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## Cross-scale understanding of cascade electrocatalysis for carbon and nitrogen utilization

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Cascade electrocatalysis is increasingly being recognized as a promising approach for achieving efficient and selective conversion of carbon and nitrogen resources, in response to critical challenges in energy sustainability and environmental management. Compared to conventional single-site systems, cascade pathways are designed to enable spatial and temporal coordination of multiple reaction steps, through which the generation, migration, and transformation of key intermediates can be precisely controlled. In this review, a multiscale perspective is provided, spanning atomic, sub-nanoscale, nanoscale, and macroscopic dimensions. Recent progress is summarized in several representative strategies, including the use of multiple active sites for relay catalysis, the engineering of crystal facets and heterointerfaces, the application of nanoconfinement, and the implementation of tandem reactor systems. Particular emphasis is placed on their applications in CO<sub>2</sub> reduction, nitrate reduction, and urea electrosynthesis. Moreover, state-of-the-art *in situ* characterization techniques are highlighted, through which dynamic insights into catalyst evolution and intermediate behaviour have been obtained. Finally, opportunities are outlined for future development, where rational catalyst design, integrated system construction, and data-driven optimization are expected to further advance cascade electrocatalysis for sustainable chemical transformations.

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## Introduction

Carbon and nitrogen cycles are fundamental processes that govern Earth's climate regulation and resource metabolism.<sup>1–3</sup> However, intensified human activities have profoundly disturbed the equilibrium of these two cycles. In the case of the nitrogen cycle, although the traditional Haber–Bosch process can effectively reduce nitrogen to synthesize ammonia, its high temperature and pressure requirements not only result in enormous energy consumption but also cause severe environmental impacts.<sup>4,5</sup> In contrast, electrochemical approaches, which can achieve the reaction under mild conditions and directly utilize renewable electricity, are considered as more sustainable alternatives. Nevertheless, electrochemical nitrogen reduction suffers from low efficiency due to the strong  $\text{N}\equiv\text{N}$  bond strength ( $945\text{ kJ mol}^{-1}$ ) and resultant high reaction overpotentials.<sup>6–8</sup> Nitrate, with its lower N–O bond dissociation energy, is more readily reduced electrochemically and is viewed as a promising alternative nitrogen source for ammonia synthesis.<sup>9,10</sup> Similarly, the carbon cycle plays a crucial role in addressing climate change and global warming, but excessive  $\text{CO}_2$  emissions have intensified the greenhouse effect, creating an urgent demand for carbon capture and conversion technologies.  $\text{CO}_2$  electroreduction, as a potential carbon resource utilization method, has emerged as a research focus.<sup>11,12</sup> However, both  $\text{CO}_2$  and  $\text{NO}_3^-$  electroreduction reactions involve complex multistep reaction pathways and face challenges such as slow reaction kinetics, poor selectivity, and high energy barriers.<sup>13</sup> Due to thermodynamic and kinetic limitations, traditional single-step electrochemical reduction processes lack sufficient control over key intermediates, thereby leading to low utilization rates and poor product selectivity, which severely hampers the efficient and directional conversion of carbon and nitrogen resources.

Cascade electrocatalysis, a strategy that converts reactants through multiple reaction steps, provides a new approach to address carbon and nitrogen resource utilization challenges. Cascade electrocatalysis refers to the integration of multiple electrocatalytic reaction steps in space and time, where different active sites sequentially transform intermediates, thus overcoming the thermodynamic and kinetic constraints of a single reaction step.<sup>14,15</sup> In microbes, the conversion of  $\text{NO}_3^-$  to  $\text{NH}_3$  is a cascade reaction: nitrate reductase reduces  $\text{NO}_3^-$  to  $\text{NO}_2^-$ , which is then further reduced to  $\text{NH}_3$  by nitrite reductase or nitrogenase.<sup>16–18</sup> Inspired by this, researchers have started applying cascade electrocatalysis to carbon and nitrogen resource utilization. Cascade electrocatalysis allows multiple electrocatalytic reactions to occur in series on a single catalyst surface or within a reaction system, not only overcoming the thermodynamic and selectivity limitations in nitrogen and carbon conversion but also significantly improving reaction efficiency and product selectivity.<sup>19,20</sup> Current research on cascade electrocatalysis primarily focuses on studies at a single scale, such as investigating single-atom catalysis mechanisms at the atomic scale. While such studies help to elucidate the reaction mechanisms of individual active sites, they face

numerous limitations, such as limited compatibility of single active sites and hindered interfacial mass transfer. To address these limitations, cross-scale cooperative effects have drawn increasing attention. In cascade catalytic systems, structural features and reaction behaviors at different scales are closely coupled. At the atomic scale, active sites govern the adsorption and transformation pathways of key intermediates. At the nanoscale, interfacial and confinement structures regulate intermediate migration, short-range spillover, and the local reaction microenvironment. At the reactor scale, mass-transfer rates, electrolyte distribution, and pH collectively dictate overall reaction kinetics and efficiency.<sup>21,22</sup> Integrating these multi-scale strategies enables precise control over the spatiotemporal distribution of reaction intermediates, thereby establishing an efficient and selective cascade pathway for complex multistep reactions. However, this cross-scale research also faces challenges, including the limitations of multiscale modeling and characterization techniques, the complexity of reaction mechanisms, and the challenges of material design. Through a deeper understanding and optimization of cascade electrocatalysis mechanisms at multiple scales, future advancements could offer viable solutions to the global energy crisis and environmental pollution issues.

This review provides a comprehensive assessment of the mechanisms and applications of cascade electrocatalysis from a multiscale perspective (Fig. 1). It begins by elucidating the reaction mechanisms underlying cascade electrocatalysis, encompassing atomic, sub-nanoscale, nanometer, and macroscopic scales. The review then highlights *in situ* characterization techniques employed to study cascade electrocatalysis. Subsequently, it summarizes key advancements in cascade electrocatalytic strategies, including multiple active sites, crystal facets and heterointerfaces, nanoconfinement and tandem reactors with a particular focus on their application in the utilization of carbon and nitrogen resources, such as nitrate reduction reaction ( $\text{NO}_3\text{RR}$ ), carbon dioxide reduction reaction ( $\text{CO}_2\text{RR}$ ), and urea synthesis. Finally, the challenges facing the field of cascade

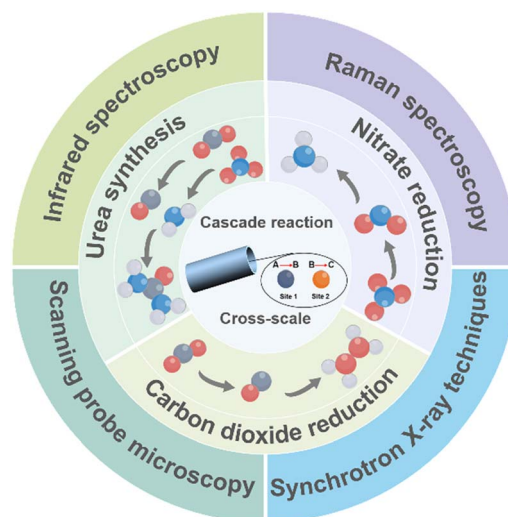


Fig. 1 Cascade electrocatalysis for carbon and nitrogen utilization.



electrocatalysis are discussed, along with a forward-looking perspective on its future prospects, aiming to promote the development of cascade electrocatalysis in the field of electrochemical technologies.

## Cross-scale strategies for cascade electrocatalysis

Cascade electrocatalytic reactions, involving sequential transformations, hold immense potential for efficient resource conversion. However, their mechanistic complexity remains a formidable challenge. At the atomic scale, catalytic behaviour is dictated by single-atom effects and synergistic interactions between multi-atom sites. At the nanoscale, catalytic performance relies on the interplay between surface structure and reactant dynamics. Given the diversity of intermediates and their varied migration pathways, single-scale analyses are insufficient to capture the full mechanistic landscape. Therefore, a comprehensive multiscale approach is indispensable for elucidating the formation, transformation, and coupling of intermediates, thereby laying a robust theoretical foundation for cascade electrocatalysis. This section systematically explores the mechanisms at the atomic, sub-nanoscale, nanoscale, and macroscopic levels (Fig. 2), highlighting the distinct contributions of each to cascade processes.

### Atomic scale: single-atom and dual/multi-atom site interactions

Cascade electrocatalysis achieves high efficiency through consecutive reactions, with atomic-scale insights proving pivotal for optimizing both selectivity and conversion. At this scale, single-atom and dual- and multi-atom site effects govern catalytic performance. Single-atom catalysts (SACs) utilize isolated metal atoms as active centers, exploiting their distinct electronic structures and maximizing atomic utilization to enhance reaction kinetics and selectivity.<sup>23</sup> In the NO<sub>3</sub>RR, SACs provide well-defined active sites and efficient electron transfer pathways, thereby lowering energy barriers and accelerating reaction rates.<sup>24–27</sup> Li *et al.*<sup>28</sup> developed a copper-based single-atom gel (Cu SAGs) catalyst that selectively adsorbs and

activates nitrite intermediates at single-atom sites during the cascade NO<sub>3</sub>RR. This configuration effectively suppresses the competing hydrogen evolution reaction (HER), enabling highly selective NO<sub>3</sub><sup>−</sup> to NH<sub>3</sub> conversion under neutral conditions. This work demonstrates the synergistic integration of pulse electrolysis and three-dimensional (3D) structured SAGs, facilitating highly efficient NO<sub>3</sub><sup>−</sup> to NH<sub>3</sub> conversion *via* tandem catalysis of otherwise unfavorable intermediates.

