 0.5 M Na₂SO₄ was used as electrolyte. The series of photocatalyst films were coated on fluorine-tin-oxide (FTO) glasses of 1 cm² area using as a working electrode. The working electrodes were prepared using doctor blade method. In short, before preparing the solution, the polyvinylidene difluoride (PVDF) binder was dried over an entire night. N-methyl-2-pyrrolidone (NMP) solvent was utilized to combine 90% active material (photocatalyst) and 10% binder agent (PVDF) to prepare a paste. Employing a doctor blade approach, the as-prepared paste was placed on the functionalized surface of the FTO glass. The decorated FTO was placed in an oven for 24 hours at 60 °C for drying it properly. A tungsten lamp (100W) was utilized to illuminate the prepared samples. N₂ gas was used to purge the electrolyte for 30 minutes prior to the tests. In a 0.5 M Na₂SO₄ solution, electrochemical impedance spectroscopy (EIS) was conducted at a frequency ranging from 0.1 Hz to 1000 Hz. In each instance, a sinusoidal potential amplitude of 5 mV was applied. Mott-Schottky plots was performed utilizing the same setup (applied voltage: -0.5 V,



frequency: 1000 Hz, AC voltage: 5 mV amplitude). Over the course of on-off cycle the transient photocurrent responses were measured at 0 V potential bias versus Ag/AgCl.

2.5 Photocatalytic performance test

The schematic diagram of experimental set up for photocatalytic CO₂ hydrogenation to CH₃OH under visible light is presented in Fig. S2. Utilizing the prepared catalyst, a cylindrical fixed-bed continuous-flow quartz-glass reactor was employed to measure the hydrogenation of CO₂ to CH₃OH. The reactor is made up of a 130 mm length and 8 mm diameter column. 1 g of photocatalyst (40–50 mesh) was installed in the middle part of column almost 10 mm in length. By filling both sides of the photocatalyst bed with quartz wool, the catalyst bed maintained fixed. The reactor was installed in a cylindrical glass furnace 4 cm away from the light source and linked to the gas inlet and outlet. An electric heater is fitted into the furnace to control the temperature of the reactor. A thermocouple is fitted in the furnace to measure the inside temperature of the furnace. A mass flow controller was employed to control the flow rate of the reactant gas mixture. For maintaining a specified pressure, a back-pressure controller was integrated into the gas line which was connected to the outlet. The reaction was carried out at atmospheric pressure during reaction circumstances with a N₂ flow along with temperature ranges up to 300 °C. Following 3 h, H₂ (generated by electrolysis) and CO₂ (99.999%) were provided throughout the reaction. In all experiments using the reaction mixture, we used the ratio H₂:CO₂=3:1 that reflects a stoichiometric equation for the CH₃OH synthesis reaction (CO₂ + 3H₂ → CH₃OH + H₂O) and has been commonly used in related prior studies. The kinetic study on the reaction was carried out between 200 °C and 300 °C. The liquid phase products (CH₃OH) resulting from photocatalytic CO₂ reduction were collected in a cold trap and subsequently analyzed on gas chromatography (GC-2014, SHIMADZU) equipped with flame ionization detector (FID). The production rate of CH₃OH in the hydrogenation of CO₂ was determined by the following Eq. (3):³⁵

$$\text{CH}_3\text{OH yield rate} = \frac{\text{amount of produced CH}_3\text{OH}}{\text{mass of photocatalyst} \times \text{time duration}} \mu\text{mol g}_{\text{cat}}^{-1} \text{ h}^{-1} \quad (3)$$

The apparent quantum yield of the as-prepared Ag-Si/MgO/ZnO photocatalyst for CH₃OH production was evaluated by using the following Eq. (4).³⁵

Apparent quantum yield for CH₃OH,

$$\text{AQY} = \frac{6 \times \text{Number of CH}_3\text{OH molecules}}{\text{Number of incident photons}} \times 100\%$$



$$= \frac{6 \times N_{CH_3OH} \times N_A}{I_i \times A \times \frac{\lambda}{hc} \times t} \times 100\%$$

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Where N_{CH_3OH} was defined as the number of moles of CH_3OH that were generated during the time interval t . The Avogadro's number was taken as $(6.023 \times 10^{23} atoms.mol^{-1})$. The area of the surface on which the light was irradiated was denoted as A (m^2). Planck's constant, h was considered as $(6.626 \times 10^{-34} Js)$; and the speed of light, c was taken as $3 \times 10^8 ms^{-1}$. The time duration of light irradiation was represented as t (s). The wavelength of the incident light, λ was measured by a bandpass filter and was taken as $\lambda=420$ nm. The average intensity of the incident light, I_i , was measured by a suitable measuring instrument, such as a pyranometer, and was expressed in Wm^{-2} .

2.6 Computational Methods

The distribution of electro-magnetic (EM) field over the Si/ZnO, Si/MgO, Si/ZnO/MgO, and Ag-Si/ZnO/MgO are conducted using finite-difference time-domain (FDTD) method. The 630 nm is used as the simulated excitation wavelength of all nano-structures. The Ag-Si/ZnO/MgO is modeled as follows: isolated Si, Si/MgO and Ag-Si/MgO NPs assemblies are placed on the surface of ZnO nanosheets, respectively. A plane wave propagating in the z-direction with an electric field parallel to the x-direction was selected to estimate the electric field distribution. The dielectric functions of Ag, Si, MgO, and ZnO were taken from the literature. Density functional theory (DFT) calculations were carried out using the DMol³ module within the Materials Studio software package. The interaction between ionic cores and valence electrons was modeled using the projector augmented-wave (PAW) formalism. The plane-wave basis set was constructed with a kinetic energy cutoff of 500 eV to ensure adequate convergence. Exchange–correlation effects were accounted for within the framework of the generalized gradient approximation (GGA), employing the Perdew–Burke–Ernzerhof (PBE) functional. Brillouin zone integrations were performed using Monkhorst–Pack k-point meshes. For the slab models considered, a final k-point mesh of $X \times Y \times 1$ was adopted, where X and Y were determined from the convergence tests. A single k-point was used along the surface normal due to the large vacuum spacing. Self-consistent field (SCF) cycles were converged to a tolerance of 1×10^{-5} eV/atom, with convergence thresholds of 0.1 eV/Å for maximum forces and 5×10^{-3} Å for atomic displacements.



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The Gibbs free energy for all reactions was obtained by the following formula Eq. (5).

$$\Delta G = \Delta E + \Delta ZPE - T\Delta S \tag{5}$$

Here, ΔE denotes the total energy change calculated using Materials Studio, while ΔZPE and ΔS correspond to the variations in zero-point energy and entropy, respectively. The values of ΔE , ZPE , ΔZPE and $T\Delta S$ are calculated by the following supplementary Eqs. S1-S4. The change of zero point energy and change of TS for various reactions in the CO₂ hydrogenation to CH₃OH are calculated by the pathways following in Table 1.

Table 1: Calculation of change of zero point energy and change of TS for various reactions in the CO₂ hydrogenation to CH₃OH pathways.

Reactions	Equations for Change of ZPE	Value of ΔZPE (eV)	Equations for Change of TS	Value of $T\Delta S$ (eV)
CO ₂ +H=COOH	$\Delta ZPE = ZPE_{COOH} - (ZPE_{CO_2} + ZPE_H)$	0.005238155	$T\Delta S = TS_{COOH} - (TS_{CO_2} + TS_H)$	-1.01506546
COOH+H=CO+H ₂ O	$\Delta ZPE = ZPE_{CO} + ZPE_{H_2O} - (ZPE_{COOH} + ZPE_H)$	0.010259345	$T\Delta S = TS_{CO} + TS_{H_2O} - (TS_{COOH} + TS_H)$	0.83977502
CO+H=HCO	$\Delta ZPE = ZPE_{HCO} - (ZPE_{CO} + ZPE_H)$	-0.120043635	$T\Delta S = TS_{HCO} - (TS_{CO} + TS_H)$	-0.27203544
HCO+H=H ₂ CO	$\Delta ZPE = ZPE_{H_2CO} - (ZPE_{CO} + ZPE_H)$	-0.114836475	$T\Delta S = TS_{H_2CO} - (TS_{CO} + TS_H)$	-0.37171585
H ₂ CO+H=H ₃ CO	$\Delta ZPE = ZPE_{H_3CO} - (ZPE_{H_2CO} + ZPE_H)$	-0.132813575	$T\Delta S = TS_{H_3CO} - (TS_{H_2CO} + TS_H)$	-0.30651881
H ₃ CO+H=CH ₃ OH	$\Delta ZPE = ZPE_{CH_3OH} - (ZPE_{H_3CO} + ZPE_H)$	-0.084275405	$T\Delta S = TS_{CH_3OH} - (TS_{H_3CO} + TS_H)$	-0.33720159

The adsorption energy (E_{ads}) was calculated using the following expression:

$$E_{ads} = E_{adsorbate+surface} - (E_{adsorbate} + E_{surface}) \tag{6}$$

Where $E_{adsorbate+surface}$ is the total energy of the surface system after adsorption of the species, $E_{adsorbate}$ is the total energy of the free adsorbate, and $E_{surface}$ is the total energy of the pristine surface.

