


 Cite this: *RSC Adv.*, 2026, 16, 8289

# Computational study of the kinetics and mechanism of radical polymerization of acrylic acid and derivatives in organic solvents

 Mai Van Bay,<sup>a</sup> Pham Thi Thuy Linh,<sup>a</sup> Truong Le Bich Tram,<sup>b</sup> Nguyen Thi Hoa,<sup>c</sup> Adam Mechler <sup>d</sup> and Quan V. Vo <sup>\*c</sup>

Free-radical polymerization of acrylic acid derivatives (AADs), such as acrylic acid (AA), methyl acrylate (MA), acrylamide (AM), methacrylic acid (MAA), and methyl methacrylate (MMA), proceeds through radical addition of monomers during initiation and propagation. Despite the extensive experimental literature on this process from both a radical chemistry and an industrial point of view, there is little information on the mechanistic pathways of the radical addition process, particularly in organic solvents. In this work, quantum chemical methods were applied to explore the solvent and initiator effects on AAD polymerization. The reactivity of di-*tert*-butyl peroxide (TBO<sup>•</sup>) and dicumyl peroxide (CMO<sup>•</sup>) and 2-cyanoprop-2-yl radical (Al<sup>•</sup>) as initiators was systematically studied in isopropanol (IP) and toluene (TL). Computational results predict that initiation is consistently faster in IP than in TL, with initiator efficiency ranked as TBO<sup>•</sup> > Al<sup>•</sup> > CMO<sup>•</sup>. At 298 K, the predictions for propagation constants in IP ( $2.80 \times 10^1$  to  $2.60 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ) are substantially higher compared to those in TL ( $2.60\text{--}1.50 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ). Additionally, solvent-derived radicals were predicted to participate actively in propagation. Temperature was found to significantly increase  $\log(k_p)$  in both toluene and isopropanol, consistent with the Arrhenius kinetic model. The computed propagation rate constants for MA polymerization in toluene ( $1.00 \times 10^3$  to  $1.10 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  at 320 K) and the activation energies of MA and MMA (3.6 and 3.4 kcal mol<sup>-1</sup>, respectively) align well with experimental results, validating the accuracy and reliability of the computational approach. The effect is more pronounced in toluene due to the absence of hydrogen-bonding interactions, underscoring the key role of the solvent in controlling propagation kinetics. This study predicts that solvent polarity and the properties of the radical strongly govern the kinetics of AAD polymerization, thereby providing useful mechanistic insights for optimizing radical polymerization in non-aqueous media.

 Received 20th December 2025  
 Accepted 4th February 2026

DOI: 10.1039/d5ra09849a

[rsc.li/rsc-advances](https://rsc.li/rsc-advances)

## 1. Introduction

In the free-radical polymerization of acrylic acid derivatives (AADs; Fig. 1), such as AA, MA, AM, MAA and MMA, the initiation and propagation steps occur *via* radical addition to the monomeric double bonds. Polymerization is routinely carried out in aqueous media<sup>1–9</sup> or in organic solvents like isopropanol (IP) and toluene (TL), using organic peroxides such as dicumyl peroxide (CMO)<sub>2</sub> and di-*tert*-butyl peroxide (TBO)<sub>2</sub>, or azo initiators like 2,2'-azobis(2-methylpropionitrile) (AIBN) as

radical sources (Fig. 1).<sup>10–20</sup> Recent studies used purpose-designed modeling and simulation frameworks, introduced as a “digital-twin” approach, to investigate free-radical polymerization processes.<sup>21–23</sup> These works reverted to unrestricted Hartree–Fock formalism with a semi-empirical quantum chemistry framework to allow the simulation of the polymerization process as a system of multiple possibilities, delivering qualitative but not quantitative insights into spin-related effects in the polymerization and copolymerization of vinyl monomers with stable radicals. Functionalization of polyolefins with AA and its derivatives using peroxide initiators—particularly dicumyl peroxide and di-*tert*-butyl peroxide (TBO)—has proven to be an effective approach for controlling polymer properties, enhancing grafting efficiency, as well as thermomechanical and surface characteristics.<sup>12,13,16–20</sup> AIBN has been used in several works as an initiator for the radical polymerization of AA and its derivatives.<sup>11,14,15,24</sup> However, mechanistic and kinetic investigations on the polymerization of AADs initiated by activators such as (CMO)<sub>2</sub>, (TBO)<sub>2</sub>, and AIBN remain unavailable.

<sup>a</sup>The University of Danang – University of Sciences and Education, Danang 550000, Vietnam

<sup>b</sup>Department of Science and International Cooperation, The University of Danang, Danang 550000, Vietnam

<sup>c</sup>The University of Danang – University of Technology and Education, Danang 550000, Vietnam. E-mail: [vvquan@ute.udn.vn](mailto:vvquan@ute.udn.vn)
<sup>d</sup>Department of Biochemistry and Chemistry, La Trobe University, Victoria 3086, Australia

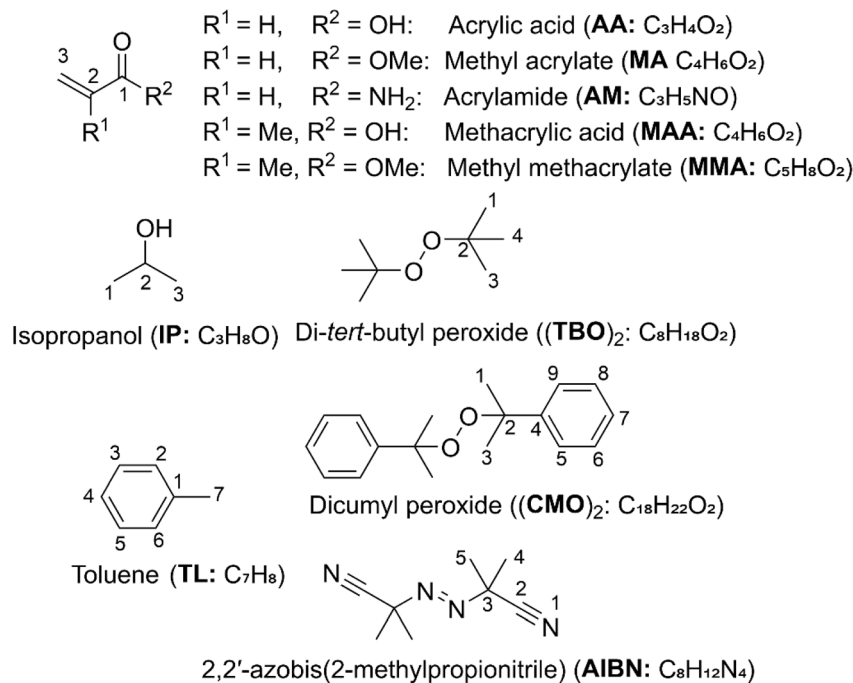



Fig. 1 Structure, molecular formulas, and numbering of AAD, (TBO)<sub>2</sub>, (CMO)<sub>2</sub>, AIBN, IP and TL.

Therefore, a comprehensive study is essential to elucidate their polymerization mechanisms and reaction kinetics.

The experimental rate constant of **MA** in toluene was reported as  $k_p(\mathbf{MA}) = 1.47 \times 10^4$  and  $2.82 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  at 293 and 323 K, respectively,<sup>25,26</sup> and by others as  $1.03 \times 10^4$  to  $3.31 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  in the temperature range of 285–354 K.<sup>27</sup> The radical polymerization of **MA** was found to follow the Arrhenius kinetic model, with activation energies ( $E_a$ ) of 4.1 (ref. 28) and 4.4 kcal mol<sup>-1</sup>,<sup>27</sup> whereas that of **MMA** in toluene ranged from 2.8 to 5.3 kcal mol<sup>-1</sup> within 303–333 K.<sup>24</sup> Several studies have also found that the radical polymerization of **AA** in **TL** and **IP** obeys the Arrhenius kinetic model,<sup>11,14,15</sup> however, comprehensive investigations on the kinetics of **AADs** have not yet been reported.

Although numerous studies have examined polymerization processes in selected solvent media,<sup>3,10–15,21,24,29</sup> none of these delved into a comprehensive investigation of the initiation mechanism and propagation kinetics. Moreover, the reports of the solvent effects on the polymerization reactions are also inconsistent. Haehnel *et al.*<sup>25</sup> observed that the propagation rate ( $k_p$ ) was largely unaffected by organic solvents such as butyl acetate and toluene, even under conditions comparable to bulk polymerization with the increasing number of C atoms in their ester side chain. Yet a range of other studies reported solvent-dependent behavior.<sup>28,30–33</sup> Nonetheless, a consistent kinetic trend has been established, indicating that  $k_p$  systematically increases with the elongation of the ester side chain under all examined conditions.<sup>28,30,31</sup> Several studies indicated that solvents may actively participate in the initiation step, thereby contributing to the characteristics of the resulting polymers.<sup>3,34,35</sup> The temperature dependence of polymerization in

various solvents has also been recognized as a crucial factor.<sup>24</sup> Yet, these aspects have not been addressed comprehensively for the polymerization reactions of **AADs**.

Building on our previous investigations into the radical polymerization of **AADs** in aqueous media,<sup>36</sup> the present work employs a quantum chemistry-based approach<sup>37–39</sup> to explore the polymerization behavior of acrylic acid derivatives initiated by alkoxy radicals (**TBO**· and **CMO**·) and the azo radical (2-cyanoprop-2-yl, **AI**·) in isopropanol (**IP**) and toluene (**TL**) solvents.

