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# Gas exclusion zones in Type II porous liquids

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Porous liquids combine permanent porosity with fluidity and may ultimately find uses which are not possible for conventional liquids or porous solids. An important general characteristic of porous liquids studied to date is that they exhibit very high gas solubilities. Here, we examine this aspect in more detail than has been done previously, in particular with regard to CO2 and CH4 solubility in the Type II porous liquid Noria<sub>OFt</sub>@15C5 (15C5 = 15-crown-5). Whilst this porous liquid exhibits increased CH<sub>4</sub> solubility compared to neat 15-crown-5, counterintuitively it actually exhibits equal or lower CO2 solubility than the neat solvent 15C5 at pressures above 1 bar. Molecular dynamics modelling reveals that although the pore space does provide a good binding site for gas molecules, there is an 'exclusion zone' around the pore space within which binding of CO<sub>2</sub> molecules is disfavoured compared to binding within the bulk solvent. The unfavourable binding in this region arises from a number of effects, including (i) steric exclusion from the bulky covalent framework of the Noria<sub>OFt</sub> host, and (ii) ordering of 15C5 solvent molecules in the solvation shell around the Noria<sub>OEt</sub>. The first porous liquid to be based on the host Cryptophane-A, Cryptophane-A@Cyrene, was prepared in the expectation that the smaller framework bulk of Cryptophane-A compared to that of Noria $_{\text{OEt}}$  should result in a smaller exclusion zone. Correspondingly, this porous liquid did indeed exhibit improved CO2 uptake compared to its neat solvent, supporting the assertion that the exclusion zone is at least in part due to exclusion of gas from the framework of the host. Overall, the work provides a more sophisticated understanding of gas solubility in Type II PLs and suggests some additional design considerations for achieving high solubility for a given gas. It also shows that, as well as being able to increase the solubility of certain gases PLs can also conceivably be designed to suppress the solubility of gases under some conditions, which could be useful in tuning selective dissolution.

# Introduction

Porous liquids (PLs) are a new class of materials which are capable of efficient and continuous separation of gases due to their combination of fluidity and permanent porosity. The presence of pores increases gas solubility through physisorption and can potentially do this on a size- and shape-selective basis.<sup>1-4</sup>

Type II porous liquids (T2PLs) consist of rigid, empty host species dissolved in size-excluded solvents. Rigidity of the host of guest molecules which could negate the porosity. The hosts should also be highly soluble to maximise the porosity of the porous liquid. Several hosts have been identified as suitable

is important, as flexible hosts could collapse upon the removal

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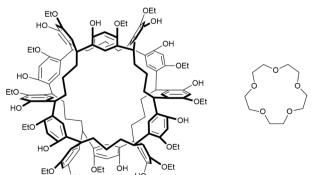


Fig. 1 Structures of Noria $_{\rm OEt}$  (left) and the size-excluded solvent 15-crown-5 (15C5, right) which were used to form the Type II porous liquid Noria $_{\rm OFI}$ @15C5.

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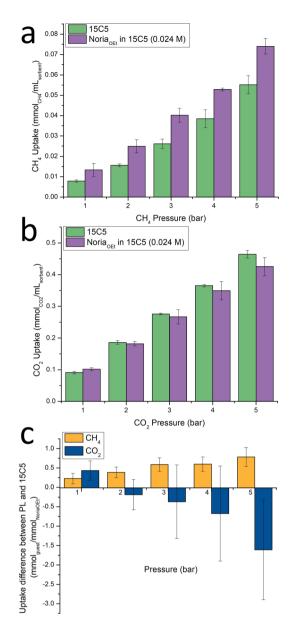


Fig. 2 Gas solubilities in  $Noria_{OEt}@15C5$  and pure 15C5 from 1-5 bar. (a)  $CH_4$ , (b)  $CO_2$ , (c) the 'apparent occupancy' of the  $Noria_{OEt}$  host, specifically the difference between the gas solubilities in 15C5 and  $Noria_{OEt}@15C5$ , expressed as a mole ratio.

generating T2PLs including imino-spherand organic cages, Noria $_{\rm OEt}$  and metal-organic cages (MOCs). $^{5,6}$ 

Studies of Type II PLs to date have all found that the solubility of gases in these phases is greatly increased with respect to the neat solvent, which is expected from the presence of permanent pores. In particular, from Scaled Particle Theory, the main energy penalty to dissolution of a solute is the energy required to form a notional 'cavity' (*i.e.* pore) in the solvent in which the solute can be accommodated.<sup>7</sup> In PLs, the pore is preformed by the molecular host and so this energy penalty to form a pore is negated.