3. Result and Discussion

The surface activation process for Ag-Si/ZnO/MgO composite photocatalyst is shown in Fig. 1A. Scanning electron microscopy (SEM) analysis was employed to investigate the morphology of the fabricated Ag-Si/MgO/ZnO catalyst. The Ag-Si/MgO/ZnO catalyst exhibited densely packed, well-defined cuboidal/prismatic particles with faceted surfaces, indicative of high crystallinity and uniform growth. These particles exhibit a relatively narrow size distribution and form an aggregated network with close particle-to-particle contact, as

depicted in Fig. 1(B-C). The morphology of Ag-Si/MgO/ZnO catalysts was also studied using transmission electron microscopy (TEM). The TEM photograph 1(D-E) displays particles that are well-defined and faceted. Their morphology is polyhedral and appears to be cuboidal or slightly truncated prismatic. The clear edges and uniform contrast show that these are single crystalline domains, not amorphous aggregates. The particle size seen in the TEM is very similar to the size value proposed by the SEM since the size is very monodispersed. Fig. 1(G-L) of the EDX elemental mapping images of the synthesized Ag-Si/MgO/ZnO catalyst showed the distributions of elements Ag, Si, Zn, Mg, and O, thereby confirming successful preparation of the nanocomposite. The elemental mapping of the Ag-Si/MgO/ZnO nanostructured catalyst confirmed the uniform presence of Ag and Si on the nanocrystalline MgO/ZnO support, showing that these elements were evenly spread throughout the catalyst. The Powder XRD analysis showed that all synthesized catalysts are highly crystalline. The XRD pattern of the Ag-Si/MgO/ZnO shows peaks at 28.48° , 42.88° , 56.22° , 69.70° , and 77.38° depicting the indexed peaks (111), (220), (110), (400), and (331) of Si (JCPDS 01-089-2955). The presence of ZnO, MgO and Ag were confirmed by matching the characteristic peaks with their respective JCPDS files (03-65-2880, 00-045-0946, and 01-089-2955).

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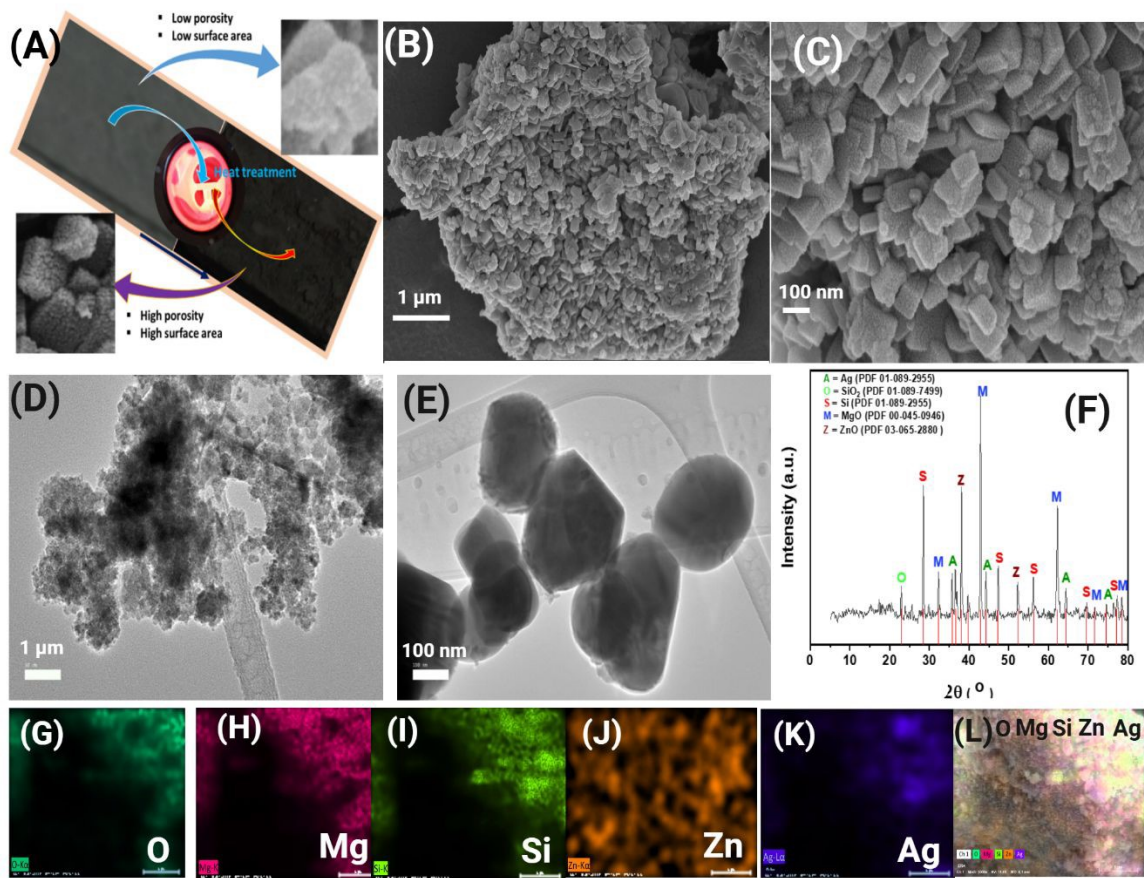


Fig. 1 Schematic diagram of the heat-induced surface activation process for Ag-Si/ZnO/MgO composite photocatalyst (A); Morphology of the as-prepared Ag-Si/MgO/ZnO blocks. SEM image of Ag-Si/MgO/ZnO (B-C); TEM images of Ag-Si/MgO/ZnO (D-E); XRD patterns of as-prepared Ag-Si/MgO/ZnO (F); Elemental mapping of Ag-Si/MgO/ZnO EDX analysis (G-L).

MgO promotion had been specifically important because MgO had provided basic sites that had strengthened CO₂ adsorption. A higher number of effective adsorption events was maintained compared with supports that were less basic or less able to stabilize highly dispersed metal particles.³⁸ The plasmonic function of Ag had increased the flux of energetic electrons under visible light, while MgO had increased reactant uptake and stabilized interfacial active sites, and this dual promotion had been consistent with the experimentally observed highest methanol rate (357.53 μmol g_{cat}⁻¹ h⁻¹ at 250 °C and 3 bar) and reduced apparent activation energy (158.14 kJ mol⁻¹) for Ag-Si/MgO/ZnO versus the Ag-free counterparts. It was inferred from these results that strong ZnO–MgO interactions occurred which generated



high dispersion of Ag and Si species on the surface of the catalyst and small active site formation.

All samples were studied under the same condition using the same excitation wavelength of 450 nm in the solid phase to study the charge-carrier dynamics and charge-separation efficiency using photoluminescence (PL) experiments (Fig.2A). Lower PL intensity mean charge separation is more efficient. There was a significantly lower number of recombination events in Ag–Si/MgO/ZnO indicating that the efficiency of charge-separation was excellent for this material. The introduction of Ag into Si/MgO/ZnO likely created additional vacancies that acted as traps for photo-generated charge carriers, thereby significantly suppressing their recombination. This property of keeping electrons in the conduction band for a longer period enhances their photocatalytic activity. The PL quenching effects seen in Ag–Si/MgO/ZnO showed that the charge transfer and separation in the system was enhanced. The outcomes of our PL tests have been confirmed to be consistent with the photocatalytic CO₂ reduction data (Fig 4B–C, E). This means the effective suppression of a result in photo-induced e[−]/h⁺ recombination means the enhancement of observed activity. Ag–Si/MgO/ZnO showed the best performance for CH₃OH production among all tested samples.

Enhancing the photocatalytic conversion of CO₂ via Ag-Si/MgO/ZnO heterostructure was due to efficient separation of photo-generated charge carriers. The presence of Ag in Ag–Si/MgO/ZnO made the charge more mobile and limited e[−]/h⁺ recombination. As a result, the transient photocurrent response (Fig.2B) of Ag–Si/MgO/ZnO was about 7.5 times stronger than that of Si/ZnO and 1.8 times stronger than that of Si/MgO/ZnO. The response of the photocurrent remains stable upon repeated on off cycles which indicates a good photoelectrochemical stability that is in line with PL results. Fig.2C presents EIS Nyquist plots (frequency range: 0.1 Hz to 1 kHz, applied bias: −0.5 V. A minor arc radius in the Nyquist plot suggested less resistance to electron migration, signifying efficient charge-carrier separation. The Ag–Si/MgO/ZnO composite had a smaller arc radius than the Si/ZnO and Si/MgO/ZnO with less charge recombination and improved electron–hole migration efficiency. These results were in agreement with the PL spectra. It can be concluded that Ag may play a crucial role in enhancing charge-separation efficiency by suppressing charge-recombination rates and improving the light-absorption behavior. Other researchers also observed that Ag loading effectively suppressed photo-induced electron–hole recombination and increased visible-light absorption, ultimately enhancing photocatalytic activity.³⁹



