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# Synthesis, characterization, and adsorptive removal of methyl blue using combustion-synthesized $\text{Al}_4\text{B}_2\text{O}_9$ and $\text{Al}_5\text{BO}_9$

 Uğur Özkan, <sup>\*a</sup> Okan Bayram, <sup>b</sup> Emel Moral, <sup>c</sup> İlhan Pekgözü <sup>d</sup> and Fethiye Göde <sup>e</sup>

This study investigates the removal process of methyl blue (MeB), an anionic dye, using synthesized  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  as adsorbent materials.  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  were synthesized *via* the combustion method. The structural, morphological, textural, thermal and surface-charge properties of the synthesized borate materials were evaluated using FTIR, XRD, SEM, BET, TGA, and zeta potential measurements. The adsorption behavior of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  was assessed by varying solution pH, contact duration, initial MeB concentration, adsorbent loading, and temperature. Kinetic, equilibrium, and thermodynamic analyses were carried out to clarify the adsorption behavior and possible interaction pathways between MeB and the synthesized borate surfaces. Kinetic modeling showed that the PSO equation most accurately describes MeB removal by both borate materials, as indicated by the high  $R^2$  values. The thermodynamic parameters showed that MeB adsorption was favored by increasing temperature and proceeded spontaneously, as confirmed by the positive  $\Delta H^\circ$  and negative  $\Delta G^\circ$  values, respectively ( $\text{Al}_4\text{B}_2\text{O}_9$ :  $\Delta H = 16.827$  kJ mol<sup>-1</sup>;  $\text{Al}_5\text{BO}_9$ :  $\Delta H = 17.130$  kJ mol<sup>-1</sup>). The positive  $\Delta S^\circ$  values indicate that the adsorption process was accompanied by increased interfacial disorder during the transfer of MeB molecules from solution to the borate surface ( $\text{Al}_4\text{B}_2\text{O}_9$ :  $\Delta S = 80.222$  J (mol<sup>-1</sup> K<sup>-1</sup>);  $\text{Al}_5\text{BO}_9$ :  $\Delta S = 82.940$  J (mol<sup>-1</sup> K<sup>-1</sup>)). Equilibrium modeling indicated that the Freundlich equation more suitably described MeB uptake by both  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$ , suggesting adsorption on heterogeneous surface sites. According to the Freundlich model, the  $K_F$  values were determined as 21.146 for  $\text{Al}_4\text{B}_2\text{O}_9$  and 27.072 for  $\text{Al}_5\text{BO}_9$ . Although the Freundlich model provided the best fit, the Langmuir model was used to estimate the maximum monolayer adsorption capacities, which were calculated as 70.547 mg g<sup>-1</sup> for  $\text{Al}_4\text{B}_2\text{O}_9$  and 105.785 mg g<sup>-1</sup> for  $\text{Al}_5\text{BO}_9$ . Overall, the results demonstrate the potential of combustion-derived  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  as inorganic borate adsorbents for removing anionic MeB from aqueous media.

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## Introduction

Water resources are essential for ecological balance, public health, and the continuity of agricultural and industrial activities. The growing discharge of chemical and biological pollutants into aquatic environments has made water security a major global concern.<sup>1,2</sup> Effluents containing synthetic dyes represent a major environmental concern due to their strong coloration, chemical persistence and possible toxic effects. The protection

of water resources is essential for sustaining life on Earth and maintaining an environmentally sustainable future.<sup>2,3</sup> It is evident that industrial and metallurgical wastewater pollutants constitute a significant source of annual water contamination. The dyeing process involves the application of synthetic or natural colorants to materials such as textiles, paper, leather, and plastics in order to impart color.<sup>3,4</sup> During the discharge of these industrial effluents into surrounding water bodies, substantial amounts of hazardous dyes have been detected. Changes in water quality due to the presence of biological, physical, or chemical components that may pose a potential threat to public health and safety are classified as water pollution. Synthetic dyes constitute an important class of industrial pollutants, particularly due to their extensive use in textile related processes.<sup>1-4</sup> The discharge of organic dyes into water bodies such as rivers and ponds has been reported to cause severe damage to flora and fauna. This is primarily attributed to the toxic, carcinogenic, and mutagenic nature of these compounds.<sup>5</sup> Dyes are known to possess complex molecular

<sup>a</sup>Department of Forest Products Engineering, Faculty of Forestry, Isparta University of Applied Sciences, 32200, Isparta, Turkey. E-mail: [ugurozkan@isparta.edu.tr](mailto:ugurozkan@isparta.edu.tr)
<sup>b</sup>Department of Chemistry, Faculty of Engineering and Natural Sciences, Süleyman Demirel University, 32200 Isparta, Turkey. E-mail: [okanbayram@sdu.edu.tr](mailto:okanbayram@sdu.edu.tr)
<sup>c</sup>Department of Chemistry, Graduate School of Natural and Applied Sciences, Süleyman Demirel University, 32200 Isparta, Turkey. E-mail: [emel32moral@gmail.com](mailto:emel32moral@gmail.com)
<sup>d</sup>Department of Environmental Engineering, Faculty of Engineering, Karabük University, 78050 Karabük, Turkey. E-mail: [ilhanpekgozlu@karabuk.edu.tr](mailto:ilhanpekgozlu@karabuk.edu.tr)
<sup>e</sup>Department of Chemistry, Faculty of Engineering and Natural Sciences, Süleyman Demirel University, 32200 Isparta, Turkey. E-mail: [fethiyegode@sdu.edu.tr](mailto:fethiyegode@sdu.edu.tr)

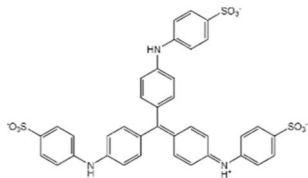

structures that confer resistance to degradation. Their persistence and strong coloration can limit light transmission in water bodies, which may suppress photosynthesis and decrease dissolved oxygen availability.<sup>6</sup> Many dyes are toxic substances that may lead to various health problems, including skin irritation, respiratory disorders, and even cancer. Moreover, their complex molecular structures pose significant challenges to natural degradation processes.<sup>7</sup> Methyl blue (MeB), a compound used in various industries including cotton, silk, and wool dyeing imparts a blue color to the applied material and is commonly detected in industrial wastewater streams. In addition, it has numerous applications in medical, biological, and chemical industries. It has been reported that MeB may cause health complications.<sup>7,8</sup> MeB is an anionic sulfonated dye that has been frequently used in staining applications, including biological and histological studies. However, it is toxic and biologically harmful to both organisms and the environment.<sup>9,10</sup> Various physical and chemical processes are employed for water treatment. A range of methods including chemical, biological, and physical approaches are used in the treatment of dye-contaminated wastewater. These include biodegradation, membrane filtration, ion exchange, electrochemical oxidation, and adsorption. Most of these techniques have been extensively investigated and applied.<sup>11</sup> Among the available treatment strategies, adsorption is widely preferred because it combines practical operation with effective pollutant uptake under different solution conditions.<sup>12</sup> Therefore, this study evaluates combustion-derived  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  as aluminum borate adsorbents for the removal of anionic MeB from water. The adsorption behavior of combustion-synthesized  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  toward anionic MeB has not been systematically evaluated in terms of pH, dosage, contact time, temperature, kinetics, isotherms, thermodynamics, and surface charge. Aluminum borates are characterized by favorable stability properties, including high thermal stability, low thermal expansion and conductivity, high creep resistance, and strong corrosion resistance.<sup>13</sup> Owing to these properties, aluminum borates particularly in the form of nanowires and whiskers are widely utilized in ceramic composites, optoelectronics, and tribological applications.<sup>14</sup> Therefore, the present study focuses on the synthesis, physicochemical characterization, and adsorption performance of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  toward MeB removal. The synthesized borate phases were examined in terms of crystalline structure, surface functional groups, morphology, textural properties, thermal behavior, and surface charge. Subsequently, adsorption experiments were conducted, and the results were interpreted in terms of fundamental adsorption properties and design parameters to assess the effectiveness of the synthesized materials.

## Materials and methods

### Chemicals and instruments

MeB was selected as the target anionic dye for the adsorption experiments. The properties of the dye, supplied by Isolab (Germany) are presented in Table 1. The chemicals used for synthesis and pH adjustment were purchased from Sigma-

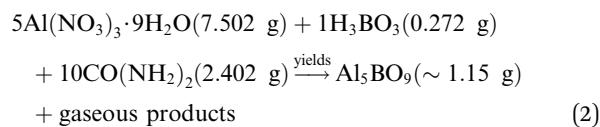
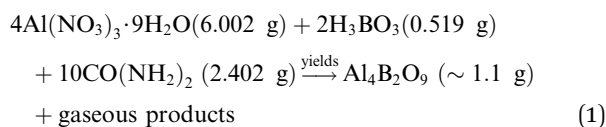
Table 1 Physicochemical properties of MeB dye

Name	Methyl blue (MeB)
Formula	$\text{C}_{37}\text{H}_{27}\text{N}_3\text{Na}_2\text{O}_9\text{S}_3$
Molecular weight	$799.814 \text{ g mol}^{-1}$
Type	Anionic
Molecular structure	

Aldrich. The maximum absorption wavelength of MeB was identified as 600 nm by wavelength scanning using Peak Instruments C-7100 and DLAB 1100 UV-Vis spectrophotometers. Solution pH values were measured during the experiments using a Hanna HI2020-02 Edge pH meter. FT-IR spectra were collected with a JASCO FT/IR-4700 Type A spectrometer in the  $4000\text{--}400 \text{ cm}^{-1}$  range to identify the characteristic vibrational features of the synthesized borates. The surface morphology of the synthesized materials was observed using a Quanta-FEG-250 scanning electron microscope and XRD analyses were conducted with a Bruker D8 Advance Twin diffractometer. The surface area and porosity of the  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  materials were determined by Brunauer–Emmett–Teller (BET) analysis using a Micromeritics Gemini VII 2390 t instrument. Thermal degradation behavior and mass-loss profiles were investigated by TG/DTG analysis from 25 to 1400 °C. The surface charge behavior of the adsorbents was evaluated using a HORIBA SZ-100 zeta potential analyzer. A Radwag AS220.R2 Plus analytical balance was used to determine solution quantities during the experiments.

### Synthesis of $\text{Al}_4\text{B}_2\text{O}_9$ and $\text{Al}_5\text{BO}_9$

Two aluminum borate materials with the chemical formulas  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  were employed in the adsorption experiments. These materials were synthesized using the combustion method. High-purity chemicals supplied by Sigma-Aldrich were used in the preparation of the adsorbents. The synthesis reactions for both adsorbents are presented in eqn (1) and (2) below.



The synthesis procedure was identical for both adsorbents. The starting reagents were accurately weighed according to the calculated stoichiometric composition before synthesis. After



weighing, the starting material reagents were transferred into a porcelain crucible and homogenized before thermal treatment. Subsequently, 50 mL of distilled water was added to dissolve the mixtures. The resulting solutions were placed on a hot plate set to 100 °C to evaporate the water. After complete evaporation, the remaining solid mixtures were thoroughly homogenized. These mixtures were then transferred to a furnace and maintained at 500 °C for 15 minutes. After cooling, the obtained powder was ground thoroughly to ensure compositional homogeneity. The homogenized powder mixtures were then separately placed into aluminum oxide boats. The homogenized powder was transferred to an alumina boat and calcined at 850 °C for 6 h. The furnace was operated under atmospheric conditions.

