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## Understanding CO<sub>2</sub> reduction selectivity in silver and gold electrocatalysts using atomically precise nanoclusters

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Au and Ag electrodes have been widely utilized as catalysts for the electrochemical CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) in aqueous solutions. Despite significant differences in their CO<sub>2</sub>RR and competing hydrogen evolution reaction (HER) activities, the fundamental reasons for these distinctions remain unclear. Herein, we present a comparative analysis employing atomically precise Ag and Au nanocluster (NC) catalysts, Ag<sub>25</sub>(SR)<sub>18</sub> and Au<sub>25</sub>(SR)<sub>18</sub> (where SR represents a thiolate ligand), to elucidate the molecular-level mechanisms governing the CO<sub>2</sub>RR and the HER on Ag and Au surfaces. While Au<sub>25</sub>(SR)<sub>18</sub> NCs demonstrate a lower onset potential for the CO<sub>2</sub>RR compared to Ag<sub>25</sub>(SR)<sub>18</sub> NCs, the CO current density of the Au<sub>25</sub>(SR)<sub>18</sub> NCs reaches a plateau and even decreases at high overpotentials due to the increased HER. Electrokinetic and *in situ* infrared spectroscopy investigations using well-defined model NC catalysts revealed that both Ag<sub>25</sub>(SR)<sub>18</sub> and Au<sub>25</sub>(SR)<sub>18</sub> NCs facilitate a CO<sub>2</sub>RR pathway through enhanced water dissociation (WD) kinetics. However, these NCs display significantly different HER behaviors under CO<sub>2</sub>: Au<sub>25</sub>(SR)<sub>18</sub> exhibits enhanced activity, while Ag<sub>25</sub>(SR)<sub>18</sub> is significantly suppressed. Theoretical studies indicate that the enhanced WD kinetics stem from direct proton abstraction by the CO<sub>2</sub>RR intermediate. Adsorption geometry analyses further demonstrate that their differing selectivities arise from distinct HER active sites, thereby explaining the variations in CO<sub>2</sub>RR and HER activities between Ag<sub>25</sub>(SR)<sub>18</sub> and Au<sub>25</sub>(SR)<sub>18</sub> catalysts.

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### Broader context

The electrocatalytic CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) to CO offers a sustainable route to mitigate greenhouse gas emissions while producing a valuable feedstock for fuels and chemicals. Au and Ag are benchmark CO-selective catalysts, yet they display different behaviours under industrially relevant conditions: Au achieves low onset potentials but rapidly loses CO selectivity at high current densities, while Ag sustains CO production at high current densities. Here, we employ atomically precise nanoclusters, Ag<sub>25</sub>(SR)<sub>18</sub> and Au<sub>25</sub>(SR)<sub>18</sub> (SR = thiolate), to isolate the role of metal identity in the CO<sub>2</sub>RR and the competing hydrogen evolution reaction (HER). Combining electrokinetic studies, *operando* infrared spectroscopy, and theoretical calculation, we reveal that both catalysts benefit from accelerated water dissociation in the presence of CO<sub>2</sub>, but Au favours the HER due to weak \*H binding, whereas Ag suppresses the HER through stronger \*H binding, thereby maintaining CO selectivity. These molecular-level insights highlight that beyond \*CO adsorption energy, interfacial proton dynamics and \*H energetics govern CO<sub>2</sub>RR selectivity, offering guidance for designing highly selective catalysts for scalable CO<sub>2</sub> utilization.

## Introduction

The electrocatalytic CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) has emerged as a promising strategy to close the carbon cycle while simultaneously producing value-added fuels and chemicals.<sup>1,2</sup>

Among various CO<sub>2</sub>RR products, CO is of particular industrial relevance, as it serves as a key feedstock for syngas production<sup>3</sup> and polymer synthesis,<sup>4</sup> thereby sustaining strong market demand.<sup>5</sup> Au and Ag are known to selectively produce CO,<sup>6</sup> a feature attributed to their weak binding affinity for \*CO intermediates.<sup>7</sup> Traditionally, Au-based electrodes have been regarded as more efficient than Ag-based electrodes for CO<sub>2</sub>-to-CO conversion.<sup>8–10</sup> In 1994, Hori *et al.* demonstrated that Au electrodes exhibit superior CO<sub>2</sub>RR performance compared to Ag electrodes, achieving lower overpotentials and higher CO selectivity at comparable current densities.<sup>8</sup> This observation is further supported by density functional theory (DFT)

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calculations, which indicate that the free energy barrier for the CO<sub>2</sub>RR is lower on Au surfaces than on Ag surfaces.<sup>10</sup>

The advancement of gas diffusion electrode (GDE)-based flow electrolyzers has enabled the attainment of commercially feasible current densities for the CO<sub>2</sub>RR by overcoming CO<sub>2</sub> mass transport constraints.<sup>11</sup> Although Au catalysts have traditionally been considered more effective than Ag catalysts for CO<sub>2</sub>-to-CO electroreduction, recent research has indicated a notable inconsistency: Ag catalysts demonstrate a rise in CO production rates with increased overpotentials,<sup>12–17</sup> while Au catalysts<sup>18–22</sup> frequently reach a plateau or experience reduced selectivity with increasing applied potentials.

Fig. 1a shows CO partial current densities for various Ag and Au electrocatalysts as a function of applied potential (vs. standard hydrogen electrode, SHE). Au catalysts generally exhibit an earlier onset potential for CO production (approximately  $-0.9$  V vs. SHE) compared to Ag catalysts (approximately  $-1.2$  V vs. SHE).

This lower onset potential of Au is attributed to its optimal CO binding strength, as reported by Jaramillo *et al.* (Fig. 1b). Metals with weaker CO binding than Au (e.g., Ag, Zn) exhibit reduced CO<sub>2</sub>RR activity due to sluggish CO<sub>2</sub> activation, whereas those with stronger CO binding (Cu, Ni, and Pt) activate CO<sub>2</sub> effectively but are limited by slow CO desorption or further CO conversion.

Despite requiring higher overpotentials, Ag catalysts achieve steadily increasing CO current densities exceeding  $400$  mA cm<sup>-2</sup>, while Au catalysts plateau at approximately  $200$  mA cm<sup>-2</sup>. Ozden *et al.* reported that Au nanoparticles (NPs) exhibited declining CO selectivity above  $100$  mA cm<sup>-2</sup>, whereas Ag NPs maintained high CO<sub>2</sub>-to-CO conversion rates even at elevated overpotentials.<sup>23</sup> Similarly, Burdyny and co-workers found that Au-coated GDEs showed decreasing CO selectivity at high current densities, while Ag-coated GDEs retained strong CO selectivity.<sup>24</sup> These findings suggest that CO binding strength alone cannot account for the diverging behaviors observed under industrially relevant current densities.