## 2. Computational details

The kinetic evaluation was carried out using the quantum mechanics-based test for the overall free radical scavenging activity (QM-ORSA) protocol.<sup>37</sup> This protocol combines density functional theory calculations of reaction energetics with transition state theory to estimate kinetic parameters in solution, and it is broadly applicable to all radical processes due to their mechanistic similarity.<sup>40,41</sup> Rate constants ( $k$ ) were determined *via* transition state theory (TST) at 298.15 K and 1 M standard state (eqn (1)).<sup>42–46</sup>

$$k = \sigma \kappa \frac{k_B T}{h} e^{-(\Delta G^\ddagger)/RT} \quad (1)$$

Here,  $\sigma$  is the reaction symmetry factor,<sup>47,48</sup>  $\kappa$  is the tunneling correction from the Eckart barrier<sup>49</sup> calculated using the Eyringpy code,<sup>45,46</sup>  $k_B$  and  $h$  are Boltzmann and Planck constants, and  $\Delta G^\ddagger$  is the Gibbs free energy of activation.

Reactions approaching the diffusion limit were corrected according to the Collins–Kimball treatment,<sup>50</sup> yielding apparent rate constants ( $k_{app}$ ) as shown in eqn (2).<sup>40,51</sup> Recent studies have



validated this model for diffusion-controlled reactions in various solvents.<sup>36,37,39–41,52–56</sup>

$$k_{\text{app}} = \frac{k_{\text{TST}}k_{\text{D}}}{k_{\text{TST}} + k_{\text{D}}} \quad (2)$$

$$k_{\text{D}} = 4\pi R_{\text{AB}}D_{\text{AB}}N_{\text{A}} \quad (3)$$

Diffusion coefficients ( $D_{\text{AB}} = D_{\text{A}} + D_{\text{B}}$ ) were obtained by the Stokes–Einstein equation (eqn (4)), using solvent viscosities of  $20.4 \times 10^{-4}$  Pa s (isopropanol) and  $5.60 \times 10^{-4}$  Pa s (toluene).<sup>50,57–59</sup>

$$D_{\text{A or B}} = \frac{k_{\text{B}}T}{6\pi\eta a_{\text{A or B}}} \quad (4)$$

Transition states were verified by single imaginary frequencies and confirmed by IRC calculations. All computations were performed at the M06-2X/6-311++G(d,p) level of theory, which provides reliable thermodynamic and kinetic predictions.<sup>36,39,52,60–63</sup> The solvent effects were modeled using SMD.<sup>64</sup> This approach is considered dependable for radical reaction studies, as the calculated-to-experimental rate constant ratios remain within 0.2–2.9.<sup>38–40,45,65</sup>

Rate constants at different temperatures (293–353 K for IP and 280–380 K for TL) were calculated using eqn (1), in which the Gibbs free energy of activation,  $\Delta G^{\ddagger}(T)$ , was evaluated according to eqn (5).

$$\Delta G^{\ddagger}(T) = \Delta H^{\ddagger}(T) - T\Delta S^{\ddagger}(T) \quad (5)$$

Here,  $\Delta H^{\ddagger}$  and  $\Delta S^{\ddagger}$  denote the enthalpy and entropy of activation ( $\text{kcal mol}^{-1}$ ), respectively, obtained in the solvent phase for IP and TL using the SMD solvation model at 298.15 K assumed to be temperature independent within the examined temperature range. The kinetic parameters were calculated with the Eyringpy program.<sup>45,46</sup> While approximate, this approach is widely used in both experimental and theoretical kinetic studies.<sup>66–69</sup> The calculations were performed with Gaussian 16.<sup>70</sup>

## 3. Results and discussion

### 3.1. Initiation reactions of TBO•/CMO• in the organic solvents

To explore the initiation stage of polymerization triggered by organic peroxides, including di-*tert*-butyl peroxide ((TBO)<sub>2</sub>), dicumyl peroxide ((CMO)<sub>2</sub>), and 2,2'-azobis(2-methylpropionitrile) (AIBN), in organic solvents such as IP or TL, the possible radical pathways were considered as described in reactions (6)–(10) (Fig. 2). Alkoxy radicals are produced *via* thermal decomposition of peroxides (reaction (6)), while decomposition of AIBN generates the 2-cyanoprop-2-yl radical (AI•) through reaction (7). Our previous findings demonstrated that TBO• and CMO• preferentially undergo formal hydrogen transfer (FHT) with IP and TL, yielding the solvent-derived radicals IP–C2• and TL–C7•, respectively.<sup>54</sup> In contrast, reactions of AI• with these solvents are thermodynamically

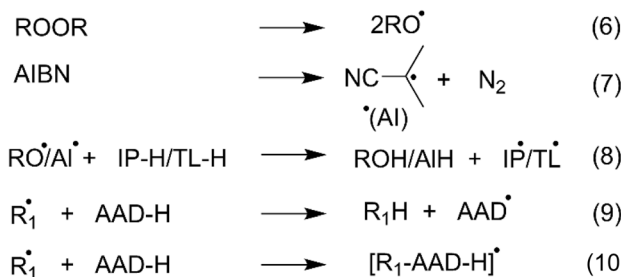


Fig. 2 The initiation reaction of the TBO•/CMO•/AI• in isopropanol (IP) and toluene (TL) (R : TB, CM; R<sub>1</sub>• : TBO•, CMO•, AI•, IP•, TL•).

unfavorable due to positive Gibbs free energies (Table S1, SI). Consequently, in IP and TL media, initiation involves interactions between CMO•, TBO•, and AI• (from the initiators) as well as solvent-derived IP–C2• and TL–C7• radicals, reacting with AADs through radical adduct formation (RAF) predominantly at the C2 and C3 positions. The kinetics of the AADs + IP–C2•/TL–C7•/TBO•/CMO•/AI• reactions were subsequently evaluated, and the results are summarized in Table 1 and Fig. 3.

The modelling of initiation reactions in the TL solvent predicted pronounced differences among the monomers (AADs) and radical species (TL–C7•/TBO•/CMO•/AI•). For AA, the overall reactivity with the solvent-derived radical (TL–C7•) was predicted to be dominant ( $k_{\text{app}} = 5.40 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ), occurring almost exclusively at the C3 position (99.9%). In contrast, the primary initiator radicals CMO•, TBO•, and AI• were far less efficient, with  $k_{\text{app}}$  values of only 1.84, 73.6, and  $19.0 \text{ M}^{-1} \text{ s}^{-1}$ , respectively. A similar trend was observed for MA and AM, where the reactions preferentially occurred at the C3 site. The highest  $k_{\text{app}}$  values were again associated with the solvent radical ( $2.40 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$  for MA and  $1.80 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$  for AM), while TBO• and CMO• displayed only moderate reactivity. Notably, the AI• radical was predicted to show only modest reactivity toward MA ( $17.0 \text{ M}^{-1} \text{ s}^{-1}$ ) and AM ( $7.50 \text{ M}^{-1} \text{ s}^{-1}$ ), highlighting significant kinetic limitations compared with the TL–C7• radical. For MAA and MMA, the differences were even more pronounced. The TL–C7• and TBO• predicted to have the highest reactivities ( $8.20 \times 10^2$  and  $4.00 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ , respectively), greatly surpassing those of CMO• (0.95 and  $14.0 \text{ M}^{-1} \text{ s}^{-1}$ ) and AI• (1.3 and  $1.5 \text{ M}^{-1} \text{ s}^{-1}$ ), respectively.

Comparison across monomers in the TL solvent for each radical suggests that initiation reactions were specific to each AAD. For instance, the TL–C7• radical is predicted to react most rapidly with MAA ( $k_{\text{app}} = 8.20 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ), followed by AA ( $5.40 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ), MMA ( $4.00 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ), MA ( $2.40 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ), and AM ( $1.80 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ). By contrast, the TBO• radical is predicted to show highest reactivity with MMA ( $3.70 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ), followed by AA ( $7.36 \times 10^1 \text{ M}^{-1} \text{ s}^{-1}$ ), AM ( $6.80 \times 10^1 \text{ M}^{-1} \text{ s}^{-1}$ ), MA ( $5.60 \times 10^1 \text{ M}^{-1} \text{ s}^{-1}$ ), and MAA ( $4.70 \times 10^1 \text{ M}^{-1} \text{ s}^{-1}$ ). Both CMO• and AI• were consistently less effective, with rate constants in the range of  $0.73\text{--}1.90 \times 10^1 \text{ M}^{-1} \text{ s}^{-1}$ .