### Batch adsorption experiments

MeB removal experiments were performed in batch mode under controlled solution conditions. The influence of key operating variables, namely pH, adsorbent amount, contact time, initial MeB concentration, and temperature, was evaluated to determine their effects on adsorption performance. The pH range selected for the experiments was 3–9, while temperature studies were carried out within the range of 25 to 55 °C. The effect of the initial dye concentration was evaluated at concentrations ranging from 25 to 200 ppm. To determine the influence of adsorbent dosage, a series of adsorbent dosages between 0.01 and 0.09 g were selected. The pH of the solutions was adjusted using 0.1 M HCl and 0.1 M NaOH. The pH meter was calibrated with appropriate buffer solutions prior to measurements. Batch adsorption experiments were performed using 30 mL of MeB solution in 50 mL containers at a shaking speed of 150 rpm. After adsorption, the suspensions were filtered using filter paper, and the filtrates were diluted to a final volume of 50 mL with distilled water prior to UV-Vis analysis. The measured concentrations were corrected for dilution before calculating adsorption capacity. The amount of dye adsorbed was determined using a UV-Vis spectrophotometer at the maximum wavelength of the dye. In the equilibrium studies, the amount of MeB adsorbed onto  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  was calculated using a mass balance approach. The equilibrium adsorption capacity of the dye was determined using eqn (3).

$$q_e = \frac{(C_0 - C_e)V}{W} \quad (3)$$

$C_0$  represents the initial concentration of MeB,  $C_e$  denotes the equilibrium MeB concentration after dilution correction,  $W$  (g) corresponds to the amount of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  used as adsorbents, and  $V$  (L) is the volume of the solution.<sup>1</sup> Subsequently, kinetic and isotherm studies were conducted under selected fixed experimental conditions, as specified in the corresponding figure captions. The kinetic experiments were performed by varying the contact time between 30 and 120 minutes, whereas the adsorption isotherms were evaluated at initial dye concentrations ranging from 25 to 200 mg L<sup>-1</sup>.

## Results & discussion

### N<sub>2</sub> adsorption–desorption analysis

The Brunauer–Emmett–Teller (BET) method is a widely used technique for determining the specific surface area of porous materials, including solids. The specific surface area of solid adsorbents is often associated with their adsorption performance, as it may be related to the number of active sites available for pollutant binding.<sup>15</sup> Surface area becomes particularly significant when working with materials possessing a porous structure. The specific surface area and pore volume of the synthesized materials were determined from N<sub>2</sub> adsorption–desorption isotherms at 77 K. Fig. 1 presents the comparative BET adsorption isotherms of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$ .

The results provide information regarding the surface area and pore structure of the porous materials. Fig. 1 indicates a positive correlation between the increase in relative pressure ( $P/P_0$ ) and the amount of gas adsorbed. Furthermore, the isotherm curve exhibits a pronounced upward trend, particularly as the relative pressure approaches unity. The pore size distribution was calculated using the Barrett–Joyner–Halenda (BJH) model.<sup>16</sup> The BET analysis results for  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  are presented in Table 2.

Table 2 shows that the specific surface areas of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  are 21.473 m<sup>2</sup> g<sup>-1</sup> and 29.599 m<sup>2</sup> g<sup>-1</sup>, respectively, while their pore volumes are 0.125 cm<sup>3</sup> g<sup>-1</sup> and 0.142 cm<sup>3</sup> g<sup>-1</sup>, respectively. Compared with  $\text{Al}_4\text{B}_2\text{O}_9$ ,  $\text{Al}_5\text{BO}_9$  exhibited higher BET surface area and pore volume, suggesting greater surface accessibility and more pronounced pore development. These textural properties may partially contribute to the higher adsorption capacity of  $\text{Al}_5\text{BO}_9$ . However, aqueous dye adsorption is not governed solely by BET surface area; surface charge, solution pH, surface active sites, and specific adsorbent–adsorbate interactions may also play important roles in MeB adsorption.

### FT-IR analysis of synthesized aluminum borates

The characteristic vibrational bands of the synthesized aluminum borate compounds were evaluated using FT-IR spectroscopy. The FT-IR spectra of the  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  materials are presented in Fig. 2. FT-IR spectra in the range of 4000–400 cm<sup>-1</sup> were recorded at room temperature using a JASCO FT/IR-4700 Type A spectrometer. The FT-IR spectra exhibited several characteristic absorption bands corresponding to the vibrational modes of B–O and Al–O bonds. In the  $\text{Al}_4\text{B}_2\text{O}_9$  material, the band observed at 3190 cm<sup>-1</sup> is attributed to O–H stretching vibrations, indicating the presence of hydroxyl groups within the sample. This peak was not observed in the  $\text{Al}_5\text{BO}_9$  material; instead, its main absorption bands were found to begin at approximately ~1420 cm<sup>-1</sup>. For both materials, the bands detected in the range of ~1330–1270 cm<sup>-1</sup> are considered to correspond to the asymmetric stretching vibrations of B–O–B linkages. The bands observed between ~1100 and 1000 cm<sup>-1</sup> are associated with B–O stretching vibrations of  $\text{BO}_3$  structural units. The bands in the ~700–600 cm<sup>-1</sup> region



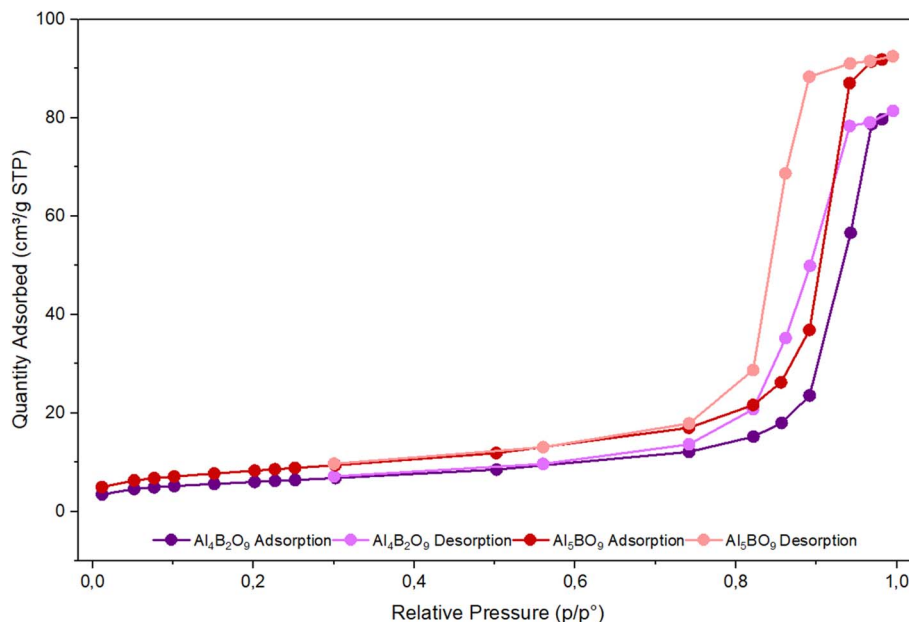


Fig. 1  $N_2$  adsorption–desorption isotherms of  $Al_4B_2O_9$  and  $Al_5BO_9$ .

Table 2 Textural properties of  $Al_4B_2O_9$  and  $Al_5BO_9$  obtained from  $N_2$  adsorption–desorption analysis

Materials	Single point ( $m^2 g^{-1}$ )	BET ( $m^2 g^{-1}$ )	<i>t</i> -Plot micropore ( $m^2 g^{-1}$ )	<i>t</i> -Plot external ( $m^2 g^{-1}$ )	BJH adsorption ( $m^2 g^{-1}$ )	Single point adsorption ( $cm^3 g^{-1}$ )	<i>t</i> -Plot micropore ( $cm^3 g^{-1}$ )	BJH adsorption ( $cm^3 g^{-1}$ )
$Al_4B_2O_9$	20.966	21.473	2.653	18.821	23.344	0.126	0.001	0.125
$Al_5BO_9$	28.893	29.599	3.114	26.485	33.286	0.143	0.001	0.142

suggest the presence of Al–O vibrations, while those at  $\sim 500\text{ cm}^{-1}$  and below are attributed to  $AlO_6$  units.<sup>17–19</sup>

### Morphological analysis by SEM

The surface morphology of the  $Al_4B_2O_9$  and  $Al_5BO_9$  materials was examined using scanning electron microscopy (SEM) at

magnifications ranging from  $1000\times$  to  $20000\times$ . The SEM images of  $Al_4B_2O_9$  and  $Al_5BO_9$  are presented in Fig. 3. SEM observations provide useful morphological information for adsorption studies by revealing surface roughness, irregular particles, pore-like regions and microstructural heterogeneity. At magnifications of  $1000\times$  and  $2000\times$ ,  $Al_4B_2O_9$  exhibits

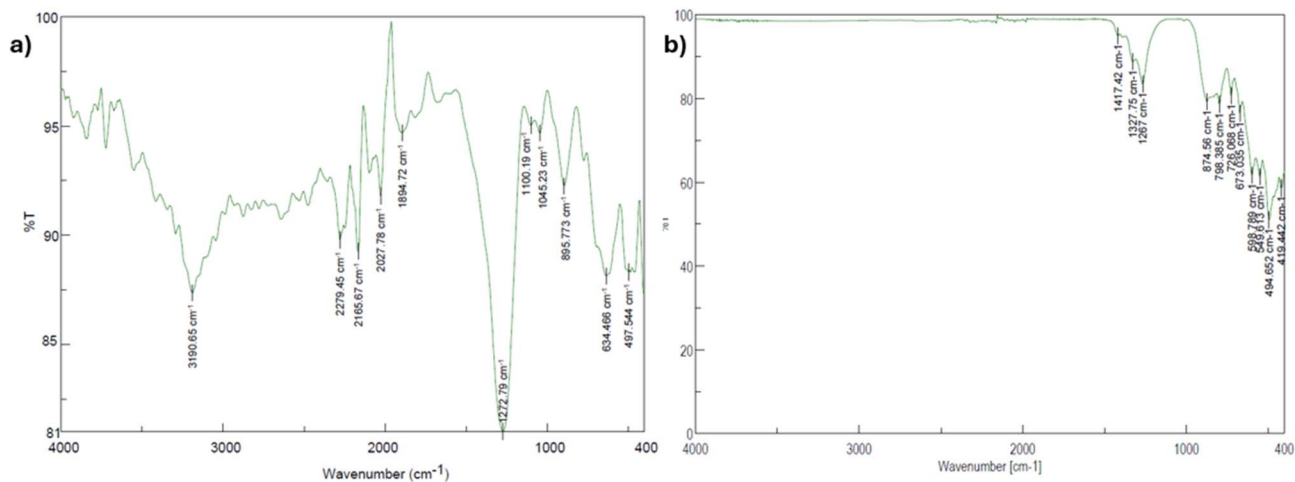


Fig. 2 FT-IR spectra of combustion-synthesized aluminum borates: (a)  $Al_4B_2O_9$  (b)  $Al_5BO_9$ .