Beyond single-atom effects, dual- and multi-atom catalysts leverage cooperative interactions between adjacent metal centers to modulate intermediate adsorption and migration, thereby enhancing both activity and selectivity.<sup>29–31</sup> In the CO<sub>2</sub>RR and NO<sub>3</sub>RR, such bimetallic sites can establish energetically favorable tandem pathways.<sup>32</sup> For instance, Xie *et al.*<sup>33</sup> reported a MOF-supported Pd–Cu bimetallic catalyst that promotes CO<sub>2</sub> to C<sub>2+</sub> conversion through a tandem mechanism: Cu facilitates \*CO adsorption and C–C coupling, while Pd stabilizes \*CH<sub>2</sub>CHO intermediates, achieving a C<sub>2+</sub> faradaic efficiency (FE) of 81.9%. Similarly, Yan *et al.*<sup>34</sup> designed a Cu–Ni bimetallic MOF catalyst where Cu reduces NO<sub>3</sub><sup>−</sup> to NO<sub>2</sub><sup>−</sup>, and Ni subsequently converts NO<sub>2</sub><sup>−</sup> to NH<sub>3</sub>. Although SACs exhibit high atom utilization and selectivity, their isolated nature limits the cooperative interactions crucial for multistep transformations.<sup>35</sup> In contrast, dual- and multi-atom configurations enable spatially adjacent, functionally complementary active centers that facilitate sequential intermediate conversion and minimize diffusion losses.<sup>36,37</sup>

### Sub-nanoscale: interfacial effects

At the sub-nanoscale, interfacial effects arising from charge redistribution and atomic coordination at boundaries between distinct catalytic phases play a pivotal role in intermediate stability, charge transfer kinetics, and reaction selectivity.<sup>38</sup> These interfacial regions can significantly influence reaction pathways by modulating local electronic structures and adsorption energetics.<sup>39</sup> Metal–metal interfaces often exhibit catalytic behavior that differs markedly from that of their individual components. As demonstrated by Zhang *et al.*,<sup>40</sup> a well-designed Cu/Ag interface promotes asymmetric CO–CHO coupling: Ag domains generate \*CO intermediates, while the

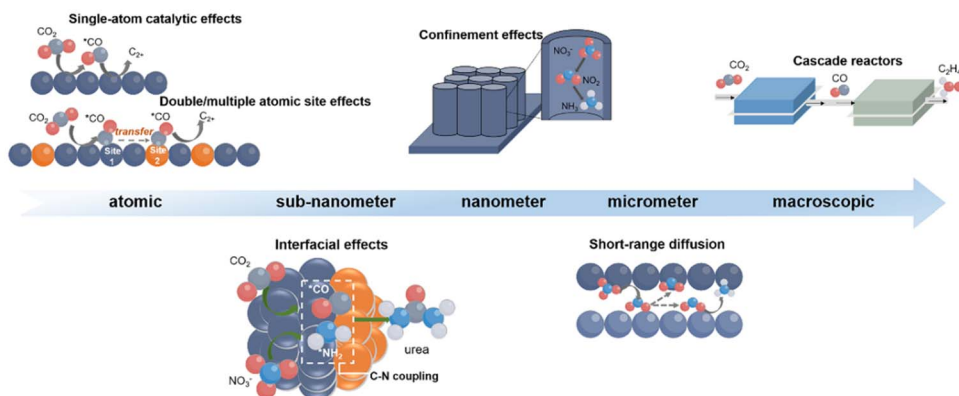


Fig. 2 Mechanistic study of cascade electrocatalytic reactions.



Cu/Ag interface concurrently suppresses the HER, favors  $^*CO$  hydrogenation to  $^*CHO$ , and enhances  $C_2H_4$  formation. Similarly, metal-support interactions can substantially tune electronic states and surface reactivity. Xu *et al.*<sup>41</sup> developed a MOF-derived CuPd/N-doped carbon nanoarrays catalyst, wherein interfacial charge polarization between the metal sites and carbon support facilitates an efficient cascade pathway for the  $NO_3RR$  to  $NH_3$ .

### Nanoscale: confinement effects

Confinement effects in nanostructured catalysts create spatially restricted environments that enhance reactant-site interaction frequency and minimize diffusion distances.<sup>42,43</sup> This spatial confinement accelerates reaction kinetics while suppressing side reactions, thereby improving selectivity.<sup>44</sup> For instance, Qiu *et al.*<sup>45</sup> validated this concept in a nanoconfinement-based cascade denitrification system, utilizing pulsed photocatalysis to mediate chlorine spillover within  $TiO_2$  nanotubes integrated with  $CuO_x$ . In this confined environment, cathodically generated  $NH_4^+$  and photogenerated chlorine radicals ( $^*Cl$ ) are localized in close proximity. The spillover of  $^*Cl$  facilitates the selective oxidation of  $NH_4^+$  to  $N_2$ . This approach demonstrates highly efficient treatment of nitrate-contaminated wastewater and holds great promise for the removal of complex nitrate pollutants from water bodies in future applications.

### Macroscopic scale: reactor cascading

At the macroscopic scale, cascade electrocatalysis can be engineered through reactor-level integration, where sequential reactions are spatially separated into interconnected electrolyzers. In these systems, the first cell produces intermediates that are subsequently converted in downstream reactors under optimized conditions of potential, pH, and electrolyte composition.<sup>46</sup> This modular approach enables precise reaction control and enhanced product selectivity. Ozden *et al.*<sup>47</sup> developed a two-step  $CO_2$  to  $C_2H_4$  system that integrates a solid oxide electrolyzer cell (for  $CO_2$  to  $CO$  conversion) with a membrane electrode assembly (for  $CO$  to  $C_2H_4$  reduction). This configuration minimizes  $CO_2$  loss to carbonate formation and reduces total energy consumption by nearly 48%, achieving efficient ethylene synthesis. Moreover, hybrid cascade systems can further integrate electrochemical, thermocatalytic, or biocatalytic processes. For example, Xia *et al.*<sup>48</sup> presented a tandem electrothermal-catalytic system that efficiently utilizes cathodic  $CO$  and anodic  $O_2$  products in the  $CO_2RR$ , converting arylboronic acids and amines into valuable organic amides within a tandem thermocatalytic reactor. This study demonstrates the feasibility of a tandem electrothermal-catalytic strategy for achieving  $CO_2$  conversion and amide synthesis. It offers a novel pathway for comprehensively exploiting  $CO_2$  electrolysis. In addition, Han *et al.*<sup>49</sup> presented a spatially decoupled electrobiological system that first utilizes tannic acid-Cu<sup>2+</sup> metal-phenolic networks to electrocatalytically convert  $CO_2$  into ethanol. Subsequently, engineered *Escherichia coli* ferment the ethanol into itaconic acid, isopropanol, and

polyhydroxybutyrate, achieving efficient conversion of  $CO_2$  into high-value chemicals.

## Advanced *in situ* techniques for probing cascade reactions

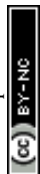
In cascade electrocatalytic reactions, the intricate and interdependent nature of successive reaction steps demands precise coordination among active sites. Achieving a comprehensive understanding of both the underlying reaction mechanisms and the catalyst's performance under working conditions is therefore essential. *In situ* characterization techniques serve as powerful, real-time analytical tools, enabling the direct observation of reaction dynamics. These techniques provide direct insights into the evolution of catalyst surface microstructures and reaction processes, thereby furnishing critical experimental evidence that can inform the optimization of catalytic performance and the design of advanced catalysts. This section highlights several widely utilized *in situ* techniques and underscores their pivotal contributions to advancing cascade electrocatalysis research.

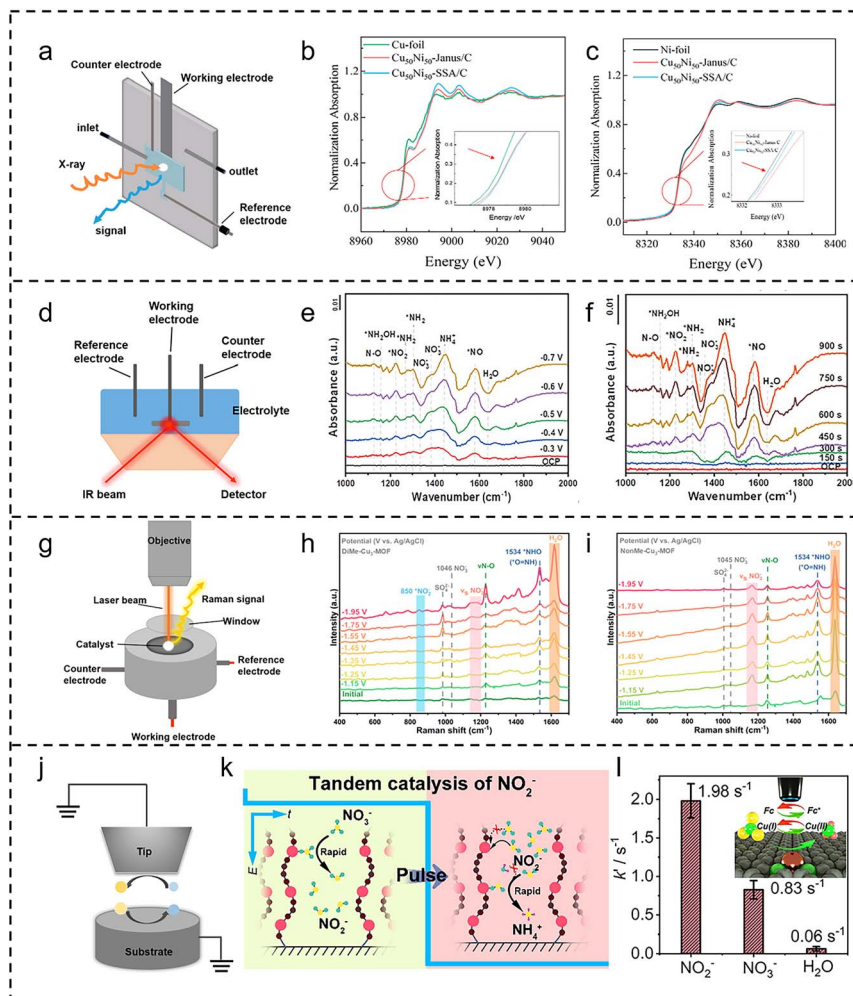
### Synchrotron X-ray techniques

Synchrotron X-ray techniques, particularly X-ray absorption spectroscopy (XAS), have found extensive application in elucidating the electronic structure, oxidation states, and local coordination environments of catalysts (Fig. 3a). Specifically, *in situ* extended X-ray absorption fine structure (EXAFS) analysis enables the tracking of variations in the coordination environments of absorbing atoms under reaction conditions, thus facilitating the determination of atomic coordination states. Concurrently, *in situ* X-ray absorption near-edge structure (XANES) offers insights into potential-dependent chemical state changes.<sup>50–52</sup> In cascade electrocatalysis, XAS is instrumental in monitoring valence state evolution within tandem catalysts across multiple reaction stages, thereby providing mechanistic insights for each step.<sup>53</sup> For instance, Lou *et al.*<sup>54</sup> employed XAS to quantitatively analyze the atomic structure of a Janus Cu@Ni catalyst (Fig. 3b and c). EXAFS confirmed the distinct Cu- and Ni-enriched domains, while XANES, in conjunction with XPS, revealed electron transfer from Ni to Cu. These findings corroborated a tandem mechanism, wherein  $NO_3^-$  adsorption and activation occur on Cu sites, while H species generated on Ni sites migrate to the interface, facilitating N–O bond cleavage. Such studies elucidate the intrinsic nature of multi-site synergy and cascade reaction mechanisms at the electronic level, advancing our understanding of the coupling between charge transfer and reaction pathways in catalytic processes.

