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Size-based sorting of dynamic bacterial clusters

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Abstract

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Group A Streptococcus (GAS) forms highly deformable aggregates with broad variations in size and morphology, complicating controlled separation and biological analysis. Reliable methods to isolate fractions of GAS clusters with defined properties are essential for studying host–pathogen interactions that depend on cluster size. Here, we present a simple deterministic lateral displacement (DLD) microfluidic device to separate complex suspensions of bacterial aggregates into two size-enriched fractions. We use a DLD with a small displacement angle to accommodate the large range of particle sizes above the critical size. We introduce an intermediate outlet, in addition to the conventional zigzag and displacement outlets, to collect the aggregates which exhibit a large dispersion due to their broad variety in shape and sizes close to the device critical diameter. In this way, we can demonstrate fractionation of GAS clusters with >90% purity based on effective size while causing minimal fragmentation or additional aggregation, as demonstrated by image analysis and dual-colour experiments. Finally, we show biological relevance through a live immune-cell assay, where human immune cells migrate more rapidly in the presence of larger GAS clusters than in smaller clusters or single bacteria. These results demonstrate that DLD-based separation provides biologically meaningful fractions of bacterial aggregates and enables new analyses of how cluster size influences immune responses.

Keywords: microfluidics; deterministic lateral displacement; bacterial aggregates; size-based sorting; host–pathogen interactions



1. Introduction

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Streptococcus pyogenes, which is commonly referred to as *group A streptococcus* (GAS), is a gram-positive human pathogenic bacterium. This human pathogen causes diseases with an estimated 700 million infected people each year, with a mortality rate of over 25% in severe cases such as necrotizing fasciitis and sepsis. A rapid recent increase in clindamycin resistance¹, the antibiotics routinely used for treating GAS infection, combined with the lack of vaccines or alternative antibiotics, makes understanding GAS pathogenicity important.

GAS, is a round-shaped bacterium (coccus) that has varying tendencies to grow in long chains which form clusters when grown in vitro in a liquid medium^{2, 3}. Based on a study by Frick et al.,⁴ this property of growing in clusters is crucial for adherence, the resistance to phagocytosis, and the virulence of GAS. Other studies on different bacteria such as *Streptococcus pneumoniae*⁵, and on yeast such as *Saccharomyces*, have shown that bio-particles of different sizes and shapes are thought to contribute differently to virulence and colonization⁶. Therefore, sorting GAS bacteria and clusters based on their physical properties can be an important first step in the study of how these properties affect pathogenicity.

Generating size-based fractions from suspensions of cultured GAS is inherently challenging because GAS form clusters when cultured⁷. With cluster sizes of hundreds of bacteria⁴, size distributions are large, and any sorting scheme needs to accommodate this large range. With smaller groups of bacteria forming chains⁸, aspect ratios can be large. Large clusters, while more spherical than shorter chains, can have intricate three-dimensional shapes where rotational effects add to the complexity by making size a poorly defined property⁹. Moreover, surface molecules which help GAS adhere to one another and to various surfaces⁸ allow clusters to stick together and to surfaces, leading to size distributions that vary over time.

Microfluidic systems are popular alternatives to traditional sorters and separators such as membrane filters and centrifugal elutriators and have been used for the separation of biological particles, including bacterial cells¹⁰. These systems can separate a wide range of biological particles and cells, from bacteria¹¹, mammalian^{12, 13}, and cancer cells¹⁴ to viruses, extracellular vesicles¹⁵, and DNA¹⁶. Label-free, microfluidics techniques functioning without the intervention of any external forces, other than those that drive flows, are among the most studied methods for the sorting of biological particles^{17, 18, 19, 20}. Filter-based sorting methods have been employed for isolating biological particles, but they often face challenges such as the clogging of pores by larger cells or debris^{18, 21}. In various studies, inertial focusing^{22, 23}, pinched flow fractionation²⁴, and viscoelastic sorting^{25, 26} have



been used to isolate biological particles, including bacteria, from human physiological samples for diagnostic purposes. These methods, sort particles of different sizes and shapes using hydrodynamic forces, with viscoelastic sorting²⁷ also utilizing elastic forces²⁸. In addition to size, these methods have been shown to be sensitive to other physical properties of the sample, including shape²⁹ and deformability^{22, 23, 25, 30, 31, 21}. However, there is a general lack of the application of these methods to the generation of fractions with well-defined properties from samples with highly heterogeneous sizes and morphologies such as cultures of GAS bacteria

DLD is a label-free, passive, and continuous microfluidic-based sorting method with sensitivity to size³², morphology^{33, 34}, and deformability³⁴ of biological particles. This sensitivity comes from interactions between particles and pillars which force particles into specific trajectories. Arrays can be designed to be more or less sensitive to different physical properties for example with optimised pillar shapes^{35, 36} but size is most often the dominant parameter. There are two dominant trajectories through a DLD array which are divided by a threshold diameter, known as the critical diameter, D_C , see Figure 1a. In the ideal operation, particles smaller than D_C follow the direction of the fluid flow in a trajectory that is referred to as the zigzag trajectory (and are collected in the zigzag outlet) and those larger than D_C follow the displacement trajectory (and are collected in the displacement outlet).

For a quadratic pillar array, D_C depends on the gap size, G , between pillars and the angle, θ , at which the array is tilted with respect to the flow direction, or equivalently the periodicity, $N = 1/\tan\theta$ of the array along the channel. The critical diameter^{37, 38} can be approximated by a simple expression.

$$D_C \cong G\sqrt{2\tan\theta} \quad \text{Equation 1}$$

DLD has been adopted for bacterial and parasite sorting in various studies. For instance, it was used by Beech et al. for the sorting of *pneumococcus* based on their chain length³⁴, by Holm et al. for the isolation of *trypanosomatid* from blood^{33, 39}, and by Ranjan et al. for sorting of *E.coli*³⁵. Although these studies have reported highly efficient sorting, their effectiveness has been demonstrated mainly in separating two populations that differed markedly in size, each of which was relatively homogeneous in size. Using DLD for size based fractionation of GAS bacteria is challenging due to the wide continuous range of sizes and heterogeneous shapes. While the individual bacteria are on the 1 μm scale, doublets, chains, and clusters are larger and span two orders of magnitude in size.

