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# Strategic integration of carbon nanotubes over the redox-active surfaces of FeCo<sub>2</sub>S<sub>4</sub> as an electrode material for developing high-efficiency supercapacitor devices

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Accelerating both electrical and ionic conductivity of spinel sulfides (AB<sub>2</sub>S<sub>4</sub>) presents a challenge that demands an urgent solution to improve their electrochemical properties for effective energy storage strategies. The need to develop electrode materials has been a significant step forward for the scientific community in enhancing electrochemical performance for supercapacitor applications. Therefore, incorporating carbon nanotubes (CNTs) into spinel sulfides could be an excellent option, serving as a model for new electrodes. To investigate this, FeCo<sub>2</sub>S<sub>4</sub> spinel sulfide was combined with CNTs via hydrothermal and solvothermal synthesis. A series of FeCo<sub>2</sub>S<sub>4</sub>/CNTs composites with 0, 3, 6, and 9 wt% CNTs were successfully prepared and confirmed via X-ray diffraction (XRD) technique. Meanwhile, Field Emission Scanning Electron Microscopy (FESEM) revealed topographical features, including web-like structures of the highest CNTs treated sample, with significantly improved interconnectivity that enhances ion and electron transport. The FeCo<sub>2</sub>S<sub>4</sub>/9% CNTs electrode delivered an efficient electrochemical response, with a specific capacity of 1059.62 C g<sup>-1</sup> at 10 A g<sup>-1</sup>, an energy density of 66.22 Wh kg<sup>-1</sup>, and a power density of 2250 W kg<sup>-1</sup>, while also retaining 98.8% of its initial capacity after 10k cycles. Electrochemical analyses further confirmed a hybrid charge-storage process, with low charge transfer resistance (5.15 Ω), stable conductivity (0.13 S cm<sup>-1</sup>), and a short relaxation time (0.010 s), yielding a maximum cation mobility of 3.81 × 10<sup>-10</sup> m<sup>2</sup> V<sup>-1</sup> s<sup>-1</sup> and a rate constant of 6.03 × 10<sup>-8</sup> cm s<sup>-1</sup> at 5.82 mA g<sup>-1</sup>. The fabricated asymmetric pseudocapacitive device facilitated the maximum energy and power density values of around 63.15 Wh kg<sup>-1</sup> and 10 800 W kg<sup>-1</sup>, respectively, in 1 M KOH electrolyte. These findings suggest that CNT-assisted FeCo<sub>2</sub>S<sub>4</sub> nanocomposites exhibit remarkable redox activity and transport properties, making them promising electrodes for high-performance supercapacitors.

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## 1. Introduction

In support of global sustainable development, research organizations are bridging the gap between energy production and consumption, thereby developing efficient and affordable energy conversion and storage solutions.<sup>1-6</sup> In this pursuit, supercapacitors (SC) have gained widespread attention as alternatives to batteries, thanks to their exceptional features such as high intrinsic power density (PD), excellent retention

capacity even at high current densities ( $I_m$ ), fast rechargeability, notable specific capacitance ( $C_{sp}$ ), and wide operating voltage.<sup>7-9</sup> Despite their rapid growth, SCs still face challenges in achieving high energy density (ED), which requires significant advancements.<sup>7,8</sup> In principle, the electrochemical performance of SC is primarily determined by its charge-storage mechanism. In this context, the electrochemical double-layer capacitance is commonly observed in high-specific-surface-area (SSA) carbon-based electrode materials, which involves rapid electrostatic adsorption at the electrode–electrolyte interface.<sup>9-12</sup> In contrast, transition metal-based compounds such as oxides (TMOs) and sulfides (TMS) typically exhibit pseudocapacitive (PC) behavior due to faradaic redox activities.<sup>13-15</sup> The presence or absence of functional groups and oxygen/sulfur vacancies are the major differences between these two categories of charge storage, determining whether an electrode material is redox-active or chemically inert.

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ammonium fluoride ( $\text{NH}_4\text{F}$ ), with a purity of 99.99%, and the functionalized CNTs with a diameter of 10–20 nm and 10–30  $\mu\text{m}$  length were purchased from Macklin Chemical Supplier.

## 2.2. Preparation of $\text{FeCo}_2\text{S}_4$ (PFCS)

A simple hydrothermal method was used to prepare the pure  $\text{FeCo}_2\text{S}_4$  (FCS) with molar ratios of F:Co:S = 1:2:4. The nitrate precursors,  $\text{SC}(\text{NH}_2)_2$  and  $\text{NH}_4\text{F}$ , with a purity of 99.99%, were used directly from the bottle without purification. Each chemical reagent, namely  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  and  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , was weighed at 0.582 g (2.0 mmol) and 0.404 g (1 mmol), respectively, and dissolved in separate beakers containing 25 mL and 20 mL of DI water.  $\text{SC}(\text{NH}_2)_2$  (0.304 g, 4.0 mmol) and  $\text{NH}_4\text{F}$  (0.148 g, 4.0 mmol) were added gradually with magnetic stirring at 250 rpm to the combined solution. This uniform solution was transferred into a thermally stable autoclave and heat-treated at 180 °C for 16 hours. After cooling, a suspension was formed, which was purified of impurities by centrifugation using DIW and ethanol several times. Thus, a precipitate was obtained that was dried at 70 °C for several hours in the Meilieur vacuum oven.

## 2.3. Preparation of $\text{FeCo}_2\text{S}_4/\text{CNTs}$

The solvothermal method was used to synthesize FCS@CNT composites at concentrations of 0% (100 mg), 3% (97 mg, 3 mg), 6% (94 mg, 6 mg), and 9% (91 mg, 9 mg). In parentheses, the values represent the weights of FCS and CNTs. The stoichiometrically weighed amounts were specified to sum to 100 mg of PFCS and CNTs. Specifically, the four samples created were labeled as PFCS (0% CNT), FCS-I (3% CNT), FCS-II (6% CNT),

and FCS-III (9% CNT). This solvothermal process is more user-friendly and cost-effective for producing particles in the nanometer range, along with improved morphology and porosity. In this process, measured amounts of CNTs (0, 3, 6, and 9 mg) were mixed into FCS (100, 97, 94, and 91 mg) in 40 mL of ethanol and subjected to vigorous ultrasonic treatment combined with stirring at 250 rpm for 1 hour to ensure homogeneous dispersion. After forming the carbonaceous mixture, it was carefully poured into a thermally stable autoclave (Fig. 2) and heated at 95 °C in a muffle furnace for 1 h. Then, the obtained precipitate was collected after the autoclave cooled, washed several times with ethanol and DIW during centrifugation, and carefully dried.

## 2.4. Preparation of the electrode

The electrode fabrication involves several primary steps. It begins with carefully cutting the nickel foam (NF) substrate into  $1 \times 1.25$  cm pieces. The reason for choosing NF over carbon cloth (CC) or metal foils is its low cost, notable conductivity, and electrochemical stability, which promote efficient conduction for the electrode material and electrolyte. To prepare the NF, pieces were immersed in an acidic solution comprising 13 mL of HCl in 37 mL of DIW. This solution helps remove contaminants and etch away the oxygen layer from the NF, thereby increasing surface roughness. Next, 85% active material, 10% binder (PVDF + DMF), and 5% activated carbon were mixed to prepare the slurry, which was then stirred vigorously for 8 hours. Herein, 10% binder was carefully added as per our lab optimizations and precautions to prepare the slurry. The binder (PVDF + DMF) facilitates excellent chemical adhesion of the

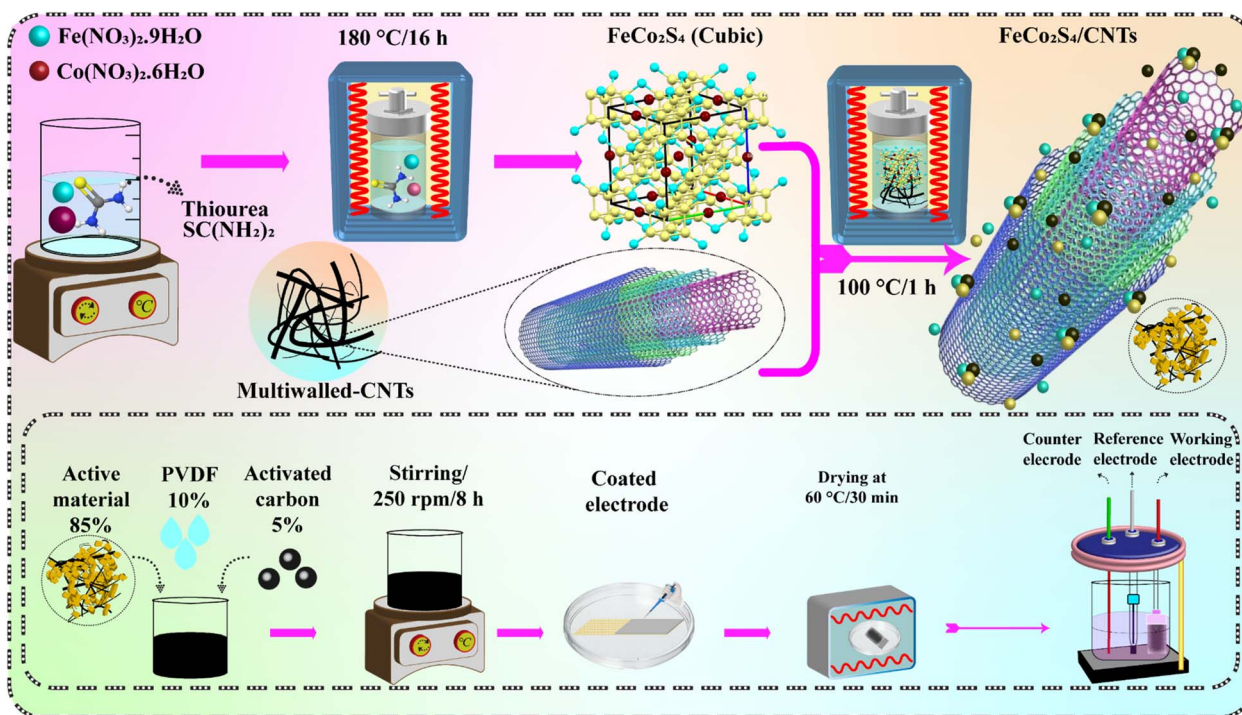


Fig. 2 Schematic profile of the sample's synthesis and electrode fabrication.



active material with NF and provides a wide electrochemical potential range. Furthermore, its addition ensures the mechanical stability of the fabricated material over repeated cycling, and the 10% binder solution is our optimized range, which ensures the stability of ion transport and limits internal resistance-related factors. Afterward, a Dragon pipette was carefully used to deposit the slurry onto the etched NF pieces. These coated NF dried at 60 °C for a few minutes before being used as an electrode for electrochemical testing, as shown in Fig. 2.