Water dissociation (WD) is a crucial process in both the CO<sub>2</sub>RR and hydrogen evolution reaction (HER), particularly under alkaline conditions.<sup>25–27</sup> Since both the CO<sub>2</sub>RR and the HER entail proton transfer from H<sub>2</sub>O to intermediates, the WD

step significantly influences the provision of protons to the reaction interface. Nevertheless, the WD mechanism is frequently disregarded because of the challenges linked to theoretical modeling and experimental isolation. Additionally, traditional nanostructured catalysts encounter issues such as ambiguous active sites and non-uniform surfaces, which hinder the clarification of structure–activity relationships.

Atomically precise metal nanoclusters (NCs) have recently garnered significant attention due to their unique electrocatalytic properties.<sup>28–31</sup> Their atom-level precision represents a breakthrough in overcoming the limitations of traditional catalysts. These NCs can be synthesized with molecular purity, and their structures can be definitively determined by single-crystal X-ray diffraction (SC-XRD),<sup>32</sup> allowing for identification through specific molecular formulas such as Au<sub>25</sub>(SR)<sub>18</sub>, Au<sub>144</sub>(SR)<sub>60</sub>, Ag<sub>25</sub>(SR)<sub>18</sub>, and Ni<sub>6</sub>(SR)<sub>12</sub>, with SR denoting a thiolate ligand. Additionally, the presence of surface-protecting ligands provides exceptional stability to these NCs, even at ultrasmall sizes ( $<3$  nm). Due to their precisely defined catalytic surfaces, metal NCs serve as valuable model catalysts for exploring fundamental catalytic mechanisms.

Kauffman *et al.* initially demonstrated that Au<sub>25</sub>(SR)<sub>18</sub> NCs exhibit excellent CO<sub>2</sub>RR activity attributed to their unique CO<sub>2</sub> adsorption sites containing tri-sulfur motifs.<sup>33</sup> Subsequent investigations utilizing Au<sub>25</sub>(SR)<sub>18</sub>, Au<sub>38</sub>(SR)<sub>24</sub>, and Au<sub>144</sub>(SR)<sub>60</sub> NCs indicated that dethiolated Au sites bridging surface sulfur atoms and core Au atoms function as the active sites for electrochemical reduction of CO<sub>2</sub> to CO.<sup>34</sup> Recently, Au active sites have been effectively incorporated into other NC frameworks such as Ag<sub>25</sub>(SR)<sub>18</sub><sup>35</sup> and Ni<sub>4</sub>(SR)<sub>8</sub>,<sup>36</sup> confirming the broad applicability and transferability of these active-site motifs. While Ag<sub>25</sub>(SR)<sub>18</sub> NCs have demonstrated lower CO<sub>2</sub>RR activity compared to Au<sub>25</sub> NCs,<sup>35</sup> a direct evaluation of their CO<sub>2</sub>RR performance and competition with the HER under industrially relevant conditions is yet to be documented.

Herein, we present a comparative analysis of CO<sub>2</sub>RR and HER activities using Ag<sub>25</sub>(SPhMe<sub>2</sub>)<sub>18</sub>, where SPhMe<sub>2</sub> = 2,4-dimethylbenzenethiolate, and Au<sub>25</sub>(SEtPh)<sub>18</sub>, where SEtPh = 2-phenylethanethiolate, as model catalysts. These two NCs,

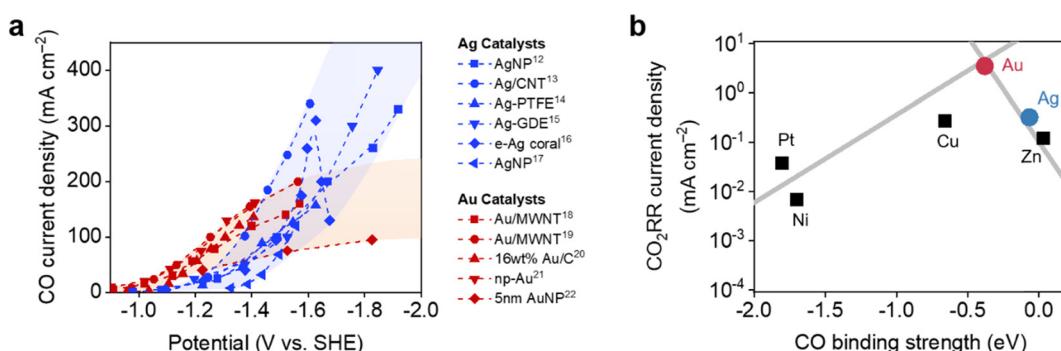


Fig. 1 (a) Benchmarks of CO current density values for AgNPs<sup>12–17</sup> and AuNPs<sup>18–22</sup> as a function of cathodic potential, with shaded regions serving as a visual guide. A pH-independent SHE scale is used to facilitate comparison across different experimental conditions. (b) CO current densities of different metal surfaces at  $-0.8$  V versus RHE plotted against CO binding strength. Grey lines are incorporated as visual aids. Reproduced with permission from ref. 7. Copyright 2014 American Chemical Society.

hereafter abbreviated as  $\text{Ag}_{25}$  and  $\text{Au}_{25}$ , respectively, exhibit nearly identical geometric structures but differ only in their metal composition, allowing a direct comparison of their intrinsic catalytic performance at the atomic scale. Although  $\text{Au}_{25}$  is generally expected to exhibit superior performance compared to  $\text{Ag}_{25}$ , our results show that this is not always the case, particularly at high overpotentials ( $>0.3$  V vs. reversible hydrogen electrode, RHE; all potentials are referenced to RHE unless stated otherwise), attributed to the presence of the competing HER. Electrokinetic and *in situ* spectroscopic analyses validate that WD kinetics are enhanced in the presence of  $\text{CO}_2$  on both NCs. DFT calculations further demonstrate that disparities in hydrogen adsorption energies between Ag and Au significantly influence their divergent  $\text{CO}_2\text{RR}$  selectivities. These insights shed light on the enhanced CO selectivity of  $\text{Ag}_{25}$  at elevated current densities and offer valuable guidance for the development of next-generation electrocatalysts tailored for efficient industrial  $\text{CO}_2$  conversion.