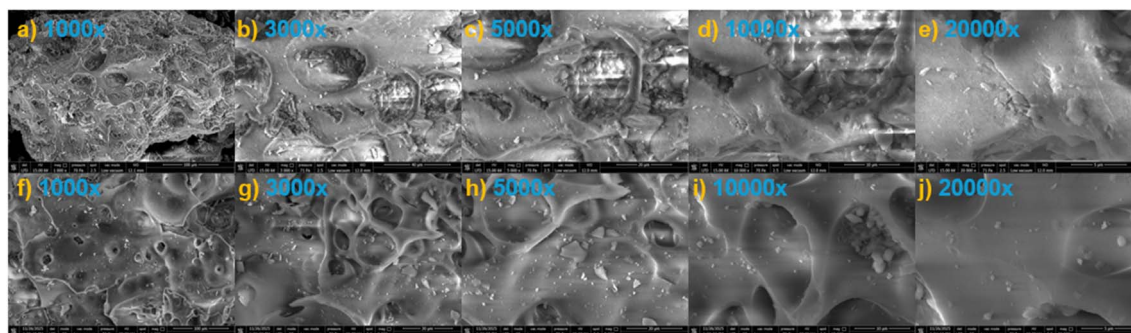


Fig. 3 SEM micrographs of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  at different magnifications: (a–e)  $\text{Al}_4\text{B}_2\text{O}_9$  and (f–j)  $\text{Al}_5\text{BO}_9$ .

a highly rough surface with visible void like regions and channel like features. In contrast,  $\text{Al}_5\text{BO}_9$  appears to display a more homogeneous structure at lower magnifications. At  $3000\times$  and  $5000\times$  magnifications,  $\text{Al}_4\text{B}_2\text{O}_9$  shows ring-like and layered formations with partially melted and cracked regions. These structures may be attributed to irregular sintering processes or phase separation. At higher magnifications ( $10000\times$  and  $20000\times$ ), the surface topography of  $\text{Al}_4\text{B}_2\text{O}_9$  is observed to consist of more compact areas along with micro porous regions. For  $\text{Al}_5\text{BO}_9$ , the images at  $10000\times$  and  $20000\times$  magnifications suggest fewer visible surface voids and smoother grain surfaces. Overall,  $\text{Al}_5\text{BO}_9$  appears to possess a more homogeneous microstructure in the SEM images. However, its higher BET surface area and pore volume suggest that smaller-scale porosity may be more developed than can be directly observed from SEM micrographs.

#### Phase structure and crystallinity by XRD

The crystalline phase formation and structural characteristics of the synthesized adsorbents were evaluated by X-ray diffraction (XRD) analysis. The XRD patterns of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  prepared *via* the combustion method are presented in Fig. 4. When the diffraction peaks obtained for both adsorbents  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  are compared with standard card no: 00-

029-0010 and 01-077-0395, respectively, they are found to be consistent. Furthermore, previous studies have reported that  $\text{Al}_4\text{B}_2\text{O}_9$  has orthorhombic unit cells with values of  $a = 14.746 \text{ \AA}$ ,  $b = 15.268$  and  $c = 5.557 \text{ \AA}$ . In addition, it has been reported that the other adsorbent  $\text{Al}_5\text{BO}_9$  also has orthorhombic unit cells with values of  $a = 5.682 \text{ \AA}$ ,  $b = 14.973$  and  $c = 7.692 \text{ \AA}$ .<sup>19–22</sup>

#### Thermal stability of $\text{Al}_4\text{B}_2\text{O}_9$ and $\text{Al}_5\text{BO}_9$

Fig. 5 presents the TG/DTG curves of the  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  materials. Thermal analysis was carried out over the temperature range of 25 to  $1400 \text{ }^\circ\text{C}$ . For the  $\text{Al}_4\text{B}_2\text{O}_9$  material, a gradual but low-rate mass loss is observed. The most pronounced mass loss occurs between  $1000 \text{ }^\circ\text{C}$  and  $1200 \text{ }^\circ\text{C}$ . The total mass loss was determined to be approximately 4%. Similarly, the  $\text{Al}_5\text{BO}_9$  material exhibits a controlled and relatively low mass loss. However, the total mass loss for  $\text{Al}_5\text{BO}_9$  is approximately 6%. The sharpest decrease in mass is observed in the temperature range of  $1200$  to  $1400 \text{ }^\circ\text{C}$ . The results indicate that both materials demonstrate high thermal stability up to  $1000 \text{ }^\circ\text{C}$ . The more significant mass losses observed above  $1000 \text{ }^\circ\text{C}$  may be associated with structural rearrangements within the borate framework, possible structural rearrangements, phase related changes or dehydroxylation and dehydration processes.

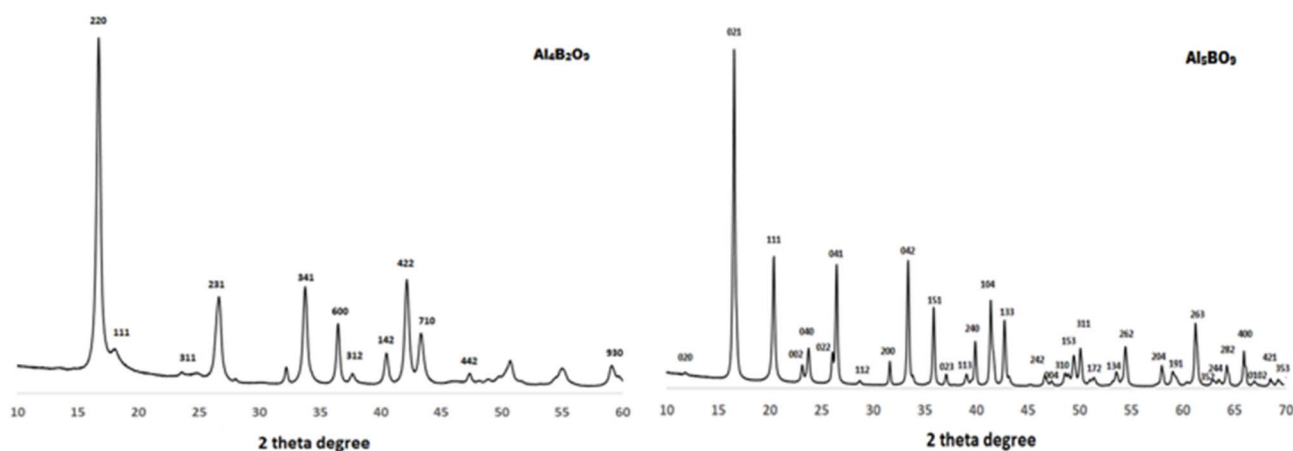
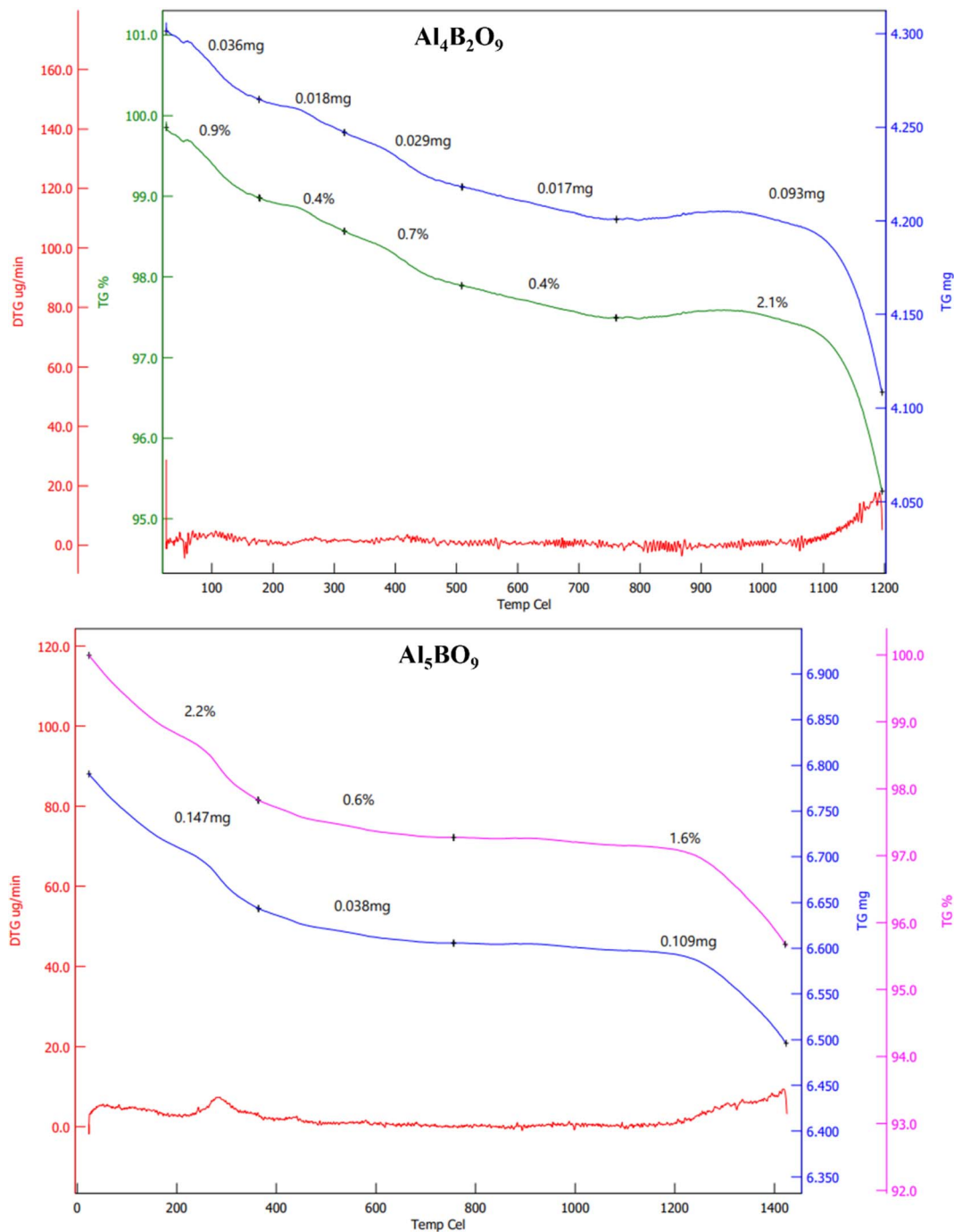


Fig. 4 XRD patterns of combustion-synthesized  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$ .



Fig. 5 TG/DTG curves of Al<sub>4</sub>B<sub>2</sub>O<sub>9</sub> and Al<sub>5</sub>BO<sub>9</sub>.

