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# Electrochemical nitrate reduction to ammonia using laser-processed Nb<sub>2</sub>AlC: the role of effective Al etching†

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Electrocatalytic nitrate reduction reaction to ammonia (NH<sub>3</sub>) is a promising approach for generating NH<sub>3</sub> compared with the widely used Haber–Bosch process. It offers the advantage of zero carbon emission and helps in recycling nitrate waste. However, the challenge remains in the synthesis and engineering of proficient electrocatalytic materials with high faradaic efficiency and yield rate. Herein, we report a unique laser-processed niobium oxide-graphene (NbO<sub>x</sub>-Gr) electrode attached to a conductive support of graphene for NH<sub>3</sub> generation. The two-step fabrication process started with spatially and temporally controlled pulsed laser writing on an Nb<sub>2</sub>AlC-coated polymer surface followed by simple electrochemical etching to remove excess Al. Electrochemical analysis elucidated that the NbO<sub>x</sub>-Gr electrode exhibited improved activity for ammonia generation. Moreover, theoretical studies provide insights into the nitrate reduction reaction mechanism, confirming that the electrochemical active site was located on the Nb atom of the NbO<sub>x</sub>-Gr electrode. Laser processing is a cost-effective, less chemically hazardous, versatile, and efficient approach to utilize MAX phases for multiple energy storage and conversion applications.

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## 1 Introduction

Ammonia (NH<sub>3</sub>) is an indispensable industrial-scale chemical feedstock used in the agriculture industry; it is a hydrogen-rich and carbon-free fuel and has environmentally friendly nature.<sup>1–3</sup> The industrial-scale synthesis of NH<sub>3</sub> is largely dependent on the Haber–Bosch process. While millions of tonnes of NH<sub>3</sub> are produced annually through the Haber–Bosch process,<sup>2–8</sup> it

consumes 1–2% of global energy and contributes to 1.0% of global carbon emissions, elevating environmental hazards.<sup>9–11</sup> Another conventional approach involves nitrogen (N<sub>2</sub>) reduction to NH<sub>3</sub>, where water molecules act as proton sources. Nevertheless, the intrinsic properties of the N<sub>2</sub> molecule, like high N≡N bond dissociation energy of 941 kJ mol<sup>−1</sup> and low solubility in water, negatively impact the yield rate and selectivity of the N<sub>2</sub> to NH<sub>3</sub> conversion process.<sup>10–15</sup> Thus, developing more sustainable approaches for NH<sub>3</sub> production have recently gained significant research interest.

In this direction, the electrocatalytic nitrate reduction reaction, NO<sub>3</sub><sup>−</sup> + 6H<sub>2</sub>O + 8e<sup>−</sup> → NH<sub>3</sub><sup>+</sup> + 9OH<sup>−</sup>, has high potential as it offers a sustainable route and provides a plethora of advantages such as (i) less environmental impact and high feedstock availability, *i.e.*, nitrate (NO<sub>3</sub><sup>−</sup>) ions are produced as agricultural fertilizers and industrial waste;<sup>15–17</sup> this waste can be utilized for NH<sub>3</sub> generation, making this route environmentally friendly while simultaneously remedying nitrate waste, (ii) high energy efficiency: NO<sub>3</sub><sup>−</sup> reduction to ammonia consumes less energy as the dissociation energy for N=O in the NO<sub>3</sub><sup>−</sup> ion is approximately 204 kJ mol<sup>−1</sup>, which is lesser compared to other approaches, (iii) high solubility: the solubility of the NO<sub>3</sub><sup>−</sup> ion (880 g L<sup>−1</sup>) in H<sub>2</sub>O is superior compared to of N<sub>2</sub> (0.02 g L<sup>−1</sup>).<sup>15–20</sup>

Thus, the adsorption of the NO<sub>3</sub><sup>−</sup> ions on the electrocatalyst surface is more efficient, leading to enhanced electrochemical performance.<sup>21,22</sup> However, a major obstacle in producing ammonia from NO<sub>3</sub><sup>−</sup> ions is the competing hydrogen evolution

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reaction (HER), leading to lower faradaic efficiency.<sup>23,24</sup> Currently, noble and non-noble metal-based electrocatalysts,<sup>25</sup> such as Pt-TiO<sub>2</sub>,<sup>26</sup> copper-based catalysts,<sup>27</sup> metal oxides,<sup>28</sup> and 2D materials,<sup>29</sup> have been explored as electroactive materials for the nitrate reduction reaction. Nevertheless, these electrocatalyst materials face some limitations, such as high cost, low abundance, susceptibility to leaching, and predominance of the HER at high potentials.<sup>30–32</sup> Therefore, developing new electrocatalyst materials for the effective conversion of NO<sub>3</sub><sup>-</sup> into NH<sub>3</sub> is crucial.

In this context, ternary-layered MAX phases with their unique blend of metallic and ceramic properties, along with high thermal stability and a combination of covalent and metallic bonds, offer substantial potential for electrochemical energy conversion applications.<sup>33,34</sup> Typically, MAX phases are employed to fabricate MXenes by removing aluminium layers using hazardous acids (HF).<sup>35</sup> Thus, HF-free approaches are gaining significant attention.<sup>36</sup> It is noteworthy here that recently MAX phases have gained significant attention for energy applications.<sup>37</sup> However, MAX phases for electrocatalytic nitrate reduction reactions have not been reported. The major obstacles in this context are tuning their electrical properties and removing aluminium layers to fabricate a well-ordered architecture that utilizes the full potential of MAX phases.<sup>33–38</sup> To resolve these issues, heterostructure engineering,<sup>39</sup> interface engineering,<sup>40</sup> and doping approach<sup>41</sup> have been explored to enhance the electrochemical performance of MAX phases.<sup>42–44</sup>

Herein, we reported a versatile, single-step, cost-effective, less chemically hazardous laser processing approach for fabricating the heterostructures of MAX (Nb<sub>2</sub>AlC) with graphene.<sup>45</sup> This involves a single-step laser processing of Nb<sub>2</sub>AlC decorated over graphene. Subsequently, to eradicate the aluminium content from the laser-processed Nb<sub>2</sub>AlC, an electrochemical etching approach is employed. The fabricated Nb matrix-loaded

graphene (NbO<sub>x</sub>-Gr) electrodes were employed for electrocatalytic nitrate reduction reaction to generate NH<sub>3</sub>. This approach to fabricate NbO<sub>x</sub>-Gr electrode using Nb<sub>2</sub>AlC-coated PI, employing laser treatment followed by electrochemical etching enables the utilisation of MAX phases more efficiently without the use of hazardous HF and opens the door for exploring a broad range of different MAX phases and other 2D materials integrated with graphene for diverse applications beyond energy conversion and storage applications.

## 2 Results and discussion

### 2.1 Fabrication process

First Nb<sub>2</sub>AlC-coated polyimide sheets are subjected to laser irradiation using a diode-pumped Nd:YAG solid pulsed laser beam (532 nm), generating niobium-based spherical nanoparticle decorated over graphene thin films. The high-energy laser pulses create substantial mechanical stress and thermal shock on the stacked 2D Nb<sub>2</sub>AlC nanosheets, leading to the formation of small fragments of NbO<sub>x</sub> spherical nanoparticles. Concurrently, the infrared energy is absorbed by the PI sheet, generating a temperature exceeding 2000 K within a millisecond range, enabling the photothermal transformation of the polyimide into graphene (Fig. 1a).

In the subsequent step, an electrochemical etching route is employed to eliminate the excess aluminium metal using the chronoamperometry method with 3 M HCl as an electrolyte in a three-electrode setup. The chloride ions (Cl<sup>-</sup>) ions in the HCl electrolyte react with the Al in the fragmented Nb<sub>2</sub>AlC and form aluminium chloride (AlCl<sub>3</sub>).<sup>46,47</sup> Nonetheless, compared to the traditional approach, this process eliminates the reliance on toxic and hazardous HF-based compounds, while maximizing the usage of the MAX phase efficiently (Fig. 1b). The details of the fabrication process are outlined in the experimental section.

