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## Exploring the determination of the standard rate constant in electrochemical metal deposition: theory and experiment

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A detailed investigation of the electrochemical metal deposition was carried out using both simulation and experimental cyclic voltammetry (CV). Kinetic curves were developed to relate peak-to-peak potential separation ( $\Delta E_p$ ) to the cathodic charge transfer coefficient ( $\alpha$ ) and the standard rate constant ( $k^0$ ). From these curves, interpolation equations were derived to estimate  $k^0$ , taking into account the effect of the transfer coefficients sum ( $\alpha + \beta$ ), whether equals to or different from 1. The validity of the equations was confirmed through the reduction of silver, copper and rhenium ions in various electrolytes, yielding  $k^0$  values of  $14.51 \times 10^{-6} \text{ m s}^{-1}$  for  $\text{Ag}^+/\text{Ag}$ ,  $5.98 \times 10^{-7} \text{ m s}^{-1}$  for  $\text{Cu}^+/\text{Cu}$  and  $10.59 \times 10^{-8} \text{ m s}^{-1}$  for  $\text{Re}^{6+}/\text{Re}$ . According to the Matsuda–Ayabe criteria for assessing electron-transfer reversibility, the  $\text{Ag}^+/\text{Ag}$  and  $\text{Cu}^+/\text{Cu}$  redox couples are regarded as quasi-reversible, while the  $\text{Re}^{6+}/\text{Re}$  couple is classified as irreversible. The simulated CVs showed strong agreement with experimental results.

## 1. Introduction

Voltammetric techniques play a crucial role in assessing both the thermodynamic and kinetic aspects of redox processes. Among the different voltammetric methods, cyclic voltammetry is the most frequently used.<sup>1–3</sup>

Linear sweep voltammetry (LSV) and cyclic voltammetry (CV) simulations have attracted significant attention from researchers.<sup>3–24</sup> By developing accurate mathematical models and gaining deep insights into the underlying mechanisms,

scientists strive to unravel the complexity of CV responses. The simulation of CV for electrochemical metal deposition was first studied by Berzins and Delahay<sup>10</sup> for a reversible system, followed by numerous other researchers.<sup>11–13</sup> Delahay<sup>14</sup> also conducted studies on irreversible systems. Different works on quasi-reversible systems have been carried out by Atek,<sup>15</sup> and other investigators.<sup>18,25–28</sup> Additionally, studies from Saila, Affoune, Avaca and Kanzaki<sup>16,17,29,30</sup> have explored the electro-oxidation of insoluble species.

The standard heterogeneous electron transfer rate constant ( $k^0$ ) is a crucial electrochemical parameter, as it provides direct insight into the kinetics of redox reactions.<sup>21,31–34</sup> Standard rate constant determination is a fundamental scientific concept with significant cross-disciplinary implications, as it provides quantitative insights into reaction mechanisms and speeds across various fields like electrocatalysis, materials science, energy storage and biology.<sup>35–48</sup> In electrocatalysis, it is used to characterize the activity and efficiency of electrocatalysts for various reactions.<sup>35–37</sup> In materials science, it aids in understanding the behavior and stability of materials and devices like batteries, electroplatings and sensors.<sup>38–46</sup> In biology, standard rate constants are crucial for quantifying protein-ligand interactions and enzyme kinetics, helping to understand biological processes like signaling, drug discovery, and the mechanisms of genetic and biochemical reaction.<sup>47,48</sup>

In contrast to soluble–soluble redox couples, for which the standard rate constant ( $k^0$ ) has been extensively investigated through linear sweep voltammetry (LSV)<sup>6,8</sup> and cyclic voltammetry

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studies,<sup>7,49–51</sup> the case of soluble–insoluble couples has received far less attention, with only a very few studies examining the determination of  $k^0$  using voltammetric techniques. Atek<sup>15</sup> presented kinetic diagrams as well as their interpolation equations to determine the kinetic rate constant through the development of interpolation equations based on peak current, half-peak width and peak potential kinetic curves, building on the approach initially introduced by Krulic,<sup>26</sup> where the sum of the cathodic ( $\alpha$ ) and anodic ( $\beta$ ) charge transfer coefficients equals 1.

As far as we are aware, the standard rate constant for electrochemical metal deposition has not been investigated based on cyclic voltammetry whatever the sum ( $\alpha + \beta$ ) across an extended ranges of  $\Delta E_p$  and charge transfer coefficient ( $\alpha$ ). This work investigates how the charge transfer coefficients  $\alpha$ ,  $\beta$ , and their sum ( $\alpha + \beta$ ) affect cyclic voltammetry, particularly the peak-to-peak potential separation ( $\Delta E_p$ ) and the accurate determination of the standard rate constant  $k^0$ . Kinetic curves and interpolation equations were developed to express  $\Delta E_p$  as a function of the dimensionless rate constant ( $\omega$ ) and charge transfer parameters. The influence of  $\alpha + \beta$  on  $k^0$  estimation was analyzed and corrected. Experimental validation was carried out, and findings enable reliable  $k^0$  determination for electro-deposition reactions using cyclic voltammetry peak separation.

## 2. Results and discussion

### 2.1. Metal deposition cyclic voltammograms characteristics

Fig. 1 presents theoretical cyclic voltammograms for electrodeposition reaction, illustrating both the effect of the dimensionless rate constant ( $\omega$ ) and the cathodic charge transfer coefficient ( $\alpha$ ).

The relationship between  $\omega$  and  $k^0$  ( $\omega = k^0 / \theta^\alpha \sqrt{n\pi FvD_{M^{n+}}/RT}$ ) is provided in the SI (S14). Simulations were performed using the following parameters:  $n = 1$ ,  $T = 298.15$  K,  $v = 0.1$  V s $^{-1}$ ,  $C_{\text{Ox}}^* = 1$  mM,  $A = 1$  cm $^2$ ,  $D = 1 \times 10^{-9}$  m $^2$  s $^{-1}$ .

Fig. 1a–c shows that the cathodic peaks of electrochemical metal deposition exhibit an asymmetric convex shape, while the anodic peaks appear sharp and narrow, accompanied by a steep current drop immediately after the peak, and does not exhibit a diffusion-controlled phase. The increase in anodic current is exclusively governed by charge transfer. The rapid current drop indicates the complete oxidation of deposit formed during the forward scan. The separation between the anodic and cathodic peak potentials ( $\Delta E_p$ ) increases with increasing irreversibility; *i.e.* with decreasing rate constant  $\omega$ , and a lower cathodic charge transfer coefficient ( $\alpha$ ).

### 2.2. Electrochemical standard heterogeneous rate constant ( $k^0$ ) determination: case where $\alpha + \beta = 1$

First, we studied how the switching potential ( $E_\lambda$ ) influences the peak-to-peak potential separation ( $\Delta E_p$ ), (see SI). After that, we investigate the combined effect of cathodic charge transfer coefficient and dimensionless rate constant on  $\Delta E_p$ .

Since the sum of the cathodic and anodic transfer coefficients ( $\alpha + \beta$ ) directly affects peak positions and, by extension, the peak-to-peak potential separation ( $\Delta E_p$ ), its impact is examined in depth in this study. Distinct analyses are conducted for systems where  $\alpha + \beta = 1$  and those where this condition is not satisfied, highlighting the differences in electrochemical behavior under each scenario.

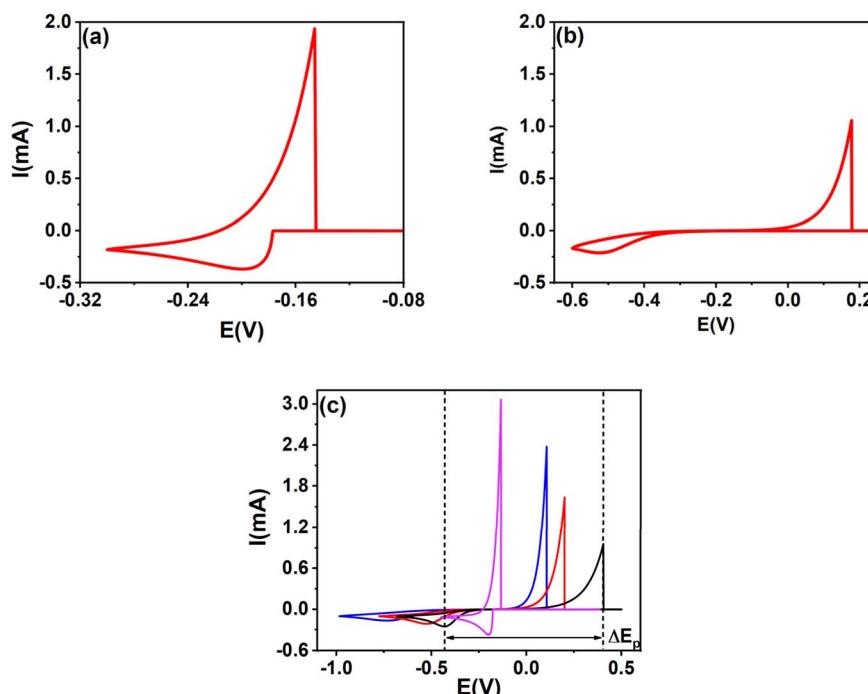


Fig. 1 The effect of  $\omega = 10^3$  (a),  $\omega = 10^{-3}$  (b), and  $\alpha$  (c) on soluble–insoluble CVs:  $\alpha = 0.7$  (black),  $\alpha = 0.5$  (red),  $\alpha = 0.3$  (blue) for  $\omega = 10^{-3}$  and  $\alpha = 0.5$  (magenta) for  $\omega = 10^3$ .



