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## Microfluidic shape-based separation for cells and particles: recent progress and future perspective

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Shape-based separation of micro- and nanoparticles has emerged as a powerful yet underdeveloped strategy in microfluidics, offering distinct advantages over conventional size-based methods, particularly for biomedical and functional material applications. Unlike size-based separation, shape-based approaches enable discrimination between particles of identical volume but differing morphology, an essential capability for isolating pathological cells, engineered particles, or anisotropic biological entities whose function is inherently linked to shape. This review provides a comprehensive and critical overview of recent progress in both passive and active microfluidic platforms tailored for shape-selective separation. Passive systems such as deterministic lateral displacement, pinched flow fractionation, inertial, and viscoelastic microfluidics exploit hydrodynamic and flow-structure interactions, while active methods including dielectrophoresis, magnetophoresis, optophoresis, and acoustophoresis utilize external fields to modulate particle trajectories based on geometric anisotropy. For example, recent advancements demonstrate high purities often exceeding 95%, with throughput rates ranging from several microliters to milliliters per minute depending on the device configuration, achieving shape-based cell and particle sorting efficiencies above 90% under optimal conditions. For each technique, we highlight the underlying mechanisms enabling shape sensitivity, key technological advancements, and emerging trends in experimental and computational approaches. We also discuss the challenges in capturing complex particle behaviors such as rotation, alignment, and deformability and emphasize the need for integrated modeling, real-time control, and system-level optimization. Finally, we outline future directions and opportunities for advancing shape-based microfluidic separation toward scalable, high-precision applications in diagnostics, therapeutics, and materials science.

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## 1. Introduction

Recent advancements in microfluidic device design have transformed traditional biochemical lab protocols by miniaturizing complex processes into efficient, cost-effective microchannel networks.<sup>1</sup> These cutting-edge microdevices integrate micro- and nano-sized components, enabling precise particle manipulation and highly sensitive detection on a single, compact platform. By seamlessly combining physics, engineering, and biology, these devices have opened new frontiers in diagnostics, drug development, and personalized medicine. While different microfluidic devices serve overlapping

biomedical functions, their mechanisms of operation set them apart. Passive systems, for example, rely on inherent natural forces such as diffusion and inertia to facilitate particle mixing<sup>2,3</sup> and movement,<sup>2,4–7</sup> whereas active systems harness external energy sources such as electric, magnetic, or acoustic fields – to exert precise control over particle trapping<sup>8–15</sup> and sensing.<sup>16–19</sup> The synergy between these two approaches has led to groundbreaking advancements in lab-on-a-chip technology, making biomedical research more accessible, scalable, and efficient. As microfluidics continues to evolve, it holds immense promise for revolutionizing healthcare, offering faster diagnostics, enhanced drug screening, innovative therapeutic solutions and localized drug delivery tailored to individual patient needs.

Building on the advancements in microfluidic technology, one of its most transformative applications lies in cell sorting and separation, a fundamental process in biomedical research, clinical diagnostics and therapy. Cells, as the basic units of life, exist in complex, heterogeneous environments where multiple distinct cell types coexist and interact.<sup>20,21</sup>

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For instance, human blood is composed primarily of red blood cells (RBCs), white blood cells (WBCs), and platelets,<sup>22</sup> yet it can also contain rare cell types such as circulating tumor cells (CTCs)<sup>23</sup> and even bacteria,<sup>24</sup> making precise isolation crucial for disease detection and treatment. Microfluidic sorting techniques have shown significant clinical promise; for example, inertial microfluidic devices have achieved up to 95% purity for WBC isolation from diluted whole blood, enhancing sample quality for downstream analysis.<sup>25,26</sup> In cancer diagnostics, microfluidic systems for CTC sorting have demonstrated capture yields better than 90% and specificities above 97%, while maintaining cell viability, supporting their application in precision oncology.<sup>27,28</sup> Similarly, label-free dielectrophoretic sorting has effectively separated live/dead cells with approximately 90% purity and 85% recovery rates, minimizing cell damage.<sup>29</sup> Similarly, even unicellular organisms like *Saccharomyces cerevisiae* (*S. cerevisiae*)<sup>30</sup> can exhibit different phenotypes, with size variations corresponding to different cell cycle phases, further highlighting the importance of efficient cell separation techniques. Traditional separation methods, while effective, often rely on complex labeling procedures and may induce stress or damage to cells, limiting their applicability in sensitive experiments and therapeutic interventions. For example, centrifugation, which is often a mandatory step for sample preparation and bulk purification, subjects cells to high shear forces causing potential cell damage, particularly in the case of shear-sensitive cells.<sup>31</sup> Similarly, fluorescence-activated cell sorting (FACS) requires fluorescent labeling, expensive instrumentation, and expert knowledge.<sup>32</sup> Microfluidic cell sorting, however, offers an innovative alternative by leveraging intrinsic and extrinsic forces to enable precise, label-free separation, on the condition that the appropriate physical principle is selected depending on the particle's properties.<sup>33</sup> This approach not only enhances efficiency but also minimizes cell damage, reduces operational costs, and allows for high-throughput analysis.<sup>26</sup>

Expanding on the remarkable advancements in microfluidic cell sorting, shape-based separation is emerging as a powerful way for isolating particles and cells based solely on their morphology, offering unprecedented precision in biological, chemical, and industrial applications. In complex biological environments where multiple cell types of similar size/volume coexist, shape-based separation provides a critical tool for targeted isolation and analysis. Unlike conventional methods that rely on size or biochemical markers, shape-based separation exploits the distinct geometries of cells and particles to enable efficient and label-free sorting. Various pioneering studies have demonstrated potential across multiple domains, including particle confinement techniques for sorting RBCs,<sup>34</sup> inertial focusing of differently shaped particles,<sup>35</sup> capillary electrophoresis for nanoparticle separation,<sup>36</sup> acoustofluidic separation of prolate and spherical shapes for *Thalassiosira eccentrica*,<sup>37</sup> and the separation of micro-objects like sickle cells using magnetic fields.<sup>38</sup> Shape-based separation is essential not only for advancing disease diagnostics and personalized medicine, but also for revolutionizing material synthesis and transforming industrial manufacturing processes.<sup>39</sup> By integrating shape-based separation with microfluidic technologies, researchers are unlocking new possibilities in high-precision sorting, ensuring greater efficiency, scalability, and applicability across biomedical and engineering disciplines.<sup>34,40</sup>

In this paper, we aim to provide a comprehensive review of microfluidic shape-based separation, consolidating the wide array of existing methods, identifying their limitations, and exploring the latest advancements in the field through a physics-oriented perspective. By critically examining current research, we analyze how the intrinsic physical behaviors of non-spherical particles such as rotational motions (tumbling, kayaking, and log-rolling), hydrodynamic interactions, and lateral migration govern their trajectories within different microfluidic environments. Both passive techniques including deterministic lateral displacement (DLD), inertial microfluidics, viscoelastic flows, and pinched flow fractionation (PFF) and active methods such as acoustic, optical, electric, and magnetic actuation are discussed in terms of their ability to exploit these shape-dependent dynamics for effective separation. We seek to clarify the operational principles, advantages, and constraints of each technique, while highlighting innovations aimed at enhancing sorting precision and throughput. This review serves as an essential reference for advancing the use of shape-based separation in healthcare diagnostics, materials synthesis, and bioprocessing. Fig. 1 presents an overview of the various types of microfluidic platforms employed for shape-based separation of micro-organisms, illustrating the diversity of approaches guided by particle physics and microfluidic design.

This review is organized as follows. In section 2 we will discuss the dynamics of differently shaped bioparticles as it significantly differs from that of spherical particles. In section 3, platforms for passive (3.1) and active (3.2) separation will be presented in detail. Section 4 emphasizes



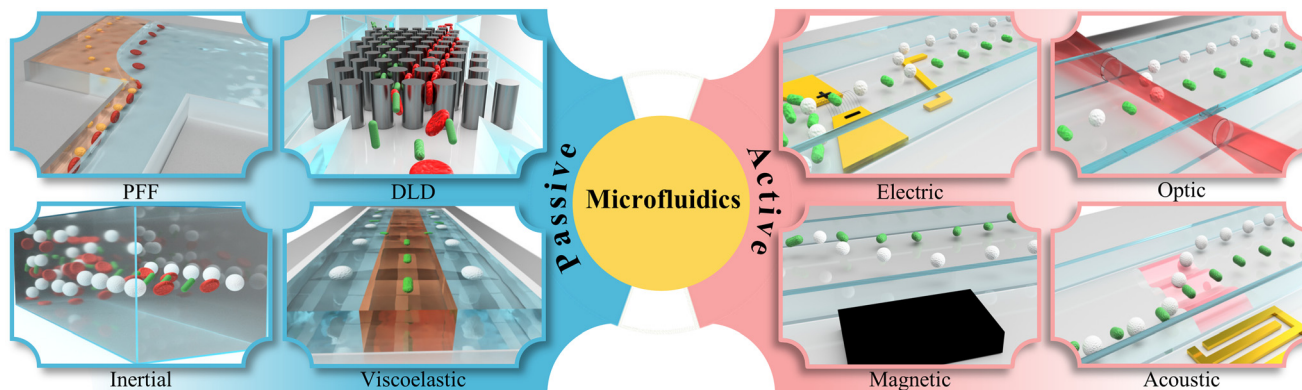
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*from fundamentals to biomedical applications. He is a board member of Acoustofluidics Society, Korean Society of Mechanical Engineers, Korean Society of Visualization, and Society of Micro and Nano Systems.*







**Fig. 1** Schematic overview of microfluidic shape-based separation techniques categorized into passive and active methods. Passive techniques such as deterministic lateral displacement (DLD), inertial, viscoelastic, and pinched flow fractionation (PFF) utilize channel geometries and intrinsic fluid forces, while active techniques based on electric, optical, magnetic, and acoustic fields apply external forces for enhanced and tunable particle manipulation.

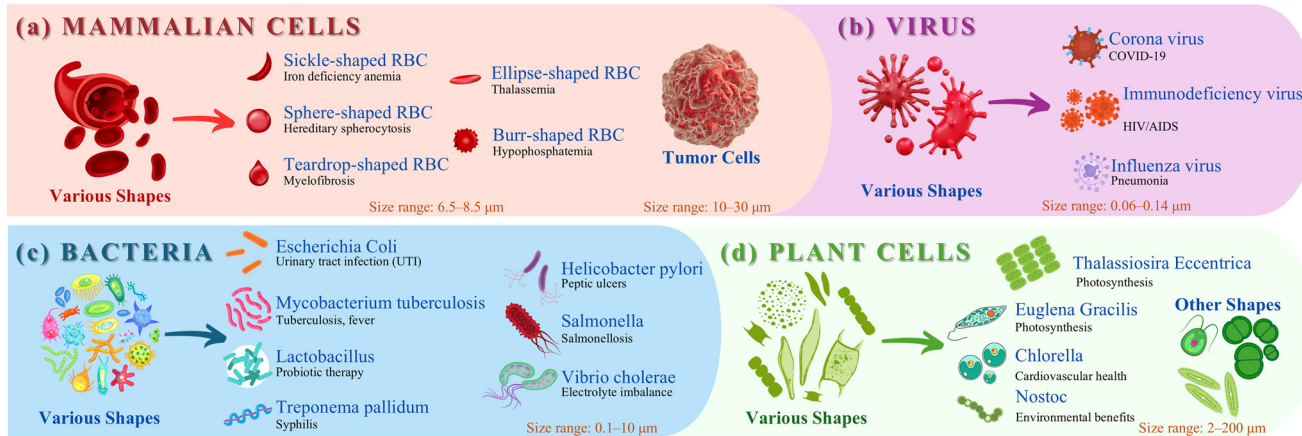
current challenges and future applications while all findings are summarized in the conclusion in section 5.

## 2. Dynamics of differently shaped bioparticles

### 2.1 Importance of shape-specific classification

Shape-specific analysis is crucial for shape-based separation in microfluidics, as the particle shape significantly influences how objects interact with relevant forces within microchannels. Unlike size-based separation, which relies on differences in volume or mass, shape-based separation exploits variations in rotational and translational motion under relevant forces. Theoretical models, such as Jeffery's equations for particle motion in shear flow and Saffman's theory for oblate particles in shear, help explain these shape-dependent dynamics. This distinction is particularly relevant for biological applications, where the cell morphology plays a critical role in function and disease identification.<sup>40–42</sup>

Fig. 2 presents various biological entities categorized as mammalian cells, viruses, bacteria, and plant cells, each exhibiting distinct shapes that critically influence their function and pathology. Mammalian cells, such as RBCs ranging from 6.5  $\mu\text{m}$  to 8.5  $\mu\text{m}$  in size, display morphological variations – normal biconcave disk shape,<sup>43</sup> sickle-shaped cells (as in sickle cell anemia, leading to vascular blockages and cardiovascular disease),<sup>44</sup> spherocytes (linked to hereditary spherocytosis),<sup>45,46</sup> and elliptocytes (seen in elliptocytosis) – with each shape affecting deformability, circulation, and disease progression (Fig. 2(a)). Viruses ranging from 0.06  $\mu\text{m}$  to 0.14  $\mu\text{m}$  in size, come in shapes like icosahedral (*e.g.*, adenovirus),<sup>47</sup> helical (*e.g.*, influenza),<sup>48</sup> and complex (*e.g.*, bacteriophages),<sup>49</sup> with the geometry impacting infectivity, immune evasion, and separation by size and drag (Fig. 2(b)). Bacteria ranging from 0.1  $\mu\text{m}$  to 10  $\mu\text{m}$  in size exhibit rod (bacillus),<sup>50</sup> spherical (coccus),<sup>51</sup> and spiral (spirillum) shapes,<sup>52</sup> which determine their mobility, adhesion, and resistance profiles, relevant in infection and treatment strategies (Fig. 2(c)). Plant cells ranging from 2  $\mu\text{m}$  to 200  $\mu\text{m}$  in size show diverse morphologies such as spherical,



**Fig. 2** Diverse shapes of biological particles including (a) cells, (b) viruses, (c) bacteria, and (d) microalgae. The figure has been particularly generated by <https://Biorender.com>.



filamentous, or star-shaped forms, with the shape influencing light absorption, nutrient uptake, and bioreactor dynamics (Fig. 2(d)).<sup>53</sup> Given the above information, shape-based separation is essential across these categories because biological function, pathology, and identity are often directly tied to their physical form. Cells deform and interact differently based on shape, viruses and bacteria may evade detection or clog systems without morphological sorting, and microalgae applications benefit from selective harvesting of specific species for example in process engineering. In microfluidics, extensive work has been done to exploit shape-dependent hydrodynamic behaviors (like tumbling, log-rolling, and margination) to develop precise, label-free separation techniques that are capable of handling heterogeneous biological mixtures for diagnostics, therapeutics, and environmental monitoring.