## Results and discussion

### $\text{CO}_2\text{RR}$ activities of atomically precise $\text{Ag}_{25}$ and $\text{Au}_{25}$ NCs

To compare the catalytic properties of Ag and Au directly, we utilized atomically precise  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs as model catalysts. These NCs possess nearly identical atomic structures but vary only in their constituent metal atoms, allowing for an atomic-level exploration of the impact of metal identity in the  $\text{CO}_2\text{RR}$ . SC-XRD analysis clearly revealed their atomic structures.<sup>32,37</sup> Both  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs consist of an icosahedral  $\text{Ag}_{13}$  (or  $\text{Au}_{13}$ ) core surrounded by six dimeric  $\text{Ag}_2(\text{SR})_3$  (or  $\text{Au}_2(\text{SR})_3$ ) staple motifs, as illustrated in Fig. 2a. The structural similarity between  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs offers an excellent basis for comparing catalytic properties using precisely defined catalyst structures.

We synthesized the  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs following procedures described elsewhere<sup>32,37</sup> with slight modifications (refer to the Methods section in the SI). The NCs were characterized using electrospray ionization (ESI) mass spectrometry and ultraviolet-visible (UV-vis) absorption spectroscopy. The ESI mass spectra displayed distinct single peaks (Fig. 2b and c), indicating the molecular purity of both NCs. Additionally, the experimentally observed peaks at 5167 and 7393 Da closely matched the isotope patterns for  $\text{Ag}_{25}(\text{SC}_8\text{H}_9)_{18}^-$  and  $\text{Au}_{25}(\text{SC}_8\text{H}_9)_{18}^-$  NC ions, respectively, confirming the atomically precise composition of the synthesized NCs (insets of Fig. 2b and c). The UV-vis absorption spectra of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs also showed characteristic features consistent with previous findings (Fig. S1 in the SI).<sup>37,38</sup>

In our previous studies, we have shown that thiolate-protected metal NCs can be electrochemically activated by partially removing thiolate ligands.<sup>34,35</sup> Here, both  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs were activated through constant potential electrolysis (CPE) at  $-0.96$  V for 2 h. The UV-vis absorption spectra of the activated  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs (Fig. S1 in the SI) remained nearly identical to those of the pristine NCs, indicating preservation of the NC structure during activation. X-ray photoelectron

spectroscopy (XPS) analysis (Fig. S2a, b and Table S1 in the SI) confirmed a reduction in ligand content to approximately twelve thiolates, resulting in  $\text{Ag}_{25}(\text{SR})_{12}$  and  $\text{Au}_{25}(\text{SR})_{12}$  compositions. These compositions align with those previously reported for electrochemically activated  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs.<sup>34,35</sup> These findings suggest that electrochemical activation exposed an equivalent number of active sites on both NCs (Fig. S2c and d in the SI). Importantly, the activated NCs remained stable throughout subsequent CPE experiments (Fig. S3 in the SI). High-angle annular dark-field scanning transmission electron microscopy images of the recovered  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs after the CPE experiments (Fig. S4, SI) further verified that both NCs preserved their structural integrity, each exhibiting a diameter of approximately 1 nm.

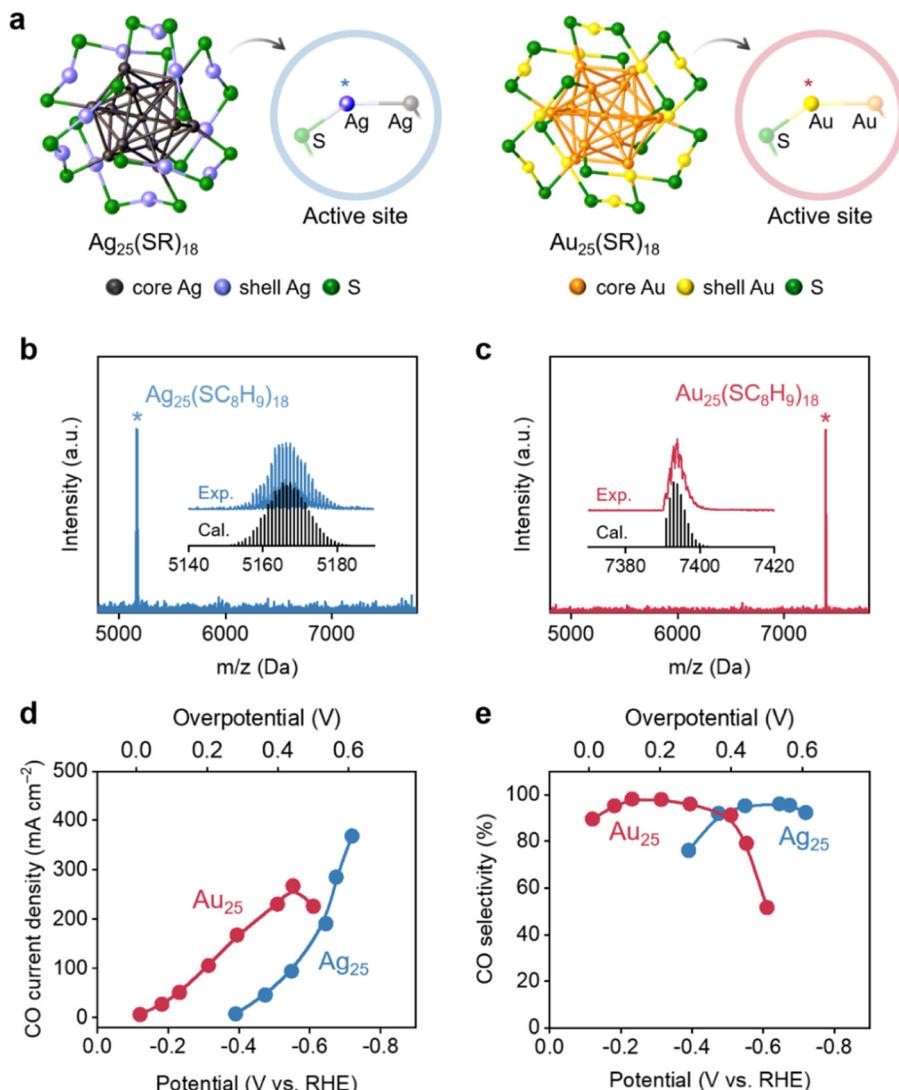
The  $\text{CO}_2\text{RR}$  activities of the  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs were assessed through CPE experiments on NC/GDEs in a  $\text{CO}_2$ -fed flow electrolyzer using a 1.0 M KOH electrolyte solution (refer to the Methods section and Fig. S5 in the SI). All electrochemical measurements were conducted after the electrochemical activation process. Fig. 2d illustrates the CO partial current densities recorded for  $\text{Au}_{25}$  and  $\text{Ag}_{25}$  NCs. The  $\text{Au}_{25}$  NC demonstrated CO production commencing near zero overpotential, which initially increased but stabilized at  $230 \text{ mA cm}^{-2}$  below  $-0.5$  V. In contrast, the  $\text{Ag}_{25}$  NC necessitated a slightly higher onset potential ( $-0.4$  V) but exhibited a continuous rise in current density with increasing overpotential. The CO selectivity profiles of the NC catalysts also exhibited notable distinctions (Fig. 2e). The CO selectivity of  $\text{Au}_{25}$  NCs peaked at 98% at  $-0.2$  V, declining significantly to 52% at  $-0.6$  V. Conversely, the  $\text{Ag}_{25}$  NC demonstrated a CO selectivity of 76% near its onset potential, which progressively increased and remained above 92% even at  $-0.7$  V. These findings align with previously reported trends for Ag and Au catalysts (Fig. 1a). Specifically, the CO current densities of Au catalysts tend to plateau or decrease at high overpotentials, while those of Ag catalysts continue to rise, highlighting a fundamental distinction in the catalytic behavior of Ag and Au surfaces.