Instead of resorting to a complicated device with multiple separation sections on one chip, where each section removes particles of a different size range sequentially^{39, 40}, we present a simplified solution with a deterministic



lateral displacement (DLD) device based on a single separation array for separating cultured GAS bacteria into two well-defined, size-based fractions. Equation 1 shows that we can accommodate the wide range of sizes in the displaced fraction by minimizing the array angle. However, the small array angle makes the separation sensitive to flow perturbations, and together with a sample that exhibits a wide variety of shapes, we expect particles with sizes close to the D_c to disperse, thereby contaminating the zigzag and displacement outlets. We addressed that problem by adding an intermediate outlet that collects most of the dispersed particles. This way we ensured that the collected fractions were as pure as possible with respect to size, allowing us to isolate two populations in the zigzag and displacement outlets with sufficient numbers of clusters for downstream biological assays.

We demonstrate the ability of the device to generate size-based fractions from the complex GAS cluster population. Careful comparison of GAS cluster size and morphology before and after sorting was used to detect any changes in shape or size as the sample is passed through the device. By running a mixture of two GAS cluster populations pre-stained in two different colours and quantifying dual colour clusters in the outlets, we could identify and estimate the extent of exchange between clusters in the device. Finally, a preliminary proof of concept study of the effect of GAS cluster size was performed with two distinct, size-based fractions. In this assay, immune cells (neutrophils) were imaged via time-lapse microscopy as they interacted with the two fractions containing different cluster sizes.

2. Experimental

2.1. DLD device design

The aim for the device was to generate one fraction containing singlets, doublets and small clusters of GAS up to approximately 10 μm in diameter for collection in the zigzag outlet and a second fraction containing clusters above 10 μm in diameter in the displacement outlet. Our design aims at achieving high throughput, low level of sample dilution, high purity and low level of sample break-up.

It is well known that in practice, the flow angle of particles moving in a DLD as a function of particle size is not described by a sharp step-function between the direction of the average liquid flow and the direction given by the obstacle array. This can be traced back to factors related to the applied flow rates, the characteristics of the particles and the device design. For low Péclet numbers, i.e. small particles and slow flow rates, the transition between the two flow directions is gradual, due to diffusion³². For very high concentrations, particle-particle interactions become important, causing a shift of the critical diameter to lower values as well as a slight broadening of the



particle trajectories^{16, 41}. For array angles such that the periodicity N is not an integer, additional particle trajectories can appear⁴², which in practice may also blur the transition. For arrays that deviate from a square lattice such as rhombic arrays and arrays with different lateral and longitudinal distances between the pillars, the flow permeability may be anisotropic, which in turn may change the fluid flow direction locally⁴³⁻⁴⁶. For high Reynolds numbers, flow anisotropy in the array may cause deviations in the flow trajectories as a function of flow rate⁴⁷. Since the D_c depends on the flow direction, these factors may introduce dispersion in the flow trajectories of the particles as well as shifts in the critical diameter. Moreover, deformable particles with non-spherical shape may change their shape and orientation dynamically as they move from pillar to pillar in the array⁴⁸, changing their effective size, which, in turn, may have a large impact on their trajectories.

The sizes of the GAS clusters range from single bacteria (1 μm) to hundreds of bacteria (many tens of micrometers). In order to create two fractions, one with single cells, doublets and small clusters and another with larger clusters, our device is required to simultaneously have a rather small critical diameter, while have large enough gaps G to allow all clusters to pass without clogging the array. From equation 1, we can see that this can be achieved by minimizing the array angle, corresponding to using the largest possible periodicity of the array, N . Moreover, large N has been shown to improve separation for soft particles especially at high flow rates¹⁶ which makes it even more important for our bacterial clusters. Large N lead to smaller deformations at each event since for a given lateral displacement the number of post interactions scales as $1/\tan(\theta)$. Devices with small θ (large N) therefore spread the lateral driving force over a larger number of particle-obstacle interactions.

To balance the need for large N with the practical requirement to fit the device on a manageable 55x75 mm glass slide (considering that the large particles are displaced by $\frac{L}{N}$, where L is the length of the array), we chose to make a device with $D_c = G\sqrt{\frac{2}{N}} \approx 8 \mu\text{m}$, $N = 69$, which corresponds to a gap of $G = 45 \mu\text{m}$. The length of the DLD array is 65590 μm . The width is selected to be 950 μm which corresponds to all large particles that enter in the inlet channel will also hit the wall once they reach the end of the array. To minimize the problems described above with rhombic arrays, we utilized a square array⁴⁶, rotated at an angle $\theta = 0.83^\circ$ with respect to the flow direction to achieve $N = 69$. Although higher periodicities have been reported ($N = 100$ ⁴⁹) in the literature, we choose an intermediate value to keep the sensitivity to any perturbations to the particles trajectories within a range that we can handle. An important concern with DLD arrays is the effects of non-integer periodicities of the array, resulting in anomalous trajectories in addition to the standard zigzag and displacement trajectories. It is however mainly a problem for small N . In our case, it can be shown that the angles for these anomalous trajectories amount to less



than 1.5% of the angle of the displacement trajectory. This in turn translates into $14\mu\text{m}$ lateral displacement at the end of the device, which is significantly less than the gap between pillars in the DLD array. We therefore conclude that the effect can be neglected for our device.

Finally, we want to minimize the volume of liquids handled by the device and minimize dilution of the sample by keeping it as narrow as possible with a width corresponding to one displacement array, the length of the DLD array divided by N . Due to the small array angle, the device becomes sensitive to any perturbations of the flow due to overall misalignment of the flow. With a narrow device, the performance is affected by local changes in flow patterns close to the wall⁵⁰. While the wall effect can be compensated for by careful and high-resolution modifications of the pillars at the boundary of the array^{51,52}, other effects, e.g. from complex particles are not. We therefore resort to a simple solution. To ensure the purity of our two collected fractions, we introduce a third outlet to our device, in addition to the zigzag and displacement outlets, which we call intermediate outlet, that collects all sample that does not move consistently in either of the zigzag or displacement trajectories (see Figure 1b for detailed description of the device). We expect to gain in terms of purity of the sample and simplicity of the device design at a cost of losing some of the sample.