### Infrared spectroscopy

Fourier-transform infrared spectroscopy (FTIR) detects molecular vibrations *via* infrared absorption at characteristic frequencies, offering real-time, molecular-level insights into the chemical species involved in electrocatalytic processes.<sup>57,58</sup> Fig. 3d illustrates a schematic of the FTIR setup. Within cascade electrocatalytic systems, this technique allows for the direct





**Fig. 3** *In situ* characterization techniques. (a) Schematic diagram of *in situ* XAS. (b) Cu K-edge and (c) Ni K-edge XANES spectra of Cu<sub>50</sub>Ni<sub>50</sub>-Janus/C, Cu<sub>50</sub>Ni<sub>50</sub>-SSA/C, and reference samples. Reproduced with permission.<sup>54</sup> Copyright 2024, American Chemical Society. (d) Schematic diagram of *in situ* FTIR spectroscopy. *In situ* FTIR spectra of Cu<sub>5</sub>/Mo<sub>0.6</sub>WO<sub>3</sub> (e) from OCP to  $-0.7$  V vs. RHE, and (f) from OCP (0 s) to 900 s at  $-0.7$  V vs. RHE. Reproduced with permission.<sup>55</sup> Copyright 2025, Wiley-VCH. (g) Schematic diagram of *in situ* Raman spectroscopy. *In situ* Raman spectra of (h) DiMe-Cu<sub>3</sub>-MOF and (i) NonMe-Cu<sub>3</sub>-MOF at various applied potentials in 50 mM KNO<sub>3</sub> and 0.5 M K<sub>2</sub>SO<sub>4</sub> electrolytes. Reproduced with permission.<sup>56</sup> Copyright 2025, Royal Society of Chemistry. (j) Schematic diagram of *in situ* SECM. (k) Schematic diagram of the NO<sub>3</sub>RR via pulse electrolysis cascade catalysis. (l) Kinetic rate constants of NO<sub>2</sub><sup>-</sup>, NO<sub>3</sub><sup>-</sup>, and H<sub>2</sub>O adsorption on Cu SAGs determined with SI-SECM. Reproduced with permission.<sup>28</sup> Copyright 2023, American Chemical Society.

monitoring of adsorbed reactants, intermediates, and products on electrode surfaces, facilitating the identification of intermediate species within the cascade pathway and their transformation processes. When integrated with complementary techniques, FTIR can effectively track the formation, conversion, and consumption of key intermediates, offering crucial evidence for understanding reaction kinetics, electron transfer, and molecular interactions.<sup>59</sup> Dai *et al.*<sup>55</sup> utilized FTIR to confirm the cascade mechanism of a Cu/Mo-WO<sub>3</sub> catalyst, dynamically capturing the spectral evolution of key intermediates. The depletion of certain peaks and the emergence of new ones provided real-time evidence of NO<sub>3</sub><sup>-</sup> reduction to NO<sub>2</sub><sup>-</sup> and subsequent conversion to NH<sub>3</sub>, validating the proposed stepwise mechanism (Fig. 3e and f). Such real-time spectral tracking under *operando* conditions underscores the power of FTIR in unraveling complex cascade reaction pathways.

### Raman spectroscopy

Raman spectroscopy, which integrates laser excitation with electrochemical measurements, provides valuable information on chemical composition and molecular structure by detecting characteristic shifts in scattered light (Fig. 3g).<sup>60,61</sup> This technique offers real-time tracking of intermediates, enabling the precise tracking of pathway changes in complex cascade reactions.<sup>62</sup> Such molecular-level insight is essential for correlating structural dynamics with the optimization of catalytic performance. For instance, Fu *et al.*<sup>56</sup> utilized Raman spectroscopy to monitor the characteristic peaks of the NHO intermediate and dynamic Cu-N bond variations on DiMe-Cu<sub>3</sub>-MOF and NonMe-Cu<sub>3</sub>-MOF surfaces (Fig. 3h and i). Based on the Raman results, the \*NHO intermediate was detected on both DiMe-Cu<sub>3</sub>-MOF and NonMe-Cu<sub>3</sub>-MOF, whereas the \*NOH intermediate was not



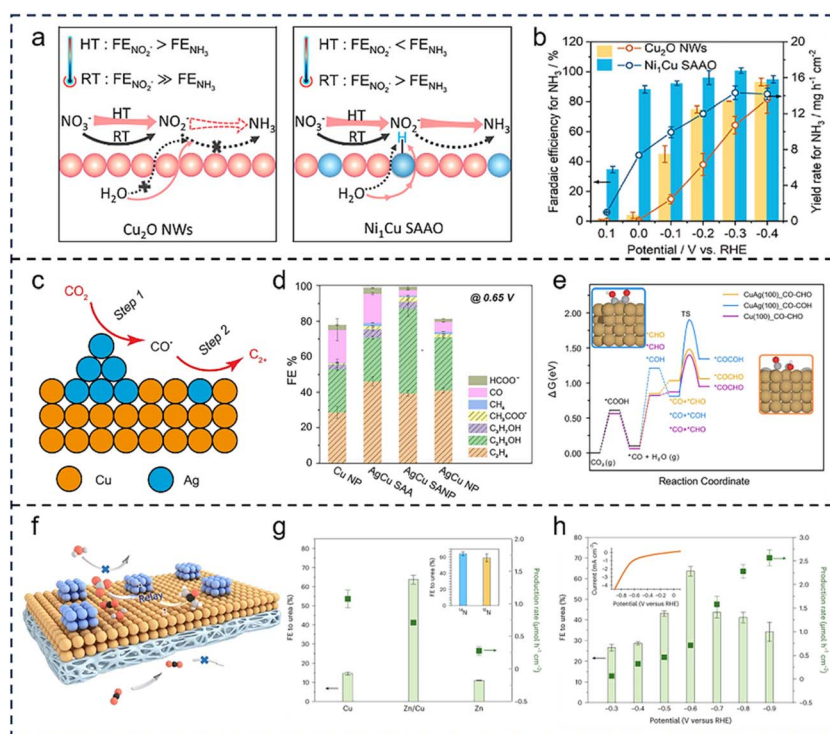
detected, indicating that  $\text{NO}_3^-$  is reduced to  $\text{NH}_3$  *via* the NHO pathway. Combined with DFT calculations, the results revealed a 0.32 eV reduction in the energy barrier for  $^*\text{NO}_2$  to  $^*\text{NO}_2\text{H}$  conversion through hydrogen bonding, thus optimizing the cascade pathway toward highly selective and industrially relevant  $\text{NO}_3\text{RR}$  to  $\text{NH}_3$  conversion.

### Scanning probe microscopy

Scanning electrochemical microscopy (SECM) is a high-resolution *in situ* electrochemical imaging technique that enables the study of local surface reactivity with micrometer spatial and millisecond-scale temporal resolution (Fig. 3j).<sup>63,64</sup> Using micro- or nanoelectrode probes, SECM quantifies current responses between the probe and the substrate, allowing real-time mapping of localized reaction activity, kinetics, and intermediate distribution.<sup>65</sup> In cascade electrocatalysis, SECM is particularly useful for visualizing how intermediates form and dissipate at different active sites. For example, in  $\text{NO}_3\text{RR}$  and  $\text{CO}_2\text{RR}$ , SECM has been employed to track key intermediates such as  $\text{NO}_2^-$  and  $\text{CO}$ , elucidating reaction coupling between spatially separated active centers.<sup>66–68</sup> He *et al.*<sup>69</sup> utilized the surface generation-tip collection (SG-TC) mode to detect  $\text{NO}_2^-$  and  $\text{NH}_3$  formed on a  $\text{Cu}/\text{Co}(\text{OH})_2$  model catalyst during  $\text{NO}_3^-$  electroreduction.  $\text{NH}_3$  generation significantly increased at the

$\text{Cu}-\text{Co}(\text{OH})_2$  interface, accompanied by a marked decrease in  $\text{NO}_2^-$  production. These results confirmed that  $\text{NO}_2^-$  preferentially forms on Cu sites and subsequently diffuses to adjacent  $\text{Co}(\text{OH})_2$  sites, where it undergoes further reduction to  $\text{NH}_3$  *via* a tandem process. In another study, Li *et al.*<sup>28</sup> employed surface interrogation scanning electrochemical microscopy (SI-SECM) to demonstrate that a Cu SAG catalyst exhibited a substantially higher adsorption affinity for  $\text{NO}_2^-$  than for  $\text{NO}_3^-$  or  $\text{H}_2\text{O}$  (Fig. 3k and l). This finding established a potential-dependent cascade mechanism, where intermediate accumulation was observed at low potentials followed by efficient conversion to  $\text{NH}_3$  at high potentials, enabling highly efficient  $\text{NO}_3\text{RR}$ .

In addition to these techniques, *in situ* electron microscopy, such as liquid-cell transmission electron microscopy (TEM), is emerging as a powerful approach for visualizing catalyst structural evolution during electrochemical reactions.<sup>70–72</sup> While its application to cascade electrocatalysis remains limited, it holds significant promise. However, current *in situ* characterization methods still face notable limitations. Their temporal and spatial resolutions are often insufficient to fully capture the short-lived intermediates and transient changes at nanoscale active sites during cascade reactions, and it remains challenging to simultaneously resolve the dynamic evolution of catalyst structures and reaction intermediates. Given the strong



**Fig. 4** Relay catalysis with multiple active sites. (a) Schematic diagram of the electrothermal synergistic effect of  $\text{Cu}_2\text{O}$  NWs and  $\text{Ni}_1\text{Cu}$  SAO in the  $\text{NO}_3\text{RR}$  process. (b) FE and yield of  $\text{NH}_3$  for  $\text{Cu}_2\text{O}$  NWs and  $\text{Ni}_1\text{Cu}$  SAO at different applied potentials. Reproduced with permission.<sup>94</sup> Copyright 2024, American Chemical Society. (c) Scheme of the cascade catalysis mechanism over  $\text{AgCu}$  SANP. (d) FE results of Cu NP,  $\text{AgCu}$  SAA,  $\text{AgCu}$  SANP, and  $\text{Ag}$  NP catalysts toward the  $\text{CO}_2\text{RR}$  at  $-0.65$  V. (e) Comparison of the C–C coupling activation barrier for the  $^*\text{CHO}$  (on CuAg and pure Cu) and  $^*\text{COH}$  intermediates (CuAg). Reproduced with permission.<sup>96</sup> Copyright 2023, Springer Nature. (f) Mixed catalyst design where one component (blue) lowers the activation energy for C–N bond formation, and the second component (orange) reduces the activation energy for protonation steps required for urea formation. (g) Zn/Cu hybrid catalyst and its single-component counterparts for urea FE. (h) FE and yield of urea on the Zn-0.5/Cu hybrid catalyst at different applied potentials. Reproduced with permission.<sup>1</sup> Copyright 2023, Springer Nature.



complementarity among different *in situ* techniques, a comprehensive understanding of cascade electrocatalytic mechanisms requires the combined use of multiple *in situ* methods to compensate for individual weaknesses and to investigate the reaction from distinct temporal and spatial perspectives. For example, coupling synchrotron-based X-ray methods with *in situ* vibrational spectroscopy enables the concurrent tracking of catalyst structural evolution and the formation and consumption of intermediates. Moreover, advancing *in situ* techniques with higher temporal and spatial resolution, such as ultra-high-resolution SECM, will provide powerful tools for probing mechanistic pathways in greater detail.

## Recent progress on cascade electrocatalysis

Carbon and nitrogen resource utilization is a pivotal link in advancing sustainable energy and green chemistry.<sup>73–75</sup> However, typical CO<sub>2</sub>RR, NO<sub>3</sub>RR, and their coupled reactions

often involve multi-electron/proton transfers and the dynamic migration of various reaction intermediates. This presents a series of challenges, including sluggish reaction kinetics, complex competitive pathways, and low product selectivity.<sup>22,76–84</sup> Traditional single-step electrocatalysis often suffers from intermediate accumulation, low energy efficiency, and limited product selectivity in these reactions. In contrast, cascade electrocatalysis, where multiple reaction steps are spatially and temporally integrated, offers a new avenue for efficient carbon–nitrogen resource utilization by enabling effective intermediate generation, transport, and transformation. This section discusses recent advancements in cascade electrocatalytic systems targeting carbon and nitrogen resource conversion.