Although sperm cells exhibit a distinct head-tail morphology, most microfluidic sperm separation techniques rely not on shape, but on motility-driven mechanisms such as rheotaxis, chemotaxis, and boundary-following behavior. These approaches aim to isolate morphologically normal, motile sperm with high DNA integrity for assisted reproductive technologies (ARTs). Recent developments include rheotaxis-based channels and microstructured designs that mimic the female reproductive tract, enabling passive yet selective isolation of high-quality sperm. Readers interested in this topic are referred to several comprehensive reviews and recent advances in microfluidic sperm separation and selection techniques.<sup>54–58</sup>

Viruses also exhibit a rich diversity in geometric architectures, ranging from icosahedral and spherical to filamentous and rod-like morphologies, each influencing their hydrodynamic behavior during flow-based separation. The geometric resistance model provides a framework to understand how the virus geometry affects translational and rotational drag forces under flow, which directly impact migration trajectories and trapping

efficiency in microfluidic and filtration systems.<sup>59</sup> For instance, elongated or filamentous viruses such as Ebola or influenza exhibit higher hydrodynamic drag and orientation-dependent resistance compared to spherical viruses like adenovirus, leading to distinct flow-alignment behaviors and separation responses. These biomechanical characteristics can be harnessed to optimize shape-based sorting or filtration by tuning parameters such as the flow rate, channel dimensions, and pore geometry. While most microfluidic approaches to virus manipulation focus on size, charge, or affinity-based mechanisms, incorporating shape-dependent hydrodynamic resistance can further enhance selectivity and throughput. Understanding how the virus morphology contributes to motion resistance and flow alignment not only aids in refining microfluidic separation design but also supports the broader goal of developing geometry-sensitive diagnostic and purification platforms.<sup>60,61</sup>

## 2.2 Rotational behavior of non-spherical particles

Various particle geometries have been investigated in the context of flow dynamics. They can be classified into two main categories: ellipsoids and spheroids. Ellipsoidal particles are further classified as prolate or oblate, depending on their aspect ratio ( $\lambda$  = radial diameter/equatorial diameter). A prolate ellipsoid has  $\lambda > 1$ , indicating an elongated shape, while an oblate ellipsoid has  $\lambda < 1$ , indicating a flattened form. In 1922, Jeffery theoretically described how a rigid, isolated, neutrally buoyant ellipsoidal particle behaves in a simple shear flow within a Newtonian fluid.<sup>41</sup> He discovered that such a particle undergoes continuous rotation around the vorticity axis (perpendicular to the flow-gradient plane), tracing one of an infinite number of closed paths known as Jeffery orbits. These orbits are uniquely determined by the particle's initial orientation, aspect ratio, and the shear rate of the flow. Among

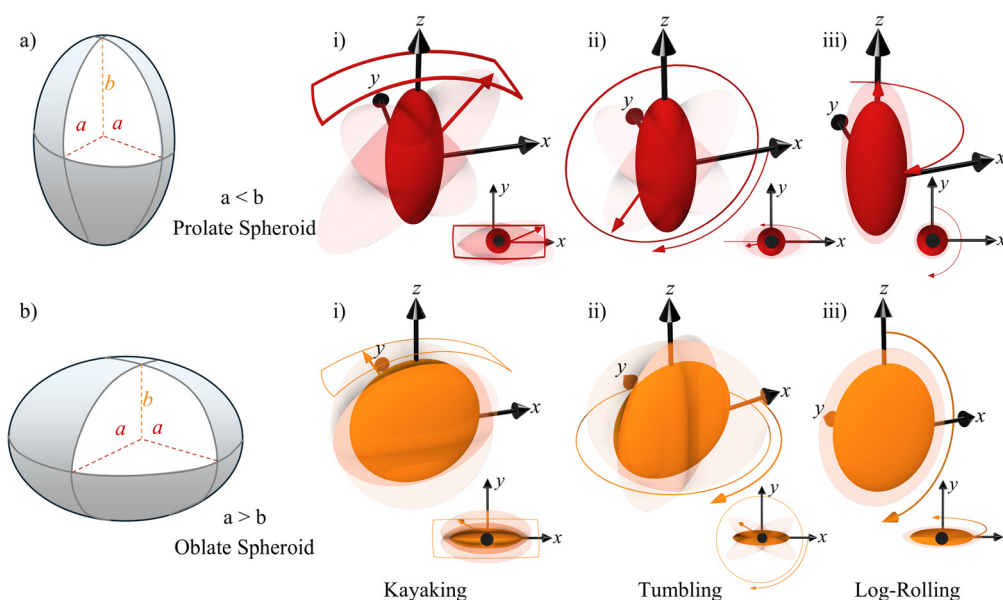


Fig. 3 Rotational motion of a) prolate and b) oblate spheroids in shear or laminar microfluidic flow: i) kayaking, ii) tumbling and iii) log-rolling motions.



the possible modes of rotation, Jeffery identified three characteristic behaviors: kayaking, where the particle's motion mimics a kayak paddle (Fig. 3ai and bi), tumbling, in which the particle's axis of revolution rotates within the flow-gradient plane (Fig. 3aii and bii), and log-rolling, where the particle spins around its symmetry axis aligned with the vorticity direction (Fig. 3aiii and biii). Importantly, Jeffery (1922) showed that the angular velocity of the particle is periodic, reaching its maximum when the particle is oriented perpendicular to the flow and its minimum when aligned with it. The rotation period  $T$ , which defines the time required to complete a full rotation, depends on both the shear rate  $\dot{\gamma}$  and the particle's aspect ratio  $\lambda$ , and is given by the expression:

$$T = (\lambda + 1/\lambda) \times 2\pi/\dot{\gamma}. \quad (1)$$

Shape-based separation of particles with differing morphologies focuses on the distinct behaviors that arise from the particle geometry under specific flow conditions, particularly emphasizing shape-induced forces like inertial lift to improve separation efficiency. As shown in Fig. 3, particles initially display a variety of rotational motions such as tumbling, kayaking, and log-rolling before the influence of external or internal forces becomes dominant. In this motion, particles rotate and orient themselves in the flow, with prolate particles continuing to exhibit this tumbling behavior as they interact with forces such as inertial lift. At a very small Reynolds number ( $Re \ll 1$ ), fluid inertia plays a role in the rotational dynamics of prolate particles. Due to the interplay of inertial lift and rotational motion, the particle gradually reorients itself within the flow-gradient plane, following the orbit with maximum energy dissipation.<sup>42</sup> This reorientation, described as kayaking, becomes more pronounced with increasing  $Re$ . Modified versions of Jeffery's model, incorporating inertial corrections, offer predictive insights into these preferred rotational states in weakly inertial regimes, where inertial effects are small but non-negligible compared to viscous forces.<sup>41</sup> For oblate particles, Saffman's theory provides an additional explanation of how inertia influences their motion; specifically, the inherent vorticity of the flow induces lift that causes their symmetry axis to align with the vorticity axis. This alignment minimizes the torque acting on the particle, eventually leading to a stable rotational motion known as log-rolling.<sup>42</sup> While Jeffery's equations lay the foundation for understanding such dynamics, Saffman's contributions are crucial for capturing the role of inertia, especially at moderate  $Re$ , where inertial effects become significant, influencing the transport and orientation of non-spherical particles in various fluid systems.<sup>41</sup> These motions, such as kayaking and log-rolling, facilitate shape-based separation by exploiting the shape-dependent dynamics induced by fluid inertia. However, spherical or symmetric particles are affected by these forces to a lesser extent, allowing for the effective separation of non-spherical particles from spherical ones in flow-based processes.

The aspect ratio of an ellipsoidal particle significantly influences its rotational dynamics in shear flow. In the absence

of fluid inertia, an increase in the aspect ratio leads to a longer rotation period, as described by eqn (1). This trend remains valid even when weak fluid inertia is present. Additionally, as the aspect ratio increases, the variation in the rotational rate increases; particles exhibit higher maximum angular velocities when oriented perpendicular to the flow and lower minimum velocities when aligned with it. The initial orientation of the particle also plays a critical role in determining its rotational trajectory. Jeffery's theory assumes that, without inertia, the initial orientation fully dictates the particle's orbit.<sup>41</sup> However, under inertial conditions, this dependency becomes more controversial. Some studies, such as those by Yu *et al.*,<sup>62</sup> suggest that the initial orientation continues to govern the trajectory at moderate shear Reynolds numbers ( $Re_s \approx 300$ ). The shear Reynolds number incorporates the shear rate and particle diameter as components, replacing the channel properties and flow velocity found in the conventional Reynolds number equation, wherein the rotation motion of the particles is induced by shear gradients present in the flow profile.<sup>63</sup> In contrast, others, including Huang *et al.*<sup>64</sup> and Rosén *et al.*,<sup>65</sup> report that this influence is only significant within certain  $Re$  ranges, indicating that the effect of initial orientation diminishes as inertial forces become dominant.

### 3. Microfluidic platforms for shape-based separation

Microfluidic devices are broadly categorized into passive and active systems, each with distinct operational principles and limitations. Passive devices rely on intrinsic hydrodynamic forces, diffusion, inertial effects, and secondary flows to manipulate particles, but their performance is heavily constrained by the channel geometry and flow conditions. Passive methods offer significant advantages, including simple design, low cost, ease of fabrication, and operation without external power sources or the need for control strategies, making them highly suitable for point-of-care and portable diagnostic applications. In contrast, active devices utilize external energy sources such as electric, magnetic, optical, and acoustic fields to achieve precise particle control. However, some external forces, like magnetic fields, are limited to act on specific particle properties, such as magnetically responsive materials. In particular, acoustic driven methods overcome many of these constraints, enabling broader applicability across diverse biomedical applications, including cell sorting, targeted drug delivery, and biofabrication. While recent reviews have addressed particle manipulation under external force fields<sup>66</sup> and design innovations in pinched flow fractionation,<sup>67</sup> a comprehensive perspective specifically centered on shape-based separation mechanisms across both passive and active microfluidic techniques is still lacking, underscoring the need for our review. This section explores recent advancements in shape-based particle separation and manipulation in microfluidics, highlighting the underlying physics and the development of both passive and active device technologies.







**Table 1** Comparative summary of key performance indicators for passive and active microfluidic platforms used in shape-based separation of cells and particles

PASSIVE						
Classification	Principle	Throughput	Cell type	Separation marker	Merits	Demerits
Deterministic lateral displacement <sup>34,80,81,85–87,89,90,91,93,94</sup>	Lateral displacement of cells by periodically arranged micropillars or other objects	0.1–10 $\mu\text{L min}^{-1}$ ( $\sim 10^3$ – $10^6$ cells per min)	<i>T. cyclops</i> from RBCs, RBC discocytes, echinocytes, stomatocytes, malaria RBCs, glutaraldehyde-treated RBCs, CTCs, skeletal stem cells, nonspherical micro-objects	Size, shape, motility, morphology, deformability, stiffness	Label-free, continuous, precise, high purity, robust	Pillar clogging, sensitivity to deformability, fabrication complexity
	Focusing of cells at the equilibrium position in the channel cross-section by hydrodynamic forces, e.g. shear-gradient induced lift force, wall-induced lift force, rotation-induced force	0.1–10 $\text{mL min}^{-1}$ ( $\sim 10^5$ – $10^7$ cells per min)	Cylindrical and disk-shaped particles, sphere and ellipsoid particles, yeast cells, non-spherical capsules, chromosomes from cell debris, RBCs and WBCs, erythrocytes and leukocytes from diluted blood sample, <i>Euglena gracilis</i>	Size, shape, stiffness	Label-free, continuous, very high throughput, robust, simple design	Needs rather high Re, shape/stiffness interplay, channel optimization needed, scalability
	Viscoelastic microfluidics <sup>30,110–118</sup>	Varying focus time of cells to equilibrium positions by inertial lift forces and elastic forces	1.7–500 $\mu\text{L min}^{-1}$	<i>E. coli</i> from RBCs, MCF-7 cancer cells from WBCs, rigid RBCs from softer RBCs, WBCs from blood, platelets from blood, sphere <i>E. coli</i> for rod-like <i>E. coli</i> , <i>C. anabaena</i> cells (5–1000 $\mu\text{m}$ )	Size, shape, stiffness, deformability	Label-free, continuous, low to high Re, simple design, handling of irregular shaped samples
Pinched flow fractionation <sup>119–121</sup>	Separation of cells by hydrodynamic forces utilizing the position and rotation in a sudden expansion of the microchannel	$\sim 0.06$ – $60 \mu\text{L min}^{-1}$	Spherical from peanut-shaped, spherical and disc-shaped from blood components (RBC and platelets), clustered disc-shaped particles, ovoid and filamentous <i>E. coli</i>	Size, shape, deformability	Label-free, continuous, low shear stress, simple design	Limited throughput, sensitive to cell orientation, concentration, scalability
ACTIVE						
Electrophoresis <sup>32,131–134</sup>	Migration of cells through a medium under the influence of an electric field	0.1–100 $\mu\text{L min}^{-1}$	Polymer-coated spherical, rod, triangular gold and silver nanoparticles, long nanorods, nanoplates, nanoclusters, nonspherical polyelectrolyte, prolute polystyrene spheroids	Size, shape, electric charge, relative permittivity, conductivity	Label-free, scalable, integrable, applicable to many cell types	Joule heating, medium constraints, fouling, sensitive to cell orientation, semi-continuous if used as in a filter
Optophoresis <sup>145,146</sup>	Migration of cells by mechanical, thermal, or electrical driving forces induced by optical energy	Single cell to small ensembles ( $<1 \mu\text{L min}^{-1}$ )	Oblate ellipsoidal particles with various aspect ratios, oblate elastic capsule	Size, shape, refractive index, surface properties, elastic properties	Label-free, high spatial precision, low mechanical stress, dynamic control, integrable	Limited scalability, low throughput, heating, photothermal damage, complex optics
Magnetophoresis <sup>38,155–159</sup>	Migration of cells by magnetic forces, particularly in the presence of a magnetic field gradient and/or gradient in the magnetization of the surrounding medium	0.1–80 $\mu\text{L min}^{-1}$	Spherical particles, peanut-shaped particles, ellipsoidal particles, drug-treated yeast cells of different shapes	Size, shape, magnetic susceptibility, morphology	Scalable, gentle, integrable, contactless, highly controllable, continuous	Magnetic labels often required, ferrofluid complexity, cell clustering, fouling
Acoustophoresis <sup>37,162,172,173,176,177</sup>	Migration of cells by acoustic forces utilizing surface acoustic waves or bulk acoustic waves	0.1–125 $\mu\text{L min}^{-1}$	Prolate spheroids, polystyrene microspheres, polystyrene prolute particles, polystyrene peanut-shaped particles, <i>T. eccentrica</i> microalgae, RBCs, CTCs	Size, shape, acoustic contrast factor	Label-free, biocompatible, orientation control, scalable, integrable, continuous	Heating at high power, acoustic streaming can complicate trapping, sensitive to cell orientation, medium throughput