### Zeta potential and effect of initial solution pH

In aqueous media, solution pH strongly affects the electrical double layer and therefore the zeta potential of solid particles. Zeta potential measurements provide information on surface-charge variation with pH and help interpret the electrostatic contribution to dye adsorption.<sup>23</sup> In dye adsorption studies, it has been reported that the surface charge, as interpreted from zeta potential results, can significantly influence the adsorption performance of a material through its interaction with dye

molecules.<sup>24</sup> Zeta potential measurements were performed by dispersing 50 mg of the sample in 10 mL of ultrapure water. The suspension was homogenized using a vortex mixer and subsequently centrifuged at 1000 rpm. The resulting supernatant was then transferred into an electrode-equipped measurement cell, and the zeta potential was measured using the instrument. An examination of the zeta potential and electrophoretic mobility results for Al<sub>4</sub>B<sub>2</sub>O<sub>9</sub> and Al<sub>5</sub>BO<sub>9</sub> shows that the zeta potential values were  $-11.5$  mV and  $-50.7$  mV, respectively. The

corresponding electrophoretic mobility values were determined as  $-0.000089 \text{ cm}^2 \text{ V}^{-1} \text{ s}^{-1}$  and  $-0.000391 \text{ cm}^2 \text{ V}^{-1} \text{ s}^{-1}$ . These results indicate that  $\text{Al}_4\text{B}_2\text{O}_9$  exhibits weak electrostatic repulsion and a higher tendency toward aggregation, whereas  $\text{Al}_5\text{BO}_9$  demonstrates strong electrostatic repulsion. Solution pH is a key variable in adsorption because it modifies adsorbent surface charge, functional-group protonation, and the interaction strength between adsorbent and adsorbate.<sup>25,26</sup> The adsorption capability may depend on the electrostatic interactions between MeB molecules and the adsorbent surface. The variation in the percentage of dye adsorbed at equilibrium as a function of solution pH is shown in Fig. 6. Maximum dye adsorption for both adsorbents was observed at pH 3. The removal efficiency of MeB decreased as the pH increased from 3 to 9. MeB, an anionic dye molecule, carries a negative charge due to the presence of sulfonate groups ( $\text{SO}_3^-$ ), which ionize in aqueous solution. Under acidic conditions, protonation of Al–O and B–O related surface hydroxyl groups may decrease the negative charge density of the borate surface, which could reduce electrostatic repulsion and favor the adsorption of anionic MeB species. Therefore, MeB can retain its anionic character even under acidic conditions due to its sulfonate groups. Surface Al-based sites may interact with the negatively charged sulfonate groups of MeB, thereby contributing to adsorption under acidic conditions. In basic environments, sulfonate groups remain in their anionic  $-\text{SO}_3^-$  form and thus retain their negative charge. Under alkaline conditions, the adsorption of hydroxide ions may increase the negative surface character of aluminum borate compounds. Consequently, electrostatic repulsion occurs between the negatively charged dye molecules and the negatively charged adsorbent surface, resulting in reduced adsorption compared with acidic conditions. Similar findings have been reported in the literature. Zhao *et al.* (2012) observed a decrease in adsorption capacity with increasing pH in the removal of Acid Red 18 dye.<sup>27</sup> Likewise, Bayram *et al.* (2026) reported a significant decrease in adsorption percentage with increasing pH during the adsorption of the anionic dye alizarin yellow GG.<sup>28</sup>

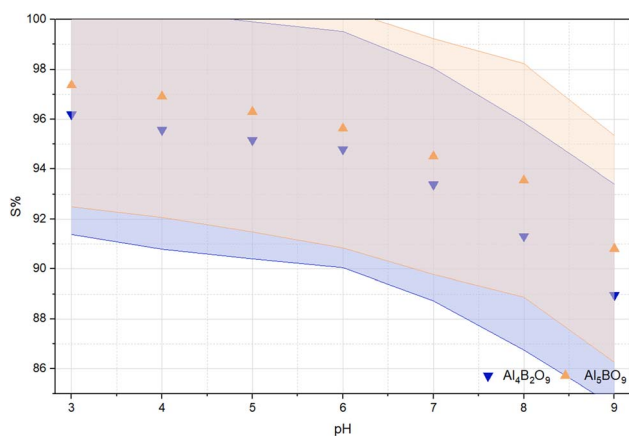


Fig. 6 Effect of initial solution pH on MeB removal by  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  (conditions: concentration:  $50 \text{ mg L}^{-1}$ , dosage:  $0.05 \text{ g}$ , temperature:  $25 \text{ }^\circ\text{C}$ , time:  $60 \text{ min}$ , pH: 3–9).

### Effect of adsorbent dosage on MeB removal

Adsorbent dosage, evaluated under various adsorption conditions, is considered a significant parameter in determining the practical applicability of an adsorbent.<sup>29</sup> The effect of varying adsorbent dosage on MeB removal using  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  is presented in Fig. 7. It is well established that the efficiency of dye adsorption is strongly influenced by the amount of adsorbent employed. Increasing the adsorbent dosage is generally associated with an enhancement in dye removal due to the greater availability of active adsorption sites.<sup>30,31</sup> In the present study, an increase in the dosage of both  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  led to a corresponding increase in dye removal efficiency. When the adsorbent dosage was increased from  $0.01$  to  $0.09 \text{ g}$ , the removal efficiency for  $\text{Al}_4\text{B}_2\text{O}_9$  increased from  $70.34$  to  $96.24\%$ . Similarly, for  $\text{Al}_5\text{BO}_9$ , the removal efficiency increased from  $74.72$  to  $99.21\%$ . These increases were observed to stabilize beyond a certain adsorbent amount.<sup>32</sup> Accordingly, for both materials, the removal efficiency remained relatively constant at dosages above  $0.05 \text{ g}$ . Since the removal efficiency showed only a slight increase above  $0.05 \text{ g}$ , this dosage was selected as the practical optimum for subsequent experiments.

### Effect of contact time and adsorption kinetics

Contact time is an important operational variable because it determines the duration of interaction between dye molecules and active adsorption sites. As the dye adsorbate approaches the active sites of the adsorbent, adsorption efficiency is expected to increase.<sup>33</sup> The effect of contact time on the sorption efficiency (%S) of MeB removal using  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  is presented in Fig. 8. Contact times were systematically investigated within the range of  $30$  to  $120$  minutes. The adsorption efficiencies of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  at  $30$  minutes were determined to be  $90.30\%$  and  $93.55\%$ , respectively. At  $120$  minutes, these values increased to  $97.03\%$  and  $98.31\%$ , respectively. The adsorption efficiency increased with contact time until equilibrium was approached.<sup>34</sup> At the initial stage, the adsorption process proceeds rapidly due to the availability of vacant active sites on

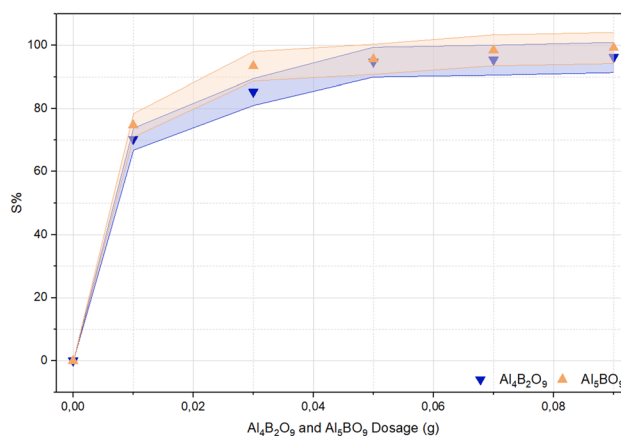


Fig. 7 Effect of adsorbent dosage on MeB removal by  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  (conditions: concentration:  $50 \text{ mg L}^{-1}$ , dosage:  $0.01 \text{ g}$ ,  $0.03 \text{ g}$ ,  $0.05 \text{ g}$ ,  $0.07 \text{ g}$ ,  $0.09 \text{ g}$ , temperature:  $25 \text{ }^\circ\text{C}$ , time:  $60 \text{ min}$ , pH: natural).



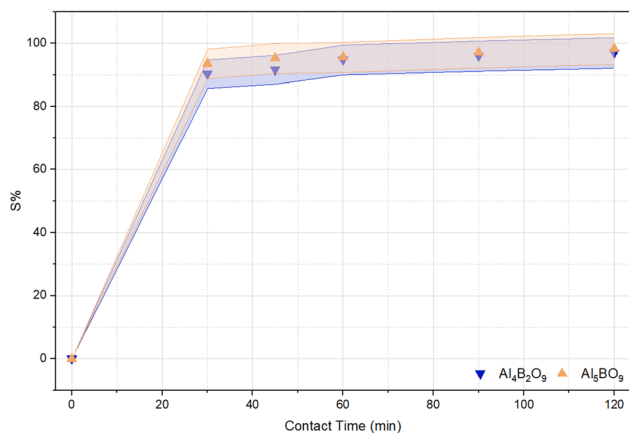


Fig. 8 Effect of contact time on MeB removal by  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  (conditions: concentration:  $50 \text{ mg L}^{-1}$ , dosage:  $0.05 \text{ g}$ , temperature:  $25 \text{ }^\circ\text{C}$ , time: 30 min, 45 min, 60 min, 90 min, 120 min, pH: natural).

the surface. However, both adsorbents were observed to reach saturation within approximately 60 minutes. Beyond 60 minutes, no significant change in adsorption percentage was detected. Over time, as the adsorption sites on the surface of the aluminum borate compounds become occupied, the adsorption rate decreases. Eventually, the rates of adsorption and desorption reach equilibrium at the final equilibrium point. Furthermore, the kinetic parameter results are presented in Table 3.

Adsorption kinetics plays a crucial role in understanding dye adsorption processes. The relationship between contact time and adsorption capacity is considered instrumental in

determining the appropriate kinetic model and its associated parameters.<sup>35</sup> The adsorption rate is governed by adsorption kinetics, which in turn provides insight into the underlying adsorption mechanism.<sup>36</sup> The adsorption process of MeB dye was investigated using the pseudo-first-order (PFO), pseudo-second-order (PSO), and intraparticle diffusion kinetic models. Among the kinetic models tested, the PSO model yielded the most suitable description of MeB adsorption on both  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$ , with  $R^2$  values approaching unity. The kinetic parameters were calculated using adsorption capacity values obtained from the mass balance equation based on the initial adsorption volume. The better agreement with the PSO model suggests that the adsorption rate is closely associated with the availability of surface active sites. However, this result alone does not conclusively confirm chemisorption. The intraparticle diffusion model plot is shown in Fig. 9.

