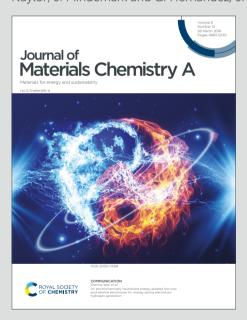
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Fluorine-Free Li-Ion Battery Features Comparable Cycling Performance to a Highly-Fluorinated Equivalent[†]

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Fluorinated compounds, including polyvinylidene fluoride (PVdF) binder and lithium hexafluorophosphate salt, are considered essential components in lithium-ion batteries due to their ability to provide good performance and cycle life. However, these compounds raise potential environmental concerns, as they can lead to the formation of toxic, corrosive and persistent compounds, such as hydrofluoric acid, phosphorus pentafluoride (PFs) and per- and polyfluoroalkyl substances. In this study, the effects of fluorine-free electrolyte consisting of lithium bis(oxalato)borate (LiBOB) salt and vinylene carbonate (VC) addtive and an aqueous-based binder based on carboxymethyl cellulose (CMC) and latex are investigated for full cells combining a silicon-graphite composite anode with LiNi_{0.6}Mn_{0.2}Co_{0.2}O₂ cathodes. Higher capacity retention is obtained at C/2 after 500 cycles with the fluorine-free binder in the cathode (61 and 65% for the fluorine-free and fluorinated electrolytes, respectively) compared to the PVdF-based binder (58 and 56% respectively). X-ray photoelectron spectroscopy analysis of the passivating layers on the cathode and anode across the four systems revealed a F-rich interfacial composition in the presence of the fluorinated electrolyte, while the fluorine-free electrolyte led to the formation of oxygen-rich layers at the interphases. Despite the chemical differences, both layers protect the cathode and anode during cycling, resulting in similar electrochemical performance. Moreover, the solid electrolyte interphase composition on the anode is dependent on the cathode's formulation. The aqueous-processed cathode resulted in higher coverage of the active material, which mitigated salt decomposition and facilitated the formation of a more stable passivating layer. This contributed to higher capacity retention despite a lower initial discharge capacity compared to the PVdF-based cathode. This study demonstrates the potential of fluorine-free components (electrolyte and binder with aqueous-processed cathode) to achieve high-energy-density full cells with comparable performance to conventional highly fluorinated lithium-ion batteries.

Introduction

The global shift toward decarbonisation and electrification of transportation entails a large production of energy storage devices. During this transition, technology advancement should not solely prioritize energy density and cycle life; ecological production, battery recycling, cost and safety are also critical to consider 1. In this context, regulations are coming strong, for example requiring higher amount of recycled materials to be used in batteries and the proposal to ban of per- and polyfluoroalkyl substances (PFAS) in the European Union from the European Chemicals Agency (ECHA) ² ³. In lithium-ion batteries (LIBs), PFAS and other fluorinated compounds are mainly found in binders and electrolytes. While fluorinated compounds are currently considered essential for good battery performance, they

pose many challenges for the environment and during battery recycling as they remain as impurities in the recycled products 2. Therefore, the search for fluorine-free alternatives is more pressing than ever 4.

In addition to LIBs, recent advancements in fluorine-free materials have demonstrated promising implementation across a range of energy storage and conversion devices beyond LIBs. For instance, electrolytes in supercapacitors5, and membranes in redox flow batteries 6, fuel cells 7, and water electrolysis 8.

High voltage cathode materials, especially those with high nickel content, still rely on PFAS-based binders, such as polyvinylidene fluoride (PVdF). Besides the source of PFAS, this binder has other environmental impacts worth highlighting. The first is the use of N-Methyl-2-pyrrolidone (NMP) solvent, which is harmful to the environment and humans, requiring solvent recovery during drying. Second, due to the high boiling point of NMP (202 °C), elevated

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temperatures are required for the drying of electrodes which makes the process less energy efficient, and increases the overall production cost. Therefore, cathode electrode fabrication is transitioning towards fluorine-free aqueous-processed binders to reduce the environmental impact and facilitate the large-scale production of more sustainable and cheaper lithium-ion batteries (LIB) ⁹. Examples of fluorine-free binders for NMC-based cathodes include polyacrylic acid (PAA) ¹⁰, Sodium carboxymethyl cellulose (CMC) ¹¹, CMC-latex ^{12,13}, and carrageenan biopolymers ¹⁴.

Another source of fluorinated compounds in batteries is in the electrolyte composed of fluorinated salts and additives, such as LiPF $_6$ and fluoroethylene carbonate (FEC), among others. Even if they do not fall into the PFAS category and regulations, they can react and degrade to release toxic and corrosive compounds (HF and PF $_5$), posing risks during manufacturing, accidents and battery dismantling and recycling 2 15 . Furthermore, they are detrimental to the recycling process as they corrode the reactors and leave fluorine as an impurity in the recycled products. Therefore, switching to fluorine-free alternative electrolytes is another approach towards realizing more sustainable and environmentally friendly batteries. Although it is worth noting that, to the best of our knowledge, life cycle assessments of fluorine-free electrolyte alternatives have not been done yet to confirm this.

In recent decades, several fluorine-free salts such as Lithium bis(glycolato)borate (BGB) ¹⁶, lithium perchloride (LiCl₄) ¹⁷, and lithium nitrate (LiNO₃) ¹⁸ have been proposed for LIBs ¹⁹. Among them, lithium bis(oxalato)borate (LiBOB) is the most studied case. However, none of them have reached their commercialization yet. The most widely use of LiBOB is as an additive in electrolytes, to passivate at the electrode surface and facilitate the formation of CEI and SEI layers²⁰ ²¹ ²². The main drawbacks of using LiBOB as main salt include its lower solubility and conductivity compared to the fluorinated electrolyte salts (0.8 M and 8–9 mS cm⁻¹ vs >1 M and > 10 mS cm⁻¹, respectively) ²³. Despite these limitations, promising electrochemical performance has been reported with fluorine-free electrolytes based on LiBOB when using graphite-based anode with various Co-poor and Co-free cathodes ²⁴ ²⁵ ²⁶ ²⁷.

For the next generation of LIBs, low-cobalt- and high-nickel-content cathode materials, along with silicon-based anodes, have garnered significant attention. Higher Ni content in $\text{LiNi}_x \text{Mn}_y \text{Co}_{1-x-y} \text{O}_2$ materials

provides higher reversible capacity at the same cut-off voltage. However, higher Ni content brings about other issues such as higher sensitivity toward moisture and oxidation/decomposition of electrolyte at the interface. The primary motivation for the development of Si-based anodes is higher theoretical capacity compared to the conventional graphite (3579 mAh g-1 vs. 372 mAh g-1). However, their application is limited due to rapid capacity fading, primarily attributed to consecutive volume changes of Si during lithiation/delithiation cycles. Recently, the effect of electrolyte fluorination on Si-graphite||NMC111 full cells with high mass loading electrodes has been investigated ²⁷. A fluorine-free electrolyte based on LiBOB and VC additive showed similar cycling performance at low current densities compared to the highly fluorinated analogue; however, the performance was limited at high current densities. Furthermore, the choice of binder and active material (graphite-silicon) affects the SEI properties and, therefore, can have implications on its stability and subsequent cell performance 28 29 30.

Herein, we have employed a fluorine-free electrolyte based on LiBOB salt and VC additive in full cells containing high-mass-loading and high-energy-density electrodes of graphite-silicon alloy as the anode and NMC622 as the cathode paired with fluorinated and fluorine-free binders. The electrochemical performance of these cells has been investigated and correlated to the morphology and chemical composition of the anode's and cathode's interphases to understand their formation and stability upon long-term cycling. This study provides a pathway toward competitive fluorine-free lithium-ion batteries compared to state-of-the-art, bringing us closer to the realization of more sustainable and environmentally friendly energy storage solutions.

