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Redox-active oxide-molten salt composites as a new family of high-capacity thermal energy storage materials†

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This study introduces a new family of redox-active oxide-molten salt (ROMS) composites for high-capacity thermal energy storage. Porous perovskite oxides serve as active support materials, facilitating thermochemical energy storage through redox reactions, while latent heat from the phase change of the salt mixture enables high energy density within a narrow temperature swing. We demonstrated the compatibility between perovskites and salt mixtures, with 12 out of 25 tested combinations proving successful. The diverse properties of perovskites and salt mixtures resulted in ROMS compositions with different functionality and performance, three of which are highlighted in this work. $\text{La}_{0.8}\text{Sr}_{0.2}\text{FeO}_{3-\delta}:\text{NaF}-\text{CaF}_2-\text{LiF}$ exhibited excellent latent heat-based energy storage as well as long-term stability with a total capacity of $\sim 530 \text{ kJ kg}^{-1}$ (510–660 °C). $\text{Sr}_{0.125}\text{Ca}_{0.875}\text{Fe}_{0.25}\text{Mn}_{0.75}\text{O}_{3-\delta}:\text{NaF}-\text{CaF}_2$ achieved the overall energy density of $\sim 523 \text{ kJ kg}^{-1}$ (670–820 °C) through both phase-transition and redox-based mechanisms, though gradual deactivation was observed over long-term operation. Lastly, $\text{La}_{0.8}\text{Sr}_{0.2}\text{FeO}_{3-\delta}:\text{Li}_2\text{MoO}_4$, a highly redox-active ROMS composition, delivered up to 875 kJ kg^{-1} when applied for waste heat recovery from fuel-containing exhaust gas streams.

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1. Introduction

The combustion of fossil fuels, which accounts for approximately 80% of the world's energy utilization, stands as the predominant contributor to greenhouse gas emissions.^{1–3} Meanwhile, only less than half of the energy derived from fossil fuels is converted into useful forms such as electric power, with the rest being discharged as waste heat.⁴ Other energy-intensive industries such as iron and steelmaking also produce vast amounts of high-grade heat ($>500 \text{ °C}$), with processes like electric arc furnaces or coke ovens generating exhaust gas at high temperatures.^{5,6} As such, capturing the excess heat for industrial applications or power generation would significantly improve the energy efficiency of the processes and substantially reduce the carbon emissions.^{4,5,7} However, the recovery of waste heat faces challenges due to the mismatch between the operational requirements of energy supply and demand.⁴ Also, the intermittency or fluctuations of many heat sources restrict the continuous operation of the waste heat recovery system.^{8,9}

Thermal energy storage (TES) can overcome these challenges by adapting to the properties of high-temperature heat sources.^{10–12} A cost-effective thermal energy storage system can capture the energy from the heat source, and store and release it on demand for industrial processes or power generation.^{12,13}

TES can find applications in the forms of sensible, latent, and thermochemical heat. Among these, sensible heat storage materials have been most widely investigated and commercially mature owing to their simplicity.^{13,14} Molten nitrate salts are the most commonly used sensible heat storage materials for medium (200–400 °C) to high ($>400 \text{ °C}$) temperature TES, often employed as heat transfer fluids due to their favorable characteristics such as high heat capacity and low melting point.^{15,16} For example, $\text{LiNO}_3-\text{NaNO}_3-\text{KNO}_3-\text{Ca}(\text{NO}_3)_2$, extensively studied for sensible heat storage application, has been utilized as heat transfer fluid in solar parabolic systems.^{11,17,18} Nitrate salts can provide energy storage densities ranging from 100 to 500 kJ kg^{-1} but they require large temperature swings of $\sim 300 \text{ °C}$ to achieve the high values.^{13,19,20} In addition, the relatively low decomposition temperatures of molten nitrate salts limit their applicability for temperatures exceeding 560 °C .¹³

Compared to sensible heat storage materials, latent heat storage systems that rely on phase change materials (PCM) exhibit notable advantages, primarily due to their superior energy storage density, which requires low volume and operates within a narrow temperature range.^{11,12} For medium- and high-temperature (200–1400 °C) applications, fluoride, and carbonate-type molten salts are particularly attractive phase-

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change materials (PCM) for latent heat storage with their considerably large heat of fusion.²¹ They are suitable for use at operating temperatures above 500 °C due to their high melting points. However, the application of molten salts is restricted by thermal instabilities above the melting point. Besides, the melting and solidification of PCMs cause handling difficulties in fluidized beds or single-tank systems. The corrosive nature of molten salts imposes additional limitations on their applications in heat storage.^{13,22}

To address the above-mentioned challenges, there has been growing interest in form-stable composite materials consisting of PCMs and supporting materials in recent years.^{10,11,23–27} Form-stable composite materials enclose the PCMs within a skeleton material and reduce the leakage of PCMs.²⁴ Various supporting materials, such as diatomite,^{25,28,29} vermiculite,²⁶ magnesium oxide,²³ and expanded graphite,³⁰ have been used to fabricate the composite materials. Among them, diatomite has attracted more interest owing to its high porosity, corrosion resistance, and low cost.^{10,25} For example, Jiang *et al.* used a porous modified diatomite-based skeleton material to improve the thermo-physical properties of NaNO₃.²⁵ They obtained a total energy storage density of 382.92 kJ kg^{−1} in the operating temperature range of 130–330 °C with 58.67 wt% salt loading and improved the micro-flow of molten salt within the large pores of the modified diatomite. Li *et al.* studied sodium nitrate-expanded vermiculite (EV) composite materials, achieving a latent heat of 157.2 kJ kg^{−1}, and a high salt : EV ratio of 734.6 wt% (defined as adsorptive capacity) using the direct impregnation method.²⁶ Jiang *et al.* developed a form-stable composite material using LiNO₃–NaNO₃–KNO₃–Ca(NO₃)₂ and calcium silicate with a melting point of 103.5 °C and latent heat of 73.59 kJ kg^{−1}.¹¹ The high porosity of calcium silicate played a vital role in preventing salt leakage by absorbing large amounts of nitrate salt, thus ensuring the long-term stability of over 1000 thermal cycles. While these studies have mainly focused on low (<200 °C) and medium temperatures (200–400 °C) applications due to the low melting point of nitrate salts, efforts have been made to extend the operating temperature range to high temperatures (>400 °C). Qian *et al.*, for instance, introduced a group of composite materials consisting of polyethylene glycol, LiNO₃, and Na₂SO₄ which were aimed to be used in low, middle, and high-temperature energy storage, respectively.²⁴ Furthermore, Ge *et al.* also proposed a composite material for the medium and high temperature ranges, by using LiCO₃–NaCO₃ as the PCM, MgO as the ceramic support material, and additionally carbon nanotubes as the thermal conductivity enhancer.²³ Their studies emphasized the significance of good wettability of the salt with ceramic material to ensure the formation of a robust composite material. Although the proposed composite materials offer promising properties and prevent salt leakage, inert support materials limit the energy efficiency of such composites, necessitating a large temperature swing for effective heat storage.

Alternatively, thermochemical energy storage (TCES) has recently gained significant attention owing to its potential for achieving high energy density in wide operating temperature ranges and extended durations.^{19,31} Particularly, TCES systems,

which utilize the chemical energy of reversible redox reactions of metal oxides, have been widely studied in recent years.^{32,33} Within the realm of redox-active metal oxide materials, perovskite oxides with the general formula of ABO₃ (where A is typically an alkali, alkaline earth, or a lanthanide metal cation and B is a transition metal cation) have shown considerable advantages over conventional redox materials.^{34,35} They have the ability to continuously exchange their lattice oxygen over a wide range of temperatures and partial oxygen pressures, facilitating thermochemical energy storage under flexible operating conditions.^{36,37} Conversely, the redox reactions of monometallic oxides are discrete and restricted to specific high temperatures.³² Furthermore, the flexible structures of perovskite oxides enable tailorable thermochemical properties, allowing them to be utilized in various energy storage applications.³⁸ The excellent kinetics of perovskites, attributed to their high lattice oxygen diffusion rate, further enhances their utility.^{33,39} To date, perovskite oxides have demonstrated TCES densities ranging from 34 to 571 kJ kg^{−1}–ABO₃ with an operating temperature window extending up to 1250 °C.^{34–47} However, they require large temperature and oxygen partial pressure swings to achieve such densities, thereby limiting the energetic efficiency of the processes.

To address the limitations of existing TES materials, this study reports a new class of materials, *i.e.* redox-active oxide-molten salt (ROMS) composites, which combine molten salts and perovskite oxides in a dual-phase composite structure.⁴⁸ In these composites, the latent heat storage from the phase change of molten salts serves as the primary energy storage mechanism, while redox-active oxide materials act as supporting structures to prevent salt leakage and contribute additional thermochemical energy density through redox reactions. ROMS composites offer several potential advantages: (1) the oxide exoskeleton stabilizes the molten salt *via* favorable surface tensions, similar to non-redox-active composites;²⁷ (2) the latent heat storage of molten salts narrows the temperature swing required for redox-based energy storage; (3) both perovskite oxides and molten salts are highly tunable, enabling compatibility with a range of operating conditions; and (4) the high redox activity facilitates efficient recovery of waste heat from fuel-containing exhaust streams. This study demonstrates the compatibility of perovskite oxides and salt mixtures as energy storage media, highlighting three compositions with varying features that cater to different application scenarios ranging from thermal energy only to high-temperature fuel containing flue gas.