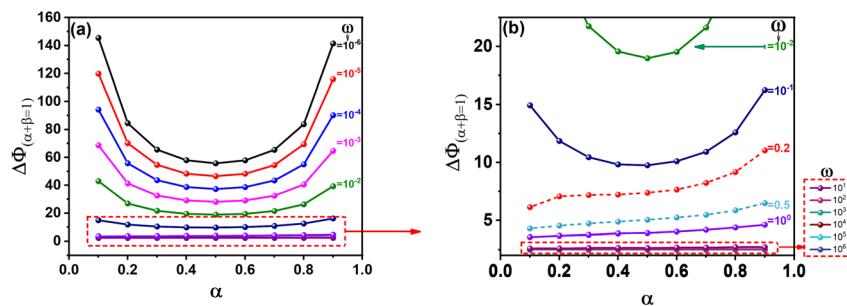


Fig. 2 Kinetic curves presenting the effect of the charge transfer coefficient ( $\alpha$ ) and the kinetic rate constant ( $\omega$ ) on the peak-to-peak potential separation ( $\Delta\Phi$ ): (a)  $10^{-6} \leq \omega \leq 10^6$ , (b)  $\omega \geq 10^{-2}$ .

The relationship between peak-to-peak potential separations ( $\Delta E_p$ ) and dimensionless peak-to-peak potential separations ( $\Delta\Phi$ ) is expressed as follows:

$$\Delta\Phi = \left( \frac{nF}{RT} \right) \times \Delta E_p \quad (1)$$

In this study, we investigate a broader range of the dimensionless kinetic rate constant ( $\omega$ ), spanning from  $10^{-6}$  to  $10^6$ , along with cathodic charge transfer coefficient ( $\alpha$ ) values varying between 0.1 and 0.9.

Fig. 2 shows kinetic curves for electrochemical metal deposition redox systems, where the dimensionless peak-to-peak potential separation ( $\Delta\Phi$ ) is plotted as a function of the logarithm of the dimensionless rate constant ( $\log \omega$ ) and the cathodic charge transfer coefficient ( $\alpha$ ). For a known value of  $\omega$ , simulated voltammograms are established for nine values of  $\alpha = [0.1-0.9]$ . From the file data of each voltammogram, the dimensionless peak-to-peak potential separation ( $\Delta\Phi$ ) is deduced. After that, the same procedure is repeated for another value of  $\omega = (10^{-6}, 10^{-5}, \dots, 10^6)$ .

Throughout this work,  $\Delta\Phi_{(\alpha+\beta=1)}$  will refer to the peak separation under the condition  $\alpha + \beta = 1$ . The dimensionless rate constant ( $\omega$ ) for metal electrodeposition reactions depends on the initial concentration of the oxidized species as indicated in eqn (S14). The diagrams presented in Fig. 2a and b were calculated with the concentration  $C_{\text{Ox}}^* = 1 \text{ mM}$ . However, these diagrams remain valid for any concentration, because the concentration affects only the current and has no influence on the peak potential.

In the range  $\omega = 10^{-6}$  to  $10^{-1}$ , Fig. 2a reveals a convex and symmetrical profile, centered around  $\alpha = 0.5$ . In contrast, Fig. 2b shows that as  $\omega$  increases beyond  $10^{-1}$ , the curves become increasingly asymmetric and flatten in shape. When the values of  $\alpha$  and  $\Delta E_p$  are known, the kinetic curves provided above allow for the determination of the dimensionless rate constant  $\omega$ . Once  $\omega$  is obtained, the standard rate constant  $k^0$  can then be calculated using eqn (S14).

As noted earlier, the symmetry of the kinetic curves for  $\omega \leq 10^{-1}$  supports the use of interpolation. Data fitting was performed using the rational Holliday equation:

$$y = \frac{1}{a + bx + cx^2} \quad (2)$$

where  $y$  represents  $\Delta\Phi$  and  $x$  represents  $\alpha$ .  $a$ ,  $b$  and  $c$  are functions of  $\log(\omega)$ .

The following equation was derived within these parameter ranges:

$$-6 \leq \log(\omega) \leq -1, 10 \leq \Delta\Phi \leq 150$$

$$\Delta\Phi_{(\alpha+\beta=1)} = \frac{1}{a_1 + b_1\alpha + c_1\alpha^2}; R^2 = 0.9999 \quad (3)$$

where:

$$a_1 = 0.0012 + 0.352 \exp((- \log(\omega))/-0.4862); R^2 = 0.9930 \quad (4)$$

$$b_1 = 0.3045 \exp(0.2641 \log(\omega)); R^2 = 0.9930 \quad (5)$$

$$c_1 = -0.3136 \exp(0.27414 \log(\omega)); R^2 = 0.9930 \quad (6)$$

When  $\alpha + \beta = 1$  and  $\omega$  is in the range  $\omega \leq 10^{-1}$ ,  $\omega$  can be accurately extracted using either the interpolation eqn (3) or the corresponding kinetic curves shown in Fig. 2. In contrast, for  $\omega$  values exceeding  $10^{-1}$ , the irregular and flattened nature of the curves prevents reliable interpolation. Nonetheless, as depicted in Fig. 2b, the impact of  $\alpha$  on  $\Delta E_p$  becomes negligible in this higher  $\omega$  range. As a result, approximate values of  $\omega$  can still be inferred from the detailed view of the kinetic curves in Fig. 2b.

### 2.3. Electrochemical standard heterogeneous rate constant ( $k^0$ ) determination: case where $\alpha + \beta \neq 1$

The electrochemical literature acknowledges that the sum of the charge transfer coefficients ( $\alpha + \beta$ ) can differ from one, either being less than or greater than unity.<sup>52-60</sup> Chen<sup>54</sup> explained that in Butler–Volmer theory, the assumption that  $\alpha + \beta = 1$  is derived from the concept of microscopic reversibility. However, this condition is only valid at the equilibrium potential. In systems that are quasi-reversible, this assumption does not hold. The Marcus–Hush theory, especially in its asymmetric form, provides an explanation for these discrepancies, relating them to the differing vibrational force constants of the redox species. Additionally, Henstridge<sup>55</sup> observed that, due to the large peak-to-peak separation, the condition  $\alpha + \beta = 1$  can be relaxed without violating the principle of microscopic reversibility. This is because the oxidation and reduction



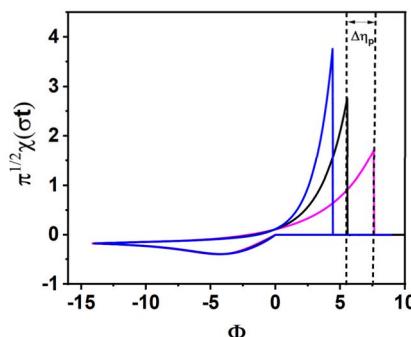


Fig. 3 Presentation of dimensionless soluble–insoluble CVs for  $\omega = 10^{-1}$ ,  $\alpha = 0.5$  and  $\beta = 0.3, 0.5, 0.7$ .

reactions take place at widely differing potentials, placing them in distinct environmental conditions. Suwatchara<sup>52</sup> showed that enforcing the condition  $\alpha + \beta = 1$  led to a poor description of the experimental CVs for the one-electron reduction of 2-nitropropane, while relaxing this constraint ( $\alpha + \beta \neq 1$ ) provided an excellent fit. Different literature studies also<sup>56–60</sup> reported experimental systems where  $\alpha + \beta \neq 1$ . To our knowledge, no theoretical investigations have examined the influence of  $\alpha + \beta \neq 1$  on cyclic voltammetry for metal electrodeposition. To address this gap, Fig. 3 demonstrates how variations in  $\alpha + \beta$  affect the anodic peak. In this analysis,  $\alpha$  is held constant at 0.5, while  $\beta$  takes values of 0.3, 0.5, and 0.7. The resulting deviation in the dimensionless anodic peak potential, observed when  $\alpha + \beta \neq 1$  compared to the reference case of  $\alpha + \beta = 1$ , is defined as  $\Delta\eta_p$ .

$$\Delta\eta_p = \eta_{p_a(\alpha+\beta \neq 1)} - \eta_{p_a(\alpha+\beta=1)} \quad (7)$$

$$\eta_{p_a} = \frac{nF}{RT} (E_{p_a} - E^0) \quad (8)$$

It is observed that the below eqn (9), used to evaluate the dimensionless peak-to-peak potential separation,  $\Delta\Phi_{(\alpha+\beta \neq 1)}$ , provides a better fit when the sum of the transfer coefficients deviates from unity. This parameter,  $\Delta\Phi_{(\alpha+\beta \neq 1)}$ , can be extracted from experimental cyclic voltammograms using eqn (1).