### 3. Results and discussion

#### 3.1. Structural analysis

A structural analysis of PFCS and its composites with 0, 3, 6, and 9% CNT contents was conducted to identify the crystalline phase within the  $2\theta$  range of 15° to 70°, as illustrated in the XRD patterns in Fig. 3(a). The methodology proposed by B. D. Cullity was used to identify and index these patterns. The major peaks were observed at  $2\theta = 21.10^\circ, 31.20^\circ, 37.95^\circ, 50.18^\circ,$  and  $55.10^\circ$ , corresponding to the respective values of  $hkl$  of (220), (311), (400), (511), and (440), which showed a good match with the JCPDS reference code 47-1738 confirming the cubic spinel structure of PFCS with no standard diffraction card and good match with a binary phase  $\text{Co}_3\text{S}_4$ . In the meantime, the remaining peaks at  $44.62^\circ, 51.98^\circ,$  and  $76.45^\circ$  were associated with diffraction probabilities for Ni with Miller indices (111), (200), and (220), respectively, originating from the nickel foam used as a substrate. It was also observed that the inclusion of CNTs did not affect the diffraction probabilities of associated planes in all samples. Matching these peaks with the exact crystal structure remains unresolved based on the literature survey of B. D. Cullity. Moreover, the crystal structure of PFCS was animated using VESTA software, with identical atomic positions in the unit cell, as displayed in Fig. 3(b). Additionally, the crystallite sizes of PFCS and FCS-III were estimated using Scherrer's equation, yielding values of 31 and 28.90 nm. The

decrease in crystallite size is attributed to lattice contraction and a reduced nucleation rate of PFCS in the composite sample, owing to strong van der Waals interactions. In principle, the high surface energy and abundant nucleation sites of CNTs promote heterogeneous nucleation, leading to a greater number of nuclei with restricted growth dimensions. The presence of CNT functional groups further suppresses crystallite growth kinetics by anchoring the growing domains.<sup>30,31</sup> From this perspective, the electrochemical properties of FCS-III are expected to outperform those of PFCS.

#### 3.2. Morphological and compositional analyses

The FESEM images were used at 25 000 $\times$  magnification to examine the morphology, shape, and arrangement of micro-particles in PFCS, FCS-I, FCS-II, and FCS-III electrode materials, as demonstrated in Fig. 4(a–d). The FESEM image in Fig. 4(a) revealed sharp morphological features of PFCS, with flake-like nanosheets combined with irregular nanoparticles. These flake-like nanosheets provide a high SSA, indicating potential for increased storage capacity due to greater interaction opportunities between electrolyte ions and the material. The image also reveals a significant porous structure in PFCS, evidenced by visible voids within the nanosheets and nanoparticles. This porosity can facilitate electrolyte ions in effectively engaging with exposed active sites, thereby maximizing electrochemical response. Additionally, the dense, agglomerated pattern of nanosheets and the clustering of nanoparticles may hinder efficient redox reactions and ion diffusion by restricting ion pathways. Nevertheless, the prominent features of this morphology are promising for future electrochemical applications.

Within this framework, the FESEM images of FCS-I, FCS-II, and FCS-III composites shown in Fig. 4(b–d) demonstrate key insights into CNTs integration with the PFCS matrix. The image of FCS-I clearly shows the growth of an interconnected fibrous network with significant nanoparticle agglomeration, as

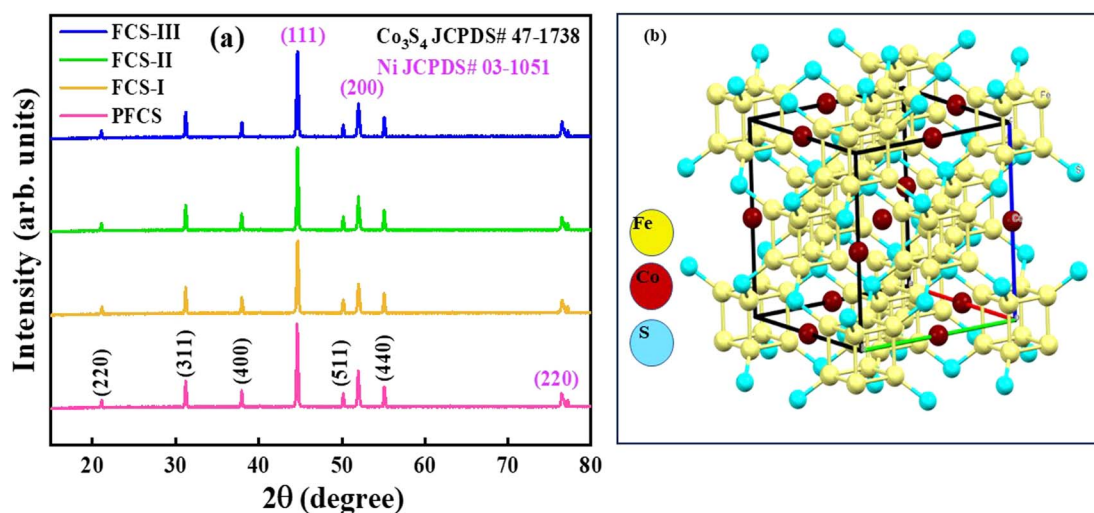


Fig. 3 (a) XRD patterns of PFCS, FCS-I, FCS-II, and FCS-III, and (b) crystal structure of PFCS.



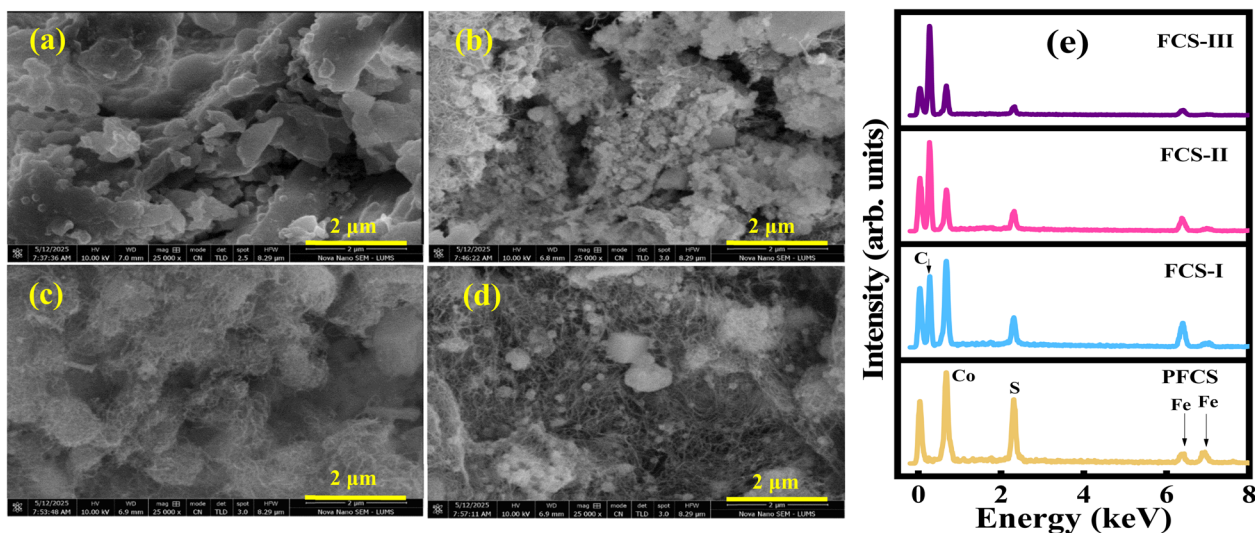


Fig. 4 (a–d) FESEM images of PFCS, FCS-I, FCS-II, and FCS-III, and (e) EDX spectra of as-synthesized materials.

illustrated in Fig. 4(b). This indicates CNTs incorporation into the parent material (PFCS). The cause of this agglomeration is a less-developed CNT network within the material due to a relatively low CNT concentration, which further limits electrochemical activities. Additionally, even with low CNT content, there is an improvement in conductivity, enhancing electron and ion transport, which is essential for electrochemical performance. In contrast, the FCS-II sample exhibits a dense, uniform CNT network anchored over the pure PFCS matrix, as seen in Fig. 4(c). The interconnected dense morphology and retained porosity of micro-particles can facilitate efficient electron transfer, leading to improved electrical conductivity and mechanical strength. However, the dense CNT coverage over the PFCS matrix reduces the number of active sites available for ion interaction and intercalation.

On the other hand, the FCS-III composite displays the most favorable morphological features among all samples, as portrayed in Fig. 4(d). The FESEM image unveiled a homogeneous, well-dispersed, web-like CNT network embedded within the PFCS micro-particles. This also confirms very little agglomeration along with an increased porosity level in the micro-particles, compared to all other samples. Additionally, the porous web-like structure is well-defined, indicating an electrochemically advantageous morphology that promotes rapid ion exchange, lower  $R_{ct}$  values, and efficient diffusion dynamics. All these outstanding morphological features suggest that FCS-III is the most enhanced electrode material for electrochemical applications and energy storage devices.