Noria<sub>OEt</sub> (Fig. 1, (left)) was shown by Alexander *et al.* to be an effective host for Type II PLs due to its rigidity, internal cavity,

ease of synthesis and chemical robustness.<sup>8</sup> It has good solubility in 15-crown-5 (15C5) (Fig. 1, (right)) which is often used in Type II PLs as a size-excluded solvent. The resulting solution, Noria<sub>OEt</sub>@15C5-24 mM (hereafter simply Noria<sub>OEt</sub>@15C5) was concluded to be a porous liquid because of the increased solubility of CH<sub>4</sub> compared to that in pure 15C5, and the presence of pores was supported by detailed modelling using molecular dynamics. The CH<sub>4</sub> solubility data are reproduced in Fig. 2a. The PL consistently exhibits greater CH<sub>4</sub> solubility than does pure 15C5 at pressures from 1–5 bar and the difference in solubility increases with pressure.

In this paper, we have explored the solubility of  $\mathrm{CO}_2$  in  $\mathrm{Noria}_{\mathrm{OEt}}$  and made some counter-intuitive findings that increase our understanding of gas uptake in Type II PLs. We also report a new T2PL, Cryptophane-A@Cyrene.

# Results and discussion

#### Porous liquid synthesis and gas uptake measurements

Noria<sub>OEt</sub> and Noria<sub>OEt</sub>@15C5 (24 mM) were prepared as described previously.<sup>8</sup> Briefly, Noria<sub>OEt</sub> was dissolved in 15C5 by gentle heating. All characterisation data for Noria<sub>OEt</sub> and Noria<sub>OEt</sub>@15C5 were in accord with the previous work.<sup>8</sup> The resulting solution was then left overnight in a refrigerator to allow for any potential precipitation and ensure that the solution was not super-saturated. CO<sub>2</sub> solubility in Noria<sub>OEt</sub>@15C5 was measured at room temperature from 1–5 bar using the same isobaric method used previously for Noria<sub>OEt</sub>@15C5 and for other porous liquids as described elsewhere and in the SI.<sup>8-10</sup> For comparison, the analogous CO<sub>2</sub> solubility data for pure 15C5 were also measured and are shown in Fig. 2b. All data were measured in triplicate and error bars indicate standard deviations.

At 1 bar,  $Noria_{OEt}$ @15C5 shows greater  $CO_2$  solubility than does 15C5, as expected for a porous liquid. However, unexpectedly, from 2–5 bar the PL exhibits equal or lower  $CO_2$  solubility than 15C5. Given the standard deviations in the data care must be taken in comparing solubilities in 15C5 and  $Noria_{OEt}$ @15C5 at specific pressures. However, the data suggest a trend of  $Noria_{OEt}$ @15C5 becoming a progressively worse  $CO_2$  solvent than 15C5 as pressure increases.

The contrast in behaviour between CH<sub>4</sub> and CO<sub>2</sub> is emphasized in Fig. 2c, which shows the 'apparent occupancy' of the Noria host. Specifically, for each gas, we plot the difference between its solubility in Noria<sub>OEt</sub>@15C5 and in pure 15C5. The data are expressed as the mole ratio of this difference in gas solubility to the amount of Noria<sub>OEt</sub> present in the PL. Here, the error bars again make it impossible to draw firm conclusions in comparing data between specific pressures within either series. However, this representation emphasises the overall trend that for CH<sub>4</sub> as pressure increases the PL is increasingly a better solvent than pure 15C5. It also shows that, notably, even at 5 bar the average degree of host occupation is still only ca. 0.78 molecules of CH<sub>4</sub>. For CO<sub>2</sub>, at 1 bar the PL is a better solvent than pure 15C5, with an apparent occupancy of 0.43, greater than that observed for CH<sub>4</sub> (0.23), which would be expected from the expected stronger binding of CO<sub>2</sub> However, above 1 bar **Edge Article Chemical Science** 

pressure Fig. 2c emphasises that the PL becomes increasingly worse than 15C5 as a solvent, as mentioned above. This is highlighted by the fact that the apparent occupancy becomes negative at pressures greater than 1 bar. Therefore, it would seem that for CO<sub>2</sub> the beneficial effect of the pore only dominates the gas uptake at relatively low pressures (1 bar), and at higher pressures other negative effects appear to dominate.