Figure 1b shows a schematic of the device with sample inputs and outputs and illustrations depicting a typical GAS sample. The inlet and outlet channels are designed to have equal fluidic resistances per unit width respectively although the outlet channels are longer with higher resistances, which we have observed to lead to stable, laminar flow throughout the separation array. Finite element simulations used in the design process can be found in SI-1.



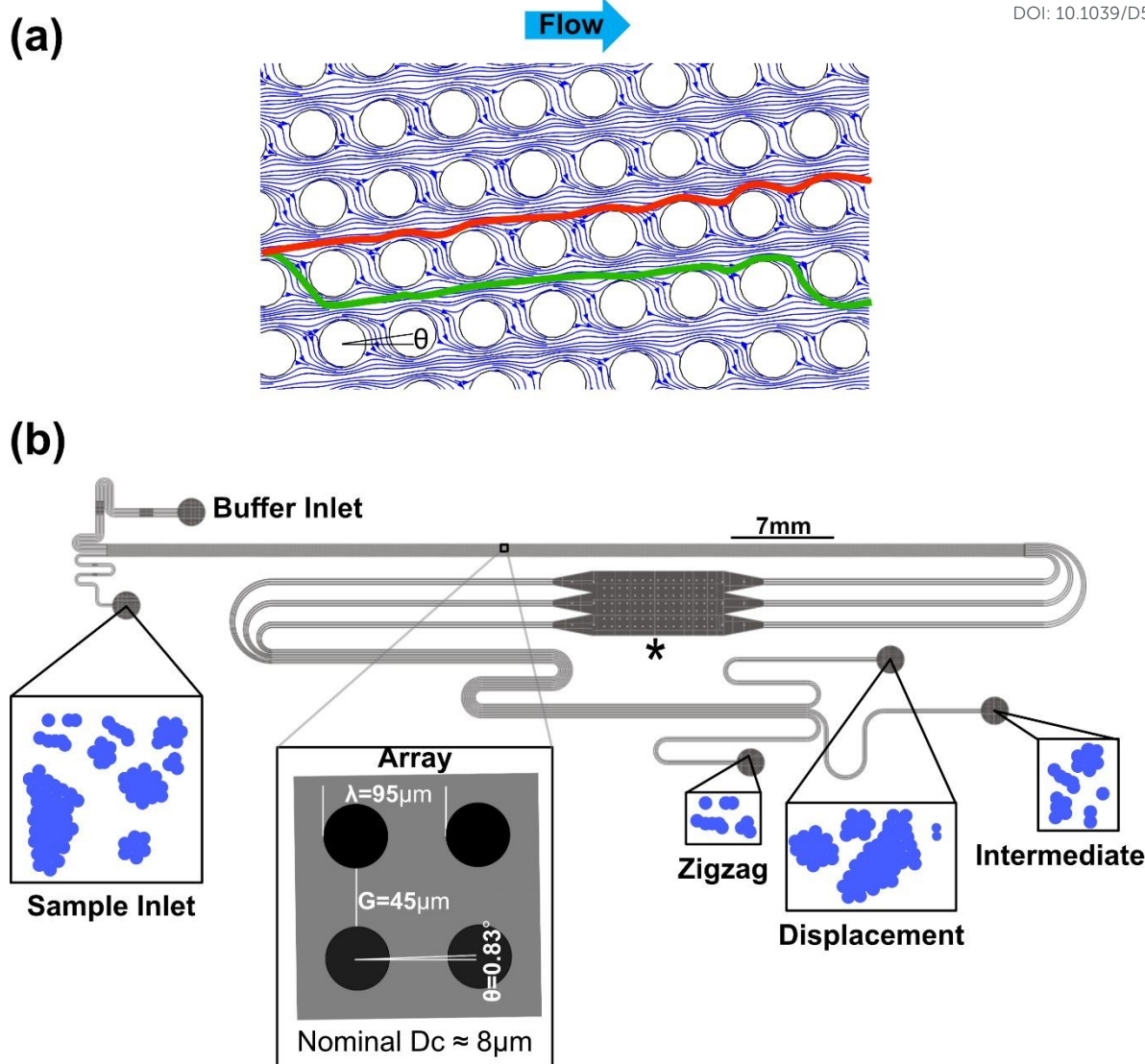


Figure 1.a) Schematic illustration of displacement and zigzag path in a DLD array. The red line shows the path for displacement and the green line shows the path for zigzag. θ is the tilted angle of the DLD device. b) Schematic overview of our device with illustrations of sample inputs and separated outputs. Separation occurs in the DLD array contained in the first long straight section of the device. The inset shows a schematic with the parameters used in the DLD array. The smallest particles move in zigzag mode and exit the device via the Zigzag outlet. Large particles move in the displacement mode and are collected in the Displacement outlet. Any particles not in one or the other of these modes exit via the Intermediate outlet which serves to maintain the purity of the other two fractions. The device also contains an observation area, indicated with an asterisk, that is used to observe lateral particle distributions.

2.2. DLD Device fabrication

Full details of device fabrication protocols and device characterization can be found in the SI-2. In short, mask-based UV-lithography was used to create a master mould in a $100\mu\text{m}$ thick dry film resist (SUEX®, K100, DJ Microlaminates, Sudbury, Massachusetts, USA) laminated onto a 4" silicon wafer and this was then used to create replicas in PDMS that were plasma bonded to glass slides.



2.3. Sample preparation: bacteria culture

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GAS strains of the M1 serotype, SF370 were cultured statically in Todd-Hewitt Yeast media (THY) at 37°C, 5% CO₂. Three weeks before culture, the strain was maintained on THY agar plates. Bacteria were grown to the logarithmic phase by diluting an overnight culture 1:20 in fresh THY. After dilution, bacteria were grown for around 2–2.5 hrs and then washed 2 times with PBS. After washing with phosphate buffer saline (PBS, Merck Life Science AB, Stockholm, Sweden), the bacteria were heat-killed. This was achieved using 15 minutes on ice, followed by a 5-minute heat shock at 80°C and a final 15 minutes on ice. The heat-killed bacteria were then stained according to the type of experiment performed. For the size-based separation characterisations and bioassays GAS were stained with Oregon Green (OG) 488-X succinimidyl ester (ThermoFisher, Massachusetts, United States) at a concentration of 20 mg/mL (a 2μL dye solution was added to 1mL of bacteria at 37°C under gentle rotation whilst protected from light for 30 min). The two-colour study of cluster dynamics was done using both OG and Wheat Germ Agglutinin (WGA) conjugated fluorescent dye 640nm emission (CR®640, Biotium, Inc., Fremont, CA, United States), (100μL of dye solution prepared in 0.15M (molar) NaCl buffer solution with a concentration of 1mg/mL was added to twice buffer-washed bacteria and incubated at room temperature under gentle rotation, protected from light, for 20 min). For all experiments, bacterial samples were diluted 40 times with bovine serum albumin (BSA, Merck Life Science AB, Stockholm, Sweden) 1 w/v% in water and a total of 1 mL of sample prepared this way was used as inputs for sorting. Heat killing of bacteria is a common practice and is not expected to change the short-term interaction of bacteria with immune cells⁵³. Note that for work with pathogenic bacteria, adherence to standard safety routines and precautions including wearing personal protective equipment is a requirement. This includes using protective gloves, goggles and face shields as appropriate as well as working in a ventilated dedicated workspace. Routines must be in place to ensure that users are properly trained accordingly.