In the IP solvent IP–C2• is predicted to have the highest reaction rates for all monomers, ranging from  $10^4$  to  $10^7 \text{ M}^{-1} \text{ s}^{-1}$ , far exceeding the other radicals. It was noted that the calculated  $k_{\text{app}}$  values were the highest for MAA and AA with  $k_{\text{app}}$



**Table 1** Calculated  $\Delta G^\ddagger$  (kcal mol<sup>-1</sup>), tunneling corrections ( $\kappa$ ), rate constants ( $k_{\text{app}}$  and  $k_{\text{overall}}$  M<sup>-1</sup> s<sup>-1</sup>) and branching ratios ( $\Gamma$ , %) for the AAD + IP-C2'/TL-C7'/TBO'/CMO'/AI' reactions in the organic solvents

Comp.	Radicals	Positions	TL				IP			
			$\Delta G^\ddagger$	$\kappa$	$k_{\text{app}}$	$\Gamma$	$\Delta G^\ddagger$	$\kappa$	$k_{\text{app}}$	$\Gamma^a$
AA	TL-C7'/IP-C2'	C2	18.3	1.5	$3.80 \times 10^{-1}$	0.1	11.7	1.2	$1.90 \times 10^4$	0.0
		C3	13.9	1.3	$5.40 \times 10^2$	99.9	6.6	1.0	$7.83 \times 10^7$	100.0
		$k_{\text{overall}}$			<b><math>5.40 \times 10^2</math></b>				<b><math>7.84 \times 10^7</math></b>	
	CMO'	C2	19.6	1.5	$3.7 \times 10^{-2}$	2.0	18.0	1.4	$5.30 \times 10^{-1}$	3.0
		C3	17.3	1.4	1.80	98.0	16.0	1.4	$1.70 \times 10^1$	97.0
		$k_{\text{overall}}$			<b>1.84</b>				<b><math>1.75 \times 10^1</math></b>	
	TBO'	C2	18.0	1.5	$6.20 \times 10^{-1}$	0.8	16.9	1.5	3.50	4.3
		C3	15.1	1.5	$7.30 \times 10^1$	99.2	15.1	1.5	$7.70 \times 10^1$	95.7
		$k_{\text{overall}}$			<b><math>7.36 \times 10^1</math></b>				<b><math>8.05 \times 10^1</math></b>	
	AI'	C2	21.7	1.5	$1.20 \times 10^{-3}$	0.0	20.5	1.5	$8.10 \times 10^{-3}$	0.0
		C3	15.9	1.3	$1.90 \times 10^1$	100.0	15.1	1.3	$7.10 \times 10^1$	88.2
		$k_{\text{overall}}$			<b><math>1.90 \times 10^1</math></b>				<b><math>7.10 \times 10^1</math></b>	
MA	TL-C7'/IP-C2'	C2					11.5	1.1	$2.40 \times 10^4$	29.6
		C3	14.4	1.3	$2.40 \times 10^2$	100.0	11.0	1.0	$5.70 \times 10^4$	70.4
		$k_{\text{overall}}$			<b><math>2.40 \times 10^2</math></b>				<b><math>8.10 \times 10^4</math></b>	
	CMO'	C3	17.4	1.4	1.70	100.0	15.7	1.4	$2.60 \times 10^1$	100.0
		TBO'	15.3	1.5	$5.60 \times 10^1$	100.0	14.8	1.5	$1.40 \times 10^2$	100.0
		AI'	15.9	1.4	$1.70 \times 10^1$	100.0	15.3	1.3	$5.30 \times 10^1$	100.0
AM	TL-C7'/IP-C2'	C2					12.5	1.2	$5.10 \times 10^3$	26.8
		C3	14.5	1.3	$1.80 \times 10^2$	100.0	12.2	1.0	$7.90 \times 10^3$	41.5
		$k_{\text{overall}}$			<b><math>1.80 \times 10^2</math></b>				<b><math>1.30 \times 10^4</math></b>	
	CMO'	C3	17.9	1.5	$7.30 \times 10^{-1}$	100.0	16.0	1.4	$1.80 \times 10^1$	100.0
		TBO'	15.2	1.5	$6.80 \times 10^1$	100.0	15.2	1.5	$7.10 \times 10^1$	100.0
		AI'	16.4	1.4	7.50	100.0	15.8	1.4	$2.30 \times 10^1$	100.0
MAA	TL-C7'/IP-C2'	C2					13.5	1.2	$9.90 \times 10^2$	0.0
		C3	13.6	1.3	$8.20 \times 10^2$	100.0	6.5	1.0	$9.17 \times 10^7$	100.0
		$k_{\text{overall}}$			<b><math>8.20 \times 10^2</math></b>				<b><math>9.17 \times 10^7</math></b>	
	CMO'	C3	17.7	1.5	$9.50 \times 10^{-1}$	100.0	15.8	1.4	$2.30 \times 10^1$	100.0
		TBO'	14.0	1.4	$4.70 \times 10^2$	100.0	13.5	1.4	$1.10 \times 10^3$	100.0
		AI'	17.5	1.4	1.30	100.0	14.3	1.3	$2.60 \times 10^2$	100.0
MMA	TL-C7'/IP-C2'	C2					13.4	1.2	$1.10 \times 10^3$	0.0
		C3	14.1	1.3	$4.00 \times 10^2$	100.0	7.9	1.0	$9.52 \times 10^6$	100.0
		$k_{\text{overall}}$			<b><math>4.00 \times 10^2</math></b>				<b><math>9.52 \times 10^6</math></b>	
	CMO'	C3	16.1	1.4	$1.40 \times 10^1$	100.0	15.5	1.3	$3.40 \times 10^1$	100.0
		TBO'	14.1	1.4	$3.70 \times 10^2$	100.0	13.8	1.4	$7.20 \times 10^2$	100.0
		AI'	17.4	1.4	1.50	100.0	14.9	1.3	$9.90 \times 10^1$	100.0

$$^a \Gamma = k_{\text{app}} \times 100/k_{\text{overall}}$$

=  $7.84 \times 10^7$  and  $9.17 \times 10^7$  M<sup>-1</sup> s<sup>-1</sup>, respectively, further confirming that the initiation reactions in the IP medium are strongly dominated by the solvent radical (IP-C2'). Among the primary initiators, TBO' showed the highest activity (up to  $1.10 \times 10^3$  M<sup>-1</sup> s<sup>-1</sup> for MAA and  $7.20 \times 10^2$  M<sup>-1</sup> s<sup>-1</sup> for MMA), with the AADs compared with the CMO' and AI' radicals. By contrast, the CMO' and AI' were less effective initiators, with  $k_{\text{app}}$  values generally limited to the range of  $10^1$ – $10^2$  M<sup>-1</sup> s<sup>-1</sup>. These findings predict that the solvent radical (IP-C2') plays a decisive role in the initiation mechanism of acrylic monomers, while substituents such as -NH<sub>2</sub>, -COOH, and -CH<sub>3</sub> exert significant influence on the reaction kinetics. Among the studied compounds, MAA was predicted to exhibit the highest reactivity in the IP solvent.

The initiation reactions proceed more rapidly in IP than in TL for all investigated AADs and radicals (IP-C2', TL-C7', TBO', CMO', and AI'). Solvent-derived radicals (IP-C2' and TL-C7') are predicted to have higher reactivity toward AADs compared

with the primary initiators (TBO', CMO', and AI'). These results suggest that the solvents, *i.e.*, IP and TL, have a strong influence on the polymerization of the AADs initiated by alkoxy radicals, such as TBO' and CMO'. Consequently, the resulting polymers are likely to incorporate structural fragments derived from the solvent molecules (IP or TL). Among the investigated initiators, the relative efficiency follows the order TBO' > AI' > CMO' in both solvents, whereas the initiation reactions of the monomers exhibit solvent- and initiator-dependent variations.

### 3.2. The propagation reaction

Our previous work predicted that the rate constants of the propagation reactions of AADs in aqueous media exhibit only negligible variation beyond the second propagation step.<sup>36</sup> Therefore, in the present study, the propagation of AADs was modeled as a two-step reaction, with the corresponding results summarized in Table 2 and illustrated in Fig. 4.