To facilitate an overall comparison of the major microfluidic strategies employed for shape-based separation, Table 1 summarizes the key performance indicators across both passive and active platforms. The table lists the primary governing forces, throughput range, target cell or particle type, and separation marker, as well as reported efficiency, purity, and recovery data, together with each technique's main merits and limitations. This comparative overview highlights recent technological improvements and establishes a foundation for the detailed analysis presented in the following subsections.

### 3.1 Passive microfluidic techniques

Passive microfluidic devices play a crucial role in various applications, including fluid mixing, particle focusing, separation, sorting, and isolation, by leveraging intrinsic hydrodynamic forces and carefully designed channel geometries. Although their reliance on geometric constraints can limit flexibility and adaptability, continuous innovations in microchannel design, surface modifications, and biomimetic architectures have significantly expanded their capabilities.<sup>68</sup> One notable advancement is the development of organ-on-a-chip systems, which integrate passive microfluidic principles to mimic physiological microenvironments, enabling more precise control over cellular behavior for biomedical applications like drug testing and disease modeling.<sup>69</sup> Additionally, shape-based separation techniques exploit the particle geometry to efficiently sort or isolate, enhancing the performance of passive devices in fields like personalized medicine and high-throughput screening.

In microcirculatory blood flow and microfluidic channels, RBCs exhibit a well-known margination phenomenon, a hydrodynamic segregation effect driven by differences in cell deformability, size, and shape. Due to their high deformability and biconcave geometry, RBCs tend to migrate away from the channel walls toward the central streamlines, while stiffer or less deformable particles such as leukocytes, platelets, or synthetic microspheres are displaced toward the periphery. This spatial redistribution occurs as a result of lift forces generated by hydrodynamic interactions between deformable cells and the channel walls, as well as shear-induced diffusion in dense suspensions. The margination behavior of RBCs plays an important role in physiological blood flow and can be exploited in microfluidic systems for passive cell separation and enrichment. For instance, by tuning the flow rate, channel geometry, and hematocrit, microfluidic designs can leverage this natural segregation to isolate stiffer cells (*e.g.*, leukocytes or circulating tumor cells) or synthetic particles from whole blood without requiring external fields or labeling. Such margination-assisted separation relies on the interplay between inertial migration, cell deformability, and hydrodynamic lift, providing a simple, label-free mechanism that complements size- and shape-based sorting strategies.<sup>70</sup>

Several studies have analyzed this phenomenon both experimentally and computationally to understand the role of

deformability and flow conditions in determining migration trajectories. For example, Kumar and Graham<sup>71</sup> demonstrated that deformability contrast is the key determinant of margination in confined flows, while Fedosov *et al.*<sup>72</sup> used numerical simulations to quantify the balance between inertial and viscous forces influencing RBC distribution. These insights have contributed to the development of microfluidic designs that exploit RBC margination to improve separation efficiency in blood-on-a-chip and diagnostic platforms.

**3.1.1 Deterministic lateral displacement.** Deterministic lateral displacement (DLD) microfluidic platforms, first introduced by Huang *et al.*,<sup>73</sup> offer a novel approach for continuous particle separation under laminar flow at low Re. These devices feature periodic arrays of micropillars or other obstacles, with the pillars arranged either in a square or in a rhombic arrangement, where each row is slightly offset from the previous one. This separates partial streams often called flow streamlines in the microchannel, causing particles larger than a critical diameter ( $D_c$ ) to be laterally displaced and follow the bump mode, while smaller particles follow a zigzag trajectory, hence, enabling size-based separation.<sup>74,75</sup> The  $D_c$  can be estimated using the following experimentally determined formula:<sup>76–79</sup>

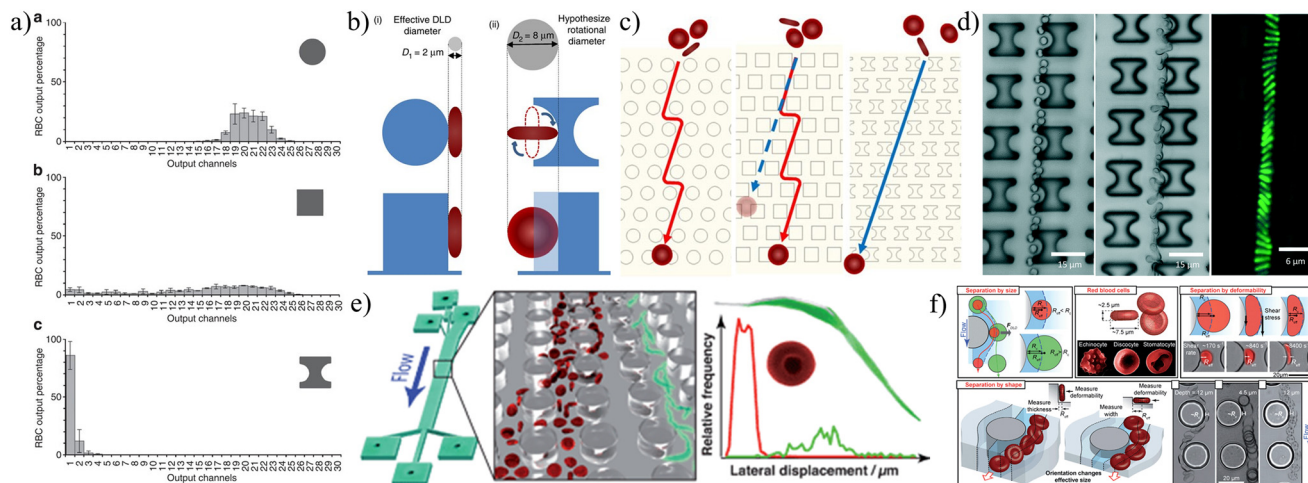
$$D_c = 1.4G\varepsilon^{0.48} \quad (2)$$

where  $G$  is the gap between adjacent pillars and  $\varepsilon$  is the row shift fraction, defined as  $\varepsilon = \tan \theta$ , with  $\theta$  representing the pillar array's tilt angle. In addition to size, particle properties such as shape,<sup>80</sup> deformability,<sup>81</sup> and density<sup>82</sup> can also influence separation. In a recent numerical study, Reinecke *et al.* (2023)<sup>83</sup> introduced corrections to eqn (2) to account for Re up to 60 and particle density. While DLD pillars are often circular, they may also adopt alternative cross-sectional geometries. For instance, shapes such as I, L, diamond, triangular, and asymmetric pillars have been employed to tailor local flow fields, promote differential particle rotation or alignment, and enhance separation based on shape, deformability, or orientation.<sup>84</sup>

Zeming *et al.*<sup>85</sup> introduced advanced pillar geometries to enhance size-based separation of non-spherical micro-objects. Their experiments showed that I-shaped pillars outperform conventional square or circular designs in separating RBCs due to their ability to induce rotation in non-spherical particles (Fig. 4a). As illustrated in Fig. 4b, I-shaped pillars feature two protrusions that initiate rotation in disc-shaped cells and a semicircular groove that accommodates this motion. This rotation shifts the basis of separation from a particle's narrowest width to its maximum rotational diameter, effectively mimicking a spherical profile, directing RBCs an oblique path to the left outlet (Fig. 4c). As a result, the design improves the separation of diverse bioparticles by accounting for their shape and orientation, not just size. Further, Ranjan *et al.*<sup>80</sup> investigated into other asymmetric pillar shapes such as anvil, T-, I- and L-shaped revealing that specific features like protrusions and grooves







**Fig. 4** Particle focusing in DLD: pillar shapes and non-spherical particle focusing: (a) comparing RBC separation efficiency using round, square, and I-shaped pillars. Reproduced from Zeming *et al.*, with permission from Nature, copyright 2013.<sup>85</sup> (b) Observing how particle rotation differs with round vs. I-shaped pillars. Reproduced from Zeming *et al.*, with permission from Nature, copyright 2013.<sup>85</sup> (c) Visualizing RBC trajectories through various pillar geometries. Reproduced from Zeming *et al.*, with permission from Nature, copyright 2013.<sup>85</sup> (d) Tracking movement of RBCs and beads in I- and L-shaped pillar arrays. Reproduced from Ranjan *et al.* with permission from RSC, copyright 2014.<sup>80</sup> (e) Isolating parasites from human blood. Reproduced from Holm *et al.* with permission from RSC, copyright 2011.<sup>87</sup> (f) Sorting based on size, shape, and deformability. Reproduced from Beech *et al.* with permission from RSC, copyright 2012.<sup>34</sup>

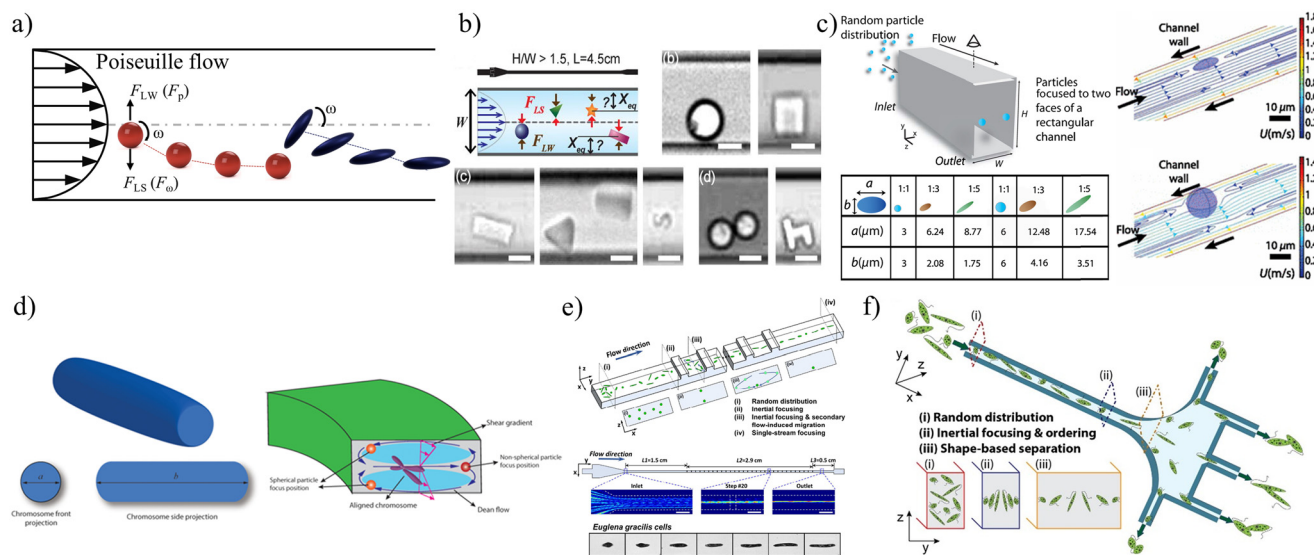
can either induce or restrict particle rotation, thereby influencing orientation and separation behavior. While I-shaped pillars effectively separated both spherical and non-spherical particles, in addition, the L-shaped ones were found to have significant effectiveness in separating the different-shaped particles (Fig. 4d). For comparison, the separation index ( $I_s$ ) used for general comparison between the efficiency and separation quality between the pillar shapes showed that I-shaped and L-shaped pillars have the highest value among the other pillar shapes (I-shaped  $I_s = 95.3$  and L-shaped  $I_s = 92.3$ ). High  $I_s$  indicates their effectiveness. These findings underscore the potential of specially designed pillars for targeted separation of diverse cell types, including spherical particles, blood cells, and rod-shaped bacteria, with experimental results confirming the superior performance of I-shaped pillars over round and square configurations in DLD systems.<sup>86</sup>