2.4. Neutrophil preparation and phagocytosis assay captured by time-lapse microscopy

Neutrophils were isolated from a single healthy donor for each experiment. All experiments with blood cells were performed in accordance with the Guidelines of the Declaration of Helsinki, and Experiments were approved by the Swedish Ethical Review Authority at Lund, permit number 2015/801. Informed consent was obtained from all human participants in this study. Isolation was done using a Polymorphoprep density gradient (Serumwerk Bernburg AG, Bernburg, Germany) according to the manufacturer's instructions. If there was any contamination with erythrocytes then the cells were pelleted and the supernatant removed. The cells were then resuspended in 1



mL of Milli-Q (Merck Millipore, Darmstadt, Germany), immediately followed by 14 mL of 1× PBS to reinstate an isotonic state. Cells were pelleted again and lysis was repeated until the cell pellet appeared clear of erythrocytes. Cells were then resuspended in Na Media (5.6 mM glucose, 127 mM NaCl, 10.8 mM KCl, 2.4 mM KH_2PO_4 , 1.6 mM MgSO_4 , 10 mM HEPES, 1.8 mM CaCl_2 ; pH adjusted to 7.3 with NaOH). Cells were counted using a Bürker chamber and the concentration was adjusted to 3×10^5 mL. The cell-permeant nucleic acid stain, Hoechst 33342 (ThermoFisher Scientific, Waltham, MA USA) was added at a final concentration of 2 μM and the cells were then kept on ice before further use. Imaging was done using 35 mm dishes with 20 mm inner chambers that were fitted with untreated No 1.5 coverslips (Cellvis, Mountain View, CA, USA). The coverslip was coated with 20 $\mu\text{g/mL}$ of fibronectin after which it was blocked with 1 % BSA in PBS. For the phagocytosis experiment, the bacteria were first heat-killed, stained as described above and added directly to the coated coverslips after sorting using the DLD device. Clusters were allowed to settle and adhere to the coated coverslip. The supernatant was then gently aspirated and 1 mL of the prepared neutrophil suspension was added before transferring the dish to the microscope with a stage incubator for time-lapse live cell imaging (37°C, 5% CO_2). The dish was left undisturbed for 30 minutes to allow the neutrophils to adhere before time-lapse microscopy was initiated at a rate of one frame every second minute.

2.5. Fluidics and microscopy

Flow was generated in our device by keeping the outlets at ambient pressure and applying nitrogen at overpressures that were carefully adjusted to obtain a stable and even flow straight through the pillar array. The pressures were applied to two 15 mL tubes using an MFCS-4C pressure controller (Fluigent, Paris, France), specifically 140 mbar for the sample and 150 mbar for the buffer. The resulting flow rate through the device is $30 \pm 2 \mu\text{L/min}$ corresponding to an average shear rate of 210 s^{-1} and, assuming the viscosity of water, a shear stress of 0.2 Pa. This is within typical ranges for biofilm studies, under physiological conditions in the airways and in e.g. microfluidic perfusion systems⁵⁴.

The fluids flow via 768 μm inner diameter capillaries from these tubes into the device. Devices were prepared by rinsing with the running buffer (BSA 1 % w/v) for 10 min prior to running the samples. Because GAS have a higher density than the running buffer, they tend to sediment in the sample collection outlets where the concentration can become high enough that clusters interact and can stick together. To avoid this, separated fractions were moved off-chip directly after sorting by allowing them to flow downwards out of the device, through short capillary tubes. The large (displacement) and middle-sized (intermediate) fractions flowed directly



into two separate wells of an *Ibidi*, microscope slide-based well plate (*Ibidi* μ -slides, 8-well high, *Ibidi GmbH*, Gräfelfing, Germany) coated with fibronectin. The small fraction (zigzag), which was at too high a concentration for both image analysis and the phagocytosis assay, flowed first into a gently shaken 1.5 mL centrifuge tube half-filled with running buffer to first decrease the concentration and was then transferred to a third well of the fibronectin-covered *Ibidi* slide. Individual GAS cells and clusters were allowed to settle and adhere to the fibronectin-covered surface of the slide. Orienting the device and collecting the sample in this way minimized the effects of sedimentation inside the capillaries which tended to lead to aggregation post separation. After collection in the petri dishes the separated fractions were left undisturbed for 30 minutes to assure the sedimentation of bacteria and clusters onto the bottom of the glass slides where they could be imaged using fluorescent microscopy. All subsequent image analyses were performed on samples prepared in this way. Phagocytosis assays were subsequently performed on samples prepared the same way but refrigerated for 2 hours and only including the zigzag and displacement fractions.

All fluidics experiments were performed under observation using an inverted epifluorescence microscope (Nikon Eclipse TE2000-U, Nikon Corporation, Tokyo, Japan) in transmission mode together with a scientific CMOS camera (Andor NEO sCMOS, Andor Technology, Belfast, Northern Ireland) at various magnifications (4x, 10x, 20 and 50x). Size distributions of GAS clusters in pre and post sorted samples together with two colour cluster dynamics measurements were done on a similar microscope (Nikon Eclipse Ti, Nikon Corporation, Tokyo, Japan) with cMOS camera (ORCA-flash 4.0, Hamamatsu Photonics, Japan) or an EMCCD camera (Andor iXon, Andor Technology, Belfast, Northern Ireland), with FITC and Cy5 filter cubes and an LED light source (Sola light engine, Lumencore, Beaverton, Oregon, USA).