With regard to these other effects, we initially reasoned that the difference in behaviour between the two gases might reflect the fact that the pure solvent 15C5 is a much better solvent for CO2, than for CH4 (based on our solubility data the Henry constants,  $H_{\rm s}^{\rm cp}$ , are 93.9  $\times$  10<sup>-3</sup> mol per L per atm and 11.9  $\times$ 10<sup>-3</sup> mol per L per atm for CO<sub>2</sub> and CH<sub>4</sub> respectively). In particular, at higher pressures, the dominant effect of the bulky Noria<sub>OEt</sub> host could be that it effectively replaces a significant number of solvent molecules with a region of space from which the gas molecules are sterically excluded by the bulk of the host's structure. These solvent molecules are much better at dissolving CO2 than CH4, and thus the observed effect is that the overall CO2 solubility is negatively impacted at higher pressures. Effectively, a gas "exclusion zone" exists around the pore due to the host's framework. We also reasoned that this exclusion could potentially extend further, into the solvation shell of Noria<sub>OEt</sub>@15C5, since in this region CO<sub>2</sub> molecules most compete with Noria<sub>OEt</sub> for solvation sites (i.e. the oxygen centres) of the 15C5 solvent.

#### Molecular dynamics simulations

These hypotheses were explored using molecular dynamics (MD) modelling. Simulations were used to examine the spatial distribution of gas molecules in the porous liquid, identifying thermodynamically favoured or disfavoured regions and characterising solvent structuring around the host. Simulation parameters, including force-field details, system preparation, and validation procedures, are provided in the SI.

To explore the free energy landscape for gas positioning around the host, Umbrella Sampling (US) simulations were used to compute the potential of mean force (PMF) for transferring a CO2 or CH4 molecule from bulk solvent to a radial distance, r, from the centre of a Noria<sub>OEt</sub> cage. This allowed the identification of exclusion zones where gas accumulation is thermodynamically disfavoured (PMF > 0). Unbiased MD simulations were also conducted on a bulk system with the experimental Noria<sub>OEt</sub>-to-solvent mole ratio to capture the spontaneous distribution of gas molecules and identify any depletion zones. Gas concentrations were set according to the experimental solubility values. Additionally, a third set of simulations, performed in the absence of gas, examined solvent structuring around Noria<sub>OEt</sub> and the distribution of interstitial voids within and around the host. All simulations were carried out at 300 K under 1 bar or 5 bar pressures to assess the impact of hydrostatic pressure on gas exclusion.

Simulations at 1 bar reveal that gas molecules do indeed experience exclusion effects in the porous liquid, consistent with the observed experimental reduction in CO2 solubility described above. The PMF profiles for CO<sub>2</sub>, shown in Fig. 3a,

indicate three distinct regions around Noria<sub>OEt</sub>. As expected, within the host cavity ( $0 \le r < 0.45$  nm), CO<sub>2</sub> is strongly stabilised, with an inclusion energy of -7 kcal mol<sup>-1</sup>, explaining why the cavity remains occupied at all pressures considered (see SI, Fig. S14). Beyond r > 1.25 nm, the CO<sub>2</sub> molecules behave as in bulk solvent, where the host molecule has no influence. However, in the intermediate region (0.45  $\leq r \leq$  1.25 nm), a wide repulsive barrier of  $\sim 1$  kcal mol<sup>-1</sup> is observed, forming an exclusion zone where the positioning of gas molecules is thermodynamically disfavoured. This repulsion is further enhanced at higher pressures (5 bar).

Radial distribution functions (RDFs) calculated from unbiased MD (see SI, Fig. S15) confirm these findings: the system exhibits a fully occupied host cavity, a gas-depleted exclusion zone (g(r) < 1), and a solvent-dominated bulk region. This spatial organisation is illustrated in Fig. 3b, where CO2 molecules preferentially occupy the host cavity (blue) or disperse in the bulk (green), while the exclusion zone (red) remains sparsely populated. In terms of the geometry of the exclusion zone for CO<sub>2</sub> and its correspondence to the host shape and size, a radius of 0.45 nm captures the entirety of the host cavity and part of its opening. The outer shell, with a radius of 1.25 nm, encloses the entirety of the Noria<sub>OEt</sub> host, reaching beyond the methyl endings of its ethoxy groups.

