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# From Illumination to Prediction: A Kinetic Model for Photoredox Catalytic Activity

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**ABSTRACT:** Photocatalysis is a powerful tool in synthesis, although the key factors that determine its performance are not fully understood. We present a kinetic model for evaluating photocatalytic performance that can be used both to interpret experiments and to optimize kinetic parameters based on experimental data. We introduce the steady-state reduction potential of the substrate or quencher  $Q$  ( $E_Q$ ) as the descriptor of photocatalytic efficiency. The model relies on key parameters, such as the ground and excited state standard reduction potentials of the photocatalyst ( $PC$ ) and  $Q$ , the reorganization energy, and excitation properties. The model is based on three reversible reactions: excitation of the  $PC$ , electron transfer (ET) between  $Q$  and the ground state  $PC$ , ET between  $Q$  and the excited state  $PC^*$  and an irreversible unproductive  $PC^* + Q \rightarrow PC + Q$  step, capturing several key geminate processes. The dependence of  $E_Q$  on the standard ground and excited state reduction potentials of the  $PC$ s shows that photocatalytic performance is strongly influenced by whether the individual ET steps occur in the Marcus normal or inverted regions. The two-dimensional plot of this function reveals the directions in which the standard ground and excited state reduction potentials should be tuned to enhance photocatalytic performance; these directions are often counterintuitive. The model incorporates cage escape, and we show that it can be treated without introducing additional kinetic substeps. An important finding is that none of the input parameters alone can reliably predict photocatalytic efficiency; this also highlights the significance of the proposed measure  $E_Q$ . The model also predicts reduction potential combinations where chemiluminescence is expected. The model is benchmarked against transient and stationary experimental data, demonstrating its ability to recover key kinetic parameters. The model is freely available on GitHub and can be easily extended to incorporate additional processes, making it a versatile tool for qualitative assessment and systematic exploration of emerging photocatalytic strategies.

## Introduction

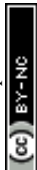
Molecular photoredox catalysis is a continuously growing field in chemistry.<sup>1</sup> Photocatalysis harnesses the increased oxidation and reduction power of the photocatalyst ( $PC$ ) in its excited state formed via absorption of photons, optimally at the visible region. The most common mechanism is the single electron transfer between the excited photocatalyst ( $PC^*$ ) and the reactant or an intermittent quencher ( $Q$ ). It provides radical intermediates to enable a wide range of transformations that are inaccessible or inefficient under conventional conditions.

A large variety of approaches are employed to obtain insight into the mechanism of molecular photocatalysis.<sup>1b,2</sup> The most important methods are time-resolved spectroscopic techniques, particularly transient absorption spectroscopy,<sup>2d,3</sup> electrochemical methods<sup>4</sup> as well as chemical probes (e.g. radical clocks, quenching probes),<sup>5</sup> trapping agents<sup>1c,6</sup> or stoichiometric experiments.<sup>7</sup>

Despite significant advancements in photoredox catalysis, the prediction of reaction rates, selectivity and the influence of system parameters are challenging, as many aspects of the process still remain poorly understood. In fact, photocatalytic efficiency depends on the combined effect of various factors such as the excitation spectrum and the standard ground and excited state reduction potentials of

the  $PC$ , redox properties of the reactant or the quencher, properties of the solvent, as well as on technical details, such as the illumination design (e.g. lamp intensity or the range of the applied wavelengths).<sup>8</sup> The correct way to account for the interplay of these factors is to integrate them into a suitable mechanistic framework and build kinetic models to provide a quantitative overview with predictive power.<sup>1b,9</sup> Most models are developed by applying a combination of steady-state photochemistry, transient laser spectroscopy, electrochemistry and electronic structure calculations to obtain kinetic parameters for a particular type of reaction or  $PC$ . This limitation on scope is due to the complexity of these techniques, especially if time-resolved properties are pursued (see e.g. Ref [10]). In addition, as rate constants are determined by empirical fitting to experimental data, the number of kinetic equations is also limited by data availability, i.e., most side reactions are excluded.

The fundamental equation which must be included in a kinetic model is the electron transfer between the photocatalyst and a quencher or reactant. While it is possible to measure electron transfer rates directly,<sup>11</sup> the use of Marcus theory<sup>12</sup> eliminates the need for advanced experimental techniques while providing molecular level insight. It can also be applied to cage escape, which has

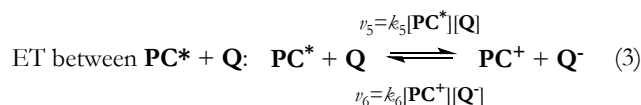
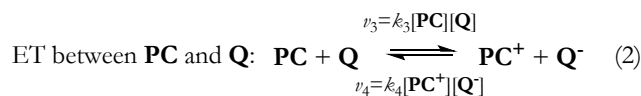
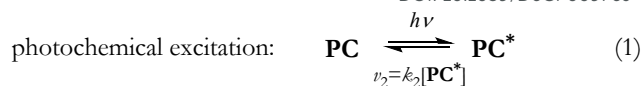


recently become the center of attention.<sup>13</sup> The trends also indicate a shift from one-dimensional approaches — where individual parameters are examined independently — to multi-dimensional frameworks capable of capturing the mutual interdependencies among variables.<sup>14</sup> These models are expected to have higher predictive power for a larger reaction scope. For example, the model of Bloh was developed for heterogeneous catalysis with large emphasis on capturing the effect of light intensity<sup>14</sup> but the same model with some simplifications can also be used for homogeneous catalysis. Interestingly, electron transfer is treated there by a simple rate constant instead of Marcus theory and cage escape is included implicitly through the combined effect of a quantum yield parameter introduced for  $\text{PC}^*$  formation and the recombination rate constant. Recent kinetic studies by Swierk and co-workers have shown that the key excited-state quenching and electron-transfer steps can be captured with compact kinetic schemes that successfully rationalize photocatalytic behavior across full cycles.<sup>1b,2b,2g,15</sup>

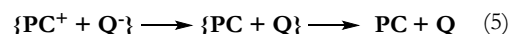
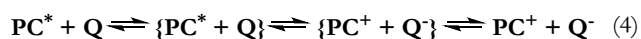
In this study, we aim to develop a general photokinetic model for quantitative prediction of photocatalytic performance. This model is designed to guide the development of new photocatalysts by describing the kinetics of a typical photoredox catalytic sequence. We model the oxidative quenching scenario, where photocatalyst  $\text{PC}$  transfers an electron to quencher  $\text{Q}$  after irradiation. The analogous kinetic model for reductive quenching can be derived in a straightforward manner and the final kinetic equations to solve are the same. The inputs are the initial concentrations of  $\text{PC}$  and  $\text{Q}$  in their ground states in a given solvent, and the intensity of the incoming beam of light.  $\text{Q}$  is characterized by its standard ground state reduction potential, whereas  $\text{PC}$  is characterized by its standard ground state and excited state reduction potentials. The performance of  $\text{PC}$  under standardized conditions is quantified by  $E_Q$ , the steady-state reduction potential of  $\text{Q}$ . In the present scheme the more negative the predicted steady-state reduction potential of  $\text{Q}$  the more powerful the  $\text{PC}$ . We show how the photocatalytically relevant parameters influence the steady-state reduction potential  $E_Q$  and how the model can help identify ways to improve photocatalytic performance. To demonstrate its practical relevance, the model is applied to a set of existing photocatalysts characterized in the literature; and we also show how effectively it can be used to fit kinetic parameters to experimental data.

### Constructing the kinetic model

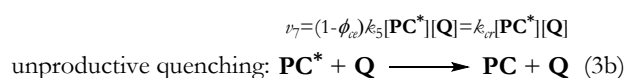
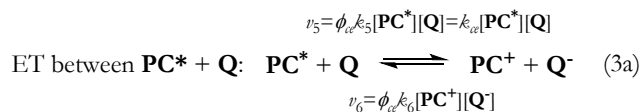
Our kinetic formulation is based on the standard excitation and electron-transfer (ET) steps broadly employed in  $\text{PC}/\text{Q}$  models, e.g. in the analyses of Swierk and co-workers. These steps can be treated as reversible when required by thermodynamic considerations, preserving the conventional model architecture while allowing additional flexibility. Hence the following equations are defined:



The key innovation is the addition of an effective step to capture nonproductive solvent-cage dynamics which prior models treated only implicitly. This assumes that a solvent cage containing an initial encounter complex of  $\text{P}^*$  and  $\text{Q}$  is formed and ET takes place within this cage.<sup>13</sup> Then, the competition between diffusive escape in Eq. 4 and geminate recombination in Eq. 5 determines whether  $\text{Q}^-$  can contribute productively to the subsequent photocatalytic process or  $\text{PC}^+$  and  $\text{Q}^-$  are quenched to  $\text{PC} + \text{Q}$  through back-electron transfer.



Eqs. 4 and 5 can be used to reformulate Eq. 3 into two distinct kinetic equations: one for the reversible ET within the solvent cage, and another for the charge recombination that leads to the ground state reactants but expressed in a way that it represents only the overall process, incorporating several individual steps (for derivation, see SI 1.2, in particular, Fig. S1).