$$\Delta\Phi_{(\alpha+\beta \neq 1)} = \Delta\Phi_{(\alpha+\beta=1)} + \Delta\eta_p \quad (9)$$

$\Delta\eta_p$  depends on  $\alpha$ ,  $\beta$  and  $\omega$ . In order to avoid interpolation equations excessively long, we define the following two types of  $\Delta\eta_p$ :

$$\Delta\eta_{p_1}; \Delta\eta_p \text{ when } -3 \leq \log(\omega) \leq -1$$

$$\Delta\eta_{p_2}; \Delta\eta_p \text{ when } \log(\omega) \leq -3$$

When analyzing a voltammogram characterized by specific values of  $\alpha$ ,  $\beta$ , and  $\Delta\Phi_{(\alpha+\beta \neq 1)}$ , an approximate estimation of the corresponding  $\omega$  range can be made using the theoretical reference tools: the kinetic diagrams in Fig. 4 or the validation data provided in Table S1 (see SI). Once a given  $\Delta\eta_{p_1}$ , or  $\Delta\eta_{p_2}$  is identified, its association with eqn (3) allows for the formulation of a new interpolation expression for the dimensionless peak-to-peak potential difference under conditions where  $\alpha + \beta \neq 1$ . Although interpolation equations cannot be derived

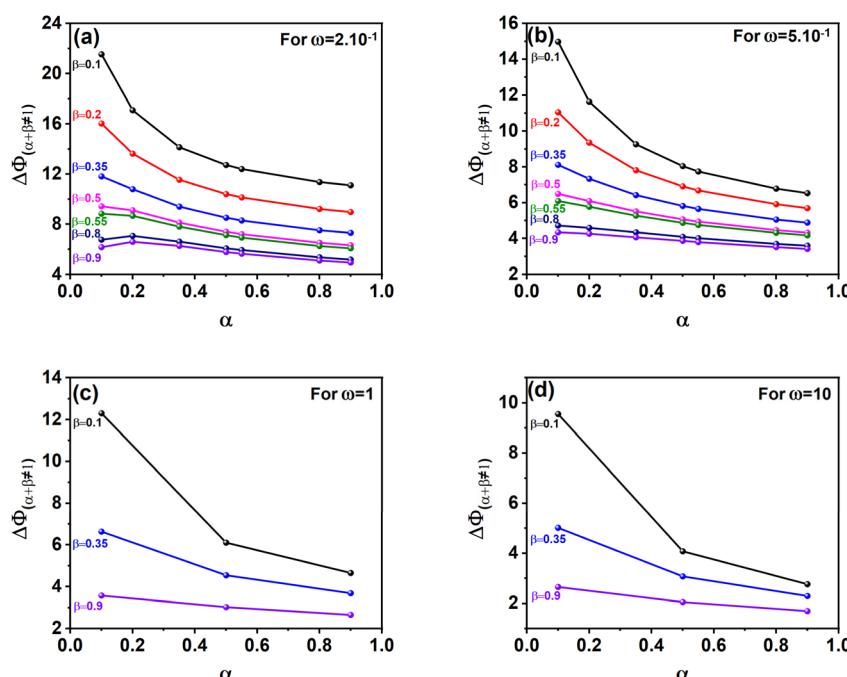


Fig. 4 Kinetic curves presenting the effect of  $\alpha$  and  $\beta$  (where  $\alpha + \beta \neq 1$ ) and the kinetic rate constant  $\omega$ , on the peak-to-peak potential separation ( $\Delta\Phi$ ) for: (a)  $\Delta\Phi_{(\alpha+\beta \neq 1)}$  for  $\omega = 2 \times 10^{-1}$ , (b)  $\Delta\Phi_{(\alpha+\beta \neq 1)}$  for  $\omega = 5 \times 10^{-1}$ , (c)  $\Delta\Phi_{(\alpha+\beta \neq 1)}$  for  $\omega = 1$ , (d)  $\Delta\Phi_{(\alpha+\beta \neq 1)}$  for  $\omega = 10$ .

when  $\log(\omega) > -1$ , it remains possible to construct new kinetic curves within this range.

Here below we present the development of equations permitting the calculation of the dimensionless standard heterogeneous rate constant for two different ranges:

**2.3.1. Interpolation equation for the dimensionless standard rate constant ( $\omega$ ):**  $-3 \leq \log(\omega) \leq -1$ . In the range of  $-3 \leq \log(\omega) \leq -1$ , we obtained by interpolation the following eqn (10) for  $\Delta\eta_{p_1}$ .

$$\Delta\eta_{p_1} = (a + b\alpha + c\alpha^2) + (a_1 + b_1\alpha + c_1\alpha^2) \times \exp((a_2 + b_2\alpha + c_2\alpha^2) \times \beta) \quad (10)$$

where:

$$a = 0.27594 + 1.43996 \log \omega - 0.01107 \log \omega^2 \quad (11)$$

$$b = -5.28228 - 9.8649 \log \omega + 0.04393 \log \omega^2 \quad (12)$$

$$c = 7.30133 + 19.49543 \log \omega - 0.31554 \log \omega^2 \quad (13)$$

$$a_1 = -58.60695 - 88.52844 \log \omega - 12.87437 \log \omega^2 \quad (14)$$

$$b_1 = 155.89195 + 214.46174 \log \omega + 53.23083 \log \omega^2 \quad (15)$$

$$c_1 = -128.3385 - 175.8604 \log \omega - 43.75774 \log \omega^2 \quad (16)$$

$$a_2 = -0.70606 + 4.20589 \log \omega + 0.80246 \log \omega^2 \quad (17)$$

$$b_2 = -5.06505 - 5.5916 \log \omega - 1.31285 \log \omega^2 \quad (18)$$

$$c_2 = 4.59224 + 4.88175 \log \omega + 1.12871 \log \omega^2 \quad (19)$$

$$R^2 = 0.9981$$

$\log(\omega)$  can be determined by substituting eqn (10) and (3) into eqn (9). This latter becomes:

$$\Delta\Phi_{(\alpha+\beta \neq 1)} = \Delta\Phi_{(\alpha+\beta=1)} + \Delta\eta_{p_1} \quad (20)$$

Although eqn (20) is lengthy and appears complex, it provides satisfactory results for the calculation of  $k^0$ , in the range of  $-3 \leq \log(\omega) \leq -1$ , as demonstrated in both Theoretical and Experimental Validation Sections. Furthermore, in the experimental section, we found that eqn (34), which is simpler than eqn (20), also remains valid within an acceptable margin of error. Eqn (34) will be defined in the following section.

**2.3.2. Interpolation equation for the dimensionless standard rate constant ( $\omega$ ):**  $\log(\omega) \leq -3$ . In the case of an irreversible system, we developed hereinafter the eqn (33) which permitted the calculation of  $\Delta\eta_{p_2}$  when  $\log(\omega) \leq -3$ .

Fig. 3 shows typical electrochemical metal deposition voltammograms with same  $\alpha$  and different  $\beta$ . Let consider  $\Delta\eta_p$  between two curves. The first curve when  $\beta = \beta_1 = 1 - \alpha$ , and the second one when  $\beta = \beta_2 \neq 1 - \alpha$  considered as the real experimental value.

$$\Delta\eta_{p_2} = \eta_{p_2} - \eta_{p_1} = \left( \frac{nF}{RT} \right) (E_2 - E_1) = v(t_2 - t_1) \left( \frac{nF}{RT} \right) \quad (21)$$

Once  $t_1$  (the anodic peak time of the curve when  $\alpha + \beta = 1$ ) is determined,  $\Delta\eta_{p_2}$  can be calculated.