The structural basis of the exclusion zone was further examined by analysing the distribution of voids in and around the host, including the interstitial voids in the space occupied by the solvent and the host cavity itself. To quantify this, we identified regions within the simulation cell where a hard sphere of radius R >0.1 nm could be inserted without overlapping with any atoms (see SI, Section S9 for details). The radial distribution function of these cavities,  $g_{cav}(r)$ , was then computed relative to the geometric centre of Noria<sub>OEt</sub>. The results reveal a clear depletion of voids within the same spatial range identified as the exclusion zone for CO2, indicating that the packing of solvent molecules around Noria<sub>OEt</sub> reduces the availability of accessible free volume, thereby restricting gas insertion. This is evident in Fig. 3c, where  $g_{cav}(r)$ shows a sharp peak at  $r \approx 0$  nm, corresponding to the intrinsic cavity of the host, while the surrounding region exhibits a marked reduction in void density ( $g_{cav}(r) < 1$ ) from 0.41 to 1.07 nm, aligning with the spatial extent of the exclusion zone. Incidentally, the maximum in the Noria<sub>OE</sub>-solvent RDF occurs at  $r \approx 1$  nm (SI Fig. S6), where the solvent density is greatest, reinforcing the correlation between solvent structuring and the lack of free space revealed by the void distribution. As might be expected, the largest depletion occurs at 0.5 nm ( $g_{cav}(r) \approx 0.2$ ), roughly the distance to the walls.  $g_{cav}(r)$  then ramps up to  $\approx 0.5$  at 1 nm. The upper limit of the depletion range has a closer match to the beginning of the asymptotic behaviour of the PMF for CO<sub>2</sub> at 1 bar (Fig. 3a), but that point is also a maximum in the PMF for CO2 at 5 bar. Thus, exclusion is not explained entirely by the steric hindrance from Noria<sub>OEt</sub>, and the interplay and competition between solvent molecules and gas molecules in the proximity to the cage must be considered as well. Effectively, within the Noria<sub>OEt</sub> solvation shell, the 15C5 molecules are more densely packed than in the bulk solvent, restricting the ability to solvate CO2 molecules in this region.

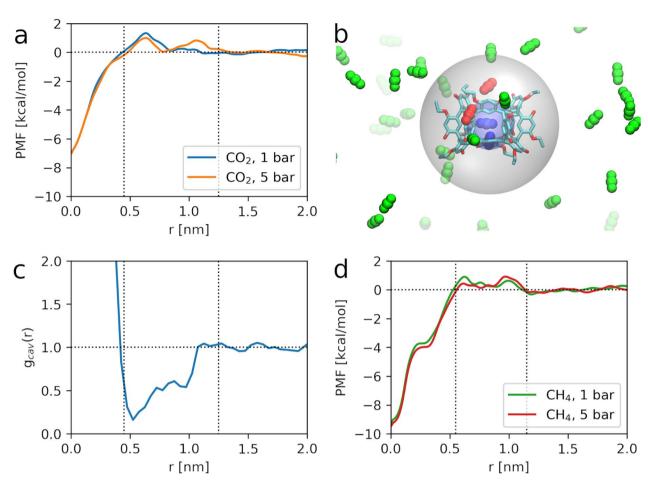


Fig. 3 (a and d) Free energy profiles, or PMF, for transferring a  $CO_2$  or  $CH_4$  molecule from bulk solvent to a radial distance r from a Noriao<sub>Et</sub> dissolved in 15C5. Three domains, illustrated with dotted lines, are observable from the energy differences relative to the bulk. (b) Snapshot of a simulation of the porous liquid loaded with  $CO_2$  at 5 bar. The translucent spheres illustrate the inner and outer shells defined from the first two domains in the free energy profiles of  $CO_2$ .  $CO_2$  molecules inside the inner shell and in the outer shell are depicted in blue and red respectively. (c) Radial distribution function of spherical cavities of radii larger than 0.1 nm relative to the centre of a single Noria<sub>OEt</sub> cage in 15C5 at 1 bar. Depletion of cavities occurs in a range that is mostly contained in the second domain of the  $CO_2$  free energy profile, deemed as an exclusion zone.