### Relay catalysis with multiple active sites

The strategy of relay catalysis with multiple active sites leverages the different selectivities of various sites for specific reaction steps, decoupling elementary steps within complex reaction

Table 1 Summary of multiple active site catalysts

Catalyst	Mechanism	Electrolyte	Potential	FE
Cu <sub>2</sub> O–CoPO-2 (ref. 88)	Cu <sub>2</sub> O: NO <sub>3</sub> <sup>−</sup> → NO <sub>2</sub> <sup>−</sup> CoPO: H <sub>2</sub> O → *H	0.1 M NO <sub>3</sub> <sup>−</sup> + 1.0 M KOH	−0.37 V vs. RHE	95%
Ru–Ni nanosheets (ref. 89)	Ru: NO <sub>3</sub> <sup>−</sup> → *HONO Ni: *HONO + *H → NH <sub>3</sub>	0.1 M K <sub>2</sub> SO <sub>4</sub> + 0.002 M KNO <sub>3</sub>	−0.8 V vs. RHE	96%
TTA–TPH–CuCo (ref. 98)	Cu: NO <sub>3</sub> <sup>−</sup> → NO <sub>2</sub> <sup>−</sup> Co: NO <sub>2</sub> <sup>−</sup> → NH <sub>3</sub>	0.5 M K <sub>2</sub> SO <sub>4</sub> + 0.3 M KNO <sub>3</sub>	−0.75 V vs. RHE	92%
Ag <sub>30</sub> Pd <sub>4</sub> nanocluster (ref. 93)	Ag: NO <sub>3</sub> <sup>−</sup> → NO <sub>2</sub> <sup>−</sup> Pd: NO <sub>2</sub> <sup>−</sup> → NH <sub>3</sub>	1.0 M NaOH + 1500 ppm NO <sub>3</sub> <sup>−</sup> -N	−0.6 V vs. RHE	90%
Ni1Cu single-atom alloy oxide nanowires (ref. 94)	Ni: H <sub>2</sub> O → *H Cu: *NO <sub>x</sub> + *H → NH <sub>3</sub>	1.0 M KOH + 0.1 M KNO <sub>3</sub>	+ 0.1 V vs. RHE	80%
Mo <sub>1</sub> Fe <sub>1</sub> Pd dual single-atom alloy (ref. 99)	Mo: NO <sub>3</sub> <sup>−</sup> → NO <sub>2</sub> <sup>−</sup> Fe: NO <sub>2</sub> <sup>−</sup> → NH <sub>3</sub>	1.0 M KNO <sub>3</sub> + 1.0 M KOH	−0.7 V vs. RHE	94%
AgCu single-atom and nanoparticle (ref. 96)	Ag NP: CO <sub>2</sub> → CO AgCu SAA: C–C coupling	1.0 M KOH	−0.65 V vs. RHE	94%
0.2% CoCu single-atom alloy (ref. 100)	Co: CO <sub>2</sub> → CO Cu: C–C coupling	1.0 M KHCO <sub>3</sub>	−1.01 V vs. RHE	51%
Cu <sub>3</sub> N–Ag nanocubes (ref. 97)	Ag: CO <sub>2</sub> → CO Cu: CO → *CHO → C <sub>2</sub> H <sub>4</sub>	1.0 M KOH	−0.7 V vs. RHE	50%
CuO/Ni single atoms (ref. 101)	Ni: CO <sub>2</sub> → CO Cu: CO → C <sub>2+</sub>	1.0 M KOH	−0.892 V vs. RHE	81%
CoCu composite (ref. 102)	Co: CO <sub>2</sub> → CO Cu: CO → C <sub>2</sub> H <sub>5</sub> OH	0.1 M KHCO <sub>3</sub>	−0.8 V vs. RHE	71%
Mo <sub>1</sub> Cu single-atom alloy (ref. 103)	Mo: H <sub>2</sub> O → *H Cu <sup>0</sup> : CO <sub>2</sub> → CO Cu <sup>δ+</sup> : C–C coupling	1.0 M KOH	−1.7 V vs. RHE	86%
Zn/Cu hybrid catalyst (ref. 1)	Zn: stabilize CO <sub>2</sub> NO <sub>3</sub> Cu: lower the protonation barrier of COOHNH <sub>2</sub>	0.1 M KHCO <sub>3</sub> + 500 ppm NO <sub>3</sub> <sup>−</sup> -N	−0.6 V vs. RHE	75%
Zn <sub>1</sub> /In <sub>2</sub> O <sub>3–x</sub> (ref. 83)	In-OV: CO <sub>2</sub> → *CO Zn <sub>1</sub> -OV: NO <sub>3</sub> <sup>−</sup> → *NH <sub>2</sub>	0.1 M KHCO <sub>3</sub> + 0.1 M KNO <sub>3</sub>	−0.7 V vs. RHE	56%
Fe <sub>1</sub> /MoS <sub>2</sub> (ref. 104)	Fe <sub>1</sub> -S <sub>3</sub> : *CO <sub>2</sub> NO <sub>2</sub> → *CO <sub>2</sub> NH <sub>2</sub> MoS <sub>2</sub> : *CO <sub>2</sub> NH <sub>2</sub> → *COOHNH <sub>2</sub>	0.1 M KHCO <sub>3</sub> + 0.1 M KNO <sub>3</sub>	−0.5 V vs. RHE	55%
Mo–PCN-222(Co) (ref. 105)	Co: CO <sub>2</sub> → *CO Mo: NO <sub>3</sub> <sup>−</sup> → *NH <sub>2</sub>	0.1 M KHCO <sub>3</sub> + 50 mM KNO <sub>3</sub>	−0.4 V vs. RHE	34%
CuPd <sub>1</sub> Rh <sub>1</sub> diatomic alloy (ref. 106)	Pd <sub>1</sub> -Cu: *CO <sub>2</sub> NO <sub>2</sub> → *CO <sub>2</sub> NH Rh <sub>1</sub> -Cu: *CO <sub>2</sub> NH <sub>2</sub> → *COOHNH <sub>2</sub>	0.1 M KHCO <sub>3</sub> + 0.1 M KNO <sub>3</sub>	−0.5 V vs. RHE	72%
CuSn composite (ref. 107)	Cu: CO <sub>2</sub> → *CO Sn: NO <sub>3</sub> <sup>−</sup> → *NH <sub>2</sub>	0.1 M KNO <sub>3</sub>	−0.7 V vs. RHE	79%



networks in space. This approach utilizes the cooperative effect between sites to integrate each reaction step in a relay fashion, optimizing the functional complementarity and energy matching between active sites, thereby significantly enhancing overall reaction efficiency and product selectivity.<sup>85,86</sup> In the typical multi-electron and multi-proton transfer process of the NO<sub>3</sub>RR, researchers have successfully achieved precise regulation of reaction pathways and directional transformation of intermediates by rationally designing multiple active site catalysts, significantly improving catalytic performance and opening new avenues for the development of efficient NO<sub>3</sub>RR processes.<sup>87–92</sup> For instance, Qin *et al.*<sup>93</sup> designed an atomically precise Ag<sub>30</sub>Pd<sub>4</sub> bimetallic nanocluster, where Ag sites preferentially adsorb NO<sub>3</sub><sup>−</sup> and efficiently convert it into NO<sub>2</sub><sup>−</sup> intermediates. Subsequently, the NO<sub>2</sub><sup>−</sup> intermediate migrates directionally to the adjacent Pd sites for deep reduction to the final product NH<sub>3</sub>. This study decoupled the NO<sub>3</sub>RR steps and allocated them to Ag and Pd sites, achieving high FE for NH<sub>3</sub> production (>90%). Furthermore, external field control can effectively enhance the relay catalysis of the NO<sub>3</sub>RR *via* multiple active sites. For instance, Liu *et al.*<sup>94</sup> designed a Ni-modified copper oxide single-atom alloy (Ni<sub>1</sub>Cu SAAO) catalyst, which achieved efficient NO<sub>3</sub>RR to NH<sub>3</sub> *via* a thermally-coupled electrocatalytic strategy. The cascade reaction mechanism, shown in Fig. 4a, involved heating (60–80 °C), which significantly promoted the hydrolysis of Ni single-atom sites to generate active hydrogen.

These active hydrogens were relayed to neighboring Cu sites, accelerating the hydrogenation of NO<sub>x</sub> intermediates (*e.g.*, NO<sub>2</sub>) adsorbed on the Cu surface, thereby overcoming the kinetic barriers of NO<sub>x</sub> hydrogenation and the competition with the HER. This catalyst exhibited optimized NH<sub>3</sub> production performance at elevated temperatures, with a FE of approximately 80% and a rate of 9.70 mg h<sup>−1</sup> cm<sup>−2</sup> (Fig. 4b).

In addition, relay catalysis with multiple active sites can significantly promote key processes such as C–C coupling and C–N coupling, enabling the efficient synthesis of high-value multi-carbon or nitrogen-containing compounds.<sup>95</sup> Du *et al.*<sup>96</sup> reported an Ag–Cu bimetallic catalytic system that demonstrated exceptional performance in the CO<sub>2</sub>RR. In this system, Ag nanoparticles efficiently reduced CO<sub>2</sub> to CO, while the Ag sites induced compression strain in the Cu lattice, enhancing the adsorption energy of the \*CO intermediate on the Cu sites and significantly promoting C–C coupling kinetics, thereby achieving a high FE for multi-carbon products (94%) (Fig. 4c–e). Similarly, Luo *et al.*<sup>1</sup> designed a Zn/Cu bimetallic catalyst that further extended the application of tandem catalysis in C–N coupling reactions. As shown in Fig. 4f, the Zn sites preferentially stabilized the key C–N coupling intermediate CO<sub>2</sub>NO<sub>3</sub>, while the Cu sites relayed the reduction of the COOHNH<sub>2</sub> protonation energy barrier. This strategy successfully optimized the reaction pathway and suppressed side reactions, achieving 75% selectivity in simulated wastewater containing 1000 ppm