### Effect of temperature and adsorption thermodynamics

Since adsorption equilibrium can vary with temperature, thermodynamic parameters were evaluated to clarify the thermal nature of MeB removal. In this study, temperatures of  $25 \text{ }^\circ\text{C}$ ,  $35 \text{ }^\circ\text{C}$ ,  $45 \text{ }^\circ\text{C}$ , and  $55 \text{ }^\circ\text{C}$  were selected to evaluate the effect of temperature, while the remaining parameters were kept constant. The influence of temperature variation on the sorption efficiency of MeB removal using  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  is presented in Fig. 10. The removal efficiencies of  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  at  $25 \text{ }^\circ\text{C}$  were determined to be 94.79% and 95.63%, respectively. At  $55 \text{ }^\circ\text{C}$ , these values increased to 97.14% and 97.65%, respectively. It is well established that temperature

Table 3 Kinetic parameters for MeB adsorption onto  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$

Sorbents	Model	$q_e \text{ (mg g}^{-1}\text{)}$	$k$	$C \text{ (mg g}^{-1}\text{)}$	$R^2$
$\text{Al}_4\text{B}_2\text{O}_9$	PFO	29.109	$0.033 \text{ min}^{-1}$	25.124	0.968
	PSO	29.927	$0.010 \text{ g mg}^{-1} \text{ min}^{-1}$		0.999
	Intraparticle diffusion		$0.380 \text{ mg g}^{-1} \text{ min}^{-1/2}$		0.928
$\text{Al}_5\text{BO}_9$	PFO	29.193	$0.051 \text{ min}^{-1}$	27.101	0.931
	PSO	29.624	$0.020 \text{ g mg}^{-1} \text{ min}^{-1}$		0.999
	Intraparticle diffusion		$0.202 \text{ mg g}^{-1} \text{ min}^{-1/2}$		0.920

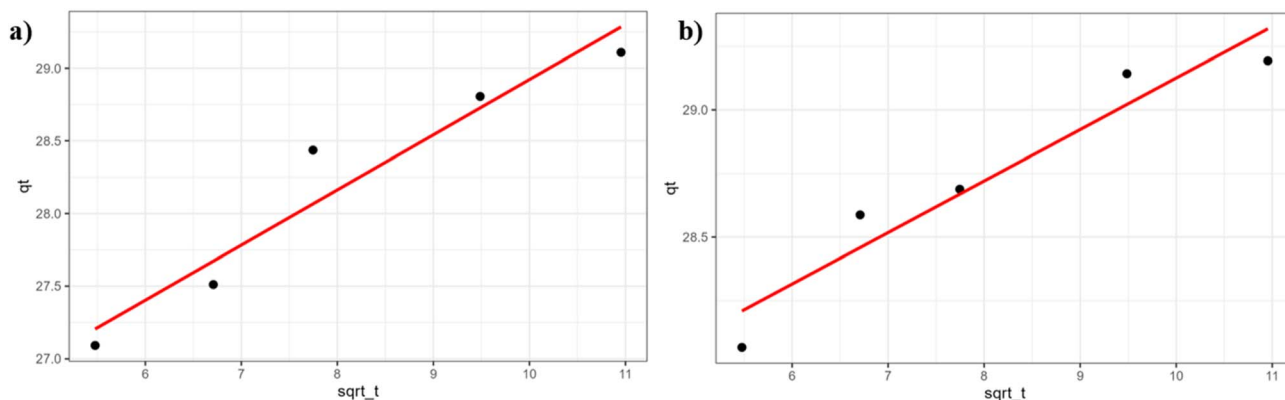


Fig. 9 Intraparticle diffusion plots for MeB adsorption. (a)  $\text{Al}_4\text{B}_2\text{O}_9$  (b)  $\text{Al}_5\text{BO}_9$ .



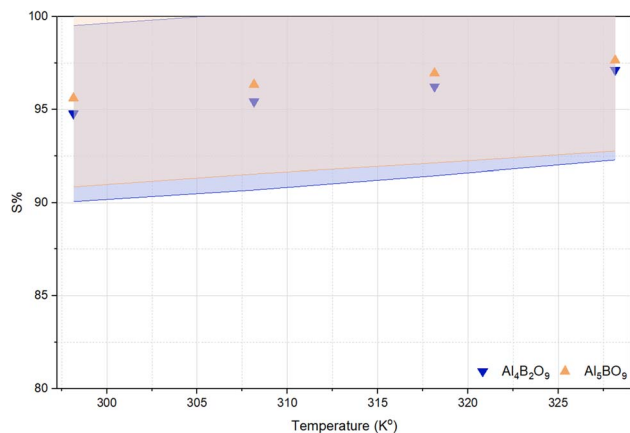


Fig. 10 Effect of temperature on MeB removal by  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  (conditions: concentration:  $50 \text{ mg L}^{-1}$ , dosage:  $0.05 \text{ g}$ , temperature:  $25 \text{ }^\circ\text{C}$ ,  $35 \text{ }^\circ\text{C}$ ,  $45 \text{ }^\circ\text{C}$ ,  $55 \text{ }^\circ\text{C}$ , time:  $60 \text{ min}$ , pH: natural).

Table 4 Thermodynamic parameters for MeB adsorption onto  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$

T (K)		298.150	308.150	318.150	328.150
$\text{Al}_4\text{B}_2\text{O}_9$	$\Delta G^\circ$ ( $\text{kJ mol}^{-1}$ )	-7.091	-7.893	-8.695	-9.498
	$\Delta S^\circ$ ( $\text{J mol}^{-1} \text{K}^{-1}$ )	80.222			
	$\Delta H^\circ$ ( $\text{kJ mol}^{-1}$ )	16.827			
$\text{Al}_5\text{BO}_9$	$\Delta G^\circ$ ( $\text{kJ mol}^{-1}$ )	-7.598	-8.428	-9.257	-10.087
	$\Delta S^\circ$ ( $\text{J mol}^{-1} \text{K}^{-1}$ )	82.940			
	$\Delta H^\circ$ ( $\text{kJ mol}^{-1}$ )	17.130			

variations affect both the thermodynamics and kinetics of adsorption processes. The increase in MeB removal efficiency with temperature suggests that adsorption onto both aluminum borates is favored at higher temperatures.<sup>37</sup> The results demonstrate that MeB removal efficiency increases with rising temperature, indicating that the adsorption process is favored at higher temperatures.<sup>38</sup>

Thermodynamic studies were conducted to investigate the effect of temperature on adsorption capacity. The calculated  $\Delta G^\circ$ ,  $\Delta H^\circ$ , and  $\Delta S^\circ$  values for MeB adsorption are summarized in

Table 4. The equilibrium constant  $K$  was calculated in dimensionless form before estimating  $\Delta G^\circ$ ,  $\Delta H^\circ$ , and  $\Delta S^\circ$ , in order to avoid the direct use of dimensional adsorption coefficients in thermodynamic calculations. The Gibbs free energy of adsorption was calculated using eqn (4) provided below.

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ \quad (4)$$

Accordingly, the thermochemical parameters  $\Delta H^\circ$  and  $\Delta S^\circ$  were calculated by applying the van't Hoff equation (eqn (5)).

$$\ln K = -\frac{\Delta H^\circ}{RT} + \frac{\Delta S^\circ}{R} \quad (5)$$

$R$  represents the universal gas constant. The enthalpy change ( $\Delta H^\circ$ ) and entropy change ( $\Delta S^\circ$ ) values were determined from the slope and intercept of the linear plot of  $\ln K$  versus  $1/T$ , in accordance with the van't Hoff approach.<sup>39</sup> The standard enthalpy change ( $\Delta H^\circ$ ) was determined to be  $16.827 \text{ kJ mol}^{-1}$  for  $\text{Al}_4\text{B}_2\text{O}_9$  and  $17.130 \text{ kJ mol}^{-1}$  for  $\text{Al}_5\text{BO}_9$ . Positive  $\Delta H^\circ$  values indicate that MeB adsorption increases with heat input and that the process proceeds *via* an endothermic pathway. The  $\Delta G^\circ$  values became more negative with increasing temperature, changing from  $-7.091$  to  $-9.498 \text{ kJ mol}^{-1}$  for  $\text{Al}_4\text{B}_2\text{O}_9$  and from  $-7.598$  to  $-10.087 \text{ kJ mol}^{-1}$  for  $\text{Al}_5\text{BO}_9$  as the temperature increased from  $298$  to  $328 \text{ K}$ . The  $\Delta G^\circ$  results confirm that the adsorption of MeB is both favorable and spontaneous. The positive value of  $\Delta S^\circ$  suggests a change in the degree of disorder at the adsorbent/solution interface during adsorption, suggesting increased randomness at the solid solution interface during MeB adsorption.<sup>40</sup>

Fig. 11 presents the variation of  $\ln K$  with respect to  $1/T$  for the  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  materials. The linear and negative trend obtained indicates that the systems follow Van't Hoff behavior. The negative slope of the  $\ln K$  versus  $1/T$  plot is consistent with the positive  $\Delta H^\circ$  values, supporting the endothermic nature of MeB adsorption.

#### Effect of initial MeB concentration and adsorption isotherms

The initial dye concentration is a critical parameter in adsorption studies, as it directly influences the driving force for mass

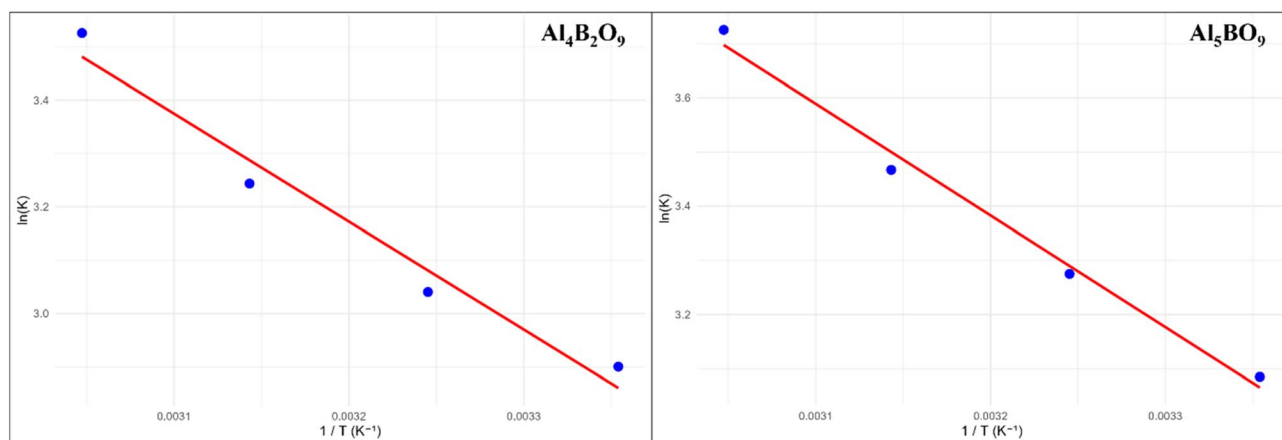


Fig. 11 Van't Hoff plots for MeB adsorption onto  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  ( $\ln K - 1/T$ ).



transfer.<sup>41</sup> The initial concentration of MeB is considered to be closely associated with the adsorption capacity. In this study, MeB concentrations ranging from 25 to 200 mg L<sup>-1</sup> were investigated. The other experimental conditions were kept constant at an adsorbent dosage of 0.05 g, a temperature of 25 °C and a contact time of 60 minutes. As the MeB concentration increases while the adsorbent dosage remains constant, the adsorbent surface may approach saturation. This behavior can be attributed to the limited number of active adsorption sites available on Al<sub>4</sub>B<sub>2</sub>O<sub>9</sub> and Al<sub>5</sub>BO<sub>9</sub>. Consequently, different maximum adsorption values are obtained for varying initial concentrations at a fixed adsorbent dosage. Adsorption isotherm parameters are widely used to describe how adsorbate molecules interact with adsorbent surface sites and how equilibrium is established. These parameters provide insight into the adsorption capacity of the adsorbent, the nature of the adsorption process, and its overall efficiency. Langmuir,<sup>42</sup> Freundlich,<sup>43</sup> Scatchard,<sup>44</sup> and Temkin<sup>45</sup> models were applied to interpret the equilibrium behavior of MeB adsorption and to assess the adsorption capacity of the synthesized borates, as presented in Table 5.