Holm *et al.*<sup>87</sup> utilized DLD to separate parasites from RBCs by exploiting their distinct physical characteristics. RBCs, being biconcave and highly deformable, align with the flow streamlines and follow a zigzag trajectory through the DLD array. In contrast, *T. cyclops* parasites are typically larger, more rigid, and often elongated with tapered bodies and a single flagellum, interacting differently with the flow field and pillar geometry. An important factor influencing this behavior is the channel height. In shallow microchannels, RBCs are confined and tend to align flat (horizontally), which enhances their ability to deform and follow streamlines. However, elongated parasites may not orient as easily due to their shape and stiffness, and thus experience more frequent interactions with the pillars, leading to displacement. Therefore, the height of the channel plays a key role by controlling the orientation and deformation of the cells,

further improving the efficiency of separating parasites from deformable RBCs (Fig. 4e). The purified fraction of the parasites achieved 99.5%. As outlined above, besides size and shape, cell deformability plays a critical role in DLD-based separation, particularly for biological particles like RBCs. Unlike rigid spheres, deformable cells undergo shape changes under flow shear, reducing their effective size and making their critical diameter unpredictable by standard DLD models (Fig. 4f).<sup>34</sup> Parameters such as the flow rate (Re number), fluid viscosity, and capillary number significantly influence this behavior.<sup>88–90</sup> For instance, diseases like malaria increase stiffness of RBCs, making them deform less and thus more likely to be laterally displaced in the array. Krüger *et al.*<sup>91</sup> demonstrated *via* simulations that stiffer RBCs show greater displacement, while experiments using glutaraldehyde-treated RBCs confirmed that increased stiffness leads to higher migration angles. Sharp-edged pillar designs such as triangular and diamond shapes further enhance deformability-based separation.<sup>92</sup> This strategy has also proven effective in isolating circulating tumor cells and stem cells, with studies showing improved separation efficiency and purity under optimized flow conditions and using multi-stage DLD designs.<sup>93,94</sup>

**3.1.2 Inertial microfluidics.** Inertial microfluidics has emerged as a powerful tool for shape-based separation in microfluidic systems, leveraging fluid dynamics at Re numbers typically ranging from  $\sim 1$  to  $\sim 100$  to achieve high-throughput focusing of particles based on size, shape, and deformability.<sup>95</sup> This technique exploits the balance between shear-gradient-induced lift forces  $F_{LS}$  pushing particles toward channel walls and wall-induced lift forces  $F_{LW}$  directing them toward the center (Fig. 5a). The interplay of these forces causes particles to migrate across streamlines to





**Fig. 5** Manipulation of non-spherical particles in inertial microfluidic channels: (a) a schematic representation of particle focusing of different shapes within a Poiseuille flow profile. (b) Focusing behavior of ellipsoidal particles with varying aspect ratios. Reproduced from Hur *et al.*, with permission from AIP, copyright 2011.<sup>100</sup> (c) Various shaped microparticles aligning within a straight microchannel. Reproduced from Masaeli *et al.*, with permission from APS, copyright 2012.<sup>103</sup> (d) Demonstration of chromosome front and side projection areas, illustrating their alignment behavior under inertial and Dean flow in microfluidic channels. Reproduced from Feng *et al.*, with permission from AIP, copyright 2020.<sup>105</sup> (e) Ellipsoidal *Euglena gracilis* cells with different aspect ratios focused in a stepped microchannel. Reproduced from Li *et al.* with permission from RSC, copyright 2016.<sup>107</sup> (f) Shape-based separation of *E. gracilis* driven by lateral inertial focusing, where equilibrium positions depend on the particle shape and aspect ratio. Reproduced from Li *et al.* with permission from Nature, copyright 2017.<sup>108</sup>

specific equilibrium positions, depending on the shape of the channel cross-section and the actual particle blockage ratio ( $\beta = a/D_h$ , where  $a$  is the particle diameter and  $D_h$  is the hydraulic diameter). A small blockage ratio  $\beta \ll 0.07$  indicates a weak inertial lift force, and the particle is unable to focus at the channel center as the slip-shear effects reduce. In curved microchannels, secondary flows, such as Dean vortices, introduce an additional drag, further modifying the equilibrium positions.<sup>96</sup> An alternative explanation considers the interplay between particle rotation-induced force  $F_{\Omega}$  and pressure-induced force  $F_p$  from the surrounding fluid, which together govern particle migration.<sup>97</sup> In circular channels, particles focus along the Segré-Silberberg annulus, while in square and rectangular channels, they migrate to four or two stable positions, respectively, due to the net force of  $F_{LW}$  and  $F_{LS}$ , and can be governed by the inertial lift force  $F_{IL}$ :<sup>98</sup>

$$F_{IL} = C_{il}\rho U^2 d^4/D_h^2 \quad (3)$$

where  $C_{il}$ ,  $\rho$ ,  $U$ , and  $D_h$  are the inertial lift coefficient, fluid density, velocity maximum, and channel hydraulic diameter, respectively. The inertial lift force is proportional to the particle diameter, implying that particles of varying sizes occupy different stable positions.

For non-spherical particles, rotational dynamics add complexity to inertial focusing. Their migration depends on the rotation perpendicular to the wall given by the expression:<sup>99</sup>

$$F_{\Omega} = (1/8)\pi d^3 \rho \Omega V \quad (4)$$

where  $V$  and  $d$  are the relative velocity and particle diameter. Eqn (4) is limited to spherical particles. In this case, there is less dominance in migrating the particle away from the wall and thus it is neglected in many analyses. Further expansion of  $F_{\Omega}$  is required to elucidate the non-spherical rotation-induced lift force for better understanding of migration of non-spherical particles. Studies such as Hur *et al.*<sup>100</sup> have classified the rotation of cylindrical and disk-shaped particles as “tumbling” and “log-rolling”, respectively, regardless of their aspect ratios or cross-sectional shapes. They also introduced the concept of a rotational diameter  $D_{max}$  to explain lateral equilibrium positions  $X_{eq}$  for non-spherical particles. Their findings suggest that particles with greater  $D_{max}$  – typically those with higher aspect ratios – tend to focus closer to the channel centerline, except for highly asymmetric “h-shape” particles which behave differently (Fig. 5b). Su’s group further refined this understanding by introducing the axial length  $D_A$  for cylindrical particles and defining an equivalent diameter, being the diameter of a spherical particle sharing the same equilibrium position. Their simulations showed that this equivalent diameter shifts from being comparable to  $D_A$  at lower Re numbers (Re = 50) towards  $D_R$  as Re increases (e.g. Re = 200 in square microchannels). This Re-dependent shift highlights the influence of rotational dynamics which becomes more significant at higher flow rates.<sup>101</sup> Reinecke *et al.*<sup>83</sup> also confirmed in a numerical/experimental study that the equilibrium position depends on the size and Reynolds number in a square wave serpentine channel. They also reported a density dependent position with higher Re



numbers ( $>100$ ). Later they extended their study to non-spherical particles and studied the equilibrium positions for oblates and rod shaped particles.<sup>102</sup> At lower Reynolds numbers, the particles tend to position on trajectories similar to those of spherical particles of the same volume. The equilibrium streaks are in general close to the center of the channel for particles of greater aspect ratio, which is in line with the above mentioned findings. One surprising conclusion was that particles can be shifted to the equilibrium position with and without strong rotation (which depends on their size and aspect ratio). Masaeli *et al.*<sup>103</sup> showed that increasing inertial forces cause prolate particles to converge from random, out-of-plane rotational modes into a stable, in-plane tumbling motion aligned with the vorticity axis. Besides, no rotation occurs when the prolate particle is aligned with the streamline. Particles with similar volumes but a higher aspect ratio experience slower rotational speeds (in line with Jeffery's orbit), which leads to closer migration toward the center, resulting from a dominant time-averaged lift away from the walls during their characteristic tumbling rotation (see Fig. 5c). Additionally, geometric confinement plays a role, when elongated particles align perpendicular to the wall, they are pushed away, further attenuating their rotation and enhancing central focusing due to higher pressure at the wall edge, inducing particle rotation. It is important to note that rotation is crucial for prolate-type particles as it is the primary factor of the particle dynamics. The non-rotating particles are aligned to the streamlines and pushed back to the wall area by the shear gradients and thus lose the ability to focus within the flow. The numerical simulation suggest that the equilibrium position  $X_{eq}$  of a rotating prolate particle is similar to that of a sphere whose diameter corresponds to the prolate's major axis. This happens by the tumbling motion and a substantially increased wall-effect lift when the prolate's major axis orients perpendicular to the wall. Moreover, Unverfehrt *et al.*<sup>104</sup> observed two key rotational behaviors in non-spherical capsules in shear flow: a tumbling mode at low shear rates, characterized by periodic  $\pm 90^\circ$  angular oscillations, and a swinging mode at higher shear rates, where the inclination oscillates around a fixed positive angle. In deformable capsules, this kayaking is often paired with tank-treading, driven by membrane elasticity and shape memory effects as also known from RBCs. These insights emphasize that both geometric and dynamic properties such as the shape, aspect ratio, rotation mode, and deformability crucially affect inertial focusing behavior in microfluidic systems.

Feng *et al.*<sup>105</sup> investigated chromosome separation based on size and shape in a low aspect ratio spiral channel and found that chromosomes have two equilibrium modes: aligned and focused. The aligned fibers stay at the center of the channel due to hydrodynamic interactions. Further downstream, the aligned particle is pushed and focused to the outer wall as it experiences the Dean forces to the outer wall and circulating Dean vortices at the near top and bottom edges, while the smaller particle is focused on the inner wall due to inertial lift force dominance (Fig. 5d). Spiral channel

designs improved continuous separation of blood cells by enhancing the influence of inertial lift and Dean flows but still faced limitations in distinguishing overlapping shape/size distributions.<sup>25</sup> To address these challenges, sheath-free separation in viscoelastic fluids introduced elasticity-driven focusing. This improved non-spherical particle sorting without requiring external sheath flow, although it was constrained by fluid viscosity effects.<sup>106</sup> Stepped microchannel configurations addressed some of these challenges by coupling inertial focusing with secondary cross-sectional flows.<sup>107</sup> Initially, ellipsoidal particles are focused on two positions in a low-aspect-ratio segment; the subsequent stepped section induces a transverse flow that merges these into a single equilibrium position.<sup>107</sup> This design not only facilitates precise focusing of asymmetrical biological cells, such as *Euglena gracilis* used by Li *et al.*,<sup>108</sup> but also simplifies 3D focusing in complex geometries (Fig. 5e).

Recent studies have extended inertial microfluidics to new frontiers, including subcellular bioparticles like chromosomes and paired-particle systems. These have revealed the profound influence of shape, softness, density, and inter-particle spacing on migration behavior, adding layers of complexity to separation processes. For example, while inertial sorting of *Euglena gracilis* achieved better control over asymmetric particles, it struggled with deformable cell types (Fig. 5f).<sup>108</sup> Paired-particle studies further revealed how particle-particle interactions, governed by shape and deformability, significantly affect focusing accuracy.<sup>109</sup> Altogether, these findings reinforce the need to carefully tailor the microchannel geometry, flow conditions, and fluid rheology to optimize shape-based separation performance. Future advancements will likely be possible on integrative designs that accommodate rotational dynamics, secondary flows, and elastic deformation to address the evolving demands of biomedical and analytical applications.

**3.1.3 Viscoelastic microfluidics.** Advancements in shape-based separation in microfluidics have been propelled by the incorporation of viscoelastic microfluidics, a technique that utilizes inertial lift force  $F_{IL}$ , consisting of  $F_{LW}$  and  $F_{LS}$ , and elastic forces  $F_{EL}$  to manipulate particle behavior.  $F_{EL}$  arises due to the first normal stress difference  $\nabla N_1$  as a product of polymer contribution to the fluids, expressed as<sup>110</sup>

$$F_{EL} = C_{el} d^3 \nabla N_1 \quad (5)$$

where  $C_{el}$  is an elastic lift force coefficient. The  $\nabla N_1$  depends on the polymeric contribution  $\mu_p$ , it can be seen from the correlation with the solution viscosity as  $\nabla N_1 = 2\mu_p \lambda \dot{\gamma}^2$  ( $\lambda$  and  $\dot{\gamma}$  are the relaxation time and average fluid shear rate, respectively). In a rectangular channel,  $F_{EL}$  focuses the particles to 5 low shear gradients at low Reynolds number ( $Re \ll 1$ ) in the center and corner channel cross-section. The combined effect of  $F_{IL}$  and  $F_{EL}$  at moderate to high Reynolds numbers ( $Re \gg 1$ ) distinguished corner effects, generating a single focused particle position at the channel center,