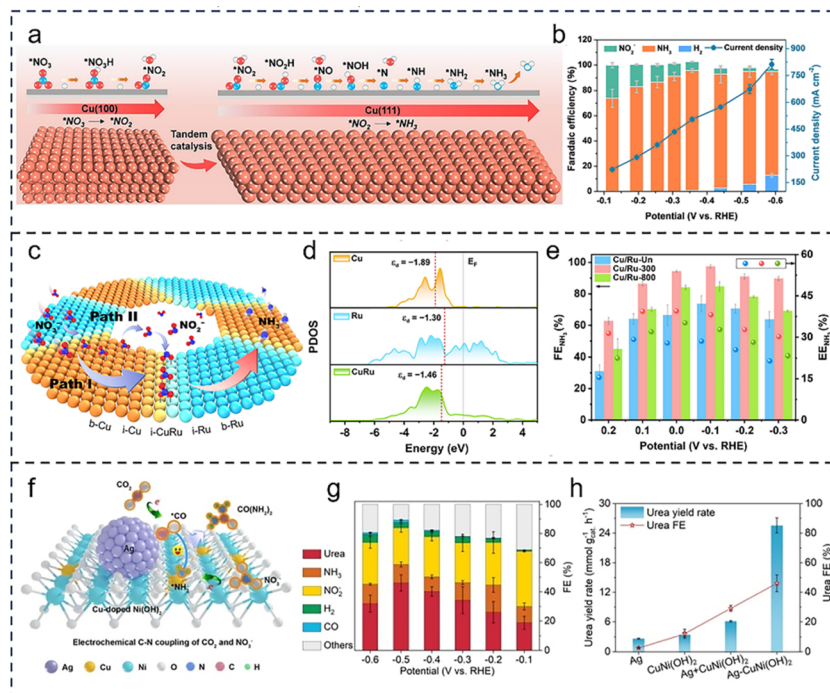


Fig. 5 Crystal facet and heterointerface coupling in cascade catalysis. (a) Synergistic effects between Cu(100) and Cu(111) crystal facets. (b) Total current density and FE of different products on Cu nanosheets. Reproduced with permission.<sup>111</sup> Copyright 2023, Wiley-VCH. (c) Schematic illustration of the proposed mechanism for NO<sub>3</sub><sup>−</sup> to NH<sub>3</sub> conversion on the Cu/Ru HHNS. (d) Projected density of states (PDOS) for b-Cu, b-Ru, and i-CuRu. (e) FE<sub>NH<sub>3</sub></sub> and EE<sub>NH<sub>3</sub></sub> of Cu/Ru-10n, Cu/Ru-300, and Cu/Ru-800 across a potential range of 0.2 to −0.3 V<sub>RHE</sub>. Reproduced with permission.<sup>112</sup> Copyright 2025, American Chemical Society. (f) Schematic diagram of CO<sub>2</sub> and NO<sub>3</sub><sup>−</sup> co-reduction to urea on the Ag–CuNi(OH)<sub>2</sub> electrocatalyst. (g) FE of possible products from the Ag–CuNi(OH)<sub>2</sub> composite material. (h) Comparison of urea yield and FE between Ag NPs, CuNi(OH)<sub>2</sub> NSs, their physical mixture, and Ag–CuNi(OH)<sub>2</sub>. Reproduced with permission.<sup>113</sup> Copyright 2024, Wiley-VCH.



$\text{NO}_3^-$  (Fig. 4g and h). In summary, multi-active-site catalysts can sequentially activate different reactants and intermediates based on the selective specificity of different sites toward reaction steps. This enables them to regulate the energy barriers and pathways of key steps, thereby achieving tandem catalysis for complex reactions. However, cascade strategies based on multiple active sites still face limitations. These include insufficient microenvironmental compatibility between sites, restricted migration of reaction intermediates, and the structural complexity of catalysts, which complicates mechanistic analysis and undermines stability.<sup>97</sup> Integrating multiscale approaches can help align individual steps more effectively and thereby improve the overall efficiency and stability of cascade

reactions. Table 1 summarizes the catalytic processes of various multiple active site catalysts. This strategy provides important theoretical and experimental paradigms for the design of high-performance cascade catalytic systems and the high-value conversion of carbon and nitrogen cycles.

### Crystal facet and heterointerface coupling

The crystal facet and heterointerface cascade catalysis enhances the overall catalytic efficiency by constructing functionally complementary active regions, which collaboratively guide the orientation and coupling of reaction pathways. This synergy optimizes the multiple step reaction energy barriers and the

Table 2 Summary of crystal facet and heterointerface-based cascade catalysts

Catalyst	Mechanism	Electrolyte	Potential	FE
Cu nanosheets (ref. 111)	Cu(100): $\text{NO}_3^- \rightarrow \text{NO}_2^-$ Cu(111): $\text{NO}_2^- \rightarrow \text{NH}_3$	1.0 M KOH + 0.2 M $\text{KNO}_3$	−0.59 V vs. RHE	88%
Cu/Ru hollow heteronanostructure (ref. 112)	Cu: $\text{NO}_3^- \rightarrow \text{NO}_2^-$ Cu/Ru: $\text{NO}_2^- \rightarrow \text{NH}_3$	0.1 M $\text{KNO}_3$ + 0.1 M KOH	−0.1 V vs. RHE	97%
4H/fcc Au–Cu heterostructures (ref. 117)	4H/fcc Au: $\text{NO}_3^- \rightarrow \text{NO}_2^-$ 4H/fcc Cu: $\text{NO}_2^- \rightarrow \text{NH}_3$	1.0 M KOH + 1.0 M $\text{KNO}_3$	−0.6 V vs. RHE	98%
CuO@CeO <sub>2-x</sub> heterostructured nanotubes (ref. 118)	Amorphous CuO: $\text{NO}_3^- \rightarrow \text{NO}_2^-$ Cu–Ce: $\text{NO}_2^- \rightarrow \text{NH}_3$	0.1 M KOH + 0.01 M $\text{KNO}_3$	−0.4 V vs. RHE	96%
c-Co <sub>3</sub> O <sub>4</sub> /a-CuO heterostructure (ref. 119)	a-CuO: $\text{NO}_3^- \rightarrow \text{*NO}_2$ c-Co <sub>3</sub> O <sub>4</sub> : $\text{*NO}_2 \rightarrow \text{NH}_3$	0.2 M $\text{K}_2\text{SO}_4$ + 0.1 M $\text{NO}_3^-$	−0.8 V vs. RHE	90%
Ni@Cu <sub>2-x</sub> Se nanoarrays (ref. 120)	Cu <sub>2-x</sub> Se: $\text{NO}_3^- \rightarrow \text{NO}_2^-$ Interface: modulating *H Ni: $\text{H}_2\text{O} \rightarrow \text{*H}$	1.0 M KOH + 0.1 M $\text{KNO}_3$	−0.4 V vs. RHE	91%
CoO–CuO <sub>x</sub> heterostructure (ref. 121)	CuO <sub>x</sub> : $\text{NO}_3^- \rightarrow \text{*NO}_2$ Interface: promoting the transfer of electrons CoO: $\text{*NO}_2 \rightarrow \text{NH}_3$	0.5 M $\text{Na}_2\text{SO}_4$ + 200 ppm $\text{NaNO}_3\text{-N}$	−0.5 V vs. RHE	92%
Ag–Cu heterostructure (ref. 116)	Ag: $\text{NO}_3^- \rightarrow \text{NO}_2^-$ Interface: facilitating the spillover of intermediates Cu: $\text{NO}_2^- \rightarrow \text{NH}_3$	0.1 M KOH + 0.1 M $\text{KNO}_3$	−0.5 V vs. RHE	>80%
SnO <sub>2</sub> /Cu <sub>6</sub> Sn <sub>5</sub> /CuO nanocatalysts (ref. 122)	Cu <sub>6</sub> Sn <sub>5</sub> /SnO <sub>2</sub> : $\text{CO}_2 \rightarrow \text{*CO}_2^-$ Cu <sub>6</sub> Sn <sub>5</sub> /CuO: $\text{H}_2\text{O} \rightarrow \text{*H}$	0.5 M $\text{NaHCO}_3$	−0.95 V vs. RHE	90%
Ag/Cu self-evolution tandem catalysts (ref. 123)	Ag: $\text{CO}_2 \rightarrow \text{CO}$ Interface: enhancing the adsorption of intermediates Cu: $\text{CO} \rightarrow \text{C}_{2+}$	1.0 M KOH	−1.8 V vs. RHE	89%
Au–Cu heterostructure (ref. 124)	AuCu: $\text{CO}_2 \rightarrow \text{CO}$ Cu: $\text{CO} \rightarrow \text{C}_{2+}$	0.1 M $\text{KHCO}_3$	−0.75 V vs. RHE	—
Au/Cu heterostructure (ref. 125)	Au (110): $\text{CO}_2 \rightarrow \text{*CO}$ Cu(110): $\text{CO} \rightarrow \text{C}_{2+}$	0.1 M $\text{KHCO}_3$	−0.75 V vs. RHE	—
Cu <sub>2</sub> O nanoparticle (ref. 126)	(100): $\text{CO}_2 \rightarrow \text{*CO}$ ; C–C coupling (111): $\text{C}_2\text{H}_4$ overflow	0.2 M KI	−1.3 V vs. RHE	57%
Ag–Cu Janus nanostructures (ref. 127)	Ag domains: $\text{CO}_2 \rightarrow \text{CO}$ Cu domains: $\text{CO} \rightarrow \text{C}_{2+}$	0.1 M $\text{KHCO}_3$	−1.2 V vs. RHE	72%
Ag–Cu biphasic heterostructure (ref. 128)	Ag: $\text{CO}_2 \rightarrow \text{CO}$ Interface: promoting the transport of intermediates Cu: $\text{CO} \rightarrow \text{C}_{2+}$	0.1 M $\text{KHCO}_3$	−1.05 V vs. RHE	44%
Cu/Cu <sub>2</sub> O heterostructures (ref. 129)	$\text{Cu}^0$ : $\text{NO}_3^- \rightarrow \text{*NH}_2$ ; C–N coupling Interface: promoting the transport of intermediates $\text{Cu}^+$ : $\text{*CH}_3\text{CNHCOO}^- \rightarrow \text{*CH}_3\text{CHNH}_2\text{COO}^-$	0.5 M $\text{KNO}_3$ ; 0.2 M PA	−0.6 V vs. RHE	75%
Ag–Cu composite (ref. 130)	Ag: $\text{CO}_2 \rightarrow \text{CO}$ Interface: promoting the transport of intermediates Cu: $\text{CO} \rightarrow \text{C}_{2+}$	3.0 M KOH	−1.0 V vs. RHE	80%



mass transfer of intermediates, ultimately improving catalytic performance. The facet-based cascade strategy involves tuning the exposed crystal facets of the catalyst, leveraging the distinct catalytic properties arising from variations in atomic arrangement, coordination, and electronic structure across different facets. These properties enable the selective catalysis of specific reaction steps.<sup>108–110</sup> Fu *et al.*<sup>111</sup> proposed a crystal facet cascade catalysis strategy, where the Cu(100) and Cu(111) facets cooperatively perform tandem catalysis (Fig. 5a). The Cu(100) facet preferentially adsorbs  $\text{NO}_3^-$  and efficiently reduces them to  $\text{NO}_2^-$ , while the  $\text{NO}_2^-$  intermediate migrates to the adjacent Cu(111) facet for the hydrogenation step. This catalyst achieves a current density of  $665 \text{ mA cm}^{-2}$  for  $\text{NH}_3$  production and a rate of  $1.41 \text{ mmol h}^{-1} \text{ cm}^{-2}$  in a flow cell under  $-0.59 \text{ V vs. RHE}$

(Fig. 5b), significantly enhancing the  $\text{NO}_3\text{RR}$  to  $\text{NH}_3$  performance.