For the immuno assay the microscope (Nikon Ti2, Nikon Corporation, Tokyo, Japan) featured a cage incubator (Okolab, Ottaviano, Italy) to allow for live cell imaging (37°C, 5% CO₂). Images were acquired with a 20 \times /0.75 N.A. Plan Apo λ objective (Nikon) with an additional 1.5 \times zoom (Nikon OptoVar, Nikon Corporation, Tokyo, Japan). All images were captured using a DS-Qi2 camera (Nikon Corporation, Tokyo, Japan), giving a size of the field of view of 1200 μ m x 797 μ m.

Further details can be found in SI-3 and SI-4.



2.6. Image and statistical analysis

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Automated scans with multiple fields of view were captured of non-sorted and sorted samples in *Ibidi* μ -slide wells. A full description of the analysis pipeline can be found in the SI-4. Briefly, images were classified into two main types using signal to background noise analysis. Those containing many single bacteria and small clusters (non-sorted and small sorted fractions) were analysed using Ilastik, a deep learning computer vision software⁵⁵ which is time and compute expensive but gives much better results for the semantic segmentation of small, high density objects with low signal to noise. Images with fewer, larger objects, and better resulting signal to noise, were segmented into background and foreground using intensity thresholding with Otsu's algorithm. Images were also manually inspected in Fiji⁵⁶ at a range of contrast levels to ensure that no small objects were missed in the segmentation process. Automated image analyses returning unrealistic size values (e.g. outside the expected range of between 1.8 and 500 pixels at 20x magnification) were rerun in Ilastik under increased user supervision. Two-colour cluster analysis involved performing all of the above in two separate colour channels and characterising and counting clusters of both single and mixed colours.

3. Results and Discussion

3.1. Sorting of GAS clusters by size

GAS clusters were separated into distinct size fractions. Figure 2 shows example microscopy images of GAS samples after separation with obvious differences in the sizes and numbers of clusters. As can be seen in Figure 2a-b, there is a significant difference in major axis length between the collected zigzag and displacement fractions, while the intermediate fraction major axis lengths span over a broader range, overlapping with the two other fractions. This clearly shows how the additional intermediate outlet successfully captures particles that move with trajectories outside the zigzag and displacement modes which would, greatly decrease the purity of the collected fractions in a conventional two-outlet device. Figure 2b also shows that there are clusters in the separated fractions that, with a major axis up to $\approx 120 \mu\text{m}$, are larger than the gaps in the array ($45 \mu\text{m}$ wide and $100 \mu\text{m}$ deep), indicating that either they are narrow enough to fit through the array and are rotating in order to do so, or unlike microspheres, they are able to deform and squeeze through the gaps. A third possibility is that the clusters dynamically break up and reform in the device before we perform the image analysis as indicated by the two-colour mixing experiment.



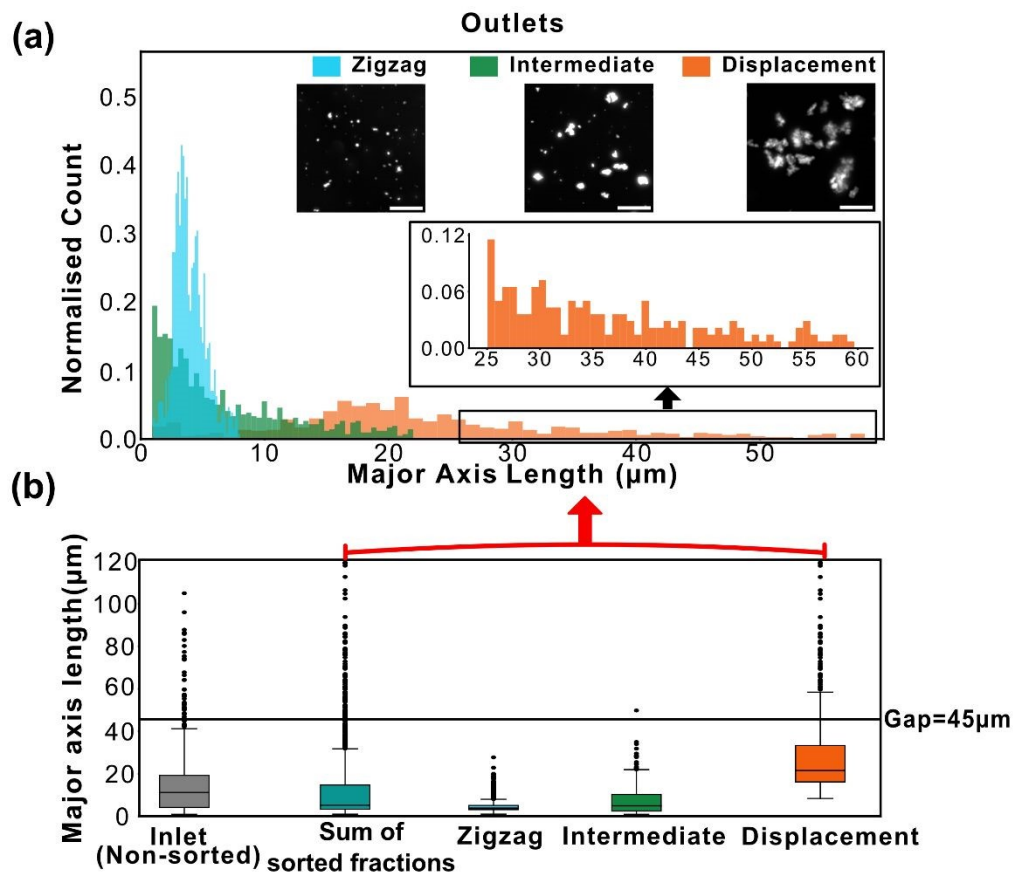


Figure 2 The results of GAS cluster separations. a) Measured major axis length distributions in GAS cluster fractions collected from each of the device outlets together with representative images of each fraction. b) Box plots of major axis length distributions for both the unsorted sample, and for the sorted fractions. The box showing the “sum of sorted fractions”, provides an estimate of any changes in the distribution due to effects in the device.

