

Cite this: *Chem. Sci.*, 2025, 16, 11359

All publication charges for this article have been paid for by the Royal Society of Chemistry

Multicycle *operando* pressure measurements enable assessment of redox mediator efficacy in lithium–oxygen batteries†

Thukshan Samarakoon,^a Ben Wood,^a Alex R. Neale,^a Elliot Coulbeck,^b Daniel J. Saccomando^c and Laurence J. Hardwick^{*,a}

Redox mediators (RMs) present a promising strategy for achieving low overpotential charging of lithium–oxygen (Li–O₂) batteries, thereby extending cycle life and improving overall energy efficiency. In this study, multi-cycle *operando* pressure measurement during galvanostatic Li–O₂ cell cycling was employed to assess the efficacy of 2,2,6,6-tetramethylpiperdinyloxy (TEMPO) as a charge RM in sulfolane- and diglyme-based electrolytes. In both mediated electrolytes, electrochemical TEMPO oxidation coincided with gas evolution, validating TEMPO activity and revealing distinct behaviour in the reactions and stability of the glyme- and sulfone-based electrolytes. Pressure measurements showed a greater extent of parasitic reactions during charging in the mediated diglyme system during early cycles. In the sulfolane-based electrolyte, initial stable cycling was observed. However, a more rapid capacity fade was subsequently observed in the latter cycles, due to increasing parasitic chemistry on charge. Furthermore, highly sensitive pressure measurements enabled small changes in the pressure response to be correlated with transitions in the electrochemical cycling profile. Analyses of the dynamic rate of pressure changes within Li–O₂ cells and correlation with differential capacity was used to identify exact points within a charge step wherein RM efficacy is diminished, thereby tracking the evolution of RM activity loss during cycling. This approach provided a valuable indicator of RM efficacy, defined in terms of maximising the number of cycles for which gas evolution is centred around the RM oxidation potential. Importantly, this method directly assesses RM cyclability in the Li–O₂ cell environment and can be applied to any electrolyte–electrode combination, proving to be a versatile approach for identification of promising mediated electrolyte formulations for longer life Li–O₂ batteries.

Received 27th March 2025

Accepted 20th May 2025

DOI: 10.1039/d5sc02350e

rsc.li/chemical-science

Introduction

Lithium–oxygen (Li–O₂) batteries offer a significantly higher theoretical specific energy (*ca.* 3500 Wh kg^{−1} based on lithium peroxide (Li₂O₂) formation/decomposition) compared to other battery chemistries.^{1–3} The electrochemical reactions taking place at the positive electrode are 2-electron oxygen reduction and evolution reactions (ORR and OER), forming and oxidatively decomposing Li₂O₂ on discharge and charge, respectively.^{4–8} Key mechanistic studies on ORR and OER in Li–O₂ cells have developed the research community's understanding of factors governing the discharge mechanism (surface- *versus* solution-driven Li₂O₂ formation) and the associated Li₂O₂ morphology on the positive electrode,^{4,9–14} as well

as charging mechanisms.^{9,15,16} The insulating nature of Li₂O₂ and distribution of the product on the electrode surface necessitates high overpotentials for its electrochemical oxidation on charge, driving high potential-induced parasitic reactions that irreversibly breakdown most organic electrolyte solvents and the carbon-based positive electrode.^{17–19} Ultimately, this leads to poor cycle life and low overall energy efficiency, diminishing the practical viability of Li–O₂ batteries.

Redox mediators (RMs) represent a promising solution to this problem, with numerous studies demonstrating their ability to reduce charging overpotentials and extend cell lifetime.^{20–33} The RM acts as an electrolyte-soluble catalyst, promoting the intended Li₂O₂ formation on discharge and/or its oxidation on charge. A large body of work has focussed on charge RMs for Li–O₂ cells, wherein the mechanism for mediated Li₂O₂ oxidation involves electrochemical oxidation of the RM (to RM⁺) at the positive electrode, followed by RM⁺-driven coupled chemical oxidation of solid Li₂O₂, evolving O₂ gas and Li⁺. Therefore, the cell charge potential depends largely on the oxidation potential of the RM, thus enabling a decrease in charge overpotentials. Considering only charge mediators, the

^aStephenson Institute for Renewable Energy, Department of Chemistry, University of Liverpool, Liverpool, L69 7ZF, UK. E-mail: hardwick@liverpool.ac.uk

^bLubrizol Limited, Blackley, Manchester, M9 8ES, UK

^cLubrizol Limited, Hazelwood, Derby, DE56 4AN, UK

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d5sc02350e>

chemical space that has been explored for candidate RMs is highly diverse, ranging from organic molecules^{20,22–26} to organometallic^{27–29} and halide-based compounds.^{30–33} Organic RMs are particularly promising due to synthetic versatility, allowing for careful control of the RM redox potential, and indeed, some of the most promising RMs reported are in this category.

Among the explored organic RMs, the majority are cyclic and contain at least one nitrogen atom.³⁴ The nitroxide-based family of RMs are well-known in the research community, with most having been evaluated in terms of thermodynamics (RM redox potentials) and kinetics (for reaction between RM^+ and Li_2O_2).^{35,36} 2,2,6,6-Tetramethylpiperidinyloxy (TEMPO) is a widely studied RM in this sub-class, with Bergner *et al.* being the first to report its use as a charge RM in Li–O₂ cells operating with lithium bis(trifluoromethanesulfonyl)imide (Li[TFSI]) in diglyme as the base electrolyte.²⁰ In this system, the redox potential for the TEMPO⁺/TEMPO couple ($E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$) is *ca.* 3.75 V vs. Li^+/Li . Subsequently, TEMPO has primarily been studied as a charge RM in ether-based electrolytes. There are little to no reports of TEMPO in other electrolytes, such as those based on dimethylsulfoxide (DMSO), sulfolane and ionic liquids (ILs) (*e.g.*, pyrrolidinium-based ILs), despite unmediated electrolytes based on each of these solvents having been explored for Li–O₂ cells.^{37–41} For unexplored electrolyte solvent systems, it is crucial to verify that the selected RM is driving Li_2O_2 oxidation, which cannot be confirmed solely through galvanostatic cycling profiles. Instead, an online approach is required, such as differential electrochemical mass spectrometry (DEMS)-based approaches and *operando* internal cell pressure measurement. DEMS analysis of Li–O₂ cell chemistry has been widely reported for a range of electrolytes,^{17,18,41} and *operando* pressure monitoring has also been employed to study Li–O₂, Na–O₂ and Li-ion battery chemistries.^{42–46} Although the former provides access to direct chemical information (*i.e.*, identifying the types of gases evolved during charging), which cannot be discerned from *operando* pressure measurements, the advantage of online pressure monitoring is that gas consumption/evolution can be tracked for the duration of the cell's lifetime. While DEMS has been applied to study gas evolution during cycling of Li-ion cells over many hours (>100 h),⁴⁷ in the context of DEMS studies focussing on Li–O₂ cell chemistry, such measurements are generally more focussed on a single discharge–charge cycle or even a half-cycle.^{20,26} Therefore, in this work, emphasis is placed on the importance of incorporating *operando* pressure measurements for studying mediated Li–O₂ cells in combination with *ex situ* characterisation techniques, such as chemical titrations for Li_2O_2 yield determination, for the exploration of novel electrolyte formulations.

In this work, the viability of TEMPO as a charge RM is explored in a series of electrolytes based on sulfolane, DMSO, 1-methyl-1-propylpyrrolidinium [TFSI][–] ([Pyrr₁₃][TFSI]) and diglyme. In-depth studies involving (i) chemical titrations for Li_2O_2 yield determination, (ii) current density and internal cell pressure variations, and (iii) *operando* pressure monitoring were conducted on Li–O₂ cells with a TEMPO-containing sulfolane-based

electrolyte to assess the efficacy of TEMPO as a charge RM in this system, with comparison to a diglyme-based electrolyte. Several different analyses were performed on the *operando* pressure data to extract gas consumption/evolution rates and the ratio of moles of charge passed to moles of gas consumed/evolved over a discharge/charge half-cycle, serving as useful markers of cycle-to-cycle evolution of parasitic chemistry. Lastly, an approach combining differential capacity analyses with internal cell pressure measurements as a function of cell potential served as a versatile indicator of RM activity loss during cycling in sulfolane- and diglyme-based electrolytes. These results demonstrate how *operando* pressure data can be a useful tool to screen novel RM-containing electrolyte formulations.

Experimental

Materials

Lithium bis(trifluoromethane)sulfonylimide (Li[TFSI], 99%+), 1-propyl-1-methylpyrrolidinium [TFSI] ([Pyrr₁₃][TFSI], 99.9%) and 1-butyl-1-methylpyrrolidinium [TFSI] ([Pyrr₁₄][TFSI], 99.9%) were purchased from Solvionic, France. Sulfolane (99%) was purchased from Alfa Aesar, US and dimethylsulfoxide (DMSO, anhydrous, 99.9%) from ROMIL, UK. Diglyme (anhydrous, 99.5%), 1.9–2.1% titanium(IV) oxysulfate solution (prepared according to DIN 38 409, part 15, DEV-18), polytetrafluoroethylene (PTFE, 60 wt% dispersion in H₂O) and silver trifluoromethanesulfonate (Ag[OTf], ≥99%) were purchased from Merck, UK. 2,2,6,6-Tetramethylpiperidinyloxy (TEMPO, 99%) was purchased from Fluorochem, UK. Ketjenblack EC-600JD was purchased from MSE Supplies, US. Isopropanol (99%) and lithium peroxide (95%) was purchased from Fisher, UK. Glass fibre (Whatman Grade GF/F) was purchased from Lab-Shop, UK. Alumina powder (Buehler, US) of varying particle sizes (1.0, 0.3 and 0.05 μm) was used to polish the glassy carbon working electrode for cyclic voltammetry measurements. All molecular solvents were successively dried over freshly activated 3 Å molecular sieves. Li[TFSI] was dried at 10^{–2} mbar at 120 °C for 24 h, followed by further drying at 10^{–5} mbar for 48–72 h at the same temperature. Glass fibre separators were washed with ethanol several times, dried under vacuum at 110 °C for 15 h in a tube oven (Buchi, Switzerland) and then transferred to an Ar-filled glovebox without exposure to air. All other materials were used as received.

Electrolyte preparation

All electrolytes were prepared and stored in an Ar-filled glovebox (H₂O and O₂ levels below 0.1 ppm). Electrolytes for cyclic voltammetry experiments were prepared volumetrically, containing 10 mM TEMPO and 1 M Li[TFSI] dissolved in diglyme, sulfolane, DMSO or [Pyrr₁₃][TFSI]. For Li–O₂ cell studies, electrolytes based on sulfolane and diglyme solvents with Li[TFSI] and with or without TEMPO were selected. A minimum amount of each electrolyte (~0.7 mL) was prepared and stored in an Ar-filled glovebox and used within 2 months in order to minimise H₂O accumulation. The water content of all electrolytes was confirmed to be <15 ppm by coulometric Karl Fischer titration performed in an Ar-filled glovebox. The mole fraction (*x*) ratio of



Table 1 Electrolyte formulations explored in Li–O₂ cells^a

Entry	Electrolyte components	$x_{\text{solvent}} : x_{\text{Li salt}}$	Molality		$\text{mol}_{\text{additives}} \text{ kg}_{\text{solvent}}^{-1}$
			$\text{mol}_{\text{solutes}} \text{ kg}_{\text{solvent}}^{-1}$	$\text{mol}_{\text{Li salt}} \text{ kg}_{\text{solvent}}^{-1}$	
1	Li[TFSI] Diglyme	9 : 1	0.828	0.828	—
2	TEMPO Li[TFSI] Diglyme	9 : 1	0.853	0.828	0.0249
3	Li[TFSI] Sulfolane	9 : 1	0.925	0.925	—
4	TEMPO Li[TFSI] Sulfolane	9 : 1	0.945	0.925	0.0204

^a x denotes the mole fraction.

solvent (x_{solvent}) to Li[TFSI] ($x_{\text{Li[TFSI]}}$) was fixed at $x_{\text{solvent}} : x_{\text{Li[TFSI]}} = 9 : 1$ and the TEMPO dosing was $25 \text{ mmol}_{\text{TEMPO}} \text{ kg}_{\text{solvent}}^{-1}$. This molal concentration equates to *ca.* 20–25 mmol dm^{-3} TEMPO. Estimation of the TEMPO concentration in terms of molarity is made to allow for comparison to literature and is based on considering solely the volume contribution from the solvent and that of the solvent and Li[TFSI] salt. Table 1 summarises the electrolyte formulations for Li–O₂ cell studies.