In contrast, the heterointerface cascade strategy capitalizes on the unique local atomic and electronic environments created at the interfaces of different materials due to lattice mismatch, electronic interactions, and other factors. These environments facilitate the effective adsorption and activation of reactants and intermediates.<sup>114,115</sup> For example, Chen *et al.*<sup>112</sup> demonstrated a Cu/Ru heterointerface shell-core nanocavity catalyst that enabled efficient cascade electroreduction of  $\text{NO}_3^-$  to  $\text{NH}_3$ , significantly enhancing the reaction rate and selectivity (Fig. 5c–e).  $\text{NO}_3^-$  is first adsorbed and reduced to  $\text{NO}_2^-$  at the Cu site, after which  $\text{NO}_2^-$  desorbs and accumulates in the nanocavity. The accumulated  $\text{NO}_2^-$  is rapidly transferred to the Cu/Ru

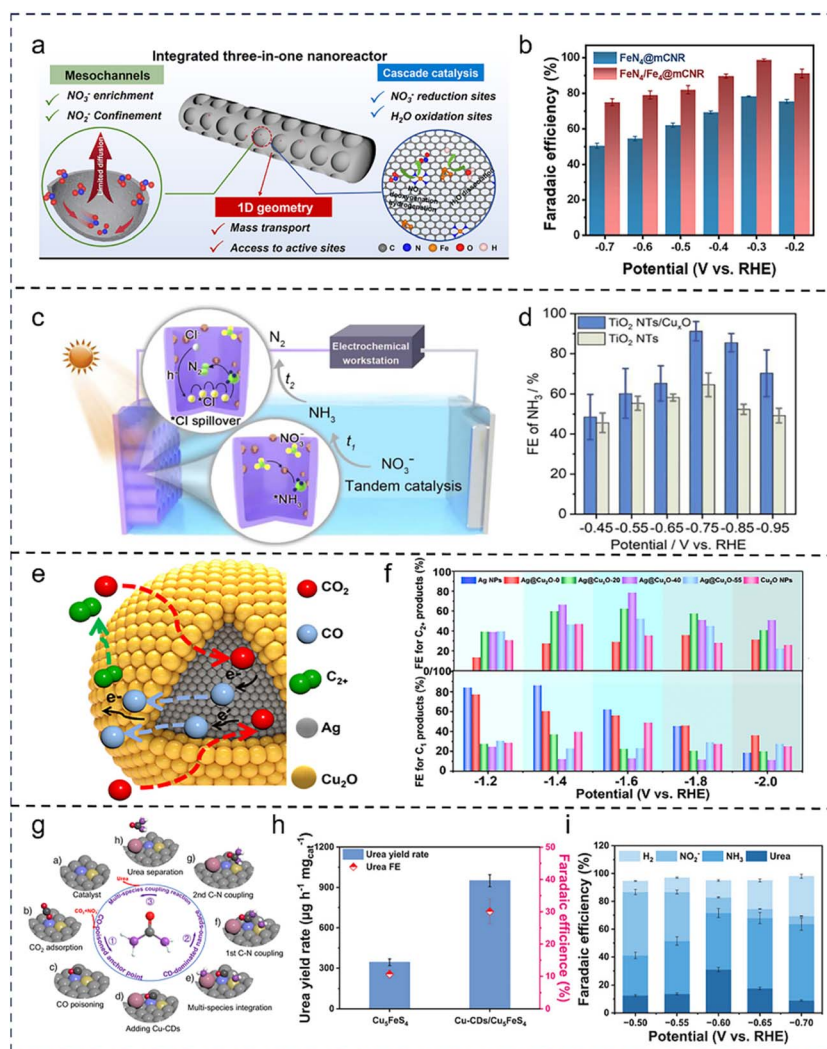


Fig. 6 Nanoconfinement in cascade catalysis. (a) Schematic illustration of the three-in-one nanoreactor design to accelerate  $\text{NO}_3\text{RR}$  to  $\text{NH}_3$  synthesis. (b)  $\text{FE}_{\text{NH}_3}$  of  $\text{FeN}_4@\text{mCNR}$  and  $\text{FeN}_4/\text{Fe}_4@\text{mCNR}$  at varied potentials. Reproduced with permission.<sup>155</sup> Copyright 2025, American Chemical Society. (c) Schematic illustration of  $\text{NO}_3^-$ -to- $\text{N}_2$  process via the pulsed photoelectrolysis-mediated reactive chlorine spillover process. (d) FE of  $\text{NH}_3$  for  $\text{TiO}_2$  NTs and  $\text{TiO}_2$  NTs/ $\text{CuO}_x$ . Reproduced with permission.<sup>45</sup> Copyright 2025, Elsevier B.V. (e) Schematic illustration of the confinement catalysis mechanism in  $\text{Ag}@Cu_2O$  cascade nanoreactors. (f) FE for  $\text{C}_{2+}$  and  $\text{C}_1$  products at various applied potentials. Reproduced with permission.<sup>136</sup> Copyright 2024, American Chemical Society. (g) The Cu-CDs/ $\text{Cu}_5\text{FeS}_4$  multisite nanoreactor for stepwise multiple species coupling to synthesize urea within the CDs-dominated nano-space via utilizing the CO poisoning effect. (h) Urea yield rate and FE of  $\text{Cu}_5\text{FeS}_4$  and Cu-CDs/ $\text{Cu}_5\text{FeS}_4$ . (i) FE of urea,  $\text{NH}_3$ ,  $\text{NO}_2^-$ , and  $\text{H}_2$  of Cu-CDs/ $\text{Cu}_5\text{FeS}_4$  in the H-cell. Reproduced with permission.<sup>137</sup> Copyright 2025, Wiley-VCH.



heterointerface, where it undergoes further reduction to  $\text{NH}_3$ . The Cu/Ru heterointerface facilitates electron transfer from Cu to Ru, improving the adsorption and activation of reaction intermediates at the interface, thus enhancing the utilization of  $\text{NO}_2^-$  intermediates. Moreover, the heterointerface cascade strategy can also be employed to regulate the generation and conversion of active hydrogen intermediates, facilitating C-N coupling reactions for the synthesis of complex carbon-nitrogen compounds. For instance, Ye *et al.*<sup>113</sup> designed an Ag-CuNi(OH)<sub>2</sub> heterostructure that efficiently catalyzed urea electrosynthesis. As shown in Fig. 5f, at the Ag site of the Ag-CuNi(OH)<sub>2</sub> catalyst,  $\text{CO}_2$  is reduced to the critical \*CO intermediate, while at the CuNi(OH)<sub>2</sub> site,  $\text{NO}_3^-$  is reduced to the \*NH<sub>2</sub> intermediate. These intermediates spontaneously couple at the adjacent heterointerface to form urea, while the interface also optimizes the H<sub>2</sub>O splitting process to provide active hydrogen atoms. The Ag-CuNi(OH)<sub>2</sub> composite material achieved an impressive urea production rate of 25.6 mmol g<sup>-1</sup> h<sup>-1</sup> and a FE of 46% (Fig. 5g and h). The cascade catalysis *via* crystal facets and heterointerfaces allows precise control over reaction pathways and intermediate transformations, substantially enhancing the overall efficiency and selectivity of cascade reactions. This approach offers valuable insights into the efficient use of carbon- and nitrogen-based resources and the sustainable synthesis of green chemicals. Although this strategy holds potential for enhancing cascade reaction efficiency, its

practical implementation remains constrained. Differences in adsorption selectivity between crystal facets and interfacial charge redistribution can impede the transfer of intermediates across interfaces. In addition, interfacial reconstruction or fluctuations in the local environment during operation may disrupt the stability of the cascade process.<sup>116</sup> Employing multiscale strategies can reinforce interfacial stability, strengthen the coupling between reaction steps, and improve system scalability, offering new pathways for practical deployment. Table 2 summarizes the catalytic processes of crystal facet and heterointerface-based cascade catalysts.

### Nanoconfinement

Nanoconfinement involves constructing nanoreactors or confined spaces that impose spatial constraints on reactants and intermediates, effectively orchestrating multistep reactions within a limited volume. Confined cascade catalysis capitalizes on these spatial constraints to enhance intermediate retention and proximity, leading to higher reaction rates and selectivity.<sup>131-134</sup> For example, Li *et al.*<sup>135</sup> designed a trifunctional nanoreactor system with a 1D geometry, open mesoporous channels, and synergistic active sites for the highly efficient electrocatalytic  $\text{NO}_3\text{RR}$  to  $\text{NH}_3$  (Fig. 6a and b). The system uses one-dimensional mesoporous carbon as a support, creating a unique microenvironment that favors  $\text{NO}_3^-$  transport and adsorption while restricting the diffusion of  $\text{NO}_x$  intermediates.

Table 3 Summary of the confined cascade catalytic systems

Catalyst	Mechanism	Electrolyte	Potential	FE
FeN <sub>4</sub> /Fe <sub>4</sub> mesoporous carbon nanorod (ref. 135)	Fe-N <sub>4</sub> : $\text{NO}_3^- \rightarrow \text{NO}_2^-$ NO <sub>2</sub> <sup>-</sup> confinement Fe <sub>4</sub> : $\text{H}_2\text{O} \rightarrow \text{*H}$	0.1 M $\text{NO}_3^-$ + 1.0 M KOH	-0.3 V vs. RHE	92%
CuFe@CuNi composite (ref. 140)	CuFe LDH: $\text{NO}_3^- \rightarrow \text{NO}_2^-$ NO <sub>2</sub> <sup>-</sup> confinement CuNi LDH: $\text{NO}_2^- \rightarrow \text{NH}_3$	0.1 M $\text{Na}_2\text{SO}_4$ + 50 ppm $\text{NO}_3^-$ -N	-1.4 V vs. Ag/AgCl	100%
(CoPc-NH <sub>2</sub> + NiPc-OCH <sub>3</sub> )/carbon nanotubes (ref. 141)	NiPc-OCH <sub>3</sub> : $\text{CO}_2 \rightarrow \text{CO}$ CO confinement NiPc-OCH <sub>3</sub> : $\text{CO} \rightarrow \text{CH}_3\text{OH}$	0.1 M KHCO <sub>3</sub>	-0.98 V vs. RHE	50%
Ni sodalite topology/NC (ref. 142)	NiN <sub>3</sub> : $\text{CO}_2 \rightarrow \text{CO}$ CO confinement Cu NPs: $\text{CO} \rightarrow \text{C}_2\text{H}_4$	0.5 M KHCO <sub>3</sub>	-0.72 V vs. RHE	62%
Ag@Cu <sub>2</sub> O cascade nanoreactor (ref. 136)	Ag core: $\text{CO}_2 \rightarrow \text{CO}$ CO confinement Cu <sub>2</sub> O shell: $\text{CO} \rightarrow \text{C}_2^+$	0.1 M KHCO <sub>3</sub>	-1.6 V vs. RHE	78%
CoPc/carbon nanotubes (ref. 44)	CoPc-out: $\text{CO}_2 \rightarrow \text{CO}$ CO confinement CoPc-in: $\text{CO} \rightarrow \text{CH}_3\text{OH}$	0.1 M KHCO <sub>3</sub>	-0.96 V vs. RHE	41%
Ag@Cu <sub>2</sub> O-x nanoreactors (ref. 143)	Ag core: $\text{CO}_2 \rightarrow \text{CO}$ CO confinement Cu <sub>2</sub> O shell: $\text{CO} \rightarrow \text{C}_2^+$	1.0 M KOH	-1.2 V vs. RHE	74%
Ag-Cu nanoporous bimetallic catalyst (ref. 144)	Ag: $\text{CO}_2 \rightarrow \text{CO}$ CO confinement Cu: $\text{CO} \rightarrow \text{C}_2^+$	0.2 M KHCO <sub>3</sub>	-1.2 V vs. RHE	73%
Cu-CDs/Cu <sub>5</sub> FeS <sub>4</sub> nanoreactor (ref. 137)	Fe: $\text{CO}_2 \rightarrow \text{CO}$ C and N intermediate confinement Cu: $\text{NO}_3^- \rightarrow \text{*NH}_2$	0.1 M KNO <sub>3</sub>	-0.35 V vs. RHE	42%
CuCo@N-doped microporous hollow carbon spheres (ref. 145)	Co: $\text{CO}_2 \rightarrow \text{CO}$ C and N intermediate confinement Cu: $\text{NO}_3^- \rightarrow \text{*NH}_2$	0.05 M KNO <sub>3</sub> + 0.1 M KHCO <sub>3</sub>	-0.55 V vs. RHE	32%