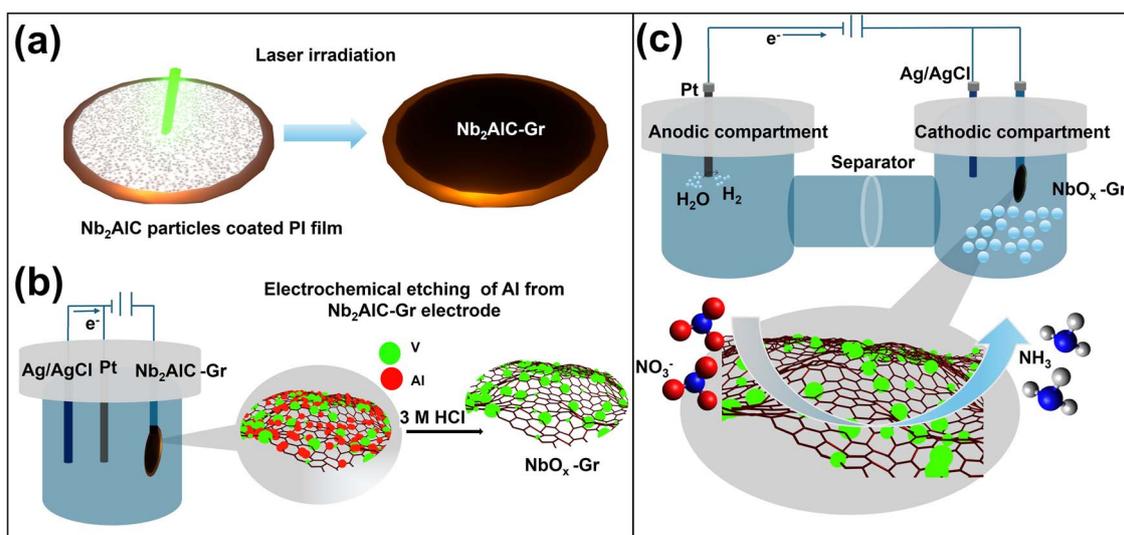


Fig. 1 (a) Schematic of the conversion of the Nb<sub>2</sub>AlC-coated polyimide sheet into Nb<sub>2</sub>AlC-graphene electrodes through laser processing. (b) Subsequent *in situ* electrochemical etching of the Nb<sub>2</sub>AlC-Gr electrode in 3 M HCl electrolyte. (c) Nitrate reduction to generate ammonia using a three-electrode setup with the NbO<sub>x</sub>-Gr electrode.



In the application context, the electrocatalytic nitrate reduction reaction to generate  $\text{NH}_3$  was carried out using a three-electrode set-up employing an H-type electrolytic cell with a frit separation. In the three-electrode setup, Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  are employed as the working electrode, Platinum (Pt) as the counter electrode and  $\text{Ag/AgCl}$  as the reference electrode utilizing 0.5 M  $\text{Na}_2\text{SO}_4$  as the electrolyte and 0.1 M  $\text{KNO}_3$  as the nitrate source (Fig. 1c). We investigated the physical and chemical composition, followed by morphological analysis of these electrodes in the following sections.

## 2.2 Material characterization

To investigate the material composition analysis and to select suitable electrodes after electrochemical etching for the electrochemical application, X-ray photoelectron spectrum (XPS) analysis was carried out. Wide survey spectrum analysis was employed to confirm the effectiveness of the etching process and to select the appropriate electrodes for the electrochemical analysis. To enable a comprehensive comparison of aluminium removal we varied the etching time (6, 12, 18, and 24 hours) during the electrochemical etching process. XPS analysis of each electrode was carried out to verify the efficiency of Al removal with varying etching times.

Note that laser-treated electrochemically etched electrodes only displayed peaks for Nb 3d, C 1s, and O 1s, indicating the effective removal of aluminium from the electrode surface (Fig. 2a). The extracted elemental composition information in atomic percentages from XPS survey spectra is provided in Table 1, which shows that aluminium accounted for 8.66% in the commercial  $\text{Nb}_2\text{AlC}$  sample, 0.39% in the  $\text{Nb}_2\text{AlC-Gr}$  electrode, and was undetectable in the electrochemically etched electrodes. This validates the effectiveness of aluminium removal through the *in situ* electrochemical etching process.

Before testing the electrodes for the electrochemical application, the selection of the appropriate electrochemically etched electrode for the nitrate reduction to ammonia is essential.

Table 1 Influence of varying time of *in situ* electrochemical etching on element composition in atomic (%) (obtained from XPS survey spectra)

| Samples   | Nb (at%) | Al (at%) | C (at%) | O (at%) |
|---|----------|----------|---------|---------|
| Commercial- $\text{Nb}_2\text{AlC}$             | 10.31    | 8.66     | 40.35   | 40.69   |
| $\text{Nb}_2\text{AlC-Gr}$                      | 1.09     | 0.39     | 88.50   | 10.02   |
| $\text{Nb}_2\text{AlC-Gr-6 h}$                  | 1.03     | —        | 90.83   | 8.14    |
| $\text{Nb}_2\text{AlC-Gr-12 h}$                 | 1.61     | —        | 89.88   | 8.52    |
| $\text{Nb}_2\text{AlC-Gr-18 h}$                 | 2.84     | —        | 84.18   | 12.98   |
| $\text{Nb}_2\text{AlC-Gr-24 h/NbO}_x\text{-Gr}$ | 2.90     | —        | 86.64   | 10.45   |

Thus, we performed linear sweep voltammetry (LSV) measurements in a three-electrode setup employing 0.5 M  $\text{Na}_2\text{SO}_4$  as the electrolyte, as illustrated in Fig. S1 in ESI.† We observed that the  $\text{NbO}_x\text{-Gr}$  electrode subjected to the etching process for 24 h exhibited enhanced electrochemical performance compared to the  $\text{Nb}_2\text{AlC-Gr}$ , and other etching time variants (6 h, 12 h, and 18 h). Thus, we selected the  $\text{NbO}_x\text{-Gr-24 h}$  electrode for further investigation, and we named the electrode  $\text{NbO}_x\text{-Gr}$  throughout the manuscript.

X-ray diffraction (XRD) patterns were acquired to investigate the phase transition of the commercial- $\text{Nb}_2\text{AlC}$ , Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  electrodes as illustrated in Fig. 2b. The diffraction peaks detected for the commercial- $\text{Nb}_2\text{AlC}$  powder correspond closely to those previously reported  $\text{Nb}_2\text{AlC}$  MAX phases, indicating the absence of impurities.<sup>48</sup> The Gr demonstrated a characteristic graphene peak and additional peaks corresponding to the PI substrate.<sup>49</sup> The (002) peak associated with  $\text{Nb}_2\text{AlC}$  disappeared in the  $\text{Nb}_2\text{AlC-Gr}$  electrode, indicating a phase transformation induced by laser treatment. Likewise, in the  $\text{NbO}_x\text{-Gr}$  electrode, the (002) peak was absent, and it exhibited new peaks, potentially corresponding to the niobium oxide composite with graphene formed after the electrochemical etching treatment.<sup>50</sup> The XRD pattern confirms the phase transformation of the  $\text{Nb}_2\text{AlC}$  MAX phase.

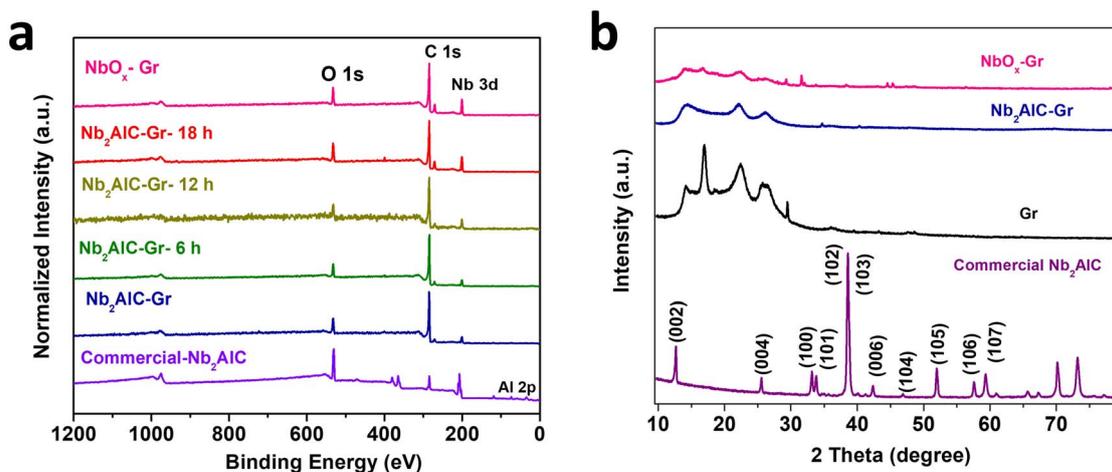


Fig. 2 Physical characterization of commercial  $\text{Nb}_2\text{AlC}$  powder, Gr,  $\text{Nb}_2\text{AlC-Gr}$  and  $\text{NbO}_x\text{-Gr}$  electrodes. (a) XPS survey spectra demonstrating the time-dependent electrochemical etching of Al metal. Commercial  $\text{Nb}_2\text{AlC}$  powder was compared with  $\text{Nb}_2\text{AlC-Gr}$ ,  $\text{Nb}_2\text{AlC-Gr-6 h}$ ,  $\text{Nb}_2\text{AlC-Gr-12 h}$ ,  $\text{Nb}_2\text{AlC-Gr-18 h}$ , and  $\text{NbO}_x\text{-Gr}$  electrodes. (b) XRD spectra of commercial  $\text{Nb}_2\text{AlC}$  powder, Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  electrodes.