To determine  $t_1$  we proceeded as follows:

Given that the anodic electrical charges for the voltammograms are the same:

$$Qa_1 = Qa_2 \quad (22)$$

Hence:

$$\int_0^{t_1} i_1 dt = \int_0^{t_2} i_2 dt \quad (23)$$

where:

$$i_1 = nFk^0 \exp \left[ \frac{\beta_1 nF}{RT} (E - E^0) \right] \quad (24)$$

$$i_2 = nFk^0 \exp \left[ \frac{\beta_2 nF}{RT} (E - E^0) \right] \quad (25)$$

Since  $E = vt$

$$\int_0^{t_1} nFk^0 \exp \left[ \frac{\beta_1 nF}{RT} (vt - E^0) \right] dt = \int_0^{t_2} nFk^0 \exp \left[ \frac{\beta_2 nF}{RT} (vt - E^0) \right] dt \quad (26)$$

$$\int_0^{t_1} \exp \left[ \frac{\beta_1 nF}{RT} (vt - E^0) \right] dt = \int_0^{t_2} \exp \left[ \frac{\beta_2 nF}{RT} (vt - E^0) \right] dt \quad (27)$$

$$\left[ \frac{1}{\exp(E^0)} \times \frac{\exp \left( \frac{\beta_1 nFvt}{RT} \right)}{\frac{\beta_1 nF}{RT} v} \right]_0^{t_1} = \left[ \frac{1}{\exp(E^0)} \times \frac{\exp \left( \frac{\beta_2 nFvt}{RT} \right)}{\frac{\beta_2 nF}{RT} v} \right]_0^{t_2} \quad (28)$$

$$\left[ \frac{\exp \left( \frac{\beta_1 nFvt}{RT} \right)}{\beta_1} \right]_0^{t_1} = \left[ \frac{\exp \left( \frac{\beta_2 nFvt}{RT} \right)}{\beta_2} \right]_0^{t_2} \quad (29)$$

$$\frac{\exp \left( \beta_1 \frac{nF}{RT} vt_1 \right)}{\beta_1} - \frac{1}{\beta_1} = \frac{\exp \left( \beta_2 \frac{nF}{RT} vt_2 \right)}{\beta_2} - \frac{1}{\beta_2} \quad (30)$$

$$\exp \left( \frac{\beta_1 nF}{RT} vt_1 \right) - 1 = \beta_1 \frac{\exp \left( \beta_2 \frac{nF}{RT} vt_2 \right) - 1}{\beta_2} \quad (31)$$

$$t_1 = \frac{RT}{\beta_1 nFv} \ln \left( \frac{\beta_1 \exp \left( \beta_2 \frac{nF}{RT} vt_2 \right) - 1}{\beta_2} + 1 \right) \quad (32)$$

By replacing the eqn (32) in (21)



We obtain

$$\Delta\eta_{p_2} = v \left( t_2 - \left[ \frac{RT}{\beta_1 nFv} \ln \left( \frac{\beta_1 \exp \left( \beta_2 \frac{nF}{RT} vt_2 \right) - 1}{\beta_2} + 1 \right) \right] \right) \frac{nF}{RT} \quad (33)$$

By determining  $\alpha$  and  $\beta_2$  using Tafel plots, we can determine  $\beta_1 = 1 - \alpha$ . The parameter  $t_2$  represents the anodic peak time of the experimental curve. We can then calculate  $\Delta\eta_{p_2}$  using eqn (33). Finally, by substituting eqn (33) and (3) into eqn (9). This latter becomes:

$$\Delta\Phi_{(\alpha+\beta \neq 1)} = \Delta\Phi_{(\alpha+\beta=1)} + \Delta\eta_{p_2} \quad (34)$$

**2.3.3. Kinetic curves for  $\alpha + \beta \neq 1$  and when  $\log(\omega) > -1$ .** As shown in Fig. 4, kinetic curves were generated for four representative values of  $\log(\omega) > -1$ . In this context, Fig. 4a–d provide practical reference curves for estimating  $\omega$  values of  $2 \times 10^{-1}$ ,  $5 \times 10^{-1}$ , 1, and 10, respectively. In this range, calculations are based exclusively on kinetic curves, as no interpolation equations have been developed. This reliance on direct curve analysis becomes even more critical when  $\alpha + \beta \neq 1$ , since each unique combination of  $\alpha$  and  $\beta$  demands a specific kinetic curve for a given  $\log(\omega)$ . As a result, the number of required curves becomes practically unlimited.

When  $\Delta\Phi$  is less than 25, the diagrams above can be used to estimate the dimensionless kinetic parameter ( $\omega$ ), provided that the values of  $\alpha$ ,  $\beta$ , and  $\Delta E_p$  are known.

#### 2.4. Theoretical validation of interpolation equations

Using MATLAB, we carried out a large set of simulations to test the validity of our interpolation equations across a broad range of electrochemical parameters. For each simulated cyclic voltammogram, values of  $\alpha$ ,  $\beta$ , and  $\omega$  were varied. The peak-to-peak separation ( $\Delta E_p$ ) was first extracted, then used to calculate a new estimated dimensionless kinetic parameter (denoted as  $\omega'$ ) via our interpolation equations. These calculated values were compared with the original input  $\omega$ , and the results are compiled in Table S1. The MATLAB code used for these computations is included in the SI. Minor deviations between  $\omega$  and  $\omega'$  values are attributed to approximation errors introduced during numerical computation.

The results in Table S1 show that the interpolation equations perform well across a wide range of  $\omega$ ,  $\alpha$ , and  $\beta$  values, for both  $\alpha + \beta = 1$  and  $\alpha + \beta \neq 1$  conditions. The accuracy of  $k^0$  estimation is highly sensitive to the value of  $\alpha + \beta$ ; assuming  $\alpha = \beta = 0.5$  or  $\alpha + \beta = 1$  without verification may lead to notable errors, particularly in irreversible systems.

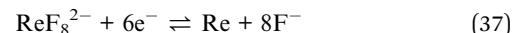
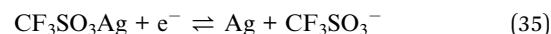
For extreme values of  $\alpha$ ,  $\beta$  ( $<0.2$  or  $>0.8$ ), or when  $\alpha + \beta$  is outside the typical range ( $<0.3$  or  $>1.2$ ), kinetic diagrams become less reliable. In such cases, interpolation equations offer more consistent results.

This work provides one of the most comprehensive validations of how  $\alpha$ ,  $\beta$ , and  $\alpha + \beta$  affect  $\Delta E_p$  and the accurate determination of  $k^0$  in metal electrodeposition reactions.

#### 2.5. Experimental validation for silver, copper and rhenium ions reductions

The experimental cyclic voltammogram presented in Fig. S2 corresponds to the reduction of silver ions at a gold electrode, performed in  $\text{HClO}_4$  electrolyte with a scan rate of  $50 \text{ mV s}^{-1}$ , the Fig. S3 corresponds to the reduction of copper ions at a platinum electrode in  $\text{TEABF}_4$  electrolyte at  $100 \text{ mV s}^{-1}$ , while Fig. S4 represents the reduction of rhenium hexafluoride  $\text{ReF}_6$  at a vitreous carbon wire in  $\text{LiF-NaF-KF}$  eutectic mixture at a scan rate of  $50 \text{ mV s}^{-1}$ . A sharp drop in the anodic peak is observed in all voltammograms, which is a characteristic feature of a metal electrodeposition reaction.

The reactions of these soluble–insoluble redox systems are as follows:



To determine  $k^0$ , the anodic and cathodic charge transfer coefficients, along with the diffusion coefficient, are required (refer to the SI). For silver ions, Tafel analysis and the semi-integration method (see Fig. S2) yielded  $\alpha = 0.302$ ,  $\beta = 0.514$ , and  $D = 5.56 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ . For copper ions (see Fig. S3), the corresponding values were  $\alpha = 0.727$ ,  $\beta = 0.460$ , and  $D = 2.58 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ . For rhenium ions (see Fig. S4), the corresponding values were  $\alpha = 0.130$ ,  $\beta = 0.110$ , and  $D = 8 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ . The calculation of  $k^0$  is performed using both the kinetic diagrams and the interpolation equations developed in this work.

Based on the experimental data, the peak-to-peak separation ( $\Delta E_p$ ) for silver ions, as shown in Fig. S2, is  $0.12 \text{ V}$ , calculated from  $\Delta E_p = E_{\text{pa}} - E_{\text{pc}} = 0.07 - (-0.05)$ . For copper ions, as shown in Fig. S3, is  $0.23 \text{ V}$ , calculated from  $\Delta E_p = E_{\text{pa}} - E_{\text{pc}} = 0.08 - (-0.16)$ . In comparison, the rhenium ions cyclic voltammogram in Fig. S4 gives a  $\Delta E_p$  of  $1.17 \text{ V}$ , determined as  $\Delta E_p = E_{\text{pa}} - E_{\text{pc}} = 3.43 - 2.26$ . Using eqn (1), these values yield the dimensionless peak-to-peak potential separations:  $\Delta\Phi_1$  for silver,  $\Delta\Phi_2$  for copper and  $\Delta\Phi_3$  for rhenium:

$$\Delta\Phi_1 = \left( \frac{nF}{RT} \right) \Delta E_p = 38.924 \times 0.12 = 4.54 \quad (38)$$

$$\Delta\Phi_2 = \left( \frac{nF}{RT} \right) \Delta E_p = 38.924 \times 0.23 = 9.01 \quad (39)$$

$$\Delta\Phi_3 = \left( \frac{nF}{RT} \right) \Delta E_p = 79.747 \times 1.17 = 93.54 \quad (40)$$

Standard heterogeneous rate constant ( $k^0$ ) values for the reduction of silver ions, copper ions as well as of rhenium ions, obtained from different kinetic curves and calculated from different equations are obtained in Tables 1–3, respectively.