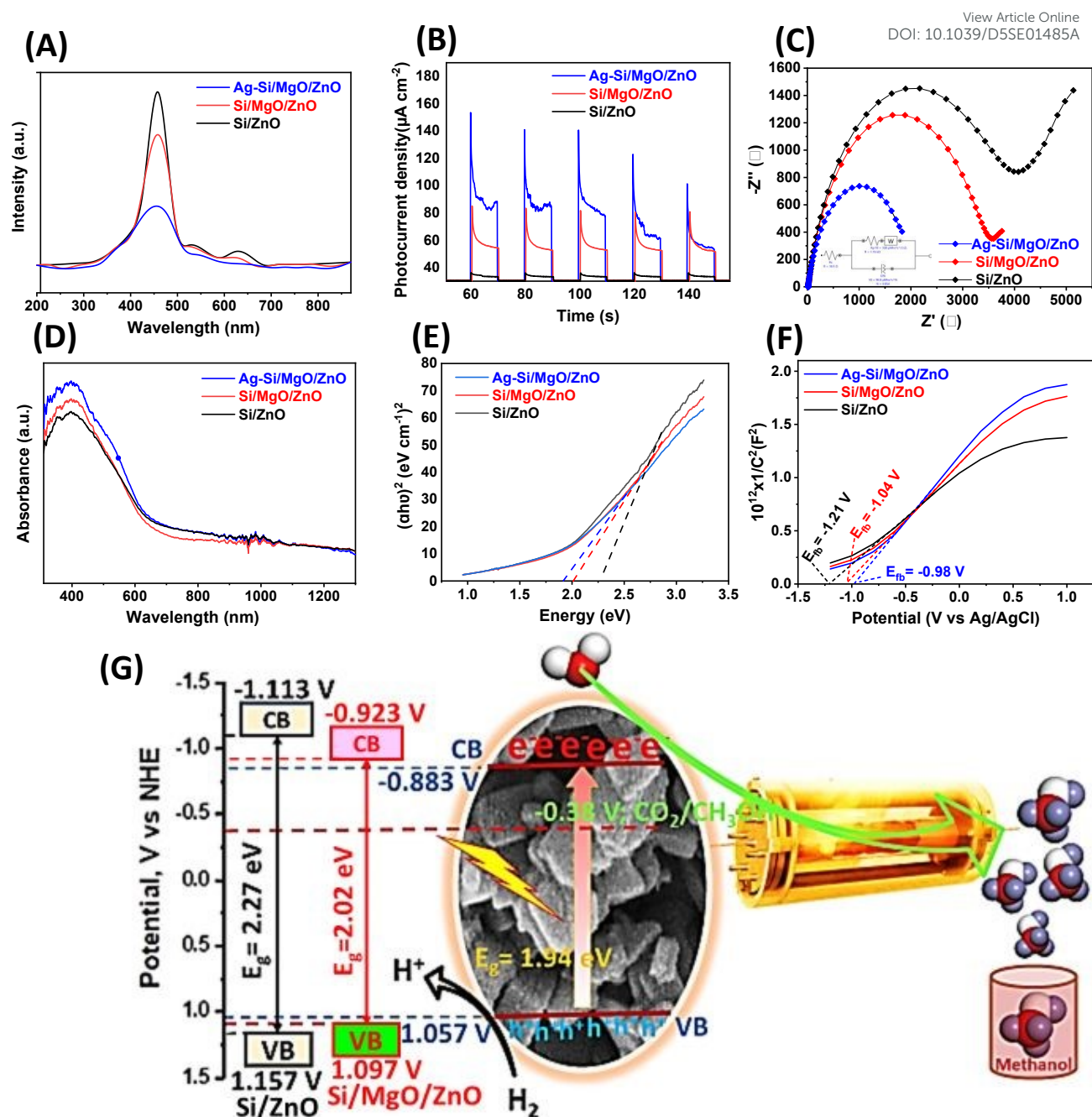


Fig. 2 (A) Photoluminescence (PL) spectra for Si/ZnO, Si/MgO/ZnO, and Ag-Si/MgO/ZnO; (B) Transient photocurrent responses; (C) EIS plots; (D) UV-vis DRS; (E) Tauc's plot of Si/ZnO, Si/MgO/ZnO, and Ag-Si/MgO/ZnO; (F) Mott-Schottky curves; and (G) band alignments of Si/ZnO, Si/MgO/ZnO, and Ag-Si/MgO/ZnO.

The UV-vis diffuse reflectance spectrophotometry studied photocatalysts prepared optical absorption characteristics. The UV-vis diffuse reflectance spectra of Si/MgO/ZnO and Ag-Si/MgO/ZnO are presented in Fig. 2D. The absorption band edge of Si/MgO/ZnO is



observed at about 600 nm. After adding Ag nanoparticles, the absorption peak in the visible range was increased as well as red-shifted to about 630 nm. Thus, the edge of absorption was changed. The main reason for this change was due to the SPR behavior of the Ag species. Thus, inclusion of Ag into Ag-Si/MgO/ZnO was found to have greatly enhanced the light-absorption range into the visible region. Similar observations were made by Chen et al. who realized Ag doping is responsible for visible light absorption due to plasmon resonance.³⁹ A shift in UV–vis light absorption toward the visible region after Ag doping was also reported by Chen et al.⁴⁰ However, it was noted that excessive Ag loading resulted in a decline in light absorption and photocatalytic CO₂ reduction activity, likely due to a shielding effect, where surplus Ag partially blocked the light absorption of ZnO and MgO. The bandgap (E_g) values of the samples were estimated using Tauc's relation, as shown in Eq. (6).⁴¹

$$\alpha h\nu = A(h\nu - E_g)^n \quad (6)$$

Here, A is a constant, E_g represents the semiconductor bandgap, and n is assigned a value of $\frac{1}{2}$ for a direct bandgap semiconductor. The plots of $(\alpha h\nu)^2$ versus photon energy are generated. In Fig. 2E, a straight line is fitted to the linear portion of the curve, and this line is extrapolated to the X-axis to determine the bandgap values. The band-gap values of Si/ZnO, Si/MgO/ZnO and Ag-Si/MgO/ZnO photocatalysts were derived from Fig. 2E as follows 2.27, 2.02 and 1.94 eV, respectively. The band-gap of Ag-Si/MgO/ZnO is shifted to left after loading of Ag and improved photocatalytic efficiency for CO₂ reduction. A suitable conduction band edge position and an adequate supply of free electrons were considered vital for achieving higher photocatalytic performance. Vu et al. suggested that the conduction band position should have been more negative than the reduction potential of CO₂ to CH₃OH (−0.38 V, NHE) in order to enable CH₃OH production.⁴² In this context, Mott–Schottky analysis was carried out to determine the semiconductor type, and the flat-band potential (E_{fb}) was obtained (Fig. 2F). Si/ZnO, Si/MgO/ZnO and Ag–Si/MgO/ZnO samples exhibited positive slopes, indicating n-type semiconductor behavior.⁴³ The flat-band potentials (E_{fb}) of Si/ZnO, Si/MgO/ZnO and Ag–Si/MgO/ZnO were evaluated to be 1.21 V, −1.02 V and −0.98 V (vs. Ag/AgCl), respectively, from the Mott–Schottky plots. The E_{fb} values (vs. NHE) for both samples were calculated using Eq. (7).⁴⁴

$$E_{fb} \text{ (vs. NHE)} = E_{fb} \text{ (vs. Ag/AgCl)} + 0.197 \quad (7)$$

The values of E_{fb} (vs. NHE) for Si/ZnO, Si/MgO/ZnO and Ag–Si/MgO/ZnO samples were determined to be −1.013 V, −0.823 V and −0.783 V, respectively. It was known that the