The cage-escape yield ( $\phi_{ce}$ ) parameter represents the efficiency of the formation of separate  $\text{PC}^+$  and  $\text{Q}^-$  and it is defined using the rates of cage escape ( $\nu_5$ ) and geminate charge recombination ( $\nu_7$ ):<sup>13a</sup>

$$\phi_{ce} = \frac{\nu_5}{\nu_5 + \nu_7} = \frac{k_{ce}}{k_{ce} + k_{cr}} \quad (6)$$

The rate equations (1)-(3) yield the time evolution of the concentrations of all species, and at longer time scales the steady-state concentrations. The concentrations can be used to calculate reduction potentials via the Nernst equation as shown by Eq 7 using quencher  $\text{Q}$  as an example:

$$E_Q = E_Q^0 + \frac{RT}{zF} \ln \left( \frac{[\text{Q}]}{[\text{Q}^-]} \right) \quad (7)$$

where  $E_Q$  is the reduction potential,  $E_Q^0$  is the standard reduction potential of  $\text{Q}$ ,  $R$  is the universal gas constant,  $T$  is the temperature,  $z$  is the number of electrons transferred (in our case  $z = 1$ ) and  $F$  is the Faraday constant. The usefulness of  $E_Q$  is seen from its connection to the Nernst



equation and specifically its direct dependence on the ratio  $[Q]/[Q^*]$ : it provides a direct measure of how effectively the targeted electron transfer from **PC** to **Q** is achieved under the given conditions.

The standard free energy of an ET reaction can be determined from the difference of the standard reduction potentials of the oxidant and the reductant:

$$\Delta G_0 = -zF\Delta E_0 \quad (8a)$$

$$\Delta G_0^* = -zF\Delta E_0^* \quad (8b)$$

where  $\Delta E_0$  and  $\Delta E_0^*$  are the standard reduction potential differences for Eq. 2 and 3, respectively; whereas  $\Delta G_0$  and  $\Delta G_0^*$  are the corresponding standard free energy differences. The rate constants for ET are obtained using transition state theory:

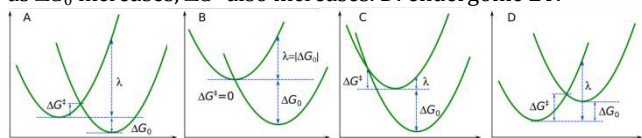
$$k = \frac{k_B T}{h c^\ominus} \exp\left(-\frac{\Delta G^\ddagger}{RT}\right) \quad (9)$$

where  $k_B$  and  $h$  are the Boltzmann and Planck constants, respectively,  $c^\ominus$  is the standard concentration (1.0 mol/l),  $\Delta G^\ddagger$  is the barrier of the ET. The preexponential is written in the Eyring formulation which implies the assumption of strong electronic coupling between the donor and acceptor states (adiabatic regime). This way the preexponential that is derived from Marcus theory is simplified,<sup>12</sup> see further discussion in SI (1.1). For the barrier, the Marcus expression for outer sphere ET is used:  $\Delta G^\ddagger$  is calculated from the free energy change ( $\Delta G_0$ ) of the actual ET and the reorganization energy  $\lambda$  of the system:

$$\Delta G^\ddagger = \frac{(\lambda + \Delta G_0)^2}{4\lambda} \quad (10)$$

Note that for the barrier of the reverse electron transfer the sign of  $\Delta G_0$  in Eq 10 is negative. This formula is also valid for ET from an excited state with  $\Delta G_0^*$  in the formula. Scheme 1 depicts illustrative examples of ETs in terms of free energy profiles, reorganization and activation energies.

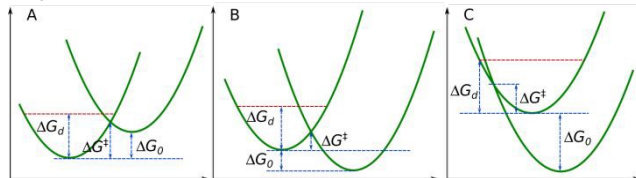
**Scheme 1.** Typical ET scenarios for electron transfer from state left to state right in terms of free energy profiles. The reorganization energy  $\lambda$  is shown for each scenario. A: exergonic ET; as reaction free energy  $\Delta G_0$  increases barrier  $\Delta G^\ddagger$  decreases. B: ideal case when  $\Delta G^\ddagger$  vanishes implying ultrafast ET and very large ET rate constant. C: Marcus inverted region, as  $\Delta G_0$  increases,  $\Delta G^\ddagger$  also increases. D: endergonic ET.



Note that there is an upper limit for bimolecular rate coefficients, namely the diffusion-limited rate constant, typically of order  $10^{10} \text{ M}^{-1} \text{ s}^{-1}$  in solution.<sup>16</sup> Equivalently, the activation barrier of ET cannot be lower than the barrier associated with diffusion ( $\Delta G_d$ ). This condition is built into our kinetic model: all ET rate coefficients are constrained not to be higher than the diffusion limit, i.e., we set the diffusion barrier as the lower bound for the activation barriers. This is visualized in Scheme 2. Details of the implementation of this condition are given in the SI.

There is a range of reaction free energies for a given  $\lambda$  which leads to diffusion control. The upper and lower bounds for this range of  $\Delta G_0$  values can be estimated by solving Eq. 10 where  $\Delta G^\ddagger$  is replaced with  $\Delta G_d$ . Equivalently, employing Eqs. 8 we can describe the diffusion-controlled region using a reduction potential range: within this range the rate of electron transfer is constant (see SI, Fig. S2 for details). It is clear that diffusion control can occur for both endergonic (Scheme 2, A) and exergonic (Scheme 2, B, C) ETs.

**Scheme 2.** Free energy profiles illustrating endergonic (A) and exergonic ET processes (B, C) where the Marcus model predicts smaller barrier for ET ( $\Delta G^\ddagger$ ) than the diffusion limit ( $\Delta G_d$ , red dashed line). Under these circumstances the ET occurs in the diffusion-controlled limit within a range of reaction free energy  $\Delta G_0$ .



The steady state established in our photocatalytic model system is due to the constant photon flow from the lamp. For a monochromatic lamp having a given effective power the volumetric photon radiation ( $I_p$ , the number of photons entering a unit volume of the system per unit time, i.e., the rate of the photon flux) can be estimated (see SI, 1.4). The rate of photon absorbance ( $I_a$ , the rate of the production of **PC\***) can then be estimated by the following equation obtained from the Beer-Lambert law:

$$I_a \approx I_p(1 - 10^{-\bar{\epsilon}[\text{PC}]l}) \quad (11)$$

where  $\bar{\epsilon}$  is the mean or effective absorption coefficient of **PC** in the narrow frequency region emitted by the lamp and  $l$  is the path length of the light in the catalytic system. (See SI, 1.5. for the derivations.) Therefore, an effective rate coefficient  $k_1$  can be derived from the following equation:

$$I_a = k_1[\text{PC}] \quad (12)$$

i.e., by dividing  $I_a$  with the instantaneous concentration of **PC**. Note that  $k_1$  depends on  $[\text{PC}]$  and thus on reaction time  $t$ . Another important approximation is using  $I_a$  in place of the true  $\nu_1$ . This assumes a quantum yield of unity for the population of the photoactive excited state. Note however, that we have evaluated the impact of this approximation by varying  $I_a$  through changes in the mean absorption coefficient; further discussion is provided in the Results section.

**PC\*** participates in ET according to Eq. 3, but it can also spontaneously relax to **PC** following first order kinetics (Eq. 1, backward). The corresponding rate constant  $k_2$  can be derived from the lifetime ( $\tau$ ) of the excited state:  $k_2 = \tau^{-1}$ . We use a default value of 10 ns in the simulations as it is a typical value for organic photocatalysts<sup>1c</sup>, but we also explore the effect of changing  $\tau$  in a dedicated section in Results. By following the time evolution of the concentrations, the steady-state properties (such as  $E_Q$ ) can be determined for arbitrary sets of parameters (standard ground and excited state reduction potentials, absorption coefficient, lamp



intensity, solvent parameters, such as  $\lambda$  and diffusion barrier, cage-escape yield, lifetime of the excited state). Optimizing photocatalyst selection requires a systematic study of how these parameters influence the photocatalytic performance measured by the steady-state reduction potential  $E_Q$ . Our strategy is the following: we define practically relevant ranges for the parameters, and study how the systematic variation of the parameters affects photocatalytic activity. Note that more sophisticated mathematical procedures are available to explore the effects of multiple parameters, such as dimensionality reduction methods (e.g. principal component analysis, partial least squares regression, etc.) or other methods such as Response Surface Methodology.<sup>17</sup> However, the results indicate that a one-by-one analysis is sufficient to understand the relevant dependencies. These findings can help to identify effective photocatalysts for given experimental conditions.