### Comparing $\text{CO}_2\text{RR}$ and HER activities of NC catalysts

To gain a deeper understanding of the differing  $\text{CO}_2\text{RR}$  selectivities of Ag and Au electrocatalysts, we investigated their competing HER activities. Fig. 3a compares the CO and  $\text{H}_2$  partial current densities of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs under  $\text{CO}_2$ - and Ar-fed conditions, respectively. Notably, both NCs showed lower onset potentials for the  $\text{CO}_2\text{RR}$  compared to the HER, suggesting that the  $\text{CO}_2\text{RR}$  is more favorable than the HER on both catalysts.

Under neutral to alkaline conditions, the  $\text{CO}_2\text{RR}$  and HER proceed *via* the following elementary steps, where \* denotes an active site:

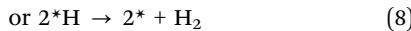
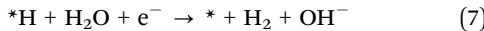
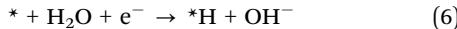




**Fig. 2** (a) Crystal structures of  $\text{Ag}_{25}(\text{SR})_{18}^-$  and  $\text{Au}_{25}(\text{SR})_{18}^-$  NCs (adapted from ref. 36 and 31, respectively). Only the sulfur atoms of the thiolate ligands are depicted for clarity. The active site units of the NCs are highlighted in circles. Negative-mode ESI mass spectra of (b)  $\text{Ag}_{25}$  and (c)  $\text{Au}_{25}$  NCs. Insets compare the experimental (lines) and simulated (bars) isotope patterns of the NC ions. (d) CO current density and (e) CO selectivity measured for  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs at different cathodic potentials in a  $\text{CO}_2$ -fed flow electrolyzer using 1.0 M KOH as the electrolyte. All potentials were *iR*-corrected. In (d) and (e), the data represent averages from 2–3 independent experiments, and the error bars were smaller than the symbol size in the graphs.



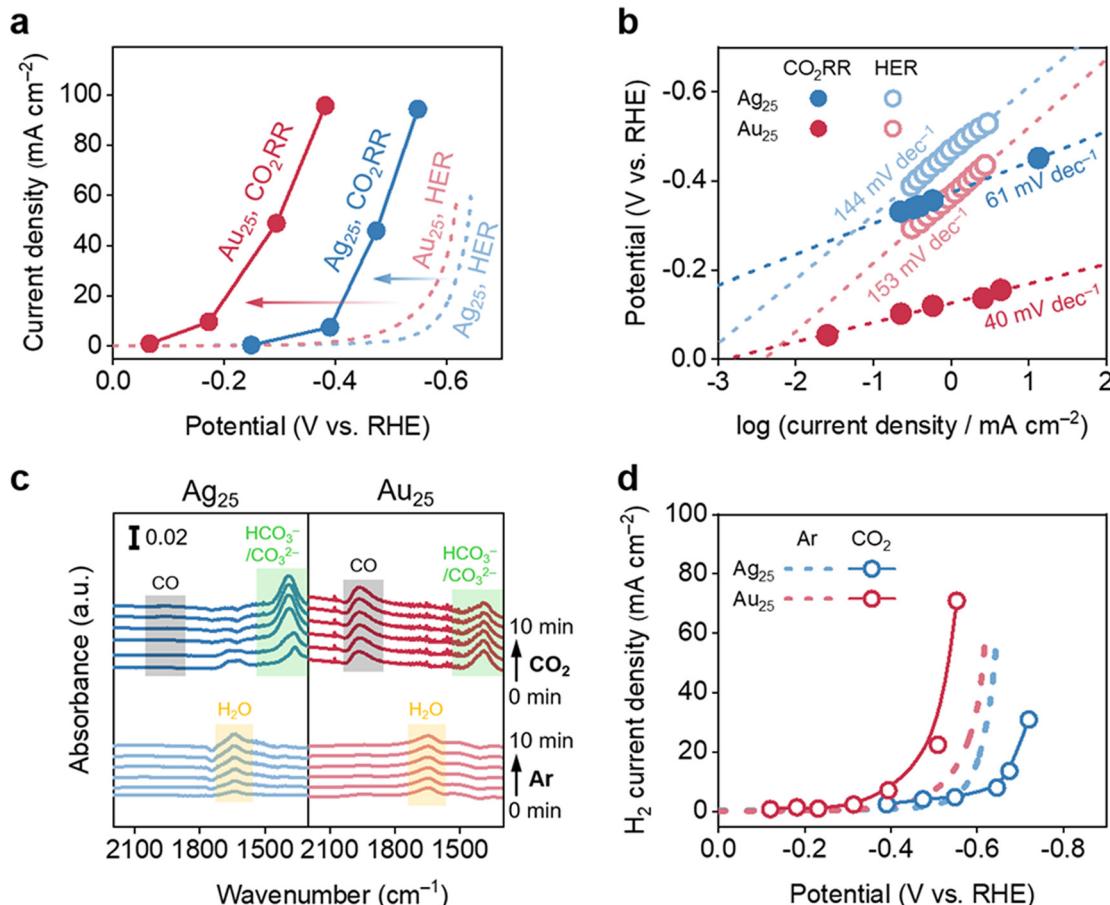
HER:<sup>40</sup>



To further investigate the mechanistic origin of differences in  $\text{CO}_2$ RR and HER activities, electrokinetic studies were conducted. For the  $\text{CO}_2$ RR, the theoretical Tafel slopes are predicted to be 120 and 40 mV dec<sup>-1</sup> when the first (eqn (1)) and second (eqn (3)) electron-transfer steps are rate-determining,