Elemental analysis was performed using EDX to verify the presence of constituent elements at the microscopic level and their weight percentages in the as-prepared PFCS and FCS/CNTs composites. The EDX spectra for all samples are shown in Fig. 4(e), with yellow, blue, pink, and magenta colors for PFCS, FCS-I, FCS-II, and FCS-III, respectively. Distinct peaks corresponding to Fe, Co, and S, along with carbon (C), were clearly observed, with no impurity peaks detected, confirming the exact

composition of FCS. When CNTs were added, a prominent peak appeared in the EDX spectra of the PFCS/CNTs composites, and the C peak intensity increased with higher CNT content. Notably, the Fe, Co, and S peaks remained consistent across all samples, indicating successful synthesis of the PFCS and PFCS/CNTs composites. In this context, Table 1 presents the precise composition of all the prepared samples.

To quantify the porosity features estimated in PFCS and FCS-III using the Brunauer–Emmett–Teller (BET) technique by allowing the adsorption/desorption of nitrogen gas at 77 K. This experiment of PFCS and FCS-III resulted in two pairs of nitrogen adsorption and desorption isotherms, as depicted in Fig. 5, reflecting the type-IV isotherm, signifying the presence of meso and micro pores in these two materials.<sup>34</sup> The behaviour showed an increase when 9% CNTs were included, indicating the presence of additional diffusion channels. For instance, a pristine sample exhibited a maximum pore volume of  $0.97 \text{ cm}^3 \text{ g}^{-1}$  and a BJH surface area of  $29.27 \text{ m}^2 \text{ g}^{-1}$ , while FCS-III provided the highest SSA of  $68.62 \text{ m}^2 \text{ g}^{-1}$ . In this way, the FCS-III appeared to be the best among all other electrode materials as an efficient electrode material to be used for high charge storage devices.

### 3.3. Electrochemical analysis

The CV provides crucial electrochemical investigations that help to elucidate how a fabricated electrode behaves when the system is subjected to a constant potential window. It provides

Table 1 Elemental composition of PFCS, FCS-I, FCS-II, and FCS-III

Sample	wt (%) Fe	wt (%) Co	wt (%) S	wt (%) C
PFCS	18.50	39.0	42.50	0
FCS-I	17.95	37.83	41.33	2.90
FCS-II	17.39	36.66	40.95	4.90
FCS-III	16.94	35.69	38.68	8.54



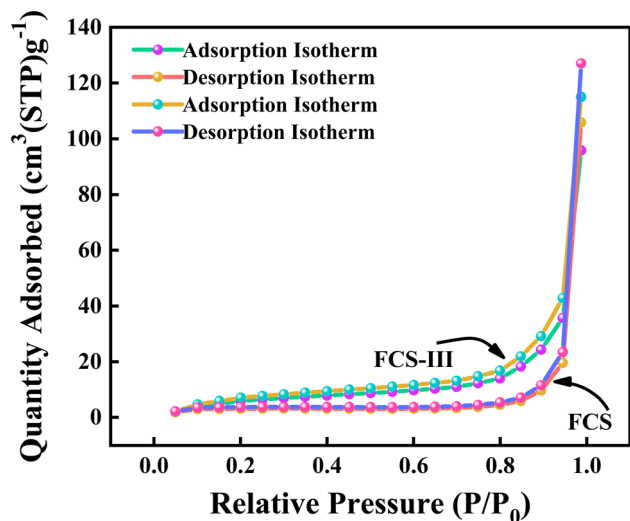
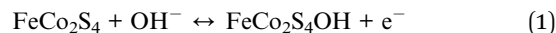


Fig. 5 Nitrogen adsorption/desorption isotherms of PFCS and FCS-III.

a detailed study of redox mechanisms, rate capability, and capacitive properties, all performed in potentiostat mode.<sup>31–38</sup> Consequently, Fig. 6(a–d) displays cyclic voltammograms (CVs) of PFCS, FCS-I, FCS-II, and FCS-III, conducted within an optimized range of 0 V to 0.43 V constant potential at scan rates (SRs) of 5, 7.5, 10, and 15  $\text{mV s}^{-1}$ . In Fig. 6(a–d), the minimum activation potentials to initiate the redox reactions for PFCS, FCS-I, FCS-II, and FCS-III are observed at (0–28) V, (0–27) V, (0–25) V, and (0–24) V, respectively. Additionally, the obtained CVs, which maintain consistent shapes across all samples in Fig. 6(a–d) redox peaks without significant distortion of the electrode materials. Notably, the stable CVs and narrow peak potential separation ( $\Delta E_p$ ) even at high scan rates, suggest high reversibility, durability, and a long cycle life for the synthesized samples. The main reason for these results appears to be smooth contact at the electrode–electrolyte interface, indicating

efficient ion migration into the porous channels of the electrode. Furthermore, in Fig. 6(a–d), the CVs exhibit faradaic processes, confirming the  $\text{Co}^{2+}$  to  $\text{Co}^{3+}$  conversions, as shown in chemical reactions eqn (1) and (2).



However, a minor shift in oxidation peaks (0.37–0.43 V) and reduction peaks (0.17–0.21 V) across SR (5–15  $\text{mV s}^{-1}$ ) was observed for all samples. This peak shift toward higher and lower potentials with increasing SR suggests highly reversible kinetics of PFCS-based electrode materials. It can also be explained that rapid charge transport occurs at higher scanning speeds compared to lower speeds. Additionally, the gradual incorporation of CNTs into PFCS increased the current, as shown on the y-axis of Fig. 6(a–d). These efficient electrochemical results are attributed to the synergistic effect of the strong interaction between CNTs and the PFCS active material.

Besides that, Fig. 6(e) shows a composite graph at the SR of 5  $\text{mV s}^{-1}$ , providing a qualitative interpretation and comprehensive analysis of the electrochemical response for PFCS-based electrode materials. In Fig. 6(e), the obtained CVs at this SR display a duck-like profile along with a capacitive region (0–0.28 V) and non-capacitive features (oxidation peaks after 0.28 V and reduction peaks before 0.28 V), confirming battery-type behaviour. Additionally, Fig. 6(e) demonstrates that FCS-II and FCS-III exhibit more prominent electrochemical responses compared to PFCS and FCS-I, due to the higher concentration of CNTs. It is worth noting that the CNTs' 3D scaffold significantly facilitates charge transportation by providing large exposed active sites, and at this lowest SR ions have more time to intercalate into the material's channels. These interpretations support the overall capacitive and diffusive behaviour. Based on these explanations, the specific

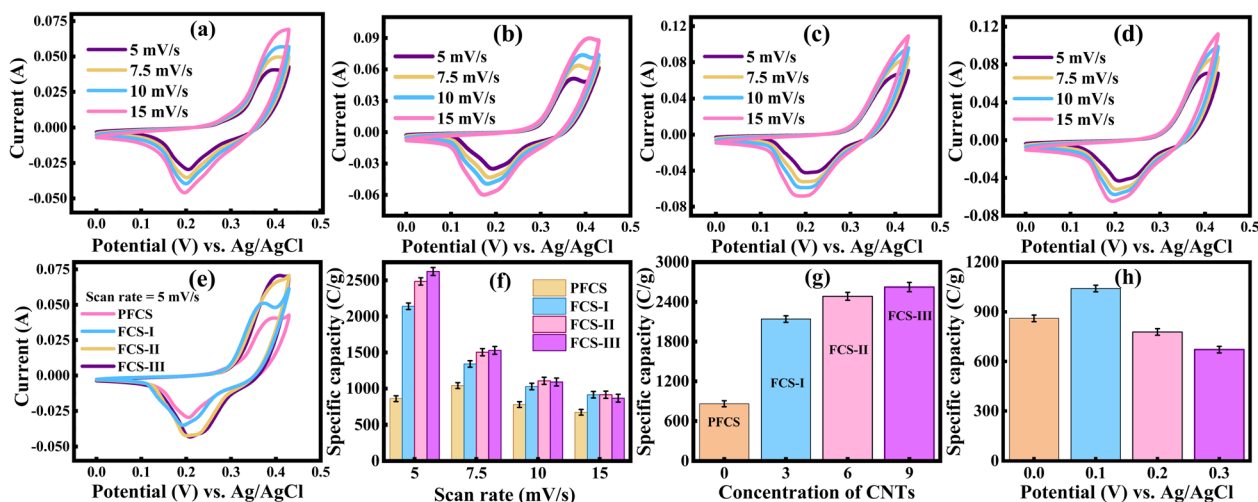


Fig. 6 (a–d) CV curves of PFCS, FCS-I, FCS-II, and FCS-III, (e) combined plot at 5  $\text{mV s}^{-1}$ , (f) scan rate vs. specific capacity, (g) CNTs concentration versus specific capacity, and (h) potential versus specific capacity.



Table 2 Specific capacities of PFCS, FCS-I, FCS-II, and FCS-III at different scan rates

Scan rate (mV s <sup>-1</sup> )	Specific capacities (C g <sup>-1</sup> )			
	PFCS	FCS-I	FCS-II	FCS-III
5	860.55	2141.15	2485.33	2624.16
7.5	1040.99	1341.67	1504.07	1529.19
10	778.22	1028.95	1106.95	1091.03
15	671.13	914.26	913.77	866.75

capacity ( $Q_s$ ) was calculated using eqn (3) for all prepared samples. The rationale behind the computation of  $Q_s$  is the matching of the ideally reported battery-type SC profile, which is what the several reports have presented.<sup>31,36,38</sup>

$$Q_s = \frac{\int_{V_i}^{V_f} IdV}{mv} \quad (3)$$

Here,  $Q_s$  refers to specific capacity in C g<sup>-1</sup>, and the integral term in this expression denotes the area under the CVs, while  $m$  and  $v$  are associated with active mass and SR, respectively.