As all **PCs** are characterized by their ground state and excited state standard reduction potentials, we consider  $E_Q$  as the 2D function of these two quantities ( $E_Q(E_{PC}^0, E_{PC^*}^0)$ ). Then we systematically study how the variation of other parameters affects this 2D function. Specifically, we seek the region where  $E_Q$  reaches its minimum (most negative) value, corresponding to the optimal photocatalytic performance. To that end, we define photocatalytically relevant ranges for  $E_{PC}^0$  and  $E_{PC^*}^0$  based on the following observation: for a given quencher **Q** with standard reduction potential  $E_Q^0$ , a suitable **PC** cannot have arbitrary  $E_{PC}^0$ . The fact that **PC** does not spontaneously reduce **Q** (otherwise we would not use light for the activation) implies that ET must be very limited between **PC** and **Q**. Assuming that at most 1% [Q<sup>-</sup>] is present when **PC** and **Q** are together without light, we can derive the following expression (the derivation is given in SI, 1.6.):

$$E_{PC}^0 > E_Q^0 + 0.35V \quad (13)$$

Regarding  $E_{PC^*}^0$  we can identify the following constraints. For a reductant **PC**, oxidation of **PC**<sup>\*</sup> is energetically more favorable than that of **PC**, hence  $E_{PC^*}^0 < E_{PC}^0$ . This can be further improved based on their relationship:<sup>1c,18</sup>

$$E_{PC^*}^0 = E_{PC}^0 - \varepsilon_{0,0}/F \quad (14)$$

where  $\varepsilon_{0,0}$  is the 0-0 transition energy between the relevant excited and ground states. However, there are two common excited states: the  $S_1$  and the  $T_1$  states. The ground state of most organic photocatalysts is singlet so light absorption initially yields the  $S_1$  state after ultrafast relaxation from higher singlet states.  $S_1$  can remain the photocatalytically active state if the main relaxation pathway is fluorescence (i.e., fluorescence quantum yield near 1) with lifetime around 10 ns.<sup>1c</sup> Such **PCs** are in high demand as they can offer exceptional reductive (or oxidative) power due to their large  $\varepsilon_{0,0}$ . Note that for **PCs** with  $S_1$  lifetimes in the 1-10 ns range a relatively large quencher concentration is required to obtain reasonable reaction rates. **PCs** with longer-lived  $T_1$  active states allow for lower reactant concentrations. Transition metal catalysts are the typical choice here, but benzophenone derivatives or more recently the targeted design of BODIPY dyes are also a

prime example.<sup>19</sup> Our model applies to all active states, irrespective of the nature of the **PC**, but the correct ( $S_1$  or  $T_1$ )  $\varepsilon_{0,0}$  energy of the photocatalyst must be specified to determine the excited state reduction potential. As we focus on absorption in the visible range, the lower and upper bounds on the reduction potential of **PC**<sup>\*</sup> can be conveniently defined. Regarding the upper bound, a conservative estimation for  $\varepsilon_{0,0}/F$  is 1.0 V, i.e.  $E_{PC^*}^0 \leq E_{PC}^0 - 1V$ ; because  $\varepsilon_{0,0}$  is located at lower energy than the lowest-energy absorption observed in the spectrum. A plausible lower bound can be set by taking 4.1 eV as the higher energy limit: this sets 300 nm as the lower bound for the 0-0 transition a visible light photocatalyst can have. Hence the range we consider for the excited state reduction potential is:

$$E_{PC}^0 - 4.1V \leq E_{PC^*}^0 \leq E_{PC}^0 - 1V \quad (15)$$

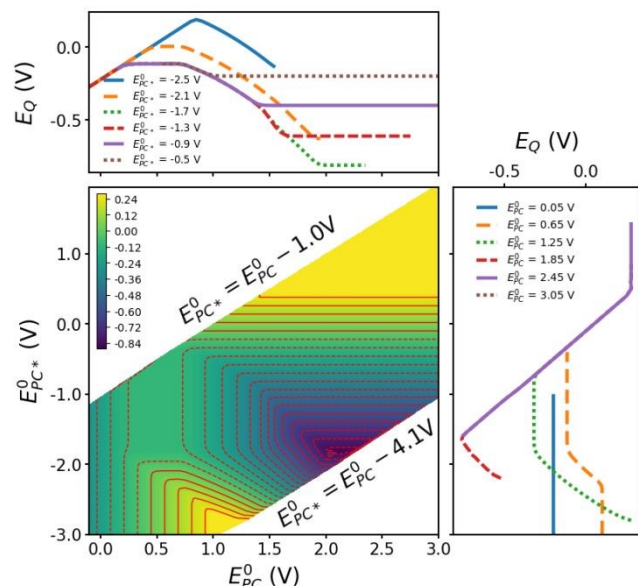
With these constraints, we can set the relevant regions of the reduction potentials, taking also into account the practically accessible range of the ground state reduction potentials of the photocatalysts and quenchers. (For reductive quenching the derivation can be found in the SI, 1.7.) We can also notice that the rate coefficients of all the ETs depend only on reduction potential differences, hence either  $E_{PC}^0$  or  $E_Q^0$  can be fixed and the other reduction potential as well as  $E_{PC^*}^0$  can be varied relative to the fixed potential. This is a useful observation because one less parameter is involved in the analysis. The conclusions are transferable to other situations where the differences in reduction potentials are the same. For example, in our analysis  $E_Q^0$  is fixed at -0.45V (with respect to SCE) to represent moderate oxidative power. Evidently, for another quencher with a different  $E_Q^0$  value the photocatalytically relevant ranges of  $E_{PC}^0$  and  $E_{PC^*}^0$  are redefined by Eqs. 13-15.

### Computational details

The kinetic modelling is carried out using the COPASI microkinetic software<sup>20</sup>. The time evolution of the reactions constituting Eqs 1-3 is followed. The initial concentration of **PC** and **Q** is 1 M. The rate of the forward reaction of Eq. 1 is given by Eq. 11. The backward rate, i.e., the spontaneous relaxation of the excited state of **PC**<sup>\*</sup> (comprising various possible channels, such as fluorescence or thermal decay) is set to  $1 \cdot 10^8$  1/s but variation of this value is also tested.<sup>21</sup> Rate coefficients  $k_3$ - $k_6$  are derived using Eq. 6. The instantaneous rates are calculated by the corresponding rate equations using the instantaneous concentrations. The activation barriers are determined using Eq. 10 assuming uniform  $\lambda$  for each step. To reach steady state we used  $10^8$  s for simulation time; we note that shorter simulation time is sufficient in most cases (see SI, Figs S3, S4). The reaction free energies in Eq. 10 are computed from the relevant standard reduction potentials using Eq. 8. The default parameter values were selected either as midpoints within their feasible ranges or to reflect typical experimental conditions. Additional details of the kinetic modelling are available in the SI and in the files uploaded on [github.com/acsstirling/photokinetics](https://github.com/acsstirling/photokinetics).

### Results





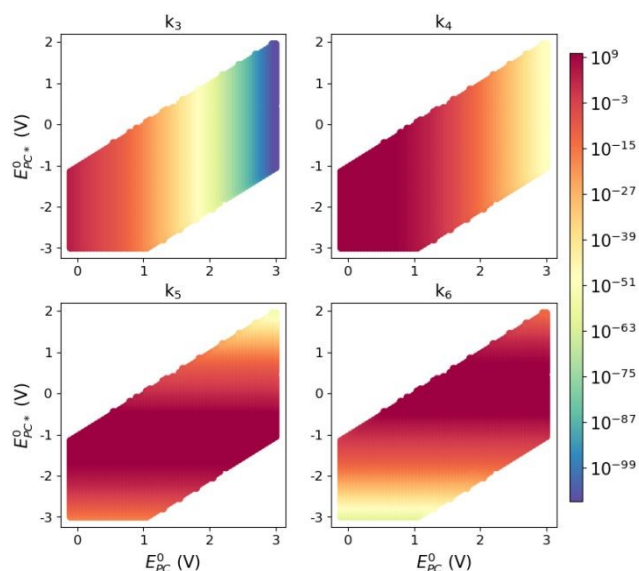
**Figure 1.**  $E_Q$  (V) as a function of  $E_{PC}^0$  and  $E_{PC}^{0*}$  when  $E_Q^0 = -0.45$  V. The side graphs show slices at constant values of  $E_{PC}^{0*}$  (top) and  $E_{PC}^0$  (right). The red contour lines are separated by 0.02 V. Concentration values of  $[Q^-]$  and  $[PC^*]$  smaller than  $5 \cdot 10^{-13}$  mol/l were set to this threshold for generating the  $E_Q$  distribution. Other parameters were kept at the following values:  $\phi_{ce}=1$ ;  $I_p = 0.0564$  mol dm $^{-3}$  s $^{-1}$ ;  $\bar{\epsilon} = 0.1$  m $^2$  mol $^{-1}$ ;  $\lambda = 0.564$  eV;  $\Delta G_d = 0.166$  eV;  $\tau = 1 \cdot 10^8$  s $^{-1}$ .

The principal quantity we are interested in is the value of  $E_Q$  (the steady-state reduction potential of **Q**) as a function of  $E_{PC}^0$  and  $E_{PC}^{0*}$ . As we consider oxidative quenching where **PC** is the reducing agent, lower  $E_Q$  values indicate stronger reduction power for the **PC**, so we seek parameter combinations that minimize  $E_Q$ . Figure 1 shows  $E_Q$ , as the function of  $E_{PC}^0$  and  $E_{PC}^{0*}$  when the other photocatalytic parameters (such as  $E_Q^0$ ,  $\lambda$ , lamp intensity, cage-effect yield, etc.) are fixed. In particular, cage-escape yield  $\phi_{ce}$  is set to 1, i.e., we assume that nonproductive recombination (Eq. 3b) does not take place. The effect of  $\phi_{ce}$  is presented later. The values of  $E_Q$  exhibit a very peculiar pattern: for specific values of  $E_{PC}^{0*}$ ,  $E_Q$  remains constant over a wide range of  $E_{PC}^0$  as shown by the straight horizontal contour lines; and the same behavior is seen for selected  $E_{PC}^0$  values, where  $E_Q$  remains constant along an interval of  $E_{PC}^{0*}$ . The ideal **PCs** that yield the lowest  $E_Q$  of  $-0.86$  V under the conditions defined by the other parameters are those featuring  $E_{PC}^0 \approx 2.1$  V and  $E_{PC}^{0*} \approx -1.8$  V.