Experimental

Materials and methods

Materials. LP57 electrolyte (SelectiLyte BASF, 1 M LiPF₆, ethylene carbonate (EC)/ethyl methyl carbonate (EMC) 3:7 v/v), EC (SelectiLyte BASF), EMC (SelectiLyte BASF), dimethyl carbonate (DMC, anhydrous ≥ 99%, Sigma-Aldrich), vinylene carbonate (VC, SelectiLyte BASF), and fluoroethylene carbonate (FEC, Gotion) were battery-grade and used as received. Lithium bis(oxalato)borate (LiBOB, Chemetall) was dried at 120 °C for 12 h under vacuum prior to electrolyte preparation.

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Electrodes. Silicon-graphite electrodes were kindly provided by VARTA Innovation GmbH. These were composed of silicon alloy (L-20772, provided by 3 M), graphite (BTR 918), super-P carbon black and lithium polyacrylate (LiPAA, 450 K) binder in a mass ratio of 25:66:2:7 and an areal capacity of 2.4 mAh cm⁻². Organic-based NMC622 cathodes with PVdF binder were kindly provided by VARTA Innovation GmbH with an areal capacity of 2.2 mAh cm⁻². Agueousprocessed NMC622 cathodes were kindly provided by CEA-Liten with electrode mass loading of 11.6 mg cm⁻² and an areal capacity of 1.9 mAh cm⁻² using 180 mAh g⁻¹ specific capacity for NMC622 cathode material. The composition of the latter was 92 wt% NMC622, 4 wt% carbon black, 1 wt% CMC and 3 wt% latex and it was coated onto carbon-coated aluminium foil (from Armor). The N:P ratios for organic-based and aqueous-processed NMC622 cathodes are 1.09 and 1.26, respectively. Electrodes were cut in Ø13 mm discs and dried at 120 °C under vacuum for 12 h.

Cell assembly and testing. Fluorinated electrolyte was prepared by adding 10 vol% FEC and 2 vol% VC to LP57. Fluorine-free electrolyte was prepared by mixing LiBOB in EC/EMC 3:7 v/v with a molal concentration of 0.7 and adding 2 vol% VC. Two-electrode full cells were assembled in coin cells in an argon glovebox with Ø17 mm Celgard 2325 separator and 50 µL of electrolyte. Three-electrode cells were assembled in pouch cells using lithium metal foil as reference electrode (ring shape with inner and outer diameters of 16 and 22 mm, respectively), Ø25 mm Celgard 2325 separator and 120 μL of electrolyte. The reference electrode was placed between the working and counter electrodes with separators on both sides. The cells rested for 6 h before cycling was initiated.

Galvanostatic cycling of NMC622/Si-graphite full cells were performed at room temperature using Arbin BT-2043 battery testing system. The C-rate used for cycling was based on the cathode's reversible capacity provided by the suppliers stated above. For NMC622 cathodes with PVdF binder, the initial two cycles were done at C/20 between 3.0 and 4.2 V with a constant voltage step at the end of the charge step until the current dropped to C/50. Afterwards, the cells were cycled at C/2 with a constant voltage at the charge state until the current was below C/20. For the aqueous-processed one, same protocol was applied without constant voltage step. The intermittent current interruption (ICI) method consisting of 1 s rest at 5 min intervals was used to determine the internal cell resistance

following the analysis procedure reported by Lacey et al. 31 and Chien et al. ³². C-rate capability tests were performed at C/10, C/5, C/2, 1C, 2C and C/2 for five cycles at each current density. Areal capacities were used to calculate the current.

Surface analysis. Prior to surface analysis, cells were disassembled in an argon glovebox and the electrodes were removed and rinsed with 2 mL of dimethyl carbonate. For SEM/EDS, the samples were transferred in a vacuum-sealed transfer chamber and measured with a field-emission scanning electron microscope (Merlin, Carl Zeiss, Germany) with an acceleration voltage of 3 kV and a beam current of 100 pA. EDS was measured with an acceleration voltage of 15 kV and a beam current of 1000 pA.

XPS measurements were performed on both pristine and cycled electrodes after 280 cycles. The fluorinated and non-fluorinated samples were washed using DMC and EMC, respectively. They were mounted to the sample holder using copper tape on top of polyimide tape, insulating the samples from the spectrometer in a 'floating' configuration. Samples were mounted in an argon glovebox, and the holder sealed and pumped before transferring to a Kratos AXIS Supra+ X-ray photoelectron spectrometer. A monochromated Al Ka X-ray source (1486.6 eV) with X-ray power of 225 W was used for measurements, with the 'slot' collimation and 'hybrid' lens modes. The analysis spot size was approximately 700 x 300 μm. The charge neutraliser system was used during measurements with current of 0.4 A, bias of 0.17 V and charge balance of 0.67 V. A pass energy of 20 eV was used for high-resolution scans.

CasaXPS software was used for spectral analysis with a Shirley background and employing the Gaussian-Lorentzian GL(30) peak shape. Energy calibration was performed using the sp³ carbon (C-C) peak at 285 eV. Probing depths (3×IMFP) were calculated using the TPP-M2 equation as detailed in the NIST database, using parameters for polyethylene, as a low-density material representative of the surface layer studied here 33 34. The approximate probing depth is estimated as 14 nm. This depth should be considered as an upper limit, since electron kinetic energies are used in calculations, while it should also be noted that a smaller probing depth would be expected for denser inorganic materials, including those making up the bulk electrodes.

Results and discussion

Electrochemical performance

The electrochemical performance of full cells with NMC622 cathode containing PVdF (NMC622(PVdF)) and Si-graphite anode, using a fluorinated electrolyte based on LiPF $_6$ and a fluorine-free based on LiBOB, is shown in Figure 1. In the first formation cycle at C/20, the NMC622(PVdF)||Si-graphite cell with highly fluorinated and fluorine-free electrolytes delivered similar discharge capacity of 2.0 mAh cm $^{-2}$ with initial coulombic efficiency of 79.2% and 79.5%, respectively. In

terms of long-term cycling, the coulombic efficiency remained stable and above 99.8% and the capacity retention for the fluorinated and fluorine-free systems were 56.2% and 58.3%, respectively, after 500 cycles at a C/2 rate (Figure 1 a,b). While the difference in cycling stability is small for the fluorinated electrolyte cell compared to the previous publication with NMC111 and the same anode ²⁷, the cycling stability of the cells with the fluorine-free electrolyte is clearly improved. For the NMC111||Si-graphite system, the capacity

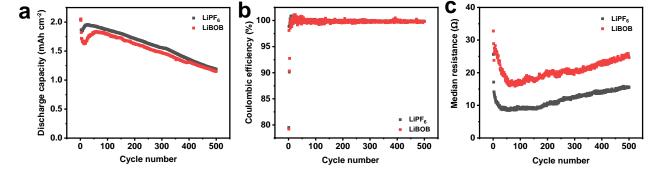


Figure 1. Electrochemical performance of NMC622(PVdF)||Si-graphite cells cycled at C/2 between 3.0-4.2 V with fluorinated (black) and fluorine-free electrolytes (red). (a) Discharge capacity, (b) Coulombic efficiency and (c) median resistance vs. cycle number.

retention for fluorinated and fluorine-free electrolytes after 300 cycles at C/2 rate were 78.5% and 59.4%, respectively; and for the current systems they are 83.4% and 80.9%, respectively. In the literature, the degradation of LiBOB is often considered one of the main reasons for capacity fading 25 26. However, despite using the same anode and electrolyte as in the previous paper, a significant improvement in capacity retention was observed. These results suggest that the cathode side limited the performance of the fluorine-free electrolyte in the case of NMC111||Si-graphite and it improved with the next-generation cell composed NMC622(PVdF)||Si-graphite. Furthermore, the obtained capacity retention for both electrolyte systems, using high-mass-loading and high-energy-density electrodes, exceeds other reported values for NMC||Si-based full cells 35 36 37. These results confirm the potential of this fluorine-free electrolyte and the importance of optimizing all the battery components.