respectively.<sup>39,41</sup> On conventional Ag and Au surfaces, the first electron-transfer step involving  $\text{CO}_2$  adsorption is typically the potential-determining step (PDS).<sup>19,42–44</sup> However, the  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs exhibited notably lower Tafel slopes of 61 and 40 mV dec<sup>-1</sup>, respectively (Fig. 3b), indicating enhanced facilitation of the first electron-transfer step on these clusters. Both NCs exhibited pH-independent and H/D isotope-independent  $\text{CO}_2$ RR activity (Fig. S6 in the SI), indicating that proton-transfer steps are not involved in the PDS. Therefore, the second electron-transfer step (eqn (3)) is likely the PDS for both catalysts. The higher Tafel slope of  $\text{Ag}_{25}$  compared to  $\text{Au}_{25}$  may be attributed to the slower electron transfer rate on the  $\text{Ag}_{25}$  NC (Fig. S7 in the SI). Conversely, for the HER under an Ar atmosphere, the Tafel slopes were measured to be 144 and 153 mV dec<sup>-1</sup> for  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs, respectively (Fig. 3b),





**Fig. 3** (a) Comparison of the CO and H<sub>2</sub> current densities measured in the CO<sub>2</sub>- and Ar-fed flow electrolyzer, respectively, on the Ag<sub>25</sub>/GDE and Au<sub>25</sub>/GDE. (b) Tafel plots for the CO<sub>2</sub>-to-CO electroreduction and HER on the Ag<sub>25</sub>/GDE and Au<sub>25</sub>/GDE. (c) *In situ* ATR-FTIR spectra recorded on the Ag<sub>25</sub>/GDE and Au<sub>25</sub>/GDE in Ar- and CO<sub>2</sub>-saturated 1.0 M NaClO<sub>4</sub> electrolyte solutions during the CPE measurement at -1.8 V versus SHE. (d) H<sub>2</sub> current densities measured on the Ag<sub>25</sub>/GDE and Au<sub>25</sub>/GDE in Ar- and CO<sub>2</sub>-fed flow electrolyzers using a 1.0 M KOH electrolyte solution. The potentials in (a), (b), and (d) were *iR*-corrected.

indicating that the Volmer step involving water dissociation (eqn (6)) serves as the PDS on both catalysts.

As both the CO<sub>2</sub>RR<sup>25,26</sup> and the HER<sup>27</sup> involve a WD step under alkaline conditions, the lower onset potential observed for the CO<sub>2</sub>RR is surprising, considering the high energy barrier associated with this step.<sup>45</sup> One possible explanation is the generation of additional proton donors in the presence of CO<sub>2</sub>. Both carbonic acid (H<sub>2</sub>CO<sub>3</sub>) and bicarbonate ions (HCO<sub>3</sub><sup>-</sup>) can form under CO<sub>2</sub> conditions. However, the concentration of H<sub>2</sub>CO<sub>3</sub> remains negligible due to the slow CO<sub>2</sub> hydration rate ( $2.9 \times 10^{-2} \text{ s}^{-1}$ ) and the rapid dissociation of H<sub>2</sub>CO<sub>3</sub> ( $3 \times 10^6 \text{ s}^{-1}$ ) under CO<sub>2</sub> conditions.<sup>46</sup> While HCO<sub>3</sub><sup>-</sup> can serve as a viable proton donor for the CO<sub>2</sub>RR<sup>43,47</sup> and the HER,<sup>42,48</sup> the experimentally determined reaction orders for the CO<sub>2</sub>RR with respect to HCO<sub>3</sub><sup>-</sup> were near-zero for both NCs (Fig. S8 in the SI), indicating that the contribution from HCO<sub>3</sub><sup>-</sup> is negligible and that water is the dominant proton source in this system.

Another possibility is that the WD step itself is accelerated under CO<sub>2</sub> conditions. To directly assess WD kinetics, the NC/GDEs were subjected to *in situ* attenuated total reflection (ATR)-Fourier transform infrared (FTIR) absorption spectroscopy<sup>49</sup>

during CPE experiments under Ar and CO<sub>2</sub> atmospheres (refer to the Methods section and Fig. S9 in the SI). A 1.0 M NaClO<sub>4</sub> electrolyte solution was utilized in this experiment to prevent interference from pre-existing bicarbonate ions.

Fig. 3c presents the *operando* FTIR spectra obtained from the Ag<sub>25</sub>/GDE and Au<sub>25</sub>/GDE during the CPE experiments. In the Ar environment, both NCs exhibited the H<sub>2</sub>O bending mode ( $\delta\text{HOH}$ ,  $\sim 1645 \text{ cm}^{-1}$ ), indicating water molecules' accumulation near the negatively charged electrode surface due to hydrated cation layering.<sup>50</sup> Upon introducing CO<sub>2</sub> gas, noticeable spectral changes occurred. Two new vibrational bands emerged at approximately  $1950 \text{ cm}^{-1}$  and  $1400 \text{ cm}^{-1}$ , corresponding to the stretching mode of adsorbed \*CO intermediates<sup>51</sup> (refer to Fig. S10a in the SI for Ag<sub>25</sub>) and the asymmetric stretching of carbonate species (HCO<sub>3</sub><sup>-</sup>/CO<sub>3</sub><sup>2-</sup>)<sup>52</sup> formed by CO<sub>2</sub> equilibrium. Simultaneously, the intensity of the  $\delta\text{HOH}$  band gradually decreased on Ag<sub>25</sub> NCs, while it promptly vanished on Au<sub>25</sub> NCs (Fig. 3c and Fig. S10b, c in the SI). This swift disappearance of the water bending peak under CO<sub>2</sub> conditions indicates a substantial reduction in accumulated water, implying enhanced WD kinetics in the presence of CO<sub>2</sub> for both NCs.

As discussed above, the Volmer step serves as the PDS for the HER on both  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs. Consequently, one would anticipate that improved WD kinetics would also enhance the HER performance of both NCs. However, while  $\text{Au}_{25}$  demonstrated increased HER activity under  $\text{CO}_2$  compared to Ar (Fig. 3d),  $\text{Ag}_{25}$  exhibited a notable decline. This suggests that the augmented WD kinetics under  $\text{CO}_2$  do not favor the HER kinetics of  $\text{Ag}_{25}$ . This divergent behavior highlights both the similarities and distinctions between  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs: although both show significantly lower onset potentials for the  $\text{CO}_2\text{RR}$  compared to the HER—attributable to the enhanced WD kinetics under  $\text{CO}_2$ — $\text{Au}_{25}$  exhibits improved HER activity under  $\text{CO}_2$ , whereas  $\text{Ag}_{25}$  exhibits markedly suppressed HER activity under  $\text{CO}_2$  flow.