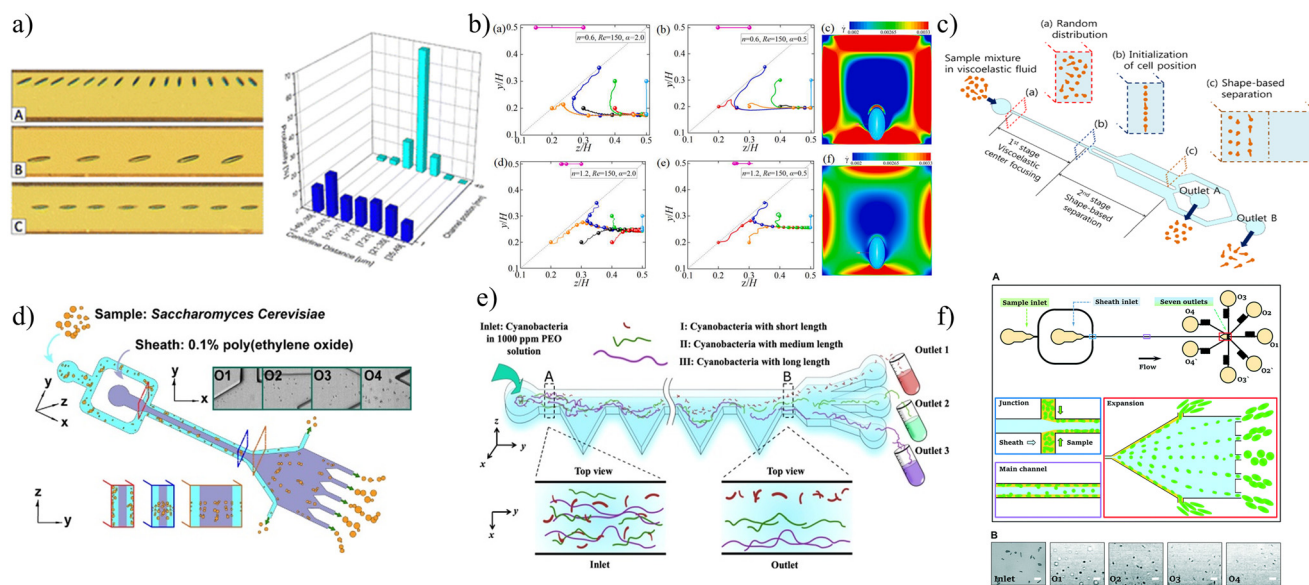




enhancing the lateral distance between a large range of particle sizes, and increasing the overall output.<sup>111</sup> By harnessing the characteristic properties of viscoelastic fluids, such as fluid elasticity and potentially shear-thinning behavior, this method enables particle differentiation based on shape, size, and deformability, without the need for external sheath flow. Similar to the inertial microfluidics, the flow rate determines the lateral distribution of the non-spherical particles. However, a study by Langella *et al.*<sup>112</sup> showed that an optimal flow rate is required to reduce the shear-thinning effect, which arises from the nature of the viscoelastic fluid. The non-spherical particles have a different lateral focusing mechanism, leaving a significant difference on particle focusing time to reach a stable position within the flow (Fig. 6a). Tai and Narsimhan<sup>113</sup> implied in their work that a spherical particle migrates faster than a non-spherical particle. Non-spherical particles undergo rotation with a period of  $T$ , which generates a lift from the wall region, whereas spherical particles do not show this rotation. These findings suggest that a longer channel length is required for the non-spherical particle to be able to focus at the channel center optimally. Non-spherical particles are able to focus in the center of the channel, and do not show a clear particle orientation there due to weak shear gradients. These findings are supported by numerical simulation using the power-law model by Hu *et al.*<sup>114</sup> They suggest that a spherical particle with an aspect ratio of one (this case is a sphere)

travels faster to the channel center than an oblate one, followed by prolate particles in a shear-thinning fluid. The longest migration time occurs for prolate particles due to oscillatory migration due to rotation-induced lift force and becomes obvious as the aspect ratio increases (Fig. 6b).

Sheathless separation of different-shaped *Candida albicans* cells demonstrated the potential of viscoelastic fluids to sort elongated and spherical cells, but faced limitations in handling irregularly shaped microorganisms (Fig. 6c).<sup>115</sup> Improved shaped-based separation and enrichment of *Saccharomyces cerevisiae* were achieved by optimizing viscoelastic effects using a co-flow configuration, utilizing the competing force of inertial and elastic lift force between two fluids at the fluid interface, able to achieve 81.2% and 90% purity of singlets and clusters. Further enhancements for the separation output can be made by optimizing the viscoelastic properties and channel geometries (Fig. 6d).<sup>30</sup> Expanding the approach to filamentous microorganisms, sheathless separation of *Anabaena* enabled the sorting of cyanobacteria based on chain-like structures, though variations in filament length impacted sorting precision (Fig. 6e).<sup>116</sup> This work concludes that an appropriate flow rate is required to enhance the separation performance of *Anabaena*. Moreover, as suggested before,<sup>30</sup> the channel length plays a crucial role in enhancing the migration of *Anabaena* of different aspect ratios. Shape-based separation of drug-treated *Escherichia coli* demonstrated how co-flow inertial and viscoelastic



**Fig. 6** Manipulation of non-spherical particles in viscoelastic microfluidic channels: (a) typical image sequences showing a spheroid undergoing tumbling motion, aligning with the flow, and captured by superimposing successive frames. Reproduced from Langella *et al.* with permission from RSC, copyright 2023.<sup>112</sup> (b) Trajectories of prolate and oblate spheroids and the final rate-of-strain tensor in the (YOZ plane) cross-section of a square channel for shear-thinning, with the dotted line representing the channel diagonal. Reproduced from Hu *et al.* with permission from Elsevier, copyright 2023.<sup>114</sup> (c) Schematic of sheathless shape-based separation of *Candida* cells in a viscoelastic microfluidics. Reproduced from Nam *et al.* with permission from MDPI, copyright 2019.<sup>115</sup> (d) Schematic of viscoelastic microfluidic sorting of *S. cerevisiae* based on shape-dependent lateral migration. Reproduced from Liu *et al.* with permission from ACS, copyright 2021.<sup>30</sup> (e) Schematic top-view representation of length-based separation of cyanobacterial cells in a viscoelastic microchannel. Reproduced from Yuan *et al.* with permission from ACS, copyright 2021.<sup>116</sup> (f) Design of a viscoelastic microfluidic device for shape-based separation of drug-treated *E. coli*. Reproduced from Zhang *et al.* with permission from RSC, copyright 2022.<sup>117</sup>

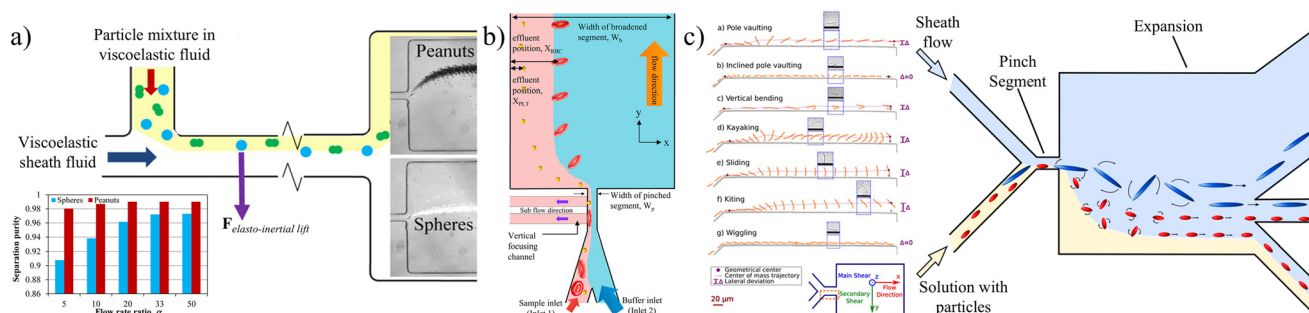


microfluidics could be applied to distinguish bacteria undergoing morphological changes, though its performance was sensitive to the flow rate and bacterial density.<sup>117</sup> Finally, bacteria separation and enrichment using viscoelastic flows in a straight microchannel further optimized the technique for high-throughput applications. However, its dependence on the fluid's properties introduced challenges in achieving consistent reproducibility across varying experimental conditions.<sup>118</sup> This shows the difference in physical phenomena acting on the spherical and non-spherical particles, in which, by manipulating their equilibrium position, the separation between the two different particle shapes can be achieved. A parameter that needs to be emphasized for the separation operations is rotation for non-spherical particles. If the flow conditions cannot meet a rotation criterion, negative isolation occurs, and the targeted particle cannot migrate in the lateral direction. This statement is supported by the findings of Zhang *et al.*,<sup>117</sup> where non-treated drug *E. coli*, which had a rod shape, cannot migrate from the channel wall due to flow conditions that prevent rotation of the prolate particles (Fig. 6f). Despite this, the integration of viscoelastic flows has shown significant promise in large-scale applications, yet further refinement is needed to mitigate the challenges and improve reliability. Advancements may focus on optimizing fluid compositions, designing microchannels for dynamic shape variations, enabling more efficient and reproducible shape-based separation.

**3.1.4 Pinched flow fractionation.** Pinched flow fractionation (PFF) is a versatile technique traditionally used for size-based separation. It has undergone significant advancements enabling its application in shape-based particle separation. Fundamentally, PFF operates by squeezing the sample flow between a sheath flow and a channel wall in a narrow pinched segment, followed by a sudden downstream expansion generating hydrodynamic forces causing particles to align based on size and shape. Due to the different position orientation for larger particles,

they detach from the original streamline in an expansion region to the channel center, and thus particle separation can occur. As the field evolved, researchers have revealed that this seemingly simple approach can exploit not only the particle size but also subtle differences in shape, rotation, and mechanical properties. For instance, Lu *et al.*<sup>119</sup> demonstrated that the elasto-inertial lift forces acting in viscoelastic fluids can induce shape-dependent migration patterns between spherical and peanut-shaped particles. The non-spherical “peanut” particles exhibit asymmetric rotational behaviors both in-plane and out-of-plane as described in the previous section, leading to lateral displacements distinct from those of spherical particles. This rotational dynamic is influenced by key parameters like the fluid's elasticity, the channel's aspect ratio, and the particle morphology. The study further highlighted that shear-thinning effects and transitions in equilibrium positions at different Re also affect separation, with optimal performance at  $Re \approx 1$  (Fig. 7a). These findings laid critical groundwork in linking particle rotation to lateral migration, thereby expanding PFF's relevance beyond conventional size separation.

Building on such insights, Nho *et al.*<sup>120</sup> advanced the PFF design by introducing structural modifications. They used tilted sidewalls and vertical focusing channels, termed t-PFF-v. These modifications significantly improved the alignment and separation efficiency of non-spherical particles. The t-PFF-v device successfully separated disc-shaped RBCs from spherical platelets by exploiting differences in particle orientation and interaction with the side wall. Time-lapse imaging revealed that both spherical platelets and disc-shaped RBCs are aligned along the lower corner of the pinched segment flow due to vertical focusing. Thereby, the RBCs likely adopt an orientation prescribed by the angle of the tilted sidewall. This shape-dependent positioning within the pinched segment leads to distinct lateral displacement compared to spherical platelets, enabling separation (Fig. 7b). This refinement illustrates how



**Fig. 7** (a) Schematic of the shape-based particle separation mechanism using elasto-inertial pinched flow fractionation (eiPFF). In a viscoelastic fluid, flow-induced elasto-inertial lift forces enhance the lateral displacement of sheath-focused spherical and peanut-shaped particles, enabling high-purity separation. Reproduced from Lu *et al.* with permission from ACS, copyright 2015.<sup>119</sup> (b) Demonstration of red blood cell (RBC) separation from platelets. Reproduced from Nho *et al.* with permission from Elsevier, copyright 2017.<sup>120</sup> (c) Depiction of tumbling behavior of two elongated, axisymmetric particles with differing aspect ratios within a PFF channel. Reproduced from de Timary *et al.* with permission from RSC, copyright 2023.<sup>121</sup>



the control of rotational dynamics through geometric design can improve the resolution in shape-based separation. However, the device still faces challenges with flow-induced particle overlapping at higher concentrations, which can reduce separation accuracy. Nevertheless, this study emphasized how structural design and flow manipulation can be harnessed to optimize the orientation and rotational states of particles for shape-specific separation.

Fundamentally, PFF leverages the hydrodynamic forces generated by a narrowed flow path often resulting in a parabolic velocity profile to induce lateral migration based on shape, size, and deformability. Elongated or flexible particles respond differently to these forces compared to compact, rigid ones, enabling their spatial separation. De Timary *et al.*<sup>121</sup> investigated the behavior of filamentous (prolate) and ovoid (spherical) *E. coli* cells in a low aspect ratio PFF device for varying flow rates. At low  $Re = 0.25$ , the initial particle distribution distance to the wall determines whether it will migrate away from the wall or not. The interaction between the filamentous cells, wall, and high-shear region near the wall induced pole vaulting, inclined pole vaulting, vertical bending, kayaking, sliding, kiting, and wiggling rotational behaviors, shifting their geometric centers toward the channel centerline, effectively increasing their separation distance and enabling their separation from ovoid cells, which remained near the walls due to either minimal rotation or no rotation. As flow rates increased, the rotational modes were suppressed by stronger shear forces, aligning cells vertically and reducing lateral migration, which in turn compromised separation resolution (Fig. 7c). These results highlight how the interplay between the flow-induced rotation and particle geometry governs separation efficiency in PFF. When combined with optimized flow conditions and tailored channel geometries, PFF proves to be a powerful platform for isolating complex cell populations based on intrinsic physical properties, though challenges remain in separating highly similar or dynamically deformable particles.

### 3.2 Active microfluidic techniques

Active microfluidic devices utilize external forces such as acoustic, electric, magnetic, and optical forces to precisely manipulate fluid flow, droplets, or particles for a wide range of applications. In comparison with passive methods, they allow adjusting control parameters so that the separation can be fine-tuned to different tasks. The effectiveness of these techniques depends on the properties of the sample and the nature of the external field. Acoustic-based transducers generate longitudinal pressure waves within the fluid that influence particles in a large range of material compositions, making them highly versatile. In contrast, electric and magnetic fields selectively act on particles with specific electrical conductivity, permittivity, or magnetic susceptibility, limiting their application to compatible materials. Optical methods offer additional control, particularly for biological and temperature-sensitive samples because of

their refractive index contrast, and optical force tuning. These active microfluidic systems are typically classified based on the type of energy applied, with the choice of transducer carefully matched to the electrical, magnetic, acoustic, or optical characteristics of the target particles. As advancements continue, active microfluidics plays an increasingly vital role in areas such as biomedical diagnostics, cell sorting, and high-precision material processing, offering greater flexibility, scalability, and efficiency compared to passive methods.