Adsorption isotherm models, such as the Langmuir model, are frequently employed to describe complex adsorption behavior. The Langmuir isotherm assumes that adsorption occurs as a monolayer on a homogeneous surface with identical

Table 6 Comparison of MeB adsorption capacities reported for different adsorbents

Adsorbent	Adsorption capacity (mg g <sup>-1</sup> )	References
MGLfsB	11.148	47
nM-MGLfsB	13.089	47
Magnetic Ni <sub>0.1</sub> Mg <sub>0.7</sub> Co <sub>0.2</sub> Fe <sub>2</sub> O <sub>4</sub>	2784.100	48
Activated carbon	53.000	48
Novel CaCO <sub>3</sub> /chitin aerogel	266.400	48
Na <sub>2</sub> Al <sub>2</sub> B <sub>2</sub> O <sub>7</sub>	2000.000	49

Adsorbent	Adsorption capacity (mg g <sup>-1</sup> )		References
	Langmuir	Freundlich (K <sub>F</sub> ) constant	
Al <sub>5</sub> BO <sub>9</sub>	105.785 mg g <sup>-1</sup>	27.072	This study
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	70.547 mg g <sup>-1</sup>	21.146	This study

binding sites and without interaction between adsorbed molecules. In this model,  $q_{\max}$  represents the maximum adsorption capacity, whereas  $K_L$  denotes the Langmuir adsorption equilibrium constant, which is commonly associated with adsorbate and adsorbent affinity.<sup>42,46</sup> The higher  $K_L$  value obtained for

Table 5 Isotherm model parameters for MeB adsorption onto Al<sub>4</sub>B<sub>2</sub>O<sub>9</sub> and Al<sub>5</sub>BO<sub>9</sub>

Isotherm	Isotherm parameters linear form			
	$q_{\max}$	$K_L$ (L mg <sup>-1</sup> )	$R^2$	
Langmuir ( $1/q_e$ vs. $1/C_e$ )	70.547	1.87	0.966	$C_0$ 25
				$R_L$ 0.0209
				$R_L$ 0.0158
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	70.547	1.87	0.966	50
				75
				100
Al <sub>5</sub> BO <sub>9</sub>	105.785	2.5	0.965	150
				200
				200
Al <sub>5</sub> BO <sub>9</sub>	105.785	2.5	0.965	200
				0.0036
				0.0027
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	70.547	1.87	0.966	0.0027
				0.0053
				0.0071
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	70.547	1.87	0.966	0.0071
				0.0053
				0.0053
Al <sub>5</sub> BO <sub>9</sub>	105.785	2.5	0.965	0.0040
				0.0040
				0.0027
Al <sub>5</sub> BO <sub>9</sub>	105.785	2.5	0.965	0.0027
				0.0027
				0.0020

Isotherm	Isotherm parameters linear form		
	$K_F$	$1/n$	$R^2$
Freundlich ( $\log C_e$ vs. $\log q_e$ )			
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	21.146	0.488	0.986
Al <sub>5</sub> BO <sub>9</sub>	27.072	0.705	0.988

Isotherm	Isotherm parameters linear form		
	$Q_s$	$K_b$	$R^2$
Scatchard ( $q_e$ vs. $q_e/C_e$ )			
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	98.903	0.268	0.680
Al <sub>5</sub> BO <sub>9</sub>	183.69	0.178	0.657

Isotherm	Isotherm parameters linear form		
	$B_t$	$K_t$	$R^2$
Temkin ( $\ln C_e$ vs. $q_e$ )			
Al <sub>4</sub> B <sub>2</sub> O <sub>9</sub>	20.758	2.78	0.885
Al <sub>5</sub> BO <sub>9</sub>	32.899	2.63	0.895



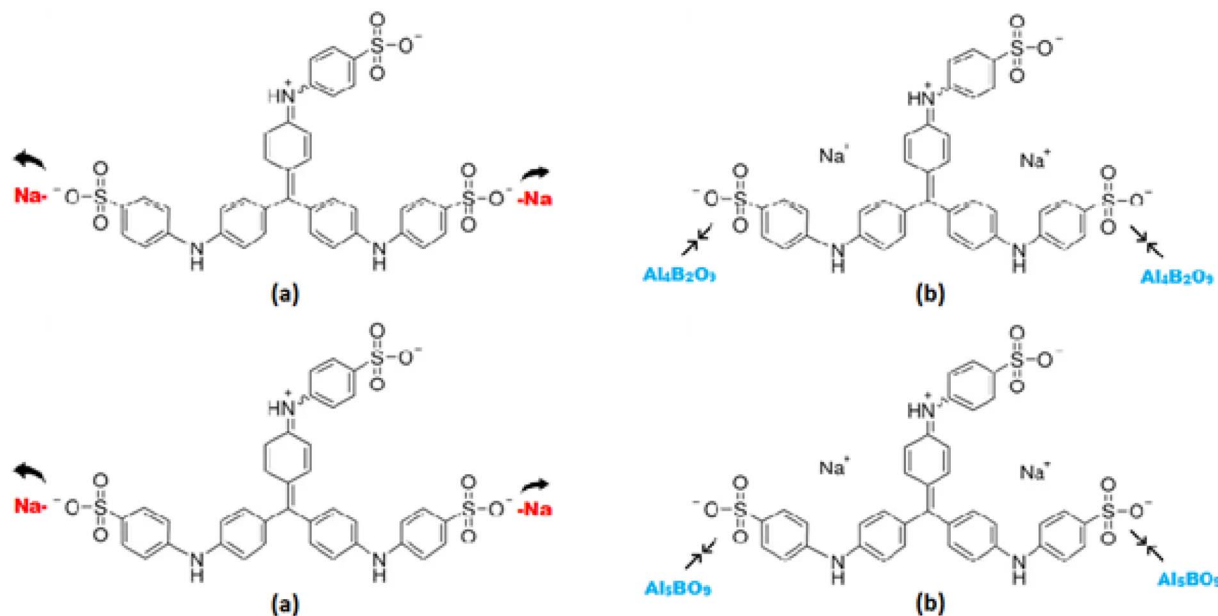


Fig. 12 Proposed adsorption mechanism of MeB onto  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$ . (a) and (b) represent possible adsorption pathways.

$\text{Al}_5\text{BO}_9$  indicates a stronger binding affinity and higher interaction energy. The calculated separation factor ( $R_L$ ) values were found to be in the range of ( $\text{Al}_4\text{B}_2\text{O}_9$ : 0.0027–0.0209,  $\text{Al}_5\text{BO}_9$ : 0.0020–0.0158) indicating highly favorable adsorption behavior. The  $R_L$  values approaching zero suggest a strong affinity between the adsorbate and the adsorbent surface, supporting the favorable nature of adsorption within the Langmuir framework. The suitability of each isotherm model was assessed by comparing the corresponding  $R^2$  values with the experimental equilibrium data. The model with a regression coefficient closest to unity is considered to provide the best fit to the adsorption process. For both adsorbents, the adsorption data were found to be more consistent with the Freundlich isotherm model ( $R^2 = 0.986$  and  $0.988$ ). According to the Freundlich model, the  $K_F$  constants were calculated as 21.146 for  $\text{Al}_4\text{B}_2\text{O}_9$  and 27.072 for  $\text{Al}_5\text{BO}_9$ . This behavior indicates that MeB removal is likely associated with heterogeneous adsorption sites and may involve multilayer adsorption contributions. Although the Freundlich model provided the best fit, the Langmuir model was also used to estimate the maximum monolayer adsorption capacities, which were determined as  $70.547 \text{ mg g}^{-1}$  for  $\text{Al}_4\text{B}_2\text{O}_9$  and  $105.785 \text{ mg g}^{-1}$  for  $\text{Al}_5\text{BO}_9$ . The Scatchard analysis yielded relatively low correlation coefficients ( $R^2 \approx 0.65$ – $0.68$ ) for both adsorbents, indicating that the adsorption process cannot be adequately described by a single class of homogeneous binding sites. Although the higher  $Q_s$  value obtained for  $\text{Al}_5\text{BO}_9$  suggests a greater theoretical adsorption capacity, the poor fit implies that the model is not suitable for this system. Overall, the Scatchard model appears insufficient to accurately represent the adsorption mechanism. Similar studies on MeB removal reported in the literature are summarized in Table 6.

Various methods and material systems have been developed in the literature for dye removal. Hybrid flocculation-photocatalysis systems have been reported to achieve high

removal efficiencies,<sup>50</sup> while dual-functional materials such as Fe@ZIF-8 enable effective treatment by combining adsorption with advanced oxidation processes.<sup>51</sup> In addition, Z-scheme photocatalysts have demonstrated rapid degradation under visible light irradiation.<sup>52</sup> In contrast, the present study focuses on the synthesis of aluminum borates ( $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$ ), offering a different adsorption-based approach.

### Proposed adsorption mechanism

$\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  are oxygen-rich aluminum borate structures, which may provide surface oxygen-containing sites involved in MeB adsorption. The measured negative zeta potential values support that the borate surfaces possess negatively charged sites under the selected measurement conditions. The ionization behavior of MeB, an anionic dye, in aqueous medium is illustrated in Fig. 12a. In aqueous solution, MeB exists predominantly as an anionic dye due to the dissociation of sulfonate groups. Under acidic conditions, partial protonation of surface hydroxyl sites on aluminum borates may reduce electrostatic repulsion and promote interactions between the adsorbent surface and the anionic sulfonate groups of MeB. In addition to electrostatic interactions, possible interactions with Al-based surface sites and pore filling effects may contribute to the overall adsorption process. The proposed adsorption mechanism between MeB and the aluminum borate surfaces is schematically presented in Fig. 12a and b.

## Conclusion

In recent years, various materials have been investigated for the adsorption of MeB dye from wastewater, and researchers have extensively examined the effectiveness of different adsorbents



for this application. In the present study,  $\text{Al}_4\text{B}_2\text{O}_9$  and  $\text{Al}_5\text{BO}_9$  were synthesized and characterized. Subsequent systematic adsorption experiments revealed that maximum MeB adsorption occurred at pH 3, while removal efficiency decreased progressively toward pH 9. Under acidic conditions, partial protonation of surface hydroxyl sites may reduce electrostatic repulsion and facilitate the adsorption of anionic MeB species onto aluminum borate surfaces. Although sulfonate groups remain negatively charged due to their strong acidity, they may interact with surface Al-based sites, thereby contributing to MeB adsorption. In alkaline conditions, both the dye molecules and the aluminum borate surface carry negative charges, leading to electrostatic repulsion and reduced adsorption. The removal efficiency of MeB increased with increasing adsorbent dosage, reaching a maximum of 96.24% for  $\text{Al}_4\text{B}_2\text{O}_9$  and 99.21% for  $\text{Al}_5\text{BO}_9$ . However, no substantial improvement in removal efficiency was observed beyond 0.05 g, indicating that this dosage represented a practical optimum under the studied conditions. Equilibrium was reached within approximately 60 min, with rapid removal at the initial stage followed by a slower adsorption rate as the available surface sites became occupied. The PSO model most suitably described the kinetic behavior of MeB adsorption on both borates, suggesting that the rate was mainly governed by the accessibility of active adsorption sites. An increase in temperature resulted in a corresponding increase in the amount of MeB adsorbed by the adsorbents. This finding indicates that MeB adsorption onto both borates proceeds as an endothermic adsorption process ( $\Delta H = 16.827 \text{ kJ mol}^{-1}$  for  $\text{Al}_4\text{B}_2\text{O}_9$ ;  $17.130 \text{ kJ mol}^{-1}$  for  $\text{Al}_5\text{BO}_9$ ). The adsorption data were more consistent with the Freundlich isotherm model ( $R^2 = 0.986$  and  $0.988$ ), suggesting adsorption on energetically heterogeneous surface sites with a possible contribution from multilayer adsorption. A key limitation of this study is that it was conducted using a single component dye system under controlled laboratory conditions, which may restrict its direct applicability to complex real wastewater matrices containing multiple competing contaminants. In addition, the reusability and regeneration performance of the adsorbents were not evaluated, statistical error analysis was not performed, and shorter contact times were not investigated, which remain critical factors for future studies in terms of large scale application and economic feasibility.