Finally, Fig. 3d shows the PMF for a single  $CH_4$  molecule at 1 bar and 5 bar.  $CH_4$  experiences a stronger stabilisation in the host cavity, with insertion free energies ranging from -9.2 to -9.4 kcal  $mol^{-1}$ . More importantly, the exclusion zone is both narrower  $(0.55 \le r \le 1.15 \text{ nm})$  and less repulsive than that of  $CO_2$ , suggesting that  $CH_4$  experiences weaker exclusion effects. While the qualitative features of the PMF are similar for both gases, the weaker exclusion for methane is consistent with its greater increase in experimental solubility in the porous liquid system relative to 15C5. It can also be noted that since the Henry constant for  $CH_4$  in 15C5 is ca. 10 times greater than that of  $CO_2$  (see above), *i.e.* 15C5 is a much poorer solvent for  $CH_4$  than for  $CO_2$ , the replacement of 15C5 solvent molecules by the bulk of the  $Noria_{OEt}$  structure has less of an effect on the overall  $CH_4$  solubility than it does on the  $CO_2$  solubility.

#### Cryptophane-based porous liquid

It follows from the above that the gas uptake of a PL can be maximised by minimising the volume of the exclusion zone. In order to test this hypothesis, Cryptophane-A was explored as a host for a T2PL (Fig. 4, left). Cryptophanes are a class of hosts based on two cyclotribenzylene (CTB) units connected by various linkers. They are potentially appropriate hosts for PLs. Collado *et al.* have computationally simulated Cryptophane-111 dissolved in  $CH_2Cl_2$  as a potential PL for encapsulation of  $CO_2$  and  $H_2$ , and for  $SO_2$  separation and storage.<sup>11,12</sup>

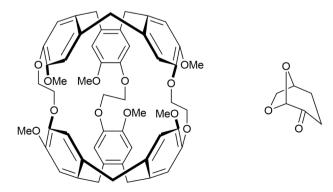


Fig. 4 Structures of Cryptophane-A (left) and Cyrene (right).

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Using a computational method described in the SI (S13), the van der Waals (vdW) and cavity volumes of Noria<sub>OEt</sub> and Cryptophane-A were estimated and compared. The structures used were the Noria<sub>OEt</sub> model that had been generated computationally in the above work and the crystal structure of the Cryptophane-A Xe inclusion complex published by Taratula et al.,13 with the Xe guest deleted. A Monte Carlo integration scheme was used to calculate the vdW volume of each molecule. For Noria<sub>OEt</sub>, the surface substituents were included in the calculation. Random points were uniformly sampled within a bounding box that enclosed the entire molecule, extended by 4 Å in each spatial direction to avoid truncating peripheral volume. For each point, we checked whether it fell within the van der Waals radius of any atom in the molecule. The vdW volume was then calculated as the fraction of points falling within any vdW sphere, multiplied by the volume of the bounding box. To compute the cavity volume, we first identified the atoms which define the inner cage of the host molecule and constructed the convex hull defined by their coordinates. We then used the same random point set to identify those points that were located within the convex hull but outside the vdW spheres of all atoms. The volume of the cavity was then estimated as the fraction of such points multiplied by the bounding box volume. This approach yields the internal volume that is geometrically enclosed by the cage but not occupied by any atom. These cavity volumes are illustrated in Fig. 5. Noria<sub>OEt</sub> was found to have a vdW volume of 1793 Å<sup>3</sup> with a cavity volume of 141  $\text{Å}^3$ . For Cryptophane-A, the vdW volume was 765  $\text{Å}^3$ , and the cavity volume was 124 Å<sup>3</sup>. This cavity volume is comparable to reported values, as discussed by El-Ayle and Holman.14 The ratio of cavity volume to vdW volume (here defined as  $\alpha$ ), for each host was calculated to be 7.8% and 15.8% for  $Noria_{OEt}$  and Cryptophane-A respectively. The greater  $\alpha$  value for Cryptophane-A in comparison with Noria<sub>OEt</sub>, combined with the similar cavity volumes of the two hosts, suggests that Cryptophane-A should have a smaller exclusion zone when used to form a PL. This in turn should lead to greater gas solubility than for Noria<sub>OEt</sub>@15C5.