The variation of  $E_{PC}^0$  and  $E_{PC}^{0*}$  within their respective ranges can induce huge changes (tens of orders of magnitude) in the rate constants, due to their exponential dependence on the free energy barriers as shown in Figure 2. This is key to understanding the observed variation patterns of  $E_Q$  in Fig. 1. We first consider the relative magnitudes of the rate constants under steady-state conditions.  $k_1$  (the effective rate constant of the production of **PC\***) is of order  $10^{10}$  s $^{-1}$  (obtained from Eq. 12). The annihilation of the excited state by relaxation to the ground state is a fast process, a typical value of  $k_2$  is  $10^8$  s $^{-1}$ .<sup>21</sup> Figure 2 displays the variation of  $k_3$ ,

$k_4$ ,  $k_5$  and  $k_6$  (see Eqs. 2 and 3) as the function of  $E_{PC}^0$  and  $E_{PC}^{0*}$  when  $E_Q^0$  is set to  $-0.45$  V. In this case  $k_3$  and  $k_4$  are determined solely by  $E_{PC}^0$ , whereas  $k_5$  and  $k_6$  are determined solely by  $E_{PC}^{0*}$  as indicated by the vertical and horizontal contours, respectively. For both  $k_3$  and  $k_4$  we can see an exponential decrease with increasing  $E_{PC}^0$  corresponding to scenarios depicted on Scheme 1A and 1D, respectively. In contrast, it is seen that as  $E_{PC}^{0*}$  becomes more negative,  $k_5$  first increases until diffusion control and remains constant within an interval of 1.15 V; then, in the Marcus inverted region, it starts to decrease below diffusion control around  $-1.65$  V. The same pattern is seen for  $k_6$ : as  $E_{PC}^{0*}$  increases, it first increases reaching the diffusion rate at  $E_{PC}^{0*} = 0.45$  V; then above 0.75 V it departs from the diffusion-controlled regime within the Marcus inverted region and starts to decrease. Note that in their seminal study Rehm and Weller showed the lack of the inverted region for selected bimolecular reactions.<sup>22</sup> Later however the existence of the inverted region for bimolecular reactions has been conclusively demonstrated.<sup>23</sup>

A closer inspection of the rate landscape (Figure 2) shows that in the region where  $E_{PC}^{0*}$  lies above roughly  $-1$  V while  $E_{PC}^0$  shifts toward strongly positive values ( $\approx +1.5$  V and beyond), the backward electron-transfer pathway leading to **PC\*** ( $k_6$ ) becomes markedly more favorable than the corresponding path regenerating **PC** ( $k_4$ ). In this domain, recombination of **PC\*** and  $Q^-$  can directly populate the excited state even in the absence of photoexcitation, consistent with known chemiluminescent and electrochemiluminescent mechanisms.<sup>24</sup> A classic example is the  $Ru(bpy)_3^{2+}$  system, where back electron transfer produces the emissive excited state.<sup>25</sup>



**Figure 2.** Calculated rate constants (mol/l/s) of equations 2 and 3 as the functions of  $E_{PC}^0$  and  $E_{PC}^{0*}$  when  $E_Q^0 = -0.45$  V,  $I_p = 0.0564$  M s $^{-1}$ ;  $\bar{\epsilon} = 0.1$  m $^2$  mol $^{-1}$ ;  $\lambda = 0.564$  eV;  $\Delta G_d = 0.166$  eV;  $\tau = 1 \cdot 10^8$  s $^{-1}$ . Coloring is logarithmic. The largest values (dark red regions) are of order  $10^{10}$  M $^{-1}$  s $^{-1}$ , corresponding to diffusion control. It is seen that since the rate constants are obtained from Eq. 9, they depend strictly on either  $E_{PC}^0$  or  $E_{PC}^{0*}$ .

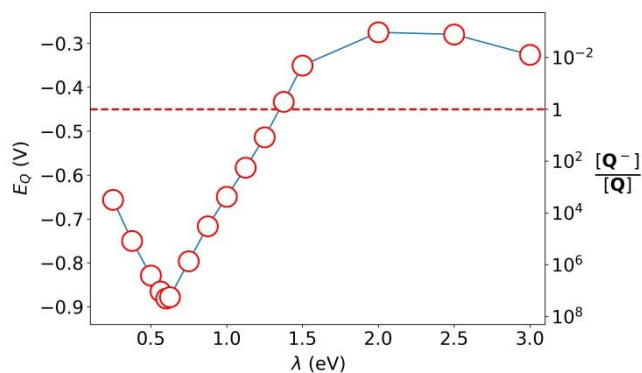


Interplay between the forward and backward rates of Eqs. 2 and 3 governs the equilibrium ratio  $[Q^-]/[Q]$  and thus  $E_Q$ . The specific patterns (straight contours) seen on Figure 1 can be understood by identifying the actual source of  $[Q^-]$  at a given  $E_{PC}^0 - E_{PC^*}^0$  pair. Horizontal contours indicate that reaction 2 has negligible role in producing and consuming  $Q^-$ , whereas vertical contours point to the negligible role of excitation. For example, the vertical contours on the left side of Figure 1 signal that the actual  $E_Q$  is higher than  $E_Q^0$  ( $-0.28$  eV when  $E_{PC}^0 = -0.1$  eV and it increases as  $E_{PC}^0$  increases), i.e.,  $[Q^-]$  is order of magnitudes smaller than  $[Q]$ . In this region reaction 2 is the main source of  $Q^-$ , both the forward and backward rates ( $v_3$  and  $v_4$ ) are significantly higher than the rates of Eqs. 1 and 3 (see SI, Figs. S5 and S6 for the actual values). For larger values of  $E_{PC}^0$ ,  $v_3$  and  $v_4$  rapidly become very small and reaction 3 becomes the main source of  $Q^-$ . The local maximum plateau at  $E_Q = -0.12$  eV indicates a shift in the relative importance of reactions 2 and 3. In particular, it is crucial that  $v_4$  diminishes significantly as this allows the accumulation of  $Q^-$ . In contrast, around the minimum region of  $E_Q$ ,  $Q^-$  is dominantly formed via reaction 3. In this region  $[Q^-]$  is orders of magnitude higher than  $[Q]$  yielding  $E_Q$  potentials far more negative than  $E_Q^0$ . In this region the largest rates are those of the photoexcitation and deexcitation, followed by the rate of the photoredox production of  $[Q^-]$  and the backward ET in reaction 2 (see SI, Figs. S5-S7 for the plots). The other rates are orders of magnitude smaller in this region. Along the rest of the contours both the ground and excited states play equally important roles in determining  $E_Q$ .

### Effect of the reorganization energy

A crucial parameter affecting the performance of a photocatalyst is the reorganization energy ( $\lambda$ ) in the actual solvent. Reorganization energy  $\lambda$  can be expressed as the sum of two terms:  $\lambda = \lambda_i + \lambda_s$ ; where  $\lambda_i$  arises from the structural changes of the solvated reactants to match the structure of the products at the moment the ET takes place; the other term  $\lambda_s$  is the energy required for the accompanying solvent rearrangements. The significance of dividing the reorganization energy into two components is that they impact photocatalytic efficiency differently:  $\lambda_i$  is large, when ET requires significant structural changes, such as when ET gives rise to Jahn-Teller distortion;<sup>26</sup> however this is not typical in most situations, and solvent contribution  $\lambda_s$  is the dominant.<sup>13a,27,28</sup> Eqs. 9 and 10 indicate complicated nonlinear relation between  $\lambda$  and the ET rates.<sup>29</sup> As the rates also depend on the  $\Delta G_0$  free energies of the ETs, the final  $E_Q$  is very difficult to predict in advance (see SI, Fig. S2 for illustrative plots). This dependence implies that  $\Delta G^\ddagger$  is minimal if  $\lambda = |\Delta G_0|$ ; for either larger or smaller  $\lambda$  values the activation barrier increases, i.e. the rate of ET continuously decreases (note that this effect is masked in the diffusion-controlled region, see earlier discussion). As the  $\Delta G_0$ -s of the ET-s depend on  $E_{PC}^0$  or  $E_{PC^*}^0$  (see eqs. 8a and 8b), the changes in the ET rates brought by variation in  $\lambda$  can be very diverse. We have performed the same simulation discussed for Figure 1 considering a wide range of relevant  $\lambda$  values and determined the optimal (lowest)  $E_Q$  for each  $\lambda$ . The results are plotted on Figure 3.

The individual plots (analogous to that of Figure 2) are in the SI, Fig. S8.



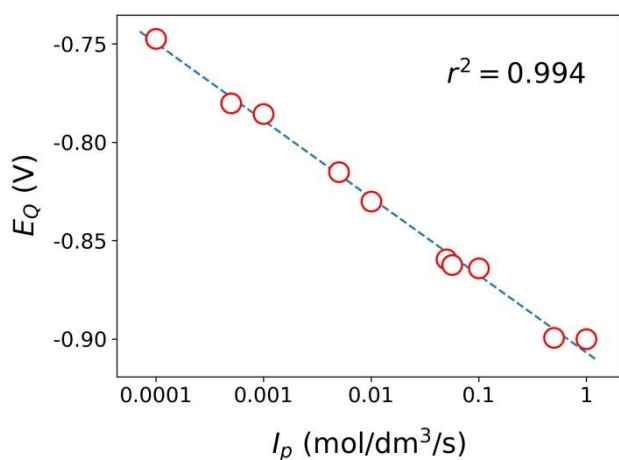
**Figure 3.** Optimal  $E_Q$  as a function of the reorganization energy  $\lambda$ . The right axis indicates the corresponding concentration ratio of the reduced and oxidized form of  $Q$ . The dashed horizontal line indicates the standard reduction potential  $E_Q^0$  of  $Q$  ( $-0.45$  V, when  $[Q] = [Q^-]$ ). Variation of  $\lambda$  has been carried out with the same parameter setup as for Figure 2. The lowest  $E_Q$  ( $-0.88$  V) is obtained at  $\lambda = 0.58$  eV. The blue line is a guide to the eye.