We utilized Raman spectroscopy to correlate the phase transformation findings observed in the XRD measurements and to investigate the changes in the Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes. The outcome reveals that two Raman-active E<sub>2g</sub> and A<sub>1g</sub> optical modes of the Nb<sub>2</sub>AlC MAX phase are absent in the Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrode samples, as illustrated in Fig. S2a–c.† According to the existing literature, the E<sub>2g</sub> optical mode (theoretical value ≈ 181.5 cm<sup>-1</sup>) corresponds to the Nb and C atoms' in-plane oscillations, coupled with minor contributions from Al atom oscillations. The observed suppression of the E<sub>2g</sub> mode could be attributed to the substitution of the Al atom with lighter O atoms. The absence of the A<sub>1g</sub> optical mode (theoretical value ≈ 262.8 cm<sup>-1</sup>) corresponds to the Nb and C atom's symmetric vibrations out-of-plane and could be associated with an expansion in layer spacing.<sup>51–53</sup> In our case the A<sub>1g</sub> optical mode could undergo a shape transformation and downshift due to the laser and etching treatment. The suppression of the optical mode in the Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes confirms the etching of Al and phase transformation, corroborated by the XRD measurements.<sup>51–53</sup> Besides, after the laser treatment, the intensity of D bands does not have a significant difference in the Gr and Nb<sub>2</sub>AlC-Gr samples. However, the D band in the NbO<sub>x</sub>-Gr increased after electrochemical etching, while the intensity of the G band decreased, which indicates an increase in defects. We also determined the coherence length (*L<sub>a</sub>*) of the graphene layered structure along *ab* planes (see details in the ESI†). The coherence lengths of NbO<sub>x</sub>-Gr, Nb<sub>2</sub>AlC-Gr, and Gr electrodes are 16.31 nm, 21.40 nm, and 22.97 nm, respectively. This trend in coherence length implies that crystallinity is crippled along the *ab* planes.<sup>54</sup> Additionally, the Raman spectra of pristine polyimide sheets are provided,<sup>55</sup>

to confirm the successful conversion of polyimide sheets into graphene (Fig. S2b†).

XRD and Raman measurements display substantial alterations in the surface chemical compositions of Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes following laser exposure and subsequent etching treatment. To validate these surface chemical composition modulations, high-resolution XPS spectra of laser treated and electrochemically etched electrodes both were recorded. To better analyze the chemical bonding environment and oxidation state of the elements and to reveal the chemical transformations in the chemical composition of the Nb<sub>2</sub>AlC-Gr electrode induced by the laser processing, individual XPS spectrum analysis for Nb 3d, Al 2p, C 1s, and O 1s was carried out. The Nb 3d high-resolution spectrum displays a doublet, with peaks at ≈ 207 eV corresponding to Nb–O 3d<sub>5/2</sub> and ≈ 210 eV to Nb–O 3d<sub>3/2</sub>, confirming the presence of Nb<sub>2</sub>O<sub>5</sub> and the Nb<sup>5+</sup> oxidation state, as illustrated in Fig. 3a.<sup>56–59</sup> Additionally, the chemical transformation of the Nb<sub>2</sub>AlC MAX phase is confirmed in the laser treated Nb<sub>2</sub>AlC-Gr electrode due to the absence of the metal-carbide bond.<sup>58,59</sup> The detailed analysis of the C 1s spectrum illustrated in Fig. 3b shows the presence of distinct types of carbon bonds like the C–C sp<sup>2</sup> bond at ≈ 284.0 eV, C–C sp<sup>3</sup> bond at ≈ 285.0 eV, and C–O bond at ≈ 286.0 eV, like those in the Nb<sub>2</sub>AlC MAX phase.<sup>52,53,59</sup> However, the absence of the Nb–C bond peak in the ≈ 282.3 eV region compared to the Nb<sub>2</sub>AlC MAX phase confirms a chemical composition transformation of the Nb<sub>2</sub>AlC phase induced by the laser processing.<sup>56–60</sup>

The high-resolution Al 2p spectrum was recorded as illustrated in Fig. 3c for the Nb<sub>2</sub>AlC-Gr electrode. A peak is detected in the ≈ 75.0 eV region, indicating the presence of oxides of

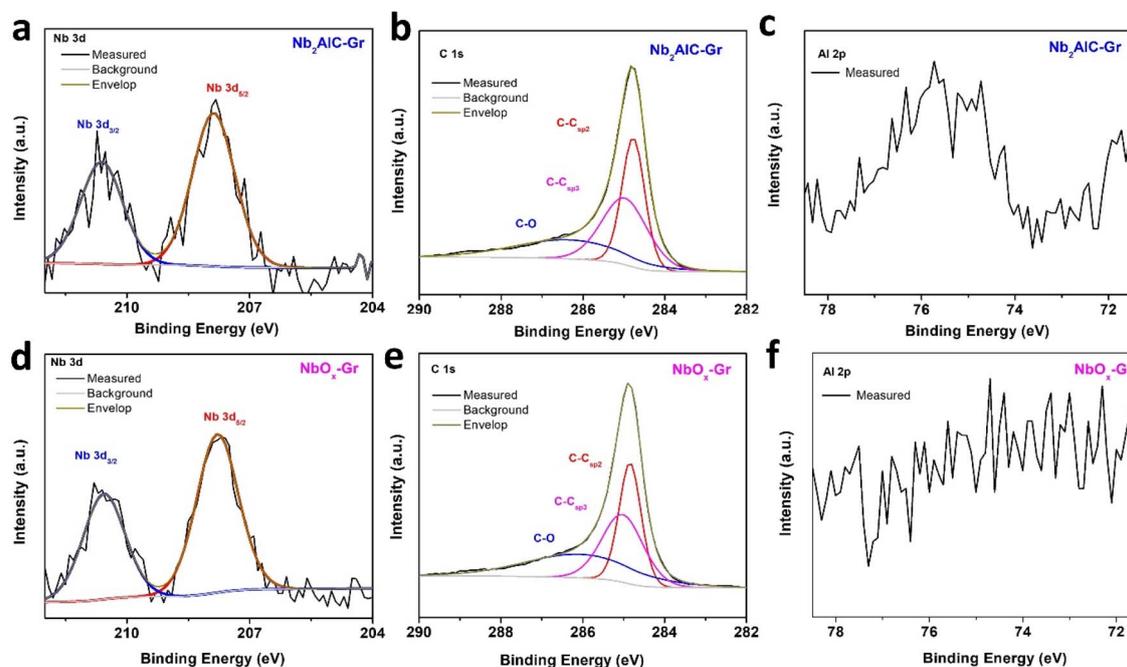


Fig. 3 Chemical composition analysis: high-resolution XPS analysis of Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes. (a and d) Nb 3d, (b and e) C 1s, and (c and f) Al 2p spectra, respectively.



Al.<sup>52,53,59</sup> Additionally, the O 1s spectrum is provided in Fig. S3a in the ESI† confirming the presence of all requisite elements in the Nb<sub>2</sub>AlC-Gr electrode.<sup>56–60</sup> For NbO<sub>x</sub>-Gr the Nb 3d core level spectrum exhibits doublet peaks, reflecting ≈ 207.0 eV for Nb–O 3d<sub>5/2</sub> and ≈ 210.0 eV for Nb–O 3d<sub>3/2</sub>, indicating the existence of the Nb<sup>5+</sup> oxidation state in Nb<sub>2</sub>O<sub>5</sub> as shown in Fig. 3d.<sup>56–60</sup> These results indicate that the Nb 3d chemical composition remains unchanged relative to the laser-processed Nb<sub>2</sub>AlC-Gr electrode.