Simultaneously, the iron single-atom sites ( $\text{Fe-N}_4$ ) and iron nanoclusters ( $\text{Fe}_4$ ) embedded within the support synergistically control the electronic structure to dominate the reduction of  $\text{NO}_3^-$  and the oxidation of  $\text{H}_2\text{O}$ , respectively. This system demonstrates excellent  $\text{NO}_3\text{RR}$  performance under both alkaline and neutral conditions. Qiu *et al.*<sup>45</sup> confined the intermediate product ( $\text{NH}_4^+$ ) and the active chlorine species ( $\cdot\text{Cl}$ ) within localized regions using  $\text{TiO}_2$  nanotubes (Fig. 6c and d). Leveraging the spillover effect of  $\cdot\text{Cl}$ , they achieved the highly efficient and directed conversion of  $\text{NH}_4^+$  to  $\text{N}_2$ . Furthermore, by precisely controlling the structure of the nanoreactor, the confinement effect can be enhanced, promoting the formation, diffusion, and subsequent utilization of reaction intermediates. For instance, Lu *et al.*<sup>136</sup> synthesized a series of  $\text{Ag}@\text{Cu}_2\text{O}$  cascade nanoreactors with tunable shell thicknesses, where the  $\text{Cu}_2\text{O}$  shell thickness was precisely controlled to achieve spatial confinement of the CO intermediate (Fig. 6e and f). In this system, the Ag core efficiently generates the CO intermediate, which, upon escaping, is confined within the porous  $\text{Cu}_2\text{O}$  shell, significantly increasing the local CO concentration and thus promoting C-C coupling to form  $\text{C}_{2+}$  products. This study not only proposes an effective strategy for fine-tuning the local

CO concentration through precise control of the  $\text{Cu}_2\text{O}$  shell thickness but also provides important theoretical insights into the confinement catalysis mechanisms within cascade nanoreactors.

Moreover, confined cascade catalysis can effectively control the accumulation behavior of toxic intermediates, converting them into beneficial factors and enabling complex reactions involving multiple species.<sup>138</sup> For example, Zhang *et al.*<sup>137</sup> designed a nanoreactor composed of copper-carbon dots (Cu-CDs) and chalcopyrite ( $\text{Cu}_5\text{FeS}_4$ ) for the efficient synthesis of urea (Fig. 6g-i). In this system, Cu-CDs provide confined nano-spaces that stabilize  $\cdot\text{CO}$  intermediates, preventing CO poisoning of the Fe sites. Meanwhile, two structurally distinct Cu sites facilitate the activation and transformation of nitrogen-containing species, driving the continuous C-N coupling steps and ultimately enabling efficient urea synthesis. This system achieved a urea yield of  $1131.84 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  with a selectivity of 42%, significantly enhancing the thermodynamic and kinetic advantages of multiple site synergy and multiple species integration in urea synthesis. These examples demonstrate that nanoscale confinement can markedly influence cascade catalysis by spatially constraining and locally enriching reactive

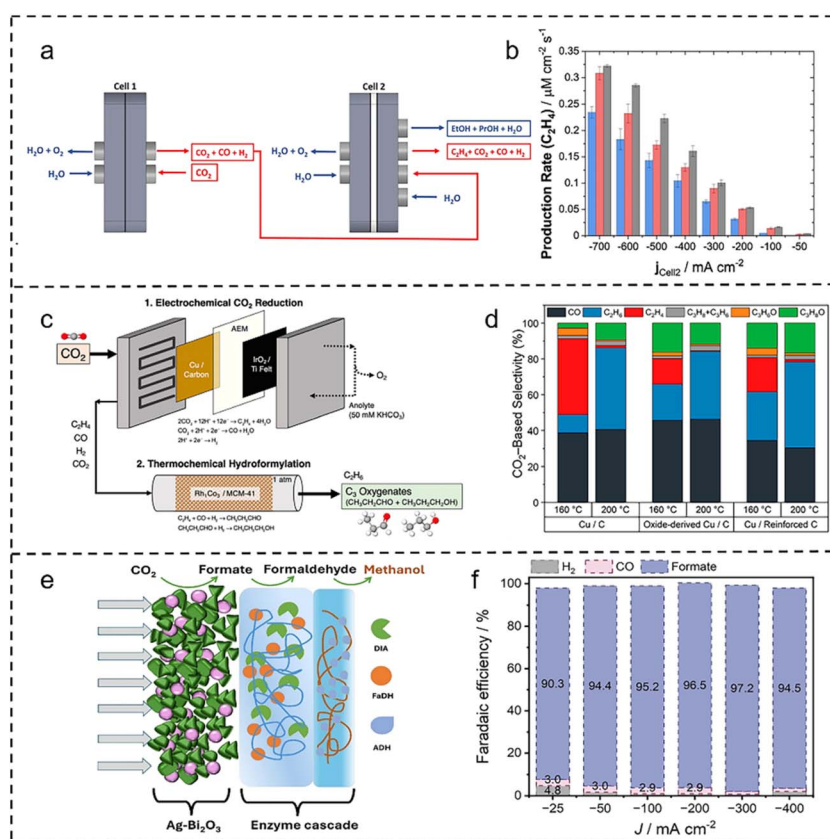


Fig. 7 Tandem reactors. (a) Schematic diagram of the tandem  $\text{CO}_2$  electrolyzer. (b) Comparison of  $\text{C}_2\text{H}_4$  yield between the tandem electrolyzer cascade structure and a single electrolyzer. Reproduced with permission.<sup>147</sup> Copyright 2023, Springer Nature. (c) Tandem electrochemical-thermochemical reactors for  $\text{CO}_2$  conversion to  $\text{C}_3$  oxygenate products. (d)  $\text{CO}_2$ -based selectivity of products for  $5 \text{ cm}^2$  Cu/C, oxide-derived Cu/C, and Cu/reinforced C cathodes at  $-220 \text{ mA cm}^{-2}$  in combination with 160 and 200 °C hydroformylation temperatures. Reproduced with permission.<sup>149</sup> Copyright 2022, American Chemical Society. (e) Hybrid electrocatalytic-bioelectrocatalytic cascade integrated on a gas diffusion electrode for the  $\text{CO}_2\text{RR}$  under selective formation of methanol. (f) FE for the  $\text{CO}_2\text{RR}$  performed with a GDE constituted of  $\text{Ag-Bi}_2\text{O}_3$  nanofibers on a hydrophobic carbon paper. Reproduced with permission.<sup>150</sup> Copyright 2025, Wiley-VCH.



intermediates, thereby promoting desired cascade pathways while suppressing side reactions. Designing catalysts with intrinsic nanoscale confinement or incorporating external confined architectures, such as porous frameworks or core-shell structures, has thus become a key strategy for enhancing the performance of cascade electrocatalytic systems.

Table 4 Summary of tandem reactors

Cascade system	Catalyst	Mechanism	Electrolyte	Reaction conditions
Electrochemical-electrochemical	Ni-N-C; Cu (ref. 147)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 0.1 M KHCO <sub>3</sub>	Cell-1: 200 mA cm <sup>-2</sup>
		Cell-2: CO → C <sub>2+</sub>	Cell-2: 1.0 M KHCO <sub>3</sub>	Cell-2: 700 mA cm <sup>-2</sup>
	Graphite flakes (ref. 148)	Cell-1: CO <sub>2</sub> → ethanol	Cell-1: 1.0 M KOH	Cell-1: -1.8 V vs. SCE
		Cell-2: ethanol → DEE	Cell-2: 0.5 M H <sub>2</sub> SO <sub>4</sub> ethanol solution	Cell-2: 20 mA cm <sup>-2</sup>
	3D single-atom Ni; Cu <sub>2</sub> O (ref. 152)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 0.5 M KHCO <sub>3</sub>	Cell-1: 140 mA cm <sup>-2</sup>
		Cell-2: CO → <i>n</i> -propanol	Cell-2: 1.0 M KOH	Cell-2: 42.5 mA cm <sup>-2</sup>
	Solid-oxide electrolysis cell; membrane electrode assembly (ref. 47)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 30 wt% aqueous ethanolamine	Cell-1: 815 mA cm <sup>-2</sup>
		Cell-2: CO → C <sub>2</sub> H <sub>4</sub>	Cell-2: 3.0 M KOH	Cell-2: 150 mA cm <sup>-2</sup>
	Ni-N-C; Cu nanoparticle (ref. 153)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 0.5 M K <sub>2</sub> SO <sub>4</sub> + H <sub>2</sub> SO <sub>4</sub>	Cell-1: 5 A
	Ni-Cu; Cu-Al (ref. 154)	Cell-2: CO → C <sub>2+</sub>	Cell-2: 0.5 M KOH	Cell-2: 4 A
Cell-1: CO <sub>2</sub> → CO		Cell-1: 1.0 M KOH	Cell-1: 400 mA cm <sup>-2</sup>	
Electrochemical-thermochemical	Cu; Rh <sub>1</sub> Co <sub>3</sub> /MCM-41 (ref. 149)	Cell-1: CO <sub>2</sub> → C <sub>2</sub> H <sub>4</sub>	Cell-1: 50 mM KHCO <sub>3</sub>	Cell-1: 220 mA cm <sup>-2</sup>
		Cell-2: C <sub>2</sub> H <sub>4</sub> → C <sub>3</sub>	Cell-2: —	Cell-2: 160, 200 °C
	Pd/C; FeCo (ref. 155)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 50 mM KHCO <sub>3</sub>	Cell-1: 150 mA cm <sup>-2</sup>
		H <sub>2</sub> O → H <sub>2</sub> Cell-2: CO <sub>2</sub> , H <sub>2</sub> → CNF	Cell-2: —	Cell-2: 450 °C
	Ag-hexamethylenetetramine/Ni-hydroxide carbonate; Pd(II) (ref. 48)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 0.5 M KHCO <sub>3</sub>	Cell-1: -0.8 V vs. RHE
		H <sub>2</sub> O → H <sub>2</sub> Cell-2: CO <sub>2</sub> , O <sub>2</sub> → organic amides	Cell-2: —	Cell-2: 120 °C
	Rh/Sm <sub>x</sub> Ce <sub>1-x</sub> O <sub>2-δ</sub> (ref. 156)	Cell-1: H <sub>2</sub> O → H <sub>2</sub>	Cell-1: acceptor-doped LaGaO <sub>3</sub>	Cell-1: 300–500 mA cm <sup>-2</sup>
		Cell-2: CO <sub>2</sub> + CH <sub>4</sub> → CO + H <sub>2</sub>	Cell-2: —	Cell-2: 800 °C
	Membrane electrode assembly; Ga/ZSM-5/P (ref. 157)	Cell-1: CO <sub>2</sub> → C <sub>2</sub> H <sub>4</sub>	Cell-1: 0.5 M KHCO <sub>3</sub>	Cell-1: 200 mA cm <sup>-2</sup>
		Cell-2: C <sub>2</sub> H <sub>4</sub> → BTEX	Cell-2: —	Cell-2: 600 °C
Electrochemical-biocatalytic	Ag-Bi <sub>2</sub> O <sub>3</sub> ; dehydrogenase (ref. 150)	Cell-1: CO <sub>2</sub> → formate	Cell-1: 0.1 M phosphate	Neutral PH
		Cell-2: formate → formaldehyde → methanol	Cell-2: —	25–400 mA cm <sup>-2</sup>
	MPN@deCOP@Ag-Cu <sub>2</sub> O; engineered <i>Escherichia coli</i> (ref. 49)	Cell-1: CO <sub>2</sub> → ethanol	Cell-1: 1.0 M KOH	Cell-1: 900 mA cm <sup>-2</sup>
		Cell-2: ethanol → itaconic acid, isopropanol, and PHB	Cell-2: —	Cell-2: ADH, ALDH
	Cu-Ag; <i>Cupriavidus necator</i> (ref. 158)	Cell-1: CO <sub>2</sub> → C <sub>2</sub> oxygenates	Cell-1: 0.1 M KH <sub>2</sub> PO <sub>4</sub>	Cell-1: 300 mA cm <sup>-2</sup>
		Cell-2: C <sub>2</sub> oxygenates → PHB	Cell-2: —	Cell-2: pH 7.0
C/Ag/carbon GDE (ref. 159)	Cell-1: CO <sub>2</sub> → CO	Cell-1: 0.05 M H <sub>2</sub> SO <sub>4</sub> + 3.0 M KCl	Cell-1: 100 mA	
	Cell-2: CO → MCFAs	Cell-2: —	Cell-2: 35 °C, pH 6.2	
Cu/Cu <sub>2</sub> O (ref. 160)	Cell-1: CO <sub>2</sub> → formate	Cell-1: 0.5 M KHCO <sub>3</sub>	Cell-1: 50 mA	
	Cell-2: formate → SCP	Cell-2: —	Cell-2: 37 °C	