Cyclic voltammetry

Cyclic voltammetry was performed using a glassy carbon (GC) working electrode (WE), a Pt counter electrode (CE) and either a Li metal or silver triflate/silver (Ag[OTf]/Ag) reference electrode (RE). The Ag[OTf]/Ag RE, based on a design by Snook *et al.*,⁴⁸ comprised a silver wire immersed in a glass capillary filled with 100 mM Ag[OTf] in [Pyrr₁₄][TFSI]. The RE electrolyte was isolated from the analyte electrolyte by a porous glass frit. The GC WE was cleaned and polished after every experiment on microfibre cloth (Buehler, US) wetted with slurries of alumina (particle sizes: 1.0, 0.3 and 0.05 μm) in ultrapure water. Cyclic voltammetry was performed on a SP-300 potentiostat (Bio-Logic, France).

Carbon black electrode fabrication

Electrodes for Li–O₂ cells were prepared by spray coating a slurry of carbon black (Ketjenblack EC-600JD) and PTFE (80 : 20 wt%) in isopropanol on to glass fibre under gentle heating at 30 °C. The slurry was stirred vigorously for 24 h prior to spray coating on to glass fibre. After spray coating, \varnothing 10 mm electrodes were punched out, dried at 110 °C for 15 h in a tube oven (Buchi, Switzerland) and then transferred to an Ar-filled glovebox without exposure to air. The carbon black loading was $1.3 \pm 0.1 \text{ mg}_c \text{ cm}^{-2}$ ($1.0 \pm 0.1 \text{ mg}_c$).

Lithium–oxygen cell assembly and cycling

Standard Li–O₂ cells were assembled in an Ar-filled glovebox (O₂, H₂O <0.1 ppm) and contained the following stack: stainless steel

mesh current collector, carbon black positive electrode (prepared as described above), glass fibre separator (\varnothing 12.7 mm) soaked with electrolyte and polished Li metal (\varnothing 12 mm) negative electrode. Standard Li–O₂ cells contained a polyether ether ketone (PEEK)-lined cell body (Microplas Mouldings Ltd. UK) that housed the electrode stack, with the positive electrode side of the cell exposed to an O₂ reservoir contained within stainless steel tubing. For the standard cell, quarter-turn gas inlet/outlet valves enabled purging of the cell with pure O₂ before cycling (see Fig. S1† for images of the standard Li–O₂ cells used in this work). After assembly, the cell was taken out of the glovebox and purged with high purity O₂ gas (N5.5, BOC, UK) at 1.25 bar_A (absolute pressure) before being sealed at 1.3 bar_A. The cycling protocol was initiated following a rest period of 8 h. The pressure cell, containing the same electrode stack within an identical PEEK-lined cell body, was assembled in the same way, except that cells were sealed at 1.5 bar_A and rested for 18–24 h to allow for a stable leak rate (*ca.* $10^{-5} \text{ bar h}^{-1}$) to be established before cycling. Cells were cycled at a current density of 80 mA g_c^{-1} ($0.11 \pm 0.01 \text{ mA cm}^{-2}$) with discharge and charge potential cut-offs of 2.0 and 4.5 V vs. Li⁺/Li, respectively, and a capacity-limit of either 500 ($0.7 \pm 0.1 \text{ mAh cm}^{-2}$) or 1000 mAh g_c^{-1} ($1.3 \pm 0.1 \text{ mAh cm}^{-2}$). For the internal cell pressure and current density variations, cells were cycled at 1.3, 1.75 and 2.2 bar_A (absolute pressure), and 80, 160 ($0.21 \pm 0.02 \text{ mA cm}^{-2}$) and 320 mA g_c^{-1} ($0.42 \pm 0.03 \text{ mA cm}^{-2}$), respectively. Standard Li–O₂ cells were cycled on a BCS-805 battery cycler (Bio-Logic, France) and the pressure cell on a SP-150 potentiostat (Bio-Logic, France).

UV-vis titration for Li₂O₂ yield determination

Li–O₂ cells with carbon black electrodes (prepared as described above) were discharged to 1000 mAh g_c^{-1} at 80 mA g_c^{-1} . Cells were then purged with Ar before being taken into an Ar-filled glovebox for disassembly and electrode extraction. The carbon electrodes were dried under vacuum in the glovebox antechamber for 2 h and then placed into septum-capped vials. The electrodes were then taken out of the glovebox and treated with a 1 : 1



solution of $\text{TiOSO}_4 \cdot \text{H}_2\text{O}$, producing a yellow solution due to formation of a $[\text{TiO}_2]^{2+}$ complex. After reacting for 30 min, an aliquot of the solution was transferred to a cuvette for determination of the absorbance at $\lambda_{\text{max}} = 407 \text{ nm}$ by UV-Vis spectroscopy (Evolution 201 UV-Vis Spectrophotometer, Thermo Fisher Scientific, US). The Li_2O_2 yield was determined using a calibration curve (Fig. S2†) prepared with known amounts of commercial Li_2O_2 , taking into account a quoted purity of 95%. For each electrolyte, yield tests were performed in duplicate.

Results and discussion

Electrolyte-dependent redox behaviour of TEMPO

The redox behaviour of TEMPO in several molecular solvent- and ionic liquid-based electrolytes under an inert atmosphere was first explored by cyclic voltammetry. Fig. 1 shows the redox behaviour of TEMPO in a range of electrolytes with $\text{Li}[\text{TFSI}]$ as the supporting electrolyte under an Ar atmosphere at a glassy carbon working electrode (GC WE). The CVs were measured with a Pt and Li metal counter electrode (CE) and reference electrode (RE), respectively. Significant differences in the TEMPO redox potential ($E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$), with a range of 360 mV, are observed in the CVs measured with a Li metal RE. These shifts are attributed primarily to the differences in Li reduction potential as a function of the electrolyte, rather than a change in $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$, as depicted by the potential scale shown in Fig. 1c. This is demonstrated in CVs performed using a silver triflate/silver ($\text{Ag}[\text{OTf}]/\text{Ag}$) RE (see Experimental for details of RE assembly). This RE is separated from the analyte electrolyte by a porous glass frit, maintaining a more electrolyte-independent reference potential. As such, $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ varies by <50 mV between the different solvent systems. However, the changes in $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ observed with the Li metal RE are still of practical significance for $\text{Li}-\text{O}_2$ cells where Li metal serves as the RE and CE.

As has been reported previously, the $\text{TEMPO}^+/\text{TEMPO}$ redox couple is reversible in the diglyme-based electrolyte.²⁰ However, upon oxidation in the dimethylsulfoxide (DMSO)-based electrolyte, the corresponding reduction peak is absent, suggesting that TEMPO^+ is irreversibly consumed *via* a coupled chemical reaction with DMSO. If the scan rate is increased (Fig. S3a†), partial recovery of the TEMPO^+ to TEMPO reduction peak can be observed, indicative of a finite reaction rate for TEMPO^+ consumption with DMSO. Furthermore, when the $\text{Li}[\text{TFSI}]$ concentration is increased such that the ratio of Li^+ -coordinated DMSO (less reactive, contact ion pairs) to free DMSO (solvent-separated ion pairs) increases,⁴⁹ a clear TEMPO^+ reduction peak is observed on the reverse sweep (Fig. S3b†), but the asymmetry of the peak currents confirm TEMPO^+ is still being chemically consumed. These results confirm that TEMPO^+ is unstable in DMSO-based electrolytes, undergoing decomposition reactions with the DMSO solvent. Conversely, the $\text{TEMPO}^+/\text{TEMPO}$ couple is chemically reversible in the sulfolane-based electrolyte, where the sulfur atom is in its highest oxidation state and so cannot be oxidised further, as well as in a pyrrolidinium-based ionic liquid ($[\text{Pyrr}_{13}][\text{TFSI}]$) electrolyte.

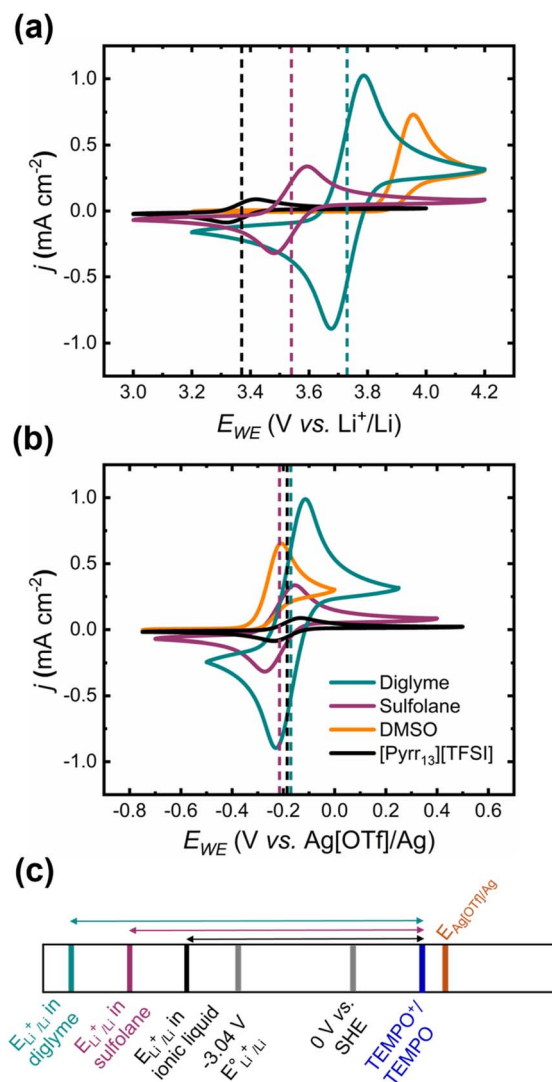


Fig. 1 Cyclic voltammograms (CVs) of 10 mM TEMPO in various electrolytes based on diglyme (cyan), sulfolane (purple), DMSO (orange) and $[\text{Pyrr}_{13}][\text{TFSI}]$ (black), with 1 M $\text{Li}[\text{TFSI}]$ as the supporting electrolyte in all systems. CVs were acquired using a glassy carbon working electrode (GC WE), Pt counter electrode (CE), and either a (a) lithium metal or (b) silver triflate/silver ($\text{Ag}[\text{OTf}]/\text{Ag}$) reference electrode (RE) at a scan rate of 50 mV s^{-1} under an Ar atmosphere. The potential scale below (c) highlights relative differences in the Li reduction potential as a function of the electrolyte and how this impacts the measured $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ values (magnitude of double-headed arrows) vs. Li^+/Li .