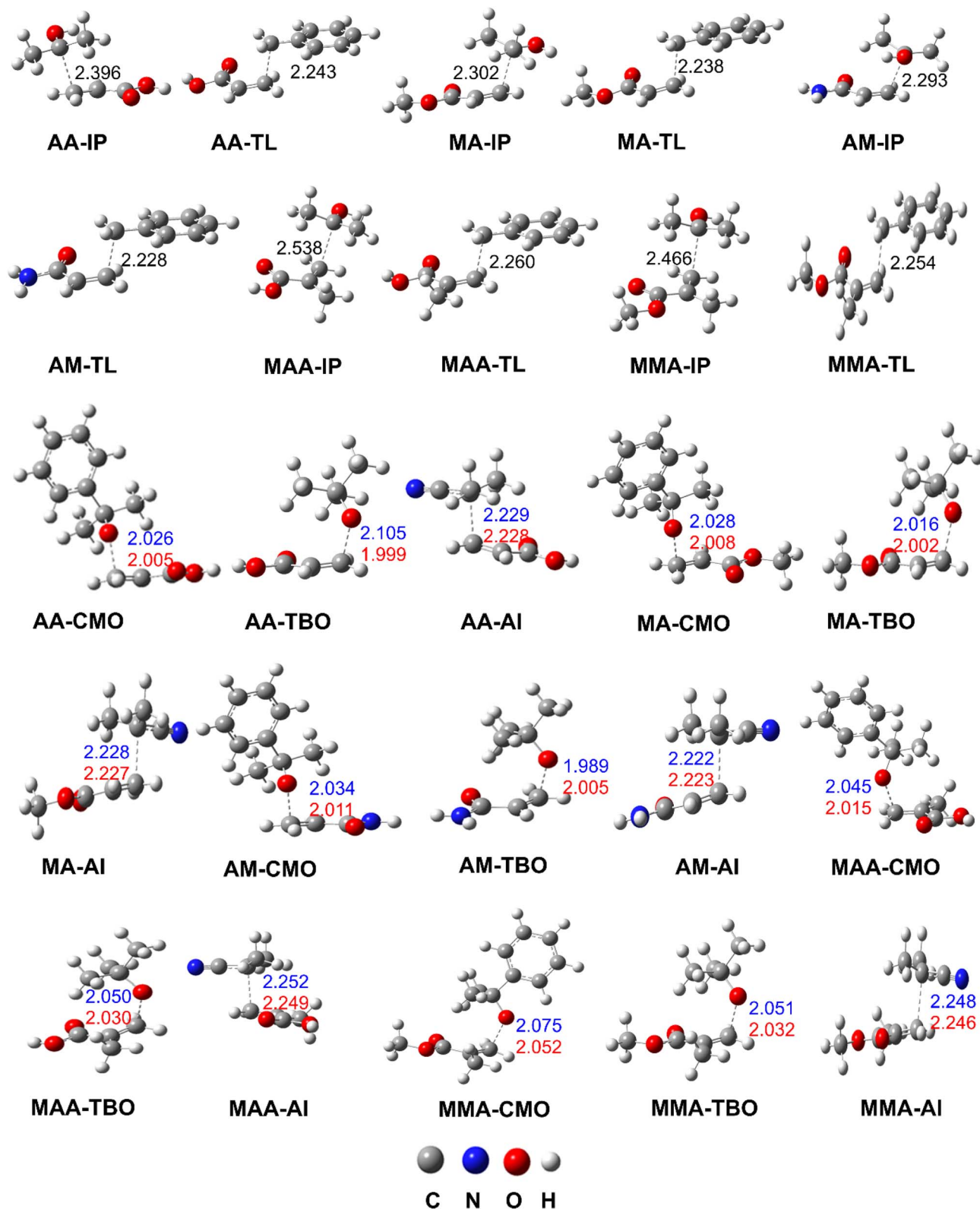


Fig. 3 Selected transition states of the reactions (green for IP and red for TL solvents).

As shown in Table 2, the activation barriers ( $\Delta G^\ddagger$ ) and propagation rate constants ( $k_p$ ) of the first-step propagation reaction ( $n = 1$ ) in the IP and TL solvents are predicted to have a strong dependence on both the monomer structure and the

nature of the initiating radical. For AA and MA, the calculated  $\Delta G^\ddagger$  values fall within 11.1–12.1 kcal mol<sup>-1</sup> in the IP (e.g., 11.6 kcal mol<sup>-1</sup> for TBO-AA and 12.1 kcal mol<sup>-1</sup> for AI-AA; 11.2 kcal mol<sup>-1</sup> for CMO-MA and 12.1 kcal mol<sup>-1</sup> for AI-MA)



Table 2 Calculated  $\Delta G^\ddagger$  (kcal mol<sup>-1</sup>),  $\kappa$ ,  $k_p$  (M<sup>-1</sup> s<sup>-1</sup>) the propagation reaction

Monomer	Intermediates	IP						TL					
		$n = 1$			$n = 2$			$n = 1$			$n = 2$		
		$\Delta G^\ddagger$	$\kappa$	$k_{app}$	$\Delta G^\ddagger$	$\kappa$	$k_{app}$	$\Delta G^\ddagger$	$\kappa$	$k_{app}$	$\Delta G^\ddagger$	$\kappa$	$k_{app}$
<b>AA</b>	<b>TL-AA/IP-AA</b>	11.4	1.3	$2.55 \times 10^4$	12.1	1.3	$1.20 \times 10^4$	13.1	1.3	$2.01 \times 10^2$	13.2	1.3	$1.70 \times 10^3$
	<b>CMO-AA</b>	11.9	1.2	$1.50 \times 10^4$	12.4	1.3	$6.10 \times 10^3$	11.7	1.3	$2.00 \times 10^4$	13.9	1.3	$5.30 \times 10^2$
	<b>TBO-AA</b>	11.6	1.2	$2.20 \times 10^4$	12.9	1.3	$2.70 \times 10^3$	12.2	1.3	$8.40 \times 10^3$	13.0	1.3	$2.30 \times 10^3$
	<b>AI-AA</b>	12.1	1.2	$1.01 \times 10^4$	12.2	1.3	$7.20 \times 10^3$	12.2	1.2	$8.49 \times 10^3$	12.3	1.3	$8.3 \times 10^3$
<b>MA</b>	<b>TL-MA/IP-MA</b>	11.3	1.3	$4.20 \times 10^4$	11.8	1.3	$1.60 \times 10^4$	12.8	1.3	$3.34 \times 10^3$	13.0	1.3	$2.40 \times 10^3$
	<b>CMO-MA</b>	11.2	1.2	$4.59 \times 10^4$	13.0	1.3	$2.20 \times 10^3$	10.5	1.2	$1.50 \times 10^5$	13.7	1.3	$7.30 \times 10^2$
	<b>TBO-MA</b>	11.1	1.2	$5.44 \times 10^4$	11.5	1.1	$2.60 \times 10^4$	10.7	1.2	$1.10 \times 10^5$	11.9	1.3	$1.50 \times 10^4$
	<b>AI-MA</b>	12.1	1.3	$1.90 \times 10^4$	12.5	1.3	$5.40 \times 10^3$	13.5	1.4	$1.20 \times 10^3$	13.9	1.3	$5.22 \times 10^2$
<b>AM</b>	<b>TL-AM/IP-AM</b>	14.2	1.3	$3.10 \times 10^2$	14.7	1.3	$1.50 \times 10^2$	16.5	1.3	6.60	16.8	1.3	4.10
	<b>CMO-AM</b>	11.6	1.2	$2.40 \times 10^4$	15.1	1.3	$7.50 \times 10^1$	12.6	1.3	$4.90 \times 10^3$	16.0	1.4	$1.60 \times 10^1$
	<b>TBO-AM</b>	12.8	1.3	$3.50 \times 10^3$	14.3	1.3	$2.70 \times 10^2$	15.5	1.3	$3.50 \times 10^1$	16.2	1.4	$1.20 \times 10^1$
	<b>AI-AM</b>	13.9	1.3	$5.20 \times 10^2$	14.8	1.3	$1.20 \times 10^2$	12.5	1.3	$5.55 \times 10^3$	12.6	1.3	$4.90 \times 10^3$
<b>MAA</b>	<b>TL-MAA/IP-MAA</b>	14.6	1.3	$1.60 \times 10^2$	15.7	1.4	$2.80 \times 10^1$	14.4	1.3	$2.40 \times 10^2$	17.1	1.3	2.60
	<b>CMO-MAA</b>	11.3	1.0	$3.23 \times 10^4$	15.0	1.3	$8.60 \times 10^1$	11.3	1.3	$4.20 \times 10^4$	15.5	1.3	$3.60 \times 10^1$
	<b>TBO-MAA</b>	12.0	1.0	$1.00 \times 10^4$	15.6	1.3	$3.30 \times 10^1$	11.6	1.2	$2.50 \times 10^4$	15.9	1.3	$1.80 \times 10^1$
	<b>AI-MAA</b>	14.8	1.3	$1.10 \times 10^2$	15.3	1.4	$5.50 \times 10^1$	15.8	1.3	$2.11 \times 10^1$	15.9	1.4	$2.00 \times 10^1$
<b>MMA</b>	<b>TL-MMA/IP-MMA</b>	14.6	1.3	$1.70 \times 10^2$	14.3	1.3	$2.60 \times 10^2$	13.5	1.2	$9.30 \times 10^2$	16.2	1.3	$1.10 \times 10^1$
	<b>CMO-MMA</b>	11.3	1.0	$3.00 \times 10^4$	13.8	1.3	$6.60 \times 10^2$	12.8	1.1	$2.97 \times 10^3$	14.8	1.3	$1.20 \times 10^2$
	<b>TBO-MMA</b>	10.9	1.0	$6.40 \times 10^4$	13.5	1.3	$9.80 \times 10^2$	11.0	1.1	$6.05 \times 10^4$	15.2	1.3	$6.20 \times 10^1$
	<b>AI-MMA</b>	14.4	1.3	$2.10 \times 10^2$	14.5	1.3	$1.80 \times 10^2$	15.1	1.3	$7.60 \times 10^1$	15.2	1.3	$6.40 \times 10^1$

and 10.5–13.5 kcal mol<sup>-1</sup> in TL. These values are slightly lower than those obtained for **AM**, **MAA**, and **MMA**, for which  $\Delta G^\ddagger$  generally exceeds 10.9 kcal mol<sup>-1</sup> and may reach up to 14.8 kcal mol<sup>-1</sup> in IP (e.g., **AI-AM** = 13.9 kcal mol<sup>-1</sup>; **AI-MAA** = 14.8 kcal mol<sup>-1</sup>; **AI-MMA** = 14.4 kcal mol<sup>-1</sup>) and extends to 16.5 kcal mol<sup>-1</sup> in TL. This variation in  $\Delta G^\ddagger$  leads to pronounced differences in the kinetics. The **AA** and **MA** monomers, with relatively low activation barriers, are predicted to have markedly higher  $k_p$  values in the order of  $10^4$ – $10^5$  M<sup>-1</sup> s<sup>-1</sup>. For instance, in IP solvent, **TBO-MA** and **CMO-MA** yield  $k_p$  values of  $5.44 \times 10^4$  and  $4.59 \times 10^4$  M<sup>-1</sup> s<sup>-1</sup>, respectively, whereas in TL solvent, **CMO-MA** and **TBO-MA** reach  $1.50 \times 10^5$  and  $1.10 \times 10^5$  M<sup>-1</sup> s<sup>-1</sup>. In contrast, calculations of **AM**, **MAA**, and **MMA** predict slightly lower  $k_p$  values, mostly within  $10$ – $10^4$  M<sup>-1</sup> s<sup>-1</sup>. For example, in IP solvent, **AI-AM**, **AI-MAA**, and **AI-MMA** possess  $k_p$  values of  $5.20 \times 10^2$ ,  $1.10 \times 10^2$ , and  $2.10 \times 10^2$  M<sup>-1</sup> s<sup>-1</sup>, respectively, while **AM-TL** shows only 6.6 M<sup>-1</sup> s<sup>-1</sup>. These findings indicate that simpler monomers (**AA**, **MA**), characterized by lower activation barriers, undergo significantly faster first-step propagation compared to bulkier or electronically perturbed monomers (**MAA**, **MMA**), in which the steric and electronic effects raise the  $\Delta G^\ddagger$  values and consequently reduce the  $k_p$  values.