476 conduction band (CB) position of an n-type semiconductor lies approximately 0.1 eV below
 477 E_{fb} .⁴³ Hence, the CB potentials for Si/ZnO, Si/MgO/ZnO and Ag–Si/MgO/ZnO were
 478 calculated as -1.113 V, -0.923 V and -0.883 V, respectively. The VB positions were then
 479 determined to be 1.157 V for Si/ZnO (-1.113 + 2.27), 1.097 V for Si/MgO/ZnO (-0.923 +
 480 2.02) and 1.057 V for Ag–Si/MgO/ZnO (-0.883 + 1.94). Ag nanoparticles were found to act
 481 as electron-trapping centers, leading to enhanced photocatalytic performance.³⁹ Based on these
 482 calculations, experimental data, and CO₂ photoreduction results, a possible band diagram of
 483 the as-synthesized photocatalysts was proposed, and the mechanism of CO₂ photoreduction to
 484 CH₃OH over the Ag–Si/MgO/ZnO heterostructure was illustrated (Fig. 2G). The conduction
 485 band-edge potential of Ag–Si/MgO/ZnO was shown to be more negative than the reduction
 486 potential of CO₂ to CH₃OH. Furthermore, the bandgap of Ag–Si/MgO/ZnO was found to be
 487 smaller than that of Si/MgO/ZnO. Under visible light illumination, photo-generated electrons
 488 were efficiently transferred from the CB of Ag–Si/MgO/ZnO to the Ag NPs. The electrons
 489 accumulated on Ag NPs then reduced CO₂ to CH₃OH. The difference in CO₂ photoreduction
 490 efficiency between Ag-undoped and Ag-doped Si/MgO/ZnO heterostructures confirmed that
 491 the electron transfer rate from Ag NPs to the adsorbed carbonate species was enhanced by Ag
 492 integration, which improved carrier separation and overall CO₂ photoreduction efficiency.
 493 Additionally, a synergistic effect between ZnO and MgO was postulated to suppress photo-
 494 induced charge recombination by transferring photo-generated species from ZnO to MgO
 495 within the heterostructure. Thus, the as-prepared Ag–Si/MgO/ZnO heterostructure was found
 496 to play a significant role in promoting CH₃OH formation by increasing its production rate. To
 497 further elucidate the hydrogenation pathway for CO₂ reduction to CH₃OH over the Ag–Si dual-
 498 metal active sites of the Ag–Si/MgO/ZnO catalyst, DFT calculations were carried out using the
 499 Material Studio software. The surface electronic state, chemical composition, and bonding
 500 environment of the synthesized catalysts were analyzed by X-ray photoelectron spectroscopy
 501 (XPS). The XPS spectra of the Ag–Si/MgO/ZnO catalyst were presented in Fig. 3A–E. The
 502 full survey spectrum confirmed the presence of Ag, Si, Mg, Zn, and O elements within the
 503 sample, which was consistent with the EDS results, thereby indicating the successful synthesis
 504 of the catalyst. The characteristic peaks corresponding to Ag 3d, Si 2p, Mg 2p, Zn 2p, and O
 505 1s were observed at their respective binding energies.

506 As shown in Fig. 3A, the Ag 3d spectrum exhibited two strong peaks at 367.7 and 374.4 eV,
 507 attributed to Ag 3d_{5/2} and Ag 3d_{3/2}, respectively, confirming the presence of metallic Ag
 508 clusters. Two weak peaks corresponding to Ag⁺ were also observed, in agreement with the



results of Tada et al.,⁴⁵ who reported that XPS spectra displayed peaks for metallic Ag at 368.0 eV (Ag 3d_{5/2}) and 374.0 eV (Ag 3d_{3/2}), as well as weak peaks for Ag⁺ at 369.7 eV (Ag 3d_{5/2}) and 375.7 eV (Ag 3d_{3/2}).^{46,47} In the Si spectrum (Fig. 3B), peaks at 99.38 and 100.3 eV were assigned to Si 2p_{3/2} and Si 2p_{1/2}, respectively, confirming the coexistence of Ag and Si in the composite. Cerofolini et al. reported that the 2p_{3/2} and 2p_{1/2} peaks in the range of 99–100.5 eV were characteristic of elemental silicon.⁴⁸ The peak at 100.3 eV was assigned to Si–H bonds, while a feature at 532.1 eV indicated the presence of Si–OH species. The presence of Si–H dangling bonds has been associated with enhanced charge separation efficiency on Si-supported photocatalysts.⁴⁹ These functional bonds acted as electron sinks, promoting charge transfer during photocatalysis. In the Mg spectrum (Fig. 3C), two peaks at 49.7 and 50.1 eV were attributed to Mg 2p_{3/2} and Mg 2p_{1/2}, respectively. Fig. 3D shows the Zn 2p spectrum with peaks at 1021.24 eV and 1022.2 eV, corresponding to Zn 2p_{3/2} and Zn 2p_{1/2}, confirming the coexistence of Zn²⁺ and Mg²⁺ species in the catalyst. A higher-binding-energy (~1023.5 eV) in the Zn 2p_{3/2} region could be attributed to surface-defective Zn²⁺ species, originating from oxygen-deficient coordination and/or hydroxylated Zn sites, which result in reduced electronic screening compared to bulk ZnO.⁵⁰ The O 1s spectrum (Fig. 3E) exhibited peaks at 529.7, 530.9, and 532.1 eV, assigned to lattice oxygen, oxygen vacancies, and surface hydroxyl groups, respectively. The 529.7 eV peak was consistent with MgO formed through solid-phase oxidation of Mg. The role of MgO as a support was attributed to its tunable acid–base properties, which regulate electron transfer between the support and active phase, as suggested by Julkapli et al.⁵¹ Additionally, Meshkani et al. reported that Lewis basicity of MgO enhanced chemisorption of surface functional groups and promoted electron transport.⁵² No detectable boron-related chemical states had been observed in the XPS spectra, indicating that residual boron-containing species were below the detection limit and negligible in the final material.

The total density of states (TDOS) for bimetallic Ag–Si/MgO/ZnO, single-metallic Si/MgO/ZnO, and Si/ZnO catalysts are presented in Fig. S3. The TDOS of bimetallic Ag–Si/MgO/ZnO exhibited a narrower bandgap compared to Si/MgO/ZnO and Si/ZnO, justifying its faster electron excitation and transfer to intermediate species. The bimetallic co-catalyst thus accelerated electron transport, enabling the six-electron reduction of CO₂ to CH₃OH. Projected partial density of states (PDOS) analysis (Fig. 3F) showed that the s-band center of Ag–Si/MgO/ZnO was located near the Fermi level (E_F), favoring activation of O-species adsorption. The weak s–p orbital overlap indicated a long-range interlayer interaction, allowing CO₂ molecules to pass through easily without significantly affecting the catalyst interface.



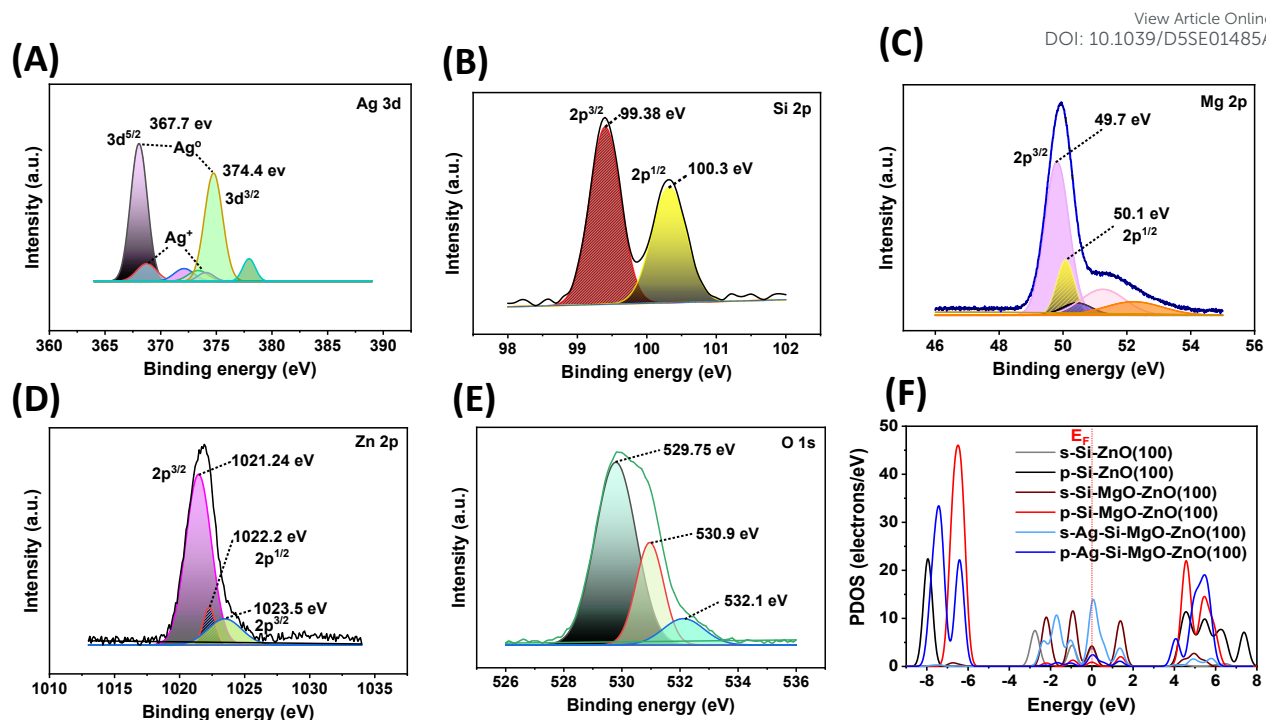


Fig. 3 XPS survey spectra of Ag-Si/MgO/ZnO; High-resolution XPS spectra of (A) Ag 3d, (B) Si 2p, (C) Mg 2p (D) Zn 2p (E) O 1s in Ag-Si/MgO/ZnO sample. DFT calculations of CO₂ reduction. F) The partial density of states for s and p-orbits of Ag-Si/MgO/ZnO, Si/MgO/ZnO, and Si/ZnO.