## Informed consent

All authors agree to this publication.

## Author contributions

U. Özkan: formal analysis, resources, methodology, investigation, writing – original draft, writing – review & editing, software, validation, visualization. O. Bayram: conceptualization, formal analysis, investigation, methodology, project administration, software, validation, visualization. E. Moral: conceptualization, data curation, investigation, validation, visualization, writing – original draft, writing – review & editing. İ. Pekgözlü: investigation, methodology, writing – original draft, writing –

review & editing. F. Göde: data curation, conceptualization, formal analysis, supervision, writing – original draft, writing – review & editing.

## Conflicts of interest

The authors declare that they have no conflict of interest.

## Data availability

Data will be available on reasonable request.

## References

- 1 S. T. Al-Asadi, F. F. Al-Qaim, H. F. S. Al-Saedi, I. F. Deyab, H. Kamyab and S. Chelliapan, Adsorption of methylene blue dye from aqueous solution using low-cost adsorbent: kinetic, isotherm adsorption, and thermodynamic studies, *Environ. Monit. Assess.*, 2023, **195**(6), 676, DOI: [10.1007/s10661-023-11334-2](https://doi.org/10.1007/s10661-023-11334-2).
- 2 A. P. Periyasamy, Recent advances in the remediation of textile-dye-containing wastewater: prioritizing human health and sustainable wastewater treatment, *Sustainability*, 2024, **16**(2), 495, DOI: [10.3390/su16020495](https://doi.org/10.3390/su16020495).
- 3 T. Javed, A. Thumma, A. N. Uddin, R. Akhter, M. Babar Taj, S. Zafar and M. Batool, Batch adsorption study of Congo Red dye using unmodified *Azadirachta indica* leaves: isotherms and kinetics, *Water Pract. Technol.*, 2024, **19**(2), 546–566, DOI: [10.2166/wpt.2024.020](https://doi.org/10.2166/wpt.2024.020).
- 4 N. Hamri, A. Imessaoudene, A. Hadadi, S. Cheikh, A. Boukerroui, J. C. Bollinger, A. Amrane, H. Tahraoui, H. N. Tran, A. O. Ezzat, H. A. A. Lohedan and L. Mouni, Enhanced adsorption capacity of methylene blue dye onto kaolin through acid treatment: batch adsorption and machine learning studies, *Water*, 2024, **16**(2), 243, DOI: [10.3390/w16020243](https://doi.org/10.3390/w16020243).
- 5 V. Watwe, S. Kulkarni and P. Kulkarni, Development of dried uncharred leaves of *Ficus benjamina* as a novel adsorbent for cationic dyes: Kinetics, isotherm, and batch optimization, *Ind. Crops Prod.*, 2023, **195**, 116449, DOI: [10.1016/j.indcrop.2023.116449](https://doi.org/10.1016/j.indcrop.2023.116449).
- 6 N. R. M. Tanure, L. C. Maia, L. C. Soares, M. M. C. Elias, G. P. da Silva, E. R. de Azevedo and L. V. A. Gurgel, Removal of a model reactive azo dye from aqueous solution by a bioadsorbent in batch and fixed-bed column modes: application of the developed technology to a textile wastewater, *Water Resour. Ind.*, 2024, **32**, 100261, DOI: [10.1016/j.wri.2024.100261](https://doi.org/10.1016/j.wri.2024.100261).
- 7 M. Taha, A. Elsayed, M. Abbas, H. Fakhry and E. M. Ali, Bio-adsorption of Methyl blue from Synthetic wastewater onto copperzinc oxides Bimetallic Nanoparticles Synthesized by *Fusarium oxysporum*: Equilibrium isotherms, Kinetic models, Process optimization, and Antibacterial activity, *Egypt. J. Chem.*, 2024, **67**(2), 513–526, DOI: [10.21608/ejchem.2023.213597.8029](https://doi.org/10.21608/ejchem.2023.213597.8029).
- 8 O. A. Oyewo, N. G. Nevondo, D. C. Onwudiwe and M. S. Onyango, Photocatalytic degradation of methyl blue



- in water using sawdust-derived cellulose nanocrystals-metal oxide nanocomposite, *J. Inorg. Organomet. Polym. Mater.*, 2021, **31**(6), 2542–2552, DOI: [10.1007/s10904-020-01847-5](https://doi.org/10.1007/s10904-020-01847-5).
- 9 C. Cui, T. Gao, C. H. Bi, L. J. Wang and D. Li, Highly efficient methyl blue dye adsorption by chitosan-gelatin-poly-L-lysine composite sponges with one-pot preparation: Characterization, adsorption performance, and DFT study, *Int. J. Biol. Macromol.*, 2026, 150630, DOI: [10.1016/j.ijbiomac.2026.150630](https://doi.org/10.1016/j.ijbiomac.2026.150630).
- 10 L. Z. Huo, C. F. Guo, Z. X. Gong, H. Xu, X. J. Yang, Y. X. Wang and X. P. Luo, Preparation of Aminated Sodium Lignosulfonate and Efficient Adsorption of Methyl Blue Dye, *Materials*, 2024, **17**(5), 1046, DOI: [10.3390/ma17051046](https://doi.org/10.3390/ma17051046).
- 11 M. D. Khan, A. Singh, M. Z. Khan, S. Tabraiz and J. Sheikh, Current perspectives, recent advancements, and efficiencies of various dye-containing wastewater treatment technologies, *J. Water Process Eng.*, 2023, **53**, 103579, DOI: [10.1016/j.jwpe.2023.103579](https://doi.org/10.1016/j.jwpe.2023.103579).
- 12 N. M. Hosny, I. Gomaa and M. G. Elmahgary, Adsorption of polluted dyes from water by transition metal oxides: A review, *Appl. Surf. Sci. Adv.*, 2023, **15**, 100395, DOI: [10.1016/j.apsadv.2023.100395](https://doi.org/10.1016/j.apsadv.2023.100395).
- 13 J. Yang, Y. Zhang, J. Liu, S. Xie, W. Cao, E. Liao, C. Chen, D. Yang, Z. Chen, X. Liu and J. Qiu, Boroaluminosilicate glass-ceramics containing mullite-type  $\text{Cr}^{3+}$ :  $\text{Al}_4\text{B}_2\text{O}_9$  nanocrystals with broadband near-infrared luminescence, *J. Eur. Ceram. Soc.*, 2023, **43**(14), 6356–6362, DOI: [10.1016/j.jeurceramsoc.2023.06.019](https://doi.org/10.1016/j.jeurceramsoc.2023.06.019).
- 14 H. Jia, Y. Guo and C. Liu, Transparent aluminoborosilicate glass-ceramics containing  $\text{Al}_4\text{B}_2\text{O}_9$  nanorods, *Ceram. Int.*, 2024, **50**(17), 29468–29475, DOI: [10.1016/j.ceramint.2024.05.241](https://doi.org/10.1016/j.ceramint.2024.05.241).
- 15 B. A. Al-Mur and M. T. Jamal, Eco-Friendly Dye Removal Using Chitosan: Characterization and Kinetic Modeling of Methylene Blue and Methyl Orange Adsorption, *Polymers*, 2026, **18**(5), 546, DOI: [10.3390/polym18050546](https://doi.org/10.3390/polym18050546).
- 16 P. Maziarka, C. Wurzer, P. J. Arauzo, A. Dieguez-Alonso, O. Mašek and F. Ronsse, Do you BET on routine? The reliability of  $\text{N}_2$  physisorption for the quantitative assessment of biochar's surface area, *Chem. Eng. J.*, 2021, **418**, 129234, DOI: [10.1016/j.cej.2021.129234](https://doi.org/10.1016/j.cej.2021.129234).
- 17 R. X. Fischer, V. Kahlenberg, D. Voll, K. J. MacKenzie, M. E. Smith, B. Schnetger, H. J. Brumsack and H. Schneider, Crystal structure of synthetic  $\text{Al}_4\text{B}_2\text{O}_9$ : A member of the mullite family closely related to boralsilite, *Am. Mineral.*, 2008, **93**(5–6), 918–927, DOI: [10.2138/am.2008.2744](https://doi.org/10.2138/am.2008.2744).
- 18 Y. Fan, J. Chen, Y. Xue, X. Xu, J. Lin, L. Hu, Z. Lu, X. Zhang, Z. Mo, C. Liu, F. Meng and C. Tang, Controlled synthesis of boron nitride (BN) coating on  $\text{Al}_4\text{B}_2\text{O}_9$  nanowhiskers, *J. Nanopart. Res.*, 2013, **15**(6), 1699, DOI: [10.1007/s11051-013-1699-x](https://doi.org/10.1007/s11051-013-1699-x).
- 19 İ. Pekgözlü, Luminescence Properties of  $\text{Al}_4\text{B}_2\text{O}_9$ : M (M =  $\text{Dy}^{3+}$ ,  $\text{Sm}^{3+}$ , and  $\text{Tb}^{3+}$ ), *J. Appl. Spectrosc.*, 2024, **90**(6), 1372–1375, DOI: [10.1007/s10812-024-01675-2](https://doi.org/10.1007/s10812-024-01675-2).
- 20 Y. Zheng and D. Chen, Luminescence studies on  $\text{Al}_4\text{B}_2\text{O}_9$ :  $\text{Eu}^{2+}$  phosphor crystals, *Luminescence*, 2011, **26**(6), 481–485, DOI: [10.1002/bio.1256](https://doi.org/10.1002/bio.1256).
- 21 L. Fan, C. Luo, X. Li, F. Lu, H. Qiu and M. Sun, Fabrication of novel magnetic chitosan grafted with graphene oxide to enhance adsorption properties for methyl blue, *J. Hazard. Mater.*, 2012, **215**, 272–279, DOI: [10.1016/j.jhazmat.2012.02.068](https://doi.org/10.1016/j.jhazmat.2012.02.068).
- 22 Y. Dong, X. Dong, L. Li, J. Wu, L. Yan, J. Liu and A. Guo, Lightweight and thermally insulating aluminum borate nanofibrous porous ceramics, *Ceram. Int.*, 2021, **47**(15), 21029–21037, DOI: [10.1016/j.ceramint.2021.04.104](https://doi.org/10.1016/j.ceramint.2021.04.104).
- 23 A. M. M. Tamboli and J. M. Tade, Zeta Potential: A Comprehensive Review, *IRJPMS*, 2025, **8**(2), 115–124.
- 24 M. Chand, A. Kumawat and S. Srivastava, Zeta Potential-Mediated Comparative Adsorption Study of Cationic (Methylene Blue) and Anionic (Congo Red) Dye onto Spent Tea (*Camellia sinensis*) Leaves Powder, *Surf. Interfaces*, 2025, 108271, DOI: [10.1016/j.surfin.2025.108271](https://doi.org/10.1016/j.surfin.2025.108271).
- 25 E. Makhado, Preparation of carboxymethyl cellulose-based silica hydrogel nanocomposite for methylene blue and malachite green dyes adsorption from aqueous solution, *Surf. Interfaces*, 2025, **56**, 105699, DOI: [10.1016/j.surfin.2024.105699](https://doi.org/10.1016/j.surfin.2024.105699).
- 26 D. Teng, C. Liu, L. Ma, P. Jin, G. Fan, P. Li, Y. Cao and W. Wang, Selective adsorption of Ga (III) from aqueous solutions using magnetic chitosan-based ion-imprinted polymers: Synthesis optimization and mechanistic insights, *Int. J. Biol. Macromol.*, 2025, **298**, 139957, DOI: [10.1016/j.ijbiomac.2025.139957](https://doi.org/10.1016/j.ijbiomac.2025.139957).
- 27 S. Zhao, F. Zhou, L. Li, M. Cao, D. Zuo and H. Liu, Removal of anionic dyes from aqueous solutions by adsorption of chitosan-based semi-IPN hydrogel composites, *Composites, Part B*, 2012, **43**(3), 1570–1578, DOI: [10.1016/j.compositesb.2012.01.015](https://doi.org/10.1016/j.compositesb.2012.01.015).
- 28 U. Ö. Bayram, İ. Pekgözlü, F. Göde and E. Esmeray, Removal of alizarin yellow GG by  $\text{K}_2\text{Al}_2\text{B}_2\text{O}_7$ : modeling with artificial neural networks (ANNs), *Int. J. Environ. Sci. Technol.*, 2026, **23**(4), 302, DOI: [10.1007/s13762-026-07075-7](https://doi.org/10.1007/s13762-026-07075-7).
- 29 M. A. A. H. Allah, H. K. Ibrahim and H. A. Alshamsi, Enhanced adsorption, anticancer and antibacterial potentials of *Pontederia crassipes* L. extract mediated ecofriendly synthesized  $\text{ZnO}$ /biochar nanohybrid, *Inorg. Chem. Commun.*, 2025, **171**, 113538, DOI: [10.1016/j.inoche.2024.113538](https://doi.org/10.1016/j.inoche.2024.113538).
- 30 A. M. Omer, R. Dey, A. S. Eltaweil, E. M. Abd El-Monaem and Z. M. Ziora, Insights into recent advances of chitosan-based adsorbents for sustainable removal of heavy metals and anions, *Arabian J. Chem.*, 2022, **15**(2), 103543.
- 31 U. Özkan, O. Bayram and H. T. Şahin, Effect of sorption parameters on the removal of malachite green with modified *Juniperus Excelsa* cone biochar, *Biomass Convers. Biorefin.*, 2025, **15**(18), 25093–25106, DOI: [10.1007/s13399-025-06797-x](https://doi.org/10.1007/s13399-025-06797-x).
- 32 A. Mishra, L. Kaur, M. Sharma, P. Sharma, S. Murab, H. Ojha, J. Pandey and M. Pathak, Magnetic Biochar from marigold floral waste: synthesis, characterization, and