**3.2.1 Electrophoresis.** Electrophoresis is a physicochemical technique used to separate and analyze charged particles based on their differential migration through a medium under the influence of an applied electric field.<sup>122</sup> This phenomenon, first observed in the early 19th century, was initially studied as a basic electrokinetic effect, where particles suspended in a fluid would migrate depending on their net charge and the strength of the applied field.<sup>123</sup> The method gained practical significance with the development of gel electrophoresis, which introduced porous gels such as agarose as separation media. These gels act as physical and entropic barriers that enhance the resolution of separation by hindering the migration of larger molecules more than smaller ones. The adaptability of gel properties to suit specific biomolecular sizes and charges significantly expanded the capabilities of electrophoretic separation.<sup>124</sup>

Since the advent of gel electrophoresis, a variety of advanced techniques have emerged to improve particle separation, including capillary electrophoresis,<sup>125</sup> microfluidic arrays,<sup>126</sup> and nanopore-based platforms.<sup>127</sup> When a charged particle or macromolecule is suspended in an electrolyte solution, it attracts counter-ions to its surface, forming a structured region called the electric double layer. This consists of a tightly bound inner layer of ions, known as the Stern layer, and a more diffuse outer region of mobile ions (diffuse layer). The characteristic thickness of this double layer is described by the Debye length. Upon application of an external electric field, the particle and its associated Stern layer are pulled in the direction of the field, while the mobile ions in the diffuse layer experience a force in the opposite direction. The net motion of the particle, or its electrophoretic mobility, depends critically on the ratio between the Debye length and the particle radius  $a$ . When the Debye length is relatively large, the electric and viscous forces acting on the particle are effectively decoupled and reach a balance. Under these conditions, the particle's electrophoretic mobility  $\mu$  can be approximated by the ratio of its net charge  $Q$  to the hydrodynamic drag it experiences.<sup>128</sup>

$$\mu = Q/6\pi\eta a \quad (6)$$

When the Debye length is much smaller than the particle size, fluid shear is restricted to a thin layer adjacent to the particle surface approximately the thickness of the Debye layer. In this regime, the particle's electrophoretic mobility becomes independent of its size and shape.<sup>129</sup>





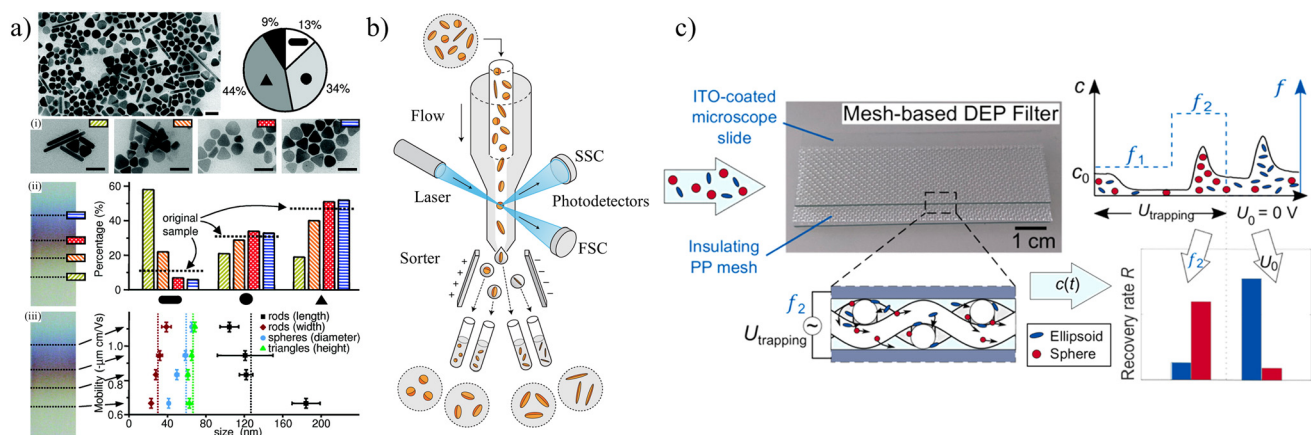
$$\mu = \frac{\varepsilon_b \varepsilon_0 \zeta}{\eta} \quad (7)$$

In this context,  $\varepsilon_b$  represents the dielectric constant of the medium (dimensionless),  $\varepsilon_0$  is the vacuum permittivity (dimensionless), and  $\zeta$  denotes the zeta potential (mV), which corresponds to the electrokinetic potential at the outer boundary of the electric double layer.<sup>130</sup> The distinction between eqn (6) and (7) highlights that the particle shape becomes relevant in electrophoretic separation primarily when the Debye layer is relatively thick, or when particles interact with microstructures in gels or other separation media. Despite this, the vast majority of electrophoresis applications to date have focused on size-based separation, while shape-based electrophoretic separation remains largely underexplored, both in experimental practice and theoretical modeling.

Hanauer *et al.*<sup>131</sup> demonstrated that gel electrophoresis can be used to separate gold and silver nanoparticles based on both shape and size. By coating the nanoparticles with polyethylene glycol to impart surface charge, they enabled electrophoretic mobility through the gel. The analysis of different gel regions revealed distinct shape distributions: the initial mixture consisted of 13% rods, 34% spheres, 44% triangles, and 9% others (Fig. 8a). Rod-shaped particles exhibited the slowest mobility and became enriched to 60% in the first gel region, while triangular particles showed the fastest migration, and spheres appeared across both moderate and fast regions (Fig. 8a(i and ii)). Further analysis in Fig. 8a(iii) indicated that longer rods migrated more slowly, and larger spheres tended to move faster, though no clear trend was found for triangles, possibly due to thickness variations undetectable by TEM. A separate experiment with a 35 : 65 mixture of spheres and rods confirmed the effectiveness of gel electrophoresis in achieving shape-based separation. Xu *et al.*<sup>132</sup> similarly demonstrated

shape- and size-based separation of gold nanoparticles using gel electrophoresis with 100 nm pores, showing that nanospheres migrated fastest, nanorods slowest, and triangular plates exhibited intermediate mobility, consistent with Hanauer *et al.*'s findings. Later, Hsu *et al.*<sup>133</sup> investigated how different parameters influence the electrophoretic behavior of non-spherical polyelectrolyte particles with equal volume but varying aspect ratios.

In 2018, Mage *et al.*<sup>32</sup> presented a label-free, high-throughput strategy for separating microparticles based purely on shape using a standard fluorescence-activated cell sorting (FACS) instrument as shown in Fig. 8b. Based on elastic scattering, they developed a four-dimensional gating strategy that analyzes four independent light scattering signals to generate unique "scattering signatures" for individual and non-fluorescently labeled particles. This approach enables classification and separation of microparticles ranging from spheres to ellipsoids and discs, and spanning sizes from 0.5 to 20  $\mu\text{m}$ , while eliminating errors caused by random particle orientation. The method achieves high purity and throughput ( $\sim 10^7$  particles per hour) and is compatible with diverse materials without requiring labels or complex sample preparation. In 2022, Weirauch *et al.*<sup>134</sup> presented an improved dielectrophoresis (DEP)-based separation method that uses a mesh material as an insulating structure between two indium tin oxide-coated electrodes (Fig. 8c). This mesh-based DEP filter enables enhanced selectivity by creating a structured porous environment that better distinguishes particles based on shape. The small electrode gap (0.6–0.8 mm) allows for effective electric field generation at relatively low voltages. Unlike traditional DEP setups using sponges or packed beds, the mesh structure provides more precise control over particle trapping and remobilization. Separation in this system occurs through DEP-induced trapping: when an alternating electric field is applied, particles experience dielectrophoretic forces that either attract



**Fig. 8** a) Gel electrophoresis enabled shape- and size-dependent separation of gold and silver nanoparticles, as evidenced by TEM images and particle distribution analysis across different gel regions. Reproduced from Hanauer *et al.* with permission from ACS, copyright 2007.<sup>131</sup> b) In the FACS-based procedure, particles are analyzed by laser-induced scattered light detected at forward and side angles, then encapsulated into droplets and sorted based on defined scattering intensity gates. Reproduced from Mage *et al.* with permission from Nature, copyright 2019.<sup>32</sup> c) Mesh-based DEP filter using a porous insulating mesh between ITO electrodes to enhance trapping selectivity at low voltages with a mixed shaped sample for shape-based separation. Reproduced from Weirauch *et al.* with permission from Elsevier, copyright 2022.<sup>134</sup>



them to high-field regions (positive DEP) or repel them (negative DEP), depending on their dielectric properties and geometry. The mesh structure amplifies these effects by generating localized field gradients, allowing particles with different shapes to interact differently with the field and become selectively trapped. Once separated, particles can be remobilized by adjusting field or flow conditions, enabling efficient, high-throughput shape-based sorting without the need for complex sample preparation.

For a prolate ellipsoidal particle with volume  $V = \frac{4}{3}\pi a_1 a_2^2$ , the DEP force along axes  $i$  is

$$\vec{F}_{\text{DEP,pr}} = 2\pi a_1 a_2^2 \epsilon_m \text{Re}(\text{CM}_i) \nabla(\vec{E}_{\text{RMS}})^2 \quad (8)$$

In this expression,  $a_1 \geq a_2 = a_3$  represents the semi-axes of the ellipsoid, with  $a_1$  as the major axis and  $a_2$  as the minor axis. The term  $\nabla(\vec{E}_{\text{RMS}})$  is the gradient of the squared electric field ( $\vec{E}_{\text{RMS}}$  in  $V_{\text{RMS}} \text{ m}^{-1}$ ), and  $\epsilon_m$  is the dielectric constant of the surrounding medium of the particle. The effective polarizability of the particle is captured by the real part of the Clausius–Mossotti factor  $\text{Re}(\text{CM}_i)$ , which is axis-specific and depends on the complex permittivities of the particles  $\tilde{\epsilon}_p$  and the medium  $\tilde{\epsilon}_m$ , as well as the depolarization factor  $L_{a_i}$ .<sup>135,136</sup>

$$\text{Re}(\text{CM}_i) = \text{Re} \left( \frac{\tilde{\epsilon}_{p,a_i} - \tilde{\epsilon}_m}{3(\tilde{\epsilon}_m + (\tilde{\epsilon}_{p,a_i} - \tilde{\epsilon}_m)L_{a_i})} \right) \quad (9)$$

In addition to traditional active separation methods, recent progress in microfluidic-based imaging cytometers has enabled real-time detection and classification of cells based on the morphology. These systems integrate optical or electrical imaging with microfluidic sorting modules to achieve label-free analysis and high-throughput classification of cells with distinct shapes or structures. By coupling deep learning or machine learning algorithms with high-speed imaging, cells can be automatically identified and sorted according to their morphological or biophysical characteristics. Such integrated systems provide a powerful extension to conventional dielectrophoretic or optical separation methods by introducing an intelligent detection layer capable of learning from imaging data and adapting sorting criteria dynamically. Readers interested in these developments can refer to several recent studies that highlight deep-learning-enabled cytometry and real-time morphological classification in microfluidic systems.<sup>137–141</sup>

**3.2.2 Optophoresis.** Optophoresis is an emerging light-driven technique that enables precise, non-contact manipulation and separation of microparticles and biological cells within microfluidic environments. It works by using optical energy to produce mechanical, thermal, or electrical driving forces acting on particles suspended in a fluid medium. Depending on the underlying mechanism, optophoresis can manifest as photophoresis (driven by light-induced thermal gradients), optoelectronic tweezers (OET) using light-patterned electric fields, or photoelectrophoresis in semiconducting fluids.<sup>142</sup> These approaches leverage particle-specific properties such as size, refractive index, surface charge, absorption, or thermal conductivity to enable selective, label-free sorting.

Particularly attractive for handling fragile biological samples, optophoresis offers high spatial resolution and low mechanical stress, making it suitable for applications such as cell sorting, particle patterning, and diagnostics in lab-on-a-chip systems.<sup>143</sup>

In a ray optics model, an incoming light ray is characterized by its direction of propagation and associated momentum. When the ray encounters a surface, momentum is transferred to that surface through reflection and refraction interactions. The resulting optical force can be described as the rate at which momentum is transferred from the photons to the surface, that is the momentum imparted per unit time.

$$F_o = \frac{\Delta p}{\Delta t} \quad (10)$$

The momentum transfer, denoted as  $\Delta p$ , is given by the expression  $\Delta p = n_m Q/c (I \cdot \Delta A) \Delta t$ , where  $n_m$  is the refractive index of the surrounding medium,  $c$  is the speed of light in a vacuum,  $Q$  is a dimensionless factor representing the efficiency of momentum transfer, and  $I$  is the intensity of the Gaussian beam. For this study, let us consider a loosely focused laser beam, allowing the incident ray to be modeled as propagating solely in the  $y$ -direction (Fig. 9a). The beam intensity  $I$  varies with both the  $y$ -position and radial distance and is computed accordingly.

$$I = \frac{2P}{\pi \omega(y)^2} \exp \left[ -\frac{2d_f^2}{\omega(y)^2} \right] \quad (11)$$

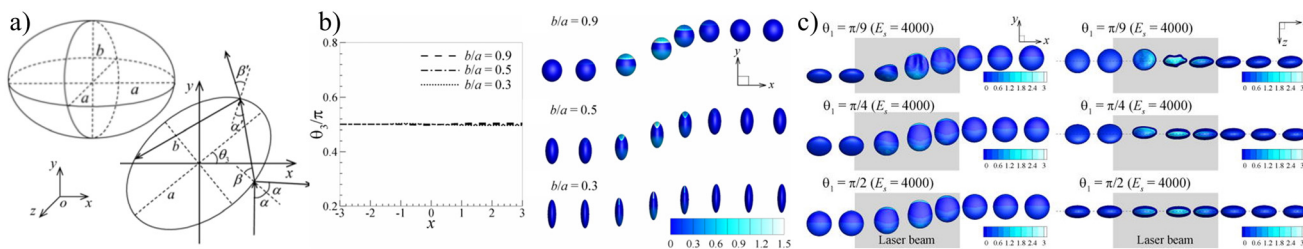
Here,  $P$  represents the power of the laser beam, and  $d_f$  is the radial distance from the focal point to the nodal position. The beam waist radius, denoted by  $\omega$ , defines the width of the laser beam at its narrowest point and is given by the following expression:

$$\omega(y) = \omega_0 \left[ 1 + \left( \frac{\lambda y}{\pi \omega_0^2} \right)^2 \right]^{\frac{1}{2}} \quad (12)$$