The redox potential of $\text{TEMPO}^+/\text{TEMPO}$ versus Li^+/Li , $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$, increases in the following order in terms of the electrolyte solvent: $[\text{Pyrr}_{13}][\text{TFSI}] < \text{sulfolane} < \text{diglyme}$ (Table 2). Assuming that changes in $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ are due to the $\text{Li}^+/\text{electrolyte}$ interface changing, this suggests that Li^+ stabilisation by solvent coordination is greatest in the diglyme-based electrolyte and lowest in $[\text{Pyrr}_{13}][\text{TFSI}]$ -based system. From a purely thermodynamic perspective, a lower $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ value that is still above the theoretical formation/decomposition potential for Li_2O_2 ($2.96 \text{ V vs. Li}^+/\text{Li}$) is favourable for low overpotential RM-mediated charging of



Table 2 Summary of $E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ in different electrolytes as determined by cyclic voltammetry using a GC WE, Pt CE and either a lithium metal or Ag[OTf]/Ag RE at a scan rate of 50 mV s^{-1} under an Ar atmosphere

Base electrolyte with 10 mM TEMPO	$E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ vs. Li^+/Li (V)	$E_{1/2}(\text{TEMPO}^+/\text{TEMPO})$ vs. Ag[OTf]/Ag (V)
1 M Li[TFSI] in diglyme	3.73	−0.17
1 M Li[TFSI] in sulfolane	3.53	−0.22
1 M Li[TFSI] in [Pyrr ₁₃][TFSI]	3.37	−0.19

Li–O₂ cells, making the ionic liquid (IL)-based electrolyte the ideal candidate system. However, the high viscosity of the neat ionic liquid (58.7 mPa s at 25 °C),⁵⁰ exacerbated further still by dissolution of Li salts, would likely result in large kinetic overpotentials in Li–O₂ cells with this electrolyte. Therefore, the efficacy of TEMPO as a charge RM was assessed in a sulfolane-based electrolyte in Li–O₂ cells, with comparison to the TEMPO-containing diglyme-based system.

First galvanostatic discharge–charge cycle and lithium peroxide yield quantification

The first cycle in Li–O₂ cells under a galvanostatic, capacity-limited cycling regime in mediated and unmediated diglyme- and sulfolane-based electrolytes with carbon black-based positive electrodes (*versus* Li metal) is shown in Fig. 2a. The “standard” Li–O₂ cell used for these experiments consisted of stainless-steel Swagelok components, with an insulating sheath within the cell body housing the electrode stack. The cell was connected to a high purity O₂ gas line to enable purging with O₂ before cycling (see Experimental for a more detailed description of the cell and Fig. S1† for images of the standard cell configuration). Cell discharge proceeds with minimal potential variation across the four electrolytes, with plateaus at *ca.* 2.70–2.75 V vs. Li^+/Li . However, there are significant differences in the charge profiles for the different electrolyte systems. Incorporating TEMPO into both electrolytes results in a significant decrease in the charge overpotential (η_{ch}); at 80% of the charge capacity limit, the unmediated electrolytes exhibit overpotentials >1 V, but introducing the TEMPO RM reduces observed η_{ch} to *ca.* 0.8 V and 0.5 V for diglyme and sulfolane-based electrolytes, respectively. However, in both mediated systems there is a sharp rise in charge potential beyond this point, which could be related to the decreasing ability of TEMPO^+ to oxidise a continually decreasing amount of Li₂O₂ left on the carbon electrode.²⁰ The lower charge overpotential in the mediated sulfolane electrolyte compared to the corresponding diglyme system is consistent with the $\text{TEMPO}^+/\text{TEMPO}$ redox potentials determined from the CVs with a Li metal RE (Fig. 1a), demonstrating that these measured redox potentials are practically relevant for mediated Li–O₂ cells.

To confirm that Li₂O₂ formed on the carbon black electrodes used, cells were discharged to 1000 mAh g^{−1} (Fig. 2b) and the extracted electrodes treated with a 1 : 1 TiOSO₄ (in H₂SO₄/H₂O) : H₂O solution. Water reacts with Li₂O₂ to form lithium hydroxide (LiOH) and hydrogen peroxide (H₂O₂). Subsequently, the Li₂O₂ yield was determined by UV-Vis spectroscopy of the resulting aliquots (Fig. 2c), quantified using a calibration curve

derived from standard solutions of Li₂O₂ in water (Fig. S2†). Across the four electrolytes, yields ranged between 70–80%, with the diglyme systems forming more Li₂O₂ than the sulfolane-based electrolytes (Table 3). The yields for the diglyme-based electrolytes are consistent with previous reports for ether-based systems.^{51,52} However, no prior reports on the application of this chemical titration method for sulfolane-based electrolytes could be found. Therefore, the reported yields in this work for the sulfolane-based systems are discussed in the context of *operando* internal cell pressure measurements later.

Current density and internal cell pressure variations

Having confirmed that Li₂O₂ is the primary discharge product, the effects of internal cell pressure and current density on discharge/charge overpotentials, discharge capacity, and cell rechargeability was evaluated. These two parameters were chosen as the former has been shown to influence discharge product morphology, and therefore, discharge/charge overpotentials,⁹ while the latter impacts oxygen diffusivity and concentration in the electrolyte.⁵³ For these parameter studies, cells were limited to 10 discharge/charge cycles under a galvanostatic, capacity-limited (1000 mAh g_c^{−1}) regime. The baseline current density and absolute internal cell pressure was 80 mA g_c^{−1} ($0.11 \pm 0.01 \text{ mA cm}^{-2}$) and 1.3 bar_A, respectively. The current density was increased to 160 mA g_c^{−1} ($0.21 \pm 0.02 \text{ mA cm}^{-2}$) and 320 mA g_c^{−1} ($0.42 \pm 0.03 \text{ mA cm}^{-2}$), and the cell pressure was varied to 1.75 and 2.2 bar_A.

Fig. 3 shows the effect of pressure variation across the four electrolytes studied in this work at cycles 1, 3, 5 and 8. Considering the unmediated diglyme electrolyte, the pressure variations have no significant effect on discharge/charge overpotentials (Fig. 3a–c) without TEMPO. The same is true for the TEMPO-mediated system (Fig. 3d–f), but at 2.2 bar_A there is an increased overpotential on charge associated with electrochemical TEMPO oxidation, which is at its greatest in cycle 10 (*ca.* 150 mV higher relative to cells cycled at 1.3 and 1.75 bar_A, Fig. S4†). This could be related to an increased driving force required for mediated Li₂O₂ oxidation into an atmosphere with a high O₂ gas concentration compared to the lower pressure measurements.

Significant differences in the discharge/charge profiles are observed as a function of pressure with the sulfolane-based electrolytes (Fig. 3g–i). In both the mediated and unmediated systems, achievable discharge capacities and rechargeability are improved with increasing pressure, which could be related to an increased dissolved O₂ concentration. Furthermore, relative to



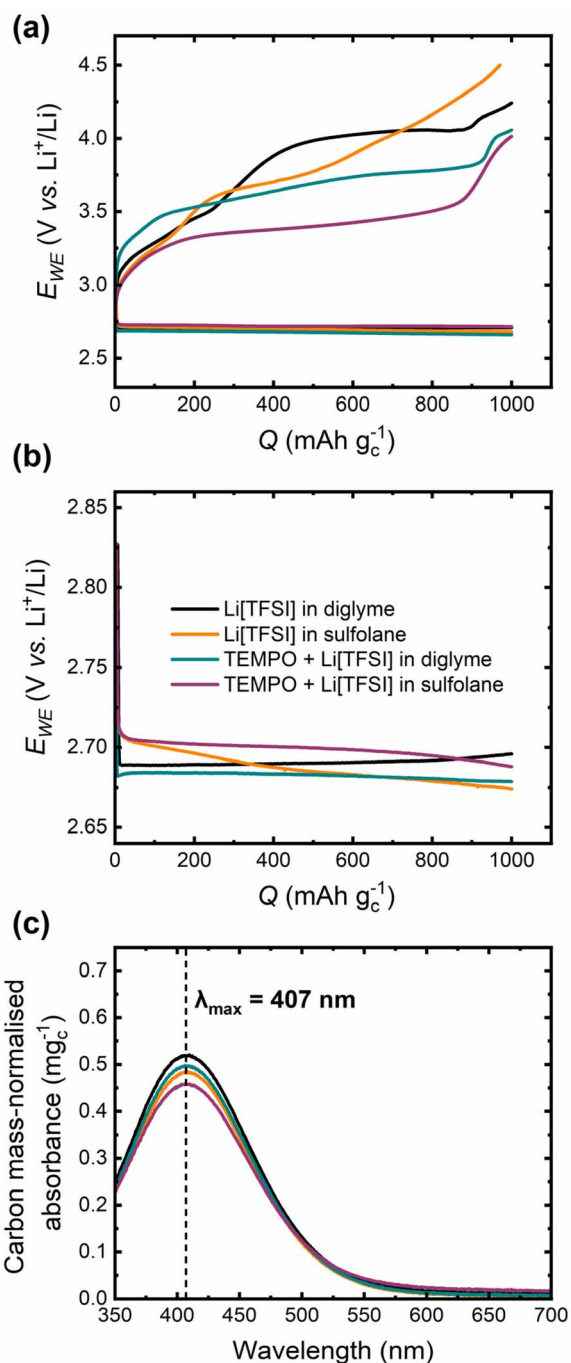


Fig. 2 (a) First capacity-limited (1000 mAh g_c⁻¹) cycle in standard Li-O₂ cells in mediated (25 mmol TEMPO kg_{solvent}⁻¹) and unmediated diglyme- and sulfolane-based electrolytes at 80 mA g_c⁻¹, where the mole fraction (x) ratio of solvent: Li[TFSI] salt was $x_{\text{solvent}} : x_{\text{Li[TFSI]}} = 9 : 1$ (see Experimental section). (b) Single 1000 mAh g_c⁻¹ discharge in the four different electrolytes at 80 mA g_c⁻¹. Electrodes from these cells were subjected to the chemical titration for Li₂O₂ yield quantification. (c) The associated UV-Vis spectra of aliquots of aqueous solutions containing the discharged electrodes treated with a 1:1 TiOSO₄ (in H₂SO_{4(aq)}): H₂O solution for determination of Li₂O₂ yield. The absorbance is normalised by the carbon black mass on the positive electrode.

Table 3 Summary of Li₂O₂ yields in mediated and unmediated diglyme- and sulfolane-based electrolytes after discharging to 1000 mAh g_c⁻¹ at 80 mA g_c⁻¹

Electrolyte	% Yield
Li[TFSI] in diglyme	80.3 ± 0.4
Li[TFSI] in sulfolane	73.8 ± 3.2
TEMPO + Li[TFSI] in diglyme	80.3 ± 3.7
TEMPO + Li[TFSI] in sulfolane	71.8 ± 1.1

the unmediated sulfolane electrolyte, rechargeability and discharge capacities are improved at all pressures with TEMPO present. Although beyond the scope of the parameter study, it is also worth noting that differences in the discharge/charge profiles across the diglyme electrolytes may occur beyond 10 cycles, whereas the capacity-fade and polarisation on charge is more severe in the sulfolane-based electrolytes, such that the influence on cyclability can be observed within 10 cycles.

Following the pressure variations, the effect of applied current density on cell cycling was explored. Fig. 4 shows the galvanostatic cycling profiles for Li-O₂ cells with unmediated and mediated diglyme- and sulfolane-based electrolytes. For the diglyme systems, discharge overpotentials (η_{dch}) increase with increasing current density. However, in cycle 1 for the unmediated diglyme electrolyte (Fig. 4a), the onset potential for Li₂O₂ oxidation on charge decreases (decreased η_{ch}) with increasing current density. This trend is consistent with previous reports and is likely a consequence of the variation in Li₂O₂ morphology formed on discharge as a function of current density. For example, Adams *et al.*⁹ demonstrated that in a Li[TFSI]-tetraethylene glycol dimethyl ether electrolyte, nanocrystalline toroidal Li₂O₂ aggregates form at low discharge rates, whereas higher current densities yield thin film-like Li₂O₂, with oxidation of the latter being more facile due to improved electrical contact with the positive electrode. However, this trend does not persist in later cycles, likely due to variations in Li₂O₂ oxidation efficiency and the accumulation of parasitic products.