The  $Q_s$  values of PFCS, FCS-I, FCS-II, and FCS-III are listed in Table 2 at various SRs (5–15 mV s<sup>-1</sup>). It is clear that a remarkable  $Q_s$  of 2624 C g<sup>-1</sup> was calculated for the FCS-III electrode material, surpassing previously reported PFCS-based composites. This also highlights the effective integration of CNTs into the ternary TMS-based material. However, a gradual decrease in  $Q_s$  values is observed with increasing SR, indicating sluggish ion migration into the electrode channels due to limited ion diffusion time at higher SR. Conversely, higher  $Q_s$  values at low SR are due to most active sites being occupied by ions, thanks to the longer diffusion time. Additionally, the influence of CNT concentration on  $Q_s$  values is evident, as illustrated in Fig. 6(f). Consequently, the FCS-III electrode material, which has maximum CNT contents, achieved an ultra-high  $Q_s$  among the electrode materials, as can be seen in Fig. 6(g). Also, a gradual

increment in CNT content causes the systematic reduction in the  $\Delta E_p$ , as shown in bar graph Fig. 6(h), plotted  $\Delta E_p$  versus concentration of CNTs at the lowest SR ( $\sim 5$  mV s<sup>-1</sup>). This progressive reduction in  $\Delta E_p$  values indicate faster electrode kinetics, more reversibility, and charge transfer efficiency of FCS-based electrode materials.

To better understand the charge storage behaviour of the synthesized PFCS-based electrode materials, Dunn's method has been used. This theoretical approach helps to clarify how charge carriers are stored in PFCS, FCS-I, FCS-II, and FCS-III. More importantly, the quantitative separation of storage processes, such as surface-controlled and diffusion-controlled mechanisms, has been estimated, which accounts for the total storage capacity. For this purpose, Dunn and his co-workers applied power's law, which is expressed in eqn (4).

$$i_{\text{peak}} = av^b \text{ or } \log(i_{\text{peak}}) = b \log(v) + \log(a) \quad (4)$$

Herein,  $i_{\text{peak}}$  clarifies the oxidation and reduction peak currents from CVs. Specifically,  $a$  and  $b$  are considered fitting parameters that depend on the SR, and they are associated with the slope and intercept obtained from the linear fitting of SR versus peak current plots. From this, the average value of  $b$  can be determined, and when it equals 0.5, it indicates completely diffusion-controlled behavior. This reflects a traditionally typical battery-type phenomenon, meaning ions are diffusing into the tunnels of the electrode material. On the other hand, a  $b$ -value of 1 represents surface-controlled phenomena. This condition includes both capacitive and pseudocapacitive (surface redox-activity) processes, suggesting double-layer formation and rapid surface-redox reactions occurring at or near the electrode's surface. More importantly if  $b$ -value is close to 0.5, it indicates the dominance of battery-type behavior. Conversely, if  $b$  is near 1, surface-controlled behavior is more prevalent. So, the combination of capacitive and diffusive behaviors, which contribute to the overall storage capacity, therefore, these conditions collectively indicate battery-type behavior of the

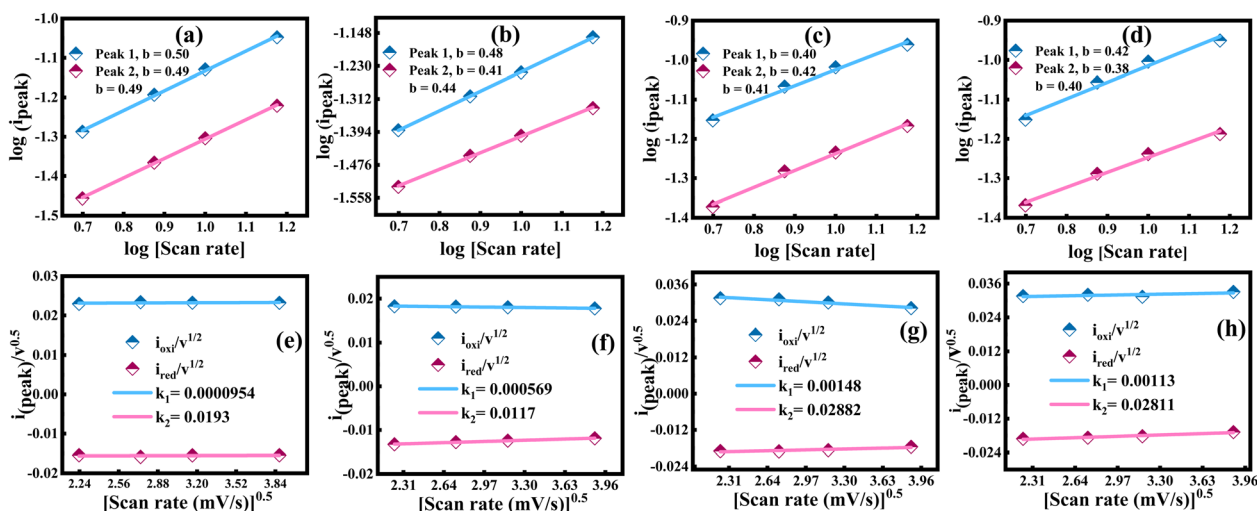


Fig. 7 (a–d) Linearly fitted graphs for all samples and (e–h) contribution parameters ( $k_1$ ,  $k_2$ ) for all samples.



electrode material. Therefore, Fig. 7(a–d) shows the graphs of  $b$ -values calculated for PFCS, FCS-I, FCS-II, and FCS-III, which are 0.49, 0.44, 0.41, and 0.40, respectively, confirming battery-type behavior. These values indicate the coexistence of capacitive and diffusive processes and clarify the presence of redox-active sites due to sulfur vacancies and additional functional groups in the surface chemistry of as-fabricated electrodes, which are associated with pseudocapacitive behavior and partial chemically inert surface-active sites belonging to non-pseudocapacitive behavior (EDLC). These contributions showed some alterations when functionalized CNTs were decorated on the surface chemistry of PFCS. That's how the battery-type behaviors in all fabricated electrodes were observed and reported after careful comparison with different reports from the literature.<sup>34–37</sup>

Furthermore, in the context of quantifying surface-controlled and diffusion-controlled contributions individually at various SR for all prepared PFCS-based electrode materials, the Dunn method was employed. This method has been quantified into eqn (5) and (6).

$$i_{\text{peak}} = k_1 v + k_2 v^{1/2} \quad (5)$$

This equation refers the current from surface-controlled ( $k_1 v$ ) and diffusion-controlled ( $k_2 v^{1/2}$ ) process, and is quantified for linear fitting,

$$\frac{i_{\text{peak}}}{v^{1/2}} = k_1 v^{1/2} + k_2 \quad (6)$$

The graph  $v^{1/2}$  vs.  $i_{\text{peak}}/v^{1/2}$  were plotted for each PFCS-based electrode materials, as depicted in Fig. 7(e–h).

By the fitting of these plots, the obtained slope and intercepts yield the values of  $k_1$  and  $k_2$  constants, and were then used to compute relative contributions at various SR. Fig. 8(a–d) demonstrates the deconvoluted plots of surface-controlled and diffusion-controlled phenomenon of PFCS, FCS-I, FCS-II, and FCS-III at various SR (5–15 mV s<sup>-1</sup>). It can be observed in contribution ratios' graphs that PFCS is exhibiting dominantly

diffusion-controlled phenomenon, which is consistent with its  $b$ -value (0.49). A transition from slow diffusion-controlled to more ideal battery-type phenomenon can be clearly observable in Fig. 8(a–d) for 3 (FCS-I), 6 (FCS-II), and 9% CNTs (FCS-III). The rationale behind this transition is the shortening of diffusion distances and conductive scaffold provided by the incorporated CNTs content into PFCS, allowing the faster kinetics. Additionally, a sharp rise in surface-controlled phenomenon can be noticed with the elevation in SR for all prepared samples. The decrease in diffusion-controlled phenomenon is likely due to insufficient time availability of ions to diffuse into the PFCS-based electrode materials at elevated SR. Such theoretical predictions support the battery-type behavior of FCS-III and confirm their suitability for next-generation HCs technology. The contribution of these behaviors (capacitive and diffusive) directly originating from the CV curves at lowest SR are displayed in Fig. 8(e–h), representing the PFCS, FCS-I, FCS-II, and FCS-III, respectively.<sup>34,38</sup>

To evaluate a comprehensive view of hybrid performance for PFCS-based electrode materials, GCD analysis was conducted over various current densities of 10, 13, 16, and 20 A g<sup>-1</sup> within an optimized potential range of 0–0.45 V. The obtained curves depicted in Fig. 9(a–d) confirmed a battery-type behavior for all PFCS-based composites, which aligns with the CV analysis. The GCD curves also maintained symmetrical shapes even at elevated current density (~20 A g<sup>-1</sup>), suggesting significant stability, cyclability, and kinetic robustness of these electrodes. This smooth charge storage phenomenon validates their suitability for SC applications. Furthermore, the fabricated electrodes experienced a reduction in charging and discharging times along with increased potential drops as the current density is elevated from 10 to 20 A g<sup>-1</sup>, as can be noticed in Fig. 9(a–d). The charging and discharging times of the electrodes are influenced by the varying content of CNTs. With the addition of different percentages of CNTs into PFCS, optimized electrochemical performances were achieved synergistically, as illustrated in Fig. 9(a–d). This phenomenon indicates that the incorporated CNTs have led to increased discharge cycles due to