Nevertheless, confined cascade strategies still present notable limitations. Excessive confinement may suppress intermediate diffusion and poison active sites. Moreover, precisely constructing confined architectures with appropriate spatial dimensions, pore connectivity, and optimized interfacial chemistry remains challenging.<sup>139</sup> Combining confinement engineering with multiscale approaches enables the coordinated optimization of intermediate transport, interfacial mass transfer, and overall system stability. Table 3 summarizes the performance data for relevant confined cascade catalytic systems.

### Tandem reactors

The strategy of tandem reactors enables the sequential integration of different reaction steps across multiple reactors, where the differential conditions between reactors (*e.g.*, pH, potential, and temperature) can be finely tuned to optimize the reaction environment. This approach enhances both the rate of target product formation and its selectivity.<sup>46,146</sup> For instance, Fig. 7a illustrates a cascaded electrolyzer system in which the reduction of CO<sub>2</sub> to CO and the subsequent reduction of CO to C<sub>2+</sub> are coupled in different electrolyzers.<sup>147</sup> By creating tailored catalytic environments in each electrolyzer, this strategy significantly accelerates the production rate of C<sub>2+</sub> products (Fig. 7b). Chi *et al.*<sup>148</sup> reported a dual electrolyzer cascade system: the first electrolyzer operates under alkaline conditions to electrochemically reduce CO<sub>2</sub> to ethanol, while the second electrolyzer, under acidic conditions, electrooxidizes ethanol and condenses it into the high-value six-carbon compound 1,1-diethoxyethane (DEE). This system achieves a highly efficient and selective conversion from CO<sub>2</sub> to multi-carbon products. The cascading reactor design not only greatly enhances product selectivity but also leads to efficient energy utilization and resource conversion.

Additionally, electrochemical reactors can be coupled with thermocatalytic and biocatalytic reactors, forming hybrid cascaded systems. This strategy effectively overcomes the limitations of single electrochemical transformations, improving reaction efficiency and enabling the synthesis of more complex, high-value products, thereby significantly enhancing the

economic viability of the entire conversion process. For example, Chen *et al.*<sup>149</sup> proposed a cascaded electrochemical-thermochemical strategy in which C<sub>2</sub>H<sub>4</sub> reacts with CO and H<sub>2</sub> to produce propanol and propionaldehyde (Fig. 7c and d). In this approach, CO<sub>2</sub> is first electrochemically reduced to C<sub>2</sub>H<sub>4</sub>, CO, and H<sub>2</sub>, followed by a thermocatalytic hydrogenation–formylation reaction that converts these intermediates into C<sub>3</sub> oxygenated compounds. This cascading method achieves approximately 18% selectivity for C<sub>3</sub> products. Wang *et al.*<sup>150</sup> proposed a system that integrates electrochemical and biocatalytic processes on a gas diffusion electrode for the CO<sub>2</sub>RR (Fig. 7e and f). Under neutral pH conditions, Ag-Bi<sub>2</sub>O<sub>3</sub> selectively reduces gaseous CO<sub>2</sub> to carbonates, which are then further reduced to formaldehyde and methanol by formaldehyde dehydrogenase and alcohol dehydrogenase, respectively. This hybrid reactor cascade not only enhances reaction efficiency but also improves the overall selectivity and sustainability of the system. In summary, the tandem reactor strategy enhances the efficiency and selectivity of complex reactions at the macroscale by optimizing environmental conditions within each reactor and precisely controlling product distribution. Although tandem reactors can optimize reaction environments and regulate product distribution, diffusion limitations in intermediate transport between reactors, system operational complexity, and coupling interference between reaction conditions at different stages still constrain their precise control and efficiency enhancement for multistep reactions.<sup>151</sup> Therefore, integrating multiscale strategies to construct an integrated catalytic system featuring active sites, nanoconfinement, interfacial mass transfer, and reactor series connection enables efficient intermediate transport, thereby enhancing the overall efficiency of cascade reactions. Table 4 summarizes the catalytic performance of tandem reactors.

## Conclusion and outlook

Based on the above, cascade electrocatalysis provides a novel pathway for the efficient conversion of carbon and nitrogen resources through atomic-scale catalyst design, nanoscale structural engineering, and macroscopic reactor integration. This review systematically summarizes the latest advancements

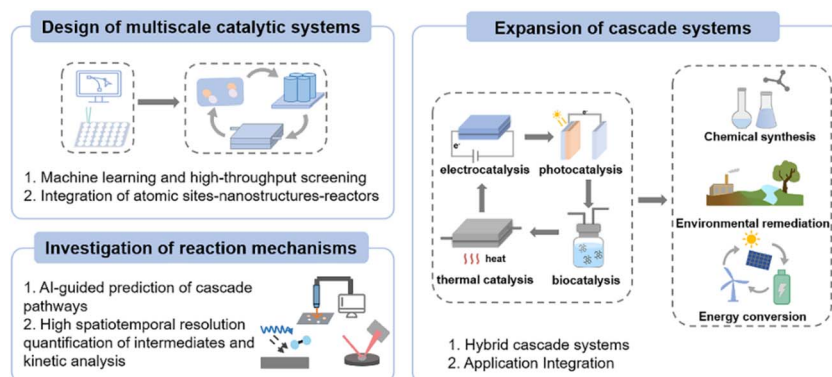


Fig. 8 Schematic illustration of future directions for the development of cascade electrocatalysis.



in this field, delving into the crucial role of the synergistic effects between single-atom/multi-atom sites at the atomic scale, interfacial and confinement effects at the sub-nanoscale and nanoscale, and reactor design at the macroscopic level in enhancing reaction activity and selectivity. Through multiscale cooperative effects, cascade electrocatalysis not only effectively reduces the energy barriers of reactions but also significantly improves reaction selectivity, especially in complex multistep reaction systems, demonstrating unique advantages. Despite substantial progress across various applications, cascade electrocatalysis continues to face several key challenges. Limited compatibility among different active sites constrains the sequential coupling required for efficient cascade pathways. The coexistence of multiple competing reaction routes further complicates selective control over the desired pathway. Moreover, the short lifetimes and low concentrations of critical intermediates hinder real-time detection and impede mechanistic elucidation. Nevertheless, with advances in cross-scale design strategies and *in situ* characterization techniques featuring high temporal and spatial resolution, cascade electrocatalysis is poised to offer broad opportunities for future applications (Fig. 8).

### Design of multiscale catalytic systems

Cascade reactions involve multiple elementary steps and diverse intermediates, with overall efficiency constrained by the synergistic interplay of active site spatial distribution, mass transport processes, and electron transfer kinetics. Therefore, constructing catalysts with a multiscale framework is pivotal for enhancing the performance of cascade reactions. Future research will focus on the deep integration of artificial intelligence with experimental methods, employing machine learning models to predict and optimize the structural features of cascade catalysts. High-throughput synthesis and characterization platforms will be employed for rapid screening, thus establishing a closed-loop research and development cycle encompassing computational design, high-throughput fabrication and testing, and machine learning-driven optimization. The ultimate goal is to construct an integrated catalytic system spanning from atom-level active sites and nanoscale mass transport structures to reactor-scale engineering.

### Investigation of reaction mechanisms

In cascade electrocatalysis, the dynamic evolution of complex intermediates and multiple reaction pathways presents significant challenges for real-time monitoring and mechanistic analysis. Future advancements may leverage artificial intelligence to predict possible reaction pathways and combine SI-SECM with *in situ* spectroscopic techniques such as infrared, Raman, and X-ray absorption spectroscopy to track the dynamic evolution of different active sites and the generation and consumption of intermediates in real time. This integrated approach will comprehensively reveal the intrinsic mechanisms and kinetic processes underlying cascade reactions.

### Expansion of cascade systems

In single-mode electrocatalysis, driving complex multistep cascade reactions is often limited by low energy efficiency. Future developments will focus on hybrid catalytic systems that couple multiple energy fields, such as electrochemical-photonic, electrochemical-thermal, and electrochemical-biological coupling. By rationally designing and optimizing these multi-energy input, multi-reaction integrated systems, this approach should overcome the constraints of traditional single-mode catalysis, substantially expanding the scope of cascade catalysis for chemical synthesis, environmental remediation, and energy conversion. Such advances may enable higher selectivity, efficiency, and sustainability in complex molecule construction, deep pollutant transformation, and renewable energy utilization.

In summary, cascade electrocatalysis has been extensively explored for carbon–nitrogen resource utilization. With continued development in multiscale catalyst design, reaction mechanism investigation, and the integration of cascade systems, cascade electrocatalysis holds great promise for achieving more efficient resource conversion, thereby advancing the sustainable development of energy and the environment.

### Author contributions

Writing – original draft, S. Li.; visualization, H. Li., R. Y., Y. P.; writing – review & editing, Z. J., P. Li.; funding acquisition, Z. J., P. Li.; supervision, P. Li, G. Y.

### Conflicts of interest

There are no conflicts to declare.

### Data availability

No primary research results, software or code have been included and no new data were generated or analysed as part of this review.

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