The same first cycle trend is observed with the TEMPO-mediated diglyme electrolyte, with the decreasing charge onset potentials reflecting the ease with which direct electrochemical oxidation of Li₂O₂ occurs. This is not surprising as these onset potentials are below the oxidation plateau ascribed to electrochemical TEMPO oxidation. Thus, mediated Li₂O₂ oxidation is not expected to be the dominant process at this stage since TEMPO is not expected to affect the discharge process significantly. In cycles 5 and 10, charge overpotentials increase with increasing current density. For the potential plateau at ca. 3.6–3.8 V vs. Li⁺/Li (depending on cycle number and current density), ascribed to electrochemical TEMPO oxidation to TEMPO⁺, the increase in overpotentials with current density could be due to cell potential being under mass transport control, *i.e.*, diffusion of TEMPO to the carbon electrode, and the accumulation of parasitic products at this electrode.^{23,24} The capacity contribution of the TEMPO oxidation

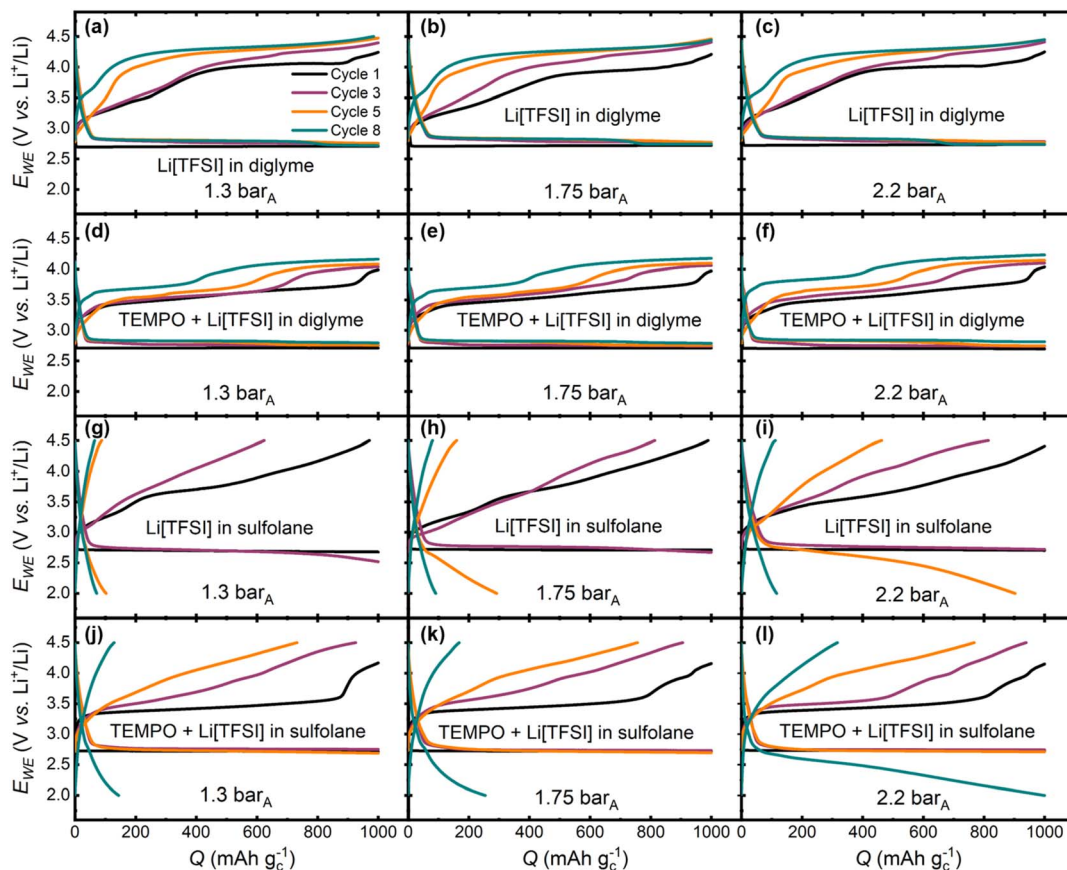


Fig. 3 Galvanostatic (80 mA g_c^{-1}), capacity-limited ($1000 \text{ mAh g}_c^{-1}$) cycles 1 (black), 3 (purple), 5 (orange) and 8 (cyan) of Li–O₂ cells sealed at internal O₂ gas pressures of 1.3, 1.75 and 2.2 bar_A for (a–c) Li[TFSI]-diglyme, (d–f) TEMPO-Li[TFSI]-diglyme, (g–i) Li[TFSI]-sulfolane and (j–l) TEMPO-Li[TFSI]-sulfolane electrolytes. See Fig. S4–7† for all cycles across the four electrolytes. [TEMPO] = $25 \text{ mmol}_{\text{TEMPO}} \text{ kg}_{\text{solvent}}^{-1}$, $x_{\text{solvent}} : x_{\text{Li}}(\text{TFSI}) = 9 : 1$, where x = mole fraction.

plateau decreases on cycling with a higher potential plateau (at *ca.* 3.8–4.3 V vs. Li⁺/Li depending on current density) making up the difference. As has been reported previously, the growth of this higher potential plateau is related to increasing decomposition of parasitic products,²⁰ which eventually contributes to *ca.* 60% of the total charge capacity by cycle 10, suggesting accumulation of parasitic products on cycling.

In the sulfolane-based electrolytes (Fig. 4g–l), discharge and charge overpotentials increase with increasing current density across all cycles with and without TEMPO. This is likely due to the higher viscosity of sulfolane (10.6 mPa s at 30°C)⁵⁴ compared to diglyme (1.1 mPa s at 20°C),⁵⁵ and therefore, mass transport of all species required for Li₂O₂ formation/decomposition govern cell potential from the first cycle. It is also important to note that incorporation of TEMPO improves achievable discharge capacities and rechargeability across all current densities, relative to the unmediated electrolyte. At 80 and 160 mA g_c^{-1} , in the TEMPO-mediated system, the sharp rise in potential towards the end of charge in cycle 1 likely reflects the challenge of oxidising small amounts of Li₂O₂, as was observed in the mediated diglyme electrolyte. However, at 320 mA g_c^{-1} , the rise in potential is not as steep and initiates at *ca.*

50% of the charge capacity. As this increase in overpotential occurs midway through the charge step, it cannot be explained by a decreasing amount of Li₂O₂. Instead, it is likely a combined effect of (i) kinetic overpotentials induced by the diffusion limitations of TEMPO in the more viscous sulfolane-based electrolyte, and (ii) an increasing proportion of direct electrochemical oxidation of Li₂O₂ at this higher rate.

Across both diglyme- and sulfolane-based electrolytes, there is also the possibility of the rate of reaction between TEMPO⁺ and Li₂O₂ not being fast enough to sustain the applied current density, thus resulting in the observed polarisation on charge. However, Chen and co-workers have demonstrated that mediated Li₂O₂ oxidation kinetics can sustain areal current densities on the order of 100 mA cm^{-2} , more than $250\times$ greater than the highest equivalent areal current density applied in this work, at charge overpotentials $<0.1 \text{ V}$ based on a model of a porous electrode filled with Li₂O₂.³⁵ Importantly, nitroxide-based RMs exhibited the highest apparent reaction rates for Li₂O₂ oxidation by RM⁺ across the tested RMs. Therefore, it is concluded that this factor is not a major source of polarisation on charge at higher rates. The differences in electrochemical behaviour between the diglyme- and sulfolane-based electrolytes as a function of current density and O₂

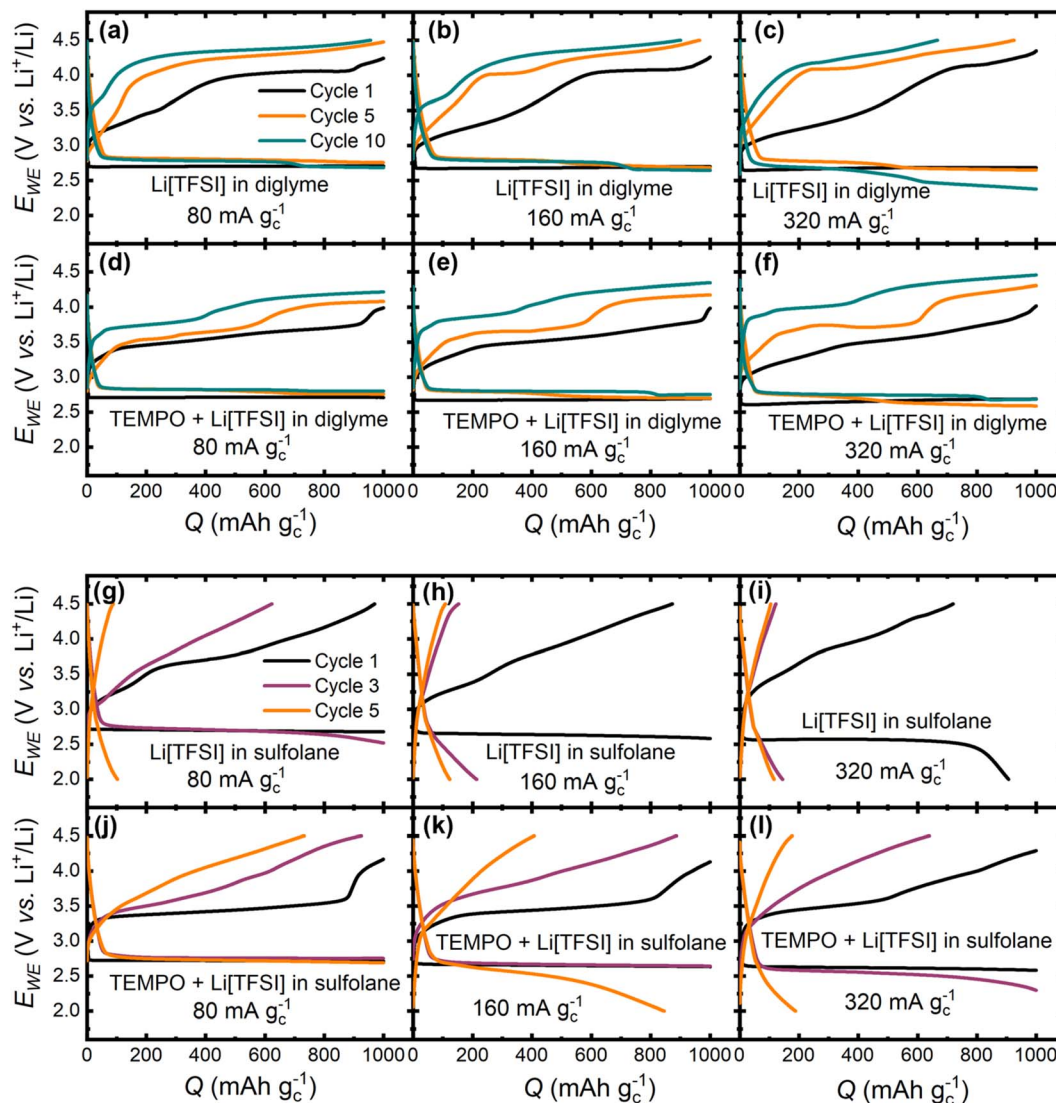


Fig. 4 Galvanostatic, capacity-limited (1000 mAh g^{-1}) cycles of $\text{Li}-\text{O}_2$ cells at varying current densities: 80, 160 and 320 mA g_c^{-1} . For (a–c) $\text{Li}[\text{TFSI}]$ -diglyme and (d–f) $\text{TEMPO}+\text{Li}[\text{TFSI}]$ -diglyme electrolytes cycles 1 (black), 5 (orange) and 10 (cyan) are shown, and, due to the lower cyclability of sulfolane electrolytes relative to diglyme systems, cycles 1 (black), 3 (purple) and 5 (orange) are presented for (g–i) $\text{Li}[\text{TFSI}]$ -sulfolane and (j–l) $\text{TEMPO}+\text{Li}[\text{TFSI}]$ -sulfolane electrolytes. All cells were sealed at 1.3 bar_A . See Fig. S8–11† for all cycles across the four electrolytes. $[\text{TEMPO}] = 25 \text{ mmol TEMPO kg}_{\text{solvent}}^{-1}$, $x_{\text{solvent}} : x_{\text{Li}[\text{TFSI}]} = 9 : 1$, where x = mole fraction.

pressure emphasizes the challenge and importance of optimising cycling parameters for $\text{Li}-\text{O}_2$ cells, as the optimal parameters depend strongly on the physicochemical properties of the electrolyte, which can vary significantly between solvent families.