For silver ions, the dimensionless kinetic parameter  $\omega$  can be estimated using two different approaches. When assuming  $\alpha + \beta = 1$ , the value is derived from the kinetic diagram in Fig. 2b



**Table 1** Dimensionless rate constant ( $\omega$ ) and standard heterogeneous rate constants ( $k^0$ ) values for the reduction of silver ions

Calculation methods of $k^0$	$\omega$	$k^0, 10^{-6} \text{ m s}^{-1}$
Kinetic curves where $\alpha + \beta = 1$ (Fig. 2)	$\approx 0.81$	$\approx 11.75$
Kinetic curves where $\alpha + \beta \neq 1$ (Fig. 4)	$\approx 1$	$\approx 14.51$

**Table 2** Dimensionless rate constant ( $\omega$ ) and standard heterogeneous rate constants ( $k^0$ ) values for the reduction of copper ions

Calculation methods of $k^0$	$\omega, 10^{-2}$	$k^0, 10^{-7} \text{ m s}^{-1}$
Kinetic curves where $\alpha + \beta \neq 1$ (Fig. 4)	$\approx 20$	$\approx 12.49$
Interpolation equation where $\alpha + \beta = 1$ (3)	14.42	9.0
Interpolation equation where $\alpha + \beta \neq 1$ (20)	9.58	5.98
Interpolation equation where $\alpha + \beta \neq 1$ (34)	8.54	5.33

**Table 3** Dimensionless rate constant ( $\omega$ ) standard heterogeneous rate constant ( $k^0$ ) values for the reduction of rhenium ions

Calculation methods of $k^0$	$\omega, 10^{-4}$	$k^0, 10^{-8} \text{ m s}^{-1}$
Kinetic curves where $\alpha + \beta = 1$ (Fig. 2)	$\approx 0.46$	$\approx 0.29$
Interpolation equation where $\alpha + \beta = 1$ (3)	0.13	0.08
Interpolation equation where $\alpha + \beta \neq 1$ (20)	17	10.59
Interpolation equation where $\alpha + \beta \neq 1$ (34)	42	21.81

using a proportional scale:  $\omega \approx (1.8 \text{ cm} \times 0.9)/2 \text{ cm} = 0.81$ . Alternatively, under the condition  $\alpha + \beta \neq 1$ , Fig. 4c suggests a value of  $\omega$  close to 1. With  $\omega$  and  $\alpha$  known, the standard heterogeneous rate constant  $k^0$  is computed using eqn (S14), yielding approximately  $11.75 \times 10^{-6} \text{ m s}^{-1}$  (for  $\omega \approx 0.81$ ) and  $14.51 \times 10^{-6} \text{ m s}^{-1}$  (for  $\omega \approx 1$ ).

All the interpolation equations, whether for  $\alpha + \beta = 1$  or  $\alpha + \beta \neq 1$ , are valid for  $\omega \leq 10^{-1}$ , whereas the estimated  $\omega$  values for silver ions are 0.81 and approximately 1. Hence, these values are outside the applicable range.

For copper ions,  $\omega$  was estimated using the kinetic diagram in Fig. 4a ( $\alpha + \beta \neq 1$ ) suggesting a value of  $\omega$  close to 0.2. With this  $\omega$  value and the known charge transfer coefficient  $\alpha$ , the standard rate constant  $k^0$  was calculated using eqn (S14), resulting in  $k^0 \approx 12.49 \times 10^{-7} \text{ m s}^{-1}$ .

Using the interpolation equations for the three cases,  $\alpha + \beta = 1$  (eqn (3)),  $\alpha + \beta \neq 1$  (eqn (20)), and  $\alpha + \beta \neq 1$  for irreversible systems (eqn (34)), the calculated  $k^0$  value for copper ions are  $9.0 \times 10^{-7} \text{ m s}^{-1}$ ,  $5.98 \times 10^{-7} \text{ m s}^{-1}$ , and  $5.33 \times 10^{-7} \text{ m s}^{-1}$ , respectively.

For rhenium ions, the dimensionless kinetic parameter  $\omega$  was estimated using the kinetic diagram in Fig. 2b ( $\alpha + \beta = 1$ ). Applying the rule of three gives  $\omega \approx (3.7 \text{ cm} \times 0.00009)/7.2 \text{ cm} = 0.46 \times 10^{-4}$ . With this  $\omega$  value and the known charge transfer coefficient  $\alpha$ , the standard rate constant  $k^0$  was calculated using eqn (S14), resulting in  $k^0 \approx 0.29 \times 10^{-8} \text{ m s}^{-1}$ .

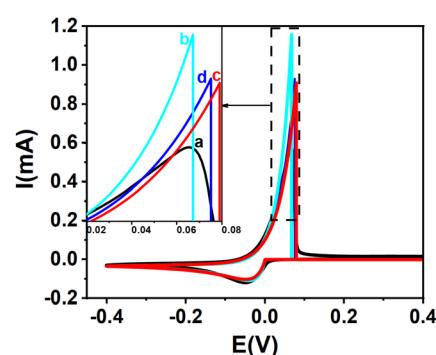
Using the interpolation equations for the three cases,  $\alpha + \beta = 1$  (eqn (3)),  $\alpha + \beta \neq 1$  (eqn (20)), and  $\alpha + \beta \neq 1$  in irreversible

systems (eqn (34)), the calculated standard rate constants  $k^0$  for rhenium ions are  $0.08 \times 10^{-8} \text{ m s}^{-1}$ ,  $10.59 \times 10^{-8} \text{ m s}^{-1}$ , and  $21.81 \times 10^{-8} \text{ m s}^{-1}$ , respectively. Since eqn (34) provides a simpler approach and yields a comparable result, it may be used in place of eqn (20) for practical  $k^0$  calculation.

Next, we simulate the cyclic voltammograms corresponding to the  $k^0$  values determined for silver, copper and rhenium ions. Fig. 5 presents both the simulated and experimental cyclic voltammograms for silver ion reduction. The simulations were carried out using the previously determined values of the charge transfer coefficient  $\alpha$ , the diffusion coefficient  $D$ , and the standard rate constant  $k^0$ . For the anodic transfer coefficient  $\beta$ , two approaches were considered: the value obtained from Tafel analysis and the one calculated using the relation  $\beta = 1 - \alpha$ .

Fig. 5 compares experimental and simulated cyclic voltammograms for silver ion reduction. In Fig. 5b, the simulated curve generated using  $k^0 = 11.75 \times 10^{-6} \text{ m s}^{-1}$ , with  $\alpha = 0.302$  and  $\beta$  estimated as  $1 - \alpha = 0.698$  (assuming  $\alpha + \beta = 1$ ), shows noticeable deviation from the experimental voltammogram (Fig. 5a), particularly near the anodic peak. Conversely, Fig. 5c displays a much better fit when the same  $k^0$  and  $\alpha$  values are used, but  $\beta$  is taken from the Tafel plot ( $\beta = 0.514$ ), highlighting the importance of using experimentally derived  $\beta$  values rather than assuming  $\beta = 1 - \alpha$ .<sup>52</sup> Finally, Fig. 5d shows the simulated curve using  $k^0 = 14.51 \times 10^{-6} \text{ m s}^{-1}$ , obtained from the kinetic model where  $\alpha + \beta \neq 1$ , which provides the closest agreement with the experimental data.

Fig. 6 represents simulated and experimental cyclic voltammograms for copper ions using various  $k^0$  values derived from different interpolation equations. When  $k^0 = 9.0 \times 10^{-7} \text{ m s}^{-1}$ , obtained from the interpolation equation assuming  $\alpha + \beta = 1$  (eqn (3)), the resulting curves (Fig. 6b), assuming  $\alpha + \beta = 1$ , shows deviations from the experimental voltammogram (Fig. 6a). In contrast, the simulation shown in Fig. 6c and d, based on  $k^0 = 5.98 \times 10^{-7} \text{ m s}^{-1}$  and  $k^0 = 5.33 \times 10^{-7} \text{ m s}^{-1}$  obtained from eqn (20) and eqn (34) where  $\alpha + \beta \neq 1$ , aligns much more closely with the experimental data.



**Fig. 5** Experimental and theoretical cyclic voltammograms for  $\text{Ag}^+/\text{Ag}$  redox couple: (a) experimental CV (black solid line) and (b-d) theoretical curves: (b) cyan solid line, from kinetic curves  $\alpha + \beta = 1$  (Fig. 2):  $k^0 = 11.75 \times 10^{-6} \text{ m s}^{-1}$ ,  $\alpha = 0.302$ ,  $\beta = 0.698$ , ( $\alpha + \beta = 1$ ); (c) red solid line, from kinetic curves  $\alpha + \beta = 1$  (Fig. 2):  $k^0 = 11.75 \times 10^{-6} \text{ m s}^{-1}$ ,  $\alpha = 0.302$ ,  $\beta = 0.514$  ( $\alpha + \beta \neq 1$ ); (d) blue solid line, from kinetic curves  $\alpha + \beta \neq 1$  (Fig. 4):  $k^0 = 14.51 \times 10^{-6} \text{ m s}^{-1}$ ,  $\alpha = 0.302$ ,  $\beta = 0.514$  ( $\alpha + \beta \neq 1$ ). Inset: magnified view of the anodic peaks.