The in-depth analysis of the carbon C 1s spectrum of the NbO<sub>x</sub>-Gr electrode as illustrated in Fig. 3e shows similar findings compared to the C 1s spectrum of the Nb<sub>2</sub>AlC-Gr electrode, the carbon bonds like the C–C sp<sup>2</sup> bond at ≈ 284 eV, C–Csp<sup>3</sup> bond at ≈ 285 eV, and C–O bond at ≈ 286.<sup>56–59</sup> The core level Al

2p spectrum, shown in Fig. 2f, confirms the absence of oxides of Al; this indicates the effective removal of Al through the electrochemical etching process. Fig. S3b in the ESI† exhibits the O 1s high-resolution spectra of the NbO<sub>x</sub>-Gr electrode. The findings from the XPS measurements corroborate the results of the XRD and Raman measurements, suggesting that laser processing modifies the chemical composition of the Nb<sub>2</sub>AlC phase, and the laser processing with the *in situ* electrochemical etching successfully removes the excess of oxides of Al from the surface of the electrodes.

The scanning electron microscopy (SEM) micrographs of the Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes are displayed in Fig. 4, where the successful integration of the Nb-rich spherical

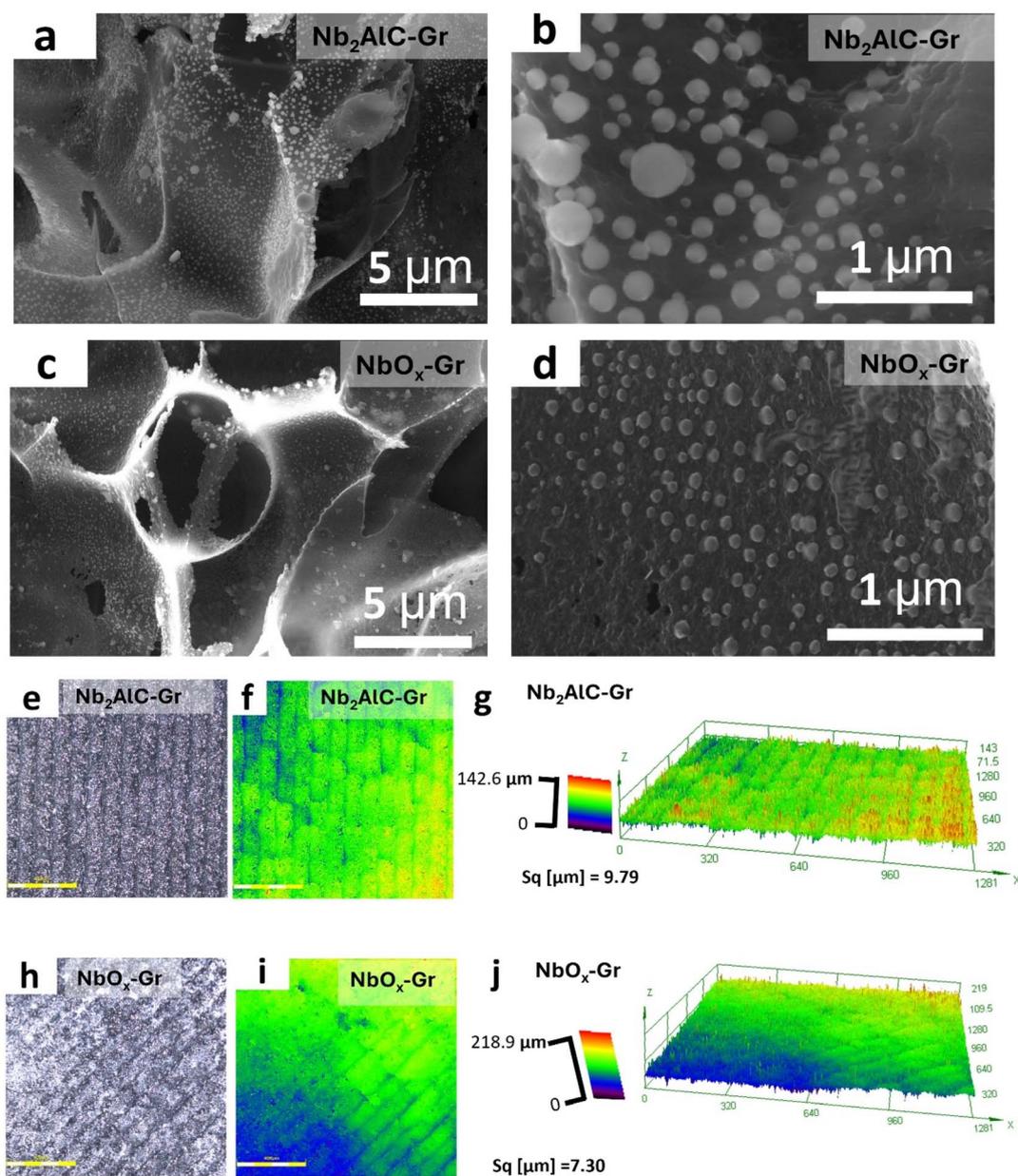


Fig. 4 Morphological characterization of Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes. SEM micrographs of Nb<sub>2</sub>AlC-Gr electrode at (a) low and (b) high magnifications, NbO<sub>x</sub>-Gr electrode at (c) low and (d) high magnifications. CLSM optical images and collective 2D and 3D false colour mapping images of (e–g) Nb<sub>2</sub>AlC-Gr electrode and (h–j) NbO<sub>x</sub>-Gr electrode; scale bar ~400 μm.



nanoparticles onto the graphene network is visualized. In the case of the Nb<sub>2</sub>AlC-Gr film, Nb-rich spherical nanoparticles are evenly distributed onto the graphene with particle sizes spanning from the micrometre ( $\mu\text{m}$ ) to the sub-nanometre (nm) scale (Fig. 4a and b). Even though the SEM images of the electrochemically etched sample NbO<sub>x</sub>-Gr elucidated a similar morphology to Nb<sub>2</sub>AlC-Gr, the particle size has decreased in NbO<sub>x</sub>-Gr as compared to Nb<sub>2</sub>AlC-Gr, as displayed in Fig. 4c and d, respectively. The SEM micrographs (low and high magnification) of bare Gr are provided in the ESI in Fig. S4a and b,<sup>†</sup> elucidating the successful formation of the graphene like structure from the polyimide sheet after laser processing.

To quantify the surface roughness of the Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes, optical micrographs were acquired using a confocal laser scanning microscope (CLSM). The topographical variations are presented in Fig. 4e and h collectively with the 2D micrographs (Fig. 4f and i) along with their 3D false colour mapping micrographs (Fig. 4g and j), where the colour variations reflect the difference in height profiles. The average surface roughness ( $S_q$ ) of the electrodes was investigated utilizing height profile analysis, yielding values of  $\approx 9.79 \mu\text{m}$  and  $\approx 7.30 \mu\text{m}$  for the Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes, respectively. These findings correlate with the SEM

morphological studies, which indicate that the particle size reduction in NbO<sub>x</sub>-Gr indeed reduces the surface roughness, causing the formation of a smoother electrode surface. Such surface modifications could potentially lead to boosting the electrochemical performance of the electrodes. STEM micrographs (Fig. S5 in ESI<sup>†</sup>) of NbO<sub>x</sub>-Gr electrodes further confirm the presence of Nb nanoparticles on the graphene sheet.

### 2.3 Electrochemical characterization for nitrate reduction reaction

Firstly, the electrochemical active surface area (ECSA) of each electrode was evaluated, as the ECSA plays an important role in the electrochemical activity of the material. The ECSA values obtained for Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr as working electrodes are  $0.03 \text{ cm}^2$ ,  $0.07 \text{ cm}^2$ , and  $0.33 \text{ cm}^2$ , respectively. The detailed experimental procedures and calculations are provided in the ESI, Fig. S6a-f.<sup>†</sup> The two-fold increase in the ECSA after integrating the Nb<sub>2</sub>AlC-MAX phase into the graphene network, followed by the additional increment due to the electrochemical etching, is beneficial for electrochemical performance.