Operando pressure measurements for assessing RM efficacy

The parameter studies discussed in the previous section provide useful insights into the effects of current density and internal cell pressure variations as a function of electrolyte. However, these galvanostatic profiles do not provide a complete picture of the electrochemical reactions occurring in the cell, particularly when charging TEMPO -mediated cells. Additionally, although the UV-Vis titration approach (Fig. 2b and c) confirms the formation of Li_2O_2 in all electrolytes used in this work, this approach is limited by the destructive nature of the electrode

treatment and does not consider any Li_2O_2 that is lost during electrode extraction and/or consumed after formation through parasitic reactions (e.g., formation of Li_2CO_3 by reaction of Li_2O_2 with the carbon electrode).^{17,18} Furthermore, the chemical titration approach becomes impractical to study Li_2O_2 yield beyond the first discharge, as the incomplete oxidation of Li_2O_2 on the subsequent charge means that Li_2O_2 yield determination on, for example, the second discharge would include Li_2O_2 left on the electrode after the first charge. Therefore, an online approach is required to study the $\text{Li}-\text{O}_2$ cell under *operando* conditions. Here, an *operando* pressure-electrochemical cell (hereafter referred to as “pressure cell”) was built using Swagelok parts to monitor internal pressure within the cell headspace over the entire lifetime of the cell, from which the efficacy of TEMPO as a charge RM can be deduced as a function of the



electrolyte. The cell headspace was interfaced with a high accuracy pressure transducer, enabling highly sensitive tracking of small pressure changes (<5 mbar) in response to changes in the electrochemical cycling profile. Importantly, *operando* pressure measurements serve as a complimentary, readily accessible technique in the Li–O₂ cell diagnostic toolkit, further strengthened by the RM efficacy analysis involving correlation of differential capacity with cell pressure changes as described later. A schematic of the cell (Fig. S11†), details of the cell volume calibration (Fig. S12–14†) and a description of the pressure cell data processing procedure (ESI Note 1 and Fig. S15†) are provided in the ESI.† The electrolyte volume (80 μ L) and dimensions of the carbon black-based positive electrode used was identical to the ‘standard’ Swagelok-type Li–O₂ cells used for cell cycling experiments where pressure was not measured. This was done to ensure flooding factors, defined as the ratio of electrolyte volume to active electrode area of the positive electrode, are comparable between the standard and pressure cells (*ca.* 6.3 ± 0.6 nL cm^{−2}, calculated using the BET specific surface area of the carbon black material used in this work (Ketjenblack EC-600JD, 1270 m² g^{−1}) and a carbon black loading of 1.0 ± 0.1 mg). Unlike with other *operando* methods, where often entirely different cell designs are required (*e.g.*, DEMS), this pressure cell enables Li–O₂ chemistry to be studied under conditions directly comparable to the standard cell.

Fig. 5 shows the first four cycles in the pressure cell with the mediated diglyme- and sulfolane-based electrolytes, wherein the cell potential (top panels), headspace pressure variation (middle panels) and first derivative of the pressure response (bottom panels) are shown as a function of time. In both mediated systems, during the discharge plateau at *ca.* 2.7 V *vs.* Li⁺/Li there is a decrease in pressure, consistent with the consumption of O₂ gas for the ORR. Charging of Li–O₂ cells relies on a coupled chemical oxidation wherein electrochemical RM oxidation to RM⁺ is followed by RM⁺ oxidation of Li₂O₂, regenerating RM and evolving O₂ gas. Therefore, it is essential to verify whether this coupled chemical oxidation takes place, and if so, how it evolves from cycle to cycle, particularly when studying novel RM-containing electrolyte formulations. Importantly, this information cannot be explicitly determined from the galvanostatic cycling profiles alone. As Fig. 5b shows, the TEMPO oxidation plateau in the first charge half-cycle in the sulfolane system coincides with gas pressure increase, confirming that the coupled-chemical oxidation process (*i.e.*, RM⁺ + Li₂O₂ → RM + 2Li⁺ + O_{2(gas)}) is occurring. A similar response is observed in the mediated diglyme system, however, the charge overpotential is greater in the first three charge steps.

Using the ideal gas law and the calibrated cell volume, the average electron-to-gas mole ratio (ne^-/n_{gas}) can be estimated. Here, ‘average’ refers to ne^-/n_{gas} values calculated based on the

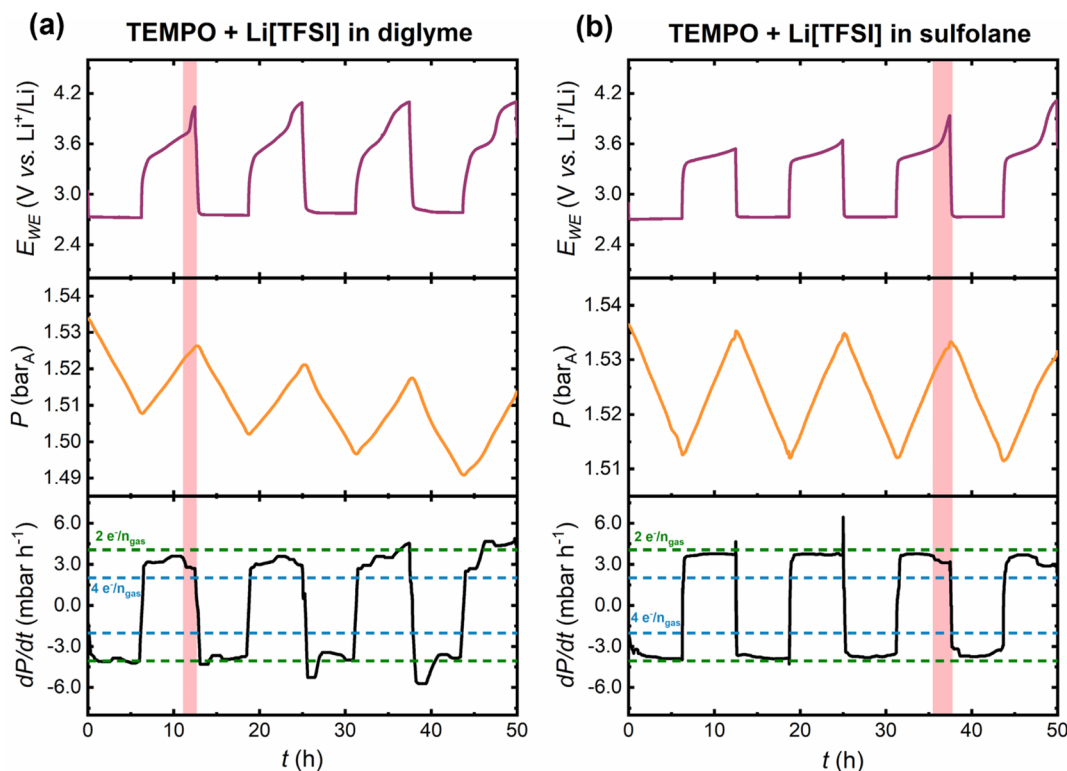


Fig. 5 Cycles 1–4 in the pressure cells cycled under a capacity-limited (500 mAh g^{−1}) regime at 80 mA g^{−1} in TEMPO-mediated (a) diglyme- and (b) sulfolane-based electrolytes. The RM loading was 25 mmol_{TEMPO} kg_{solvent}^{−1} and the mole fraction (*x*) ratio of solvent : Li[TFSI] salt was *x*_{solvent} : *x*_{Li[TFSI]} = 9 : 1. The cell potential (purple), pressure response (orange) and first derivative of the pressure response (black) are shown as a function of time. The dotted green and blue lines indicate the theoretical gas consumption/evolution rates for 2e[−]/*n*_{gas} and 4e[−]/*n*_{gas} processes, respectively. The red shaded regions highlight the sensitivity of the pressure measurement, capturing drops in gas evolution rate that coincide with sharp rises in cell potential, which serve as a marker for decreased RM efficacy.



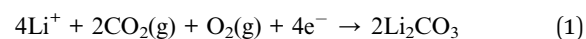
total pressure change for a discharge/charge half-cycle (see ESI Note 2† for example calculations). For the desired two-electron ORR and OER, the ideal ne^-/n_{gas} value should correspond to 2 moles of electrons per mole of gas consumed/evolved ($2e^-/n_{\text{gas}}$), assuming that all the gas being evolved is O_2 and that the only $2e^-/n_{\text{gas}}$ processes are 2-electron ORR and OER. For example, in the first discharge half-cycle, the average ne^-/n_{gas} is calculated as 2.06 and 2.09 in the mediated diglyme and sulfolane systems, respectively. This is consistent with the overpotentials on discharge being almost identical. However, in the subsequent charge half-cycle, there is greater polarisation in the mediated diglyme cell as compared to the sulfolane electrolyte; the former polarises to *ca.* 4 V *vs.* Li^+/Li , whereas the latter remains below 3.6 V *vs.* Li^+/Li . Consequently, the deviation in the average ne^-/n_{gas} ratio for the entire charge step from the ideal value of $2e^-/n_{\text{gas}}$ is greater in the mediated diglyme electrolyte ($2.55e^-/n_{\text{gas}}$) relative to the mediated sulfolane-based electrolyte ($2.14e^-/n_{\text{gas}}$).

During charging of mediated $\text{Li}-\text{O}_2$ cells, sharp rises in potential are observed, which deviates significantly from the charge plateau ascribed to electrochemical RM oxidation. As described earlier, this may be related to the difficulty in mediated oxidation of small amounts of Li_2O_2 left on the carbon electrode and oxidation of parasitic products. This effect is exacerbated on cycling, with a decreasing capacity contribution to the total charge capacity stemming from the TEMPO oxidation plateau, as was observed during cycling in standard $\text{Li}-\text{O}_2$ cells (Fig. 3 and 4). Fig. 5a shows a transition point (see red shaded region) wherein a sharp rise in potential in the 1st charge half-cycle in the mediated diglyme electrolyte, results in a decrease in the slope of the pressure response. This can be clearly seen in the first derivative plots (dP/dt) showing instantaneous gas consumption/evolution rates and the corresponding ideal rates. The ideal rates were calculated as follows (see ESI Note 3† for example calculations): using the cell volume, the pressure change for consumption/evolution of a known amount (moles) of gas was calculated. As a fixed capacity limit and current density was applied, the time required for a single discharge/charge is known, and therefore, the theoretical gas consumption/evolution rate can be determined. The deviation in the instantaneous gas evolution rate from the ideal rate for a $2e^-/n_{\text{gas}}$ process is indicative of the extent of parasitic chemistry. Crucially, tracking instantaneous gas consumption/evolution rates provides information on when during a given charge half cycle RM efficacy is diminished, which cannot be understood solely from average ne^-/n_{gas} values. A sharp rise in potential is also observed in the 3rd charge half-cycle in the mediated sulfolane system (Fig. 5b). In both mediated electrolytes, the instantaneous gas evolution rates decrease during these sharp potential increases (Fig. 5, red highlighted regions), indicating that $ne^-/n_{\text{gas}} > 2$, demonstrating that the pressure cell can be used to accurately correlate small changes in cycling behaviour, providing insight into transition points in a half-cycle where RM functionality is reduced.