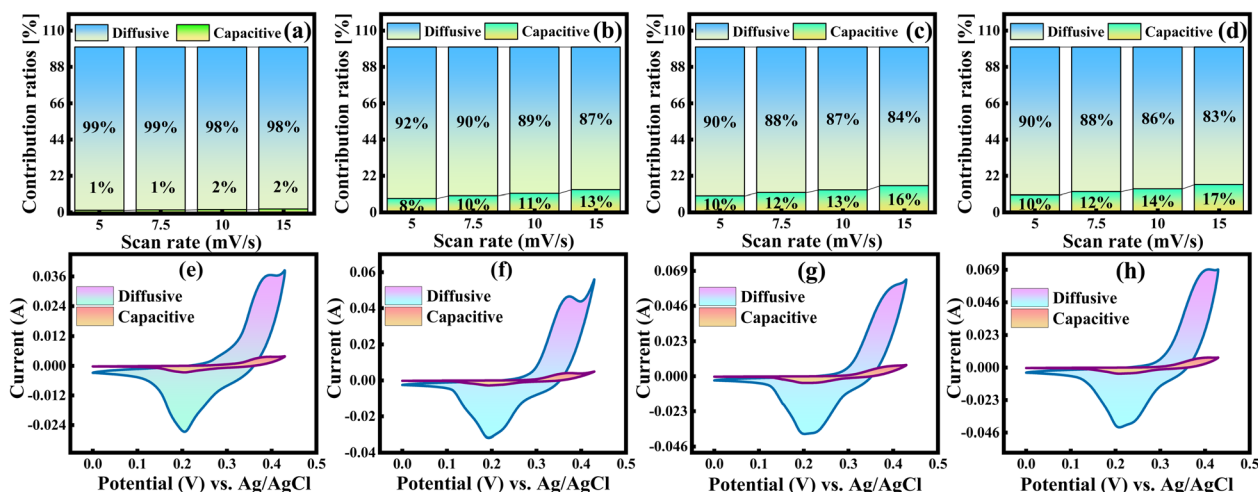


Fig. 8 (a–d) Contribution graphs for all samples and (e–h) capacitive and diffusive contributions in CV curves at 5 mV s<sup>-1</sup> for all samples.



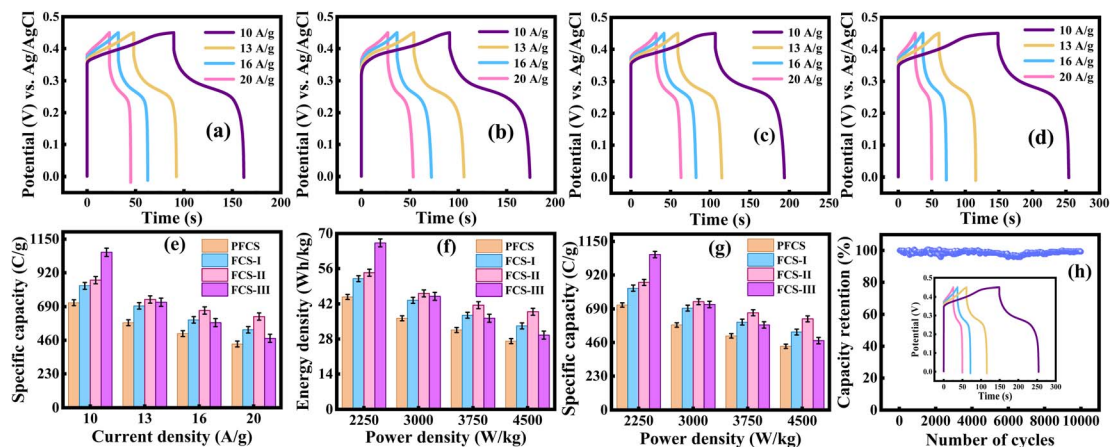


Fig. 9 GCD profiles (a) PFCS, (b) FCS-I, (c) FCS-II, (d) FCS-III, (e) current density vs. specific capacity, (f) Ragone plot, (g) power density vs. specific capacity, and (h) stability test.

enhanced ionic mobility and a reduction in potential drop ( $iR$  drop). With the incorporation of CNTs content, the  $iR$  drop at the lowest  $I_m$  ( $\sim 10 \text{ A g}^{-1}$ ). The  $iR$  drop is responsible for the voltage loss during electrochemical reaction due to the internal resistance of any electrochemical system. Thus, the lowest  $iR$  drop for FCS-III (9% CNTs) suggests an effective strategy for mitigating the internal resistances of PFCS-based electrode materials. Also, at low current densities, the faradaic process is more effectively facilitated thanks to the maximum available time for electrolyte species to intercalate into the exposed active sites of PFCS-based electrode materials. Thus, the  $Q_s$  was computed using eqn (7).

$$Q_s = I_m \times \Delta t \quad (7)$$

where  $I_m$  represents the current density ( $\text{A g}^{-1}$ ) while  $\Delta t$  expresses discharging time for electrode materials. The  $Q_s$  of 716, 831, 869, and  $1059 \text{ C g}^{-1}$  were acquired at  $10 \text{ A g}^{-1}$ , including PFCS, FCS-I, FCS-II, and FCS-III electrode materials.

In the case of FCS-based electrode materials, the FCS-III electrode exhibited superior  $Q_s$  due to its advantageous web-like morphology. Additionally, Fig. 9(e) illustrates a graph showing the relationship between  $Q_s$  and  $I_m$  for all prepared samples. This graph indicates a gradual decrease in  $Q_s$  as  $I_m$  increases. It also highlights the effects of CNTs' concentration and  $I_m$  on the charge-storage capabilities of the fabricated electrode materials. Notably, the PFCS shown in Fig. 9(e) achieved the maximum  $Q_s$  of  $716 \text{ C g}^{-1}$  at  $I_m$  equal to  $10 \text{ A g}^{-1}$ , which substantially decreased to  $386 \text{ C g}^{-1}$  at  $20 \text{ A g}^{-1}$ . Similarly, a parallel trend was observed for the sample with 3% CNTs (FCS-I), where the storage capacity of about  $831 \text{ C g}^{-1}$  at  $10 \text{ A g}^{-1}$  dropped to approximately  $513 \text{ C g}^{-1}$  at  $20 \text{ A g}^{-1}$ . Furthermore, adding 6% and 9% CNTs into PFCS increased this  $Q_s$  to 869 and  $1059 \text{ C g}^{-1}$  at  $10 \text{ A g}^{-1}$  for FCS-II and FCS-III, respectively, but it decreased significantly at higher  $I_m$ . This reduction in capacity is due to less time available for ions to migrate into the electrode's pores and active sites, as shown clearly in the FESEM images in Fig. 4(a–d). Furthermore, the  $Q_s$  values for all samples

at all current densities have been reported in different conversion units, aiming to provide a comprehensive quantitative overview in Table 3. The rationales behind these significant improvements are a highly porous nickel foam substrate and a stable contact between the electrode/electrolyte interface. At low current densities, these values are within the expected range, reflecting efficient ion diffusion due to the proper response of electrolyte ions to the applied electrical signal. These achievements reflect our optimized electrochemical testing, in which the active mass loading was ensured across multiple experiments under the same and different conditions. Whereas the ED and PD for all PFCS-based samples are listed in the Table 4 and were calculated using eqn (8) and (9).

$$\text{ED} = \frac{\Delta V \times Q_s}{2 \times 3.6} \quad (8)$$

$$\text{PD} = \frac{\text{ED} \times 3600}{\Delta t} \quad (9)$$

These are standard equations used to estimate precise performance metrics like ED and PD of as-synthesized electrodes. Compared to other prepared samples, the FCS-III achieved the maximum ED of  $66.22 \text{ Wh kg}^{-1}$  along with a notable PD of  $2250 \text{ W kg}^{-1}$  at  $10 \text{ A g}^{-1}$ . These impressive metrics are summarized in Table 4 alongside reported literature. Furthermore, these performance metrics are plotted against various  $I_m$  (Ragone plot), which further highlights the behavior of all samples, observable in Fig. 9(f). In this context, the Ragone plot shows that an increase in ED often results in a decrease in PD, or *vice versa*, because fewer ions are available for delivery. Additionally, Fig. 9(g) illustrates the trend of PD with  $Q_s$ , showing how varying the concentration of CNTs affects the ED values of all samples. Alongside these advantageous charge-storage traits, the stability of FCS-III was evaluated by establishing an asymmetric setup in which FCS-III served as the cathode and activated carbon as the anode, with 10 000 GCD cycles, yielding 98.76% charge storage retention, as depicted in



Table 3 Conversions of specific capacities of PFCS, FCS-I, FCS-II, and FCS-III into different units

Sample	Mass loading (mg cm <sup>-2</sup> )	Current density (A g <sup>-1</sup> )	Specific capacitance (F g <sup>-1</sup> )	Specific capacity (C g <sup>-1</sup> )	Specific capacity (mAh g <sup>-1</sup> )	Areal capacity (C cm <sup>-2</sup> )
PFCS	1.5	10	1592.56	716.65	199.07	1.074
	1.5	13.34	1288.94	580.02	161.11	0.870
	1.5	16.67	1122.89	505.30	140.36	0.757
	1.5	20	964.43	433.99	120.55	0.650
FCS-I	1.5	10	1846.78	831.05	230.84	1.246
	1.5	13.34	1544.30	694.93	193.03	1.042
	1.5	16.67	1331.88	599.35	166.48	0.899
	1.5	20	1181.03	531.46	147.62	0.797
FCS-II	1.5	10	1931.14	869.01	241.39	1.303
	1.5	13.34	1642.26	739.01	205.28	1.108
	1.5	16.67	1474.59	663.56	184.32	0.995
	1.5	20	1382.17	621.97	172.77	0.932
FCS-III	1.5	10	2354.71	1059.62	294.33	1.589
	1.5	13.34	1600.54	720.24	200.06	1.080
	1.5	16.67	1289.87	580.44	161.23	0.870
	1.5	20	1050.56	472.75	131.32	0.709

Table 4 Specific capacity, energy density, and power density of PFCS, FCS-I, FCS-II, and FCS-III at multiple current densities