To understand the enhancement in photocatalytic performance after loading Ag and Si nanoparticles, finite-difference time-domain (FDTD) calculations were conducted in the visible range at different wavelengths (400 nm-800 nm) to simulate the local electric field distribution between the Ag and Si nanoparticle assemblies on MgO/ZnO with an interparticle distance of 2 nm (Fig. 4A and Fig. S4(A-F)). The electric field intensity distribution was visualized on a logarithmic scale. Fig. S4(G) shows the electric field distribution, $|E|^2$, around the surface of the Ag-Si/MgO/ZnO as a function of wavelength using FDTD simulations. Upon light irradiation, the electric field distribution $|E|^2$ around the surface of the Ag-Si/MgO/ZnO was enhanced, and a maximum value of $|E_{\max}|^2$ of ≈ 800 was obtained at a wavelength of 457.143 nm. This improved local electric field, originating from the LSPR effect, was believed to have accelerated the transfer of hot electrons in the Ag-Si nanoparticles and promoted the separation of electron-hole pairs in MgO/ZnO. Furthermore, the visible-light absorbance was increased by Ag loading, thereby improving the photocatalytic activity, consistent with the photoluminescence results. The photocatalytic performance of the prepared samples was evaluated in a continuous-flow reactor system using CO₂ as the reactant at temperatures up to



300 °C and atmospheric pressure. The H₂/CO₂ ratio was maintained at 3:1. The results (Fig. 4B–F) showed that CH₃OH was the predominant product. At 160 °C, CH₃OH formation was detected under light irradiation, whereas no CH₃OH was observed under dark conditions. These results suggested that below 160 °C, the Ag–Si/MgO/ZnO nanocrystal superstructures could only catalyze the RWGS reaction. CH₃OH formation was most likely kinetically inhibited at low temperatures and pressures. The highest CH₃OH production rate was obtained at 250 °C, reaching 357.53 μmol g_{cat}⁻¹ h⁻¹ under light illumination (Fig. 4B and 4C). This value at 3 bar was higher than that produced over Si/MgO/ZnO and Si/ZnO composites by factors of 1.12 and 4.7, respectively. The as-prepared Ag–Si/MgO/ZnO photocatalyst exhibited a high apparent quantum yield (AQY) of 21.27% at an excitation wavelength of 420 nm for CH₃OH production, demonstrating its excellent visible-light-driven photocatalytic efficiency. When the temperature was increased to 300 °C, the CH₃OH production rate decreased to 121.84 μmol g_{cat}⁻¹ h⁻¹. This decline was attributed to the exothermic nature of CH₃OH synthesis (Eq. 1), which shifted the equilibrium toward the reactants at higher temperatures according to Le Chatelier's principle. The reaction thermodynamics at 300 °C favored the RWGS pathway, confirming that 250 °C was the optimal temperature for CH₃OH formation.

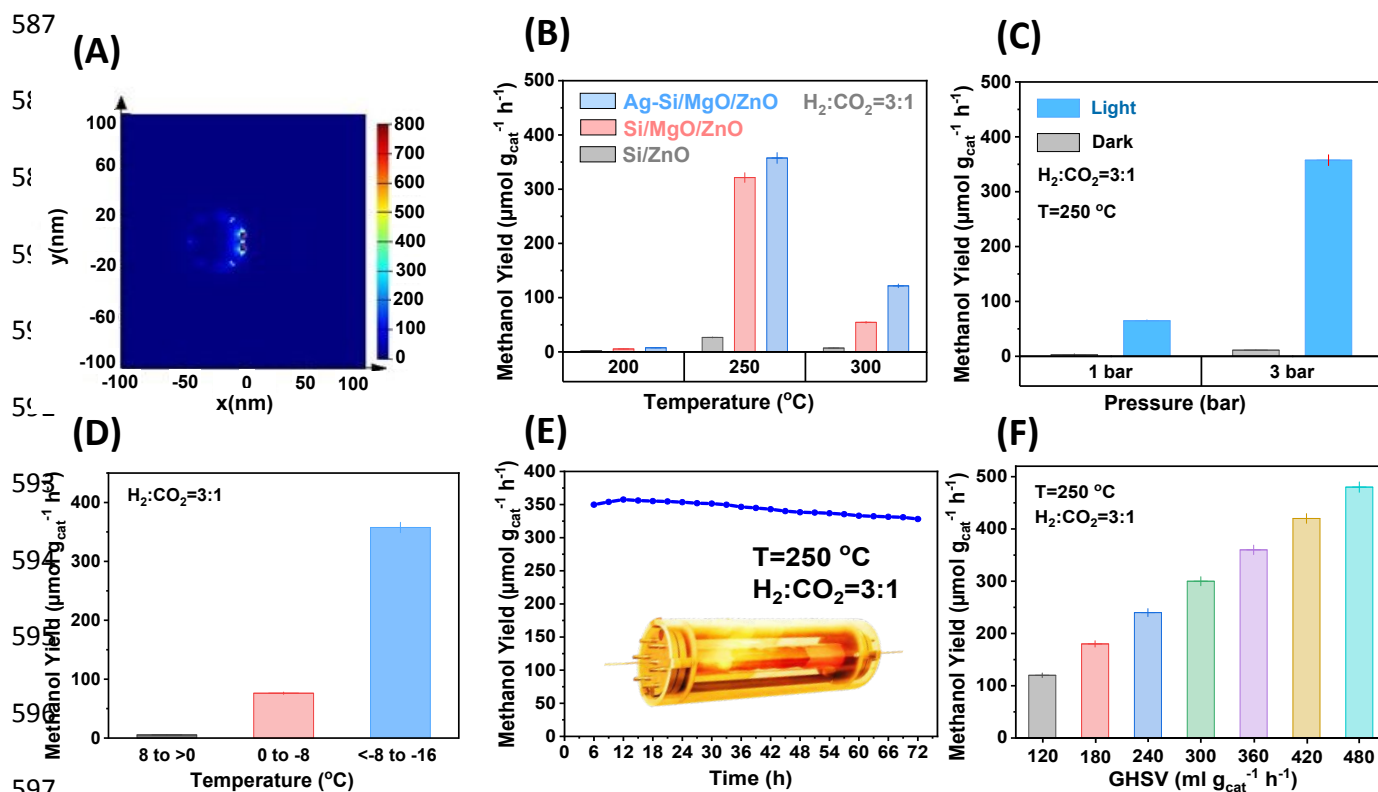




Fig. 4 A) FDTD simulation of the electric field distributions, $|E|^2$ around the surface of Ag-Si nanoparticles placed on MgO/ZnO excited by visible light at wavelength of 457.143 nm. Photo-thermo-catalytic performance: B) Temperature-dependent CH_3OH generation rate over Si/ZnO, Si/MgO/ZnO, and Ag-Si/MgO/ZnO photocatalysts under photo-thermal conditions. C) Influence of pressure on CH_3OH evolution rate over Ag-Si/MgO/ZnO under dark and light conditions; D) Influence of cooling temperature on methanol condensation in the reservoir; E) Stability performance of Ag-Si/MgO/ZnO photocatalyst in photocatalytic CO_2 hydrogenation to CH_3OH during continuous 72h at 250 °C and 3 bar pressure under irradiation of light; F) Methanol production rate as a function of GHSV over Ag-Si/MgO/ZnO; Reaction conditions: 1 g of catalyst, 300 W lamp, 250 °C, and $\text{H}_2:\text{CO}_2 = 3:1$ for Fig. 5(C, E-F).