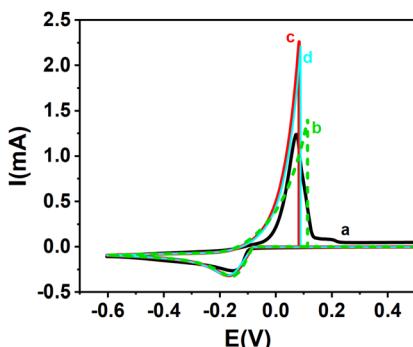


Fig. 6 Experimental and theoretical cyclic voltammograms for  $\text{Cu}^+/\text{Cu}$  redox couple: (a) experimental CV (black solid line), along with (b-d) theoretical curves derived from various interpolation equations: (b) green dashed line: theoretical curve from eqn (3), with  $k^0 = 9.0 \times 10^{-7} \text{ m s}^{-1}$ ,  $\alpha = 0.727$ ,  $\beta = 0.273$  ( $\alpha + \beta = 1$ ); (c) red solid line: eqn (20),  $k^0 = 5.98 \times 10^{-7} \text{ m s}^{-1}$ ,  $\alpha = 0.727$ ,  $\beta = 0.460$  ( $\alpha + \beta \neq 1$ ); (d) cyan solid line: eqn (34),  $k^0 = 5.33 \times 10^{-7} \text{ m s}^{-1}$ ,  $\alpha = 0.727$ ,  $\beta = 0.460$  ( $\alpha + \beta \neq 1$ ).

Fig. 7 and Fig. 8 display the experimental and simulated cyclic voltammograms for rhenium ion reduction. The simulations were performed using the previously determined parameters:  $\alpha$ , the diffusion coefficient  $D$ , and the standard rate constant  $k^0$ . For the anodic charge transfer coefficient  $\beta$ , two approaches were considered, either the value obtained directly from Tafel analysis or the one estimated using the assumption  $\beta = 1 - \alpha$ .

As shown in Fig. 7, the simulated voltammogram in Fig. 7b, calculated using  $k^0 = 0.29 \times 10^{-8} \text{ m s}^{-1}$  from the kinetic curves assuming  $\alpha + \beta = 1$  (Fig. 2) (with  $\alpha = 0.130$  and  $\beta = 1 - \alpha = 0.870$ ), deviates significantly from the experimental data (Fig. 7a), particularly at the anodic peak. In Fig. 7c, a second simulation using the same  $k^0$  and  $\alpha$  values but with  $\beta$  obtained from the Tafel analysis ( $\beta = 0.110$ ) shows a partial improvement where the anodic peak current is more aligned with the

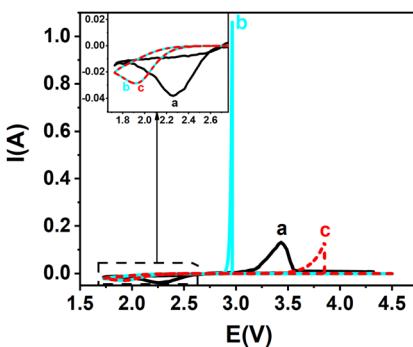


Fig. 7 Experimental and theoretical cyclic voltammograms for  $\text{Re}^{6+}/\text{Re}$  redox couple: (a) experimental CV (black solid line), adapted from Affoune *et al.*, *J. Appl. Electrochem.*, 2002, 32, 721–728, <https://doi.org/10.1023/A:1016532912889>, with permission from Springer Nature; (b and c) theoretical curves are shown for comparison: (b) cyan solid line:  $\alpha = 0.130$ ,  $\beta = 0.870$  ( $\alpha + \beta = 1$ ); (c) red dashed line:  $\alpha = 0.130$ ,  $\beta = 0.110$  ( $\alpha + \beta \neq 1$ ). The standard rate constant was calculated from the kinetic curves  $\alpha + \beta = 1$  (Fig. 2):  $k^0 = 0.29 \times 10^{-8} \text{ m s}^{-1}$ . Inset: magnified view of the cathodic peaks.

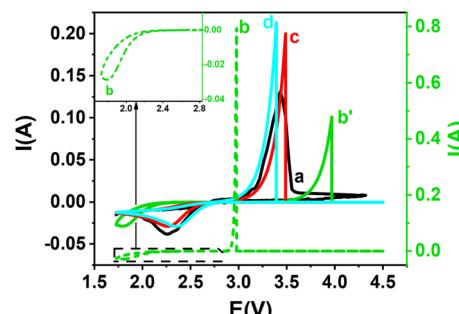


Fig. 8 Experimental and theoretical cyclic voltammograms for  $\text{Re}^{6+}/\text{Re}$  redox couple: (a) experimental CV (black solid line), adapted from Affoune *et al.*, *J. Appl. Electrochem.*, 2002, 32, 721–728, <https://doi.org/10.1023/A:1016532912889>, with permission from Springer Nature, along with (b-d) theoretical curves derived from various interpolation equations: (b) green dashed line (right Y-axis): theoretical curve from eqn (3), with  $k^0 = 0.08 \times 10^{-8} \text{ m s}^{-1}$ ,  $\alpha = 0.130$ ,  $\beta = 0.870$  ( $\alpha + \beta = 1$ ); (b') green solid line (left Y-axis): eqn (3),  $k^0 = 0.08 \times 10^{-8} \text{ m s}^{-1}$ ,  $\alpha = 0.130$ ,  $\beta = 0.110$  ( $\alpha + \beta \neq 1$ ); (c) red solid line (left Y-axis): eqn (20),  $k^0 = 10.59 \times 10^{-8} \text{ m s}^{-1}$ ,  $\alpha = 0.130$ ,  $\beta = 0.110$  ( $\alpha + \beta \neq 1$ ); (d) cyan solid line (left Y-axis): eqn (34),  $k^0 = 21.81 \times 10^{-8} \text{ m s}^{-1}$ ,  $\alpha = 0.130$ ,  $\beta = 0.110$  ( $\alpha + \beta \neq 1$ ). Inset: zoomed view of the cathodic peak (b).

experimental value. However, the overall shape remains inconsistent. These discrepancies confirm that the kinetic curves assuming  $\alpha + \beta = 1$  (Fig. 2) are not appropriate in this case, as the experimentally determined sum  $\alpha + \beta$  is approximately 0.24.

Fig. 8 compares simulated and experimental cyclic voltammograms for rhenium ions using various  $k^0$  values derived from different interpolation equations. When  $k^0 = 0.08 \times 10^{-8} \text{ m s}^{-1}$ , obtained from the interpolation equation assuming  $\alpha + \beta = 1$  (eqn (3)), the resulting curves (Fig. 8b and b'), whether assuming  $\alpha + \beta = 1$  or  $\neq 1$ , show significant deviations from the experimental voltammogram (Fig. 8a). In contrast, the simulation shown in Fig. 8c, based on  $k^0 = 10.59 \times 10^{-8} \text{ m s}^{-1}$  obtained from eqn (20) ( $\alpha + \beta \neq 1$ ), aligns much more closely with the experimental data. Additionally, Fig. 8d presents the simulation using  $k^0 = 21.81 \times 10^{-8} \text{ m s}^{-1}$ , calculated from the interpolation equation for irreversible systems (eqn (34)). Overall, the simulated voltammograms using interpolation equations tailored for  $\alpha + \beta \neq 1$ , particularly eqn (20), show the best agreement with experimental results.

These results suggest that the number of electrons involved in the redox process may significantly affect the estimated values of  $k^0$ . In particular, the one-electron transfer of silver leads to a comparatively high  $k^0$  ( $14.51 \times 10^{-6} \text{ m s}^{-1}$ ), whereas the multielectron transfer of rhenium results in a much smaller value ( $10.59 \times 10^{-8} \text{ m s}^{-1}$ ). Such differences are consistent with the general trend that multielectron processes are kinetically less favorable, as they require more complex reorganization steps at the electrode–electrolyte interface.

It is generally assumed that  $\alpha + \beta = 1$ , so that when one coefficient is determined, the other can be deduced.<sup>61</sup> In electrodeposition studies, authors typically determine only the cathodic charge transfer coefficient, which is directly involved



in the electrodeposition reaction.<sup>62,63</sup> The anodic charge transfer coefficient is usually determined in studies focused on the oxidation or corrosion of metallic substrates.<sup>64,65</sup> However, the literature shows that for soluble–soluble systems,<sup>56,57,66,67</sup> there are significantly more references where the sum of ( $\alpha + \beta$ ) differs from unity in a single article, compared to electrodeposition systems.<sup>53,58,59</sup> The results we obtained indicate that the sum ( $\alpha + \beta$ ) varies across different cases. For rhenium, ( $\alpha + \beta$ ) is 0.24; for silver, it is 0.816; and for copper, it is 1.187. Through this work, we have demonstrated that assuming  $\alpha + \beta = 1$  can lead to significant errors, as  $k^0$  is highly sensitive to the individual values of  $\alpha$  and  $\beta$ .