2. Experimental methods

2.1 Material preparation

The abbreviations and synthesis methods of metal oxides that were used are listed in Table 1. LSF1 and LSCo were commercial La_{0.8}Sr_{0.2}Fe_{0.97}O_{3–δ} and La_{0.8}Sr_{0.2}Co_{0.8}Fe_{0.2}O_{3–δ}, respectively obtained from Praxair Surface Technologies while the rest was synthesized either by solid-state or sol-gel method. Detailed descriptions regarding the solid-state method can be found in our previous study.⁴⁹ The procedure for the sol-gel



Table 1 The abbreviation of metal oxides that were used in composite materials

| Sample name | Abbreviation | Synthesis method |
|---|--------------|------------------|
| $\text{Ca}_2\text{AlMnO}_{5+\delta}$ | CAM | Sol-gel |
| $\text{SrFeO}_{3-\delta}$ | SF | Ball mill |
| $\text{Sr}_{0.75}\text{Ba}_{0.25}\text{FeO}_{3-\delta}$ | SBF | Ball mill |
| $\text{Sr}_{0.25}\text{Ca}_{0.75}\text{Fe}_{0.25}\text{Mn}_{0.75}\text{O}_{3-\delta}$ | SCFM1 | Sol-gel |
| $\text{Sr}_{0.125}\text{Ca}_{0.875}\text{Fe}_{0.25}\text{Mn}_{0.75}\text{O}_{3-\delta}$ | SCFM2 | Sol-gel |
| $\text{Sr}_{0.05}\text{Ca}_{0.95}\text{Mn}_{0.95}\text{Co}_{0.05}\text{O}_{3-\delta}$ | SCMCo1 | Ball mill |
| $\text{Sr}_{0.05}\text{Ca}_{0.95}\text{Mn}_{0.9}\text{Co}_{0.1}\text{O}_{3-\delta}$ | SCMCo2 | Ball mill |
| $\text{La}_{0.8}\text{Sr}_{0.2}\text{FeO}_{3-\delta}$ | LSF1 | Commercial |
| $\text{La}_{0.6}\text{Sr}_{0.4}\text{FeO}_{3-\delta}$ | LSF2 | Ball mill |
| $\text{La}_{0.7}\text{Sr}_{0.3}\text{FeO}_{3-\delta}$ | LSF3 | Ball mill |
| $\text{La}_{0.3}\text{Sr}_{0.7}\text{Co}_{0.9}\text{Mn}_{0.1}\text{O}_{3-\delta}$ | LSCoM1 | Ball mill |
| $\text{La}_{0.7}\text{Sr}_{0.3}\text{Co}_{0.9}\text{Mn}_{0.1}\text{O}_{3-\delta}$ | LSCoM2 | Ball mill |
| $\text{La}_{0.8}\text{Sr}_{0.2}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_{3-\delta}$ | LSFCo | Commercial |

method is provided in the ESI.† Eutectic and ternary salt mixtures were prepared by mixing the salts in a mortar with the specific ratios provided in Table 2. The salts used in this study were LiF (97%), NaF (99%), CaF_2 (99%), MgF_2 (99%), and KF (99%), from Thermo Fisher Scientific and Li_2CO_3 ($\geq 99\%$), Na_2CO_3 ($\geq 99.5\%$), NaCl ($\geq 99.5\%$), and Li_2MoO_4 (99.9%) from Sigma Aldrich. The composite materials were prepared by using facile mixing and sintering, as illustrated in Fig. 1b. Fig. 1b is adopted to prepare the composites using either as received oxides or the porous oxides prepared *via* Fig. 1a. Detailed descriptions regarding material preparation for XRD, TGA-DSC tests as well as preparation of pellets for thermal conductivity measurements can be found in the ESI.†

For the long-term tests, we applied the salt-grinding method to the perovskite oxides to obtain a porous structure before preparing the composite material. Schematic representation of this method is provided in Fig. 1a. The perovskite oxides were mixed with NaCl and 3 mm ZrO_2 beads in a stainless-steel sample jar with a specific mass ratio. The jar was ball milled at 1200 rpm for 24 h using a high-energy ball mill. The resulting mixtures were rinsed with distilled water to remove NaCl using the centrifuge tube for 8 min at 6000 rpm. This rinsing step was repeated 3 times. Afterward, the remaining wet particles were

dried in a vacuum oven at 80 °C for 30 min and then at 130 °C overnight. BET surface area, pore width, and volume of LSF1 were determined using a Micromeritics ASAP 2020 instrument. First, the samples were degassed at 200 °C for 10 hours to get rid of the adsorbed species on the surface. After that, nitrogen adsorption isotherms were obtained in the relative pressure range (P/P^0) of 0.01–1 at 77 K.

2.2 Characterization

We characterized the crystal structures of the composite materials using an Empyrean PANalytical XRD with $\text{Cu-K}\alpha$ radiation ($\lambda = 1.5406 \text{ \AA}$) at an operating voltage of 45 kV and a current of 40 mA. XRD patterns were collected over a 2θ range of 15° to 80°, with a step size of 0.0262° holding for 0.4 s for each step. Additionally, LSF1:LiF–NaF– CaF_2 (post-100 cycles) was scanned using a high-temperature stage XRK900 since the spent sample was more prone to absorb moisture. The sample was ramped up to 200 °C in an N_2 atmosphere to remove hydrates. Phase analysis was performed using *HighScore* software. We examined the surface morphologies of LSF1 and LSF1:LiF–NaF– CaF_2 using a Hitachi SU8700 field-emission scanning electron microscope (FESEM) coupled with energy-dispersive X-ray spectroscopy (EDS).

2.3 TGA-DSC and thermal conductivity measurements

We determined melting/crystallization enthalpy and temperature by means of a differential scanning calorimeter (DSC with $\pm 2\%$ accuracy) coupled with a thermogravimetric analyzer (TGA, TA-Instrument, SDT Q650). The heat flow was calibrated using a sapphire reference with a known heat capacity. Prior to each experiment, cell constant calibration was verified using aluminum wire to obtain a calibration constant, which was then used to correct the measured heat of fusion. In each experiment, we placed 10–13 mg of YSZ (yttria-stabilized zirconia) as inert material and then 10–15 mg of the sample into a 110 μm platinum (Pt) pan. Inert material was necessary to prevent the salt from sticking to the Pt pan upon melting.⁵² For the composite materials containing NaF– CaF_2 , an additional $\sim 30 \text{ mg}$ of YSZ was placed on top to diminish the thermal losses. To minimize potential inaccuracies caused by the

Table 2 The ratios and phase change properties of eutectic salts reported in the literature

| Salt mixture | Weight ratio | Heat of fusion ($\text{kJ kg}_{\text{salt}}^{-1}$) | Melting point (°C) |
|---|----------------|--|--------------------|
| Li_2CO_3 – Na_2CO_3 ⁵⁰ | 0.44–0.56 | 370 | 496 |
| LiF–NaF– CaF_2 ⁵¹ | 0.35–0.38–0.26 | 640 | 615 |
| NaF– CaF_2 ^{52,53} | 0.53–0.47 | 520–600 | 810 |
| MgF_2 –NaF– CaF_2 ^{52,53} | 0.14–0.52–0.34 | 510–540 | 745–754 |
| NaF–NaCl ⁵⁴ | 0.26–0.73 | 572 | 674 |
| NaF–KF ⁵³ | 0.33–0.67 | 550–560 | 721 |
| LiF– CaF_2 ⁵³ | 0.54–0.46 | 750–760 | 766 |
| LiF–NaF ^{51,55} | 0.49–0.51 | 816 ^a | 649 |
| Li_2MoO_4 ⁵⁶ | — | 280 | 705 |

^a The eutectic point for LiF–NaF was provided with a mole ratio of 0.61–0.39 in the FactSage database, heat of fusion was reported for a ratio of 0.6–0.4 in Phillips *et al.*'s study.⁵¹



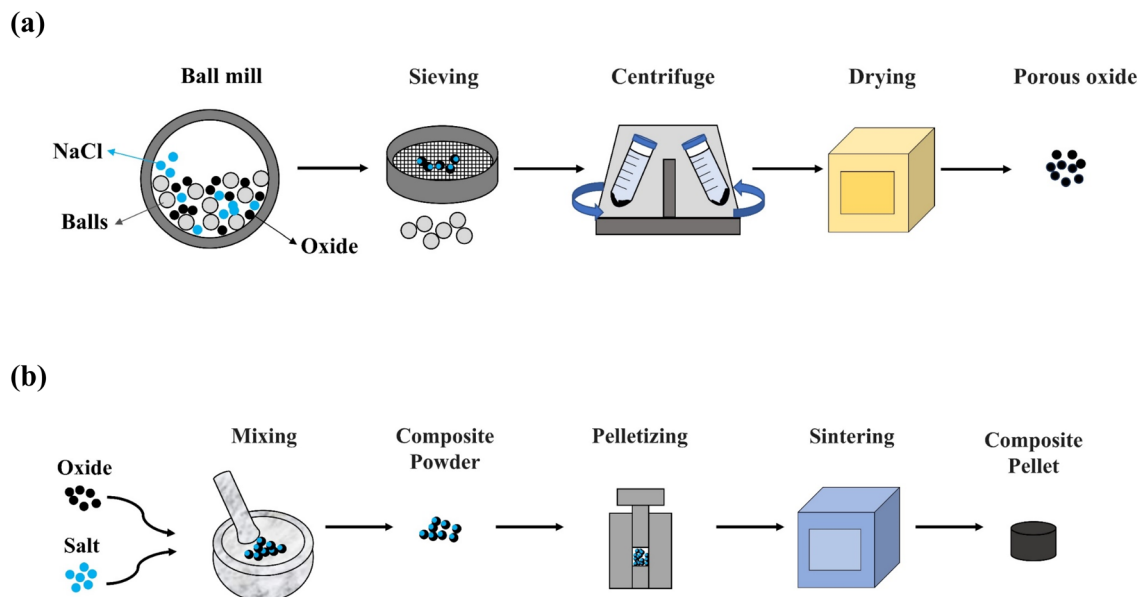


Fig. 1 Schematic representation of material preparation (a) salt-grinding method for the formation of porous oxide (b) composite material preparation *small portion of the composite particles were used for TGA-DSC tests, while the rest was prepared for the XRD analysis.*