Cryptophane-A was synthesised by the method described by Della-Negra et al.15 Prior to testing the host solubility in

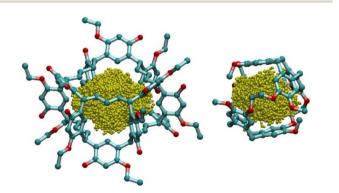


Fig. 5 A graphical illustration of cavity volumes of Noria<sub>OFt</sub> (left) and Cryptophane-A (right). Cavity volumes are illustrated by yellow spheres, each of which represents a sampling point in the simulation. The cavity volumes are similar whilst the total volume of Noria<sub>OFt</sub> is greater than that of Cryptophane-A.

candidate solvents, Cryptophane-A samples were dried under vacuum at 80 °C. Unfortunately, Cryptophane-A was found to be Therefore, we investigated insoluble in 15C5. hydrolevoglucosanone (Cyrene, Fig. 4, right) as an alternativesolvent. Cyrene is a biorenewable solvent with similar solubility parameters to polar aprotic solvents such as DMF and NMP, suggesting that it is capable of strong solvation. It also has a bulky, globular shape due to its bicyclic structure, suggesting that it should be excluded from pore windows of up to 7 Å. Also, Cyrene has no known toxicity issues and is produced from biomass. Compared to existing solvents for T2PLs, Cyrene is therefore attractive in terms of sustainability and safety. Due to its level of oxygenation, Cyrene was expected to have a similar gas uptake profile to 15C5. Cryptophane-A exhibited good solubility in Cyrene, which actually allowed for the preparation of more concentrated PLs than for Noria in 15C5. This would allow for a clearer evaluation of the effect of a potentially smaller exclusion zone. The resulting 48 mM solution is hereafter referred to as Cryptophane-A@Cyrene.

Since the solubility of gases in pure Cyrene has not previously been reported we first established this, using the same method as described above for Noria<sub>OEt</sub>@15C5.8 CH<sub>4</sub> solubility in Cyrene was found to be 0.006 mmol<sub>CH4</sub> per mL at 1 bar, increasing linearly (within error) up to 0.052  $\mathrm{mmol}_{\mathrm{CH_4}}$  per mL at 5 bar. CO<sub>2</sub> solubility was measured to be 0.12 mmol<sub>CO<sub>2</sub></sub> per mL at 1 bar, increasing linearly (within error) to 0.52 mmol<sub>CO</sub> per mL at 5 bar. The good CO<sub>2</sub>/CH<sub>4</sub> selectivity (17.8 at 1 bar; 10.0 at 5 bar) is as expected for an oxygenated solvent due the favourable interactions between Lewis acidic CO2 and the basic oxygen centres, as in commercial polyethylene glycol-diether solvents such as Genosorb for example.9 Using the above data, the Henry constants,  $H_s^{cp}$ , for  $CH_4$  and  $CO_2$  in Cyrene were calculated to be 11.8 imes 10<sup>-3</sup> mol per L per atm and 10.3 imes10<sup>-2</sup> mol per L per atm respectively. These values are similar to those for 15C5 (see above).

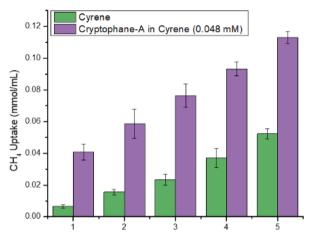
As expected, CH<sub>4</sub> was more soluble in the porous liquid Cryptophane-A@Cyrene (e.g. 0.04 mmol<sub>CH4</sub> per mL<sub>PL</sub> at 1 bar and 0.11 mmol<sub>CH</sub>, per mL<sub>PL</sub> at 5 bar, Fig. 6, left) than in pure Cyrene. The enhancement corresponds to ca. 0.7 molecules of CH<sub>4</sub> per molecule of Cryptophane-A at 1 bar, rising to 1.3 molecules at 5 bar. These average levels of occupancy are consistent with 1H-NMR studies conducted by Garel et al.16 on solid Cryptophane-A, which showed that one molecule of CH4 can readily be accommodated within the Cryptophane-A cavity, and potentially two at higher pressures.

<sup>1</sup>H-NMR spectroscopy confirmed that inclusion of CH<sub>4</sub> occurs within the cavities of the Cryptophane in the PL. CH4 was bubbled through Cyrene in an NMR tube containing a  $d^6$ acetone capillary. A <sup>1</sup>H-NMR spectrum showed the CH<sub>4</sub> peak at -0.73 ppm (Fig. 7). A similar experiment conducted using Cryptophane-A@Cyrene in place of neat Cyrene showed a CH<sub>4</sub> peak at -3.95 ppm. This clear upfield shift is consistent with that reported for the inclusion of CH<sub>4</sub> in Cryptophane-A by Collet et al.17 A similar experiment with C2H6 showed analogous behaviour (Fig. S10 and S11) with inclusion in the Cryptophane host causing an upfield shift from -0.02 ppm to -3.66 ppm.