Figure 3 clearly shows that large reorganization energies are detrimental to photocatalytic activity. In fact, above  $\lambda = 1.4$  eV, the photocatalysts become ineffective as  $E_Q$  is above  $E_Q^0$  (i.e.,  $[Q^-] < [Q]$ ). In contrast, we can find an ideal  $\lambda$  where the strongest possible reductive power can be obtained under the given conditions. Looking at the underlying 2D plots for each point in Fig. 3 (see SI, Fig. S7) we can infer that as  $\lambda$  increases, the position of the optimal  $E_Q$  shifts toward larger values of  $E_{PC}^0$ , beyond the photocatalytically relevant domain (to regions where the excitation of  $PC$  requires UV energy). It is also seen that as  $\lambda$  increases, the relevant  $E_{PC}^0 - E_{PC^*}^0$  domain features a larger region where their variations do not affect the steady-state  $E_Q$  value. This is related to the fact that larger  $\lambda$  results in broader reduction potential ranges where the rate of ET is diffusion controlled (see SI, eq. 15). This implies that higher  $\lambda$  leads to stronger leveling effects and an overall adverse impact on the catalytic efficiency of visible-light photocatalysts. Specifically, employing a solvent where  $\lambda$  is more than 1 eV larger than its optimal value for a given  $PC - Q$  pair, less than half of  $Q$  can be reduced under the given circumstances. For small reorganization energies the efficiency again decreases, the optimal  $E_Q$  values are less negative. This is related to the fact that for small  $\lambda$  values the rate constants for most  $E_{PC}^0 - E_{PC^*}^0$  pairs are smaller. It is also seen that around the optimal reorganization energies, a change of 0.5 eV in  $\lambda$  results in a decrease of  $\sim 0.2$  V in  $E_Q$ . This is a significant change that highlights the importance of the reorganization energy for photocatalysis. From a practical point of view, it shows that the solvent selection strategy for photocatalysis must carefully consider reorganization energy. Also note that in real-world applications the choice of the solvent affects the value of not only  $\lambda$  but also  $E_{PC}^0$  and  $E_{PC^*}^0$ .

### Effect of the intensity of the lamp



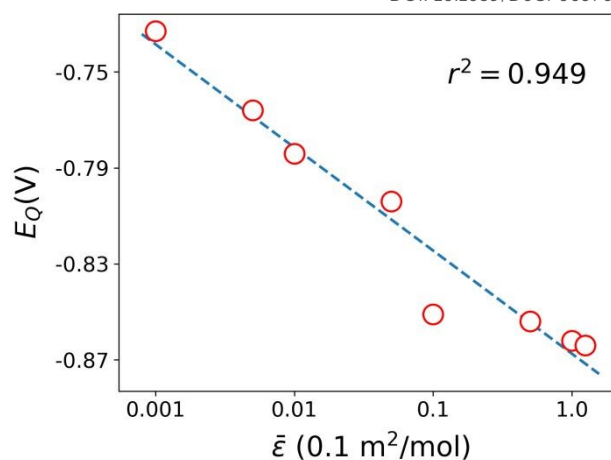
The effect of lamp intensity is straightforward as seen in Figure 4. The stronger the light intensity  $I_p$  the more effective the photocatalyst is in terms of reduction power. Note that the  $E_{PC}^0 - E_{PC^*}^0$  pair that characterizes the optimal PCs (i.e., where  $E_Q$  is minimal) remains in the same region, indicating that its dependence on the light intensity is marginal (see SI, Fig. S9). The slope of the line is -39 mV, i.e. it is close to the ideal Nernstian slope (59 mV). This suggests that the observed trend is partly governed by Nernst-type behavior; however, the deviation from the ideal value points to additional kinetic and transport effects, and no simple analytical relationship could be identified. It follows that orders of magnitude change in the intensity results in fractions of eV change in the reduction potential. The model therefore suggests that lamp intensity is not the primary factor to consider for improving photocatalytic performance. In turn, only a significant loss of intensity can lead to an observable loss of steady-state performance, as far as the light setup is concerned.



**Figure 4.** Optimal  $E_Q$  (V) as a function of the photon intensity of the illuminating lamp ( $I_p$ ). The horizontal scale is logarithmic. The dashed blue line is the linear regression fit to the data.

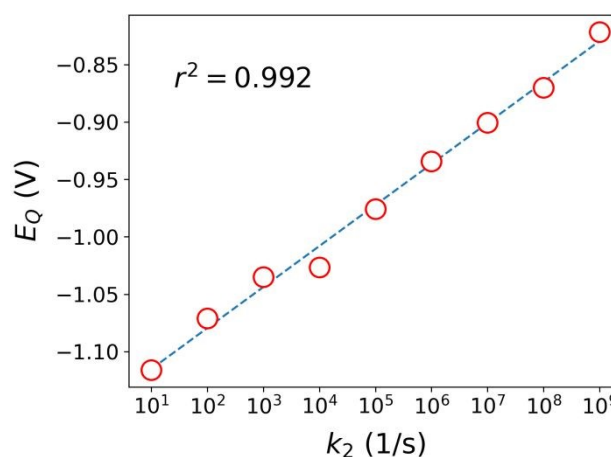
#### Effect of the mean absorption coefficient of the PC

Another important property related to the activity of a PC is its mean absorption coefficient ( $\bar{\epsilon}$ ) in the frequency region of the illuminating light. The exponential dependence of the absorbed light on  $\bar{\epsilon}$  translates to a near linear dependence of the optimal  $E_Q$  on the logarithm of  $\bar{\epsilon}$  as seen in Figure 5 (slope is -43 mV). Similarly to the case of light intensity, if the other parameters are fixed, then changes in the optimal  $E_{PC}^0 - E_{PC^*}^0$  values are minimal when  $\bar{\epsilon}$  is varied (see Fig. S10 for the corresponding plots). Indeed, we can see that three orders of magnitude change in  $\bar{\epsilon}$  results in only a  $\sim 0.1$  V change in the optimal reduction potential.



**Figure 5.** Optimal  $E_Q$  (V) as a function of the effective absorption coefficient of the PC. The horizontal scale is logarithmic. The dashed blue line is the linear regression fit to the data.

#### Effect of the excited state lifetime



**Figure 6.** Optimal  $E_Q$  (V) as a function of  $k_2$  (i.e., the inverse of the lifetime ( $\tau$ ) of  $PC^*$ ) when the rate of diffusion is  $1 \cdot 10^{10}$  l/mol/s. The horizontal scale is logarithmic. The dashed blue line is the linear regression fit to the data.

The lifetime of the excited state of the photocatalysts ( $\tau$ ) is the crucial timescale defining how long the catalyst remains in its active state. For higher efficiency, this lifetime should be longer than the diffusion-controlled timescale to ensure reactive encounters. PCs with triplet active states usually satisfy this condition which is the reason why transition-metal photocatalysts are widely employed in photocatalysis.<sup>30</sup> The design of organic PCs is evidently more challenging for this reason, however, there are already several scaffolds like cyanoarene, acridinium, phenazine, etc. that offer either a longer-lived active  $S_1$  state, access to higher lying triplets or even super reducing excited radicals.<sup>1a</sup> Note that this does not mean that PCs with short lifetimes cannot react. To compare the timescales of diffusion and fluorescence decay, the diffusion rate constant first needs to be converted to effective first order using  $k_{eff} = k_d[Q]$  so it can be compared to  $k_2$  (we can do this because  $[Q] \gg [PC^*]$ ). This implies that promoting the probability of collisions by increasing the initial

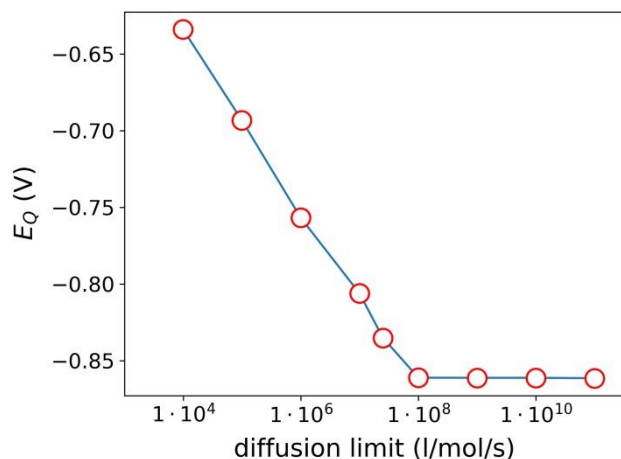


concentrations of the reactants (preferably **Q**), **PC**s with short lifetimes can also be effective. Also note that while  $\tau$  has an important limiting effect, this parameter alone is not a reliable predictor of photocatalytic activity.<sup>31</sup>

Our simulations indicate that  $\tau$  and equivalently the rate constant of deexcitation of **PC\*** has again a straightforward effect on the strongest attainable reduction potential when the other parameters are fixed: the longer the lifetime (i.e., the smaller the corresponding annihilation rate constant  $k_2$ ) the deeper the optimal potential is as shown by Figure 6 (full plots are in SI, Fig. S11). Indeed, longer excited state lifetimes yield larger **PC\*** concentrations which in turn result in concentration increase for **Q**<sup>-</sup>. The linearity on the logarithmic  $k_2$  scale (slope is 36 mV) is again related to the logarithmic dependence of the reduction potential on concentrations via the Nernst equation.