### DFT calculations

To comprehend the differing  $\text{CO}_2\text{RR}$  selectivities of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs, we conducted DFT calculations using  $\text{Ag}_{25}(\text{SCH}_3)_{17}^-$  and  $\text{Au}_{25}(\text{SCH}_3)_{17}^-$  as model systems, representing their singly dethiolated forms (Fig. S11 in the SI). To ensure that protons were provided from water, the calculations were conducted with six explicit water solvent molecules. Initially, we computed the Gibbs free energies of crucial intermediates involved in the alkaline  $\text{CO}_2\text{RR}$  pathway on both NCs. As illustrated in Fig. 4a and Fig. S12 in the SI, the formation of the  $^*\text{COOH}$  intermediate from  $^*\text{CO}_2^-$  occurs with a low energy barrier (transition state 1, TS1), succeeded by  $^*\text{CO}$  generation through a potential-determining electron transfer (transition state 2, TS2) for both NCs. Notably, the energy barrier for TS2 was lower on  $\text{Au}_{25}$  (1.07 eV) than on  $\text{Ag}_{25}$  (1.27 eV), aligning with the experimentally observed lower onset potential for the  $\text{CO}_2\text{RR}$  on  $\text{Au}_{25}$  (Fig. 2d).

Since the WD step plays a role in both the  $\text{CO}_2\text{RR}$  and HER, we compared the corresponding barriers between the  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs. Fig. S13 in the SI illustrates that the initial WD step acts as the PDS for the HER on both  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs, with energy barriers of 1.57 and 0.93 eV, respectively. A direct comparison of the WD barriers during the  $\text{CO}_2\text{RR}$  and the HER (Fig. 4b) indicates that WD proceeds more favorably during the  $\text{CO}_2\text{RR}$  than during the HER for both NCs. The adsorption configurations of crucial reaction intermediates offer valuable insights into the promotion of WD during the  $\text{CO}_2\text{RR}$ . As depicted in Fig. 4c, the formation of  $^*\text{COOH}$  from  $^*\text{CO}_2^-$  involves a direct proton transfer from a neighboring water molecule. This is attributed to the capability of  $^*\text{CO}_2^-$  intermediates to nucleophilically abstract a proton from nearby water molecules, thereby reducing the activation barrier for proton transfer. Furthermore, the Au–COOH bond length (2.08 Å) was shorter than that of Ag–COOH (2.23 Å), indicating a stronger stabilization of the intermediate on  $\text{Au}_{25}$  and contributing to its enhanced  $\text{CO}_2\text{RR}$  kinetics.

Furthermore, the disparity in limiting potentials between the  $\text{CO}_2\text{RR}$  and the HER offers mechanistic insight into the selectivity profile (Fig. 4d). In the case of  $\text{Ag}_{25}$ , the limiting potential for the  $\text{CO}_2\text{RR}$  (1.27 eV) is significantly lower than that for the HER (1.57 eV), indicating a pronounced preference for the  $\text{CO}_2\text{RR}$ . Conversely, for  $\text{Au}_{25}$ , the limiting potentials for the

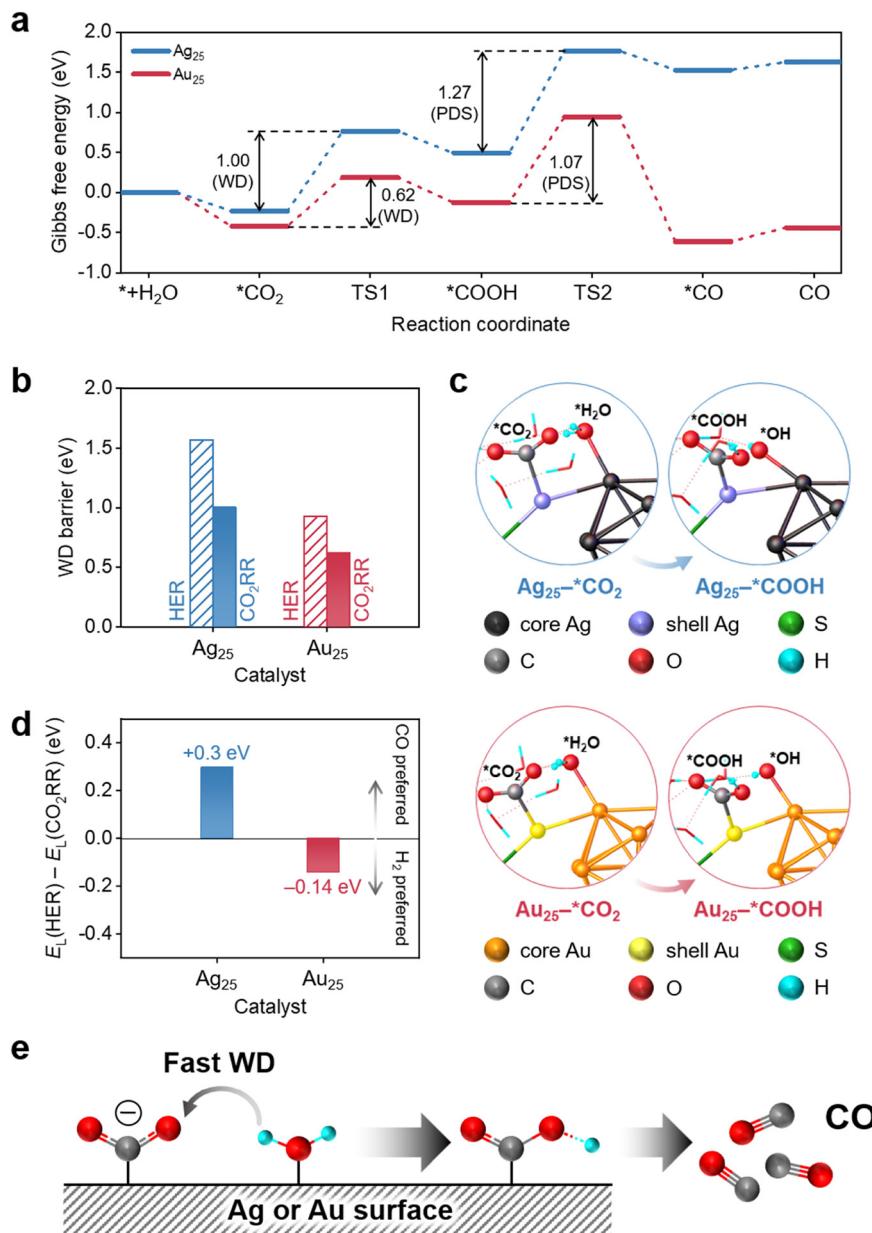
$\text{CO}_2\text{RR}$  (1.07 eV) and the HER (0.93 eV) are similar, explaining the experimentally observed decline in CO selectivity at elevated overpotentials (Fig. 2e). These computational results collectively demonstrate that the WD kinetics are significantly enhanced by direct proton abstraction by the  $^*\text{CO}_2^-$  intermediates, resulting in a reduced kinetic barrier for  $^*\text{COOH}$  formation and increased  $\text{CO}_2\text{RR}$  activity. A simplified schematic of this mechanistic pathway is depicted in Fig. 4e, emphasizing the contribution of  $^*\text{CO}_2^-$  in expediting the WD step on both Ag and Au surfaces.