The simulated voltammograms exhibit a higher peak current than the experimental ones because the simulated curve reaches a maximum current and then drops sharply, unlike the smoother behavior of the experimental curve. Despite this small discrepancy, the methodology we applied here for silver, copper and rhenium provided a reliable determination of  $k^0$ .

### 3. Experimental and computational methods

#### 3.1. Theory

The theoretical approach used to simulate cyclic voltammograms for the metal electrodeposition reactions is described in detail in the SI file.

#### 3.2. Materials and methods

**3.2.1. Calculation methods.** The numerical simulations were carried out using Fortran 90 and compiled with Microsoft Fortran PowerStation 4.0. Post-processing and graphical analysis of the simulation data were performed using Origin 2018, which offered a complete suite of tools for data visualization. Using the non-linear fitting tools of Origin software, we carefully analysed our kinetic curves (Fig. 2) to derive the equations. For  $\Delta\phi = f(\alpha)$ , we applied the Rational/Holliday function with the Levenberg–Marquardt algorithm, while for  $\Delta\phi = f(\omega)$  we used Exponential models (ExpDec1, Exp2PMod1, Exp2P) with the same algorithm.

The charge transfer coefficient was estimated through Tafel plot analysis, while the diffusion coefficient was evaluated using the semi-integration technique, based on the method originally proposed by Oldham.<sup>16,68,69</sup>

**3.2.2. Reagents.** For the electrochemical reduction reaction of silver ions, we used silver trifluoromethanesulfonate  $\text{CF}_3\text{SO}_3\text{Ag}$  (10 mM) in perchloric acid  $\text{HClO}_4$  (1 M) from Sigma-Aldrich Company. For the electrochemical reduction reaction of copper ions, we used tetrakis(acetonitrile)copper(I) tetrafluoroborate  $[\text{Cu}(\text{CH}_3\text{CN})_4]\text{BF}_4$  (10 mM) from (TCI) in tetraethylammonium tetrafluoroborate TEABF<sub>4</sub> (0.1 M) from (ABCR). For the electrochemical reduction reaction of rhenium ions, we used rhenium hexafluoride  $\text{ReF}_6$  (26 mM) in LiF–NaF–KF eutectic mixture from Sigma-Aldrich Company; more details on the preparation of rhenium electrolyte are provided in the article of Affoune *et al.*<sup>18</sup> All reagents were used without purification.

**3.2.3. Instrumentation and procedures.** The cyclic voltammetric measurements for the reductions of  $\text{CF}_3\text{SO}_3\text{Ag}$  and  $[\text{Cu}(\text{CH}_3\text{CN})_4]\text{BF}_4$  were carried out using an Autolab model PGSTAT302N potentiostat and for the reduction of  $\text{ReF}_6$  a potentiostat–galvanostat (PAR EG&G model 273), respectively.

For the reduction of  $\text{CF}_3\text{SO}_3\text{Ag}$ , a gold disc electrode (0.0707  $\text{cm}^2$ ) was employed, with platinum wire as a counter electrode and a silver wire as a comparison electrode. For the reduction of  $[\text{Cu}(\text{CH}_3\text{CN})_4]\text{BF}_4$ , a platinum electrode (0.0707  $\text{cm}^2$ ) was employed, with platinum wire as a counter electrode and a copper wire as a comparison electrode. The reduction of  $\text{ReF}_6$  was performed using a vitreous carbon wire (1.884  $\text{cm}^2$ ) as a working electrode, graphite crucible as a counter electrode, and a platinum wire as a comparison electrode. The potentials were referred to the equilibrium potential of  $\text{K}^+/\text{K}$  couple, the cathodic limit of the solvent.

The potential was swept between 0.4 V and –0.4 V at a scan rate of 50  $\text{mV s}^{-1}$  for silver ions reduction, 0.7 V and –0.6 V at a scan rate of 100  $\text{mV s}^{-1}$  for copper ions reduction and between 3.73 V and 1.73 V at a scan rate of 50  $\text{mV s}^{-1}$  for rhenium reduction. The first two reactions were carried out at room temperature, whereas the rhenium ions reduction was performed at 600 °C.

### 4. Conclusions

Using the Butler–Volmer framework and a semi-analytical method, cyclic voltammograms were simulated for metal electrodeposition across reversible, quasi-reversible, and irreversible regimes. Kinetic curves were constructed from peak-to-peak separations over a wide range of  $\alpha$  and dimensionless rate constants ( $\omega$ ), leading to interpolation equations for both  $\alpha + \beta = 1$  and  $\alpha + \beta \neq 1$ .

Experimental validation was performed *via* silver, copper and rhenium ions reduction. The extracted parameters were:

Silver couple:  $\alpha = 0.302$ ,  $\beta = 0.514$ ,  $D = 5.56 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ ,  $k^0 = 14.51 \times 10^{-6} \text{ m s}^{-1}$

Copper couple:  $\alpha = 0.727$ ,  $\beta = 0.460$ ,  $D = 2.58 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ ,  $k^0 = 5.98 \times 10^{-7} \text{ m s}^{-1}$

Rhenium couple:  $\alpha = 0.130$ ,  $\beta = 0.110$ ,  $D = 8 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ ,  $k^0 = 10.59 \times 10^{-8} \text{ m s}^{-1}$

Simulated voltammograms closely matched the experimental data, confirming the reliability of the proposed method.

This study provides a validated and practical approach for determining the standard rate constant  $k^0$  in metal electrodeposition systems using both kinetic curves and interpolation equations. Experimental results show that the derived  $k^0$  values reproduce cyclic voltammograms with excellent agreement. The interpolation equations offer superior precision, especially when  $\alpha + \beta$  deviates from 1; where traditional kinetic curves become unreliable.

Importantly, our findings underline that assuming  $\alpha + \beta = 1$  can lead to significant errors, as  $k^0$  is highly sensitive to the individual values of  $\alpha$  and  $\beta$ . This work delivers a generalizable method for extracting  $k^0$  from CV data, supported by both theory and experiment.



To our knowledge, it is the most thorough investigation to date on how  $\alpha$ ,  $\beta$ , and their sum influence cyclic voltammetry and peak-to-peak separation, filling key gaps in previous models and offering tools of wide relevance in electrochemical kinetics.

## Author contributions

Rania Saad Guermeche: data curation, formal analysis, software, visualization, writing – original draft, writing – review & editing. Abed Mohamed Affoune: conceptualization, data curation, formal analysis, methodology, investigation, project administration, supervision, validation, visualization, writing – original draft, writing – review & editing. Sabrina Houam: data curation, formal analysis, validation, writing – review & editing. Imene Atek: data curation, formal analysis, validation, writing – review & editing. Christine Vautrin-Ul: formal analysis, writing – review & editing. Mouna Nacef: software, writing – review & editing. Mohamed Lyamine Chelaghmia: validation, writing – review & editing. Hubert H. Girault: resources, validation, visualization, writing – review & editing. Craig E. Banks: validation, visualization, writing – review & editing. Ilhem Djaghout: supervision, writing – review & editing. Jacques Bouteillon: investigation (posthumous contribution of previously published experimental data used in this study). Jean Claude Poignet: investigation (posthumous contribution of previously published experimental data used in this study).

## Conflicts of interest

There are no conflicts to declare.

## Data availability

The data supporting this article have been included as part of the supplementary information (SI). Supplementary information: computational details of cyclic voltammetry simulation, effect of switching potential, analysis of charge transfer and diffusion coefficients, theoretical validation of interpolation equations, MATLAB code used for kinetic calculations, nomenclature and additional references. See DOI: <https://doi.org/10.1039/d5sc05636e>.