In this context,  $\omega_0$  denotes the minimum beam waist, while  $\lambda$  is its wavelength. The calculation of momentum transfer, which is central to determine the optical force, is closely related to the Poynting vector. The Poynting vector represents the energy flux density, the amount of energy transmitted per unit area per unit time in the direction of beam propagation. Consequently, the time-averaged Poynting vector corresponds to the laser beam's intensity.<sup>144</sup>

Despite the versatility of optophoresis, its potential for shape-based particle separation remains largely unexplored. Most existing studies focus on size, refractive index, or surface properties, with very limited attention to particle shape as a key separation parameter. Notably, there is a lack of experimental demonstrations validating shape-selective optophoretic manipulation. Early investigations, such as those by Chang *et al.*,<sup>145</sup> showed that shape influences optical trapping efficiency, as elongated particles experience different optical forces compared to spherical ones (Fig. 9b). However, this method was limited to well-defined ellipsoidal particles and struggled with biological samples that exhibit irregular morphologies. With this, Chang *et al.*<sup>146</sup> introduced a more advanced optical trapping configuration, allowing the





**Fig. 9** a) An oblate spheroidal particle with major and minor semi-axes  $a$  and  $b$ , respectively, and the trajectory of an incident ray interacting with the particle at an inclination angle  $\theta_3$  in the  $x$ - $y$  plane (rotated about the  $z$ -axis). Reproduced from Chang *et al.* with permission from AIP, copyright 2014.<sup>145</sup> b) Inclination angle evolution of an ellipsoidal particle with initial  $\theta_3 = \pi/2$  along the streamwise direction, along with instantaneous positions and surface optical force distributions near the laser beam axis for aspect ratios:  $b/a = 0.9, 0.5$ , and  $0.3$ . Reproduced from Chang *et al.* with permission from AIP, copyright 2014.<sup>145</sup> c) Instantaneous shapes and optical force distributions of an oblate capsule with varying inclination angle  $\theta_1$  and  $E_s$  (surface Young's modulus) = 4000 near the laser beam axis: side views and top views, respectively, with the dotted line marking  $z = 0$ . Reproduced from Chang *et al.* with permission from AIP, copyright 2015.<sup>146</sup>

selective separation of soft, shape-dependent capsules under uniform flow (Fig. 9c). While this improved the handling of deformable particles, it still faced challenges in efficiently separating highly complex or heterogeneous shapes. Both of these studies relied on optical radiation pressure and gradient forces, where particle shape affects light scattering and absorption, leading to distinct migration behaviors. Despite these advances, optical shape-based separation remains largely unexplored compared to acoustic, inertial, or viscoelastic methods, mainly due to limitations in scalability and throughput. Improvements could focus on integrating tunable optical landscapes to provide more precise control over particle manipulation, as well as combining optical forces with fluidic mechanisms for enhanced separation efficiency. By addressing these challenges, optical shape-based separation has the potential to expand its application across a wider range of biological and synthetic particles, offering a non-invasive and highly versatile sorting method.

**3.2.3 Magnetophoresis.** Magnetophoresis refers to the migration of particles under the influence of a magnetic field, particularly in the presence of a magnetic field gradient, a gradient in the magnetization of the surrounding medium, or a combination of both.<sup>147</sup> The primary goal of magnetophoretic manipulation is to efficiently control and separate a large number of particles within a short period of time. A key advantage of this technique is that it does not alter the properties of the sample solution such as pH, ion concentration, surface charge, or temperature, and thus is non-invasive, contactless, and highly controllable.<sup>148</sup> An essential factor influencing magnetophoresis is the difference in magnetic susceptibility between the particles and their surrounding medium. In magnetic separation, the underlying mechanism is governed by the magnetic force and torque exerted on the particles, which dictate their motion and alignment within the fluidic environment. These interactions can be quantitatively described as follows:<sup>147</sup>

$$F_m = (m \cdot B) = \frac{\Delta\chi \cdot V_p}{\mu_0} (\nabla B) \cdot B \quad (13)$$

$$T_m = m \times B \quad (14)$$

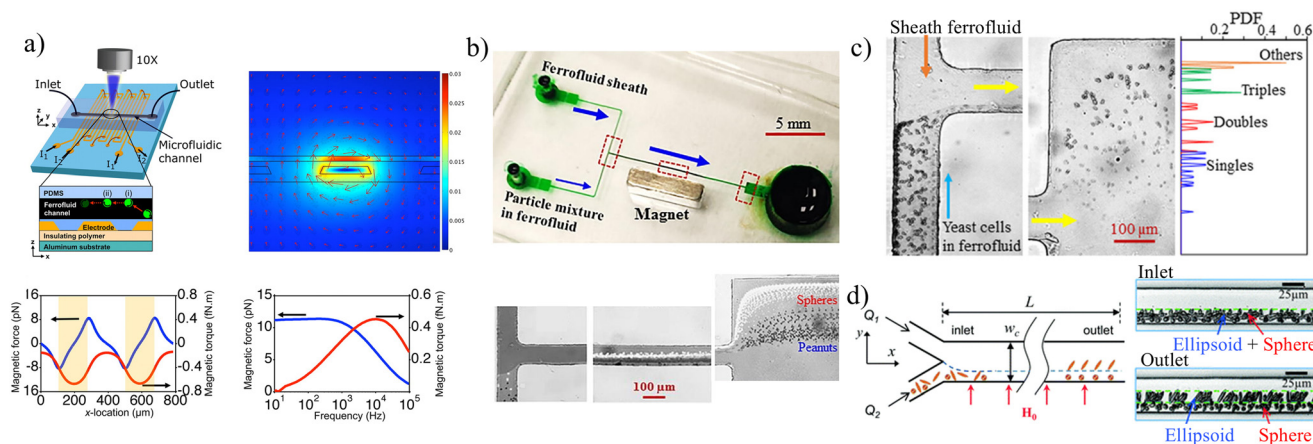
Here,  $\mu_0 = 4\pi \times 10^{-7}$  N/A is the magnetic permeability of vacuum,  $V_p$  represents the particle volume ( $\text{m}^3$ ),  $\nabla B$  is the gradient of the magnetic flux density  $B$  (T),  $m$  is the magnetic moment of the particle ( $\text{Am}^2$ ), and  $\Delta\chi$  is the difference in magnetic susceptibility between the particle ( $\chi_p$ ) and the surrounding fluid ( $\chi_f$ ), both dimensionless. To drive separation, both static and time-varying magnetic fields can be employed to generate the necessary magnetic forces and torques acting on the particles.

In conventional magnetic separation, non-uniform magnetic fields generate magnetic forces that drive particle movement, a process referred to as magnetophoresis. When  $\Delta\chi > 0$ , particles are attracted toward the magnetic field source, this is known as positive magnetophoresis. Conversely, when  $\Delta\chi < 0$ , particles are repelled from the magnetic field source, referred to as negative magnetophoresis. Typically, positive magnetophoresis is used to manipulate paramagnetic or ferromagnetic particles, or magnetically labeled cells, in a diamagnetic medium like water.<sup>149–151</sup> In contrast, negative magnetophoresis is employed to separate diamagnetic particles or cells within a magnetized medium such as ferrofluids.<sup>152–154</sup> Most studies have focused on size-based separation,<sup>147</sup> where particles experience different forces based on size (eqn (7)). Shape-based separation in microchannels using magnetic fields is more recent and achieved mainly by (1) shape-dependent forces in non-uniform magnetic fields or (2) shape-dependent torques in uniform fields without net magnetic force.

Kose *et al.*<sup>38</sup> demonstrated separation of sickle cells from healthy red blood cells using a periodic, non-uniform magnetic field in a ferrofluid-filled microchannel. Electrodes beneath the channel generated time-varying magnetic forces and torques, pushing cells upward by negative magnetophoresis as shown in Fig. 10a. Once at the top, cell rotation caused linear movement along the channel. Key factors like excitation frequency, current amplitude, and electrode position influenced cell velocity. Above a critical frequency dependent on cell size, shape, and elasticity, magnetic torque-driven translation overcame magnetic forces, enabling selective trapping of sickle cells at 300 Hz, while







**Fig. 10** a) The ferromicrofluidic device uses phase-shifted sinusoidal currents through patterned electrodes to generate traveling magnetic fields that levitate and propel nonmagnetic particles *via* magnetic force and torque. Simulations confirm frequency-dependent control of particle motion, enabling continuous transport along the channel ceiling. Reproduced from Kose *et al.* with permission from PNAS, copyright 2009.<sup>38</sup> b) The PDMS-based microfluidic chip features observation windows and defined flow directions for monitoring particle separation. Shape-based separation of spherical and peanut-shaped diamagnetic particles is demonstrated in a ferrofluid-filled T-shaped microchannel using sequential imaging along key channel regions. Reproduced from Zhou *et al.* with permission from AIP, copyright 2016.<sup>155</sup> c) Magnetic fractionation of yeast cells in ferrofluid is demonstrated using a T-shaped microchannel. Experimental images and PDF plots show distinct separation of four yeast cell groups based on their spatial distribution at key channel locations. Reproduced from Chen *et al.* with permission from AIP, copyright 2017.<sup>156</sup> d) Magnetic separation of microparticles by shape (prolate and sphere). Reproduced from Zhou *et al.* with permission from RSC, copyright 2017.<sup>157</sup>

healthy cells continued flowing. Zhou *et al.*<sup>155</sup> demonstrated shape-based separation of same volume spherical and peanut-shaped diamagnetic particles using a T-shaped microfluidic device with a perpendicular permanent magnet to create non-uniform magnetic fields (Fig. 10b). They explored how the flow rate and sheath-to-sample flow ratio influenced separation efficiency. This technique was later extended by Chen *et al.*<sup>156</sup> to separate drug-treated yeast cells with varying sizes and shapes in ferrofluids (Fig. 10c).

Zhou *et al.*<sup>157</sup> introduced a straightforward and effective method to separate equal-volume prolate paramagnetic ellipsoidal and spherical particles based solely on shape-dependent magnetic torque in a uniform static magnetic field, under low Re conditions (Fig. 10d). In the absence of a magnetic field, ellipsoidal particles rotate symmetrically in shear flow without any net lateral movement, preventing separation. However, applying a uniform magnetic field perpendicular to the flow ( $\alpha = 0^\circ$ ) generates a magnetic torque:

$$T_m = \mu_0 \int_{V_p} [(M_p - M_f) \times H_0] dV \quad (15)$$

where  $M_p$  and  $M_f$  are the magnetizations of the particle and fluid, respectively. This torque disrupts the symmetric rotation, and in combination with hydrodynamic wall interactions, induces lateral migration of the ellipsoidal particles. From eqn (12), we can see that the separation is only possible when there's a difference in magnetic susceptibility between the particles and the medium. The study also demonstrated the separation of nonmagnetic spherical and ellipsoidal particles in ferrofluid. Follow-up studies<sup>157–159</sup> showed that the magnetic field direction influences the migration path, while the field strength affects the migration speed. Another interesting possibility

using magnets in microfluidic environments is that they can be used to drive and alter the fluid flow itself by Lorentz forces or magnetic gradient forces.<sup>160</sup>

**3.2.4 Acoustophoresis.** Acoustofluidics is a technology that integrates acoustic wave fields with microfluidics to enable the precise and contactless manipulation of fluids and suspended particles or cells. Two main types of acoustic waves are employed: bulk acoustic waves (BAWs), which propagate through the entire volume of the microfluidic device, and surface acoustic waves (SAWs), which travel along the surface of a piezoelectric substrate. SAWs can be further classified into traveling SAWs (TSAWs), which move in a single direction, and standing SAWs (SSAWs), formed by the interference of counter-propagating TSAWs, resulting in stationary pressure nodes and antinodes.<sup>161</sup> When SAWs or BAWs refract into a fluid-filled microchannel, they generate longitudinal waves (LWs) that exert an acoustic radiation force (ARF) and acoustic streaming flow (ASF)-induced drag on suspended particles or cells. Both forces are combined in the acoustic force  $F_{ac}$  according to:<sup>162–164</sup>

$$F_{ac} = \int_{S_0} [\langle \sigma \rangle - \rho_0 \langle v_1 v_1 \rangle] \cdot n \, dS$$

where  $S_0$  denotes the particle equilibrium surface,  $\sigma$  the viscous stress tensor,  $\rho_0$  the undisturbed density of the particle,  $v_1$  the acoustic velocity, and  $n$  the outward pointing normal vector at the particle surface. Several studies have successfully leveraged the ARF and ASF induced drag force to separate spherical particles according to their size and acoustic contrast factor, which scales with the density and compressibility of the particle and surrounding fluid.<sup>165–170</sup> In these studies, different regimes in the particle behavior



can be distinguished by the Helmholtz number ( $\kappa = \pi d_p / \lambda_t$ ), which relates the particle diameter ( $d_p$ ) to the acoustic wavelength ( $\lambda_t$ ). For  $\kappa < 1$  (Rayleigh regime), particles are primarily affected by ASF and can be trapped in streaming vortices. For  $\kappa \geq 1$  (Mie regime), particles experience dominant ARF, enabling effective manipulation based on the size and acoustic contrast factor of the particle.<sup>171</sup>