The combination of simple laser treatment with electrochemical etching is responsible for the effective improvement

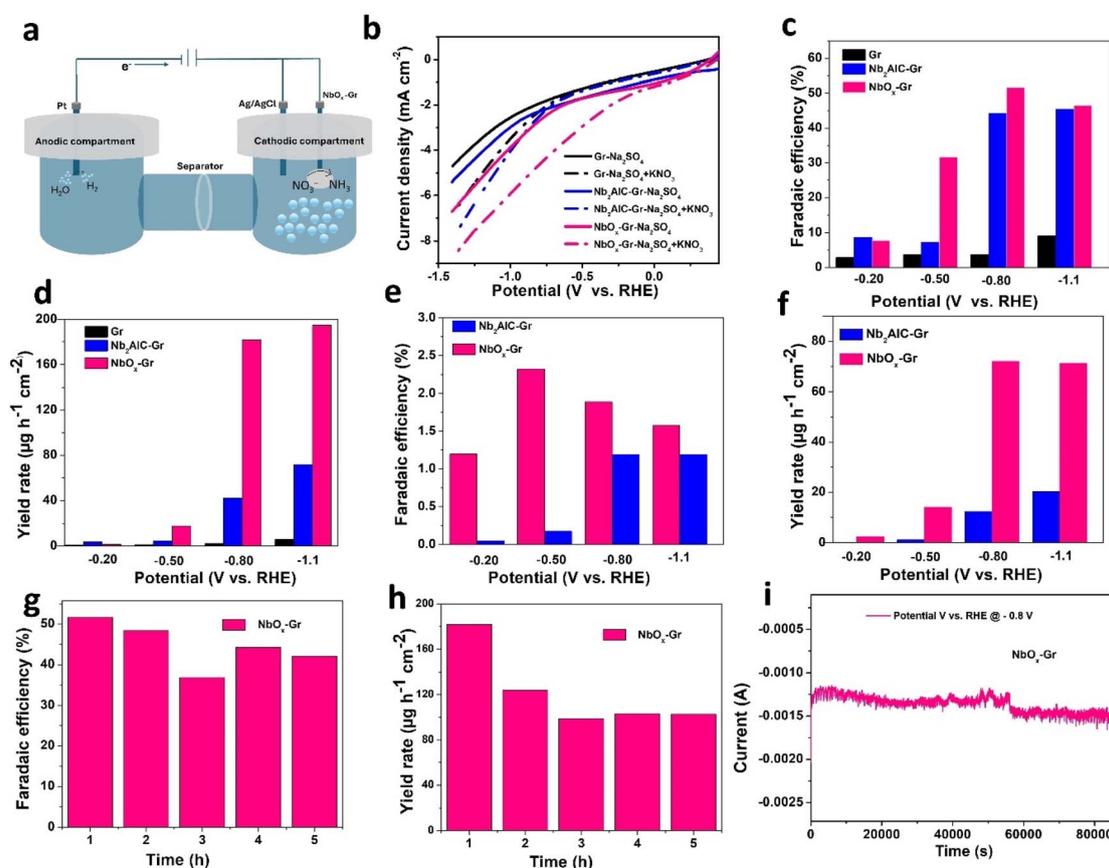


Fig. 5 Electrochemical characterization of the fabricated Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes: (a) three electrode set-up for nitrate reduction to ammonia. (b) Linear sweep voltammetry curve of Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes. (c and d) Faradaic efficiency and yield rate of Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes for ammonia detection at different potentials. (e and f) Faradaic efficiency and yield rate of Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes for nitrite detection at different potentials. (g and h) Ammonia generation measurement: faradaic efficiency and yield rate of the NbO<sub>x</sub>-Gr electrode at different times. (i) Long-term stability measurement of the NbO<sub>x</sub>-Gr electrode for 24 hours.



of ECSA of the NbO<sub>x</sub>-Gr sample. Furthermore, the electrochemical activity of the electrocatalyst material for nitrate reduction to generate NH<sub>3</sub> and by-product NO<sub>2</sub><sup>-</sup> ions is evaluated employing a three-electrode setup in an H-type glass cell, separated *via* a frit in an ambient environment, as shown in Fig. 5a. The Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr pendulum-shaped electrodes were employed as the working electrodes as illustrated in ESI Fig. S7,<sup>†</sup> where Pt acted as the counter electrode and Ag/AgCl acted as the reference electrode.

First, the linear sweep voltammetry (LSV) curve was recorded for Gr, Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr as working electrodes in the absence of NO<sub>3</sub><sup>-</sup> ions (0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolyte) and the presence of NO<sub>3</sub><sup>-</sup> ions (0.5 M Na<sub>2</sub>SO<sub>4</sub> + 0.1 M KNO<sub>3</sub> electrolyte) at a scan rate of 5 mV<sup>-1</sup> as depicted in Fig. 5b. The LSV curves demonstrate that the Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes exhibit electrochemical activity for nitrate reduction as proven by the increment in the current density, in the presence of NO<sub>3</sub><sup>-</sup> ions. The comparative LSV study further indicates that the NbO<sub>x</sub>-Gr as a working electrode is the most efficient for nitrate reduction reaction, demonstrating the highest increment in the current density among all the tested electrodes. This enhanced electrochemical performance towards the nitrate reduction reaction of NbO<sub>x</sub>-Gr aligns with the physical characterization findings, suggesting that the fabrication process involving laser treatment and *in situ* electrochemical etching of Al metal improves the electrochemical activity of the material.

To further confirm the electrochemical activity of Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes for nitrate reduction reaction, electrolysis was performed at selected potentials in the range of -0.20 to -1.10 V *vs.* RHE for 1-hour time duration, as illustrated in ESI Fig. S8a-c.<sup>†</sup> The electrolysis findings demonstrate an increase in the current density for the NbO<sub>x</sub>-Gr electrode compared to the Gr and Nb<sub>2</sub>AlC-Gr electrodes, aligning with the findings of LSV measurements. Next, the NH<sub>3</sub> concentration in the electrolytic solutions was quantified by employing the well-known indophenol blue colorimetric approach. The electrolytic solution upon the reaction with the indophenol blue reagent changes its colour from yellow to dark green, suggesting the formation of higher concentration of NH<sub>3</sub> for the electrolytic solution of the NbO<sub>x</sub>-Gr electrode sample as depicted in ESI Fig. S9.<sup>†</sup> This indicates that ammonia is generated in high concentration when the potential is increased. The UV-vis spectra were recorded as shown in ESI Fig. S10a-c,<sup>†</sup> displaying an increase in peak intensity at 655 nm, which corresponds to ammonia detection.

The UV-vis spectra reveal a progressive increase in the ammonia peak as the potential is increased for the Gr, Nb<sub>2</sub>AlC-Gr, and NbO<sub>x</sub>-Gr electrodes. The NbO<sub>x</sub>-Gr electrode shows the most efficient results for NH<sub>3</sub> generation compared to Gr and Nb<sub>2</sub>AlC-Gr electrodes, corroborating with the results of LSV and electrochemical measurements. The faradaic efficiency (FE) and ammonia yield rate were calculated, utilizing the ammonia concentration acquired from the indophenol colorimetric approach utilizing eqn (1) and (2), illustrating a gradual enhancement when the potential is increased from -0.20 V to -1.1 V, as demonstrated in Fig. 5c and d. At -1.1 V *vs.* RHE, the FE and yield rates are ≈9.05% and ≈5.68 μg h<sup>-1</sup> cm<sup>-2</sup> for the

Gr electrode, ≈45.47% and ≈71.50 μg h<sup>-1</sup> cm<sup>-2</sup> for the Nb<sub>2</sub>AlC-Gr electrode, and ≈46.50% and ≈194.79 μg h<sup>-1</sup> cm<sup>-2</sup> for the NbO<sub>x</sub>-Gr electrode, respectively. The obtained yield rate is comparable with those of the previously reported MXene-based electrocatalysts for nitrate reduction to ammonia. The comparative table is provided in ESI Table S1.<sup>†</sup>

In addition to ammonia generation, nitrite ions are a primary by-product formed during the nitrate reduction reaction electrolysis process. Thus, to evaluate NO<sub>2</sub><sup>-</sup> ions in the electrolytic solution, UV spectra were recorded for Nb<sub>2</sub>AlC-Gr and NbO<sub>x</sub>-Gr electrodes, as shown in ESI Fig. S11a and b.<sup>†</sup> The observed peaks at 540 nm indicate the presence of NO<sub>2</sub><sup>-</sup> ions. Consequently, FE and yield rate were calculated utilizing the nitrite ion concentration, using eqn (1) and (2) as demonstrated in Fig. 5e and f. The FE and the yield rate of NO<sub>2</sub><sup>-</sup> ions are lower compared to those of NH<sub>3</sub>, which confirms that the electrocatalyst materials generate NO<sub>2</sub><sup>-</sup> ions as a by-product. Furthermore, a potential of -0.8 V is selected for the stability measurements of the NbO<sub>x</sub>-Gr electrode. The chronoamperometry measurement and UV spectra measurement are shown in ESI in Fig. S12 and 13,<sup>†</sup> confirms the formation of NH<sub>3</sub> at different times, as presented in Fig. 5g and h. Long-time electrolysis at a potential of -0.8 V was performed, which suggests that the NbO<sub>x</sub>-Gr electrode was able to generate ammonia for 24 hours as demonstrated in Fig. 5i. Furthermore, the UV spectra (Fig. S14<sup>†</sup>) confirm the presence of an ammonia peak at 655 nm, with a calculated ammonia yield rate of 194.04 μg h<sup>-1</sup> cm<sup>-2</sup>. Moreover, to validate the conversion of NO<sub>3</sub><sup>-</sup> ions into NH<sub>3</sub> through electrolysis, we acquired the <sup>1</sup>H NMR spectra of the electrolysis solution of the NbO<sub>x</sub>-Gr electrode in a<sup>15</sup>N-labeled NO<sub>3</sub> + 0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolyte and a blank electrolyte containing 0.5 M Na<sub>2</sub>SO<sub>4</sub>. The obtained spectra demonstrate that the blank solution has no signal (Fig. S15<sup>†</sup>), while in the <sup>15</sup>N-labeled NO<sub>3</sub> + 0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolytic solution we observed a 1 : 1 doublet and a 1 : 1 : 1 triplet peak, which could be related to NH<sub>4</sub><sup>+</sup> and its by-product.<sup>61</sup> Furthermore to confirm the presence of requisite elements on the surface and structural stability of NbO<sub>x</sub>-Gr electrodes, SEM-EDS mapping micrographs were acquired before and after electrochemical analysis, which confirm the presence of elements like C, O, Nb, and Al on the surface of electrodes after electrochemical analysis, suggesting that the electrodes are stable as illustrated in Fig. S16 in the ESI.<sup>†</sup>