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## Notes and references

- 1 R. G. Compton, E. Laborda and K. R. Ward, *Understanding voltammetry: simulation of electrode processes*, Imperial College Press, London, 2014.
- 2 H. H. Girault, *Électrochimie physique et analytique*, Presses polytechniques et universitaires romandes [diff. Geodif], Lausanne [Paris], 2e éd, 2007.
- 3 Y. Saito and T. Kikuchi, Eds., *Voltammetry: theory, types and applications*, Nova Publ, New York, 2014.
- 4 J. E. B. Randles, *Trans. Faraday Soc.*, 1948, **44**, 327–338.
- 5 A. Ševčík, *Collect. Czech. Chem. Commun.*, 1948, **13**, 349–377.
- 6 H. Matsuda and Y. Ayabe, *Z. für Phys. Abtl. A-chemische Thermodyn. Kinet. Elektrochem. Eig.*, 1955, **59**, 494–503.
- 7 R. S. Nicholson, *Anal. Chem.*, 1965, **37**, 1351–1355.
- 8 S. Houam, A. M. Affoune, I. Atek, F. Kesri, R. Saad Guermeche, M. L. Chelaghmia, M. Nacef, O. Khelifi and C. E. Banks, *Electrochim. Acta*, 2023, **449**, 142200.
- 9 R. S. Nicholson and I. Shain, *Anal. Chem.*, 1964, **36**, 706–723.
- 10 T. Berzins and P. Delahay, *J. Am. Chem. Soc.*, 1953, **75**, 555–559.
- 11 G. Mamantov, D. L. Manning and J. M. Dale, *J. Electroanal. Chem.*, 1959, **9**, 253–259.
- 12 N. White and F. Lawson, *J. Electroanal. Chem. Interfacial Electrochem.*, 1970, **25**, 409–419.
- 13 D. J. Schiffrin, *J. Electroanal. Chem. Interfacial Electrochem.*, 1986, **201**, 199–203.
- 14 P. Delahay, *J. Am. Chem. Soc.*, 1953, **75**, 1190–1196.
- 15 I. Atek, S. Maye, H. H. Girault, A. M. Affoune and P. Peljo, *J. Electroanal. Chem.*, 2018, **818**, 35–43.
- 16 S. Abdelkader, *Badji Mokhtar University*, Annaba, 2010.
- 17 A. M. Affoune, A. Saila, J. Bouteillon and J. C. Poignet, *J. Appl. Electrochem.*, 2006, **37**, 155–160.
- 18 A. M. Affoune, J. Bouteillon and J. C. Poignet, *J. Appl. Electrochem.*, 2002, **32**, 521–526.
- 19 A. J. Bard and L. R. Faulkner, *Electrochemical methods: fundamentals and applications*, Wiley, New York Weinheim, 2. edition., 2001.
- 20 J. Heinze, *Angew. Chem. Int. Ed. Engl.*, 1993, **32**, 1268–1288.
- 21 J. Heinze, *Angew. Chem. Int. Ed. Engl.*, 1984, **23**, 831–847.
- 22 S. R. Belding, J. G. Limon-Petersen, E. J. F. Dickinson and R. G. Compton, *Angew. Chem., Int. Ed.*, 2010, **49**, 9242–9245.
- 23 H. Chen, M. Yang, B. Smetana, V. Novák, V. Matějka and R. G. Compton, *Angew. Chem., Int. Ed.*, 2024, **63**, e202315937.
- 24 C. K. Terry Weatherly, H. Ren, M. A. Edwards, L. Wang and H. S. White, *J. Am. Chem. Soc.*, 2019, **141**, 18091–18098.
- 25 H. Chen, Y. Chen and R. G. Compton, *Anal. Chem.*, 2022, **2c04794**.
- 26 D. Krulic, N. Fatouros and D. Liu, *J. Electroanal. Chem.*, 2015, **754**, 30–39.
- 27 D. Liu, D. Krulic, H. Groult and N. Fatouros, *J. Electroanal. Chem.*, 2016, **775**, 91–104.
- 28 Y. Liu, H. Ren, T. Yin, D. Yang, Z. Chai and W. Shi, *Electrochim. Acta*, 2019, **326**, 134971.
- 29 L. A. Avaca, S. Kaufmann, K. Kontturi, L. Murtomäki and D. J. Schiffrin, *Ber Bunsenges Phys Chem*, 1993, **97**, 70–76.
- 30 Y. Kanzaki and S. Aoyagi, *J. Electroanal. Chem. Interfacial Electrochem.*, 1972, **36**, 297–310.
- 31 E. P. Randviir, *Electrochim. Acta*, 2018, **286**, 179–186.
- 32 Q. Li, S. Xie, Z. Liang, X. Meng, S. Liu, H. H. Girault and Y. Shao, *Angew. Chem., Int. Ed.*, 2009, **48**, 8010–8013.
- 33 N. Plumeré and B. A. Johnson, *J. Am. Chem. Soc.*, 2024, **146**, 34771–34785.
- 34 Y. Chen, X. Gao, L. R. Johnson and P. G. Bruce, *Nat. Commun.*, 2018, **9**, 767.



35 E. Sramkova, T. Bystron and K. Bouzek, *Electrochim. Acta*, 2021, **379**, 138177.

36 E. S. Rountree, B. D. McCarthy, T. T. Eisenhart and J. L. Dempsey, *Inorg. Chem.*, 2014, **53**, 9983–10002.

37 S.-Q. Liu, W.-H. Sun, L.-C. Li, H. Li and X.-L. Wang, *Int. J. Electrochem. Sci.*, 2012, **7**, 324–337.

38 K. Gong, X. Ma, K. M. Conforti, K. J. Kuttler, J. B. Grunewald, K. L. Yeager, M. Z. Bazant, S. Gu and Y. Yan, *Energy Environ. Sci.*, 2015, **8**, 2941–2945.

39 M. Liu, S. J. Visco and L. C. D. Jonghe, *J. Electrochem. Soc.*, 1990, **137**, 750–759.

40 A. Mahapatro and S. Kumar Suggu, *Adv. Mater. Sci.*, 2018, **3**, 1–9.

41 F. I. Danilov and V. S. Protsenko, *Prot. Met.*, 2001, **37**, 223–228.

42 H. Noma, T. Koga, C. Hirakawa, K. Nonaka and K. Shobu, *Meet. Abstr.*, 2013, **MA2013–02**, 2085.

43 C. Zhang, S. Govindaraju, K. Giribabu, Y. S. Huh and K. Yun, *Sens. Actuators, B*, 2017, **252**, 616–623.

44 F. J. Del Campo, L. Abad, X. Illa, E. Prats-Alfonso, X. Borrisé, J. M. Cirera, H.-Y. Bai and Y.-C. Tsai, *Sens. Actuators, B*, 2014, **194**, 86–95.

45 J. P. Metters, S. M. Houssein, D. K. Kampouris and C. E. Banks, *Anal. Methods*, 2013, **5**, 103–110.

46 K. Gong, F. Xu, J. B. Grunewald, X. Ma, Y. Zhao, S. Gu and Y. Yan, *ACS Energy Lett.*, 2016, **1**, 89–93.

47 C. Storky, M. J. Davies and D. I. Pattison, *Free Radical Biol. Med.*, 2014, **73**, 60–66.

48 I. Yamazaki and L. H. Piette, *J. Biol. Chem.*, 1990, **265**, 13589–13594.

49 I. Lavagnini, R. Antiochia and F. Magno, *Electroanalysis*, 2004, **16**, 505–506.

50 R. J. Klingler and J. K. Kochi, *J. Phys. Chem.*, 1981, **85**, 1731–1741.

51 T. W. Swaddle, *Chem. Rev.*, 2005, **105**, 2573–2608.

52 D. Suwatchara, M. C. Henstridge, N. V. Rees and R. G. Compton, *J. Phys. Chem. C*, 2011, **115**, 14876–14882.

53 J. Besson, *Précis de thermodynamique et cinétique électrochimiques [Handbook of electrochemical thermodynamics and kinetics]*, Ellipses-Marketing, Paris, 1984.

54 H. Chen and R. G. Compton, *J. Electroanal. Chem.*, 2021, **880**, 114942.

55 M. C. Henstridge, E. Laborda, N. V. Rees and R. G. Compton, *Electrochim. Acta*, 2012, **84**, 12–20.

56 I. Kröner, M. Becker and T. Turek, *ChemElectroChem*, 2020, **7**, 4314–4325.

57 M. Becker, N. Bredemeyer, N. Tenhumberg and T. Turek, *Electrochim. Acta*, 2017, **252**, 12–24.

58 G.-S. Tzeng, *Plat. Surf. Finish.*, 1995, **82**, 67–71.

59 F. J. Barry and V. J. Cunnane, *J. Electroanal. Chem.*, 2002, **537**, 151–163.

60 L. Cifuentes and J. Simpson, *Chem. Eng. Sci.*, 2005, **60**, 4915–4923.

61 J. A. Corona-Castro, G. A. Álvarez-Romero, M. Rivera, C. H. Ríos-Reyes, L. E. Bañuelos-García, E. García-Sánchez and L. H. Mendoza-Huizar, *J. Chil. Chem. Soc.*, 2022, **67**, 5500–5502.

62 K. H. Lim, S. Park and J.-I. Yun, *J. Electrochem. Soc.*, 2015, **162**, E334–E337.

63 Z. Hou, X. Wang, J. Li, Z. Li, Y. Wang and H. Xing, *Front. Chem.*, 2022, **10**, 871420.

64 J. Ress, U. Martin and D. M. Bastidas, *Front. Mater.*, 2022, **9**, 1052261.

65 Universidad de Antioquia, J. A. Tamayo-Sepúlveda, F. A. Vásquez-Arroyave and Universidad de Antioquia, *Rev. Fac. Ing. Univ. Antioquia*, 2017, 36–42.

66 S. K. Guin, A. S. Ambolikar and J. V. Kamat, *RSC Adv.*, 2015, **5**, 59437–59446.

67 E. Agar, C. R. Dennison, K. W. Knehr and E. C. Kumbur, *J. Power Sources*, 2013, **225**, 89–94.

68 K. B. Oldham and J. Spanier, *J. Electroanal. Chem.*, 1970, **26**(2–3), 331–341.

69 K. B. Oldham, *J. Electroanal. Chem. Interfacial Electrochem.*, 1981, **121**, 341–342.