In terms of radical type, TBO<sup>•</sup> generally predicted to have the highest initiation activity, with  $k_p$  values (e.g.,  $5.44 \times 10^4$  and  $1.10 \times 10^5$  M<sup>-1</sup> s<sup>-1</sup> for **MA**,  $n = 1$  in the IP and TL, respectively), whereas AI<sup>•</sup> exhibits considerably lower efficiency, particularly in monomers with bulky substituents such as **MAA** and **MMA** in the IP solvent. By contrast, the reactivity of CMO<sup>•</sup> and IP-C2<sup>•</sup>/TL-C7<sup>•</sup> varies substantially depending on the monomer structure. These trends suggest that TBO<sup>•</sup> serves as the most stable

and efficient initiator across diverse monomer systems, while AI<sup>•</sup> displays intrinsically low activity, especially in sterically hindered monomers in the IP solvent, highlighting the selective interplay between the nature of the initiating radical and the monomer framework.

Transitioning from the first propagation step ( $n = 1$ ) to the second ( $n = 2$ ) generally results in an increase in  $\Delta G^\ddagger$  by 0.1–3.5 kcal mol<sup>-1</sup> in IP and 0.1–4.3 kcal mol<sup>-1</sup> in TL, accompanied by a decrease in the corresponding  $k_p$  values, indicating that propagation proceeds more slowly after the initial step. For example, in the propagation reaction of **TBO-AA**,  $\Delta G^\ddagger$  rises from 11.6 to 12.9 kcal mol<sup>-1</sup> for the IP and 12.2 to 13.0 kcal mol<sup>-1</sup> for the TL, while  $k_p$  decreases from  $2.20 \times 10^4$  to  $2.70 \times 10^3$  M<sup>-1</sup> s<sup>-1</sup> and  $8.40 \times 10^3$  to  $2.30 \times 10^3$  M<sup>-1</sup> s<sup>-1</sup> for the IP and TL, respectively. A similar behavior is observed in **TBO-MA**, whereas in the TL solvent, the predicted  $k_p$  values of **TBO-MA** reduce from  $1.10 \times 10^5$  to  $1.50 \times 10^4$  M<sup>-1</sup> s<sup>-1</sup> (the  $\Delta G^\ddagger$  values increase from 10.7 to 11.9 kcal mol<sup>-1</sup>), whereas the rate constant propagation of **TBO-MA** in the IP changes minor in the second step ( $k_p = 4.59$ – $2.60 \times 10^4$  M<sup>-1</sup> s<sup>-1</sup>). This trend is also evident in other monomers such as **AM**, **MAA**, and **MMA**; for instance, in the IP solvent, the  $\Delta G^\ddagger$  of the **CMO-AM** rises from 11.6 to 15.1 kcal mol<sup>-1</sup>, while the  $k_p$  decreases from  $2.40 \times 10^4$  to  $7.50 \times 10^1$  M<sup>-1</sup> s<sup>-1</sup>.

A comparison between the two solvents, IP and TL, clearly suggests that the solvent has a significant influence on the propagation kinetics. In IP, calculations for the monomers **AA** and **MA** yield remarkably high rate constants, typically in the range of  $10^4$ – $10^5$  M<sup>-1</sup> s<sup>-1</sup>. In contrast, although **MA** retains relatively high reactivity in TL, its  $k_p$  values decrease substantially, reaching a maximum of only  $1.50 \times 10^5$  M<sup>-1</sup> s<sup>-1</sup> for the



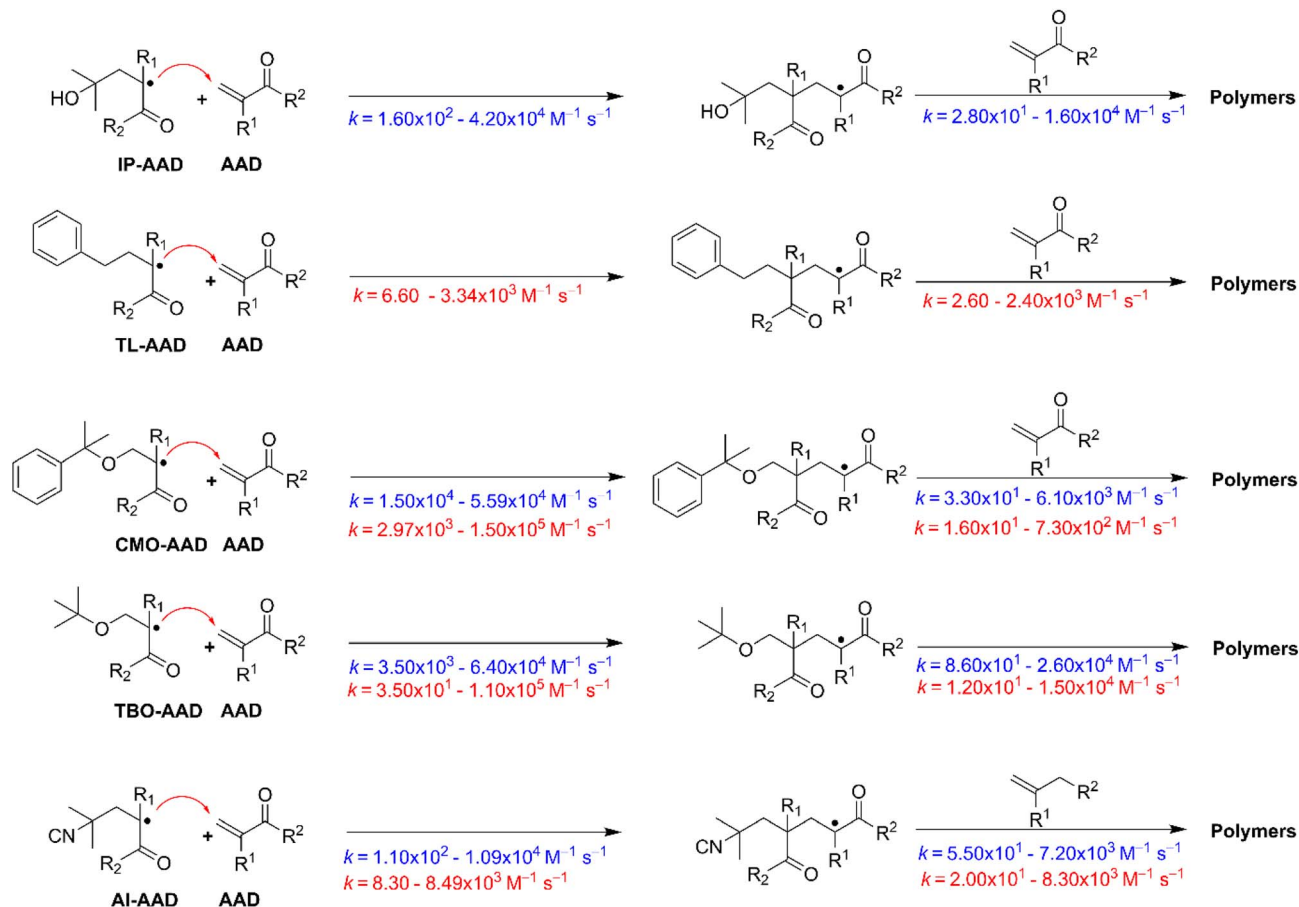


Fig. 4 The propagation reactions (green for IP and red for TL solvents) at 298.15 K.

**CMO-MA.** Bulkier monomers (MAA, MMA) are more strongly affected by the TL solvent, with predicted  $k_p$  values only within  $10^{-3} \text{ M}^{-1} \text{ s}^{-1}$  (e.g.,  $k_p(n=2)\text{AM-TL} = 6.60 \text{ M}^{-1} \text{ s}^{-1}$ ;  $k_p(n=2)\text{AI-MAA} = 21.1 \text{ M}^{-1} \text{ s}^{-1}$ ), whereas the corresponding reactions in IP maintain considerably higher  $k_p$  values in the range of  $10^2 - 10^4 \text{ M}^{-1} \text{ s}^{-1}$ . These results emphasize the critical influence of solvent properties on the reactivity of both simple and sterically hindered monomers during propagation.