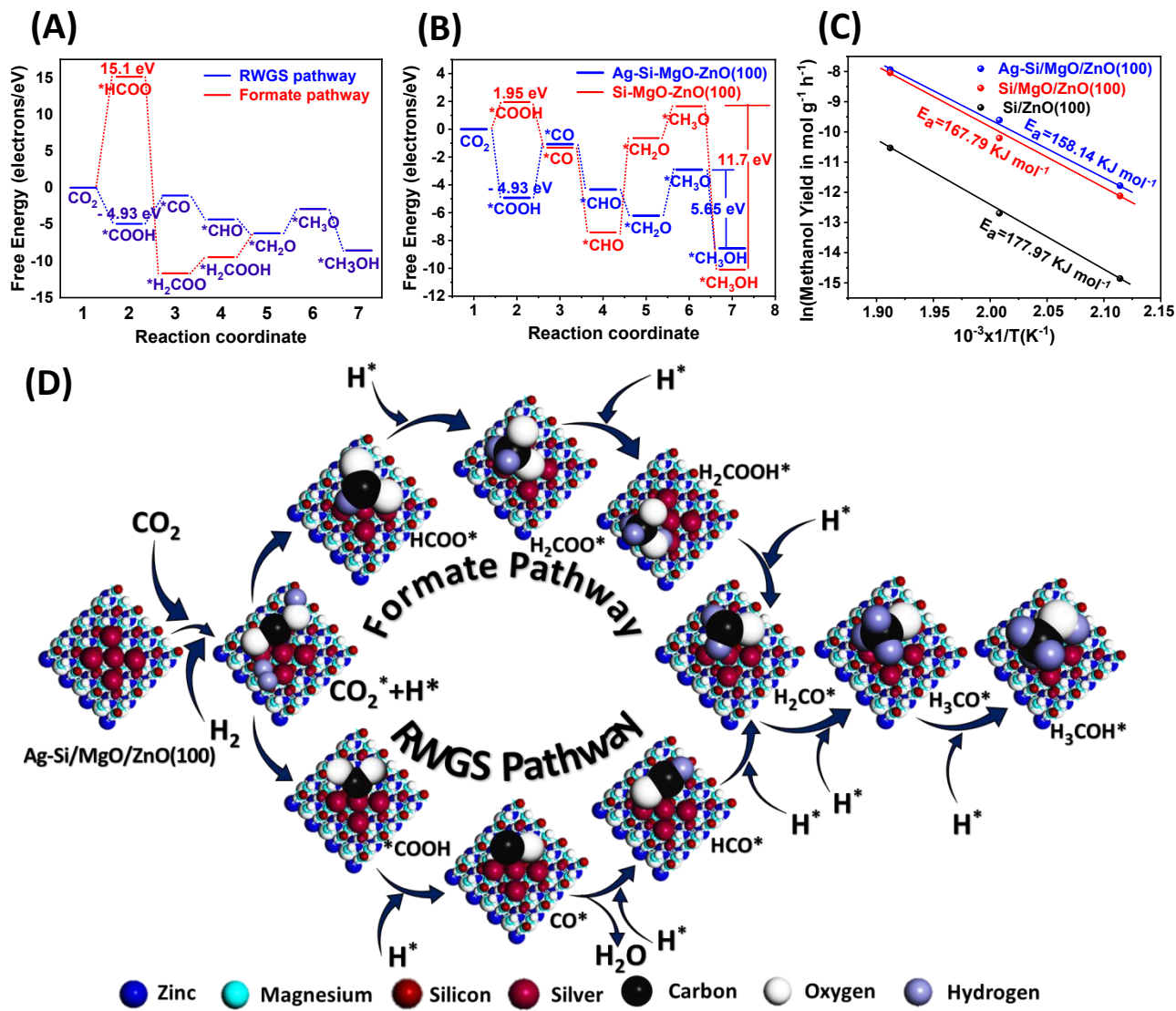


Fig. 5 DFT calculations of CO₂ reduction. (A) Free energy profiles of CO₂ to CH₃OH in different pathways over Ag-Si/MgO/ZnO; (B) Free energy profiles of CO₂ to CH₃OH in COOH pathway over Ag-Si/MgO/ZnO, and Si/MgO/ZnO; (C) Apparent activation energy (E_a) evaluated using Arrhenius plots based on hydrogenation of CO₂ into methanol under light condition; (D) Structural CO₂ hydrogenation pathways for methanol production within Ag-Si/MgO/ZnO interface system.

A preliminary evaluation of the temperature-dependent solar CH₃OH production over Ag-Si/MgO/ZnO is shown in Fig. 2b. The largest amount of CH₃OH was condensed between -8 °C and -16 °C (Fig. 4D). The stability of the Ag-Si/MgO/ZnO photocatalyst was tested during continuous operation for 72 h at 250 °C and 3 bar under light irradiation (Fig. 4E). Only a slight decrease in CH₃OH production rate was observed, indicating excellent long-term stability. CH₃OH production rates of various photocatalysts and comparable systems are listed in Table 2.⁵³⁻⁵⁹ A significant enhancement of CH₃OH generation from 159.84 to 357.53 $\mu\text{mol g}_{\text{cat}}^{-1} \text{h}^{-1}$ achieved when the GHSV was increased from 120 to 480 $\text{ml g}_{\text{cat}}^{-1} \text{h}^{-1}$ at 250 °C and 3 bar (Fig. 4F). This improvement was attributed to the synergistic effect of Ag-Si bimetallic loading, consistent with previous findings by Chen et al.,⁴⁰ who reported that Ag doping effectively suppressed electron-hole recombination and Si increased the catalyst surface area, jointly promoting visible-light photocatalysis. Plasmonic enhancement had been imparted by Ag because the optical response had been extended into the visible region and red-shifted toward ~630 nm after Ag incorporation, and stronger charge separation/transport had been evidenced by pronounced PL quenching, higher transient photocurrent, and a smaller EIS semicircle, indicating that a larger fraction of photoexcited electrons had been delivered to surface reaction sites than in non-plasmonic semiconductor-only systems.⁶⁰ This behavior had contrasted with common strategies such as band-gap narrowing by bulk doping or simple heterojunction formation, where photon harvesting and interfacial electron flux had often remained limited by weak visible absorption or fast recombination; in the present architecture, plasmonic near-field/hot-carrier effects had been expected to raise the local excitation rate and accelerate interfacial electron injection under visible irradiation, thereby increasing the effective electron supply for CO₂/CO activation and hydrogenation.⁶¹



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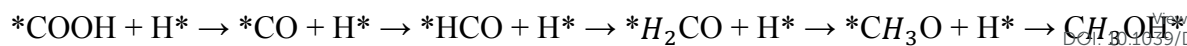
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Table 2: Comparison of heterogeneous photocatalysts for hydrogenation of CO₂ into CH₃OH

Catalysts	T	P	V _{CO₂} :V _{H₂}	Methanol Yield	Reference
Au/In ₂ O ₃	-	-	3:1	320 μmol g _{cat} ⁻¹ h ⁻¹	53
CaCu ₃ Ti ₄ O ₁₂	250 °C	8 bar	3:1	308.5 μmol g _{cat} ⁻¹ h ⁻¹	54
Ru/In ₂ O ₃	-	atmP	3:1	280.4 μmol g _{cat} ⁻¹ h ⁻¹	55
Cu/ZnO	220 °C	atmP	2.5:1	127.8 μmol g ⁻¹ h ⁻¹	56
In ₂ O _{3-x} (OH) _y -NR-14h	250 °C	atmP	3:1	97.30 μmol g _{cat} ⁻¹ h ⁻¹	57
CoO/Co/TiO ₂	120 °C	atmP	3:1	39.6 μmol g _{cat} ⁻¹ h ⁻¹	58
H ₂ In ₂ O _{3-x} (OH) _y	300 °C	atmP	3:1	31.2 μmol g _{cat} ⁻¹ h ⁻¹	59
H ₂ In ₂ O _{3-x} (OH) _y	250 °C	atmP	3:1	14.92 μmol g _{cat} ⁻¹ h ⁻¹	59
Ag-Si/MgO/ZnO	250 °C	3 bar	3:1	357.53 μmol g _{cat} ⁻¹ h ⁻¹	This work

A schematic summary had been proposed in which CO₂ had been adsorbed at basic MgO sites, COOH*/CO* formation had been favored at the Ag-Si/MgO/ZnO and terminal hydrogenation to CH₃OH had been completed predominantly at Ag sites supplied by efficiently separated photoelectrons under visible irradiation. The most favorable pathway for CO₂ hydrogenation to CH₃OH over this interface system was determined. Formate (HCOO*) and carboxyl (*COOH) species were identified as the key intermediates in the HCOO* and RWGS pathways. The Ag-Si/MgO/ZnO(100) system demonstrated the most energetically favorable *COOH pathway, with the lowest barrier (-4.93 eV) and a strongly exothermic reaction energy for CH₃OH formation (-8.55961 eV). In contrast, the HCOO* pathway exhibited a high barrier (15.1 eV) and endothermic CO₂ → HCOO* conversion. Therefore, the *COOH route was identified as the preferred pathway over Ag-Si/MgO/ZnO(100) (Fig. 5A). Starting from *COOH, the Gibbs free-energy profiles for the 6H⁺/6e⁻ reduction of CO₂ to CH₃OH over Ag-Si/MgO/ZnO(100) and Si/MgO/ZnO(100) were analyzed (Fig. 5B). CO₂ hydrogenation to *COOH was exothermic (-4.93 eV) over Ag-Si/MgO/ZnO(100) but endothermic (+1.95 eV) over Si/MgO/ZnO(100), demonstrating the greater favorability of COOH formation in the presence of Ag. Incorporation of MgO enhanced *COOH adsorption, enabling its conversion to *CO, which was readily hydrogenated to methoxy (CH₃O*), as also reported by Li et al.⁶² Compared with Si/MgO/ZnO, Ag-Si/MgO/ZnO had little effect on the free energies of *COOH→*CO, *CO→CHO, or *CHO→*CH₂O. However, the last three proton-transfer steps were identified as the decisive steps controlling performance. It was inferred that the first three intermediates were adsorbed on Si sites, while the final three were stabilized on Ag sites.