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Pressure (bar)

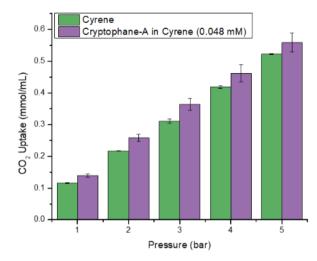


Fig. 6 (Left) CH<sub>4</sub> uptake of Cyrene and of Cryptophane-A in Cyrene from 1-5 bar at 298.15 K. (Right) CO<sub>2</sub> uptake of Cyrene and of Cryptophane-A in Cyrene from 1-5 bar at 298.15 K.

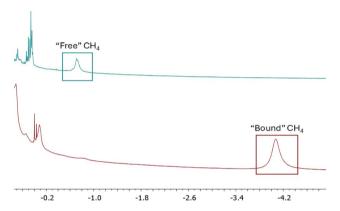


Fig. 7  $\,^{1}$ H-NMR spectra of Cyrene (top) and Cryptophane-A@Cyrene (bottom) after having CH<sub>4</sub> bubbled through the sample. The upfield shift of the CH<sub>4</sub> signal is characteristic of inclusion within a Cryptophane.

The  $CO_2$  solubility in Cryptophane-A@Cyrene was then measured to test the hypothesis that a smaller exclusion zone would increase  $CO_2$  solubility relative to neat Cyrene. Cryptophane-A@Cyrene did indeed exhibit an enhanced  $CO_2$  solubility, ranging from 0.14  $\text{mmol}_{CO_2}$  per  $g_{PL}$  at 1 bar to 0.55  $\text{mmol}_{CO_2}$  per  $g_{PL}$  at 5 bar. This increase in solubility compared to neat Cyrene corresponds to an apparent occupancy 0.5 at 1 bar. Interestingly, the apparent occupancy reaches a maximum of 1.1 at 3 bar before falling to 0.75 at 5 bar (as discussed further below). Overall, this range of occupancies is intuitively reasonable and similar to that seen for  $CH_4$ .

Finally, by analogy with Fig. 2c, it is interesting to plot for each gas the apparent occupancy of the Cryptophane-A hosts in the PL, specifically the difference between the gas's solubility in Cryptophane-A@Cyrene  $\nu s$ . pure Cyrene, expressed as a mole ratio of gas to Cryptophane-A in the PL (Fig. 8). As with Noria<sub>OEt</sub>@15C5 (Fig. 2c), the error bars which represent ESDs preclude comparisons between specific data points within each

series. However, with regard to overall trends, it is notable, firstly, that the behaviour of CH4 is similarly to that in Noria<sub>OEt</sub>@15C5, i.e. as pressure increases the PL becomes progressively a better solvent than Cyrene, with steadily increasing apparent occupancy of the host. However, the behaviour of CO<sub>2</sub> in this regard is different from that in Noria<sub>OEt</sub>@15C5. Specifically, at lower pressures Cryptophane-A@Cyrene becomes increasingly better as a solvent than Cyrene with increasing pressure. This trend is the opposite to that seen for Noria<sub>OEt</sub>@15C5 (Fig. 2c), and is consistent with the exclusion zone for Cryptophane-A being smaller than for Noria<sub>OEt</sub>. As mentioned above, the apparent occupancy for CO<sub>2</sub> increases with pressure up to a maximum at 3 bar, above which the trend reverses, reverting to that seen in Fig. 2c (i.e. the as pressure increases above 3 bar the apparent occupancy decreases as the PL performs comparatively less well compared to neat Cyrene). This latter behaviour reveals that although the exclusion zone is smaller for Cryptophane-A than for Noria<sub>OEt</sub>, it

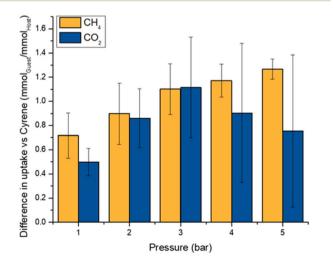


Fig. 8 Difference between the gas uptake of Cryptophane-A@Cyrene and Cyrene in terms of  $mmol_{Guest}$  per  $mmol_{Host}$ .