In cycles 1–4 in both electrolytes, discharge proceeds close to the $2e^-/n_{\text{gas}}$ gas consumption rate. However, charging proceeds closer to the $2e^-/n_{\text{gas}}$ gas evolution rate in the mediated sulfolane electrolyte, which is consistent with the lower charge

overpotentials measured in this system. Furthermore, comparing the first four cycles in the corresponding unmediated electrolytes in the pressure cell (Fig. S16a†) with the mediated systems reveals some important differences. While instantaneous gas consumption/evolution rates do not differ significantly in the unmediated and mediated diglyme electrolytes, the overpotentials on charge are reduced with TEMPO present. Incorporation of TEMPO into the sulfolane-based electrolytes brings the instantaneous gas evolution rates closer to the ideal rate with at least a 0.3 V decrease in charge overpotentials in the first four cycles (Fig. 5b and S16b†). However, the question remains how the electrochemical behaviour and pressure responses observed in early cycles evolve with continued cell cycling.

Fig. 6 shows cycles 5–8 in the pressure cell with the mediated electrolytes, where distinct differences in the discharge–charge profiles and associated gas consumption/evolution rates are observed. Firstly, on discharge in the mediated diglyme electrolyte, there is a significant overconsumption of gas, that is, $ne^-/n_{\text{gas}} < 2$. This overconsumption of gas in diglyme-based electrolytes has been reported previously by Lepoivre *et al.* suggesting that a discharge reaction involving both O_2 and CO_2 consumption was taking place (eqn (1)).⁴⁴



Eqn (1) would result in a ne^-/n_{gas} ratio of 1.33 and is consistent with the formation of Li_2CO_3 due to decomposition reactions associated with the carbon electrode (in contact with Li_2O_2) and the electrolyte.^{17,18} Subsequently, at high charging potentials (>4 V *vs.* Li^+/Li), Li_2CO_3 is electrochemically oxidised evolving CO_2 , which is then present to be consumed in the following discharge reaction as described in eqn (1). It should be noted that this cannot be explicitly confirmed with pressure cell data alone, as direct chemical information cannot be extracted from this approach. It is likely that two or more discharge reactions are occurring simultaneously, including the desired 2-electron ORR forming Li_2O_2 . The overconsumption of gas is independent of whether TEMPO is present or not in the diglyme electrolyte, as demonstrated by the pressure cell measurements reported in this work in the unmediated electrolyte (Fig. S17a†), consistent with previous reports.⁴⁴ Conversely, in the mediated sulfolane electrolyte, cell discharge proceeds more consistently close to the $2e^-/n_{\text{gas}}$ gas consumption rate. Again, comparison to the corresponding unmediated sulfolane system (Fig. S16b and S17b†) shows that this behaviour is independent of TEMPO, suggesting that the $\text{Li}[\text{TFSI}]$ -sulfolane electrolyte is a better medium for facilitating the 2-electron ORR than the $\text{Li}[\text{TFSI}]$ -diglyme electrolyte under these conditions.

On charging in cycles 5–8, the instantaneous gas evolution rates in the mediated and unmediated diglyme electrolytes are consistently above the $2e^-/n_{\text{gas}}$ rate (*i.e.*, overproduction of gas, $ne^-/n_{\text{gas}} < 2$), whereas in the mediated sulfolane-based electrolyte the gas evolution rate is largely below the $2e^-/n_{\text{gas}}$ rate ($ne^-/n_{\text{gas}} > 2$), indicating that the nature of parasitic reactions is



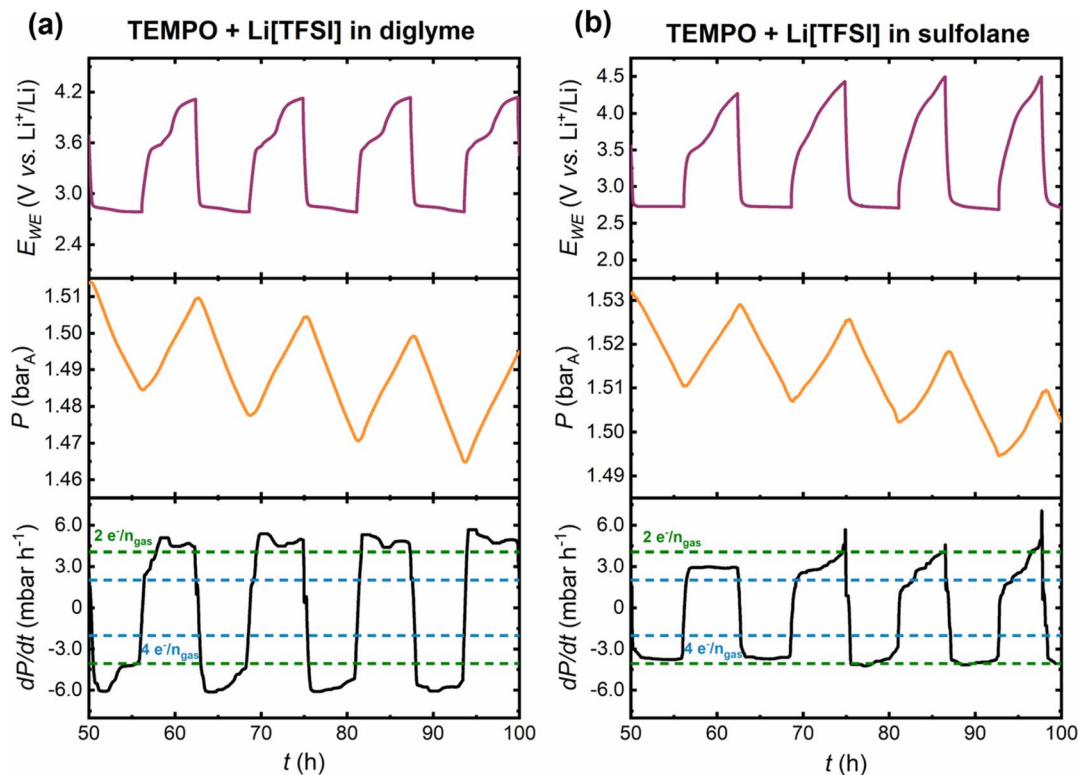


Fig. 6 Cycles 5–8 of the pressure cells with TEMPO-mediated (a) diglyme- and (b) sulfolane-based electrolytes. The RM loading was $25 \text{ mmol}_{\text{TEMPO}} \text{ kg}_{\text{solvent}}^{-1}$ and the mole fraction (x) ratio of solvent : $\text{Li}[\text{TFSI}]$ salt was $x_{\text{solvent}} : x_{\text{Li}[\text{TFSI}]}$ = 9 : 1. The cell potential (purple), pressure response (orange) and first derivative of the pressure response (black) are shown as a function of time. The dotted green and blue lines indicate the theoretical gas consumption/evolution rates for $2\text{e}^-/\text{n}_{\text{gas}}$ and $4\text{e}^-/\text{n}_{\text{gas}}$ processes, respectively.

different. In the mediated diglyme electrolyte, the deviation from the ideal gas evolution rate is attributed to a decreasing capacity contribution from the TEMPO oxidation plateau and oxidation of parasitic products evolving other gases in addition to O_2 (e.g., CO_2 from Li_2CO_3 oxidation).²⁰ The successive loss of TEMPO functionality is even more severe in the sulfolane-based electrolytes; comparing the unmediated (Fig. S17b†) and mediated sulfolane electrolytes (Fig. 6b) shows that by cycle 6

the cell potential and instantaneous gas evolution profiles appear similar. This comparison shows that any indication of electrochemical TEMPO oxidation is lost. Therefore, $\text{Li}-\text{O}_2$ cells with sulfolane-based electrolytes have a shorter lifetime than diglyme systems, exhibiting more severe polarisation on charge and capacity-fade due to build-up of parasitic products. The loss of the TEMPO oxidation plateau in the sulfolane electrolyte may be related to parasitic product accumulation blocking

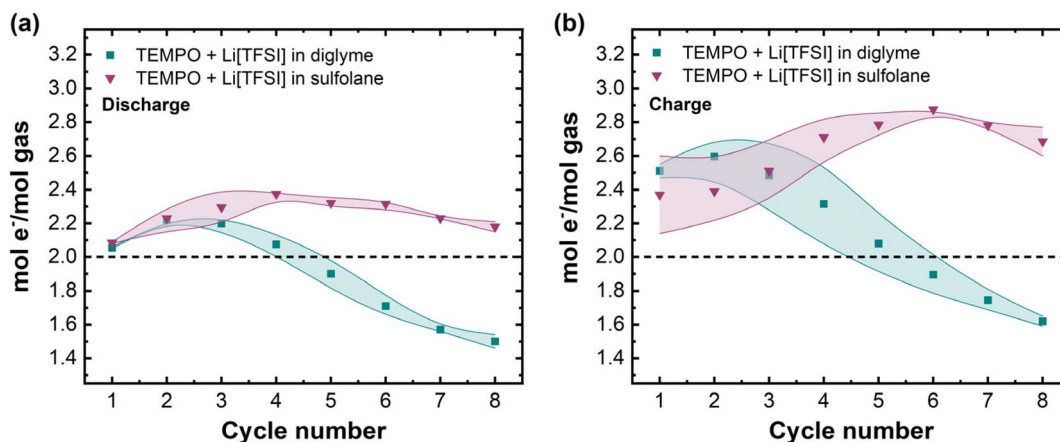


Fig. 7 Average electron-to-gas mole ratios for mediated diglyme- and sulfolane-based electrolytes during (a) discharge and (b) charge over 8 discharge/charge cycles. Data points represent average $ne^-/\text{n}_{\text{gas}}$ values calculated for two cells per electrolyte and the shaded areas represent absolute uncertainty between measurements. The black dotted line shows the ideal ratio of $2\text{e}^-/\text{n}_{\text{gas}}$.

electrochemically active sites on the carbon electrode and/or TEMPO decomposition during cycling.

A key parasitic product that has been reported in both diglyme- and sulfolane-based electrolytes is Li_2CO_3 .^{17,39} Bardé *et al.* suggested Li_2CO_3 accumulation as the cause for the rapid capacity fade in unmediated sulfolane electrolytes, as detected by infrared spectroscopy and powder X-ray diffraction on cycled carbon and nanoporous gold (NPG) positive electrodes.³⁹ Despite the improved oxidative stability of NPG electrodes, Li_2CO_3 accumulation was still observed, highlighting electrolyte

solvent decomposition as a route towards this parasitic product. Furthermore, the reactivity of Li_2O_2 formed may change as a function of the electrolyte; Li_2O_2 formed in the sulfolane-based system could be more reactive in this electrolyte environment than that formed in the diglyme system, which is consistent with the lower Li_2O_2 yields shown in Fig. 2 for the former. Such differences in Li_2O_2 reactivity depending on the electrolyte solvent have previously been reported for electrolytes based on dimethoxyethane (DME), DMSO and tetraglyme, where discharging in DMSO and tetraglyme-based systems gave