## 2.4 Theoretical calculations

Density functional theory (DFT) calculations were employed to investigate the mechanism of electrocatalytic conversion of NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub> over NbO<sub>x</sub>-Gr. A model comprising a NbO<sub>x</sub> nanocluster supported on pristine graphene was used to examine the structural reorganization of NbO<sub>x</sub> upon adsorption on the graphene surface, construct the Gibbs free energy profile, and analyze charge density differences (CDD) and Bader charges.

Our calculations revealed a negative binding energy of -2.99 eV, indicating thermodynamically favorable adsorption of the NbO<sub>x</sub> nanocluster on graphene (see details in the ESI<sup>†</sup>). Additionally, a geometry analysis showed that the NbO<sub>x</sub> model underwent no substantial structural reorganization after adsorption on the graphene surface (Fig. S17<sup>†</sup>). The most



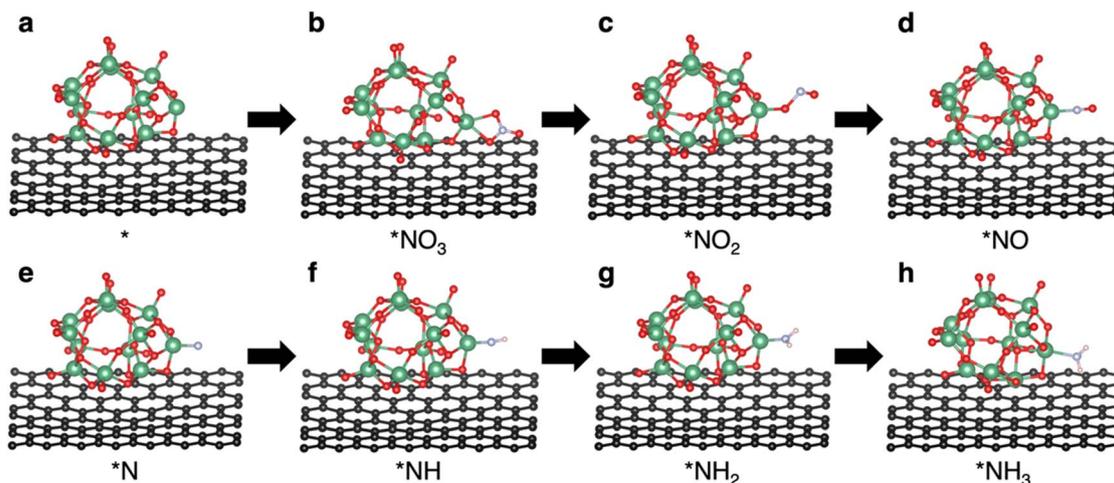


Fig. 6 (a–h) DFT optimized structures of the reaction intermediates for nitrate reduction over  $\text{NbO}_x\text{-Gr}$ .

pronounced deviation was observed for the O16 atom (Table S2<sup>†</sup>), attributed to the interaction of the Nb2 atom with the graphene sheet (see Fig. S17<sup>†</sup> for atom labelling). The observed changes correspond to those occurring upon non-covalent interaction between nanoclusters and graphene. Furthermore, the optimized structure of the  $\text{NbO}_x\text{-Gr}$  catalyst confirmed the absence of a covalent bond between the  $\text{NbO}_x$  nanocluster and the graphene support (Fig. 6a).

The Gibbs free energy profile displays the energy changes during nitrate reduction, which involves nine proton and eight electron transfers, following the sequence:<sup>62</sup>  $\text{NO}_3^- \rightarrow \text{*NO}_3 \rightarrow \text{*NO}_2 \rightarrow \text{*NO} \rightarrow \text{*N} \rightarrow \text{*NH} \rightarrow \text{*NH}_2 \rightarrow \text{*NH}_3 \rightarrow \text{NH}_3(\text{g})$  (Fig. 6).

Furthermore, DFT-optimized structures of the reaction intermediates identified the Nb atom on the  $\text{NbO}_x$  cluster surface as the active site. The reaction starts with the favourable

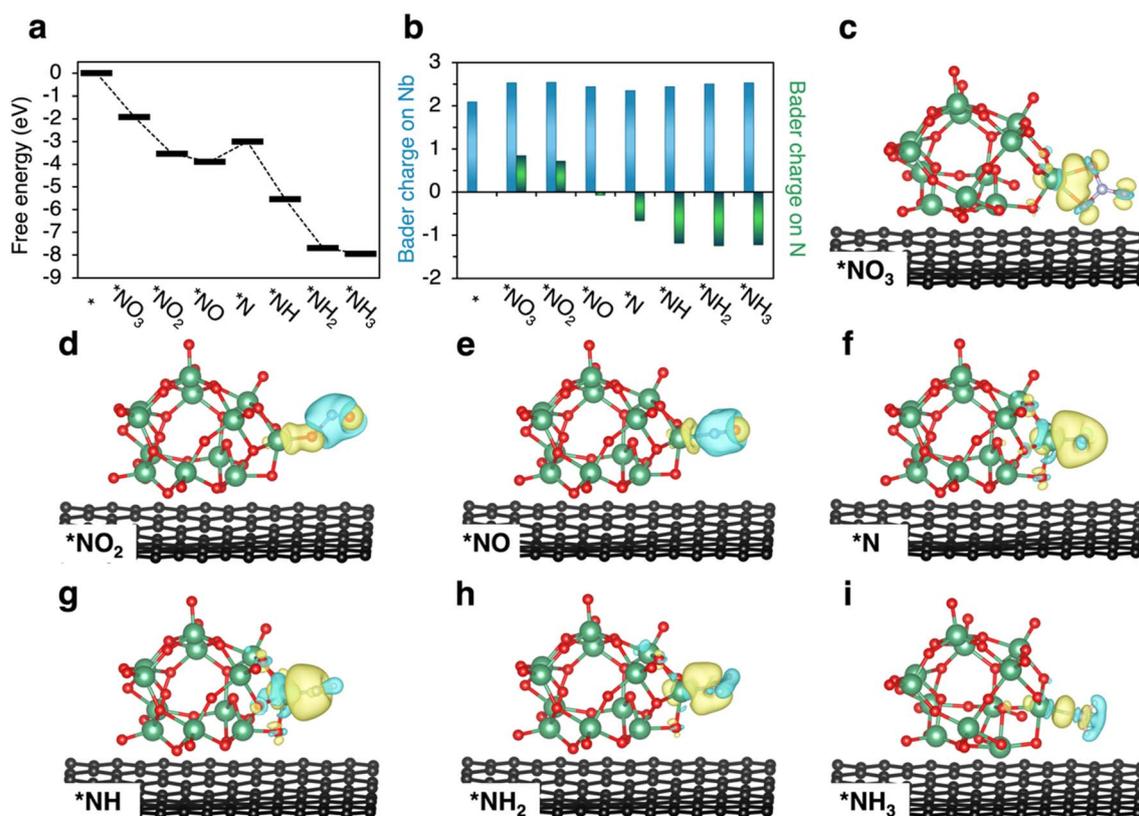


Fig. 7 (a) Gibbs free energy diagram of nitrate reduction ( $U = 0$  V) catalysed by the model of  $\text{NbO}_x\text{-Gr}$ . (b) Bader charge of Nb atom (blue), which is the active site of the nitrate reduction intermediates, and N atom (green). (c–i) DFT calculated charge density difference (CDD) of the intermediate structures of nitrate to ammonia reduction. Yellow and blue display charge accumulation and depletion, respectively.



adsorption of the  $\text{NO}_3^-$  anion, which is strongly bound, exhibiting a Gibbs free change ( $\Delta G$ ) of  $-1.91$  eV for this reaction step. Furthermore, Gibbs free energy changes were negative for all examined reaction steps along the reduction pathway, except for the  $^*\text{NO} \rightarrow ^*\text{N}$  step, which may serve as the potential-determining step (PDS). As depicted in Fig. 7a, the  $\Delta G$  for this step is  $0.88$  eV. The corresponding limiting potential ( $U_L$ ) of  $-0.44$  V for the overall energy profile suggests that  $\text{NbO}_x\text{-Gr}$  can act as an effective electrocatalyst for nitrate reduction.