In the IP solvent, the propagation rate constants of AADs initiated by TBO $\cdot$ , CMO $\cdot$  and AI $\cdot$  were predicted to be within the ranges of  $8.60 \times 10^1$  to  $2.60 \times 10^4$ ,  $3.30 \times 10^1$  to  $6.10 \times 10^3$  and  $5.50 \times 10^1$  to  $7.20 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ , respectively (Fig. 4). By contrast, in the TL solvent, these values decrease to  $1.20 \times 10^1$  to  $1.50 \times 10^4$ ,  $1.60 \times 10^1$  to  $7.30 \times 10^2$  and  $2.00 \times 10^1$  to  $8.30 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$  for TBO $\cdot$ , CMO $\cdot$  and AI $\cdot$ , respectively. Furthermore, the propagation rate constants of AADs initiated by solvent-derived radicals (IP-C2 $\cdot$  and TL-C7 $\cdot$ ) are found in the range of  $2.80 \times 10^1$  to  $1.60 \times 10^4$  and  $2.60 - 2.40 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$  for the IP and TL, respectively. These data highlight the marked solvent effect on the kinetic profiles of radical-mediated propagation processes. In comparison with the HO $\cdot$ -initiated AAD reactions in aqueous solution ( $k_p = 1.40 \times 10^3$  to  $3.90 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ ),<sup>36</sup> the polymerization of AADs initiated by TBO $\cdot$ , CMO $\cdot$ , and AI $\cdot$  in IP and TL solvents proceeds at relatively lower rates, predicting

slower reactivity in these non-aqueous media. This difference suggests that solvent polarity and hydrogen-bonding capability play a critical role in stabilizing transition states and influencing radical propagation efficiency. Consequently, the reduced reactivity observed in IP and TL highlights the importance of solvent effects in determining the kinetics and mechanism of AAD polymerization.

### 3.3. The effect of temperature on the propagation rate constant in the radical polymerization of AAD in the solvents

The dependence of the propagation rate constant ( $\log(k_p)$ ) on temperature was systematically evaluated in the IP and TL over the range of 293–353 K and 280–380 K, respectively, and the results are shown in Fig. 5 and 6.

The results presented in Fig. 5 suggest that the  $\log(k_p)$  values of all investigated propagation reactions increase almost linearly with temperature in the range of 280–380 K, clearly reflecting the Arrhenius-type dependence of the propagation process. Nevertheless, the pronounced differences among the initiating radicals (i.e. TL-C7 $\cdot$ , TBO $\cdot$ , CMO $\cdot$ , AI $\cdot$ ) and monomers reveal that polymerization kinetics are not solely governed by temperature but are also substantially influenced by the intrinsic properties of the radical initiator and the chemical structure of the monomers (AA, MA, AM, MAA and MMA).



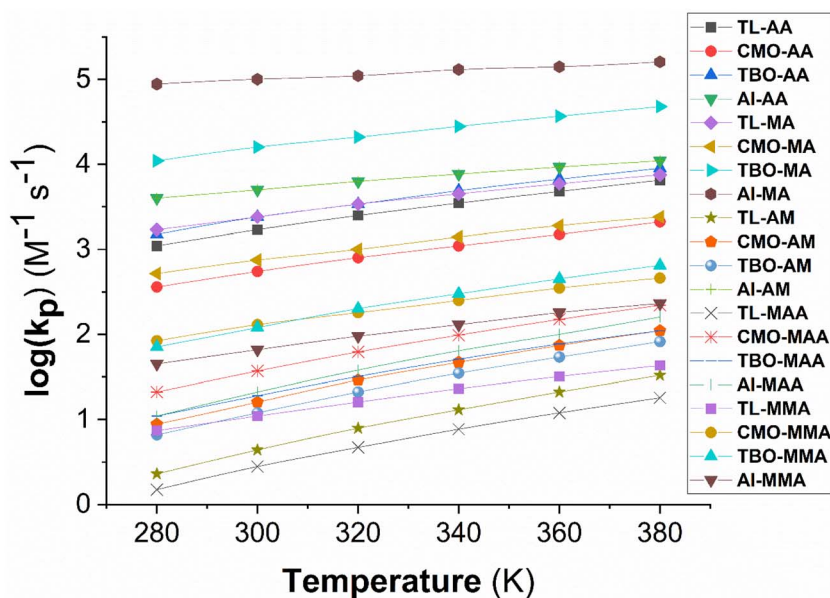


Fig. 5 The temperature influence on propagation rate constants ( $\log(k_p)$ ) in TL at 280–380 K.

For the propagation reaction of **AA**,  $\log(k_p)$  varies from 2.56 (**CMO-AA**, 280 K) to 4.04 (**AI-AA**, 380 K). Throughout the entire temperature range, **AI'** consistently provides the highest values, while **CMO'** gives the lowest, demonstrating the superior initiating efficiency of **AI'** toward **AA**. In the case of **MA**,  $\log(k_p)$  ranges from 2.72 (**CMO-MA**, 280 K) to 5.20 (**AI-MA**, 380 K), indicating that **MA** possesses significantly higher propagation activity than **AA**, particularly in the **AI'** initiation. By contrast, **AM** exhibits striking variations:  $\log(k_p)$  for **AI-AM** reaches 4.04 at 380 K, whereas **TL-AM** shows only 0.36 at 280 K, underscoring the critical importance of initiator selection.

Conversely, **MAA** and **MMA** were predicted to have considerably lower  $\log(k_p)$  values. At 380 K, **AI-MAA** reaches only 2.20, whereas **TL-MAA** remains at 1.26. The **TBO-MMA** and **CMO-MMA** intermediates provide higher  $\log(k_p)$  values than the **AI-MMA** (2.81 and 2.66 vs. 2.36 at 380 K), suggesting that bulky substituents strongly influence the stability of the transition state, thereby modifying initiating efficiency. A comparison among the monomers reveals that  $\log(k_p)$  generally follows the order: **MA** > **AA**  $\approx$  **AM** > **MMA**  $\approx$  **MAA**. For instance, at 380 K under **AI'** initiation, the  $\log(k_p)$  values are 5.20 (**MA**), 4.04 (**AA**), 4.04 (**AM**), 2.20 (**MAA**), and 2.36 (**MMA**). This trend reflects the

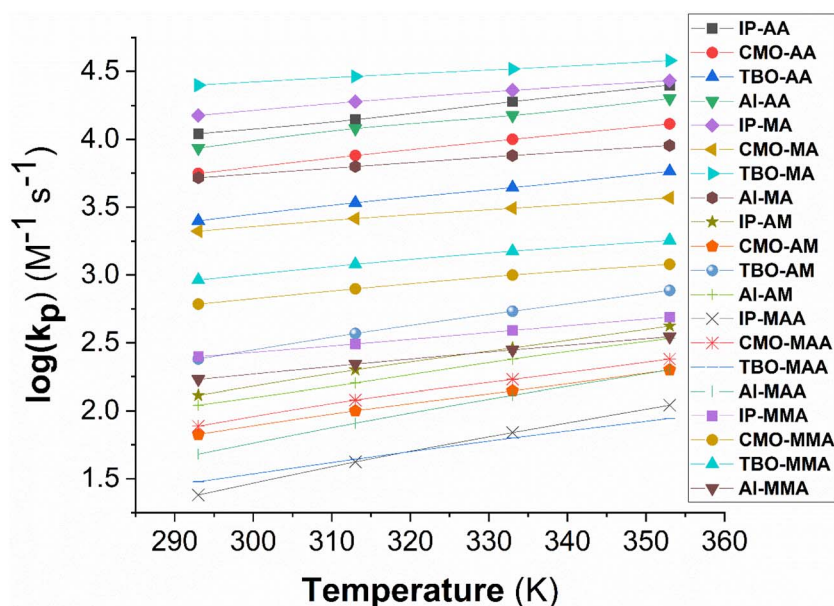


Fig. 6 The temperature influence on propagation rate constants ( $\log(k_p)$ ) in IP at 293–353 K.



combined influence of substituent effects and polarity: acrylates (**MA**, **AA**) exhibit higher propagation activity than methacrylates (**MAA**, **MMA**) due to their smaller substituents, which reduce steric hindrance. The calculated data predict that the propagation rate constant of **MA** polymerization in toluene at 320 K ranges from  $1.00 \times 10^3$  to  $1.10 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Fig. 5), which shows strong agreement with the reported experimental value ( $k_p(\text{exp}) = 2.82 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ).<sup>25</sup> The results further indicate that the radical polymerization of **MA** and **MMA** follows the Arrhenius kinetic model, with activation energies of 3.6 and 3.4 kcal mol<sup>-1</sup> in the temperature range of 280–380 K, respectively. These values are in good agreement with experimental data ( $E_a(\text{MA}) = 4.1$  (ref. 28) and 4.4 kcal mol<sup>-1</sup>,<sup>27</sup> and  $E_a(\text{MMA}) = 2.8\text{--}5.3$  kcal mol<sup>-1</sup> at 303–333 K (ref. 24)), thereby confirming the reliability of the computational approach employed in this study. Thus, in the TL solvent, the data demonstrate that **AI**· is the most effective initiator for the majority of monomers, except for **MMA**, where **TBO**· and **CMO**· show higher performance. At the same time, monomer structure plays a decisive role in determining propagation reactivity.