To estimate the probabilities of a particle of a given size to end up in each one of the three outlets we use an Bayesian approach. We used the measured size distributions of the bio particles (mainly bacterial clusters) in the three outlets to derive the, see Figure 3. The probability of a particle of size d_i ending up in outlet k is given by:

$$P(k | d_i) = \frac{P(d_i | k)}{\sum_j P(d_i | j)}$$

Here, $P(d_i | k)$ represents the probability of finding a particle of size d_i among all particles in outlet k . We define a reference cut-off size as the particle size for which the probabilities of exiting through the zigzag outlet and the displacement outlet are equal ($D_c \approx 11\mu\text{m}$). This would be the equivalent to the critical diameter D_c for ideal spherical particles in an ideal DLD device. We use this value to calculate the purity of the sorted fractions. Purity of a subpopulation in an outlet is defined as the number of particles in the desired size range divided by the total



number of particles in that outlet. Being aware that the bacteria and the bacterial clusters do stick inside the device or sometimes do not enter the device, we define a nominal yield defined as the fraction of the number of particles in the desired size range and in the desired outlet among all outlets.

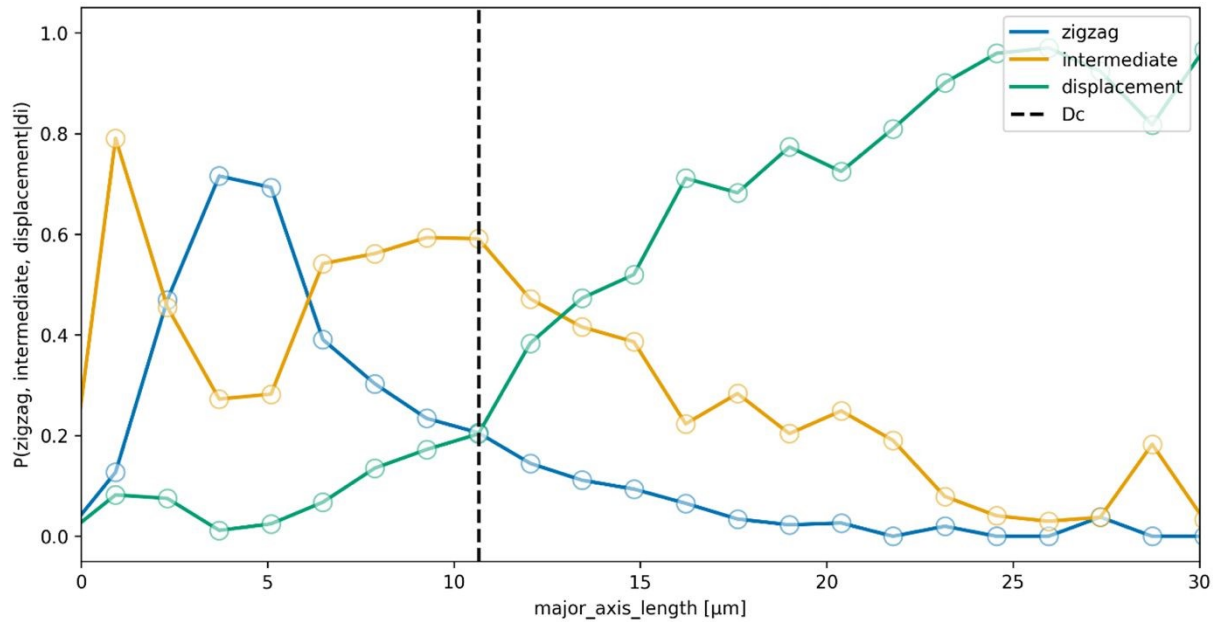


Figure 3 Routing probabilities to the three outlets of particles of different sizes for bacteria. The crossover for the zigzag and displacement outlets gives the critical diameter $\approx 11\mu\text{m}$, in this case with a significant overlap between the two fractions.

We find that the purity for the small fraction is 91% and for the large fraction is 90%, with yields 74% for the small and 73% for the large. Expressions for the purities and yields are defined in SI-4.

3.2. GAS cluster dynamics during separations

To assess the cluster breakup and reaggregation in our experiments, we analysed the problem from two perspectives. To start with, we compared the size distributions of the unsorted (inlet) and the pooled outlet subpopulations, and found an increase among the small clusters. This raises the question whether the change in size distribution is due to selective losses or due to breakup of the clusters. We therefore followed up by mixing two identical bacterial cluster populations that differ only in colour. The mixture was studied in bulk as well as in our separation device.

We plotted the sum of all measured clusters in the three outlets and compared the resulting distribution to that measured for the sample that we introduced in the inlet, see Figure 4. We observed a moderate decrease in relative abundance of large clusters. This can either be due some large clusters not entering the device or being stuck in the device. Alternatively, this could be due to large clusters breaking into smaller ones. Since we could not see



any major clogging in our device, and since we observed a noticeable increase in the relative abundance of small clusters (with major axis length $<10\text{ }\mu\text{m}$), we can speculate that some clusters break into smaller pieces. Note that the data is normalised as a probability density distribution so that any increase in small particles by definition leads to a smaller fraction of larger particles. The apparent decrease in larger particles is therefore expected to be somewhat exaggerated.

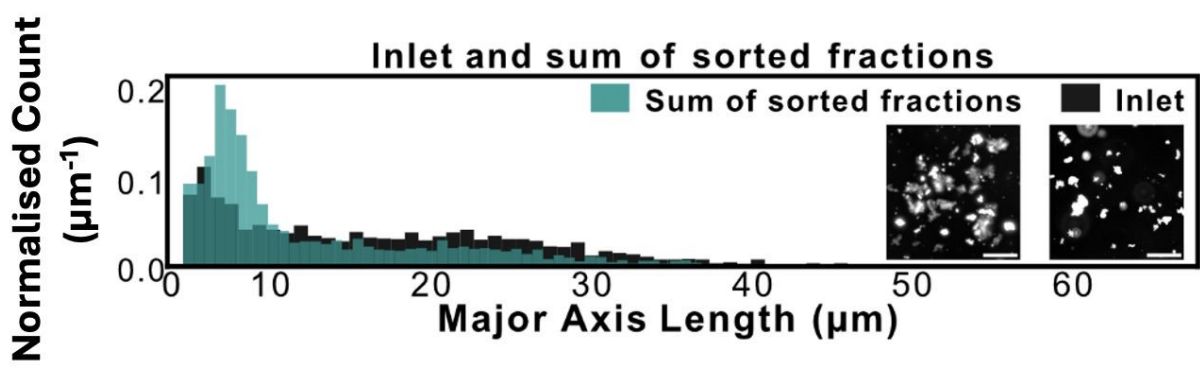


Figure 4. Histograms of inlet and sum of collected fractions. Micrographs show a representative image of the unsorted sample on the right and an image compiled by overlaying images of the three sorted fractions on the left. Scale bars are $50\mu\text{m}$.