Sample	Current density (A g <sup>-1</sup> )	Specific capacitance (F g <sup>-1</sup> )	Specific capacity (C g <sup>-1</sup> )	Energy density (Wh kg <sup>-1</sup> )	Power density (W kg <sup>-1</sup> )
PFCS	10	1592.56	716.65	44.79	2250
	13.34	1288.94	580.02	36.25	3000
	16.67	1122.89	505.30	31.58	3750
	20	964.43	433.99	27.12	4500
FCS-I	10	1846.78	831.05	51.94	2250
	13.34	1544.30	694.93	43.43	3000
	16.67	1331.88	599.35	37.45	3750
	20	1181.03	531.46	33.21	4500
FCS-II	10	1931.14	869.01	54.31	2250
	13.34	1642.26	739.01	46.18	3000
	16.67	1474.59	663.56	41.47	3750
	20	1382.17	621.97	38.87	4500
FCS-III	10	2354.71	1059.62	66.22	2250
	13.34	1600.54	720.24	45.01	3000
	16.67	1289.87	580.44	36.27	3750
	20	1050.56	472.75	29.54	4500

Table 5 Comparison of performance parameters of different electrode materials

Sample	Specific capacitance (F g <sup>-1</sup> )	Energy density (Wh kg <sup>-1</sup> )	Power density (W kg <sup>-1</sup> )	Cyclic stability (%)	References
FeCo <sub>2</sub> S <sub>4</sub> @MXene	2415.3	68	800	90.50% after 5k cycles	19
FeCo <sub>2</sub> S <sub>4</sub> /MWCNTs	432	49.40	20k	93.9% after 5k cycles	26
FeCo <sub>2</sub> S <sub>4</sub> @Ni@graphene	390 mAh g <sup>-1</sup>	65.8	754.8	89% after 6k cycles	27
FeCo <sub>2</sub> S <sub>4</sub> /NF	4035	37.7	603	80.40% after 5k cycles	32
FeCo <sub>2</sub> S <sub>4</sub> /rGO/Ag/NF	1840	59	817	94% after 10k cycles	33
FeCo <sub>2</sub> S <sub>4</sub> /CNTs	1059.62 C g <sup>-1</sup>	66.22	2250	98.76% after 10k cycles	This work

Fig. 9(h). The supporting literature has been reported in Table 5.<sup>19,26,27,32,33</sup>

The EIS analysis tests were conducted within an optimized frequency range from 10<sup>-2</sup> to 10<sup>4</sup> Hz to gain a more comprehensive understanding of electrochemical responses such as ionic mobility, diffusion dynamics, and ion transport in all

samples. In this context, circuit elements such as solution resistance ( $R_s$ ),  $R_{ct}$ , and Warburg impedance ( $W$ ) are fundamental parameters. These parameters help us to examine the influence of varying CNT concentration more deeply. In this regard, the Nyquist plot is displayed in Fig. 10(a), where the real and imaginary impedances are represented on the  $x$  and  $y$ -axes,



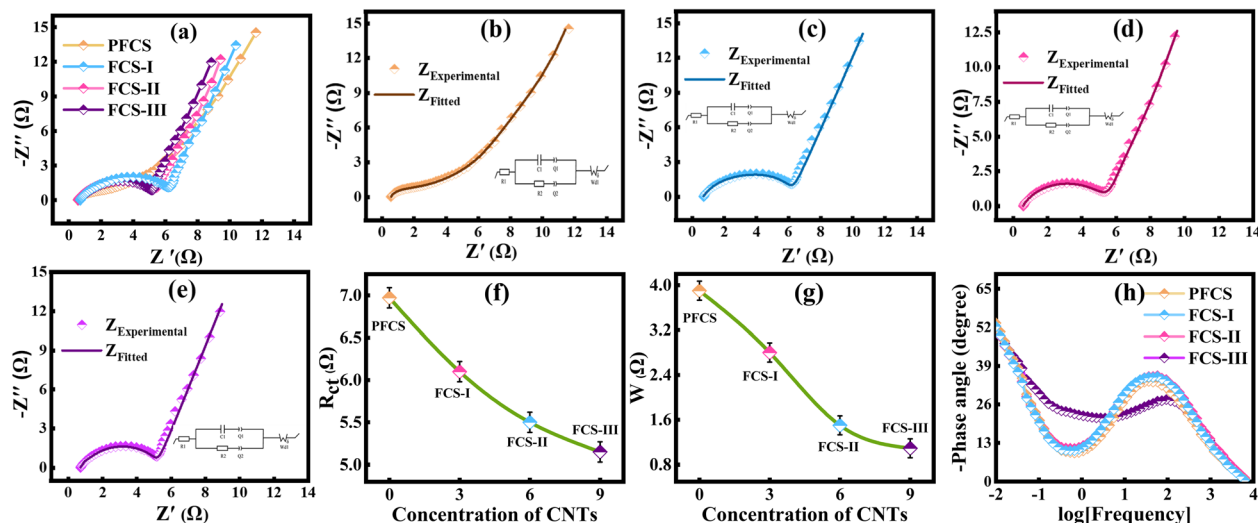


Fig. 10 (a) Combined EIS spectra of all samples, (b–e) fitting spectra of PFCS, FCS-I, FCS-II, and FCS-III, (f) concentration of CNTs vs. charge transfer resistance, (g) concentration of CNTs vs. Warburg resistance, and (h) Bode plot.

respectively. This Nyquist plot shows the EIS spectra of PFCS, FCS-I, FCS-II, and FCS-III. In these spectra, dynamic changes in capacitive and resistive parameters can be observed with varying CNT concentrations. To better interpret this behavior, the Nyquist plot is divided into high, intermediate, and low-frequency regions. These regions demonstrate the circuit elements mentioned earlier, such as  $R_s$ ,  $R_{ct}$ , and  $W$ , which are useful for optimizing the electrochemical response of electrode materials for SC technology.

Within this framework, the Biologic EC Lab V11.60 software, using the well-suited Randle circuit, was employed to evaluate the exact values of the circuit elements for all PFCS-based electrodes, as displayed in Fig. 10(b–e). For all samples, the fitted and experimental data are separated by two distinctive legends, indicating a well-matched equivalent circuit with real measurements. Consequently, all the PFCS-based composites with CNTs (PFCS, FCS-I, FCS-II, and FCS-III) exhibit  $R_s$  (0.59, 0.53, 0.60, and 0.55  $\Omega$ ),  $R_{ct}$  (6.97, 6.10, 5.50, and 5.15  $\Omega$ ), and  $W$  (3.9, 2.8, 1.50, and 1.09  $\Omega$ ), as listed in the Table 6. Nonetheless, the balanced  $R_s$  values in the high-frequency region suggest optimal ionic conductivity ( $\sigma$ ) for all samples. More importantly, the  $R_{ct}$  in the intermediate-frequency region helps quantify the resistance barrier during electron transfer and reveals how easily or difficult it is for a redox reaction to occur at interface of

the electrode and electrolyte. The  $R_{ct}$  can also be calculated by subtracting  $R_s$  from the width of the semicircle on a Nyquist plot, shown in Fig. 10(a). As a result, the  $R_{ct}$  values and the width of the semicircle gradually decrease with the incorporation of CNT content, as can be seen in Fig. 10(f). This low  $R_{ct}$  values signifies the importance of CNT addition, further indicating faster electron transfer which is critical for enhancing the electrochemical response of electrode materials.

Moreover, the line growing vertically in the low-frequency region, just after the semicircle, is associated with  $W$  and diffusion dynamics, as shown in Fig. 10(a). The significant reduction in  $W$  values from 3.9 to 1.09  $\Omega$  with the gradual addition of CNTs, as shown in Fig. 10(g), indicates excellent diffusion of ionic species through the electrode–electrolyte interface. Additionally, it can be inferred that ionic species rapidly fill the vacancies created by quick electron transfer due to low  $R_{ct}$ , leading to improved ion transport and diffusion dynamics. Notably, the  $W$  value decreased significantly with the highest CNTs' content in PFCS and shifted toward the y-axis, as clearly be seen in Fig. 10(a). This shift confirms the transition toward capacitive-dominated behavior of FCS-III by enhancing its diffusion-limited characteristic. These low  $R_{ct}$  and  $W$  values, as listed in Table 6, highlight the efficient electrochemical response of FCS-III, making it a superior electrode material for advanced SCs.

The electrochemical kinetics and storage mechanism dynamics of PFCS, FCS-I, FCS-II, and FCS-III were analyzed using Bode analysis, as shown in Fig. 10(h). This plot illustrates the frequency-dependent characteristics of all samples against phase angle ( $\theta$ ), showing how the impedance of the SC shifts between ideal capacitive ( $\theta = -90^\circ$ ) and pure resistive ( $\theta = 0^\circ$ ) behaviors at very low and high frequencies, respectively. When the resistive and capacitive impedances are considered to be equally contribution at  $\theta = -45^\circ$ , known as the knee frequency ( $f$ ), it is an important metric for evaluating the relaxation time constant ( $\tau$ ). This  $\tau$  indicates the minimum timescale required

Table 6 Values of elements for the corresponding fit circuit.  $R_1 = R_s$ ,  $R_2 = R_{ct}$ ,  $C_1 =$  capacitance,  $Q_1$ ,  $Q_2 =$  constant phase elements, and  $W_1 =$  Warburg impedance

Sample	$R_1$ ( $\Omega$ )	$R_2$ ( $\Omega$ )	$C_1$ (mF)	$Q_1$ ( $F s^{(a-1)}$ )	$Q_2$ ( $F s^{(a-1)}$ )	$W_1$ ( $\Omega$ )
PFCS	0.63	6.99	0.032	0.217	0.0023	3.9
FCS-I	0.53	6.16	0.011	0.0082	0.619	2.8
FCS-II	0.60	5.13	0.015	0.011	0.716	2.05
FCS-III	0.55	4.41	0.056	0.035	0.077	1.39



for an SC device to discharge all stored energy efficiently at constant power. Crucially, lower  $\tau$  values suggest better rate performance of the SC device. Therefore,  $\tau$  is calculated as the inverse of for all samples, using eqn (10).

$$\tau = \frac{1}{f} \quad (10)$$

Herein,  $\tau$  for PFCS, FCS-I, FCS-II, and FCS-III were computed to be 27, 17, 16, and 10 ms, respectively. Such a systematic decrease in  $\tau$  values is attributed to the inclusion of CNTs, which manifests excellent rate capability in the FCS-III electrode material for advanced SC technology.