### Effect of the diffusion-controlled rate

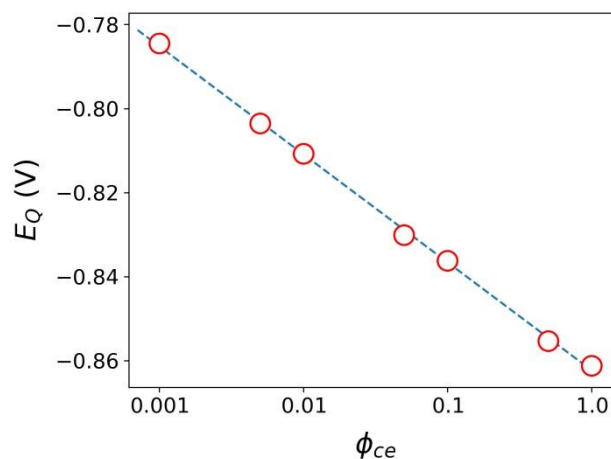
An important factor that influences the optimal reduction potential  $E_Q$  is the maximal possible rate of the reaction steps. For the ET steps this rate is the diffusion-controlled rate. The rate constant of diffusion ( $k_D$ ) can be given in typical situations under reasonable assumptions (such as neutral reactants and similar sizes; see Ref. 16):  $k_D = 8k_B T / 3\eta$ , where  $\eta$  is the viscosity of the solvent. Clearly, as viscosities do not have orders of magnitude differences for typical solvents, the diffusion limit predicted by the above equation varies in a small range. However, when long range interactions are important, such as when charged species are involved, then the previous formula is not valid and  $k_D$  can change significantly.<sup>16,32</sup> We therefore set the range of the diffusion-controlled rate constant considered here to span 7 orders of magnitude (from  $1 \cdot 10^4$  to  $1 \cdot 10^{11}$  l/mol/s) and determined the optimal  $E_Q$ , when the other parameters were unchanged. We can see in Figure 7 (full plots are in SI, Fig. S12) that departure from the typical diffusion-controlled limit ( $\sim 10^{10}$  l/mol/s) starts to influence the performance below the threshold of  $10^8$  l/mol/s (with a slope of  $-55$  mV). From this value onwards the diffusion-controlled rate is smaller than the deexcitation rate hence the formation of **Q**<sup>-</sup> is suppressed. Indeed,  $k_2$  can be decreased to compensate for the effect of the decreasing diffusion rate (see SI, S13). This is in accord with our observations that a longer lifetime for **PC\*** results in better  $E_Q$  (i.e. more negative; see Figure 6).



**Figure 7.** Optimal  $E_Q$  (V) as a function of the diffusion-controlled rate constant when  $k_2 = 10^8$  1/s. The horizontal scale is logarithmic. The blue line is drawn to guide the eye.

### Effect of cage-escape yield $\phi_{ce}$

We have performed kinetic simulations with various  $\phi_{ce}$  values. Figure 8 shows how the optimal  $E_Q$  obtained under steady-state conditions depends on  $\phi_{ce}$ . Clearly, as shown in Figure 8 the magnitude of  $E_Q$  decreases with decreasing  $\phi_{ce}$  exhibiting a linear dependence when plotted as a function of  $\log(\phi_{ce})$ . We can also see that under steady-state conditions, the photocatalytic process approaches the optimal performance even for smaller  $\phi_{ce}$  values.

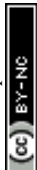


**Figure 8.** Optimal  $E_Q$  (V) as a function of the cage-effect yield under steady-state conditions. The linear regression line is dashed blue. The horizontal scale is logarithmic.

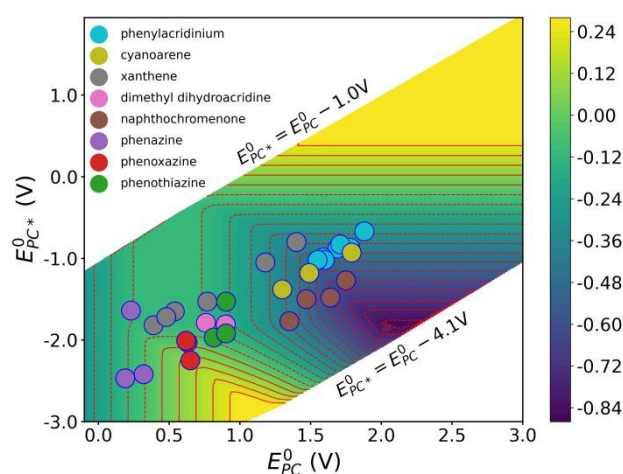
### Discussion

Kinetic modelling offers significant utility in catalysis;<sup>33</sup> it can help understand the effect of the various parameters that define a photocatalytic setup and it can identify the optimal photocatalysts for that particular setup. As an example, Figure 9 displays the distribution of selected photocatalysts as a function of their  $E_{PC}^0$  and  $E_{PC^*}^0$  values projected onto the computed  $E_Q$  surface. Note that displaying a set of photocatalysts on the same plot assumes identical reorganization energies, cage-effect yields, excited-state lifetimes, and absorption properties, all measured in the solvent associated with the plot. Still, the distribution in the figure clearly shows that the different photocatalysts form well-defined groups based on their core structures.

The contour patterns seen for specific regions in Figure 1 and the distribution of the photocatalysts represented by the colored circles on Figure 9 give pragmatic hints for achieving higher photocatalytic efficiencies. First, it is quite clear that the compounds with the same scaffold form well-defined clusters on the plot indicating that the role of the side chains is more about fine-tuning. (Note, that independent tuning of  $E_{PC}^0$  and  $E_{PC^*}^0$  in practice may not be possible, as both are inherently linked to the molecular structure.) Horizontal contours imply that strategic



modifications of a PC affect  $E_Q$  only via the induced variations in its  $E_{PC^*}^0$  but changes in  $E_{PC}^0$  has no effect along the horizontal contours. Vertical contours imply the same perspective but swapping the role of  $E_{PC^*}^0$  and  $E_{PC}^0$ . This, in turn, signifies design flexibility, as the straight vertical and horizontal contours indicate that in those regions, variations in the corresponding reduction potential do not affect the photocatalytic potential. In particular, the vertical contour pattern at the region  $1.0V \leq E_{PC^*}^0 \leq 1.6V$  suggests a counterintuitive strategy to improve the efficiency of a PC by increasing its ground state reduction potential: indeed, this strategy exploits the fact that at very large  $E_{PC}^0$  values the increasing exergonicity of the backward ET of reaction 2 shifts its rate to the Marcus inverted region and it becomes less effective to oxidize  $Q^-$  back to  $Q$ . Overall, Figure 9 shows that both the standard ground state and the excited state potential of a photocatalysts have to be taken into account for optimizing the photocatalytic efficiency.

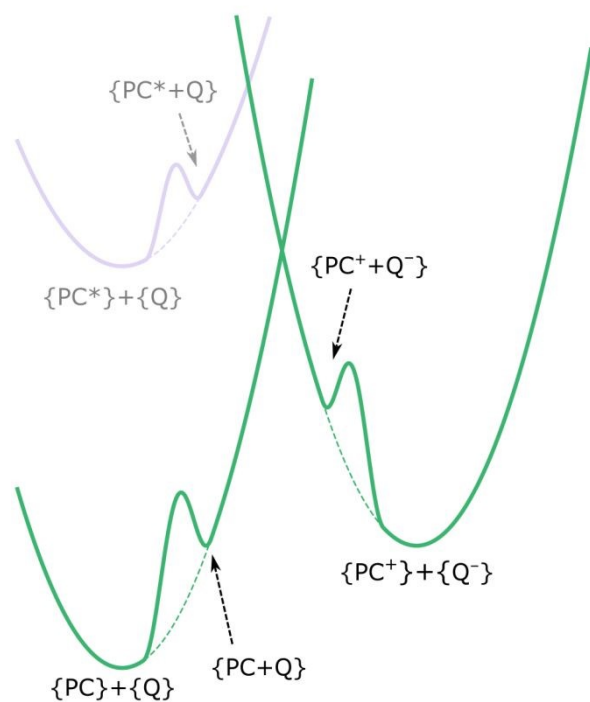


**Figure 9.** Distribution of organic PCs from the database of Ref. [18] as a function of their standard ground state ( $E_{PC}^0$ ) and excited state ( $E_{PC^*}^0$ ) reduction potentials relevant for oxidative quenching projected onto the computed  $E_Q$  surface. Colors indicate the molecular scaffolds of the photocatalysts. Experimental data are taken from Ref. [18].

The selection of solvent plays a critical role,<sup>8</sup> as it impacts several key parameters - such as excitation energies, reduction potentials, reorganization energy, diffusion limit, cage-escape yield, excitation state lifetime - that, in turn, influence the efficiency of photocatalysis. We now take a closer look at each relevant parameter separately. For the model to be applicable, the reduction potentials must be determined in the selected solvent, as solvents with different polarity stabilize the oxidized and reduced forms differently.<sup>8b</sup> Similarly, the diffusion limit that determines the maximum achievable reaction rate can be very different in typical solvents used for photocatalytic reactions, but as we have shown, this effect is limited. We note that in traditional catalysis mass transfer limitations must be carefully considered.<sup>34</sup> Our kinetic model assumes ideal mixing for proper diffusion. Regarding the lifetime of the excited state of the photocatalyst, it has been found that polar media can enhance it,<sup>35</sup> but this effect is often limited.<sup>36</sup> Another key parameter affected by the solvent is

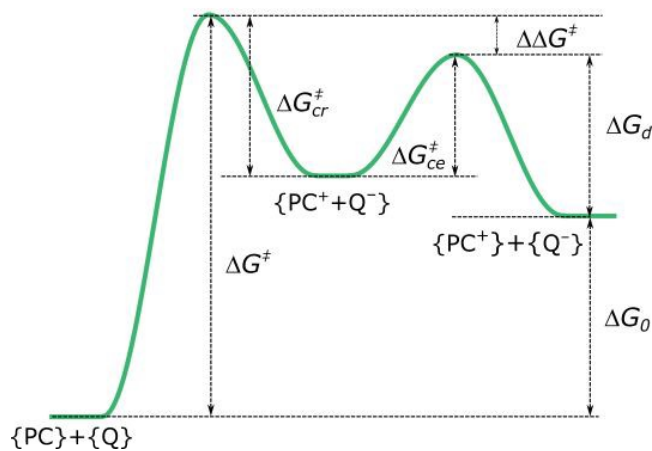
the reorganization energy that is comprised of two components: the outer-sphere  $\lambda_s$  reorganization energy of the solvent and the inner-sphere  $\lambda_i$  reorganization energy of the reactants. According to classical solvation models, the solvent reorganization energy for the electron-transfer reaction is expected to decrease with decreasing solvent polarity.<sup>12</sup> However, nonpolar solvents often exhibit significant reorganization energies, challenging earlier assumptions.<sup>37</sup> In fact, it can reach 0.3 eV in typical nonpolar solvents.<sup>37d</sup> Inner sphere reorganization energies can also vary significantly depending on the oxidant and reductant<sup>38</sup> but specific ligand-sphere designs can effectively decrease them<sup>39</sup> by minimizing the extent of geometrical stabilization required during electronic relaxation upon ET. Note that the reorganization energy can be readily calculated using quantum chemical methods with implicit solvation models, based on Marcus' theory.<sup>40</sup> Altogether, the solvent is a pivotal factor in photocatalytic systems, because it influences key electron-transfer parameters, i.e., it affects both the mechanism and the efficiency.