To test for any breakup and reaggregation of the clusters in more detail during DLD separation, we performed a two-colour mixing experiment. In these experiments two identical suspensions of GAS clusters are stained each with a different colour and subsequently mixed immediately before sorting. The final concentration of the mixture is the same as that of the bacterial solution used for sorting GAS ($50\text{ }\mu\text{L}$ of each sample, resulting in a final volume of $100\text{ }\mu\text{L}$ in 4 mL of 1% BSA buffer). Any clusters containing both colours must have formed based on an exchange between the clusters. Figure 5 shows how this experiment was done. The separation process took 30 minutes, with the inlet bacterial sample continuously shaken in 15 mL Falcon tubes at 20 rpm . After collection at the outlets, the samples were left to rest for 30 minutes to allow sedimentation at the bottom of Petri dishes. Figure 5b shows examples of clusters with those containing both colours marked with a blue ring. Due to the finite time between mixing the two suspensions and taking the images before loading them into the device, during which clusters can interact and merge, we detect a small number of two-colour clusters in the inlet population. For the collected outlet fractions, there is a small but significant increase in the numbers of two-colour clusters when compared to the inlet. We can also observe that the number of mixed clusters is greater for the intermediate and the displacement outlets. This can be explained by two mechanisms. First, it is reasonable to assume that clusters consisting of a combination of two clusters are larger than other clusters and therefore are found in the displacement outlet. Second, since the contact between the particles and the pillars in the DLD array is significantly more frequent for displacement mode than for zigzag mode, roughly by a factor of N , the shear



experienced by the large clusters is greater, which may cause them to shed more smaller clusters, which in turn may bind randomly to the surrounding clusters. Note that care needs to be taken when interpreting the absolute numbers of clusters because the high density of clusters in the images may lead to cluster overlap, even if they have not physically joined. Taken together the above results show a relative clustering of about 10% for the outlets. See Figure 5c. We can thus conclude that we have a good size-based separation of GAS clusters with only minor cluster breakup and merging taking place in the device with sufficient GAS clusters in each fraction for bioassays. Control experiments of cluster dynamics in bulk are described in SI-5.

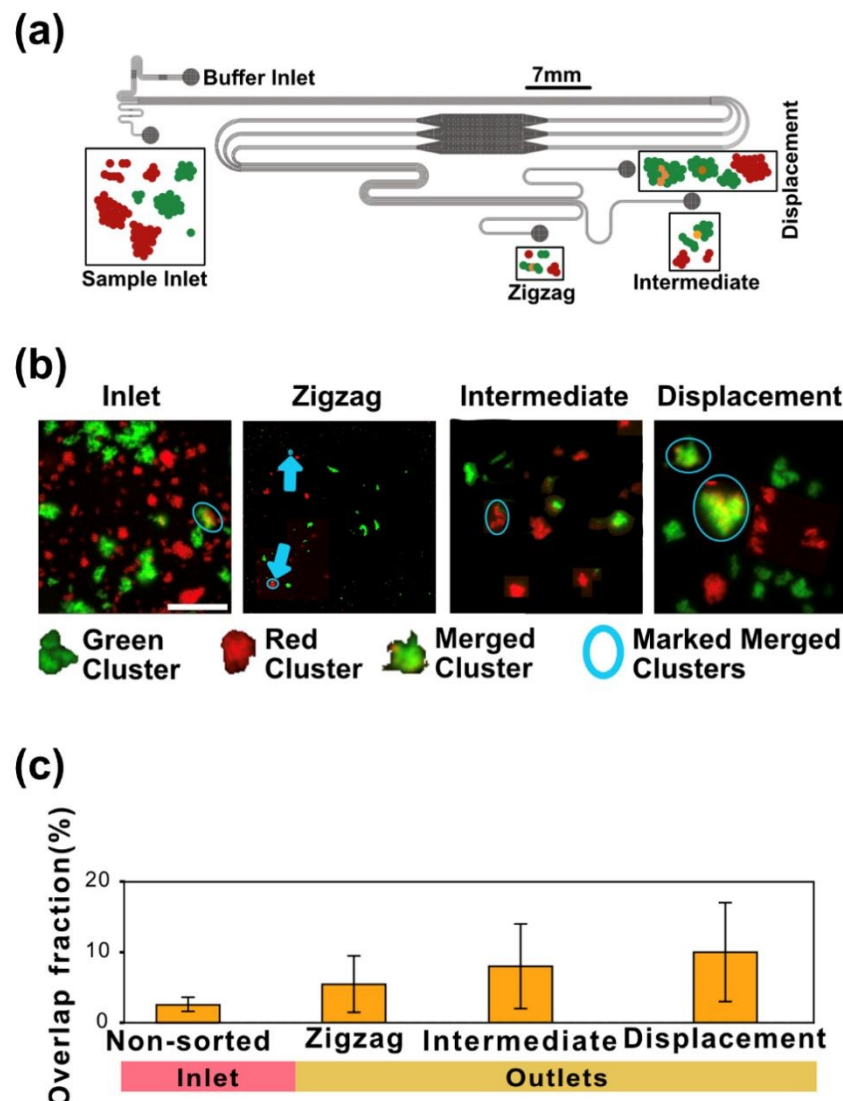


Figure 5. Two-colour experiments exploring the formation of clusters during sorting. a) A suspension containing a mixture of clusters stained with one of two distinct colours, WGA-640 (red clusters) and OG-488 (green clusters), is sorted in our device. Image analysis is used to measure the colour composition of clusters in the sorted fractions. b) Fluorescence micrographs (false colour) showing single and two-colour clusters in unsorted and sorted fractions. c) Bar charts show the ratio of two-colour GAS clusters to the total number of clusters and bacteria detected in the unsorted and sorted fractions. Scale bars 50µm.