The electronic structure of the intermediates was further probed, and the calculated CDDs revealed distinct charge accumulation patterns. For oxygen-containing intermediates ( $^*\text{NO}_3$ ,  $^*\text{NO}_2$ , and  $^*\text{NO}$ ), charge accumulation primarily occurs on bonds connecting the active site (Nb atom) and oxygen atoms (Fig. 7c–e). In contrast, a high accumulation of charge on the N atom was observed for the  $^*\text{N}$  intermediate (Fig. 7). This can explain the strongly negative  $\Delta G$  of  $-2.53$  eV associated with the  $^*\text{N} \rightarrow ^*\text{NH}$  reaction step. Similar charge accumulation on the nitrogen atoms was found for  $^*\text{NH}_2$  and  $^*\text{NH}_3$  intermediates (Fig. 7h–i). The facile hydrogenation steps in nitrate reduction on  $\text{NbO}_x\text{-Gr}$  can also be inferred from Bader charge analysis, which reveals an increasing negative charge on nitrogen atoms as the reaction progresses (Fig. 7b).

### 3 Conclusion

In summary, we reported a new kind of electrode material for nitrate reduction to ammonia, which was fabricated by employing a single-step lasing process followed by the electrochemical etching technique. The lasing process concurrently modified the chemical composition of the  $\text{Nb}_2\text{AlC}$  phase and converted the polyimide substrate into a graphene structure. Moreover, the *in situ* electrochemical etching technique etched the aluminium metal from the surface of the electrocatalyst electrode, enhancing its electrochemical activity. This fabricated heterostructure of  $\text{NbO}_x\text{-Gr}$  electrode delivered a faradaic efficiency and ammonia yield rate of  $\approx 46.50\%$  and  $\approx 194.79$   $\mu\text{g h}^{-1} \text{cm}^{-2}$ , respectively, at  $-1.1$  V vs. RHE. Additionally, theoretical calculations provided a deeper understanding of the reaction mechanism of the nitrate reduction to  $\text{NH}_3$ , confirming that the electrochemical active site is present on the Nb atom of the  $\text{NbO}_x\text{-Gr}$  electrode. In the future direction, the present work exhibits huge potential for the fabrication of cost-effective  $\text{Nb}_2\text{AlC}$  electrocatalyst materials for nitrate reduction to ammonia, offering an advanced material fabrication strategy to achieve high faradaic efficiency and yield rate for ammonia generation through the introduction of suitable MAX phases.

## 4 Materials and experimental methods

### 4.1 Materials

$\text{Nb}_2\text{AlC}$  powder was obtained from Laizhou Kai Ceramic Materials Co., Ltd, China. Polyimide sheets (PI,  $0.005''$ ) were used as received from Fiedler Scientific Instruments, Czech Republic. Hydrochloric acid (35%) was obtained from Penta Chemicals

Unlimited. Potassium nitrate was procured from Alfa Aesar. Sodium hypochlorite solution, phosphoric acid, salicylic acid, sodium hydroxide, citric acid, sodium nitroferrocyanide, *N*-(1-naphthyl) ethylenediamine dihydrochloride, sulfanilamide,  $\text{Na}^{15}\text{NO}_3$  and sodium sulfate were acquired from Merck. All the chemicals were used as procured and all the solutions were prepared using Millipore water with a resistivity of  $>18$   $\text{M}\Omega \text{cm}$ .

### 4.2 Laser treatment of $\text{Nb}_2\text{AlC-Gr}$ electrodes

The Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  electrodes were fabricated using a Laser dicer Oxford Lasers A-Series equipped with a diode-pumped solid-state Nd:YAG laser operating at  $532$  nm wavelength. The defocused laser writing technique was directly applied on polyimide sheets to fabricate the Gr electrode. In contrast, for the  $\text{Nb}_2\text{AlC-Gr}$  electrode, firstly,  $\text{Nb}_2\text{AlC}$  dispersed in ethanol was drop-cast onto the polyimide sheets before defocused laser writing. The laser parameters used in this study were as follows: a pulse frequency of  $7$  kHz, a scanning speed of  $50$   $\text{mm s}^{-1}$ , and a laser power of  $3$  W.

### 4.3 *In situ* electrochemical etching

A three-electrode set-up, where Ag/AgCl acts as the reference electrode, Platinum (Pt) acts as the counter electrode, and  $\text{Nb}_2\text{AlC-Gr}$  acts as the working electrode, was employed for the electrochemical etching process. A potential of  $2$  V vs. Ag/AgCl was applied for the chronoamperometry measurement in  $3$  M HCl as the electrolyte. The etching process was performed for different time durations like  $6$  h,  $12$  h,  $18$  h, and  $24$  h under room temperature conditions. After the etching the electrodes were rinsed with  $\text{H}_2\text{O}$ , to remove any residual impurity and  $\text{AlCl}_3$  on the surface of the electrodes.

### 4.4 Electrochemical measurement

All the electrochemical experiments were carried out employing a three-electrode setup. The linear sweep voltammetry profile was obtained in  $0.5$  M  $\text{Na}_2\text{SO}_4$  and  $0.5$  M  $\text{Na}_2\text{SO}_4 + 0.1$  M  $\text{KNO}_3$  (nitrate source) electrolyte with the scan rate of  $5$   $\text{mV}^{-1}$  using a potentiostat instrument (PGSTAT 204 from Metrohm Autolab, Netherlands) that was operated through NOVA software version 2.1, connected with a computer. The chronoamperometry measurements were carried out using  $0.5$  M  $\text{Na}_2\text{SO}_4 + 0.1$  M  $\text{KNO}_3$  (nitrate source) as the electrolyte, a Ag/AgCl electrode filled with the KCl gel electrolyte as the reference electrode, Platinum (Pt) as the counter electrode, and Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  as the working electrode in a similar setup.

To investigate the nitrate reduction reaction activity. The electrolysis process to generate ammonia was conducted in an H-cell separated *via* a frit. To ensure a balanced distribution of electrolytes,  $20$  mL of electrolyte was added to both the anodic and cathodic compartments. The electrolysis process was carried out for one hour for each electrode like Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  with continuous stirring to investigate the faradaic efficiency (FE%) and the ammonia yield rate. During the electrolysis process, different potentials were applied in the range of  $-0.20$  to  $-1.10$  V vs. RHE. The potential was converted



into a reversible hydrogen electrode (RHE) scale using the following equation:  $E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.0591 \text{ pH} + 0.199$ .<sup>63</sup>

#### 4.5 Colorimetric procedure for the quantification of $\text{NH}_3$ and $\text{NO}_2^-$ concentrations

A well-established colorimetric analysis procedure was employed to evaluate the  $\text{NH}_3$  and  $\text{NO}_2^-$  ion concentration after the electrolytic measurements. A UV-vis spectrophotometer was employed to identify the concentration of  $\text{NH}_3$  and  $\text{NO}_2^-$  ions. The detailed procedure is described in subsequent sections.