The evolution of cell resistance with the two electrolytes was monitored using the intermittent current interruption (ICI) technique ^{31 32}. The median cell resistance is higher throughout the long-term cycling for the cell with the fluorine-free electrolyte than the highly fluorinated electrolyte (Figure 1c). The voltage profiles with the two

electrolytes are very similar during the formation cycles, except for a short plateau in the first cycle at 1.9 V for the fluorine-free electrolyte from LiBOB decomposition and at 2.5 V for the fluorinated electrolyte from the FEC decomposition 38 (Figure S1). The resistance evolution during this first cycle is higher for the cell with the fluorinefree electrolyte indicating that it is the contribution from the LiBOBbased decomposition products. The voltage profiles during cycling at C/2 are also similar throughout cycling, except for the initial stabilization cycles when the capacity drops slightly and is soon recovered. This difference is not contributing to the higher resistance of the fluorine-free electrolyte because the median resistance decreases with both electrolytes. Despite the overall higher cell resistance with LiBOB-based electrolyte, the resistance evolution is the same in both systems, with a decrease in the initial 50 cycles followed by a steady increase until 500 cycles, indicating this evolution is related to the active materials and not the electrolyte itself.

To investigate the effect of each electrode, three-electrode cells were assembled with lithium metal as the reference electrode. As shown in Figure S1 and mentioned before for the two-electrode cells, the main difference in the voltage profiles of the first formation cycle

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at C/20 appears as a short plateau at low voltages. This can be observed in the corresponding derivative of capacity with respect to full-cell voltage (dQ/dV) plots for the full cell and each electrode

(Figure S1 d-f). The full cell with fluorinated electrolyte featured appear at around 2.5 V, corresponding to a peak in the negative electrode at 1.3 V vs. Li $^+$ /Li, indicating the reduction of the additives

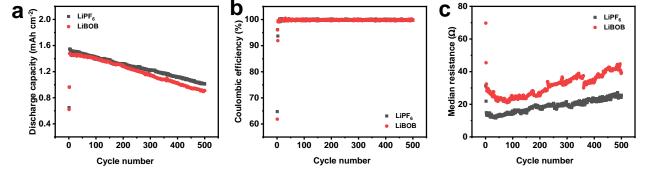


Figure 2. Electrochemical performance of NMC622(aqueous) ||Si-graphite cells cycled at C/2 between 3.0-4.2 V with fluorinated (black) and fluorine-free (red) electrolytes. (a) Discharge capacity, (b) Coulombic efficiency and (c) median resistance during discharge vs. cycle number.

FEC/VC. In the case of the cell with the fluorine-free electrolyte, there is a peak at 1.9 V, which also corresponds to a peak for the negative electrode at 1.8 V vs. Li⁺/Li, indicating the reduction of LiBOB ²⁶. Similar peaks were observed in the full cell of NMC111||Si-graphite²⁷, suggesting that they originate from the negative electrode, as that is the electrode in common, due to the formation of the SEI layer.

Figure S2 compares the rate capability of full cells using fluorinated and non-fluorinated electrolytes from C/20 to 2C. At low C-rates below 1C, the electrochemical performance between the two systems is very similar. Increasing the C-rate results in a lower coulombic efficiency in the first cycle that is recovered in the following ones. However, that is not the case at 2C; the decrease in coulombic efficiency is more abrupt and not recovered in the following cycles, indicating the presence of parasitic reactions, more evident for the cell with the fluorine-free electrolyte. The discharge capacity also decreases at higher C-rates (1C and 2C) for both cells and an initial increase in resistance is observed at 2C that decreases in the following cycles. However, the limited capacity at high C-rates for the fluorine-free electrolyte might be due to its lower ionic conductivity. Furthermore, the capacity at C/2 was not fully recovered after the C-rate test for the two cells showing 97.9% and 95.8% capacity retention with the fluorinated and fluorine-free electrolytes, respectively. This trend indicates parasitic reactions and relatively slow Li+ transport occurring during cycling, which limit these systems at high C-rates and are more pronounced with the fluorine-free electrolyte.

Despite the promising results observed from the long-term cycling at C/2 also with the fluorine-free electrolyte, the cathode still contains a fluorinated PVdF binder (PFAS source) processed with NMP. To further improve the sustainability of these systems, the PVdF binder was replaced with fluorine-free water-processable binders, such as a mixture of CMC and latex.

Figure 2 shows the performance of these two electrolytes in cells containing an aqueous-processed NMC622 cathode with the same silicon-graphite anode. Both cells delivered initial discharge capacities of 1.55 and 1.48 mAh cm⁻² at C/2 rate after the formation cycles at C/20 for fluorinated and fluorine-free electrolytes, respectively (Figure 2a). After 500 cycles, the capacity retention was 65% and 61% for the fluorinated and fluorine-free cells, respectively, and the coulombic efficiency above 99.8% for both cells (Figure 2b). The cell resistance follows the same trend as with the PVdF-based cathodes, a decrease in the initial 50 cycles and then a continuous increase for the following 500 cycles. However, the values are slightly higher with the aqueous-processed cathode with both electrolytes and higher for the cell with the fluorine-free electrolyte compared to the highly fluorinated one (Figure 2c). Overall, despite the lower discharge capacity of the aqueous-based electrodes, the capacity retention was slightly higher (61-65%) than with the PVdF-based cathode (56-58%) after 500 cycles, indicating that the fluorine-free electrolyte is also a promising alternative for aqueous-processed cathodes. Moreover, to compare SEI layer formation, the voltage profiles and corresponding derivatives of capacity from two-

electrode cells with aqueous-processed cathodes are presented in Figure S3a and S3b, respectively. Similar peaks are observed in both fluorinated and fluorine-free electrolytes, corresponding to the decomposition of FEC and LiBOB in cycled cells respectively, confirming the formation of the SEI layer similar with both electrodes.

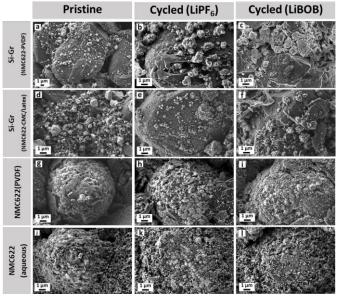


Figure 3. SEM images of (a, d, g, j) pristine electrodes and after 280 cycles with (b, e, h, k) fluorinated and (c, f, i, l) fluorine-free electrolytes. (a, d) Pristine Sigraphite at different magnifications and extracted from the cells containing (b, c) NMC622(PVdF) and (e, f) NMC622(aqueous) cathodes. Corresponding images of the (g, h, i) NMC622(PVdF) and (j, k, l) NMC622(aqueous) cathodes.

Surface morphology and elemental mapping analysis

To further analyze the contribution of the electrolytes to the formation of the SEI and CEI layers and to understand how cycling affects their properties, we studied the morphology and elemental mapping of the electrodes in their pristine state and after 280 cycles using SEM and EDS.