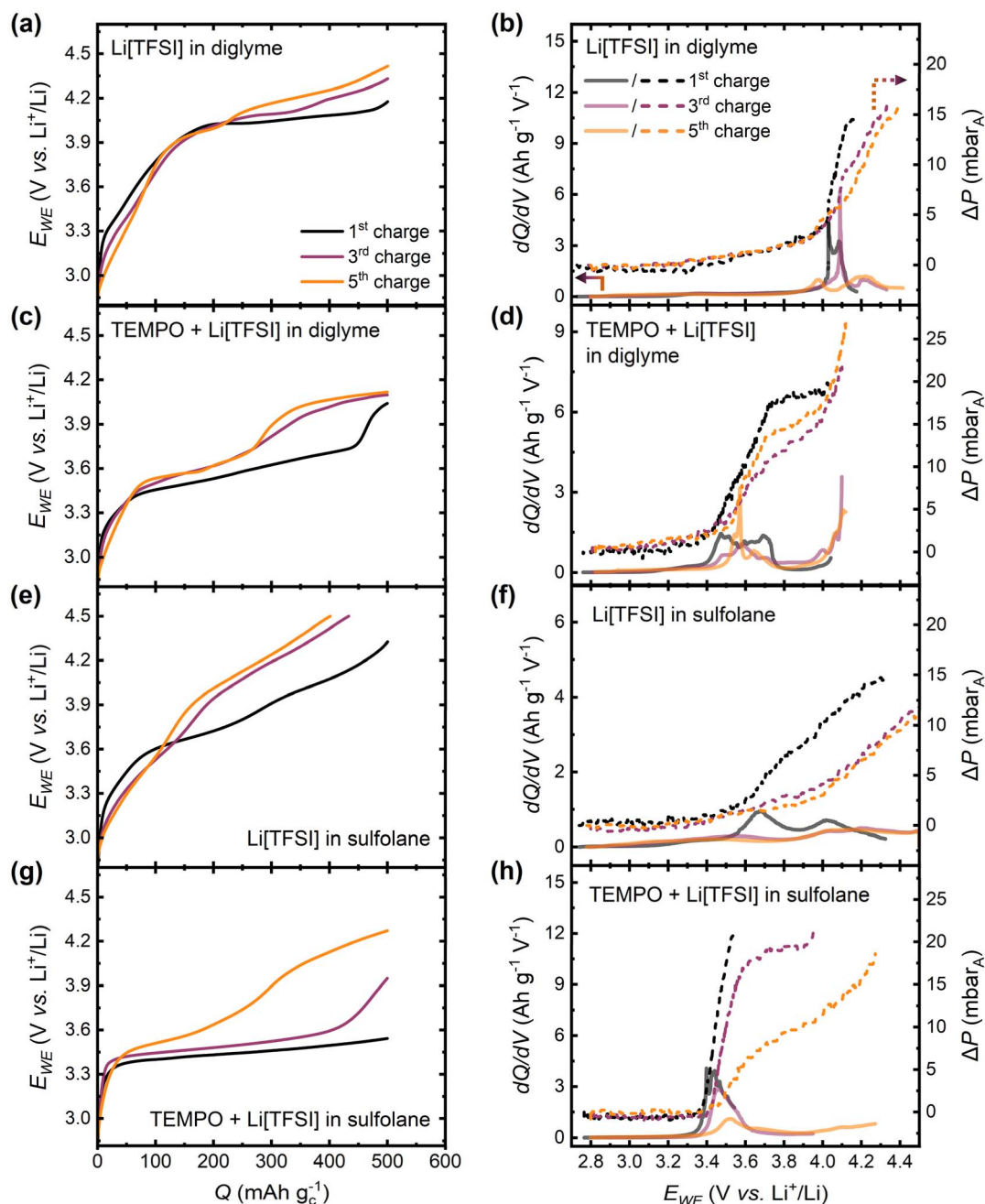


Fig. 8 (a, c, e and g) Galvanostatic charging profiles and (b, d, f and h) differential capacity (dQ/dV , solid lines) and change in pressure (ΔP , dotted lines) as a function of cell potential in the 1st, 3rd and 5th charge half-cycles in (a and b) Li[TFSI]-diglyme and (c and d) TEMPO-Li[TFSI]-diglyme electrolytes, (e and f) Li[TFSI]-sulfolane and (g and h) TEMPO-Li[TFSI]-sulfolane electrolytes. The pressure at the start of each charge half-cycle is defined as $\Delta P = 0$.



lower Li_2O_2 yields compared to discharge in DME-based electrolytes.⁵⁶

The instantaneous gas consumption/evolution rates are useful to identify and correlate transition points in cell potential to changes in the dynamic pressure response, particularly during mediated cell charge. Importantly, such transition points cannot be discerned by considering only the average ne^-/n_{gas} ratio per half-cycle. However, the evolution of average ne^-/n_{gas} values over successive cycles can provide useful insight into whether the extent of parasitic chemistry grows from cycle to cycle. Fig. 7 shows the average ne^-/n_{gas} ratio calculated for each discharge/charge half-cycle over a total of 8 cycles.

In cycle 1, in the mediated diglyme electrolyte, average $ne^-/n_{\text{gas}} = 2.06 \pm 0.01$, and after an initial rise, decreases to $1.50 \pm 0.04e^-/n_{\text{gas}}$. This is consistent with the overconsumption of gas observed in the instantaneous gas consumption rates (Fig. 6) for this electrolyte and shows that this overconsumption becomes more severe on cycling, *i.e.*, the continual decrease in ne^-/n_{gas} is indicative of the extent of parasitic chemistry increasing with every cycle. In contrast, in the mediated sulfolane system, $ne^-/n_{\text{gas}} = 2.09 \pm 0.01$ in cycle 1, and then ranges between 2.18 ± 0.03 to $2.38 \pm 0.01e^-/n_{\text{gas}}$, indicating that while there is still a deviation from the ideal value of $2e^-/n_{\text{gas}}$, the extent of parasitic chemistry on discharge does not grow as quickly relative to the mediated diglyme electrolyte. For the charge half-cycles, decrease in ne^-/n_{gas} is again observed for the diglyme system, starting at $2.51 \pm 0.04e^-/n_{\text{gas}}$ and decreasing to $1.62 \pm 0.03e^-/n_{\text{gas}}$ by cycle 8, which supports previous reports of CO_2 evolution (in addition to O_2 evolution) from Li_2CO_3 oxidation in ether-based electrolytes.^{17,18} In the sulfolane electrolyte, ne^-/n_{gas} increases from $2.37 \pm 0.23e^-/n_{\text{gas}}$ (cycle 1) to a maximum of $2.88 \pm 0.01e^-/n_{\text{gas}}$ (cycle 6). Therefore, in the mediated sulfolane system, the increasing extent of parasitic chemistry during cell charging is likely the cause for the severe capacity fade.

The pressure cell data discussed above (Fig. 5–7) demonstrates that this technique can be used to assess RM efficacy using the instantaneous gas consumption/evolution profiles. This understanding is essential given the likelihood that a practical, viable Li-O_2 battery will require RMs for operation.^{57,58} Furthermore, the pressure cell also provides an indication of trends in parasitic chemistry over successive cycles. Further analysis was used to correlate cell potential changes with maximal gas evolution by plotting the change in cell pressure (ΔP) and differential capacity (dQ/dV) as functions of cell potential. This methodology is useful for close inspection to identify over what potential ranges the majority of gas evolution occurs, providing insight into the cycle-to-cycle evolution of RM activity loss.

Fig. 8 shows dQ/dV and ΔP as functions of cell potential, alongside galvanostatic charging profiles, for charge half-cycles 1, 3 and 5 in mediated and unmediated diglyme and sulfolane-based electrolytes. Compared to the mediated electrolytes, the unmediated systems (Fig. 8b and f) exhibit gas evolution in cycle 1 at higher charging overpotentials and over considerably wider potential ranges. This is consistent with the mechanism of mediated *vs.* unmediated charging of Li-O_2 cells; in the case where no TEMPO is present, Li_2O_2 is primarily decomposed by

electrochemical oxidation, for which large overpotentials are required. In contrast, with TEMPO present (Fig. 8d and h), only electrochemical oxidation of TEMPO (occurring at lower charge overpotentials) is required to subsequently initiate chemical oxidation of Li_2O_2 by TEMPO^+ .

The progression of these gas evolution and dQ/dV profiles over a series of charge steps also provides another useful test for RM efficacy in Li-O_2 cells. In cycles 3 and 5, in both mediated electrolytes, the loss in capacity of the TEMPO oxidation plateau in the galvanostatic charging profiles (Fig. 8c and g) results in gas evolution that occurs over a wider potential range (Fig. 8d and h), instead of being localised around the dQ/dV peak at the potential corresponding to TEMPO oxidation as seen in cycle 1. This is similar to what is observed in the corresponding unmediated electrolytes from the very first cycle (Fig. 8b and f), which suggests that the mechanism of charging shifts from mediated charging where Li_2O_2 oxidation is achieved primarily *via* chemical oxidation by TEMPO^+ , to a combination with electrochemical oxidation of Li_2O_2 and/or accumulated parasitic products (*e.g.*, Li_2CO_3). This emphasizes the importance of RMs that can also oxidise parasitic species for longer life Li-O_2 cells.⁵⁹ Furthermore, the loss of a distinct peak in gas evolution over cycles 1, 3, and 5 is more exacerbated in the mediated sulfolane-based electrolyte compared to the mediated diglyme-based system, consistent with the poorer rechargeability in the former upon cycling. Based on data shown in Fig. 8, some key requirements for an effective RM can be deduced. It is important that for as many charge half-cycles as possible, (i) the dQ/dV peak is centred around the RM oxidation potential (*i.e.* minimise RM oxidation plateau capacity fade) and (ii) the majority of the coupled gas evolution should be centred around the dQ/dV peak corresponding to the RM oxidation potential. Therefore, using readily accessible *operando* pressure measurements, the cell pressure change-differential capacity analysis provides a useful approach to screen RMs for the above requirements, aiding in the establishment of structure–activity relationships that are critical to the design of more effective mediators.

Conclusion

In conclusion, *operando* pressure measurement during galvanostatic cycling of Li-O_2 cells has been shown to be a versatile technique for assessing RM efficacy. For unexplored mediated electrolyte formulations, it is particularly useful to verify that the charging reaction proceeds *via* coupled chemical oxidation of Li_2O_2 (mediated by RM^+) to evolve O_2 gas. While this may be inferred from differences in cell potential profiles during cycling, this was confirmed during charging of Li-O_2 cells with a TEMPO-mediated sulfolane-based electrolyte in this work. In early cycles with this electrolyte, the charge potential plateau ascribed to electrochemical TEMPO oxidation occurred at a lower potential compared to the mediated diglyme electrolyte, consistent with the redox potentials *versus* Li metal for the $\text{TEMPO}^+/\text{TEMPO}$ couple measured by cyclic voltammetry. Although cycling at higher O_2 pressures improved achievable discharge capacities and rechargeability in sulfolane-based systems, capacity-fade was still more severe in this system



compared to diglyme-based electrolytes. In both mediated systems, sharp rises in potential were observed during cell charging and loss of the TEMPO oxidation plateau was more rapid in the sulfolane-based electrolyte.

Interfacing a high accuracy, fast response time pressure transducer with the Li–O₂ cell headspace enabled these rises in potential to be related to gas evolution to understand when, in a given charging step, the efficacy of the RM is diminished. The technique provides a straightforward, non-destructive/non-invasive methodology to extract the evolution of average and instantaneous ne^-/n_{gas} ratios over many cycles, critical for a viable Li–O₂ cell and understanding RM activity and stability. In-depth analyses demonstrated that cycle-to-cycle growth in parasitic chemistry on discharge was more severe in the mediated diglyme system, associated with an overconsumption of gas, as compared to the mediated sulfolane-based electrolyte. However, ne^-/n_{gas} ratios on charging in the sulfolane systems deviate significantly from ideal, approaching $3e^-/n_{\text{gas}}$, which is thought to be the primary cause for capacity fade in this electrolyte system. This was corroborated by the evolution of both differential capacity and pressure profiles as functions of the cell potential over a series of charge half-cycles. From these data, it was established that TEMPO is most effective when the majority of gas evolution is confined to a narrow potential window that centres around its redox potential in the given electrolyte. Maximising the number of cycles for which this type of response can be sustained will improve cell rechargeability and lifetime.

By combining differential capacity plots and *operando* pressure data, this analysis approach can be applied to any electrode–electrolyte combination, making it a versatile method for screening RM-containing electrolyte formulations. This is of timely importance for the Li–O₂ battery research field, where high throughput/(semi)automated synthesis of novel RMs could be used to generate large libraries of candidate mediators, which will then require readily accessible methods for RM efficacy testing under *operando* conditions. Therefore, in the pursuit of longer-life Li–O₂ cells, this methodology utilising on-line, highly sensitive pressure measurements in conjunction with data processing/analysis methods described herein is a valuable technique for assessing RM stability to identify and support the design of new promising RMs/electrolyte formulations.