deflection of heat from shiny Pt pans, we used an alumina lid on top, resulting in more consistent measurements. The experiments were conducted over a temperature range of 150 °C, determined based on the melting/solidification point of the salt used in the ROMS (*e.g.*, 670–820 °C for SCFM2:NaF–CaF₂). First, the samples were heated up to 180 °C to remove the absorbed moisture, and the weight at the end of this step was used as the initial weight. The samples were then cycled between the lower and upper temperature limits at a ramping rate of 10 °C min^{−1}, with 15 min isothermal steps. Typically, the first two cycles were carried out in an Ar atmosphere at a total gas flow rate of 200 ml min^{−1}, followed by alternating between 20% O₂/80% Ar at the upper temperature and Ar at the lower temperature. For the experiments under reducing conditions, samples were first ramped up to 730 °C under Ar and then exposed to 20% H₂/80% Ar until equilibrium was reached. After that, the samples were ramped down to 580 °C under Ar, followed by exposure to 20% O₂/80% Ar. Details regarding TGA-DSC analysis and calculation of overall energy density are described in the ESI.†

We measured the thermal conductivities of LSF1, LiF–NaF–CaF₂, and the composite material LSF1:LiF–NaF–CaF₂ *via* the transient plane source technique using the Hot Disc sensor, which is a widely accepted approach for determining thermal properties of materials.^{57–59} Details regarding this method can be found in the ESI.†

3. Results and discussion

3.1 Compatibility between perovskite oxides and eutectic salt mixtures

The compatibility between various metal oxides and eutectic salt mixtures was first evaluated using XRD. The formation of new phases other than the target oxide and salt phases would

indicate a reaction between the oxides and the salts. This is undesirable as it degrades the energy capacity of the sample, as demonstrated by the measured melting enthalpies of SF:LiF–NaF and SBF:LiF–NaF, detailed in Table S2† (exact compositions of metal oxides can be found in Table 1). Overall, 12 out of 25 samples screened were compatible. The XRD patterns of the compatible samples were presented in Fig. 2 and 3 and the identified crystal phases for all the samples were summarized in Table 3. In general, the Ca- and Ba-based oxides were less likely to react with NaF, CaF₂, and NaCl. However, when LiF or MgF₂ were introduced in the salt mixtures, the B-site cation(s) of the perovskite oxides tended to form new oxide phases with the cations of fluoride salts. Additionally, cations of SBF and SF led to the formation of new fluorides by breaking the eutectic phase of the salt mixture. Some of the resulting fluoride phases, such as SrF₂ or KCaF₃, can be associated with their relatively higher stability compared to initial fluoride phases, as shown in Table S1† based on data from the Materials Project database.⁶⁰ Although the relative stability of fluorides based on the Materials Project database offers a useful guide, it cannot explain all the formed phases, since it does not consider the potential favorability of competing mixed oxide phases; the benefits and limitations of this approach are further discussed in ESI.†

On the other hand, La-based oxides were revealed to be more stable as they showed less tendency to react with salt mixtures in general. Our results suggested that increasing Sr in the A-site reduced the stability of the oxide structure. The higher stability of perovskite oxides with rare earth metals compared to alkaline earth metals was also supported by Jacobs *et al.*'s study through convex hull analysis.⁶¹ Thus, lower Sr in the A-site ensured a compatible composite structure with LiF–NaF–CaF₂ and MgF₂–NaF–CaF₂. This phenomenon was observed for LSCM2 and LSCM1; the former formed a compatible composite



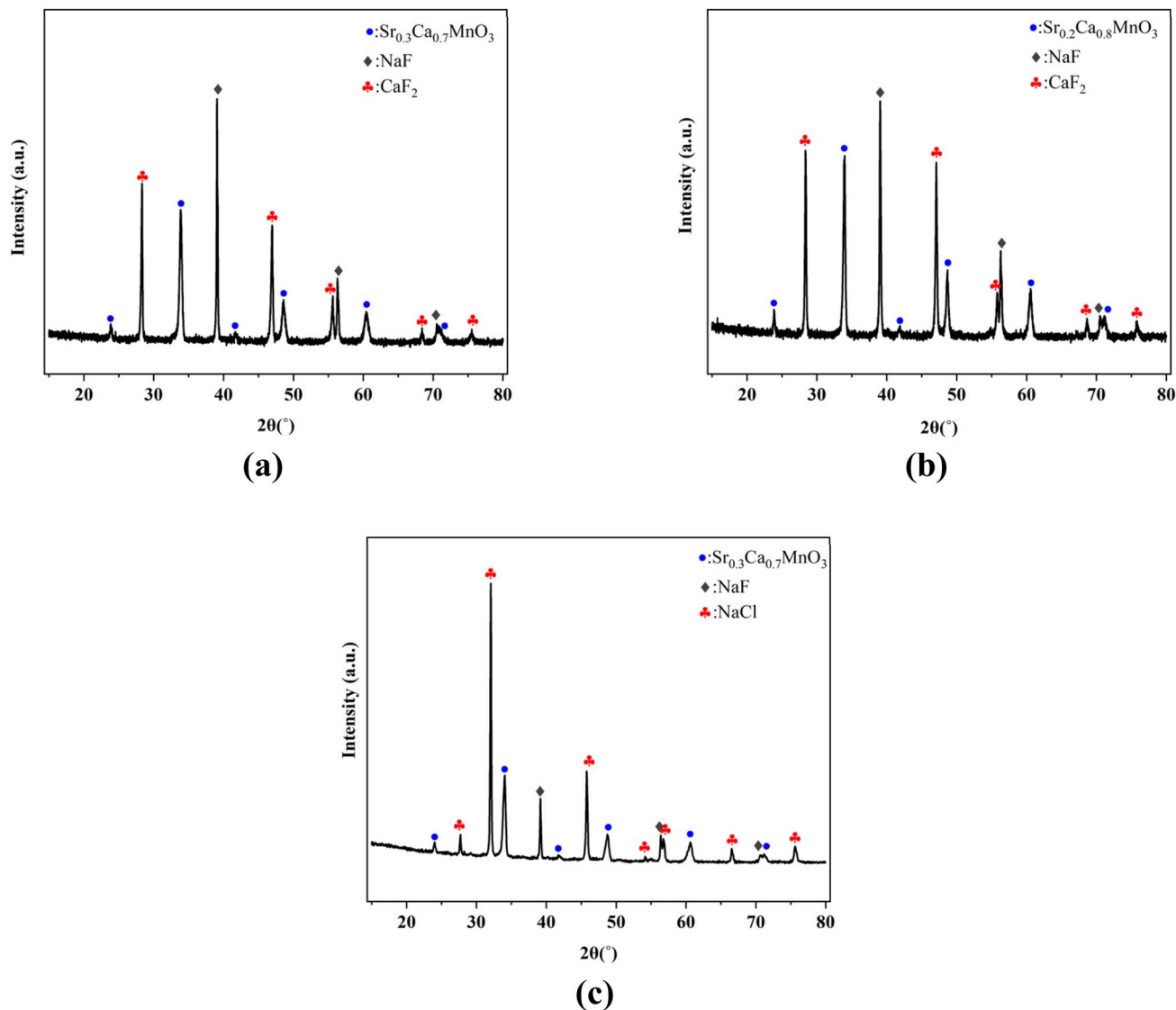


Fig. 2 XRD patterns of composite materials with Ca-based perovskites (a) SCFM1:NaF–CaF₂, (b) SCFM2:NaF–CaF₂ and (c) SCFM2:NaF–NaCl.

material with LiF–NaF–CaF₂ while the latter couldn't. A similar case that supports the high stability of La-based perovskite oxides was observed for Li₂CO₃–Na₂CO₃. The carbonate salt formed a compatible composite with a La-based material while a reaction with a Sr-based oxide occurred, causing incompatibility. Regarding the composites containing Li₂MoO₄, a minor peak of SrMoO₄ was detected from a possible reaction between LSF2 and Li₂MoO₄, whereas there seemed to be better compatibility for LSF1: Li₂MoO₄.

In our previous high-throughput study, we showed that among the substituted SrFeO_{3–δ}-based materials, SCFM2 achieved the highest thermochemical energy density.³⁸ Due to the high redox activity of SCFM2, SCFM-based composites stored heat in both thermochemical and latent forms. On the other hand, LSF-based composites have shown better compatibility with various metal oxides and higher stability in the long term. Considering that many waste streams contain reducible gases such as H₂ and CO, we extended the application of LSF-based

composites for chemical energy recovery from the waste gas. Therefore, SCFM and LSF-containing composites were focused upon, with further details provided in Sections 3.2 and 3.3.