SEM images of the pristine and cycled electrodes with fluorinated and fluorine-free electrolytes are presented in Figure 3. The anode is composed of silicon particles distributed homogeneously over larger graphite particles. Figure 3a and d show the same silicon-graphite pristine anode at two different magnifications, focusing on the graphite and the silicon particles, respectively. The large particles in the range of 20-30 μ m correspond to graphite, while the smaller particles, in the range of 0.5-3 μ m, to silicon ³⁹ ²⁷. The change in morphology of the anodes extracted from the cells containing PVdF-based cathodes, cycled in fluorinated and fluorine-free electrolytes,

can be seen in Figure 3b and c, respectively. Graphite particles cycled with the fluorinated electrolyte do not show much difference compared to the pristine anode; however, with a fluorine-free electrolyte, the graphite particles surface appear slightly smoother 40 ²⁸. In both electrolytes, the silicon particles remain homogeneously distributed over the electrode but they are larger and seem to be less compact, exhibiting a rough, coarsely vesicular appearance. In the case of the fluorine-free electrolyte, more agglomeration of the silicon particles can be observed. The corresponding morphologies of the anode materials extracted from the cells containing aqueousprocessed cathodes are presented in Figure 3e and f for the fluorinated and fluorine-free electrolytes, respectively. With a fluorine-free electrolyte, the graphite particles show similar morphology regardless of the cathode used in the cell. However, with the fluorinated electrolyte and the aqueous-processed cathode, the graphite particles show a rough surface (Figure 3e) not seen when cycled with the PVdF-based cathode (Figure 3b). A similar morphology evolution is observed for the silicon particles, with an increase in the size during cycling and less agglomeration with the fluorine-free electrolyte. The enhancement of Si particle size can be attributed to the formation of the SEI layer and the volume changes during cycling. The more pronounced change in surface morphology for the anode, especially from the silicon particles, cycled with the fluorine-free electrolyte regardless of the cathode used, could also explain the higher resistance observed during cycling with both cathodes.

The morphological evaluation of the cathodes were conducted for the two types of NMC622 electrodes, with PVdF and aqueous-processed binders, and are shown in Figure 3 g,h,i and j,k.l, respectively. The particle size of NMC622 is 10-15 µm with a granular structure on the surface for both pristine electrodes. For both sets of cathodes, cycled with fluorinated and fluorine-free electrolytes (Figure 3h,i and Figure 3k,l, respectively), morphology changes are observed on the surface, although the granular structure remains visible. These results imply the formation of a CEI layer during cycling with both electrolytes on both cathodes. Furthermore, the aqueous-processed NMC622 shows particle coverage from the conductive carbon and binder, which has been reported previously with similar electrode processing ^{13,41}. This explains the lower discharge capacity observed with the aqueous-based NMC622 and higher cell resistance.

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Elemental mapping of the pristine electrodes and after 280 cycles with fluorinated and fluorine-free electrolytes was done with EDS. As shown in Figure 4, for the anode electrodes extracted from the cells with aqueous-processed cathode, there was an increase in the

oxygen content from 3.6% in the pristine sample (mainly from the LiPAA binder and native oxide on Si particles) to 16.0% after cycling with the fluorinated electrolyte, likely due to the decomposition of

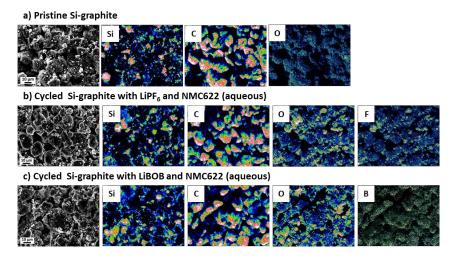


Figure 4. SEM images and elemental mapping of the silicon-graphite composite (extracted from the cells containing NMC622(aqueous)): a) Pristine and after 280 cycles with b) fluorinated and c) fluorine-free electrolytes. The intensity of each element is color coded, ranging from black/blue for low intensity to pink/white for higher intensity.

the solvent and/or additives. The corresponding value for the anode cycled with the fluorine-free electrolyte is higher, 23.5%, suggesting the additional decomposition of the BOB anion, as observed in previous studies ²⁸ ¹⁹. The elemental mapping of F in the cell with the fluorinated electrolyte (Figure 4b) shows higher intensity on the silicon particles compared to the graphite particles, indicating a preferential decomposition of electrolyte on the silicon. In contrast, in the cell with the fluorine-free electrolyte (Figure 4c), there is a high correlation between B and C, indicating that boron preferentially deposits on graphite particles ²⁸. However, the oxygen distribution seems to cover both type of particles without a clear preference for silicon or graphite. A similar elemental mapping trend in the case of the fluorine and boron distributions can be observed on the anodes extracted from the cells with PVdF-based cathodes (Figure S4). However, lower oxygen content is observed, 11.0% and 21.4% for the fluorinated and fluorine-free electrolytes, respectively, compared to the anode from the aqueous-processed cathode. These results show that changing the cathode formulation (binder and solvent during processing) influences the electrolyte decomposition and SEI layer

on the anode side towards a more oxygen-rich SEI with aqueousprocessed fluorine-free cathodes ²⁹.

Figure 5 shows the elemental mapping for the aqueous-processed cathode. As expected, the pristine sample lacks F, but in the cycled sample with fluorinated electrolyte, its content increases to 5.9% indicating the decomposition of salt and/or FEC additive. On the other hand, the oxygen content changes from 18.3% in the pristine sample to 16.4% and 19.7% in the cycled samples with fluorinated and fluorine-free electrolytes, respectively. The decrease in oxygen for the fluorinated cell indicates the presence of a fluorine-rich CEI layer covering the cathode's surface and burying the oxygen contribution. The increase in oxygen with fluorine-free electrolytes is attributed to the decomposition of BOB anion on the cathode's surface 42. Furthermore, the fluorine distribution is predominantly on the active material particles whereas the boron distribution seems to follow where the carbon black/binder is, mirroring the correlation between B and C on the anode. Figure S5 shows the elemental mapping of the PVdF-based cathode electrodes. The oxygen content

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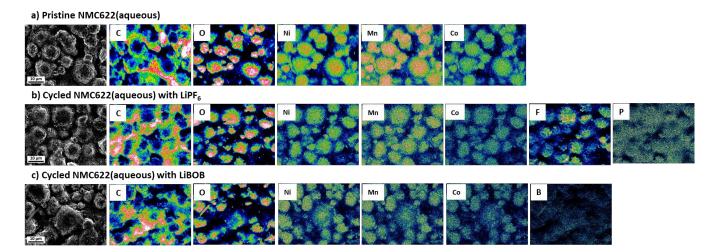


Figure 5. SEM images and elemental mapping of the NMC622(aqueous) cathode: a) Pristine and after 280 cycles with b) fluorinated and c) fluorine-free electrolytes. The intensity of each element is colour coded, ranging from black/blue for low intensity to pink/white for higher intensity.

increases slightly after cycling, from 16.3% in the pristine cathode to 16.8% and 18.5% in the cycled cells with fluorinated and fluorine-free electrolytes, respectively. This indicates that besides the oxygen from the NMC622(PVdF), a CEI layer with oxygen-based species is also formed and to a larger degree with the fluorine-free electrolyte. Fluorine is present in all samples due to the presence of PVdF as a binder in the cathode. As expected, the variation in amount of fluorine is guite small after cycling with the fluorine-free electrolyte. However, the fluorine content increases when cycled with the fluorinated electrolyte, rising from 2.1% in the pristine cathode to 5.6%, indicating the formation of an F-containing CEI layer from the decomposition of fluorinated components in the electrolyte (salt and/or FEC). Furthermore, the presence of phosphorus corroborates the salt decomposition on the cathode surface. The boron mapping shows a similar trend as with the other cathode, with a preferential distribution together with carbon species.

Chemical composition analysis of the interphases

Using SEM for morphological analysis and EDS for elemental mapping provided insights into the surface layers and their compositions as well as the effect of different electrolyte and cathode formulations

on such surfaces. To complement this, XPS analysis was employed to provide more information about the chemical composition and environment of the surface of electrodes and the CEI and SEI layers after 280 cycles.