Partial density of states (PDOS) analysis at Ag sites demonstrated that Ag facilitated more rapid electron transfer from *CH₂O, accelerating its hydrogenation to *CH₃O. The free energy for the step CH₃O + H⁺ + e⁻ → CH₃OH was reduced to 5.65 eV (Fig. 5B). Overall, CH₃OH formation over Ag-Si/MgO/ZnO proceeded predominantly via the pathway:



which was both kinetically and thermodynamically preferred. This mechanism aligns with the literature reported by Shan et al.,⁶³ where CO₂ was adsorbed and activated to CO₂*, subsequently forming COOH* and CO* and undergoing stepwise hydrogenation to CH₃OH. Both of the final steps were enhanced at the bimetallic sites, indicating that Ag–Si/MgO/ZnO enabled more efficient and selective CO₂ conversion to CH₃OH. The apparent activation energy for Ag–Si/MgO/ZnO was 158.14 kJ mol^{−1}, lower than that of Si/MgO/ZnO (167.79 kJ mol^{−1}) and Si/ZnO (177.97 kJ mol^{−1}) under light irradiation (Fig. 5C). On the contrary, the apparent activation energy for Ag–Si/MgO/ZnO under purely thermal conditions as a reference was 172.48 KJ mol^{−1}, lower than that of Si/MgO/ZnO (184.51 kJ mol^{−1}) and Si/ZnO (201.38 kJ mol^{−1}) under dark condition (Fig. S5). The apparent activation energy that measured when the system is not exposed to light (under dark conditions) is termed as the apparent activation energy under purely thermal conditions. Because the reaction in this scenario entirely drives by thermal energy, it is the appropriate baseline or reference condition to compare with the photo-catalytic conditions (under light irradiation). A comparison of the apparent activation energy (E_a) between light irradiation and dark condition reveals that light significantly reduces the energy barrier for the reaction across all catalysts (Fig. 5C and Fig. S5). Under dark conditions, the reaction relies solely on thermal energy to overcome the activation barrier. The more significant values (172.48 KJ mol^{−1}) to (201.38 KJ mol^{−1}) (Fig. S5) appear the substantial energy required to initiate the reaction without external photonic contribution. However, light irradiation consistently lowers the activation energy through generating electron-hole pairs by using photonic energy. These photo-induced charge-carriers efficiently reduce the thermal threshold needed to achieve the transition state, facilitating redox processes at the surface. In both circumstances, the synergistic impact of adding Ag and MgO further reduces this barrier. The observed reduction of E_a for Si/MgO/ZnO compared to Si/ZnO under both light and dark conditions was triggered by this modification that facilitated charge transfer easier and provided more active sites. Although, Ag can maintain a lower E_a than its non-doped counterparts in the dark by contributing in charge separation through defect levels. However, Ag acts as an electron sink, trapping photo-induced electrons to prevent their recombination with holes, which significantly boosted activity and lowered E_a under light condition. The inclusion of Ag and Si bi-metals in the Ag-Si/MgO/ZnO catalyst creates a multifaceted enhancement that reduced activation energy (E_a) more effectively than single-metal systems. These results indicated that simultaneous Ag and Si doping significantly improved reactant



activation. The DFT calculations were therefore consistent with the experimental activity trends.

Fig. 5D shows the structural CO₂ hydrogenation pathways for methanol production within Ag-Si/MgO/ZnO interface system. Ag and Si had synergistically generated a dual-site catalytic landscape on Ag-Si/MgO/ZnO(100), where the initial CO₂ activation had been promoted through a COOH-mediated route that had been calculated as exothermic on Ag-Si/MgO/ZnO(100) (−4.93 eV) but endothermic on Si/MgO/ZnO(100) (+1.95 eV). This indicates that the bimetallic interface reduced the energy barrier for forming early oxygenated intermediates compared with the Ag-free surface. The decisive hydrogenation sequence had been described as spatially partitioned, such that early intermediates had been preferentially stabilized at Si-associated interfacial/oxide sites while the late hydrogenation steps (CHO* → CH₃OH) had been stabilized at Ag-rich sites acting as electron-accepting and hydrogenation centers,

which had been consistent with the reported DOS features near the Fermi level.⁶⁴ This mechanistic assignment had been directly linked to experimental observables because suppressed recombination and improved charge transport had been evidenced by PL quenching, increased transient photocurrent, and a smaller EIS semicircle for Ag-Si/MgO/ZnO, and the same sample had delivered the highest methanol rate (357.53 μmol g_{cat}^{−1} h^{−1} at 250 °C and 3 bar) with the lowest apparent activation energy (158.14 kJ mol^{−1}), which had been aligned with the computed facilitation of key elementary steps.⁶⁵

4. Conclusion

The Ag and Si-bimetal-doped MgO-promoted ZnO photocatalysts were synthesized via a solid-phase reaction approach. Using the 10 wt.% Ag-Si/MgO/ZnO catalyst, the highest CH₃OH production rate of 357.53 μmol g_{cat}^{−1} h^{−1} was achieved for CO₂ hydrogenation at 250 °C under light illumination. A strong interaction between ZnO and MgO, resulting in a synergistic effect, could be responsible for the excellent selectivity of the 10 wt.% Ag-Si/MgO/ZnO catalyst in the photocatalytic hydrogenation of CO₂ to CH₃OH. No significant deactivation was observed after 72 h of reaction. CO₂ adsorption on the Ag-Si/MgO/ZnO(100) surface (−1.04 eV) was 0.35 eV stronger than on Si/MgO/ZnO(100), which was inferred to have enhanced CO₂ activation and promoted higher CO₂ conversion. The stronger adsorption observed at the Ag-Si/MgO/ZnO(100) interface compared with the Si/MgO/ZnO(100) interface was inferred to enhance CO₂ adsorption, thereby promoting higher CO₂ conversion



over the Ag–Si/MgO/ZnO(100) catalyst. This study thus provides new insights into the rational design of photocatalysts with well-defined heterojunctions for efficient photocatalytic CO₂ reduction.

CRediT authorship contribution statement

AM: Writing – original draft, Methodology, Formal analysis, Data curation; **A-TH:** review & editing, Writing; **MTI:** Writing – review & editing, Validation; **MAH:** Writing – review & editing; **TI:** Writing – review & editing, Writing – original draft, Visualization; **AI:** Writing – review & editing, Writing – original draft, Supervision, Funding acquisition, Conceptualization.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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References:

- 1 P. Ndem, O. Biose, E. Effiong, S. Udegbe, J. E. Ukpebor, I. H. Ifijen and E. E. Ukpebor, Environ. Monit. Assess., 2025, 197(8), 925.
- 2 C. Zhang, J. Fang, Z. Han, P. Chen, X. Xu, K. Wang, Y. Shi and J. Liao, IScience, 2025, 28(8), 113127.
- 3 F. Yan, H. Chen, T. Chi, J. Lu, X. Shen, F. Xie, P. Wang and Z. Zhang, Chem. Eng. J., 2025, 520, 166450.
- 4 J. He, G. Tian, D. Liao, Z. Li, Y. Cui, F. Wei, C. Zeng and C. Zhang, J. Energy Chem., 2025.
- 5 J. Zhao, Z. Wen, R. Zhu, Z. Li, R. Ding, Y. Zhu, T. Gu, R. Yang and Z. Zhu, Chem. Eng. J. Adv., 2020, 3, 100029.
- 6 A. Baig, V. Goswami and Sonal, Asian J. Water Environ. Pollut., 2024, 21(6), 49–57.
- 7 F. A. Rafi, M. M. Rana, B. Agili and A. S. Al Shahrany, Eur. J. Eng. Res., 2025, 5(2), 1–15.
- 8 M. M. Rana, S. M. Alam, F. A. Rafi, S. B. Deb, B. Agili, M. He and M. H. Ali, IEEE Access, 2025.