- adsorptive removal of methylene blue, *J. Mol. Struct.*, 2025, **1341**, 142657, DOI: [10.1016/j.molstruc.2025.142657](https://doi.org/10.1016/j.molstruc.2025.142657).
- 33 M. Kurniasih, N. H. Aprilita, R. Roto and M. Mudasir, Modification of coal fly ash for high capacity adsorption of methylene blue, *Case Stud. Chem. Environ. Eng.*, 2025, **11**, 101101, DOI: [10.1016/j.cscee.2025.101101](https://doi.org/10.1016/j.cscee.2025.101101).
- 34 W. T. Sibhat, H. S. Ayele, M. Atlabachew, K. S. Mohammed, B. A. Aragaw, B. Abebaw and D. T. Ayele, Effect of Ethiopian kaolin treatment on the performance of adsorptive removal of methylene blue dye, *Results Chem.*, 2025, **13**, 102027, DOI: [10.1016/j.rechem.2025.102027](https://doi.org/10.1016/j.rechem.2025.102027).
- 35 R. Zein, J. S. Purnomo, P. Ramadhani, M. F. Alif and C. N. Putri, Enhancing sorption capacity of methylene blue dye using solid waste of lemongrass biosorbent by modification method, *Arabian J. Chem.*, 2023, **16**(2), 104480.
- 36 G. Muteeb, K. Ansari, M. Eyvaz, M. Farhan, M. Aatif, D. Agrawal, M. E. Oirdi and M. H. Dehghani, Removal of methylene blue (MB) dye from water and wastewater using acid-activated chicken bone in a batch adsorption process, *Sci. Rep.*, 2025, **15**(1), 23098, DOI: [10.1038/s41598-025-08341-3](https://doi.org/10.1038/s41598-025-08341-3).
- 37 B. Kuppusamy, F. R. Mohamed Ismail, P. Balakrishnan, S. C. Kim, S. P. Asrafali and T. Periyasamy, From Biomass to Adsorbent: A Comprehensive Review on Bio-Derived Carbons for Dye Removal, *Polymers*, 2026, **18**(2), 180, DOI: [10.3390/polym18020180](https://doi.org/10.3390/polym18020180).
- 38 K. W. Jung, B. H. Choi, M. J. Hwang, T. U. Jeong and K. H. Ahn, Fabrication of granular activated carbons derived from spent coffee grounds by entrapment in calcium alginate beads for adsorption of acid orange 7 and methylene blue, *Bioresour. Technol.*, 2016, **219**, 185–195, DOI: [10.1016/j.biortech.2016.07.098](https://doi.org/10.1016/j.biortech.2016.07.098).
- 39 A. El Jery, H. S. K. Alawamleh, M. H. Sami, H. A. Abbas, S. S. Sammen, A. Ahsan, M. A. Imteaz, A. Shanableh, Md. Shafiquzzaman, H. Osman and N. Al-Ansari, Isotherms, kinetics and thermodynamic mechanism of methylene blue dye adsorption on synthesized activated carbon, *Sci. Rep.*, 2024, **14**(1), 970, DOI: [10.1038/s41598-023-50937-0](https://doi.org/10.1038/s41598-023-50937-0).
- 40 M. Bellaj, K. Aziz, M. El Achaby, M. El Haddad, L. Gebrati, T. A. Kurniawan, Z. Chen, P. S. Yap and F. Aziz, Cationic and anionic dyes adsorption from wastewater by clay-chitosan composite: an integrated experimental and modeling study, *Chem. Eng. Sci.*, 2024, **285**, 119615, DOI: [10.1016/j.ces.2023.119615](https://doi.org/10.1016/j.ces.2023.119615).
- 41 S. El Meziyani, H. Agnaou, H. El Haddaj, W. Boumya, N. Barka and A. Elhalil, Sustainable adsorption technologies for textile dye removal: advances in biomass-derived and magnetically modified activated carbons, *Clean. Chem. Eng.*, 2025, 100210, DOI: [10.1016/j.clce.2025.100210](https://doi.org/10.1016/j.clce.2025.100210).
- 42 I. Langmuir, The Constitution And Fundamental Properties of Solids And Liquids. Part I. Solids, *J. Am. Chem. Soc.*, 1916, **38**(11), 2221–2295, DOI: [10.1021/ja02268a002](https://doi.org/10.1021/ja02268a002).
- 43 H. Freundlich, Über die adsorption in lösungen, *Z Phys Chem*, 1907, **57**(1), 385–470.
- 44 G. Scatchard, The attractions of proteins for small molecules and ions, *Ann. N. Y. Acad. Sci.*, 1949, **51**, 660–672, DOI: [10.1111/j.1749-6632.1949.tb27297.x](https://doi.org/10.1111/j.1749-6632.1949.tb27297.x).
- 45 M. J. Temkin and V. Pyzhev, *Acta Physico Chem USSR*, 1940, **12**, 217–222.
- 46 H. N. Tran, Improper estimation of thermodynamic parameters in adsorption studies with distribution coefficient KD ( $q_e/C_e$ ) or Freundlich constant ( $K_F$ ): Considerations from the derivation of dimensionless thermodynamic equilibrium constant and suggestions, *Adsorpt. Sci. Technol.*, 2022, **2022**, 5553212, DOI: [10.1155/2022/5553212](https://doi.org/10.1155/2022/5553212).
- 47 O. Bayram, U. Özkan, S. Kardeş, E. Moral, F. Göde and E. Pehlivan, Sustainable decolorization of methyl blue and malachite green from an aqueous environment using magnetic biochar prepared from the fruit seeds of *Mespilus germanica* L, *Chem. Ecol.*, 2025, **41**(4), 528–551, DOI: [10.1080/02757540.2024.2447582](https://doi.org/10.1080/02757540.2024.2447582).
- 48 C. Ling, Z. Wang, Y. Ni, Z. Zhu, Z. Cheng and R. Liu, Superior adsorption of methyl blue on magnetic Ni-Mg-Co ferrites: Adsorption electrochemical properties and adsorption characteristics, *Environ. Prog. Sustainable Energy*, 2022, **41**(6), e13923, DOI: [10.1002/ep.13923](https://doi.org/10.1002/ep.13923).
- 49 O. Bayram, U. Özkan, İ. Pekgözlü and F. Göde, Methyl blue removal by  $\text{Na}_2\text{Al}_2\text{B}_2\text{O}_7$  modeled with artificial neural networks: Synthesis, kinetics, isotherm, thermodynamic studies, *Sep. Sci. Technol.*, 2025, **60**(11), 1406–1420, DOI: [10.1080/01496395.2025.2498450](https://doi.org/10.1080/01496395.2025.2498450).
- 50 Y. Wang, Q. Geng, J. Yang, Y. Liu and C. Liu, Hybrid system of flocculation–photocatalysis for the decolorization of crystal violet, reactive red X-3B, and acid orange II dye, *ACS Omega*, 2020, **5**(48), 31137–31145, DOI: [10.1021/acsomega.0c04285](https://doi.org/10.1021/acsomega.0c04285).
- 51 X. Wu, Y. Lin, Z. Pi and X. Tan, Dual-functional Fe@ ZIF-8 for efficient phosphite removal from wastewater: Synergistic peroxymonosulfate activation and adsorption, *Sep. Purif. Technol.*, 2025, **377**, 134236, DOI: [10.1016/j.seppur.2025.134236](https://doi.org/10.1016/j.seppur.2025.134236).
- 52 Y. Lin, S. Wu, X. Li, X. Wu, C. Yang, G. Zeng, Y. Peng, Q. Zhou and L. Lu, Microstructure and performance of Z-scheme photocatalyst of silver phosphate modified by MWCNTs and Cr-doped  $\text{SrTiO}_3$  for malachite green degradation, *Appl. Catal., B*, 2018, **227**, 557–570, DOI: [10.1016/j.apcatb.2018.01.054](https://doi.org/10.1016/j.apcatb.2018.01.054).