**4.5.1 Quantification of ammonia ( $\text{NH}_3$ ).** The quantification of ammonia is carried out using the electrolytic solution obtained after the chronoamperometry analysis employing a UV-visible spectrophotometer (JASCO V-750). To quantify the presence of the generated ammonia in the electrolytic solution, a certain volume of the solution was taken out from the H-cell and diluted up to 600  $\mu\text{L}$  to reach the detection limit, followed by the addition of 600  $\mu\text{L}$  of a solution comprising 3 M NaOH, 10 wt% salicylic acids, and 10 wt% citric acid, 300  $\mu\text{L}$  of a solution consisting of 0.2 M NaClO, and 60  $\mu\text{L}$  of a solution containing 2.0 wt% sodium nitroferrocyanide. This mixture was kept for two hours. The UV-vis absorbance spectrum was acquired. The ammonia concentration was estimated on the formation of the indophenol blue product in the above mixture and the absorbance spectrum was recorded at 655 nm wavelength. Additionally, the ammonia concentration was calculated using the equation  $y = 0.0079 \times -0.0071$ ,  $R^2 = 0.999$ , utilizing a calibration curve derived from a series of standard ammonium chloride solutions in the 0.5 M  $\text{Na}_2\text{SO}_4$  electrolyte.<sup>63</sup>

**4.5.2 Quantification of nitrite ( $\text{NO}_2^-$ ).** The nitrite concentration in the electrolytic solution was determined following a reported protocol, where a colouring reagent was formulated by adding *N*-(1-naphthyl) ethylenediamine dihydrochloride (0.02 g) and *p*-amino benzenesulfonamide (0.4 g) in water (5 mL) along with phosphoric acid (1 mL,  $\rho = 1.70 \text{ g mL}^{-1}$ ). Later, a specified amount of the electrolytic solution was taken out and diluted to 1.5 mL to meet the detection range. Subsequently, 50  $\mu\text{L}$  of colour reagent was mixed in the above diluted electrolytic solution. The mixture of the solution was kept for 20 minutes. Then, the UV-visible absorption spectra were acquired. The nitrite concentration was investigated by recording the peak intensity at 540 nm wavelength and the concentration is calculated using the calibration curve.<sup>63</sup>

#### 4.6 Calculation to determine the performance of the working electrodes (electrocatalysts)

The faradaic efficiency (FE) and yield rate (YR) were obtained by the following equations:<sup>63</sup>

$$\text{FE (\%)} = (n \times F \times c_{\text{NH}_3/\text{NO}_2^-} \times V)/Q \quad (1)$$

$$\text{YR} = (c_{\text{NH}_3/\text{NO}_2^-} \times V \times M)/(t \times A) \quad (2)$$

where  $n$  is the number of electrons (8 for  $\text{NH}_3$  and 2 for  $\text{NO}_2^-$ ),  $F$  represents the faradaic constant ( $96485 \text{ C mol}^{-1}$ ),  $c_{\text{NH}_3/\text{NO}_2^-}$  is the concentration of  $\text{NH}_3$  or  $\text{NO}_2^-$ ,  $V$  is the electrolytic solution

volume (20 mL) at the cathodic compartment,  $Q$  is the total charge observed during the process of electrolysis,  $M$  is 17.03 for  $\text{NH}_3$  or 46.005 for  $\text{NO}_2^-$ ,  $t$  is the electrolysis time, and  $A$  is the surface area of the working electrode.

#### 4.7 Evaluation of ammonia by the $^1\text{H}$ NMR quantitative technique and isotopic labelling measurement

For the isotopic labelling analysis, the electrolysis was recorded in the 0.5 M  $\text{Na}_2\text{SO}_4$  + 0.1 M  $\text{Na}^{15}\text{NO}_3$  electrolyte solution. Following electrolysis, an aliquot of 5 mL catholyte was collected from the H-cell and 250  $\mu\text{L}$  of concentrated  $\text{H}_2\text{SO}_4$  was added to create an acidic environment, which is the standard for the quantification of  $\text{NH}_4^+$  ions. After this, 0.002 g of maleic acid was added as an internal standard to the above solution. 500  $\mu\text{L}$  of this solution was taken in the NMR tube and 50  $\mu\text{L}$  deuterium oxide ( $\text{D}_2\text{O}$ ) was added for the NMR detection.<sup>63</sup>

#### 4.8 Material characterization

SEM (FEI VERIOS 460 L) is used for the surface morphology investigation of the Gr,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  electrodes. An Olympus Lext-OLS4100 confocal laser scanning microscope is utilized to obtain the optical images of the  $\text{Nb}_2\text{AlC-Gr}$  and  $\text{NbO}_x\text{-Gr}$  electrodes. Physical characterization of  $\text{Nb}_2\text{AlC-Gr}$  and  $\text{NbO}_x\text{-Gr}$  electrodes was performed using a Rigaku SmartLab 3 kW X-ray diffractometer for the X-ray diffraction (XRD) investigation. This XRD device was operated with a current of 30 mA and a voltage of 40 kV. The XRD investigation was carried out following the Bragg Brentano geometry with Cu  $K\alpha$  radiation ( $\lambda = 0.15418 \text{ nm}$ ). The chemical composition investigation was carried out using an X-ray photoelectron spectroscopy device (XPS, Kratos AXIS Supra). The XPS wide survey scan and core level spectra of the elements like Nb, C, O, and Al present in Gr, commercial  $\text{Nb}_2\text{AlC}$ ,  $\text{Nb}_2\text{AlC-Gr}$ , and  $\text{NbO}_x\text{-Gr}$  are acquired. The software Casa XPS is employed for the fitting of XPS spectra curves, and the calibration of the obtained spectra is done against the carbon C 1s peak *i.e.*, 284.8 eV. A Witec Alpha 300R instrument is utilized to obtain the Raman spectra curve. The UV-visible absorption spectra studies are performed with a UV-Vis-spectrophotometer JASCO V-750.

#### 4.9 Theoretical calculations

Spin-polarized DFT calculations were carried out using the Vienna *Ab initio* Simulation Package (VASP), introducing the projector augmented wave (PAW) potentials with a plane-wave cutoff energy of 520 eV.<sup>64–67</sup> The Perdew–Burke–Ernzerhof (PBE) parametrization of the generalized gradient approximation (GGA) was used to describe the electronic exchange–correlation energies, and the DFT-D3 method of Grimme with zero-damping was also introduced to describe the van der Waals interactions.<sup>68,69</sup> All structures were fully optimized until forces acting on all atoms were reduced to  $0.03 \text{ eV \AA}^{-1}$ , and electronic degrees of freedom were relaxed until the change in total electronic energy between successive iteration steps was smaller than  $10^{-5} \text{ eV}$ . For structural optimization, the Brillouin zone was sampled using a  $1 \times 1 \times 1$   $k$ -point grid based on the Monkhorst–Pack scheme, centred at Gamma. Since the nitrate



reduction proceeds in an aqueous environment and involves  $H^+$  transfer, the solvation effects of water were considered by VASPsol.<sup>70</sup> To eliminate the effects between two adjacent layers, a vacuum region of 15 Å was added in the  $z$ -direction. For electronic structure calculations, the Brillouin zone integrations were performed with a gamma-centred  $3 \times 3 \times 1$  Monkhorst-Pack  $k$ -point mesh grid.<sup>71</sup> The computational hydrogen electrode (CHE) model was used to calculate the Gibbs free energy of reactions involving electron-proton transfer. The vibrational modes were calculated at 298.15 K to obtain the zero-point energy, entropy, and temperature corrections to enthalpy, and VASPKIT was used for the post-processing.<sup>72,73</sup> To avoid calculating the charged molecule  $NO_3^-$ , the Gibbs free energy of aqueous  $NO_3^-$  was derived from those of gaseous  $HNO_3$  and  $H_2$ . The Gibbs free energy for nitrate  $NO_3^-$  to adsorb on the  $NbO_x$ -Gr model in aqueous solution forming  $*NO_3$  was calculated as follows:<sup>74,75</sup>

$$\Delta G_{*NO_3} = G_{*NO_3} - G^* - G_{*HNO_3(g)} + \frac{1}{2}G_{H_2(g)} + 0.392,$$

where  $G_{*NO_3}$ ,  $G^*$ ,  $G_{*HNO_3(g)}$ , and  $G_{H_2(g)}$  are the Gibbs free energies of  $NO_3^-$  adsorbed on the  $NbO_x$ -Gr model, the  $NbO_x$ -Gr model itself,  $HNO_3$  and  $H_2$  molecules in the gas phase, respectively. The value of 0.392 is the correction of adsorption energy.<sup>76</sup> Limiting potential  $U_L$  ( $U_L = -\Delta G_{max}/e$ ) was employed to describe the lowest bias requirement for the nitrate reduction.<sup>77</sup>

## Data availability

Data for this article are available at ZENODO at <https://zenodo.org>.

## Author contributions

S. N., S. D., and M. P. conceived the idea. S. N. carried out laser treatment, *in situ* etching of the  $Nb_2AlC$  electrodes and their characterizations (such as SEM, CLSM, XPS, XRD, Raman, electrochemical characterization, and ammonia production), data acquisition, investigation and preparation of the first draft of the manuscript. S. D. carried out laser treatment, managed the project, and revised the manuscript. M. L. performed theoretical calculations and wrote the theoretical section. M. O. participated in the validation of the theoretical calculations, writing of the manuscript and funding acquisition. M. P. supervised the research, acquired funding, and revised the manuscript. All the data included in the manuscript were discussed and approved by all the authors.

## Conflicts of interest

The authors affirm no conflict of financial interest.

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