3.2 SCFM-based composite materials

3.2.1 Phase change properties and redox activity. Here, we assessed the latent heat and melting/solidification points of the composite materials under redox cycling conditions, the key parameters for thermal energy storage of molten salts.^{21,25} The significant results for SCFM-based composites are summarized in Table 4, with additional data in Table S2 and Fig. S3–S9.† This evaluation was essential in confirming that phase change properties of composite materials align with those of the individual salts, thereby validating the compatibility between salt and perovskites. For example, SCFM2:NaF–NaCl exhibited a large discrepancy between the theoretical salt properties and measured properties of the composite, suggesting a potential



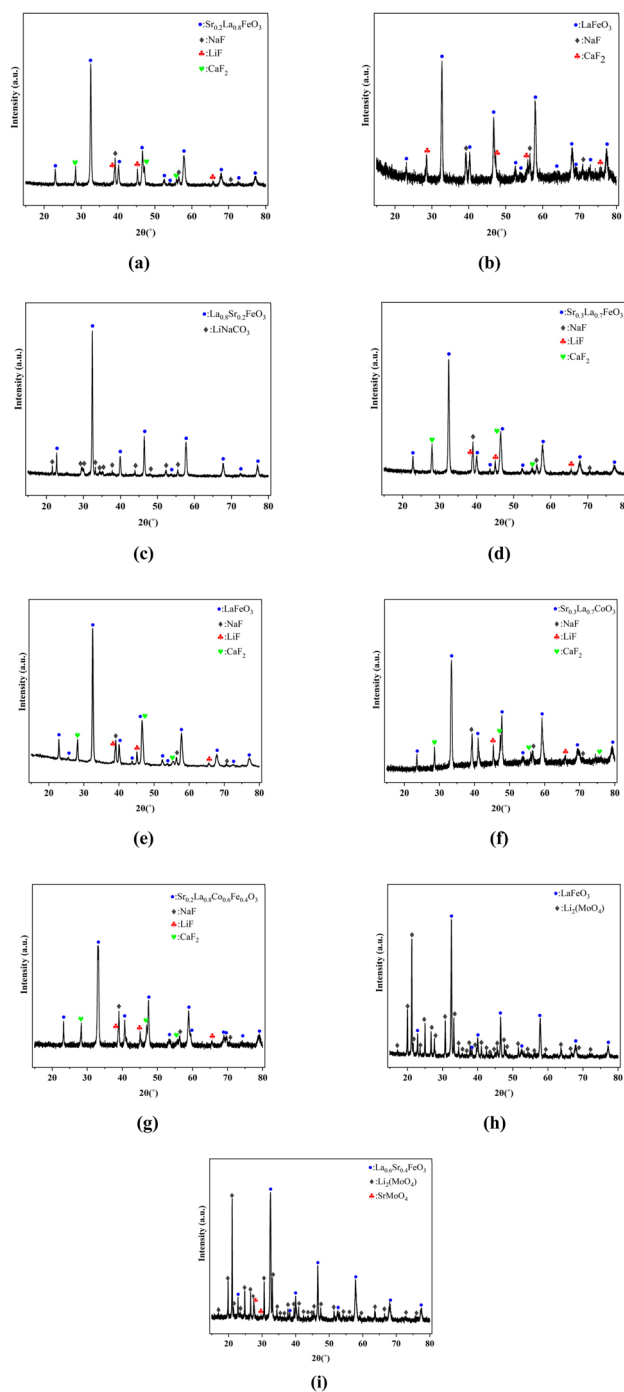


Fig. 3 XRD patterns of composite materials with La-based perovskites (a) LSF1:LiF–NaF–CaF₂, (b) LSF1:MgF₂–NaF–CaF₂, (c) LSF1:Li₂CO₃–Na₂CO₃, (d) LSF2:LiF–NaF–CaF₂, (e) LSF3:LiF–NaF–CaF₂, (f) LSCM7391:LiF–NaF–CaF₂, (g) LSFCo:LiF–NaF–CaF₂, (h) LSF1:Li₂MoO₄ and (i) LSF2:Li₂MoO₄.

reaction between salt and perovskite during redox cycling; further details are provided in the ESI.[†] Meanwhile, the composite material SCFM2:NaF–CaF₂ with a weight ratio of 0.4 : 0.6 has shown promising performance in terms of high latent heat of $\sim 532 \text{ kJ kg}_{\text{salt}}^{-1}$ (mechanical stability information can be found in Section 5 of the ESI[†]). The measured latent heat

for the composite material was slightly lower than that of pure salt, as shown in Table 4. It should be noted that variations up to $\pm 10\%$ in repeated measurements were observed, likely due to differences in the Pt pan geometry and varied contact between the salt and the inert material at the bottom of the pan. Also, the melting point of the composite (798°C) was measured to be slightly lower than that of pure salt ($\sim 805^\circ\text{C}$).

In addition, we examined the redox activity of the SCFM2:NaF–CaF₂, associated with O₂ release and uptake of the perovskite oxides during the reduction and oxidation steps, respectively. Upon switching from Ar to 20% O₂/Ar, an oxidation capacity of 1.05 wt% per oxide was determined. This was slightly less than the redox capacity (1.13 wt%) of pure perovskite under the same conditions (Fig. S7[†]), indicating that molten salt may slightly inhibit oxygen diffusion and exchange. When the atmosphere was returned to Ar, the reduction capacity matched the oxidation, indicating a reversible oxygen exchange behavior. Using the previously obtained enthalpy data of SCFM2, a thermochemical energy density of $\sim 105 \text{ kJ kg}_{\text{oxide}}^{-1}$ ($\sim 42 \text{ kJ kg}_{\text{composite}}^{-1}$) was calculated. With the contributions from the sensible heat of salt and oxide, an overall energy density of $\sim 523 \text{ kJ kg}^{-1}$ (4th cycle) was determined. Although the contribution of thermochemical energy was less than latent heat, using a redox-active support material instead of an inert material was advantageous for the overall energy density of the composite.

We evaluated the stability of phase change properties and redox activity in SCFM2:NaF–CaF₂ (0.4 : 0.6). Under a temperature swing of $740\text{--}890^\circ\text{C}$, the composite exhibited a weight loss of 3.92 wt% (5.88 wt% per salt) over 10 redox cycles, which can be attributed to the evaporation of fluoride salt due to high vapor pressures.⁵² However, the weight loss was still significantly lower than the loss of $\sim 10.2 \text{ wt\%}$ in the pure salt under similar conditions (Fig. S3[†]), indicating that perovskite stabilizes the fluoride salt by inhibiting its evaporation. To further decrease this loss, the experiments were conducted under a swing between $670\text{--}820^\circ\text{C}$, with a layer of YSZ particles covering the composite. As shown in Fig. S4–S6[†] and 4a, both the composite material and salt demonstrated more stable performance under this lower temperature range. Over 10 cycles, the latent heat decreased from ~ 532 to $\sim 513 \text{ kJ kg}_{\text{salt}}^{-1}$ in the composite. The redox capacity of SCFM2 also gradually declined from 1.05 to 0.56 wt% (per oxide) over the 10 cycles (Fig. 4b), possibly due to the partial decomposition of SCFM2 or the fluoride salt suppressing oxygen diffusion. Despite the slight deactivation, the overall energy density of the composite material remained high after 10 cycles ($\sim 501 \text{ kJ kg}^{-1}$).

3.2.2 Long-term performance evaluation. Despite the slight deactivation of SCFM2:NaF–CaF₂ over 10 cycles, its good redox activity and large latent heat capacity made it an interesting candidate for long-term performance evaluation. As shown in Fig. 5a and S8,[†] the overall energy density decreased from ~ 523 to $\sim 430 \text{ kJ kg}^{-1}$ over 100 cycles under the conditions of $670^\circ\text{C}/20\% \text{ O}_2\text{--}820^\circ\text{C}/\text{Ar}$, with a 23% reduction in latent heat. This deactivation is likely due to the evaporation of the fluoride salt, as indicated by an 11.6 wt% loss, suggesting that SCFM2 was unable to fully stabilize the NaF–CaF₂ salt material. Choosing a salt mixture with a lower melting point could potentially