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is still present, although only observed at greater CO<sub>2</sub> pressures. This is intuitively reasonable since increasing the CO<sub>2</sub> pressure increases the amount of CO2 that would be dissolved in pure Cyrene, and therefore the effect of replacing Cyrene solvent molecules by the framework bulk of the Cryptophane (from which CO<sub>2</sub> molecules are sterically excluded) becomes more apparent at high pressure.

Overall, a key aspect is that the enhanced solubility of CO<sub>2</sub> in Cryptophane-A@Cyrene compared to that in neat Cyrene supports the hypothesis that by reducing the size of the exclusion zone in a porous liquid, the gas solubility in the porous liquid can be increased relative to the neat solvent.

# Conclusions

In summary, experimental gas solubility measurements show that, counterintuitively, CO2 solubility in Noria<sub>OEt</sub>@15C5 is equal or even reduced compared to that in its neat solvent, 15C5, despite the presence of empty pores. To our knowledge such behaviour has not previously been observed for a porous liquid. Simulations suggest that although the Noria<sub>OEt</sub> pore provides a strongly favourable site for enhanced gas binding, there exists a gas exclusion zone surrounding the pore, in which binding is disfavoured. The exclusion zone arises from two aspects, (i) steric exclusion of gas molecules from the region defined by the bulky host framework (i.e. replacement of solvent molecules by the bulk of the host) and (ii) solvent ordering in the solvation shell of the host. This latter aspect consists of a complex interplay between the distribution of interstitial voids around the host and intermolecular interactions involving the gas, solvent, and host. In the MD simulations conducted these latter interactions are inherently tied to the force-field model used. Although the force-field parameters yield gas insertion energies in the host cavity comparable to DFT calculations (see Section S5 of the SI), it can be borne in mind that small discrepancies in host-solvent-gas interactions may alter the delicate balance of forces governing gas exclusion. Given that the energy barriers associated with exclusion are relatively small, future implementations of the force-field may require fine-tuning to fully capture subtle solvation effects that distinguish CO2 from CH4 quantitatively. Nevertheless, within the accuracy of the current model, the simulations are qualitatively consistent with the experimental trends, correctly capturing the stronger exclusion effect for CO2 and the weaker, less pronounced effect for CH4.

It was also shown experimentally, that by using a porous host which is calculated to have a smaller exclusion zone than Noria<sub>OEt</sub> (Cryptophane-A), the effect of the exclusion zone can be reduced. Specifically, this was demonstrated Cryptophane-A@Cyrene, having increased CO2 solubility compared to its neat solvent. This latter material is also noteworthy in being the first reported porous liquid based on a Cryptophane host.

In related work, it is interesting to note that non-additive CO<sub>2</sub> uptake has recently been reported in which iminospherand-based Type 2 PLs demonstrated enhanced CO<sub>2</sub> uptake which is greater than the weighted sum of the uptakes

for the pure solvent and the porous host in its solid form. 18-21 In that case the discrepancy was ascribed to there being good binding sites for CO<sub>2</sub> molecules on the outer surface of the host which are not available for gas binding in the solid form of the host due to crystal packing. We also note that a study of gas uptake kinetics into Type III PLs has pointed to the significance of an adsorbed layer (i.e. solvation shell) around MOF particles dispersed in a carrier liquid in determining gas uptake kinetics.22 Taking these reference points together with the current work, it suggests that the interface between the solvent and the host in PLs can be important in determining overall behaviour (both kinetic and thermodynamic) with regard to the dissolution of gases. Greater elucidation of this region will be important in more fully understanding and exploiting gas uptake in PLs. Also, intriguingly, it suggests that in developing PLs toward high gas selectivity, there may be mechanisms to reduce, as well as increase, the solubility of a given gas.

### Author contributions

CFK conducted the synthetic and analytical work. Gas solubility measurements were carried out by CFK and EMFR. SFF, JLB, and MDdP conducted the MD simulations. KTH contributed to the ideation. SLJ obtained funding, contributed to ideation and supervised the project. The paper was drafted jointly by CFK, SLJ, MGdP, SFF, and JLB. All authors have given approval to the final version of the manuscript.

# Conflicts of interest

There are no conflicts to declare.

# Data availability

The supporting data of this manuscript are available in the supplementary information (SI). Supplementary information is available. See DOI: https://doi.org/10.1039/d5sc06588g.

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