Cathodes. Figure 6 shows the C 1s and O 1s spectra of PVdF- and aqueous-processed NMC622 electrodes, respectively, in their pristine state and after 280 cycles with fluorinated and fluorine-free electrolytes, obtained from full cells of NMC622||Si-graphite. The corresponding positions of the deconvoluted peaks are provided in Table S1. By analyzing the relative peak intensities of the C=C peak in the C 1s spectra (Figures 6a and 6c) and the M-O peak in the O 1s spectra (Figures 6b and 6d) of both pristine and cycled samples which originate from carbon black and metal oxides, respectively the thickness of the CEI layers can be evaluated. For the PVdF-based cathode, the relative peak intensity of C=C decreases after cycling for both electrolytes, although to a larger extent with the fluorine-free electrolyte, suggesting a thicker CEI with this electrolyte. In addition, the relative peak intensity of M-O in the pristine sample is almost completely diminished after cycling with both electrolytes, indicating that a CEI layer has formed over the cathode active material.

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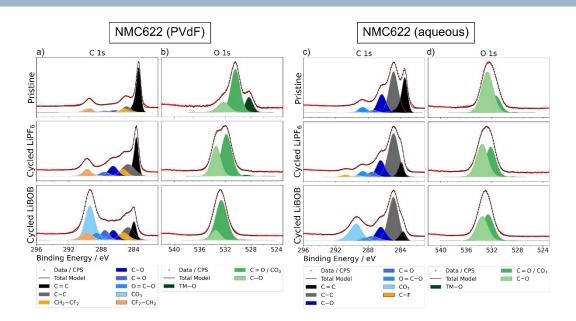


Figure 6. XPS a,c) C 1s and b,d) O 1s spectra of NMC622(PVdF) and NMC622(aqueous) cathodes, respectively: pristine (top row) and after 280 cycles using fluorinated (middle row) and fluorine-free (bottom row) electrolytes.

In the C 1s spectra of NMC622(PVdF), the presence of the PVdF binder can be identified through the CH_2 (PVdF) and CF_2 (PVdF) groups in the pristine electrode. After 280 cycles in both electrolytes, the PVdF peaks persist, and the corresponding signal in the F 1s spectra confirms this as well (Figure S6). Notably, the single F 1s peak observed in the fluorine-free sample further confirms that any detected fluorine originates from the binder in that system. However, upon cycling, newly formed carbonate and ether species begin to overlap with the CH_2 (PVdF) and CF_2 (PVdF) peaks. As a result, the apparent increase in intensity at these binding energies reflects not only the presence of the PVdF binder but also the CEI layer growth.

Upon cycling, the relative peak intensities of ether (C–O), carbonyl (C=O), ester (O=C–O) and carbonate (CO₃) groups increase compared to the pristine electrode (where any such peaks likely come from surface groups on the conductive carbon additive or the cathode material), again confirming the decomposition of the solvent and/or additives on the cathode surface to form the CEI layer. This CEI layer

includes Li₂CO₃, ROLi, and ROCO₂Li (R: alkyl group) coming from the interaction between the cathode and the electrolyte components ⁴³.

A key difference between the fluorinated and fluorine-free electrolytes is the relative peak intensity of the carbonate group, which is much larger in the latter electrolyte. Furthermore, the appearance and noticeable contribution of the ester group in the cycled sample with the fluorine-free electrolyte might originate from the decomposition of the electrolyte components or could simply be residual LiBOB salt (from the oxalate groups) remaining in the CEI layer or trapped in the electrode's porous structure after washing with EMC. Although gas evolution was not observed in the cycled pouch cells, CO₂ evolution from LiBOB decomposition has been investigated with mass spectrometry 44,45. However, the released CO₂ can react further with EC forming polycarbonate-like oligomers, which could explain the high concentration of carbonates seen in this study when using LiBOB as the main salt and not only as an additive 46.

The O 1s spectra can be resolved into three peaks: transition metal oxide (M–O), C=O/CO₃, and C–O. It can be observed that the cycled samples exhibit peaks that shift to higher binding energies, likely due to changes in the chemical environment caused by surface reactions and the formation of a CEI layer ⁴⁷. In the O 1s spectra of the PVdF-based cathode (Figure 6b), in addition to the decrease in the M–O peak with both electrolytes, an increase in the C=O/CO₃ and C–O peaks is observed, suggesting the formation of the CEI layer from electrolyte decomposition products. The fluorinated electrolyte leads to a mixture of C=O/CO₃ and C–O-based species, while the fluorine-free electrolyte, the CEI layer is mainly composed of carbonate species as indicated by the large peak in both C 1s and O 1s.

The O 1s spectrum of the pristine aqueous-processed cathode (Figure 6d) displays oxygen-containing groups - namely, C-O, C=O, and O-C=O - which correspond to the binder (CMC and latex). The low relative intensity of the TM-O peak in the pristine O 1s spectrum indicates that the NMC particles are completely covered by the binder and conductive additive, whose thickness exceeds the probing depth of XPS of ~14 nm (estimated from the Al Kα kinetic energy, see Experimental section), as also observed in the SEM images (Figure 5j), in contrast to the cathode with PVdF binder. Therefore, this peak cannot be used to compare the CEI thicknesses. However, the persistent C=C signal in C 1s from the conductive additives suggests a thinner or more porous binder coating on the conductive additive, allowing to compare the CEI layer thickness with cycling. The fact that the C=C peak remains observable confirms that the formed CEI layer is also thinner than the XPS probing depth. However, the relative peak intensity of C=C decreases slightly more after cycling with the fluorine-free electrolyte, suggesting a slightly thicker CEI compared to the fluorinated electrolyte, similar to the PVdF-based cathodes. Furthermore, upon cycling, the ester peak grows and the carbonate peak appears, with a higher contribution in the sample cycled with the fluorine-free electrolyte. This correlates with the C 1s spectra in the PVdF-based cathode, although the relative intensity of the carbonate peak with the fluorine-free electrolyte is lower with the aqueous-based cathode. These results could be due to the better coverage of the active material preventing to more extent the decomposition from the LiBOB-based electrolyte. F1s spectra of PVdF and aqueous-based NMC622 are shown in Figure S6 a,b, respectively. For the NMC622(PVdF), the peak at

around 687 eV corresponds to CF2 (PVdF) from the binder in all the samples. Additionally, a LiF peak was observed in both the pristing and fluorine-free samples, possibly coming from the parasitic dehydrofluorination of PVdF ⁴⁸ ⁴⁹ ⁵⁰. The spectrum after cycling with the fluorine-free electrolyte does not show any additional peaks besides the binder and LiF also observed in the pristine sample. Clearer changes can be observed after cycling with the fluorinated electrolyte. The LiF peak is dominating the spectrum, followed by organofluorine species and P–F from the presence or decomposition of LiPF₆. For the aqueous-based NMC622, the F 1s spectra show no fluorine present in either the pristine sample or the sample cycled with the fluorine-free electrolyte. However, the F 1s spectra (Figure S6b) of the cathode cycled with the fluorinated electrolyte exhibits the presence of LiF (to a lower extent), P-F, and other organofluorine compounds, most likely from the FEC additive, confirming a fluorinerich CEI layer.

In the P 2p spectra (Figure S7 a,b) for PVdF- and aqueous-based NMC622, cycling with the fluorinated electrolyte leads to the appearance of three peaks, assigned to PO₄ PO_xF_y, and PF₆⁻ compounds. Each peak splits into two components due to spin-orbit coupling, with a separation of 0.84 eV. These peaks indicate the decomposition of the LiPF₆ salt as well as possible residual salt that was not completely rinsed off from the electrode during washing with DMC ⁴⁷. The P 2p spectrum of NMC622(aqueous) shows a larger contribution of phosphate-based decomposition products from LiPF₆, and also residual LiPF₆ salt compared to the NMC(PVdF). The lower contribution from LiF and higher P-F in the F 1s spectrum as well as higher PF₆⁻ in the P 2p spectrum with aqueous-based NMC622 suggest less salt decomposition compared to the PVdF-based cathode, which could be due to the better coverage of the active material in the former electrode from the binder and carbon additives, as seen with the fluorine-free electrolyte.