Table 3 The summary of compatibility between salt mixtures and metal oxides *Undesirable phases are highlighted in italic*

| Salt mixture | Perovskite | XRD phases | Compatibility (yes/no) |
|--|------------|--|------------------------|
| Li ₂ CO ₃ –Na ₂ CO ₃ | SBF | Na ₂ CO ₃ , SrFeO _{2.6} , SrCO ₃ , Li _{1.05} Fe _{0.95} O ₂ , Sr ₂ Fe ₃ O ₆ , Na ₃ FeO ₃ | N |
| | LSF1 | La _{0.8} Sr _{0.2} FeO ₃ , LiNaCO ₃ | Y |
| LiF–NaF–CaF ₂ | CAM | CaF ₂ , NaF, Ca ₂ AlMnO ₅ , Li ₂ MnO ₃ , CaO, LiAlO ₂ , CaMn ₇ O ₁₂ | N |
| | SF | NaF, Sr _{0.88} Ca _{0.08} Na _{0.02} Fe _{0.02} F ₂ , Li _{1.05} Fe _{0.95} O ₂ , CaO, FeF ₃ | N |
| | SBF | NaF, Sr _{0.88} Ca _{0.08} Na _{0.02} Fe _{0.02} F ₂ , Li _{0.5} Fe _{0.5} O ₂ , Ca _{0.5} Sr _{0.5} FeO ₂ , LiFeO ₂ , LiBaF ₃ , Sr ₃ Fe ₂ O ₆ | N |
| | SCMC01 | NaF, CaF ₂ , CaMnO ₃ , Li ₂ MnO ₃ | N |
| | SCMC02 | NaF, CaF ₂ , CaMnO _{2.656} , Li _{1.33} Mn _{0.667} O ₂ | N |
| | LSF1 | La _{0.8} Sr _{0.2} FeO ₃ , CaF ₂ , NaF, LiF | Y |
| | LSF2 | La _{0.7} Sr _{0.3} FeO ₃ , CaF ₂ , NaF, LiF | Y |
| | LSF3 | LaFeO ₃ , CaF ₂ , NaF, LiF | Y |
| | LSCoM2 | La _{0.7} Sr _{0.3} CoO ₃ , CaF ₂ , NaF, LiF | Y |
| | LSCoM1 | NaF, Sr _{0.4} La _{0.6} CoO ₃ , Sr _{0.5} Ca _{0.5} F ₂ , LiCoO ₂ | N |
| | LSFCo | La _{0.8} Sr _{0.2} Co _{0.6} Fe _{0.4} O ₃ , CaF ₂ , NaF, LiF | Y |
| | SCFM1 | Sr _{0.3} Ca _{0.7} MnO ₃ , NaF, CaF ₂ | Y |
| | SCFM2 | Sr _{0.2} Ca _{0.8} MnO ₃ , NaF, CaF ₂ | Y |
| | SCFM1 | CaF ₂ , Sr _{0.5} Ca _{0.5} MnO ₃ , NaF, Na _{0.15} Ca _{0.85} F _{1.85} , CaFe ₂ O ₄ , Na _{0.457} Fe _{0.67} Mn _{0.33} O ₂ | N |
| MgF ₂ –NaF–CaF ₂ | LSF1 | La _{0.6} Sr _{0.4} FeO _{2.997} , CaF ₂ , NaF | Y |
| NaF–NaCl | SCFM2 | Sr _{0.3} Ca _{0.7} MnO ₃ , NaF, NaCl | Y |
| NaF–KF | SCFM2 | NaF, CaMnO ₃ , KCaF ₃ , K ₃ NaFe ₂ O ₈ ^b | N |
| | CAM | NaF, CaMnO _{2.97} , Ca ₂ MnO ₄ , CaAl ₂ O ₄ , KCaF ₃ , KAlO ₂ | N |
| LiF–CaF ₂ | SCFM1 | CaF ₂ , Li _{1.259} Mn _{0.519} Fe _{0.225} O ₂ | N |
| LiF–NaF | SF | SrFeO _{2.6} , LiF, NaF, SrF ₂ , LiFeO ₂ , Sr ₃ Fe ₂ O ₇ , FeF ₃ , Fe ₃ O ₄ ^b | N |
| | SBF | LiF, NaF, SrF ₂ , Li _{0.5} Fe _{0.5} O, Fe ₂ O ₃ ^b | N |
| Li ₂ MoO ₄ | LSF1 | Li ₂ MoO ₄ , LaFeO ₃ | Y |
| | LSF2 | Li ₂ MoO ₄ , La _{0.6} Sr _{0.4} FeO ₃ , SrMoO ₄ | Y ^a |

^a Trace amount of SrMoO₄ was detected. ^b Minor unidentified peaks were present in the XRD pattern.

Table 4 Measured melting enthalpy (kJ kg_{salt}^{−1}) and melting points (°C) of composite materials. The weight ratios of eutectic salt mixtures are provided in Table 2

| Sample name (weight ratio) | Melting enthalpy (kJ kg _{salt} ^{−1}) | | Melting temperature (°C) | |
|---|---|-----------------|--------------------------|----------|
| | Reported | Measured (±10%) | Reported | Measured |
| NaF–CaF ₂ | 560–600 | 561.80 | 810 | 804.67 |
| NaF–CaF ₂ :SCFM2 (0.4 : 0.6) | 560–600 | 532.47 | 810 | 797.91 |
| NaF–NaCl:SCFM2 (0.5 : 0.5) | 572 | 340.84 | 674 | 672.13 |

enhance the stability of ROMS composites by lowering the thermal losses.

On the other hand, SCFM2 maintained its redox activity, although the redox capacity gradually decreased from ~1.05 wt% to ~0.45 wt%, reducing thermochemical heat from ~105 to ~50 kJ kg_{oxide}^{−1} (~42 to ~20 kJ kg_{composite}^{−1}) over 100 cycles. Post-experimental XRD (Fig. S33†) showed that the reduced perovskite was transitioned to a Brownmillerite phase (Sr₂Fe₂O₅) with additional minor peaks suggesting the partial decomposition of the oxide, which would explain the decrease in thermochemical heat. However, phase identification was challenging due to the presence of inert material that could not be fully separated from the sample. Nevertheless, the XRD results indicated that compatibility between salt and oxide was maintained after 100 redox cycles. Despite the deactivation of SCFM2:NaF–CaF₂, these results support the hypothesis that molten salts and perovskite oxides can be compatible, storing

heat *via* both phase change of the molten salt and redox reactions of the metal oxide.

3.3 LSF-based composite materials

3.3.1 Phase change properties and redox-activity. Most of the compatible composite materials included La-containing perovskites due to their stability in the presence of salt mixtures. In SCFM2:NaF–CaF₂, the high melting point of the salt restricted the operating temperature to higher temperatures (>670 °C). Meanwhile, La-based perovskites paired with lower melting point salts enabled lower operating temperatures, reducing thermal losses. The summary of the measurements for LSF-based composites is presented in Table 5 below, with additional data in Fig. S10–S25 and Table S2.†

Our results revealed that the oxide:salt ratio has a significant impact on the phase change property of the composite materials. Fig. 6 demonstrates that melting enthalpy for



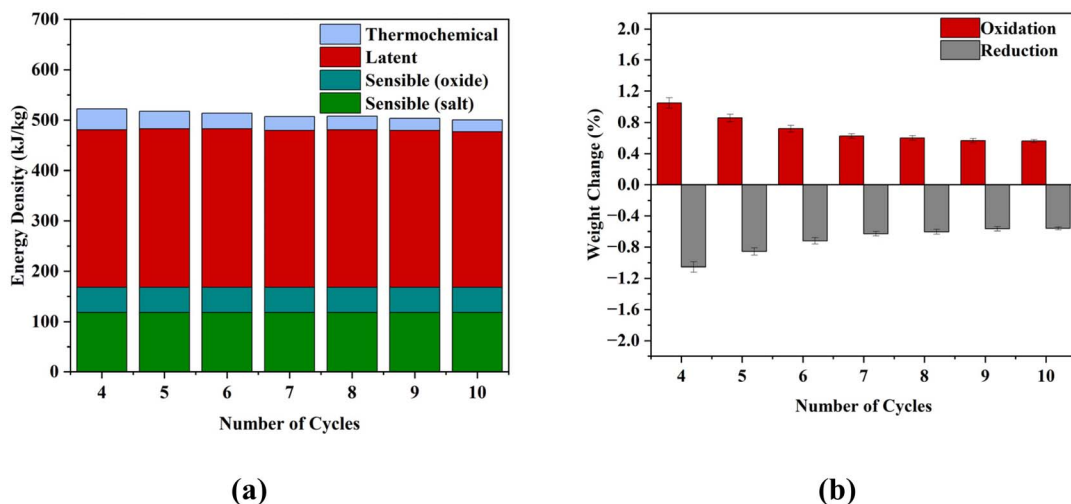


Fig. 4 TGA-DSC measurements for SCFM2:NaF–CaF₂ with the weight ratio of 0.4 : 0.6 at 670 °C/20% O₂–820 °C/Ar during 10 cycles. (a) Overall energy density (kJ kg^{−1}), (b) weight change (%) normalized to the weight of SCFM2. Latent heat is the measured melting enthalpy from DSC. Thermochemical heat is calculated using the previous data on SCFM2.⁵⁸ Sensible heat is based on estimated heat capacities through an additive principle using NIST database.⁶²