We will now compare the contrasting HER behaviors of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs under  $\text{CO}_2$  and Ar atmospheres, as shown in Fig. 3d. To clarify these distinctions, we examined the adsorption geometry of  $^*\text{H}$  intermediates. Among the adsorption sites tested (Fig. S14 in the SI), the hollow sites at the  $\text{Ag}_3/\text{Au}_3$  triangular facet exhibit the lowest hydrogen adsorption energies for both NCs. Accordingly, under an Ar atmosphere, the dissociated hydrogen from  $\text{H}_2\text{O}$  is adsorbed at the hollow site of the  $\text{Ag}_3$  ( $\text{Au}_3$ ) triangle, with distances of 1.88 Å and 2.44 Å from the central atom on  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs, respectively (Fig. 5). This observation suggests that the Au surface exhibits a weaker affinity for hydrogen in comparison to the Ag surface.

The difference in behavior can be attributed to stronger aurophilic (Au–Au) interactions<sup>53,54</sup> compared to argentophilic (Ag–Ag) interactions,<sup>55</sup> which arise from relativistic effects linked to the heavy atomic mass of Au. These effects lead to the contraction of the 6s orbital and the expansion of the 5d orbitals.<sup>56,57</sup> The expanded 5d orbitals not only enhance both Au–ligand and Au–Au bonding but also widen the d-state energy distribution, thereby reducing the binding strength with adsorbates.<sup>58</sup> Consistent with this, numerous Ag–H multinuclear complexes<sup>59–61</sup> and clusters<sup>62,63</sup> have been documented, while Au–H clusters<sup>64,65</sup> are comparatively rare. In our system, the weak  $\text{Au}_3$ –H binding likely results from this relativistic effect, which facilitates the easy release of the  $^*\text{H}$  intermediate from the  $\text{Au}_3$  triangle, ultimately promoting  $\text{H}_2$  evolution.

The HER activity of  $\text{Au}_{25}$  is expected to increase further in the presence of  $\text{CO}_2$ . Calculations of alkaline HER reaction energetics with an adsorbed  $\text{CO}_2$  molecule showed that, on  $\text{Au}_{25}$ , the dissociated H from  $\text{H}_2\text{O}$  relocates from the hollow site to the staple Au site, while on  $\text{Ag}_{25}$ , it remains at the strongly favored hollow site (Fig. S15 in the SI). Previous studies on the HER of  $\text{Au}_{25}$  catalysts have mainly focused on  $^*\text{H}$  adsorption at the core atoms of the cluster.<sup>66,67</sup> However, it has also been reported that the preferred adsorption site can vary depending on the electronic structure of the catalyst.<sup>68</sup> Notably, the  $^*\text{H}$  adsorption site can shift depending on the reaction environment. Compared with the alkaline HER in an Ar atmosphere, the calculated PDS barrier on  $\text{Au}_{25}$  decreases from 0.93 to 0.83 eV due to the participation of the more active staple Au site. Conversely, the PDS barrier on  $\text{Ag}_{25}$  increases from 1.57 to 1.65 eV in the presence of  $\text{CO}_2$ , possibly due to the competition with the  $\text{CO}_2\text{RR}$ . These results provide a clear explanation for the differing HER behaviors of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs under  $\text{CO}_2$  and Ar atmospheres.





**Fig. 4** (a) Free energy diagrams illustrating  $\text{CO}_2$ -to-CO reduction with six explicit water solvent molecules on  $\text{Ag}_{25}(\text{SCH}_3)_7^-$  and  $\text{Au}_{25}(\text{SCH}_3)_7^-$  NCs. (b) Comparison of WD energy barriers for the CO<sub>2</sub>RR and HER on  $\text{Ag}_{25}(\text{SCH}_3)_7^-$  and  $\text{Au}_{25}(\text{SCH}_3)_7^-$  NCs. (c) Optimized intermediate structures of  $^*\text{CO}_2$ - and  $^*\text{COOH}$ - adsorbed onto  $\text{Ag}_{25}(\text{SCH}_3)_7^-$  (blue circles) and  $\text{Au}_{25}(\text{SCH}_3)_7^-$  (red circles). Only structures near the active sites are shown for clarity. (d) Differences in limiting potentials for the CO<sub>2</sub>RR and HER on  $\text{Ag}_{25}(\text{SCH}_3)_7^-$  and  $\text{Au}_{25}(\text{SCH}_3)_7^-$  NCs. (e) Proposed mechanism of the alkaline CO<sub>2</sub>RR occurring on Ag and Au surfaces.

To summarize, the DFT calculations unequivocally offer a molecular-level explanation for the distinct selectivities observed for the  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs. The WD step is significantly accelerated by the direct abstraction of protons by  $^*\text{CO}_2^-$  intermediates during the CO<sub>2</sub>RR on both NCs, thereby amplifying the CO<sub>2</sub>RR. The disparate active sites implicated in the HER contribute to the differing HER performances of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs. While the strongly adsorbed  $^*\text{H}$  intermediate at the hollow site notably hinders the HER activity on  $\text{Ag}_{25}$ , the participation of the more active staple Au site significantly enhances the HER activity of  $\text{Au}_{25}$ , resulting in a preference for H<sub>2</sub> production over CO.