3.3. Effect of GAS cluster size on immune cell behaviour

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To show that our device is generating two subpopulations with sufficient sample volume and purity for bioassays, we performed a cell motility study where we exposed neutrophils to each of the two sorted subpopulations of the bacterial clusters (singlets/doublets and clusters up to $\sim 10\mu\text{m}$ in one fraction, and clusters larger than $\sim 10\mu\text{m}$ in the other). The assay demonstrates that neutrophils are more mobile and exhibit faster migration speed when exposed to large bacterial clusters. However, the meandering index, which quantifies chemotactic signalling between immune cells and bacteria, does not show a significant difference suggesting that the size of clusters of GAS bacteria may not contribute to chemotactic signalling. This observation is also evident in the scatter plot, where, although distinct regions correspond to each sample, the difference is primarily reflected in the speed of neutrophil cells rather than their meandering index. While very preliminary, this proof-of-concept analysis shows that DLD-based separation could be helpful to start teasing apart the complex biology underlying host-bacteria interactions. See Figure 6.



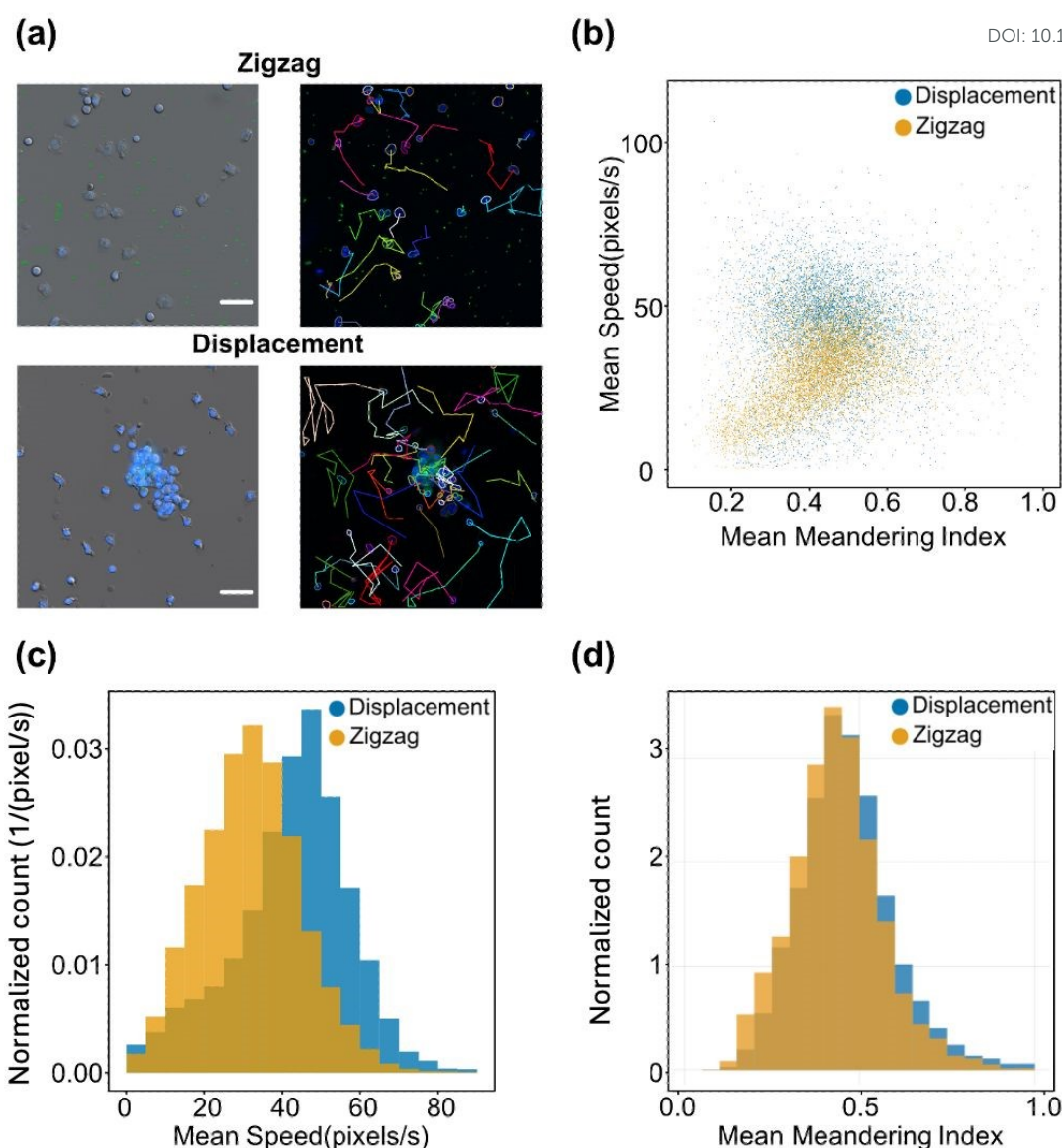


Figure 6. Results of neutrophil phagocytosis assay with two distinct subpopulations of GAS cluster sizes. a) Left panes: Neutrophils (blue) phagocytosing clusters of GAS bacteria (green). Right panes: Trajectories of neutrophils from tracking analysis. b) Scatter plot showing mean speed against meandering index for neutrophils exposed to the small (yellow) and large (blue) cluster fractions. c) Histograms of mean speed for the two experiments. d) Histograms of meandering index for the two experiments. Scale bars = 50 μm .

4. Conclusions

We have demonstrated that we can overcome the challenges of separating GAS bacteria suspensions that have very broad distributions in size and morphology using a simple DLD device with a single D_c . The large N allows us to handle a broad range of particle sizes without clogging and it minimizes deleterious effects of shear on the clusters. The device is narrow which minimizes the dilution of the sample. We demonstrate the usefulness of the intermediate outlet to remove particles with sizes close to D_c , thereby improving the purity of the zigzag and displacement output fractions. There is a minimal change of the cluster size distribution and the device generates



two populations of high purity. We were able collect sufficient sample for a proof of principle of downstream bioassays by testing the activity of neutrophils on collected fractions. To fully address the biological question, more extensive studies are needed. These may be based on pure size-based sorting or they may be complemented by including the effect of shape, deformability and other physical characteristics on the particle sorting using DLD, which, in turn, will pave the way for a refined separation of, not only GAS populations, but also a plethora of other types of complex and dynamic samples.

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