In the following, we discuss how the cage escape yield ( $\phi_{ce}$ ), which is the main descriptor of the cage effect,<sup>13a,b</sup> can be derived within the framework of our model. The cage-escape yield is independent of how the cage is formed; it describes the competition between charge recombination and diffusive escape processes. These main substeps are highlighted using the relevant parts of the simple Marcus parabolas shown in Fig. 10 and the energy profile in Fig. 11.



**Figure 10.** Marcus parabolas depicting the ET-s occurring between PC and Q as well as between PC\* and Q, indicating the energy penalties required by the cage effect, shown somewhat overstated for clarity. Dashed lines indicate the original parabolas. Curly brackets indicate solvated species. The excited state parabola is lighter to indicate the limited role of the excitation state in the cage-effect.





**Figure 11.** Schematic free energy profiles representing the two competing processes in a solvent cage shortly after the ET from  $\text{PC}^*$  occurred. Curly brackets indicate solvated species. The new free energy quantities shown in the figure are as follows:  $\Delta G_{cr}^\ddagger$  is the barrier for charge recombination,  $\Delta G_{ce}^\ddagger$  is the barrier for cage-escape, whereas  $\Delta\Delta G^\ddagger$  is the difference between the former two activation energies. The barrier of the formation of  $\{\text{PC} + \text{Q}\}$  is not shown for simplicity (cf. Fig. 10). Note that  $\Delta G^\ddagger$  denotes here the barrier for ET from the ground state  $\text{PC}$  to  $\text{Q}$ .

The cage-escape yield ( $\phi_{ce}$ ) characterizes the efficiency of the separation of the target  $\text{PC}^+$  and  $\text{Q}^-$  ion pair as shown by eq 6. For the purpose of kinetic modeling, simple algebraic manipulation yields an expression that allows cage-escape to be characterized by experimentally available quantities:

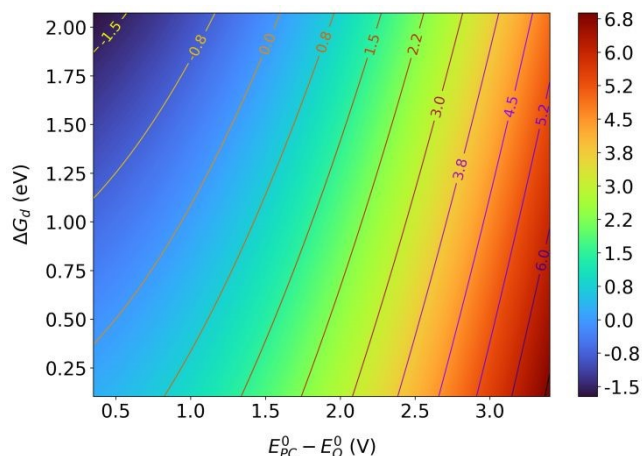
$$\begin{aligned}\phi_{ce} &= \frac{k_{ce}}{k_{ce} + k_{cr}} = \frac{1}{1 + \frac{k_{cr}}{k_{ce}}} \\ &= \frac{1}{1 + \exp\left(-\frac{\Delta G_{cr}^\ddagger - \Delta G_{ce}^\ddagger}{RT}\right)} \quad (16) \\ &= \frac{1}{1 + \exp\left(-\frac{\Delta\Delta G^\ddagger}{RT}\right)}\end{aligned}$$

Here we assume the validity of Eq. 9 (Eyring formula) for the rate constants. As Figure 11 indicates:  $\Delta\Delta G^\ddagger = \Delta G^\ddagger - \Delta G_d - \Delta G_0$ . Using Eq. 10 it can be further transformed into the following expression:  $\Delta\Delta G^\ddagger = (\lambda + \Delta G_0)^2/4\lambda - \Delta G_d - \Delta G_0$ ; i.e.,  $\phi_{ce}$  is a nonlinear function of the properties of  $\text{PC}$ ,  $\text{Q}$  and the solvent. Substituting Eq. 8 into this expression reveals the link between cage-escape efficiency and the standard reduction potential difference of  $\text{PC}$  and  $\text{Q}$ :  $\Delta\Delta G^\ddagger = (\lambda - zF\Delta E_0)^2/4\lambda - \Delta G_d + zF\Delta E_0$ . Eq. 17 shows the final formula for cage-escape yield:

$$\phi_{ce} = \frac{1}{1 + \exp\left(-\frac{(\lambda - zF\Delta E_0)^2/4\lambda - \Delta G_d + zF\Delta E_0}{RT}\right)} \quad (17)$$

An important observation is that  $\phi_{ce}$  does not depend on  $E_{\text{PC}^*}^0$ , only on the ground state reduction potentials  $E_{\text{PC}}^0$  and  $E_{\text{Q}}^0$ . It is quite remarkable, that  $\phi_{ce}$  can be predicted for a given  $\text{PC} - \text{Q}$  pair from Eq. 17 within the assumptions of the

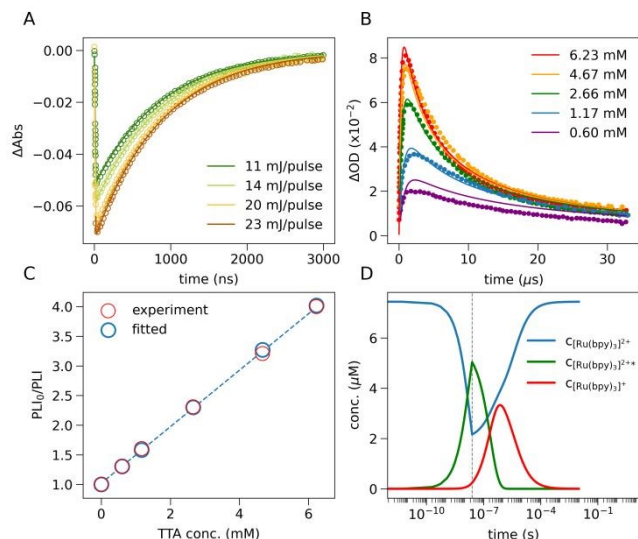
kinetic framework introduced above, if reorganization energy  $\lambda$  is available. Given the importance of  $\Delta\Delta G^\ddagger$ , Figure 12. shows its distribution as a function of  $E_{\text{PC}}^0 - E_{\text{Q}}^0$  and  $\Delta G_d$ .



**Figure 12.** Distribution of  $\Delta\Delta G^\ddagger$  (eV) as a function of  $E_{\text{PC}}^0 - E_{\text{Q}}^0$  and  $\Delta G_d$ .  $\lambda = 0.564$  eV.

Fig. 12 provides several insights.  $\Delta\Delta G^\ddagger$  is mostly positive, becoming negative only in the upper left region of the plot where the  $\Delta E_0$  values are very small and diffusion barriers are large. In typical photocatalytic processes  $\Delta E_0$  exceeds 0.8-1 eV,<sup>41</sup> therefore negative  $\Delta\Delta G^\ddagger$  values are expected only in viscous solvents that exhibit high diffusion barriers. From a reaction kinetics perspective, a negative  $\Delta\Delta G^\ddagger$  indicates that the activation barrier for the reverse ET reaction (Eq. 2) is higher than that predicted by Marcus theory. Conversely, a positive  $\Delta\Delta G^\ddagger$  indicates that the simple Marcus model is valid for the reverse ET process. In fact, this is the situation depicted by both Figs. 10 and 11. Chemical intuition and also formal analysis indicate that the net rate of a reversible reaction remains unchanged if it is replaced by a sequence of lower-barrier substeps, provided all newly introduced intermediates are less stable than the original reactant and product states (pre-equilibrium assumption).<sup>42,43</sup> This implies that the intermediate states do not accumulate and remain kinetically inaccessible on the timescale of the overall process. Therefore, as long as  $\Delta\Delta G^\ddagger$  is positive and the assumptions of the Marcus model hold, our model can deliver its central quantity  $E_{\text{Q}}$  without explicitly including the cage-bound ion pair in the kinetic equations. Despite treating the cage effect at an effective level, the model still captures essential features of the cage effect and allows us to extract mechanistic insight, as shown below.