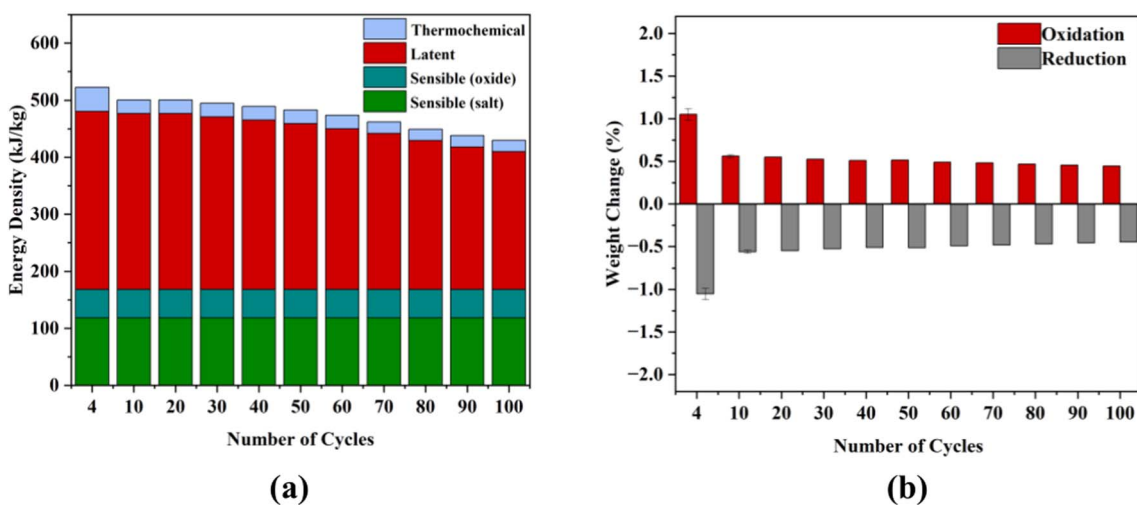


Fig. 5 TGA-DSC measurements for SCFM2:NaF–CaF₂ with the weight ratio of 0.4 : 0.6 at 670 °C/20% O₂–820 °C/Ar during 100 cycles. (a) Overall energy density (kJ kg_{composite}^{−1}), (b) weight change (%) normalized to the weight of SCFM2. Latent heat is the measured melting enthalpy from DSC. Thermochemical heat is calculated using the previous data on SCFM2.⁵⁸ Sensible heat is based on estimated heat capacities through additive principle using NIST database.⁶²

LSF1:LiF–NaF–CaF₂ decreases with increasing oxide content. While the melting enthalpy of pure LiF–NaF–CaF₂ was measured as ~623 kJ kg_{salt}^{−1}, it dropped to ~580 kJ kg_{salt}^{−1} when mixed with LSF1 at an oxide : salt ratio of 0.4 : 0.6. Similar trends were also observed for the composites of NaF–CaF₂:SCFM2, LSFC:LiF–NaF–CaF₂, and LSF2:Li₂MoO₄. Since the absence of chemical interaction between the salt and oxide phase was confirmed by XRD, the decrease in the latent heat with increasing salt content can be attributed to physical interactions. Previous research has also observed latent heat reduction in a porous supporting medium and linked this to the confinement of the phase change material.^{63–65} Additionally, melting temperatures also decreased with increasing oxide

contents, consistent with the previous findings.^{27,64,66} The LSF-based composite materials with the other salts either faced stability issues or did not have a competitive energy density due to low latent heat, as briefly discussed in the ESI† (for LSF1:Li₂CO₃–Na₂CO₃ and LSF1:LiF–NaF–MgF₂).

In terms of redox activity, most of the La-based perovskites in the composite materials failed to exchange their lattice oxygen during the redox cycles due to: (i) the intrinsic stability of these perovskite oxides, and (ii) the additional mass transfer resistance due to the presence of the salt. While pure LSFCo showed a redox capacity of ~0.08 wt%, no significant weight change was observed for LSFCo in the composite (Fig. S18†). Noting that the temperature range was not high enough to activate the redox



Table 5 Measured melting enthalpy ($\text{kJ kg}_{\text{salt}}^{-1}$) and melting points ($^{\circ}\text{C}$) of composite materials. The weight ratios of eutectic salt mixtures are provided in Table 2

| Sample name (weight ratio) | Melting enthalpy ($\text{kJ kg}_{\text{salt}}^{-1}$) | | Melting temperature ($^{\circ}\text{C}$) | |
|---|--|----------------------------------|--|----------|
| | Reported | Measured (error bar $\pm 10\%$) | Reported | Reported |
| LiF–NaF–CaF ₂ | 640 | 622.93 | 615 | 609.69 |
| LSF1:LiF–NaF–CaF ₂ (0.5 : 0.5) | 640 | 542.73 | 615 | 603.36 |
| LSF1:LiF–NaF–CaF ₂ (0.4 : 0.6) | 640 | 579.74 | 615 | 606.66 |
| LSF2:LiF–NaF–CaF ₂ (0.5 : 0.5) | 640 | 544.00 | 615 | 600.06 |
| LSF3:LiF–NaF–CaF ₂ (0.5 : 0.5) | 640 | 466.54 | 615 | 600.88 |
| LSCoM2:LiF–NaF–CaF ₂ (0.5 : 0.5) | 640 | 549.55 | 615 | 605.17 |
| LSFCo:LiF–NaF–CaF ₂ (0.5 : 0.5) | 640 | 537.41 | 615 | 602.98 |
| LSFCo:LiF–NaF–CaF ₂ (0.4 : 0.6) | 640 | 595.05 | 615 | 606.73 |
| Li ₂ MoO ₄ | 280 | 281.49 | 705 | 693.40 |
| LSF1:Li ₂ MoO ₄ (0.5 : 0.5) | 280 | 254.59 | 705 | 685.08 |
| LSF2:Li ₂ MoO ₄ (0.5 : 0.5) | 280 | 252.46 | 705 | 687.55 |
| LSF2:Li ₂ MoO ₄ (0.6 : 0.4) | 280 | 219.95 | 705 | 688.18 |

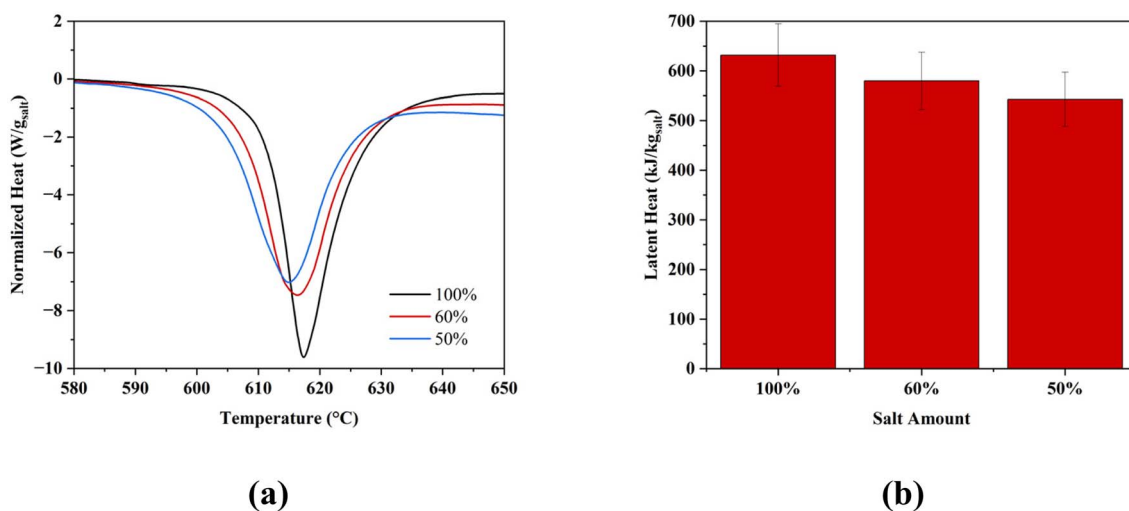


Fig. 6 Comparison of LSF1:LiF–NaF–CaF₂ at various salt amounts. (a) Normalized heat flows ($\text{W g}_{\text{salt}}^{-1}$) and (b) latent heats ($\text{kJ kg}_{\text{salt}}^{-1}$)

behavior of La-based perovskite. Previous studies have shown that La-based perovskite can achieve high reaction enthalpy and oxygen capacity at elevated temperatures.^{67,68} Among the LSF-based composites, only LSF2 exhibited a weight gain corresponding to oxidation (Fig. S13, S22 and S23†). Increased Sr : La ratio was found to benefit the redox activity by lowering the reduction temperature but also increased the likelihood of chemical interactions with the salt. In LSF2:Li₂MoO₄, the redox capacity increased from ~ 0.08 to ~ 0.15 wt% per oxide with oxide content increasing from 50 to 60%. Optimizing the oxide microstructure can potentially decrease the mass transfer resistance but LSF-based composites require a more reducing environment (*e.g.* higher temperatures or reducing gases) in order to exhibit substantial redox capacity. This will be further discussed in a later section.

3.3.2 Long-term performance evaluation. Due to its high latent heat storage and compatibility, LSF1:LiF–NaF–CaF₂ with the weight ratio of 0.4 : 0.6 was selected as a promising

candidate for long-term performance evaluation (see Section 5 in ESI† with respect to mechanical stability). As shown in Fig. 7, the composite demonstrated excellent stability over 100 cycles under the conditions of 510 $^{\circ}\text{C}/20\% \text{ O}_2$ –660 $^{\circ}\text{C}/\text{Ar}$, with no significant change in the latent heat. The good stability of this composite material can be attributed to its lower operating temperature range compared to that of SCFM2:NaF–CaF₂. The addition of LiF to NaF–CaF₂ lowers the melting point, thus allowing for a lower operating temperature range and preventing salt weight loss from evaporation. Since no O_2 release/uptake was observed, there was no thermochemical energy contributed to the overall energy density. After 100 cycles, the total energy density, including latent and sensible heat, remained as high as $\sim 534 \text{ kJ kg}^{-1}$.