The results presented in Fig. 6 demonstrate that  $\log(k_p)$  values for all systems increase as the temperature rises from 293 K to 353 K, confirming the acceleration of the chain propagation stage in free-radical polymerization under thermal energy. The near-linear relationship between  $\log(k_p)$  and temperature indicates that the reaction kinetics are primarily governed by thermodynamic factors rather than being restricted by diffusion processes.

Considering the individual monomers, calculations for **AA**, **MA**, and **AM** generally yield higher  $\log(k_p)$  values than **MAA** and **MMA**. At 293 K, the  $\log(k_p)$  of the propagation of **IP-AA** reaches 4.04, whereas that of **IP-MAA** is only 1.38, a difference of 2.66 log units. Similarly, in the propagation of **IP-MA**,  $\log(k_p)$  is 4.18, more than three times higher than in the **IP-MMA** (2.40). Whereas that of the **TBO-MA** achieves 4.40, substantially higher than **TBO-MMA** (2.61) and **TBO-MAA** (1.57). This clearly reflects the steric hindrance imposed by the  $-\text{CH}_3$  substituent in methacrylic monomers, which reduces the radical addition efficiency and thereby suppresses chain propagation. This trend remains consistent throughout the investigated temperature range. With increasing temperature, all systems display growth in  $\log(k_p)$ , though to varying extents. For instance, in the **IP-AA** reaction,  $\log(k_p)$  increases from 4.04 (293 K) to 4.40 (353 K), yielding  $\Delta\log(k_p) = 0.36$ . In contrast, for **IP-MMA**,  $\log(k_p)$  rises only from 2.40 to 2.69 ( $\Delta\log(k_p) = 0.29$ ). The smaller increment in methacrylic systems suggests that although temperature enhances kinetics, steric hindrance remains a significant limiting factor. Studies in the **AM** monomer indicate that although its  $\log(k_p)$  values are lower than those of **AA** and **MA**, they are still noticeably higher than those of the methacrylic systems. For example, at 353 K,  $\log(k_p)$  of **IP-AM** (2.62) surpasses those of **IP-MAA** (2.04) and **IP-MMA** (2.69). This may imply that hydrogen-bonding interactions between isopropanol and the  $-\text{CONH}_2$  group of **AM** provide an additional stabilizing effect, enhancing radical orientation during the propagation step.

The influence of the radical species is also clearly evident. Calculations for **TBO**· consistently yields the highest  $\log(k_p)$  values. For example, with **MA** at 353 K, **TBO-MA** reaches 4.58, while **CMO-MA** is 3.57 and **AI-MA** is 3.95. This indicates that **TBO**· possesses superior electronic stabilization and a more favorable transition state, facilitating efficient chain propagation. In contrast, **CMO**· generally produces lower  $\log(k_p)$  values. With **AA** at 293 K,  $\log(k_p)$  of **CMO-AA** is only 3.14, compared with 4.22 for **TBO-AA** and 4.04 for **IP-AA**. **AI**· exhibits intermediate values, ranging from 2.04 (**AI-AM**, 293 K) to 4.20 (**AI-AA**, 353 K), reflecting its moderate stability in propagation reactions. Comparisons within the same monomer show a consistent trend: **TBO**· dominates, **AI**· is intermediate, and **CMO**· is the lowest. For example, with **AM** at 353 K,  $\log(k_p)$  of **TBO-AM** is 2.89, compared with 2.53 for **AI-AM** and 1.98 for **CMO-AM**. These results highlight the decisive role of radical identity in controlling propagation kinetics.

The comparative analysis between isopropanol and toluene demonstrates that  $\log(k_p)$  consistently increases with rising temperature in both solvents, in agreement with Arrhenius kinetics. However, the predicted magnitude of this increase is more pronounced in toluene, where steric and polarity effects of the solvent impose fewer restrictions on radical propagation. In contrast, hydrogen-bonding interactions in isopropanol partially moderate the temperature effect. These findings not only validate the Arrhenius-based kinetic model but also highlight that the judicious choice of initiator and rational monomer design are critical strategies for controlling free-radical polymerization kinetics.

## 4. Conclusion

Quantum chemical calculations were conducted to study the radical polymerization of **AADs**, including **AA**, **MA**, **AM**, **MAA**, and **MMA**, initiated by **CMO**·, **TBO**·, and **AI**· in the **IP** and **TL** solvents. The results predict that initiation reactions proceed more rapidly in **IP** than in **TL** for all examined **AADs** and radicals (**IP-C2**·, **TL-C7**·, **TBO**·, **CMO**·, and **AI**·). Among the initiators, the relative efficiency follows the order **TBO**· > **AI**· > **CMO**· in both solvents, although the initiation of individual monomers exhibits solvent- and initiator-dependent variations. In **IP** at 298 K, the propagation rate constants of **AADs** initiated by **TBO**·, **CMO**·, and **AI**· were predicted to be in the ranges of  $8.60 \times 10^1$  to  $2.60 \times 10^4$ ,  $3.30 \times 10^1$  to  $6.10 \times 10^3$  and  $5.50 \times 10^1$  to  $5.40 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ , respectively, while in **TL**, these values were significantly lower, ranging from  $1.20 \times 10^1$  to  $1.50 \times 10^4$ ,  $1.60 \times 10^1$  to  $7.30 \times 10^2$  and  $2.00 \times 10^1$  to  $4.90 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ , respectively. Additionally, solvent-derived radicals also contributed to the propagation reactions, with  $k_p$  values of  $2.80 \times 10^1$  to  $2.60 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  in **IP** and  $2.60\text{--}1.50 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  in **TL**. The investigation of temperature effects on the polymerization rate constant reveals that temperature markedly enhances  $\log(k_p)$  in both solvents, consistent with the Arrhenius kinetic model. The calculated  $k_p$  of **MA** polymerization in toluene ( $1.00 \times 10^3$  to  $1.10 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  at 320 K) and the activation energies for **MA** and **MMA** (3.6 and 3.4 kcal mol<sup>-1</sup>, respectively) show excellent agreement with experimental data,



confirming the reliability of the computational method. Nevertheless, the acceleration is more pronounced in toluene than in isopropanol due to the absence of hydrogen-bonding constraints, emphasizing the defining role of solvent nature in governing propagation kinetics. These findings underscore the pronounced influence of solvent environments on both the initiation and propagation stages of radical polymerization, thereby providing valuable mechanistic insights for optimizing reaction conditions in non-aqueous media.

## Conflicts of interest

There are no conflicts to declare.

## Data availability

The data supporting this article have been included as part of the supplementary information (SI). Supplementary information is available. See DOI: <https://doi.org/10.1039/d5ra09849a>.

## Acknowledgements

This research is funded by the Vietnamese Ministry of Education and Training under project number B2025-DNA-12.