**Figure 13.** Reproduction of spectroscopic measurements of the photoinduced reaction  $[\text{Ru}(\text{bpy})_3]^{2+*} + \text{TTA} = [\text{Ru}(\text{bpy})_3]^{3+} + \text{TTA}^{\cdot}$ . A: Excited state absorbance (at 450 nm) decay of  $[\text{Ru}(\text{bpy})_3]^{2+*}$  produced by different laser powers. B: Photoluminescence quenching of  $[\text{Ru}(\text{bpy})_3]^{2+*}$  in the presence of increasing amounts of TTA in  $\text{CH}_3\text{CN}$ . C: Experimental and fitted Stern-Volmer plots. D: simulated transient concentrations of the different Ru species. Note that for this plot the horizontal scale is logarithmic. The length of the laser-pulse is 25 ns (also obtained from fitting). Its duration is indicated by the vertical dashed grey line.

Having justified the approach taken to account for the cage effect, we now show that the model can reproduce experimental observations including steady-state as well as transient measurements. As a benchmark, we selected the  $[\text{Ru}(\text{bpy})_3]^{2+}$  – tri-*p*-tolylamine (TTA) system and collected experimental data from Refs. [28 and [13b]. We use our kinetic model to reproduce the experimental kinetic measurements associated with the photoinduced reaction of this photoredox system. Note that the underlying process is reductive quenching, but the same formalism can be applied. Using COPASI, we fit the key kinetic parameters ( $\phi_{ce}$ ,  $\tau$ ,  $k_4$ ,  $k_5$ ), along with additional experimental parameters (such as the initial concentration of  $[\text{Ru}(\text{bpy})_3]^{2+}$  and the laser pulse duration) required to reproduce the measurement conditions. The absorption coefficients  $\epsilon$  were taken from the literature. The parameters were determined using a global fit to obtain a consistent description of the spectroscopic data published in Refs. [28] and [13b], simultaneously considering measurements at different laser intensities and quencher concentrations (for details see SI, chap. 4). Given that ground-state electron transfer and excited-state regeneration via back electron transfer are expected to be negligible under the present conditions, and that the corresponding rate constants cannot be reliably determined from the available experimental data, we employ a simplified version of the model and set  $k_3$  and  $k_6$  to zero. The results of the fitting procedure are summarized in Figure 13 and Table 1.

Figs 13 A, B and C display the results of kinetic parameter fitting to experimental measurements. We can see that the

fitted datapoints closely match the experimental curves, demonstrating that the fitted parameters reliably capture the observations. This also supports that the kinetic model captures the key steps and species, and can accurately describe the behavior of the photocatalytic system even without explicitly including the cage-bound ion pair. Table 1 lists the fitted parameters together with values derived directly from experiment. Figure 13 D displays the simulated concentration changes of the Ru species. The concentration of  $[\text{Ru}(\text{bpy})_3]^{2+*}$  increases until 25 ns (i.e., during the excitation time), and roughly 65% of the photocatalyst molecules become excited. Based on the peak maxima, 67% of  $[\text{Ru}(\text{bpy})_3]^{2+*}$  transforms to  $[\text{Ru}(\text{bpy})_3]^{3+}$ , which relaxes back to  $[\text{Ru}(\text{bpy})_3]^{2+}$  on the ms timescale. It is seen that the back electron transfer is significant during the formation of the oxidized quencher, which explains the difference between the globally fitted cage escape yield and the experimentally determined value (0.96 vs. 0.84).

**Table 1.** Most important kinetic parameters for the photochemical reaction of  $[\text{Ru}(\text{bpy})_3]^{2+*} + \text{TTA}$ . Reported values are best-fit parameters; the accompanying values represent standard deviations as obtained from the parameter estimation procedure in COPASI. Note that the reported parameter uncertainties do not fully address parameter identifiability or covariance issues inherent to multiparameter kinetic fitting.

parameter	fitted value	experiment <sup>a</sup>
$\phi_{ce}$	0.96±0.01	0.84
$\tau$ (ns)	880±8	890
$c_0([\text{Ru}(\text{bpy})_3]^{2+})$ (μM)	7.4±0.1	– <sup>b</sup>
$k_4$ ( $\text{M}^{-1} \text{s}^{-1}$ )	$6.15 \cdot 10^{10} \pm 7 \cdot 10^8$	– <sup>b</sup>
$k_5$ ( $\text{M}^{-1} \text{s}^{-1}$ )	$5.23 \cdot 10^8 \pm 9 \cdot 10^6$	$6.4 \cdot 10^8$ ; $8.5 \cdot 10^8$

<sup>a</sup>Experimental values are from Refs. [28] and [13b].

<sup>b</sup>Experimental value is not available.

This kinetic analysis provides a unified mechanistic interpretation of all transient spectroscopic data for the Ru complex. An important advantage of the model is its explicit treatment of excited-state formation: instead of assuming instantaneous population of  $[\text{Ru}(\text{bpy})_3]^{2+*}$ , it accounts for the finite laser-pulse duration by integrating the absorbed photon flux. This yields a physically accurate estimate of the initial  $[\text{Ru}(\text{bpy})_3]^{2+*}$  concentration, avoids systematic errors inherent in delta-function excitation approximations and improves the reliability of all downstream kinetic parameters. The model also enables quantitative determination of back electron transfer, a process that overlaps with several microscopic pathways in the experiment, making it difficult to measure directly. Hence, the model can provide a good estimate of the fraction of the  $\text{TTA}^{\cdot}$  lost prior to a potential photocatalytic turnover. In summary, the kinetic modeling furnishes mutually consistent and physically meaningful rate constants, while offering predictive capability beyond what can be inferred from experiment alone, thereby enabling a more complete mechanistic understanding of the Ru-based photoredox cycle.



A crucial issue for our kinetic model is to use reliable values for those parameters which are not fitted to experiment.<sup>8b</sup> These parameters can be taken from measurements or can be derived from analogous systems. Temperature dependent cyclic voltammetry can yield reduction potentials and reorganization energies.<sup>44</sup> The lifetime of a PC\* can be determined by time-resolved spectroscopic methods.<sup>3</sup> Optical measurements provide the Beer-Lambert coefficients. The technical details of the illumination setup can be used for determining the light intensity to input into the kinetic model. Computational chemistry can be a complementary source of key parameters and its integration with kinetic modeling often provides a powerful strategy for preliminary screening.<sup>33</sup>

## Conclusions

We have presented a kinetic model to assess the dependence of the performance of photocatalysts on several, photocatalytically relevant parameters including the ground and excited state reduction potentials of the photocatalysts and the quencher (or substrate), reorganization energy, excitation properties of the photocatalysts and other parameters. In addition, we have also highlighted its capability to extract kinetic parameters by fitting the simulations to experimental measurements. The model comprises the kinetics of the following processes: photoexcitation and subsequent decay, electron transfer (ET) between the photocatalyst (in both ground and excited states) and the quencher with explicit treatment of solvent-cage escape, and the unproductive quenching of the excited-state photocatalyst. We use steady-state reduction potential  $E_Q$  as an effective measure of photocatalytic performance. To demonstrate the utility of the model, we have systematically mapped the dependence of  $E_Q$  on the ground and excited state reduction potentials of the photocatalyst within their catalytically relevant ranges while keeping the remaining parameters at fixed values selected to reflect typical photocatalytic conditions. The plot of  $E_Q(E_{PC}^0, E_{PC^*}^0)$  can be effectively used to identify the directions in which the ground and excited state reduction potentials can be tuned to improve photocatalytic efficiency. To demonstrate this, we have presented an example that employs photocatalysts commonly used in practice. Our analysis reveals that the dependence of  $E_Q$  on the reduction potentials is far from trivial: it is critically shaped by whether each electron-transfer step occurs in the Marcus normal or inverted region. This further suggests that the performance of a photocatalyst cannot be reliably assessed using only one parameter (e.g., only the excited state reduction potential, or the free energy of an ET). It is also clear that, of all the parameters considered in the model, only the reorganization energy affects the photocatalytic performance in a non-intuitive way. The model was also applied to a set of known photocatalysts, providing a practical demonstration of how it can assist in evaluating and comparing real systems. We have also presented an example where the model performance has been tested by fitting crucial kinetic parameters to transient and stationary measurements, and predicting other key experimental observables, as well as accessing information that was not directly available from the experiments. The

model can also be used to predict reduction potential combinations to obtain chemiluminescence. The kinetic model presented here can be easily modified or extended with additional reaction steps as it is available freely on Github. It can be used for a rapid qualitative assessment of photocatalytic performance or for systematic exploration of how key parameters influence new photocatalytic strategies and reactivities.

In cases where a specific quencher is targeted, optimal photocatalyst can be identified by considering multiple parameters simultaneously, which the model integrates in a unified framework. Beyond catalyst selection, the model can also support the optimization of experimental setups, such as the choice of solvent, light intensity, or reactant concentrations. Furthermore, by fitting the model to experimental data, it may help interpret measurements or estimate parameters that are otherwise difficult to access. The steady-state reduction potential  $E_Q$  introduced here thus acts as a comprehensive descriptor of photocatalytic efficiency, suitable for rational design of new photocatalytic systems. We also note that the actual kinetic model can be straightforwardly extended to heterogeneous photocatalysis.

## Data Availability

The supporting data (additional derivations, discussions, and plots of  $E_Q$  as a function of systematic changes of parameters, Figs S1-S13) have been provided as part of the Supplementary information. Simulation files are uploaded on [github.com/acsstirling/photokinetics](https://github.com/acsstirling/photokinetics).

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## Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

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## Conflicts of Interest

The authors declare no competing financial or non-financial interests.

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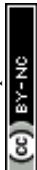
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**Data Availability**

The supporting data (additional derivations, discussions, and plots of  $E_Q$  as a function of systematic changes of parameters, Figs S1-S13) have been provided as part of the Supplementary information. Simulation files are uploaded on [github.com/acsstirling/photokinetics](https://github.com/acsstirling/photokinetics).