Additionally, we compared the XRD pattern of the LSF1:LiF–NaF–CaF₂ before and after 100 cycles in Fig. 8a. The additional peak corresponds to the thin layer of YSZ, which covered the bottom of the pan during the experiment. No significant change



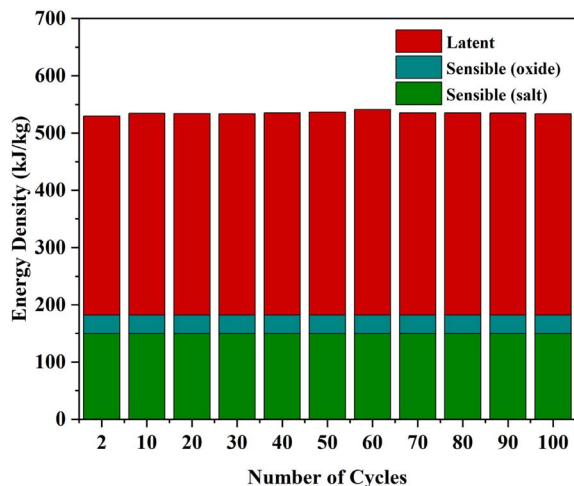
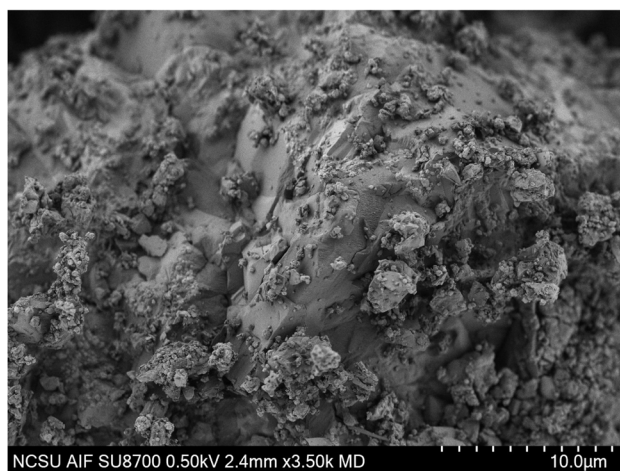
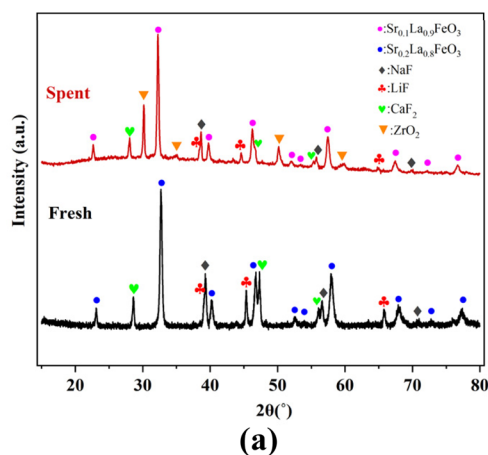


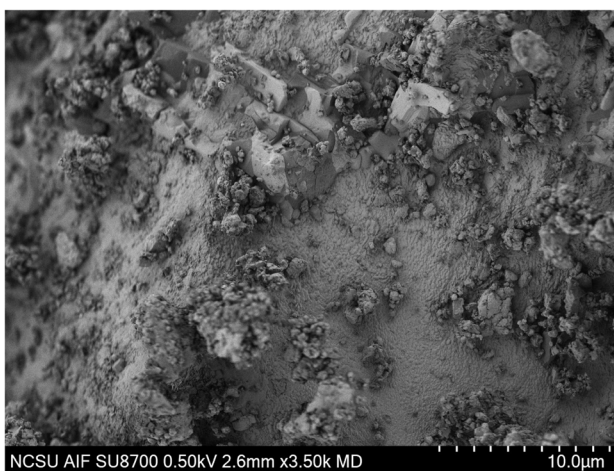
Fig. 7 TGA-DSC measurements for LSF1:LiF-NaF-CaF₂ with the weight ratio of 0.4 : 0.6 at 510 °C/20% O₂–660 °C/Ar during 100 cycles. (a) Overall energy density (kJ kg^{−1}). Latent heat is the measured melting enthalpy from DSC. Sensible heat is based on estimated heat capacities through additive principle using NIST database.⁶²

in the phases of perovskite and salts was seen. This shows that no reactions between LSF and fluoride salt occurred during redox cycles, thus the ROMS composite maintained its compatibility and energy density during 100 cycles. According to Fig. 8b and c, the morphology of the composite material was also maintained after 100 cycles (EDX mappings can be found in Fig. S36†).

3.3.3 Thermal conductivity. For LSF1: LiF-NaF-CaF₂ (0.4 : 0.6), we also measured thermal conductivity, a key factor in heat transfer efficiency.^{11,14} Table 6 presents the measured thermal conductivities and compares them with other composite materials reported for thermal energy storage. Using the transient plane source principle, the thermal conductivity of LSF1: LiF-NaF-CaF₂ (0.4 : 0.6) was found to be 2.51 W m^{−1} K^{−1}, which falls within the range of measured thermal conductivities of individual components. While LSF1 showed relatively low thermal conductivity, consistent with the results of other metal oxides in the literature,^{69,70} the elevated thermal conductivity of fluoride salt led to a competitively high thermal conductivity for the composite material compared to some other reported composites. The high thermal conductivity of the ROMS



(b)



(c)

Fig. 8 Comparison of fresh and spent (after 100 cycles between 510 °C/20% O₂–660 °C/Ar) LSF1:LiF-NaF-CaF₂ (0.4 : 0.6). (a) XRD patterns and SEM images of (b) after sintering, which corresponds to the morphology of composite material after 1 cycle (c) after 100 cycles.

Table 6 Comparison of thermal conductivities at room temperature

| Material | Thermal conductivity ($\text{W m}^{-1} \text{K}^{-1}$) | Measurement method |
|--|--|--------------------|
| LSF1 | 0.76 | Transient |
| LiF-NaF-CaF_2 | 2.96 | Transient |
| $\text{LSF1:LiF-NaF-CaF}_2$ (0.4 : 0.6) | 2.51 | Transient |
| $\text{LiNO}_3\text{-NaNO}_3\text{-KNO}_3\text{-Ca(NO}_3)_2$:calcium silicate ¹¹ | 1.18 | Steady state |
| NaNO_3 : modified diatomite ²⁵ | ~ 0.28 | Transient |
| $\text{Li}_2\text{CO}_3\text{-Na}_2\text{CO}_3\text{:MgO:carbon}^{23}$ | $\sim 3\text{-}5.25$ | Transient |
| Polyethylene glycol:diatomite: expanded graphite ²⁸ | 0.32–0.67 | Transient |

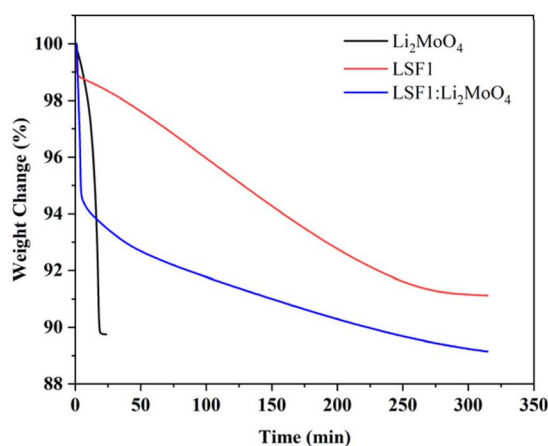
composite enables rapid heat exchange, enhancing adaptability in various reactor designs.

3.3.4 Alternative applications under a reducing gas environment. Despite the stable performance of $\text{LSF1:LiF-NaF-CaF}_2$ composite, the limited redox performance of La-based perovskites decreases the overall energy density. To address this, we explored an alternative usage of ROMS composites. The exhaust gas emitted by electric arc furnaces or blast furnaces in the steel industry carries substantial waste heat, often rich in reducing agents like H_2 and $\text{CO}^{8,71,72}$ which holds valuable potential for thermochemical energy storage applications. Thus, we performed experiments under a reducing gas atmosphere for a composition with Li_2MoO_4 since previous research indicated Mo salts in the liquid phase improve oxygen diffusion.⁷³ Although LSF2 exhibited better potential for redox activity than LSF1 under cyclic conditions between 20% $\text{O}_2\text{-Ar}$, $\text{LSF2:Li}_2\text{MoO}_4$ was not tested due to the trace amount of SrMoO_4 impurity detected in its XRD pattern (Fig. 3i). Therefore, $\text{LSF1:Li}_2\text{MoO}_4$ (0.5 : 0.5) was tested as a potential candidate, with the results presented in Fig. 9 and S26–S32.†

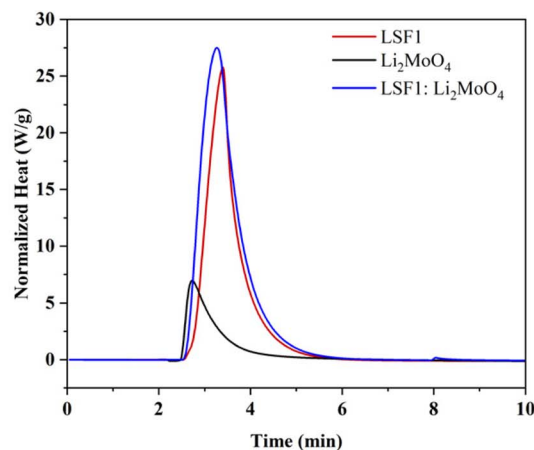
$\text{LSF1:Li}_2\text{MoO}_4$ (0.5 : 0.5) achieved thermochemical energy storage capacity as high as 1813 kJ kg^{-1} after a sufficiently long

reduction time ($\sim 8 \text{ h}$) to reach equilibrium. However, in electric arc furnaces, tap-to-time per batch is typically much shorter, around 30–70 min^{8,72} When a shorter reduction time of 35 min applied, the composite material still achieved an excellent thermochemical energy storage capacity of $\sim 664 \text{ kJ kg}^{-1}$. Comparing this to the oxidation enthalpies of LSF1 ($\sim 239 \text{ kJ kg}^{-1}$) and Li_2MoO_4 ($\sim 683 \text{ kJ kg}^{-1}$) (Table 7), it appears that the redox activity of Li_2MoO_4 primarily enhanced the energy storage capacity of LSF1: Li_2MoO_4 rather than LSF1. Additionally, reduction kinetics, shown in Fig. 9, indicate that rapid weight loss in LSF1: Li_2MoO_4 was mainly attributable to the fast reduction kinetics of Li_2MoO_4 . The fast kinetics resulted in a ROMS composition with improved thermochemical energy compared to pure LSF1. Including the estimated sensible heat and latent heat, the overall energy density for $\text{LSF1:Li}_2\text{MoO}_4$ (0.5 : 0.5) reached 875 kJ kg^{-1} .