The Li 1s spectra of PVdF and aqueous-based NMC622 are shown in Figure S8 a,b, respectively. For both cathodes, in the Li 1s spectra, the pristine displays a single peak, corresponding to TM–Li which diminishes in the cycled sample with fluorinated and fluorine-free electrolytes, respectively. The dominant peak in the cycled samples is near 55 eV arising from Li₂CO₃ peaks, however in the fluorinated electrolyte this peak also contains overlapping contributions from LiF

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and Li_xPO_yF_z (from LiPF₆/FEC decomposition), which they have very The B 1s spectra in Figure S9 a,b for NMC622(PYdF) and similar binding energies in the Li 1s region.

NMC622(aqueous), respectively, from cycled sample with fluorine-

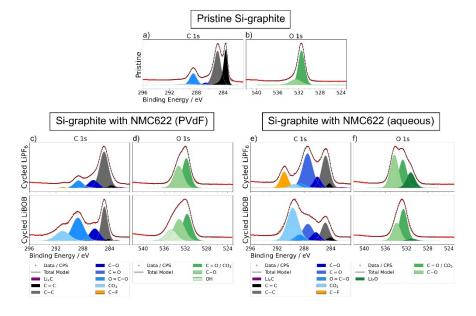


Figure 7. XPS a,c,e) C 1s and b,d,f) O 1s spectra of Si-graphite anodes pristine (top row) and after 280 cycles with NMC622(PVdF) and NMC622(aqueous), respectively, using fluorinated (middle row) and fluorine free (bottom row) electrolytes.

free electrolyte confirm the presence of boron-based species on the surface indicating residues and/or decomposition of LiBOB salt. The B 1s can be deconvoluted into two peaks: one originating from B-O bonds formed by LiBOB decomposition on the cathode, and the other one at higher energy from oxalate groups of the BOB anion that remain adsorbed on the electrode surface 51. The higher relative intensity of BOB to B-O in the aqueous-based NMC622 compared to the PVdF-based cathode indicates less salt decomposition in agreement with the other spectra.

Overall, from the XPS analysis of the PVdF- and aqueous-processed NMC622, a complete coverage of the active material particles is observed with the aqueous-processed (CMC-latex) formulation. While this can contribute to higher cell resistances and lower discharge capacity observed with this cathode, the capacity retention is slightly higher. These results indicate that the coverage of the cathode particles contributes to the resistance but at the same time prevents electrolyte decomposition to a larger extent compared to the uncovered particles in the PVdF-based cathode. Furthermore, more carbonate species are observed on the NMC622(PVdF) surface than on the aqueous-processed NMC622 with both electrolytes, although to a larger extent with the fluorine-free electrolyte. Salt decomposition from the presence of phosphate and boron-based

species is detected in all cells. Comparing the two electrolytes, a thicker layer is observed with the LiBOB-based electrolytes which correlates with the higher resistance seen with this electrolyte already in the first cycle with both types of cathode formulations.

Anodes. The C 1s and O 1s spectra of the silicon-graphite anode electrode pristine and cycled against NMC622(PVdF) and NMC622(aqueous) are shown in Figure 7. In the C 1s spectra of the pristine sample (Figure 7 a), the largest components are C-C, C=C and C=O-O. C-C mostly originates from binder (LiPAA), graphite and carbon black. The C=C bond component can be attributed to graphitic carbon from graphite and carbon black. The other peak attributed to C=O-O mainly comes from the LiPAA binder. The other bonds, C-O, C=O, and CO₃ come from the surface species from graphite, carbon black, and the binder ²⁷.

The cycled samples show a significant decline in the peak intensity for the C=C, indicating the formation of the SEI layer. However, the continued visibility of the C=C peak in all cycled samples indicates that the SEI layer thickness does not exceed the XPS probing depth. Moreover, analysis of the Si 2p spectra (Figure S10) shows a clear Si signal in the anode samples – most pronounced in those paired with the PVdF-based cathode. Given the XPS probing depth of

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approximately 14 nm, this confirms that the SEI layer thickness is near 14 nm.

The remaining components with different relative intensities in the C 1s spectra C–O, C=O, O=C–O, and CO_3 arise from lithium alkoxides (ROLi), lithium alkyl carbonates (ROCO₂Li), and Li_2CO_3 , all formed by decomposition of the electrolyte during cycling ⁵². The partially lithiated phase of carbon leads to formation of Li_xC ²⁷ and the C–F peak appears only for the fluorinated electrolyte.

The C 1s and O 1s spectra of the anode electrode cycled against the PVdF-based cathode with fluorinated electrolyte shows an increase in C-O compared to the pristine anode attributed to the decarboxylation of the carbonate solvents and/or additives 53. With the fluorine-free electrolyte, the main peaks correspond to ester and carbonate species followed by C-O. This is indicative of BOB anion decomposition leading to oxalates (esters) 44 28 and carbonates from solvents and VC additive 40. In the case of the O 1s, the fluorine-free electrolyte shows an additional peak corresponding to OH, observed previously for the same anode and electrolyte ²⁷. Different features are observed when cycled against the aqueous-based cathode. With the fluorinated electrolyte, there is a large contribution from C=O and C-F species and to a minor degree C-O species. The C-F bond at a high energy arising from organic fluorinated species most likely comes from the reduction of FEC 54. The O 1s spectrum shows a relatively intense peak attributed to Li₂O observed previously with silicon electrodes 55 56 40.

The anode cycled in the fluorine-free electrolyte features mainly carbonates, followed by C=O and esters most likely from LiBOB and VC/solvent decomposition or LiBOB residues remaining on the electrode after washing with EMC ²⁸. Li₂O is also present in the O 1s spectrum although to a much lower degree compared to the fluorinated electrolyte.

The F 1s of anodes cycled with fluorinated electrolyte with NMC622(PVdF) and NMC622(aqueous) are shown in Figure S11a,b, respectively. In both cases, it is dominated by LiF, although there are other minor components assigned to organofluorine compounds, and P–F, coming from the degradation of the additive FEC and the LiPF₆ salt on the anode surface 57 . The corresponding P 2p spectra (Figure S12) shows different phosphate peaks, confirming that the SEI layer with the fluorinated electrolyte has inorganic species from

salt decomposition and LiPF $_6$ salt remaining on the anode AS shown in Figure S11b and S12b, the F 1s and P 2p spectra of the anode cycled with the fluorinated electrolyte and NMC622(aqueous) cathode contain larger contributions from PF $_6$ - and organofluorine compounds, compared to the anode cycled with the NMC622(PVdF) cathode that mainly contain LiF and PF $_x$ O $_y$. This suggests more salt decomposition on the anode when cycled with NMC622(PVdF).

B 1s spectra of Si-graphite electrodes cycled in fluorine-free electrolyte from cells with PVdF-based cathodes (Figure S13a) and aqueous-processed cathodes (Figure S13b) show the presence of B—O and BOB- species. The B 1s spectrum can be deconvoluted into two peaks: one originating from B—O bonds formed by LiBOB decomposition on the anode, and the other from oxalate groups of the BOB anion that remain adsorbed on the electrode surface. These could come from LiBOB salt residues and/or decomposition of LiBOB on the anode side with higher relative intensity of the latter when paired with NMC622(PVdF) ⁵⁸. This follows the same trend as with the fluorinated electrolyte, with less salt degradation with the aqueous-based NMC622.