- 787 9 M. M. Rana, F. A. Rafi, B. Agili and A. S. Al Shahrany, *Eur. J. Electr. Eng. Comput. Sci.*,
788 2024, 8(2), 1–8.
- 789 10 S. Yasar Aurko, R. Salehdin, F. Allahma Rafi and K. Habibul Kabir, Singapore: Springer
790 Nature Singapore, 2023, 277–290.
- 791 11 Y. Yang, C. Shen, K. Sun, D. Mei and C. J. Liu, *ACS Catal.*, 2023, 13(9), 6154–6168.
- 792 12 Q. Wu, S. Liang, T. Zhang, B. Louis and Q. Wang, *Fuel*, 2022, 313, 122963.
- 793 13 C. Clavero, *Nat. Photonics*, 2014, 8(2), 95–103.
- 794 14 M. M. J. Li and S. C. E. Tsang, *Catal. Sci. Technol.*, 2018, 8(14), 3450–3464.
- 795 15 M.L. Brongersma, N.J. Halas and P. Nordlander, *Nat. Nanotechnol.*, 2015, 10(1), 25–34.
- 796 16 K.K. Ng and S.M. Sze, Wiley-Interscience, 2007.
- 797 17 H.A. Atwater and A. Polman, *Nat. Mater.*, 2010, 9(3), 205–213.
- 798 18 W. Sheng, J. Yang, X. Li, G. Liu, Z. Lin, J. Long, S. Xiao, L. Tan and Y. Chen, *Energy*
799 *Environ. Sci.*, 2021, 14(6), 3532–3541.
- 800 19 T. Kong, A. Liao, Y. Xu, X. Qiao, H. Zhang, L. Zhang and C. Zhang, *RSC Adv.*, 2024,
801 14(24), 17041–17050.
- 802 20 J. Zhao, B. Liu, L. Meng, S. He, R. Yuan, Y. Hou, Z. Ding, H. Lin, Z. Zhang, X. Wang and
803 J. Long, *Appl. Catal., B*, 2019, 256, 117823.
- 804 21 A.O. Yusuf, R.Y. Tekle, H.K. Amusa and G. Palmisano, *Case Stud. Chem. Environ. Eng.*,
805 2025, 11, 101172.
- 806 22 M.T. Khalil, X. Wu, S. Liu, Y. Liu, S. Ashraf, R. Shen, H. Zhang, Z. Peng, J. Jiang and B.
807 Li, *Green Chem.*, 2025, 27(30), 9016–9054.
- 808 23 Z.J. Wang, H. Song, H. Pang, Y. Ning, T.D. Dao, Z. Wang, H. Chen, Y. Weng, Q. Fu, T.
809 Nagao and Y. Fang, *Appl. Catal., B*, 2019, 250, 10–16.
- 810 24 J.L.G. Fierro, M.A. Peña and M.C. Alvarez-Galvan, *Supported Metal Catal.*, 2005, 229–
811 255.
- 812 25 V.D. Dasireddy and B. Likozar, *Renewable Energy*, 2019, 140, 452–460.
- 813 26 Q. Chen, S. Meng, R. Liu, X. Zhai, X. Wang, L. Wang, H. Guo and Y. Yi, *Appl. Catal., B*,
814 2024, 342, 123422.
- 815 27 Q. He, Z. Li, D. Li, F. Ning, Q. Wang, W. Liu, W. Zhang, Y. Cui, J. Zhang and C. Liu,
816 *Mol. Catal.*, 2024, 558, 114008.
- 817 28 N. Joshi and S. Loganathan, *ACS Omega*, 2023, 8(14), 13410–13420.
- 818 29 R. Pothu, H. Mitta, P. Banerjee, R. Boddula, R.K. Srivastava, P.K. Kalambate, R. Naik,
819 A.B. Radwan and N. Al-Qahtani, *Mater. Sci. Energy Technol.*, 2023, 6, 484–492.
- 820 30 K. Sun, N. Rui, C. Shen and C.J. Liu, *J. Phys. Chem. C*, 2021, 125(20), 10926–10936.
- 821 31 H. Liu, M. Zhao, J. Guo, S. Sun, D. Li, D. He and Y. Lei, *ACS Sustainable Chem. Eng.*,
822 2025, 13(15), 5787–5795.
- 823 32 X. Zhang, H. Liu, Y. Wang, S. Yang, Q. Chen, Z. Zhao, Y. Yang, Q. Kuang and Z. Xie,
824 *Chem. Eng. J.*, 2022, 443, 136482.
- 825 33 Y. Wang, Y. Liu, L. Tan, X. Lin, Y. Fang, X.F. Lu, Y. Hou, G. Zhang and S. Wang, *J.*
826 *Mater. Chem. A*, 2023, 11(48), 26804–26811.



- 827 34 Y. Wang, B. Su, S. Wang, L. Tan, G. Zhang, Y. Fang and X. Wang, *Angew. Chem. Int. Ed.*, 2025, e202508611. View Article Online
DOI: 10.1039/D3SE01485A
- 829 35 A. Islam, S.H. Teo, M.R. Awual and Y.H. Taufiq-Yap, *J. Cleaner Prod.*, 2020, 244, 118805.
- 830 36 C. Hu, Z. Jiang, Q. Wu, S. Cao, Q. Li, C. Chen, L. Yuan, W. Yang, J. Yang and J. Peng,
- 831 *Nat. Commun.*, 2023, 14(1), 4767.
- 832 37 H. Yu, F. Chen, X. Li, H. Huang, Q. Zhang, S. Su, K. Wang, E. Mao, B. Mei, G. Mul and
- 833 T. Ma, *Nat. Commun.*, 2021, 12(1), 4594.
- 834 38 H.J. Freund and G. Pacchioni, *Chem. Soc. Rev.*, 2008, 37(10), 2224–2242.
- 835 39 S. Chen, B. Lv, D. Wu and Y. Xu, *J. Nanosci. Nanotechnol.*, 2013, 13(2), 1569–1573.
- 836 40 Q. Chen, W. Shi, Y. Xu, D. Wu and Y. Sun, *Mater. Chem. Phys.*, 2011, 125(3), 825–832.
- 837 41 I.H. Alsohaimi, A.M. Nassar, T.A.S. Elnasr and B. Amar Cheba, *J. Cleaner Prod.*, 2020,
- 838 248, 119274.
- 839 42 N.N. Vu, S. Kaliaguine and T.O. Do, *Adv. Funct. Mater.*, 2019, 29(31), 1901825.
- 840 43 N. Ojha, A. Bajpai and S. Kumar, *J. Colloid Interface Sci.*, 2021, 585, 764–777.
- 841 44 N. Ojha, A. Bajpai and S. Kumar, *Catal. Sci. Technol.*, 2019, 9(17), 4598–4613.
- 842 45 S. Tada, F. Watanabe, K. Kiyota, N. Shimoda, R. Hayashi, M. Takahashi, A. Nariyuki, A.
- 843 Igarashi and S. Satokawa, *J. Catal.*, 2017, 351, 107–118.
- 844 46 R. Grabowski, J. Słoczynski, M. Sliwa, D. Mucha, R.P. Socha, M. Lachowska and J.
- 845 Skrzypek, *ACS Catal.*, 2011, 1(4), 266–278.
- 846 47 I.C. Freitas, J.M.R. Gallo, J.M.C. Bueno and C.M. Marques, *Top. Catal.*, 2016, 59(2), 357–
- 847 365.
- 848 48 G.F. Cerofolini, C. Galati and L. Renna, *Surf. Interface Anal.*, 2003, 35(12), 968–973.
- 849 49 S.H. Teo, A. Islam, Y.H. Taufiq-Yap and M.R. Awual, *J. Cleaner Prod.*, 2021, 313, 127909.
- 850 50 P. Devaraji, M. Mapa, H.M. Abdul Hakkeem, V. Sudhakar, K. Krishnamoorthy and C.S.
- 851 Gopinath, *ACS Omega*, 2017, 2(10), 6768–6781.
- 852 51 N.M. Julkapli and S. Bagheri, *Rev. Inorg. Chem.*, 2016, 36(1), 1–41.
- 853 52 F. Meshkani and M. Rezaei, *Catal. Commun.*, 2011, 12(11), 1046–1050.
- 854 53 L. Wang, D. Yao, C. Zhang, Y. Chen, L. Amirav and Z. Zhong, *Chem Catal.*, 2024, 4(9).
- 855 54 Z. Jiang, Z. Yuan, P.N. Duchesne, W. Sun, X. Lyu, W. Miao, C.J.V. Pérez, Y. Xu, D. Yang,
- 856 B. Huang and Y. Dai, *Chem Catal.*, 2023, 3(2).
- 857 55 B. Deng, H. Song, Q. Wang, J. Hong, S. Song, Y. Zhang, K. Peng, H. Zhang, T. Kako and
- 858 J. Ye, *Appl. Catal., B*, 2023, 327, 122471.
- 859 56 Z.J. Wang, H. Song, H. Pang, Y. Ning, T.D. Dao, Z. Wang, H. Chen, Y. Weng, Q. Fu, T.
- 860 Nagao and Y. Fang, *Appl. Catal., B*, 2019, 250, 10–16.
- 861 57 L. Wang, M. Ghoussoub, H. Wang, Y. Shao, W. Sun, A.A. Tountas, T.E. Wood, H. Li,
- 862 J.Y.Y. Loh, Y. Dong and M. Xia, *Joule*, 2018, 2(7), 1369–1381.
- 863 58 Z.H. He, C.S. Jiang, K. Wang, Z.Y. Wang, N. Li, W.T. Wang and Z.T. Liu, *Catal. Today*,
- 864 2020, 356, 579–588.



- 865 59 Z. Zhang, C. Mao, D.M. Meira, P.N. Duchesne, A.A. Tountas, Z. Li, C. Qiu, S. Tang, R.
866 Song, X. Ding and J. Sun, *Nat. Commun.*, 2022, 13(1), 1512. View Article Online
DOI: 10.1039/D3SE01485A
- 867 60 S. Linic, P. Christopher and D.B. Ingram, *Nat. Mater.*, 2011, 10(12), 911-921.
- 868 61 M.L. Brongersma, N.J. Halas and P. Nordlander, *Nat. Nanotechnol.*, 2015, 10(1), 25-34.
- 869 62 K. Li and J.G. Chen, *ACS Catal.*, 2019, 9(9), 7840-7861.
- 870 63 X. Shan, G. Zhang, Y. Zhang, S. Zhang, F. Guo and Q. Xu, *Catalysts*, 2024, 14(11), 756.
- 871 64 J. Greeley, T.F. Jaramillo, J. Bonde, I.B. Chorkendorff and J.K. Nørskov, *Nat. Mater.*,
872 2006, 5(11), 909-913.
- 873 65 Z. Zeng, K.C. Chang, J. Kubal, N.M. Markovic and J. Greeley, *Nat. Energy*, 2017, 2(6),
874 17070.



Data availability statement

The data that support the findings of this study are available from the corresponding authors upon reasonable request.