The  $\sigma$  of the electrolyte immediately estimates the electrochemical efficiency of electrode materials for SCs based on their ion-conduction capability. For comparison, this fundamental property is crucial for assessing the ease with which charge carriers flow during charging and discharging within the electrolyte. To evaluate this, the  $R_s$  of all prepared samples are measured using EIS with the help of EC Lab software, an important factor in calculating  $\sigma$  ( $\text{S cm}^{-1}$ ). Eqn (11) has been used to determine the  $\sigma$  values of each electrode material.<sup>30–37</sup>

$$\sigma = \frac{L}{A \times R_i} \quad (11)$$

In this equation,  $L$  and  $A$  relate to the thickness (0.09 cm) and cross-sectional area ( $1.0 \text{ cm}^2$ ) of the electrode material being dipped into the electrolyte. The symbol  $R_i$  signifies the solution resistance to charge carriers at the electrode surface and the reference electrode in an electrolyte (KOH). The ionic conductivities for PFCS, FCS-I, FCS-II, and FCS-III were calculated to be 0.152, 0.169, 0.150, and 0.163  $\text{S cm}^{-1}$ , respectively. These consistent values indicate stable  $\sigma$  across all samples, even with the addition of CNTs, suggesting no disruption to ionic pathways and indicating gradual improvements in ionic conduction. It can be concluded that incorporating CNTs enhances electronic and ionic conductivity while maintaining stable  $\sigma$  values. Therefore, FCS-based electrode materials exhibit excellent electrochemical efficiency, confirming their suitability for SC applications.

The cation transference number ( $t_+$ ) is another important parameter for evaluating the fraction of the total ionic current carried by cations ( $\text{K}^+$ ,  $\text{OH}^-$ ) in a 1 M KOH electrolyte. Specifically, this parameter indicates which ion migrates more efficiently. It is important to note that an equal distribution of ionic current is not possible due to factors such as the size of solvated ions, electrostatic polarization interactions, and temperature, which all influence an ionic species' migration efficiency relative to others. In this context,  $t_+$  values for PFCS, FCS-I, FCS-II, and FCS-III electrode materials have been estimated using the following eqn (12), proposed by Sorenson & Jacobsen.<sup>30,34</sup>

$$t_+ = \frac{1}{1 + Z_d(0)/R_b} \quad (12)$$

Here,  $Z_d(0)$  demonstrates the Warburg impedance's real part at approximately 0 Hz, and  $R_b$  represents solution resistance. Our findings show that  $t_+$  values increased significantly from 0.13,

0.15, 0.22, and 0.28 for PFCS, FCS-I, FCS-II, and FCS-III, indicating a strong shift toward leading ion migration. Additionally, the very small  $t_+$  value of PFCS highlights a diffusion-limited mechanism for  $\text{K}^+$  ions due to its bulk form, resulting in anion ( $\text{OH}^-$ ) dominated kinetics. A gradual increase in  $t_+$  values is clearly observable, which is attributed to the addition of CNTs into the parent material. The incorporation of CNTs enhances cation mobility and promotes a balanced contribution of both ions ( $\text{K}^+$ ,  $\text{OH}^-$ ) in the charge storage process by reducing the kinetic limitations of the parent material, thanks to the conductive scaffold provided by CNTs. It is important to note that this ionic participation significantly helps in reducing the polarization at higher SR. Furthermore, the increased cation mobility substantially improves storage efficiency, thereby enhancing the intercalation of  $\text{K}^+$  ions into the FCS-III electrode during faradaic reactions.

The rate constant indicates how quickly a reaction occurs and provides an estimate of electron transfer between the electrode and electrolyte ions during a redox reaction. It is a kinetic parameter closely related to charge-transfer resistance. A high rate constant indicates a fast redox reaction, resulting in greater charge storage, higher power, and better performance. The rate constant is calculated using eqn (13).<sup>30,36</sup>

$$\text{Rate constant} = \frac{RT}{F^2 \times R_{ct} \times C} \quad (13)$$

Here,  $R$  and  $T$  in the numerator represent the gas constant and room temperature, while parameters in the denominator, such as  $F$ ,  $R_{ct}$ , and  $C$ , are related to the Faraday constant, charge transfer resistance calculated from EIS analysis, and electrolyte concentration, respectively. Within this context, the values of the rate constant for each fabricated electrode are  $3.80 \times 10^{-8}$ ,  $4.32 \times 10^{-8}$ ,  $5.18 \times 10^{-8}$ , and  $6.03 \times 10^{-8} \text{ cm s}^{-1}$ , respectively.

Exchange current density is a crucial parameter in electrochemistry, indicating how readily charge-transfer reactions occur at the electrode–electrolyte interface at equilibrium (when no current flows). It represents the rate at which electrons are exchanged between the electrode and ions in the electrolyte at the equilibrium potential. A high exchange current density signifies rapid reaction kinetics and a lower overpotential to drive current. This can be evaluated using eqn (14).<sup>29,30,36</sup>

$$J_0 = \frac{RT}{n \times F \times R_{ct}} \quad (14)$$

The quantitatively estimated values are 1.83, 4.16, 5.01, and 5.82  $\text{mA g}^{-1}$ , respectively. This indicates the highest exchange current density for FMO-III ( $5.82 \text{ mA g}^{-1}$ ), providing additional evidence that it truly exhibited excellent ion transport characteristics compared to all other materials in the as-fabricated electrode series.

Discussing cation mobility in electrochemistry is vital for understanding how ions move within an electrochemical cell, which directly impacts the system's performance. This property reveals how easily positive ions, or cations, can move through an electrolyte against an applied electrical signal to maintain



neutrality, thereby suppressing polarization effects. For example, high cation mobility allows ions to move quickly and store charge, resulting in greater energy storage capacity in a cell. This characteristic varies among different electrolytes and systems, with common electrolytes like KOH and NaOH chosen for their low cost, minimal side effects, and anti-corrosive properties. A key factor affecting the system's efficiency is the size of the solvated ionic radii, typically defined as the ratio of charge to volume for a cation. Therefore, cations with smaller hydrated radii are preferred because they have lower solvent shell energy, enabling them to diffuse more easily within the electrolyte. In this context, cation mobility in KOH is described by eqn (15).<sup>36</sup>

$$u_+ = \frac{t_+ \times \sigma}{n \times z^2 \times e} \quad (15)$$

In the above equation,  $t_+$  and  $\sigma$  are the transference number of the cation and ionic conductivity, respectively. Meanwhile,  $n$ ,  $z^2$ , and  $e$  are parameters known as number density, charge number, and elementary charge. The quantitative examination of cation mobility for PFCS, FCS-I, FCS-II, and FCS-III yields values approximately  $2.03 \times 10^{-10}$ ,  $2.65 \times 10^{-10}$ ,  $2.81 \times 10^{-10}$ , and  $3.81 \times 10^{-10} \text{ m}^2 \text{ V}^{-1} \text{ s}^{-1}$ , respectively, expressing the highest cation mobility for FCS-III.

Extending the earlier-discussed electrochemical investigations, an in-depth study of the FCS-III//AC device has been systematically conducted using CV, GCD, and EIS characterizations with 1 M KOH electrolyte. A charge storage setup is illustrated in Fig. 11, in support of its application perspective. Particularly, in CV analysis, as depicted in Fig. 12(a), the absence of significant distortions in the obtained symmetrical

CVs, along with redox humps at SR ranging from 50 to 500  $\text{mV s}^{-1}$ , suggests excellent stability and a hybrid (PC and EDLC) nature of this assembled device. Also, remarkable reversibility for FCS-III//AC is observed across variable potential windows (0–1.2 V). This reversibility is reflected in a gradual increase in CV area while maintaining symmetry, as clearly seen in Fig. 12(b). The rationale behind these stable electrochemical features is attributed to smooth contact at the electrode/electrolyte interface and efficient electrode kinetics, thereby promoting the effectiveness of the FCS-III//AC device.<sup>36,38</sup>

GCD tests were carried out to precisely estimate the performance metrics at various current densities, ranging from 1.5 to 9  $\text{A g}^{-1}$ , within the same potential window, consistent with CV analysis. The obtained nonlinear and consistent GCD curves confirm good rate capability and indicate dominant faradaic contributions from the FCS-III positive electrode, as illustrated in Fig. 12(c). Additionally, this hybrid device delivers the longest discharge time at the minimum current density of 1.5  $\text{A g}^{-1}$ , signifying the impact of the electrode matrix that utilizes redox-active sites effectively. However, at elevated current densities, the discharge period shrinks systematically, mainly due to limited ion intercalation and increased polarization from Helmholtz layer formation at the electrode surface at higher rates. Notably, the positive electrode (FCS-III) promotes swift reversible redox activity, and the negative electrode (AC) facilitates fast charge delivery even at higher current densities.<sup>38</sup> This synergistic configuration also minimizes internal resistances by reducing the  $iR$  drop, as portrayed in Fig. 12(c), further promoting efficient charge transport in electrode channels. Overall, these traits validate this FCS-III//AC configuration for optimizing pseudocapacitive-type storage and capacitive rate