Overall, fluorine-free electrolytes form an oxygen-rich SEI layer on the anode composed of carbonates, esters and ether species in different ratios as previously reported ²⁷. In addition, these results show different electrolyte decomposition mechanisms on the anode depending on the cathode's formulation. More salt decomposition is observed on the anode when cycled with NMC622(PVdF), as seen from the higher relative intensity of PF_xO_y and B–O species for each electrolyte. In contrast, with the fluorinated electrolyte more decomposition products from the solvent and additives are observed in the C 1s and O 1s spectra on the anode cycled with NMC622(aqueous) forming C-F, C=O and Li₂O products. With the fluorine-free electrolyte it is the ratio of the decomposition products that is the main difference between the two cells with the different cathode formulations. The one with NMC622(PVdF) shows higher contribution from ester compared to carbonates, which has been previously assigned to LiBOB decomposition and VC unable to protect the silicon electrode fully 40. When cycled with NMC622(aqueous), a higher contribution from carbonate species is observed, which is assigned to VC decomposition and therefore preventing to some degree LiBOB decomposition resulting in a better SEI. These results correlate with the improved cycling stability, and

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higher capacity retention, as reported previously with silicon wafers $_{\rm 40}$

In summary, the LiBOB-based electrolyte mainly forms carbonate species on the cathode's surface regardless of its composition and a slightly thicker CEI compared to the LiPF₆-based electrolyte. Between the PVdF- and aqueous-processed cathodes, the better coverage of the latter seems to prevent electrolyte decomposition to a larger extent, influencing the SEI layer on the anode. The higher intensity of the carbonate peaks with the fluorine-free electrolyte and NMC622(aqueous) also suggests a better SEI formed from the VC additive instead of LiBOB decomposition. These results agree with the higher capacity retention observed with the fluorine-free aqueous-based NMC622 cathode. Furthermore, the similar cycling stability obtained with the two electrolytes confirm the potential competitiveness of fully fluorine-free lithium-ion batteries, contributing to lower toxicity and more sustainability.

Conclusion

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The effect of fluorine-free components in the electrolyte and binder in full cells containing a silicon-graphite composite anode and NMC622 cathode was investigated. Long-term galvanostatic cycling at C/2 show that the fluorine-free electrolyte can perform comparably to state-of-the-art fluorinated electrolytes with capacity retention of 56.2% and 58.3%, respectively, after 500 cycles. The capacity retention increased when using an aqueous-processed fluorine-free binder (CMC-Latex) in the cathode, reaching 61% and 65% after 500 cycles for the fluorine-free and fluorinated electrolytes, respectively. Despite the similar capacities, cell resistance measurements from the intermittent current interruption technique revealed slightly larger values for the cells cycled with the aqueous-processed cathodes and the fluorine-free electrolytes compared to the highly fluorinated electrolyte and binder. Furthermore, the rate capability measurements showed that increasing the C-rate to 2C limits the performance of both cells, with the performance deterioration being relatively more pronounced with the fluorine-free electrolyte.

Surface analysis by SEM, EDS, and XPS was performed on the pristine and cycled samples after 280 cycles. The basic morphology of both electrodes remained well-preserved after cycling with both electrolytes, however, interfacial layer coverage can be seen on both

electrodes attributed to the electrolyte decomposition forming the SEI and CEI layers. On the cathode side, the fluorine-free electrolyte decomposes forming more carbonate-based species than the fluorinated electrolytes, regardless of the cathode's formulation. The coverage of the active material with CMC-latex and aqueous-based processing increases cell resistance but prevents electrolyte decomposition. On the anode side, a preferential decomposition of the fluorinated electrolyte was observed on the silicon particles while LiBOB preferentially decomposed on the graphite particles. Furthermore, the SEI composition was different depending on the cathode's formulation. With the aqueous-based cathode, less salt decomposition was observed on the anode with both electrolytes. In particular, with the fluorine-free electrolyte a preferential decomposition of VC on the anode surface prevented the LiBOB decomposition improving the cycling stability.

In conclusion, these results demonstrate that the high-energy-density full cells (NMC622||Si-graphite) with PFAS-free binders and fluorine-free electrolyte could perform as well as highly fluorinated cells. This study serves as a proof of concept and paves the way towards more environmentally friendly, high-energy-density, and safer lithium-ion batteries.

Author contributions

Conceptualization: G.H.; Data curation, analysis, investigation, validation and visualization: G.H., S.M. and A.J.N. Funding acquisition: J.M.; Project administration: G.H. and J.M.; Supervision: G.H. Writing — original draft: G.H. and S.M.; review & editing: S.M., A.J.N., J.M. and G.H.

Conflicts of interest

There are no conflicts to declare.

Data availability

The data that support the findings of this study are available from the corresponding author upon reasonable request.

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References

- S. Duehnen, J. Betz, M. Kolek, R. Schmuch, M. Winter and T. Placke, *Small Methods*, 2020, **4**, 2000039.
- A. Rensmo, E. K. Savvidou, I. T. Cousins, X. Hu, S. Schellenberger and J. P. Benskin, *Environmental Science: Processes & Impacts*, 2023, **25**, 1015–1030.
- 3 F. Spyrakis and T. A. Dragani, *Toxics*, 2023, **11**, 721.
- T. F. Burton, J. L. Gómez Urbano, Y. Zhu, A. Balducci and O. Fontaine, *Nature Communications*, 2025, **16**, 5957.
- K. S. Teoh, M. Melchiorre, S. Darlami Magar, M. Hermesdorf, D. Leistenschneider, M. Oschatz, F. Ruffo, J. L. Gómez Urbano and A. Balducci, *Advanced Materials*, 2024, 36, 2310056.
- 6 S. Lander, M. Vagin, V. Gueskine, J. Erlandsson, Y. Boissard, L. Korhonen, M. Berggren, L. Wågberg and X. Crispin, Advanced Energy and Sustainability Research, 2022, 3, 2200016.
- J. Miyake and K. Miyatake, *Polymer journal*, 2017, 49, 487–495.
- 8 H. J. Lee, H.-S. Jung, J. G. Kim, Y. W. Kim and C. Pak, ACS Applied Materials & Interfaces, 2025, 17, 5268–5277.
- D. Bresser, D. Buchholz, A. Moretti, A. Varzi and S.
 Passerini, Energy & Environmental Science, 2018, 11, 3096–3127.
- 10 R. Shunmugasundaram, R. S. Arumugam, P. Benedek, M. Yarema, P. Baade and V. Wood, *Journal of The Electrochemical Society*, 2022, **169**, 60504.
- 11 F. Nagler, N. Christian, A. Gronbach, F. Stahl, P. Daubinger, A. Flegler, M. Hofmann and G. A. Giffin, *ChemElectroChem*, 2024, **11**, e202300748.
- 12 M. Bichon, D. Sotta, N. Dupré, E. De Vito, A. Boulineau, W. Porcher and B. Lestriez, *ACS applied materials & interfaces*, 2019, **11**, 18331–18341.
- M. Bichon, D. Sotta, E. De Vito, W. Porcher and B. Lestriez, *Journal of Power Sources*, 2021, **483**, 229097.
- 14 A. C. Rolandi, C. Pozo-Gonzalo, I. de Meatza, N. Casado, M. Forsyth and D. Mecerreyes, *ACS Applied Energy Materials*, 2023, **6**, 8616–8625.
- W. Mrozik, M. A. Rajaeifar, O. Heidrich and P. Christensen, Energy & Environmental Science, 2021, 14, 6099–6121.
- 16 Y. Xu, A. Filippov, M. R. Shimpi, F. Ullah Shah and P. Johansson, *Batteries & Supercaps*, 2025, **8**, e202400672.
- 17 P. Jiang, L. Chen, H. Shao, S. Huang, Q. Wang, Y. Su, X. Yan, X. Liang, J. Zhang and J. Feng, *ACS Energy Letters*, 2019, **4**, 1419–1426.
- 18 Y. Shuai, Y. Hu, X. Gong, Z. Xu, L. Li, L. Zhang, M. Li, J. Zhou