## References

- J. Ilare, M. Sponchioni, G. Storti and D. Moscatelli, *React. Chem. Eng.*, 2020, **5**, 2081–2090.
- L. Schöne, J. Schindelka, E. Szeremeta, T. Schaefer, D. Hoffmann, K. J. Rudzinski, R. Szmigielski and H. Herrmann, *Phys. Chem. Chem. Phys.*, 2014, **16**, 6257–6272.
- F.-D. Kuchta, A. M. van Herk and A. L. German, *Macromolecules*, 2000, **33**, 3641–3649.
- F. Lorandi, M. Fantin, Y. Wang, A. A. Isse, A. Gennaro and K. Matyjaszewski, *ACS Macro Lett.*, 2020, **9**, 693–699.
- M. Fujita, Y.-i. Izato and A. Miyake, *J. Therm. Anal. Calorim.*, 2021, **144**, 435–442.
- M. Buback, P. Hesse and I. Lacík, *Macromol. Rapid Commun.*, 2007, **28**, 2049–2054.
- I. Lacík, S. Beuermann and M. Buback, *Macromolecules*, 2003, **36**, 9355–9363.
- S. Beuermann, M. Buback, T. P. Davis, R. G. Gilbert, R. A. Hutchinson, O. F. Olaj, G. T. Russell, J. Schweer and A. M. Van Herk, *Macromol. Chem. Phys.*, 1997, **198**, 1545–1560.
- S. Beuermann, M. Buback, P. Hesse, S. Kukučková and I. Lacík, *Macromol. Symp.*, 2007, 41–49.
- C. Ladavière, N. Dörr and J. P. Claverie, *Macromolecules*, 2001, **34**, 5370–5372.
- K. C. Betz, A. Westhues and W. Pauer, *Appl. Sci.*, 2021, **11**, 9719.
- G. S. Rao, M. Choudhary, M. Naqvi and K. Rao, *Eur. Polym. J.*, 1996, **32**, 695–700.
- A. Senuma, *J. Polym. Sci., Polym. Chem. Ed.*, 1974, **12**, 2631–2638.
- C. Bunyakan and D. Hunkeler, *Polymer*, 1999, **40**, 6213–6224.
- C. Bunyakan, L. Armanet and D. Hunkeler, *Polymer*, 1999, **40**, 6225–6234.
- P. Ghosh and D. Dev, *Eur. Polym. J.*, 1998, **34**, 1539–1547.
- S. Ding and M. Liu, *Polyolefin Characterization: ICPC*, Wiley Online Library, 2007, pp. 162–170.
- L. P. Amaro, B. L. Rivas, S. Coiai, E. Passaglia, S. Augier and F. Ciardelli, *J. Appl. Polym. Sci.*, 2009, **113**, 290–298.
- L. Jiayu, C. Wanghua, C. Liping, T. Yingtao and S. Xin, *Procedia Eng.*, 2012, **43**, 312–317.
- K. Yilmaz, E. S. Mercan, M. Gürsoy and M. Karaman, *Konya J. Eng. Sci.*, 2024, **12**, 586–595.
- E. F. Sheka, *Fullerenes, Nanotubes Carbon Nanostruct.*, 2025, **33**, 195–203.
- E. F. Sheka, *Int. J. Mol. Sci.*, 2024, **25**, 1317.
- E. F. Sheka, *Polymers*, 2023, **15**, 2999.
- M. Fernández-García, J. Martínez and E. Madruga, *Polymer*, 1998, **39**, 991–995.
- A. P. Haehnel, B. Wenn, K. Kockler, T. Bantle, A. M. Misske, F. Fleischhaker, T. Junkers and C. Barner-Kowollik, *Macromol. Rapid Commun.*, 2014, **35**, 2029–2037.
- M. Buback, *Macromol. Rapid Commun.*, 2015, **36**, 1979–1983.
- T. Junkers, M. Schneider-Baumann, S. S. Koo, P. Castignolles and C. Barner-Kowollik, *Macromolecules*, 2010, **43**, 10427–10434.
- C. Barner-Kowollik, S. Beuermann, M. Buback, P. Castignolles, B. Charleux, M. L. Coote, R. A. Hutchinson, T. Junkers, I. Lacík and G. T. Russell, *Polym. Chem.*, 2014, **5**, 204–212.
- S. Srichan, S. Prasertsri, N. Phansroy, P. Chutinantakul, W. Charoenrach, A. Sri-ang, M. Tongsuphun, R. Janthaduang, S. Boonyod and K. Katuengngnan, *Polym. Eng. Sci.*, 2024, **64**, 534–553.
- L. Couvreur, G. Piteau, P. Castignolles, M. Tonge, B. Coutin, B. Charleux and J. P. Vairon, *Macromol. Symp.*, 2001, 197–208.
- M. Buback, *Macromol. Symp.*, 2009, 90–101.
- F. Ganachaud, R. Balic, M. Monteiro and R. Gilbert, *Macromolecules*, 2000, **33**, 8589–8596.
- S. Beuermann, M. Buback, P. Hesse and I. Lacík, *Macromolecules*, 2006, **39**, 184–193.
- S. C. Thickett and R. G. Gilbert, *Polymer*, 2004, **45**, 6993–6999.
- A. Chapiro and J. Dulieu, *Eur. Polym. J.*, 1977, **13**, 563–577.
- T. L. B. Tram, M. V. Bay, N. T. Hoa, A. Mechler and Q. V. Vo, *J. Phys. Chem. A*, 2025, **129**, 8337–8345.
- A. Galano and J. R. Alvarez-Idaboy, *J. Comput. Chem.*, 2013, **34**, 2430–2445.
- Q. V. Vo, N. T. Hoa and A. Mechler, *Polym. Degrad. Stab.*, 2021, **185**, 109483.
- Q. V. Vo, T. L. B. Tram, N. T. Hoa, A.-N. Au-Duong and A. Mechler, *Polym. Degrad. Stab.*, 2023, **216**, 110483.
- M. E. Alberto, N. Russo, A. Grand and A. Galano, *Phys. Chem. Chem. Phys.*, 2013, **15**, 4642–4650.
- A. Galano and J. Raúl Alvarez-Idaboy, *Int. J. Quantum Chem.*, 2019, **119**, e25665.
- M. G. Evans and M. Polanyi, *Trans. Faraday Soc.*, 1935, **31**, 875–894.



- 43 H. Eyring, *J. Chem. Phys.*, 1935, **3**, 107–115.
- 44 D. G. Truhlar, W. L. Hase and J. T. Hynes, *J. Phys. Chem.*, 1983, **87**, 2664–2682.
- 45 E. Dzib, J. L. Cabellos, F. Ortíz-Chi, S. Pan, A. Galano and G. Merino, *Int. J. Quantum Chem.*, 2019, **119**, e25686.
- 46 E. Dzib, J. L. Cabellos, F. Ortiz-Chi, S. Pan, A. Galano and G. Merino, *Eyringpy 1.0.2*, Cinvestav, Mérida, Yucatán, 2018.
- 47 E. Pollak and P. Pechukas, *J. Am. Chem. Soc.*, 1978, **100**, 2984–2991.
- 48 A. Fernández-Ramos, B. A. Ellingson, R. Meana-Pañeda, J. M. Marques and D. G. Truhlar, *Theor. Chem. Acc.*, 2007, **118**, 813–826.
- 49 C. Eckart, *Phys. Rev.*, 1930, **35**, 1303.
- 50 F. C. Collins and G. E. Kimball, *J. Colloid Sci.*, 1949, **4**, 425–437.
- 51 M. Von Smoluchowski, *Z. Phys. Chem.*, 1917, **92**, 129–168.
- 52 A. Galano and J. R. Alvarez-Idaboy, *J. Comput. Chem.*, 2014, **35**, 2019–2026.
- 53 P. McPherson, R. MacDonnell and B. Johnston, *Phys. Chem. Chem. Phys.*, 2025, **27**, 20484–20492.
- 54 Q. V. Vo, T. L. B. Tram, L. P. Hoang, N. T. Hoa and A. Mechler, *RSC Adv.*, 2023, **13**, 23402–23408.
- 55 S. Li, Z.-X. Liu, S.-Y. Li, Y.-J. Ding, Z.-L. Xiao, J. Zhou, X.-Q. Wu, H.-L. Fan, Z.-H. Luo and X.-B. Zhang, *Chem. Eng. J.*, 2025, **504**, 158617.
- 56 Y. Liu, B. Shi, W. Wang, Y. Guo, Y. Zeng, Z. Sun and M. Ge, *ACS Earth Space Chem.*, 2025, **9**, 934–943.
- 57 D. G. Truhlar, *J. Chem. Educ.*, 1985, **62**, 104.
- 58 A. Einstein, *Ann. Phys.*, 1905, **17**, 549–560.
- 59 G. G. Stokes, *Mathematical and Physical Papers*, University Press, Cambridge, 1905.
- 60 M. Carreon-Gonzalez, A. Vivier-Bunge and J. R. Alvarez-Idaboy, *J. Comput. Chem.*, 2019, **40**, 2103–2110.
- 61 Y. Zhao and D. G. Truhlar, *Theor. Chem. Acc.*, 2008, **120**, 215–241.
- 62 H. Boulebd, I. Amine Khodja, K. Benarous, M. Maczynski and M. Spiegel, *J. Org. Chem.*, 2025, **90**, 3257–3268.
- 63 M. Spiegel, *J. Org. Chem.*, 2024, **89**, 8676–8690.
- 64 A. V. Marenich, C. J. Cramer and D. G. Truhlar, *J. Phys. Chem. B*, 2009, **113**, 6378–6396.
- 65 C. Iuga, J. R. I. Alvarez-Idaboy and N. Russo, *J. Org. Chem.*, 2012, **77**, 3868–3877.
- 66 L. Kazmierczak, D. Swiatla-Wojcik and M. Wolszczak, *RSC Adv.*, 2017, **7**, 8800–8807.
- 67 N. D. Coutinho, H. G. Machado, V. H. Carvalho-Silva and W. A. da Silva, *Phys. Chem. Chem. Phys.*, 2021, **23**, 6738–6745.
- 68 D. Minakata, W. Song and J. Crittenden, *Environ. Sci. Technol.*, 2011, **45**, 6057–6065.
- 69 Y.-i. Izato, K. Shiota and A. Miyake, *J. Anal. Appl. Pyrolysis*, 2019, **143**, 104671.
- 70 M. J. Frisch, G. W. Trucks, H. B. Schlegel, G. E. Scuseria, M. A. Robb, J. R. Cheeseman, G. Scalmani, V. Barone, B. Mennucci, G. A. Petersson, H. Nakatsuji, M. Caricato, X. Li, H. P. Hratchian, A. F. Izmaylov, G. Z. J. Bloino, J. L. Sonnenberg, M. Hada, M. Ehara, K. Toyota, R. Fukuda, J. Hasegawa, M. Ishida, T. Nakajima, Y. Honda, O. Kitao, H. Nakai, T. Vreven, J. A. Montgomery Jr, J. E. Peralta, F. Ogliaro, M. Bearpark, J. J. Heyd, E. Brothers, K. N. Kudin, V. N. Staroverov, T. Keith, R. Kobayashi, J. Normand, K. Raghavachari, A. Rendell, J. C. Burant, S. S. Iyengar, J. Tomasi, M. Cossi, N. Rega, J. M. Millam, M. Klene, J. E. Knox, J. B. Cross, V. Bakken, C. Adamo, J. Jaramillo, R. Gomperts, R. E. Stratmann, O. Yazyev, A. J. Austin, R. Cammi, C. Pomelli, J. W. Ochterski, R. L. Martin, K. Morokuma, V. G. Zakrzewski, G. A. Voth, P. Salvador, J. J. Dannenberg, S. Dapprich, A. D. Daniels, O. Farkas, J. B. Foresman, J. V. Ortiz, J. Cioslowski and D. J. Fox, *Gaussian 16, Revision B.01*, Gaussian, Inc., Wallingford CT, 2016.