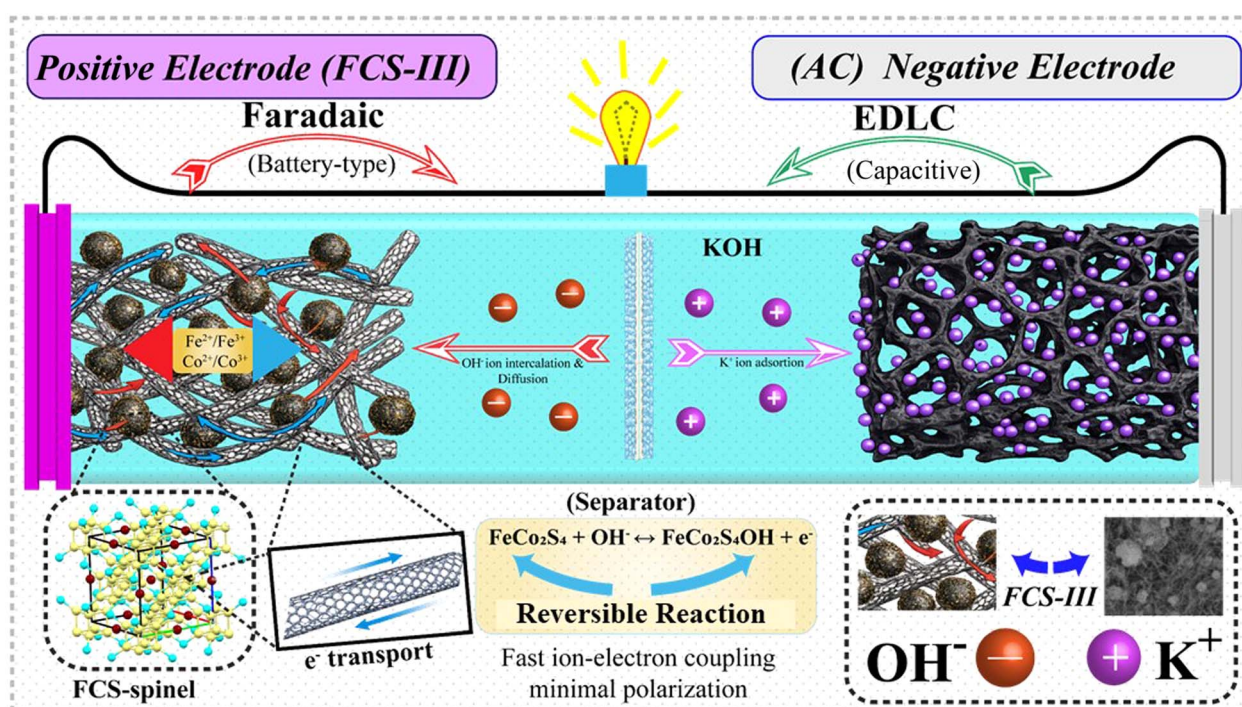


Fig. 11 Pictorial representation of charge storage mechanism.



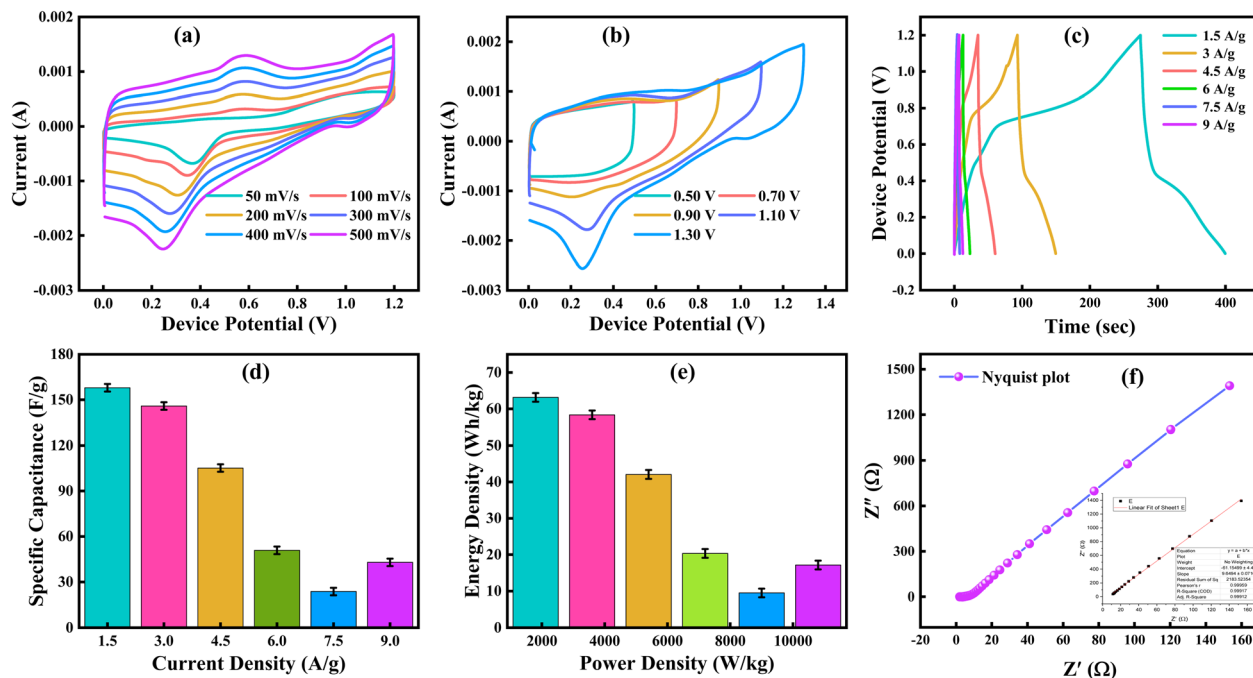


Fig. 12 (a and b) CV curves of FCS-III//AC at 1.2 V and at different potential windows, (c) GCD profiles at multiple current densities, (d) current density vs. specific capacitance, (e) Ragone plot, and (f) Nyquist plot.

performance, showing its suitability for SC applications.<sup>36,38,39</sup> The quantification of this charge storage type has been done with the help of the stated eqn (16)–(18).<sup>38</sup>

$$C_{sp} = \frac{I \times \Delta t}{m \times \Delta V} \quad (16)$$

$$ED = \frac{\Delta V^2 \times C_{sp}}{3.6} \quad (17)$$

$$PD = \frac{ED \times 3600}{\Delta t} \quad (18)$$

Additionally, the trend of  $C_{sp}$  as a function of current density is shown in Fig. 12(d), indicating a gradual decrease in charge storage with increasing current density. This fact is associated with the inefficient response of the applied electrical signal towards the electrolyte ions, which limits their diffusion time. Therefore, at 1.5 A g<sup>-1</sup>, the constructed device facilitated the highest capacitance of 157.88 F g<sup>-1</sup> and 42.90 F g<sup>-1</sup> at 9 A g<sup>-1</sup>. A

similar trend has been observed in the Ragone plot, corresponding to the PD *versus* ED trend, as supplemented in Fig. 12(e). At this instance, the maximum ED and PD values were 63.15 Wh kg<sup>-1</sup> and 10 800 W kg<sup>-1</sup>, respectively. The rest of the values are provided in Table 7.

To evaluate comprehensive insights into the electrochemical response of the FCS-III//AC device, including charge transport and diffusion dynamics, EIS is employed across a wide range of frequencies. The EIS spectra, as depicted in Fig. 12(f), are categorized into three effective regions; (i) the high-frequency region describes  $R_s$ , (ii) the intermediate region demonstrates  $R_{ct}$ , and (iii) the third region represents  $W_d$ . More importantly, these elements exhibit the interfacial characteristics of the electrode in a given solution.  $R_s$ ,  $R_{ct}$ , and  $W_d$  are simulated using EC Lab software to estimate them accurately, where the line represents simulated data and the solid spheres indicate experimental impedances. From the simulation, extremely small impedance values, such as  $R_s$  (1.96 Ω),  $R_{ct}$  (1.39 Ω), and  $W_d$

Table 7 Performance parameters of FCS-III//AC based asymmetric device

Current density (A g <sup>-1</sup> )	Discharge time (s)	Potential window (V)	Specific capacitance (F g <sup>-1</sup> )	Energy density (Wh kg <sup>-1</sup> )	Power density (Wh kg <sup>-1</sup> )
1.5	126.31	1.2	157.88	63.15	1800
3.0	58.36	1.2	145.90	58.36	3600
4.5	28.04	1.2	105.15	42.06	5400
6.0	10.17	1.2	50.85	20.34	7200
7.5	3.79	1.2	23.88	9.47	9000
9.0	5.72	1.2	42.90	17.16	10 800



(9.64  $\Omega$ ), were obtained, suggesting swift electrode kinetics in FCS//AC.

## 4. Conclusion

In summary, we synthesized  $\text{FeCo}_2\text{S}_4$  and its composites with different CNTs compositions (3%, 6%, and 9%) using hydrothermal and solvothermal methods. Various analysis techniques, including XRD, EDX, and SEM, were used to confirm that all samples had a crystalline structure with a simple cubic phase. The successful incorporation of CNTs into the PFCS structure was validated by EDX analysis, while morphological analysis revealed well-defined grains with a non-uniform distribution. To evaluate the EC, a three-electrode system was employed. Among the fabricated electrodes, the FCS-III composite showed the best performance, delivering a specific capacity of  $1059.62 \text{ C g}^{-1}$ , an energy density of  $66.22 \text{ Wh kg}^{-1}$ , and a power density of  $2250 \text{ W kg}^{-1}$  at  $10 \text{ A g}^{-1}$ . Additionally, the electrode demonstrated excellent cycling durability, retaining 98.76% of its capacity after 10 000 cycles and maintaining a stable coulombic efficiency. EIS results indicated that the prepared material exhibited good electrical performance, with low charge transfer resistance ( $4.41 \Omega$ ), improved ionic conductivity ( $0.13 \text{ S cm}^{-1}$ ), and a short relaxation time ( $0.010 \text{ s}$ ). The incorporation of 9% CNTs into FCS enhanced its potential as an excellent electrode material for advanced supercapacitor applications.

## Conflicts of interest

The authors declare that there are no financial or any other types of conflicts of interests to declare for this submission.

## Data availability

Data will be made available on request.

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