While the acoustofluidic separation of spherical particles is well understood and widely used, recent studies found dependencies of the acoustic force also on the shape and orientation of non-spherical particles due to scattering effects and gradients in the acoustic fields.<sup>37,172,173</sup> Moreover, non-spherical particles not only experience translational forces but also an acoustic torque  $T_{ac}$  according to:<sup>163,164</sup>

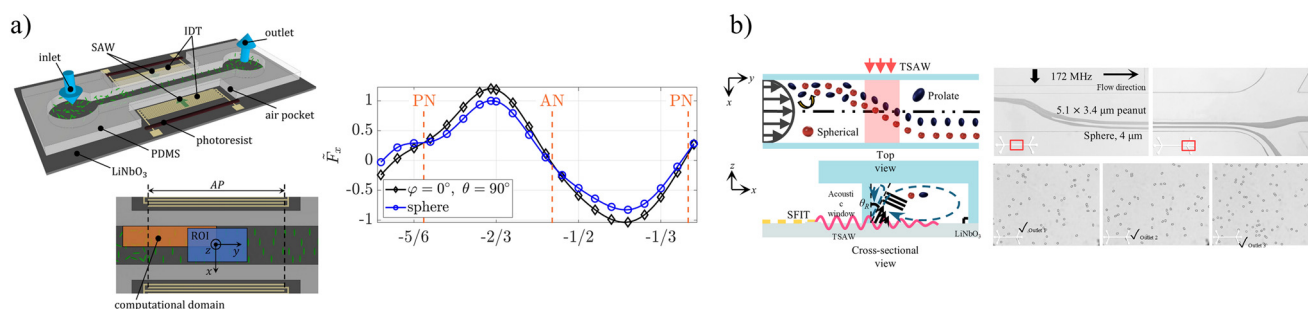
$$T_{ac} = \int_{S_0} \mathbf{r} \times [\langle \sigma \rangle - \rho_0 \langle v_1 v_1 \rangle] \cdot \mathbf{n} \, dS$$

where  $\mathbf{r}$  is a vector pointing from the center of mass to the surface of the particle. The acoustic torque acts to align particles and cells to stable orientations, as demonstrated for red blood cells,<sup>174</sup> prolate polystyrene spheroids<sup>162,173</sup> and disk-shaped aluminum particles.<sup>175</sup> By modulating the amplitude, phase, frequency, or propagation direction of the acoustic waves, non-spherical particles such as fibers can be rotated precisely.<sup>176,177</sup>

Analytical predictions of the acoustic force and torque that govern the behavior of non-spherical particles in an acoustic wave field are typically limited to inviscid fluids,<sup>178–180</sup> predefined incident waves,<sup>181,182</sup> and specific particle geometries.<sup>183–186</sup> To overcome these limitations, Hahn *et al.* (2015) set up a three-dimensional numerical model that allows the migration of arbitrarily shaped particles in a standing acoustic wave field to be predicted.<sup>187</sup> Based on this model, Hoque *et al.* (2022) revealed only a slight influence of the aspect ratio of an oblate shaped particle on the resulting acoustic force.<sup>188</sup> However, the acoustically induced fluid velocity field was assumed constant across the particle surface, and thermoviscous boundary layers surrounding the particle were neglected. These thermoviscous effects can cause localized

microstreaming, which was included in the axisymmetric numerical model derived by Pavlic *et al.* (2022).<sup>189</sup> The axisymmetric setup of the numerical model significantly reduced the numerical effort, but restricted investigations on the effect of the orientation of the particle relative to the incident acoustic wave on the acoustic force. With a three-dimensional numerical model, Wijaya and Lim (2015) confirmed the direct influence of the particle orientation and shape on the acoustic force, although less significant than on the acoustic torque.<sup>172</sup> These dependencies result in a shape-dependent migration of the particles in microfluidic devices, which laid the foundation for separation.

Focusing on prolate polystyrene spheroids in an acoustic field induced by SSAWs, Sachs *et al.* (2023) were among the first to show that the shape-dependent acoustic force can be used to separate elongated from spherical particles by tailoring the design of the microfluidic device (Fig. 11a).<sup>173</sup> In a subsequent study,<sup>162</sup> they further found that the electric field accompanying the SSAWs causes a dielectrophoretic force and torque on the particles, which influence the orientation and 3D position of the particles in the microchannel. Relying on the combined effect of the acoustic and electric fields, the particle separation could be improved as shown by Collins *et al.* (2014) for spherical particles.<sup>190</sup> However, the work of Sachs *et al.* (2023, 2024) primarily focused on theoretical analysis and lacked practical separation demonstrations. To address this, Khan *et al.* (2024) applied TSAWs to successfully separate spheroids from spheres, demonstrating a functional, shape-based acoustic sorting system (Fig. 11b).<sup>37</sup> While effective, this method still faced challenges in handling highly irregular or deformable particles. Compared to passive methods like DLD and viscoelastic microfluidics, acoustofluidic shape-based separation provides tunable, non-contact manipulation without relying on sheath flow. Unlike active magnetic and optical techniques, which are often material- or refractive index-dependent, acoustics can separate a broader range of materials of particles without external labeling. Furthermore, acoustofluidic manipulation is biocompatible, which allows for handling of complex biological samples and particle shapes. Despite its advancements, the



**Fig. 11** a) Schematic representation of an acoustofluidic device with prolate spheroids inside a microchannel sealed with a PDMS cover, which was omitted for visualization. In the middle, the numerically calculated acoustic force component  $\tilde{F}_x$ , normalized by its maximum, is shown for a prolate spheroid and sphere with identical volume in a region between two pressure nodes (PN). Reproduced from Sachs *et al.* with permission from Springer, copyright 2023.<sup>173</sup> b) The schematic and top-view show an acoustofluidic device used to separate 6  $\mu\text{m}$  spheres and similarly sized peanut-shaped particles under a 117 MHz acoustic field. Images at the midstream, downstream, and collection outlets demonstrate effective shape-based separation across three outlets. Reproduced from Khan *et al.* with permission from Nature, copyright 2024.<sup>37</sup>



method is less sensitive to shape than to particle size ( $F_{ac} \sim d_p^3$ ), which poses challenges when separating industrial particles, which may vary both in volume and shape. While the technique has demonstrated significant potential, further research is needed to explore its full capabilities. By refining acoustic parameters and improving the design of microfluidic devices, selectivity and throughput can be greatly enhanced.

## 4. Challenges and future perspectives

This review has comprehensively analyzed the current state of shape-based microfluidic separation techniques, categorizing them into passive and active approaches. While microfluidics has already proven its efficacy for size-based particle manipulation, the extension toward shape-based separation reveals a promising yet underexplored frontier. The shape of a particle or cell is often a more sensitive and informative marker than size, especially in biological and medical contexts. For instance, abnormally shaped cells such as the crescent-shaped erythrocytes in sickle cell anemia, or the irregular morphologies seen in various cancers and infections, can serve as valuable diagnostic or prognostic indicators.<sup>191,192</sup> Therefore, separating particles and cells based on their shape can enhance detection sensitivity and specificity in clinical and research applications. Below, we discuss current challenges, emerging trends, and future directions to advance the field.

### Underlying mechanisms

Despite considerable advancements across microfluidic platforms utilizing hydrodynamic forces, viscoelastic stresses, and external fields such as acoustic, electric, magnetic, and optical forces, many current techniques still fall short in fully exploiting the complex shape-dependent behaviors of particles and cells. A fundamental limitation lies in the lack of generalized models such as lift force equations for non-spherical particles suspended in Newtonian or viscoelastic fluids, which hinders predictive control in passive systems like inertial, viscoelastic, or pinched flow devices. Existing theoretical models are largely based on idealized spherical assumptions, making them inadequate for accurately describing the migration of elongated, asymmetric, or deformable particles. Additionally, particle–particle interactions involving non-spherical geometries remain poorly understood, particularly in how they influence rotational behaviors and trajectory stability. In the case of active methods, rotational modes such as tumbling, kayaking, and log-rolling induced by torque under electric, acoustic, or magnetic fields are known to occur but are rarely harnessed in device design. To bridge this gap, future research must focus on the integration of the comprehensive particle dynamics – from rotation and deformation to material compliance – into theoretical models and experimental platforms. A better understanding of how shape interacts with flow regimes, local shear gradients, and field distributions will enable the development of more robust,

high-resolution, and versatile shape-based separation systems across both passive and active modalities.

### Separation efficiency

One of the primary challenges in shape-based microfluidic separation is achieving high separation efficiency and resolution, as shape differences often induce subtler hydrodynamic effects compared to size-based distinctions. This becomes particularly problematic when dealing with particles that differ only slightly in aspect ratio, making it difficult to establish a clear separation threshold. Moreover, many biological samples are inherently heterogeneous, exhibiting variability in both size and shape, often within polydisperse populations. This complexity makes it challenging to isolate shape as the sole parameter governing migration behavior. To improve performance, future efforts should therefore focus on developing strategies that can effectively decouple shape from size influences through both device design and integrated sensing, adapting to the presence of mixed populations. Advancements in simulation-guided design and adaptive control mechanisms will be essential for tailoring microfluidic platforms to address these multifactorial challenges with greater precision and robustness.

### Enhancing throughput and multiplexing

Many shape-based microfluidic systems are still constrained by relatively low throughput, which hinders their utility in large-scale biological screening or industrial processing. Furthermore, multiplexed separation, *i.e.*, distinguishing and isolating multiple distinct shapes simultaneously, remains a challenge. Future systems need to integrate intelligent flow control, real-time feedback, and potentially AI-assisted image recognition to enhance decision-making during sorting processes.

### Sensor–actuator integration and intelligent control

An important future direction for shape-based microfluidic separation is the integration of intelligent feedback-driven control systems using sensors and actuators. While many current platforms rely on passive hydrodynamic effects or externally applied fields, these mechanisms often offer limited resolution when shape-induced forces are weak or ambiguous. In such cases, a promising alternative is to actively detect particle shape – for example, through optical imaging or real-time shape recognition – and precisely trigger an actuation event (*e.g. via* fluidic, acoustic, and electric forces) only when a target particle enters a specific region. This sensor–actuator framework offers maximum flexibility, allowing programmable, shape-specific sorting even within complex, heterogeneous samples. However, implementing such systems introduces new challenges, including device complexity, real-time data processing, and the development of robust control algorithms capable of synchronizing sensing and actuation. Addressing these issues will require interdisciplinary collaboration across microfluidics, optics,





control engineering, computer vision, and computational analysis, ultimately paving the way for adaptive, high-precision separation systems.

### Scalability and sustainability

As microfluidic technologies transition from laboratory to industrial applications, scalability and sustainability emerge as critical considerations. High-throughput shape-based separation is essential for several applications such as bioprocessing and materials synthesis. However, most current platforms are designed for low-volume, high-precision tasks, limiting their scalability. Innovations in parallelized microfluidic architectures could address this scalability gap by increasing processing capacity without compromising resolution. Furthermore, sustainable fabrication methods, such as recyclable materials or energy-efficient actuation, will align shape-based separation with global efforts to reduce environmental impact. These advancements will broaden the applicability of microfluidic systems in large-scale industrial processes, fostering their adoption through enhanced sustainability.

### Interdisciplinary opportunities

The advancement of shape-based separation requires interdisciplinary collaboration between physicists, engineers, chemists, and biologists. Machine learning techniques could be employed for predictive modeling of particle trajectories based on shape and flow characteristics. Similarly, 3D printing and hybrid soft-lithography methods could aid in designing more sophisticated channel geometries that magnify shape sensitivity.

### Microfluidic-based imaging cytometers

Recent developments in microfluidic imaging cytometry have introduced systems that combine real-time imaging with cell sorting capabilities. These systems utilize algorithms to classify and sort cells based on their morphological features, offering label-free and high-throughput solutions for cell analysis. For instance, advancements in deep learning have enabled real-time cell sorting with high precision and speed, utilizing brightfield and fluorescence microscopy data. Such integration allows for the sorting of cells with specific shapes or morphologies, which is crucial for applications in disease diagnostics and personalized medicine. Incorporating these emerging technologies into microfluidic platforms could significantly enhance the sensitivity and specificity of cell separation techniques. Future research should focus on developing hybrid systems that combine the advantages of microfluidic shape-based separation with advanced imaging and machine learning algorithms. This integration holds the potential to revolutionize cell sorting processes, making them more efficient and applicable to a broader range of biomedical applications.

## 5. Conclusion

Shape-based separation in microfluidics has advanced significantly, enabling the selective manipulation of particles and cells based on morphology rather than size. This capability is crucial for applications in biomedicine, diagnostics, and materials science. This review has outlined key developments across both passive (*e.g.*, DLD, pinched flow, inertial, and viscoelastic systems) and active (*e.g.*, dielectrophoresis, magnetophoresis, optophoresis, and acoustophoresis) approaches, each leveraging distinct physical principles to exploit shape-induced behaviors such as orientation, rotation, and deformability. Importantly, combining numerical modeling and experimental validation has been essential for designing and optimizing these platforms, especially in three-dimensional systems with complex or unknown boundary conditions. As the field advances, continued research is needed to address challenges such as limited throughput, sensitivity to particle shape, and integration with real-time control systems. We encourage stronger interdisciplinary collaboration to develop robust, predictive, and adaptable shape-based separation technologies capable of meeting the demands of real-world biological and engineering applications.

## Author contributions

M. S. K.: writing – original draft (lead); investigation (lead). R. H. J.: writing – original draft (supporting). M. A.: investigation (supporting). S. S.: investigation (supporting); writing – review & editing (supporting). C. C.: writing – review & editing (supporting). J. K.: conceptualization (supporting); writing – review & editing (supporting). J. P.: conceptualization (lead); funding acquisition (lead); writing – review & editing (lead).

## Conflicts of interest

There are no conflicts to declare.

## Data availability

No primary research results, software or code have been included, and no new data were generated or analyzed as part of this review.

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