Finally, it is instructive to compare the catalytic behaviors of the model catalysts with those of more conventional catalysts. Fig. 6 illustrates CO<sub>2</sub>RR and HER performances of commercial Ag and Au NP catalysts. Consistent with the patterns noted for  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs, Au NPs demonstrate a low onset potential for CO production but achieve a limiting current density of around  $50 \text{ mA cm}^{-2}$  (Fig. 6a). This is accompanied by a decrease in CO selectivity and an escalation in HER activity at high overpotentials. In contrast, Ag NPs exhibit a steadily increasing current, maintaining CO selectivity above 80% at elevated overpotentials (Fig. 6a). Notably, the divergent HER



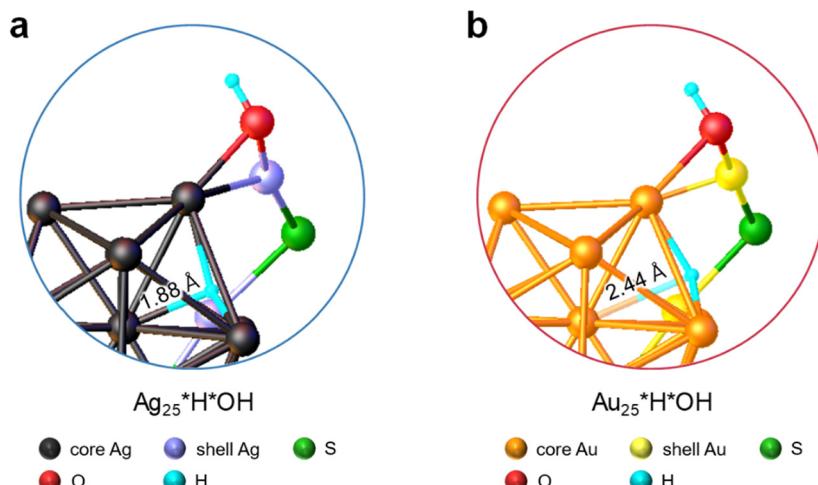


Fig. 5 Optimized intermediate structures of \*H- and \*OH co-adsorbed (a)  $\text{Ag}_{25}(\text{SCH}_3)_{17}^-$  and (b)  $\text{Au}_{25}(\text{SCH}_3)_{17}^-$ . The alkyl chains and other five staple units are omitted for clarity.

behaviors of  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs are also evident for Ag and Au NPs (Fig. 6b). Specifically, relative to their HER activities under an Ar atmosphere, Au NPs exhibit enhanced HER activity, whereas Ag NPs exhibit diminished HER activity in the

presence of  $\text{CO}_2$ , despite their markedly distinct structural characteristics, particularly the absence of ligand protection in the NPs in contrast to the NCs.

## Conclusions

In this study, we investigated the contrasting  $\text{CO}_2\text{RR}$  and HER behaviors of Ag and Au electrocatalysts. Leveraging the atomically well-defined surfaces of NC catalysts, we conducted a molecular-level analysis of their catalytic activities. We observed that while Au catalysts exhibit higher  $\text{CO}_2\text{RR}$  activity compared to Ag catalysts, they also exhibit significantly enhanced HER activity, leading to reduced CO selectivity. Electrokinetic and *operando* spectroscopic analyses indicated that both  $\text{Ag}_{25}$  and  $\text{Au}_{25}$  NCs demonstrate accelerated WD in the presence of  $\text{CO}_2$ , resulting in increased CO production over  $\text{H}_2$ . However, they exhibit distinct HER behaviors under  $\text{CO}_2$  conditions: the HER activity of  $\text{Au}_{25}$  NCs is enhanced, whereas that of  $\text{Ag}_{25}$  NCs is notably suppressed. These findings are supported by DFT calculations, illustrating that WD kinetics are greatly influenced by direct proton abstraction by  ${}^*\text{CO}_2^-$  intermediates. Additionally, adsorption geometry analyses revealed their distinct active sites for the HER under  $\text{CO}_2$ , explaining the varying  $\text{CO}_2\text{RR}$  selectivities observed. Overall, this study highlights that well-defined, atomically precise NCs provide valuable molecular-level insights into  $\text{CO}_2\text{RR}$  and HER processes, which can be extrapolated to traditional catalysts.

## Author contributions

H. S. and D. L. designed the project. H. S. carried out material synthesis and characterization, electrochemical test, and electrokinetic studies. F. S. performed the DFT calculation with Q. T.'s guidance. Q. T. and D. L. supervised the project. H. S. and D. L. wrote the manuscript. All authors discussed the results and provided comments on the manuscript at all stages.

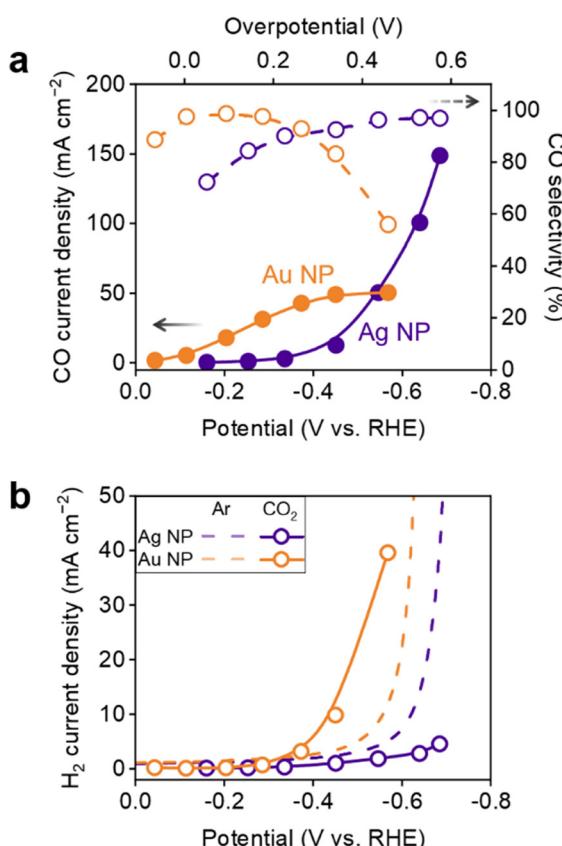


Fig. 6 (a) CO current densities and selectivities of Ag and Au NPs at different cathodic potentials in a  $\text{CO}_2$ -fed flow electrolyzer employing 1.0 M KOH as the electrolyte. (b)  $\text{H}_2$  current densities of Ag and Au NPs in Ar- and  $\text{CO}_2$ -fed flow electrolyzers using 1.0 M KOH as the electrolyte. The potentials were  $iR$ -corrected.

## Conflicts of interest

There are no conflicts to declare.

## Data availability

The data supporting this article have been included as part of the supplementary information (SI). Supplementary information: methods, schematics of cell configurations, UV-vis and IR absorption spectra, XPS results, electrochemical data, and DFT calculation results. See DOI: <https://doi.org/10.1039/d5ey00269a>.

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