- and M. Li, Chemical Engineering Journal, 2025, 505 ticle Online 159101. DOI: 10.1039/D5TA06760J
- 19 G. Hernández, R. Mogensen, R. Younesi and J. Mindemark, *Batteries & Supercaps*, 2022, **5**, e202100373.
- F. Wu, A. Mullaliu, T. Diemant, D. Stepien, T. N. Parac-Vogt, J. Kim, D. Bresser, G. Kim and S. Passerini, *InfoMat*, 2023, 5, e12462.
- T. M. Nguyen, D. W. Kim, D. Y. Kim, G. Choi, J. Suk and Y. Kang, *ACS Applied Energy Materials*, 2022, **5**, 15768–15779.
- S. Wen, Y. Han, P. Wang, D. Zhao, X. Cui, L. Zhang and S. Li, Acs Applied Energy Materials, 2021, 4, 12525–12534.
- 23 K. Xu, S. Zhang, T. R. Jow, W. Xu and C. A. Angell, *Electrochemical and Solid-State Letters*, 2001, **5**, A26.
- 24 K. Xu, S. Zhang, B. A. Poese and T. R. Jow, *Electrochemical and Solid-State Letters*, 2002, **5**, A259.
- 25 K. Xu, S. S. Zhang, U. Lee, J. L. Allen and T. R. Jow, *Journal of Power Sources*, 2005, **146**, 79–85.
- 26 K. Xu, Journal of The Electrochemical Society, 2008, 155, A733.
- 27 G. Hernández, A. J. Naylor, Y.-C. Chien, D. Brandell, J. Mindemark and K. Edström, ACS Sustainable Chemistry & Engineering, 2020, 8, 10041–10052.
- Y.-C. Weng, R. Andersson, M.-T. Lee, J. Mindemark, A. Lindblad, M. Hahlin and G. Hernández, *Journal of The Electrochemical Society*, 2024, **171**, 60527.
- 29 R. Gond, H. D. Asfaw, O. Hosseinaei, K. Edstrom, R. Younesi and A. J. Naylor, *ACS Sustainable Chemistry & Engineering*, 2021, **9**, 12708–12717.
- L. Dettmann, L. O. S. Colbin and A. J. Naylor, Advanced Materials Interfaces, 2025, 2500262.
- 31 M. J. Lacey, K. Edström and D. Brandell, *Chemical Communications*, 2015, **51**, 16502–16505.
- 32 Y.-C. Chien, H. Liu, A. S. Menon, W. R. Brant, D. Brandell and M. J. Lacey, *Nature Communications*, 2023, **14**, 2289.
- A. Jablonski and C. Powell, *National Institute of Standards* and *Technology, Gaithersburg*.
- S. Tanuma, C. J. Powell and D. R. Penn, *Surface and interface analysis*, 1994, **21**, 165–176.
- M. Gautam, G. K. Mishra, K. Bhawana, C. S. Kalwar, D. Dwivedi, A. Yadav and S. Mitra, ACS Applied Materials & Interfaces, 2024, 16, 45809–45820.
- N. Hamzelui, M. Linhorst, G. Martin Nyenhuis, L. Haneke,
 G. G. Eshetu, T. Placke, M. Winter, B. M. Moerschbacher
 and E. Figgemeier, *Energy Technology*, 2023, 11, 2201239.
- 37 S. Hiwase, N. Kumar and M. Furquan, *Chemical Engineering Journal*, 2024, **498**, 155085.
- K. Kim, I. Park, S.-Y. Ha, Y. Kim, M.-H. Woo, M.-H. Jeong, W.
 C. Shin, M. Ue, S. Y. Hong and N.-S. Choi, *Electrochimica Acta*, 2017, 225, 358–368.
- 39 C. L. Berhaut, D. Z. Dominguez, P. Kumar, P.-H. Jouneau, W. Porcher, D. Aradilla, S. Tardif, S. Pouget and S. Lyonnard, *ACS Nano*, 2019, **13**, 11538–11551.
- Z. Lu, T. Patranika, A. J. Naylor, J. Mindemark, S. Tardif, G. Hernández and S. Lyonnard, Small, 2025, 2410654.
- 41 R. Sahore, D. L. Wood III, A. Kukay, K. M. Grady, J. Li and I. Belharouak, ACS Sustainable Chemistry & Engineering,

Dpen Access Article. Published on 21 October 2025. Downloaded on 10/24/2025 1:28:11 AM.

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Journal Name ARTICLE

2020, **8**, 3162–3169.

W. Zhao, I. Zou, I. Zheng, H. Jia, I. Song, M. H. Engelhard, C.

DOI: 10.1039/D5TA067603

- W. Zhao, L. Zou, J. Zheng, H. Jia, J. Song, M. H. Engelhard, C. Wang, W. Xu, Y. Yang and J. Zhang, *ChemSusChem*, 2018, 11, 2211–2220.
- 43 T. Kim, L. K. Ono and Y. Qi, *Journal of Materials Chemistry A*, 2023, **11**, 221–231.
- 44 T. Melin, R. Lundström and E. J. Berg, *The Journal of Physical Chemistry Letters*, 2024, **15**, 2537–2541.
- C. Misiewicz, K. Edstrom and E. J. Berg, Chemistry of Materials, 2024, 36, 9729–9740.
- 46 Y. Zhu, Y. Li, M. Bettge and D. P. Abraham, *Electrochimica Acta*, 2013, **110**, 191–199.
- 47 H. Liu, A. J. Naylor, A. S. Menon, W. R. Brant, K. Edström and R. Younesi, *Advanced Materials Interfaces*, 2020, **7**, 2000277.
- 48 A. M. Andersson, D. P. Abraham, R. Haasch, S. MacLaren, J. Liu and K. Amine, *Journal of The Electrochemical Society*, 2002, **149**, A1358.
- 49 K. Edstroem, T. Gustafsson and J. O. Thomas, *Electrochimica Acta*, 2004, **50**, 397–403.
- 50 K. Beltrop, S. Klein, R. Nölle, A. Wilken, J. J. Lee, T. K.-J. Köster, J. Reiter, L. Tao, C. Liang and M. Winter, *Chemistry of Materials*, 2018, **30**, 2726–2741.
- 51 E. K. W. Andersson, L.-T. Wu, L. Bertoli, Y.-C. Weng, D. Friesen, K. Elbouazzaoui, S. Bloch, R. Ovsyannikov, E. Giangrisostomi, D. Brandell, J. Mindemark, J. C. Jiang and M. Hahlin, *Journal of Materials Chemistry A*, 2024, 12, 9184–9199.
- Y. He, Z. Chen and Y. Zhang, Iscience.
- E. Markevich, G. Salitra and D. Aurbach, *ACS Energy Letters*, 2017, **2**, 1337–1345.
- S. Ahn, M. Fukushima, H. Nara, T. Momma, W. Sugimoto and T. Osaka, *Electrochemistry Communications*, 2021, 122, 106905.
- B. Philippe, R. Dedryvère, M. Gorgoi, H. Rensmo, D.
 Gonbeau and K. Edström, *Chemistry of Materials*, 2013, 25, 394–404.
- C. Cao, I. I. Abate, E. Sivonxay, B. Shyam, C. Jia, B. Moritz, T.
 P. Devereaux, K. A. Persson, H.-G. Steinrück and M. F.
 Toney, *Joule*, 2019, 3, 762–781.
- 57 G. Jiang, J. Liu, J. He, H. Wang, S. Qi, J. Huang, D. Wu and J. Ma, *Advanced Functional Materials*, 2023, **33**, 2214422.
- S. Jiao, X. Ren, R. Cao, M. H. Engelhard, Y. Liu, D. Hu, D.
 Mei, J. Zheng, W. Zhao and Q. Li, *Nature Energy*, 2018, 3, 739–746.

Data Availability Statement

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Fluorine-Free Lithium-Ion Battery Features Comparable Cycling Performance to a Highly Fluorinated Equivalent

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Data Availability Statement

- The data presented in this article are in the format of figures
- The data supporting this article have been included as part of the Supplementary Information