While Li_2MoO_4 exhibited rapid weight loss, weight gain didn't match weight loss in Li_2MoO_4 , potentially caused by slow oxidation kinetics as shown in Fig. S28.† Meanwhile weight loss and gain were approximately the same in LSF1 and $\text{LSF1:Li}_2\text{MoO}_4$, indicating reversible redox behaviors. This indicates that mixing LSF1 and Li_2MoO_4 created a synergistic benefit:



(a)



(b)

Fig. 9 Comparison of LSF1, Li_2MoO_4 , and $\text{LSF1:Li}_2\text{MoO}_4$ with the weight ratio of 0.5 : 0.5 during long reduction. (a) Weight changes (%) at $730^\circ\text{C}/20\% \text{H}_2$ and (b) heat flow (mW) at $580/20\% \text{O}_2$.



Table 7 Weight changes (%) and energy densities of LSF1, Li_2MoO_4 , and LSF1: Li_2MoO_4 (0.5 : 0.5). Weight loss and weight gain correspond to the weight changes in the samples during gas switch to 20% H_2 and 20% O_2 , respectively

| Material | Weight loss (wt%) | Weight gain (wt%) | Oxidation enthalpy (kJ kg^{-1}) $\pm 10\%$ | Overall energy density (kJ kg^{-1}) |
|---|-------------------|-------------------|---|--|
| Li_2MoO_4 | 10.0 | 8.17 | 682.7 | 1051 |
| LSF1 (short reduction) | 2.10 | 2.49 | 238.9 | 319.4 |
| LSF1 (long reduction) | 8.90 | 8.85 | 1309 | 1389 |
| LSF1: Li_2MoO_4 (short reduction) | 6.37 | 6.39 | 664.1 | 874.7 |
| LSF1: Li_2MoO_4 (long reduction) | 11.5 | 11.5 | 1813 | 2024 |

LSF1 facilitates rapid oxidation and Li_2MoO_4 drives fast reduction. As can be seen from Fig. S31 and S32,[†] in a cyclic experiment, the fast reduction and oxidation behavior of LSF1: Li_2MoO_4 with the weight ratio of 0.6 : 0.4 was maintained. While a detailed understanding of the reduction and oxidation mechanisms for this interesting composite is beyond the scope of this study, its promising performance can encourage future research aimed at recovering waste heat.

4. Comparison of ROMS composites

As can be seen from Table 8, ROMS composites offer superior thermal energy storage performance compared to phase change composites with inert skeletons. They can achieve higher energy densities within narrower temperature ranges. Fig. 10 compares the thermal energy densities of three ROMS composite materials with different performance features. LSF1: LiF-NaF-CaF_2 exhibited the highest latent heat capacity of $580 \text{ kJ kg}_{\text{salt}}^{-1}$ though it showed no redox activity under a pressure swing between 20% O_2 -Ar, leading to a total energy density of $\sim 530 \text{ kJ kg}_{\text{composite}}^{-1}$ over a relatively low-temperature range (510–660 °C). Meanwhile, SCFM2: NaF-CaF_2 exhibited both thermochemical and latent heat based energy storage. Still, latent heat storage was the main contributor to its overall energy density of $\sim 523 \text{ kJ kg}^{-1}$ under the cycling conditions of 670/20% O_2 -820 °C/Ar. Lastly, LSF1: Li_2MoO_4 achieved the highest overall energy density up to 875 kJ kg^{-1} at 580/20% O_2 -730 °C/20% H_2 , driven primarily by redox activity of both salt and oxide. This material is proposed for harnessing fuel containing off-gas from the steel industry. In terms of sensible heat storage, LiF-NaF-CaF_2 had the highest capacity among salts, reaching $250 \text{ kJ kg}_{\text{salt}}^{-1}$, while SCFM2 was expected to achieve the highest among oxides, at

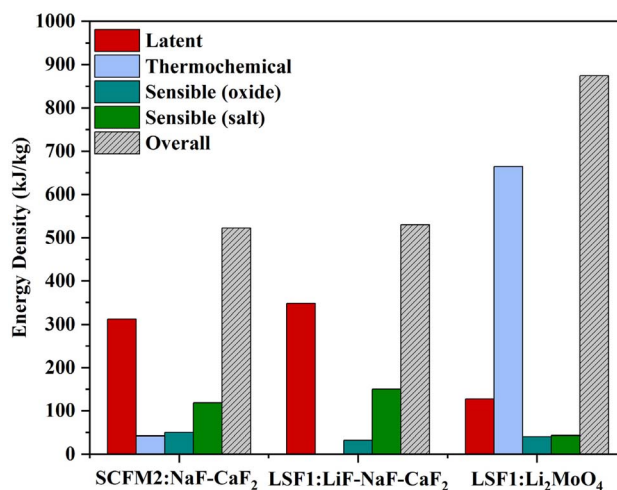


Fig. 10 Comparison of energy densities for SCFM2: NaF-CaF_2 (0.4 : 0.6), LSF1: LiF-NaF-CaF_2 (0.4 : 0.6), and LSF1: Li_2MoO_4 (0.5 : 0.5) under the redox cycling conditions of 670/20% O_2 -820 °C/Ar, 510/20% O_2 -660 °C/Ar, and 580/20% O_2 -730 °C/20% H_2 , respectively. The units of $\text{kJ kg}_{\text{composite}}^{-1}$ were used for each component. Sensible heat is based on estimated heat capacities through additive principle using NIST database.⁶²

$\sim 125 \text{ kJ kg}_{\text{oxide}}^{-1}$. LSF1: LiF-NaF-CaF_2 showed excellent stability and robustness over 100 cycles, whereas SCFM2: NaF-CaF_2 showed deactivation with a gradual decline in latent and thermochemical heat over time. LSF1: Li_2MoO_4 showed good stability over the 5 cycles tested under a more reducing atmosphere.

5. Conclusions

This study introduces redox-active oxide-molten salt (ROMS) composites, where a porous perovskite oxide serves as a support to prevent salt leakage. This novel family of materials has the potential to utilize both latent heat from the phase transition of salt and thermochemical heat from the redox reactions to achieve high energy density within narrow temperature swings. Among 25 tested perovskite-salt combinations, 12 were found to be compatible with La-based perovskites showing superior compatibility and Sr and/or Ca-containing oxides exhibiting good redox activity. SCFM271: NaF-CaF_2 (0.4 : 0.6) was identified for both phase transition and redox-based energy storage with an overall capacity of $\sim 523 \text{ kJ kg}^{-1}$ (670–820 °C) but faced

Table 8 Comparison of energy densities storage densities over the corresponding temperature ranges

| Material | Energy storage density (kJ kg^{-1}) | Temperature range (°C) |
|--|--|------------------------|
| SCFM2: NaF-CaF_2 | 523 | 670–820 |
| LSF1: LiF-NaF-CaF_2 | 530 | 510–660 |
| LSF1: Li_2MoO_4 | 875 | 580–730 |
| NaNO_3 : Modified diatomite ²⁵ | 383 | 130–330 |
| NaNO_3 : Ca(OH)_2 ⁷⁴ | 265–468 | 140–340 |
| Graphite: Na_2CO_3 - Li_2CO_3 : MgO ²⁷ | 525 | 300–600 |
| NaCl-KCl : diatomite ¹⁰ | 393 | 550–750 |



stability and deactivation issues over the long term. Meanwhile, LSF1:NaF–CaF₂–LiF (0.4:0.6) maintained a latent heat-based energy storage capacity of ~530 kJ kg⁻¹ although it did not exhibit redox activity under the cycling conditions of 510/20% O₂–660 °C/Ar. It demonstrated excellent stability over 100 cycles, while compatibility and morphology were also maintained. The thermal conductivity of LSF1: LiF–NaF–CaF₂ was found to be 2.51 W m⁻¹ K⁻¹. Lastly, LSF1: Li₂MoO₄ (0.5:0.5) exhibited high redox activity with an overall energy density up to ~875 kJ kg⁻¹ and was proposed as a promising candidate for recovering waste gas streams rich in residue fuels. The interesting characteristics and versatility of the ROMS composites reported in this study can potentially find applications for various thermal energy storage scenarios.

Data availability

Data supporting this article have been included as part of the ESI.†

Conflicts of interest

There are no conflicts to declare.

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