Data availability

The data supporting this article have been included as part of the ESI.†

Author contributions

TS: conceptualisation, formal analysis, investigation, supervision, methodology, writing original draft manuscript, review and editing, and visualisation. BW: investigation, and formal analysis. ARN: conceptualisation, investigation, supervision, methodology, writing manuscript, review, and editing, and visualisation. EC: review and editing of manuscript. DJS: review

and editing of manuscript. LJH: conceptualisation, funding acquisition, project administration, supervision, writing manuscript, review, and editing.

Conflicts of interest

The authors have no conflicts of interest to declare.

Acknowledgements

TS acknowledges Lubrizol Ltd for providing PhD funding and funding for the work presented in this article. All authors acknowledge Dr Tyler Petek (Lubrizol Ltd, Wickliffe, Ohio, 44092, US) for constructive discussions on the manuscript. LH and AN acknowledge Engineering and Physical Sciences (EPSRC) Research Council funding (EP/R020744/1) that supported the development of the *operando* pressure cell.

References

- 1 P. G. Bruce, S. A. Freunberger, L. J. Hardwick and J.-M. Tarascon, Li–O₂ and Li–S batteries with high energy storage, *Nat. Mater.*, 2012, **11**, 19–29.
- 2 D. Aurbach, B. D. McCloskey, L. F. Nazar and P. Bruce, Advances in understanding mechanisms underpinning lithium–air batteries, *Nat. Energy*, 2016, **1**, 16128.
- 3 T. Liu, J. P. Vivek, E. W. Zhao, J. Lei, N. Garcia-Araez and C. P. Grey, Current Challenges and Routes Forward for Nonaqueous Lithium–Air Batteries, *Chem. Rev.*, 2020, **120**, 6558–6625.
- 4 L. Johnson, C. Li, Z. Liu, Y. Chen, S. A. Freunberger, P. C. Ashok, B. B. Praveen, K. Dholakia, J.-M. Tarascon and P. G. Bruce, The role of LiO₂ solubility in O₂ reduction in aprotic solvents and its consequences for Li–O₂ batteries, *Nat. Chem.*, 2014, **6**, 1091–1099.
- 5 N. B. Aetukuri, B. D. McCloskey, J. M. García, L. E. Krupp, V. Viswanathan and A. C. Luntz, Solvating additives drive solution-mediated electrochemistry and enhance toroid growth in non-aqueous Li–O₂ batteries, *Nat. Chem.*, 2015, **7**, 50–56.
- 6 C. O. Laoire, S. Mukerjee, K. M. Abraham, E. J. Plichta and M. A. Hendrickson, Elucidating the Mechanism of Oxygen Reduction for Lithium–Air Battery Applications, *J. Phys. Chem. C*, 2009, **113**, 20127–20134.
- 7 B. D. McCloskey, R. Scheffler, A. Speidel, G. Girishkumar and A. C. Luntz, On the Mechanism of Nonaqueous Li–O₂ Electrochemistry on C and Its Kinetic Overpotentials: Some Implications for Li–Air Batteries, *J. Phys. Chem. C*, 2012, **116**, 23897–23905.
- 8 G. A. Attard, P. G. Bruce, E. J. Calvo, Y. Chen, L. A. Curtiss, D. Dewar, J. H. J. Ellison, J. Fernández-Vidal, S. A. Freunberger, X. Gao, C. P. Grey, L. J. Hardwick, G. Horwitz, J. Janek, L. R. Johnson, E. Jónsson, S. Karunarathne, S. Matsuda, S. Menkin, S. Mondal, S. Nakanishi, N. Ortiz-Vitoriano, Z. Peng, J. P. Rivera, I. Temprano, K. Uosaki, E. D. Wachsmann, Y. Wu and S. Ye,



- Mechanism of ORR and OER in non-aqueous electrolytes: general discussion, *Faraday Discuss.*, 2024, **248**, 210–249.
- 9 B. D. Adams, C. Radtke, R. Black, M. L. Trudeau, K. Zaghib and L. F. Nazar, Current density dependence of peroxide formation in the Li–O₂ battery and its effect on charge, *Energy Environ. Sci.*, 2013, **6**, 1772.
 - 10 B. Horstmann, B. Gallant, R. Mitchell, W. G. Bessler, Y. Shao-Horn and M. Z. Bazant, Rate-Dependent Morphology of Li₂O₂ Growth in Li–O₂ Batteries, *J. Phys. Chem. Lett.*, 2013, **4**, 4217–4222.
 - 11 C. M. Burke, V. Pande, A. Khetan, V. Viswanathan and B. D. McCloskey, Enhancing electrochemical intermediate solvation through electrolyte anion selection to increase nonaqueous Li–O₂ battery capacity, *Proc. Natl. Acad. Sci. U. S. A.*, 2015, **112**, 9293–9298.
 - 12 D. Sharon, D. Hirsberg, M. Salama, M. Afri, A. A. Frimer, M. Noked, W. Kwak, Y.-K. Sun and D. Aurbach, Mechanistic Role of Li⁺ Dissociation Level in Aprotic Li–O₂ Battery, *ACS Appl. Mater. Interfaces*, 2016, **8**, 5300–5307.
 - 13 I. Gunasekara, S. Mukerjee, E. J. Plichta, M. A. Hendrickson and K. M. Abraham, A Study of the Influence of Lithium Salt Anions on Oxygen Reduction Reactions in Li–Air Batteries, *J. Electrochem. Soc.*, 2015, **162**, A1055–A1066.
 - 14 S. Meini, M. Piana, N. Tsiouvaras, A. Garsuch and H. A. Gasteiger, The Effect of Water on the Discharge Capacity of a Non-Catalyzed Carbon Cathode for Li–O₂ Batteries, *Electrochem. Solid-State Lett.*, 2012, **15**, A45.
 - 15 Y. Wang, N.-C. Lai, Y.-R. Lu, Y. Zhou, C.-L. Dong and Y.-C. Lu, A Solvent-Controlled Oxidation Mechanism of Li₂O₂ in Lithium–Oxygen Batteries, *Joule*, 2018, **2**, 2364–2380.
 - 16 S. Ganapathy, B. D. Adams, G. Stenou, M. S. Anastasaki, K. Goubitz, X.-F. Miao, L. F. Nazar and M. Wagemaker, Nature of Li₂O₂ Oxidation in a Li–O₂ Battery Revealed by Operando X-ray Diffraction, *J. Am. Chem. Soc.*, 2014, **136**, 16335–16344.
 - 17 B. D. McCloskey, A. Speidel, R. Scheffler, D. C. Miller, V. Viswanathan, J. S. Hummelshøj, J. K. Nørskov and A. C. Luntz, Twin Problems of Interfacial Carbonate Formation in Nonaqueous Li–O₂ Batteries, *J. Phys. Chem. Lett.*, 2012, **3**, 997–1001.
 - 18 M. M. Ottakam Thotiyl, S. A. Freunberger, Z. Peng and P. G. Bruce, The Carbon Electrode in Nonaqueous Li–O₂ Cells, *J. Am. Chem. Soc.*, 2013, **135**, 494–500.
 - 19 T. A. Galloway, G. Attard and L. J. Hardwick, An electrochemical investigation of oxygen adsorption on Pt single crystal electrodes in a non-aqueous Li⁺ electrolyte, *Electrochem. Commun.*, 2020, **119**, 106814.
 - 20 B. J. Bergner, A. Schürmann, K. Peppler, A. Garsuch and J. Janek, TEMPO: A Mobile Catalyst for Rechargeable Li–O₂ Batteries, *J. Am. Chem. Soc.*, 2014, **136**, 15054–15064.
 - 21 X. Gao, Y. Chen, L. Johnson and P. G. Bruce, Promoting solution phase discharge in Li–O₂ batteries containing weakly solvating electrolyte solutions, *Nat. Mater.*, 2016, **15**, 882–888.
 - 22 Y. Chen, S. A. Freunberger, Z. Peng, O. Fontaine and P. G. Bruce, Charging a Li–O₂ battery using a redox mediator, *Nat. Chem.*, 2013, **5**, 489–494.
 - 23 A. Tkacheva, B. Sun, J. Zhang, G. Wang and A. M. McDonagh, Nitronyl Nitroxide-Based Redox Mediators for Li–O₂ Batteries, *J. Phys. Chem. C*, 2021, **125**, 2824–2830.
 - 24 A. Tkacheva, J. Zhang, B. Sun, D. Zhou, G. Wang and A. M. McDonagh, TEMPO-Ionic Liquids as Redox Mediators and Solvents for Li–O₂ Batteries, *J. Phys. Chem. C*, 2020, **124**, 5087–5092.
 - 25 D. Kundu, R. Black, B. Adams and L. F. Nazar, A Highly Active Low Voltage Redox Mediator for Enhanced Rechargeability of Lithium–Oxygen Batteries, *ACS Cent. Sci.*, 2015, **1**, 510–515.
 - 26 J. Zhang, B. Sun, Y. Zhao, A. Tkacheva, Z. Liu, K. Yan, X. Guo, A. M. McDonagh, D. Shanmukaraj, C. Wang, T. Rojo, M. Armand, Z. Peng and G. Wang, A versatile functionalized ionic liquid to boost the solution-mediated performances of lithium–oxygen batteries, *Nat. Commun.*, 2019, **10**, 602.
 - 27 K. P. C. Yao, J. T. Frith, S. Y. Sayed, F. Bardé, J. R. Owen, Y. Shao-Horn and N. Garcia-Araez, Utilization of Cobalt Bis(terpyridine) Metal Complex as Soluble Redox Mediator in Li–O₂ Batteries, *J. Phys. Chem. C*, 2016, **120**, 16290–16297.
 - 28 W.-J. Kwak, A. Mahammed, H. Kim, T. T. Nguyen, Z. Gross, D. Aurbach and Y.-K. Sun, Controllable and stable organometallic redox mediators for lithium oxygen batteries, *Mater. Horiz.*, 2020, **7**, 214–222.
 - 29 S. Matsuda, S. Mori, K. Hashimoto and S. Nakanishi, Transition Metal Complexes with Macrocyclic Ligands Serve as Efficient Electrocatalysts for Aprotic Oxygen Evolution on Li₂O₂, *J. Phys. Chem. C*, 2014, **118**, 28435–28439.
 - 30 H.-D. Lim, H. Song, J. Kim, H. Gwon, Y. Bae, K.-Y. Park, J. Hong, H. Kim, T. Kim, Y. H. Kim, X. Lepró, R. Ovalle-Robles, R. H. Baughman and K. Kang, Superior Rechargeability and Efficiency of Lithium–Oxygen Batteries: Hierarchical Air Electrode Architecture Combined with a Soluble Catalyst, *Angew. Chem.*, 2014, **126**, 4007–4012.
 - 31 W.-J. Kwak, D. Hirshberg, D. Sharon, M. Afri, A. A. Frimer, H.-G. Jung, D. Aurbach and Y.-K. Sun, Li–O₂ cells with LiBr as an electrolyte and a redox mediator, *Energy Environ. Sci.*, 2016, **9**, 2334–2345.
 - 32 C. K. Lee and Y. J. Park, CsI as Multifunctional Redox Mediator for Enhanced Li–Air Batteries, *ACS Appl. Mater. Interfaces*, 2016, **8**, 8561–8567.
 - 33 J. Liu, Y. Li, Y. Ding, L. Wu, J. Qin, T. Chen, C. Meng, F. Zhou, X. Ma and Z. Wu, A Bifunctional Imidazolyl Iodide Mediator of Electrolyte Boosts Cathode Kinetics and Anode Stability Towards Low Overpotential and Long-Life Li–O₂ Batteries, *Angew. Chem., Int. Ed.*, 2025, e202421107.
 - 34 H. Lee, J. Hwang, J. Kim, G. N. Morais, K. S. Tang, M. Choi, H. Choi, H. Youn, S. Kim, J. H. Ha, S. J. Kang, S. Chen, S. Suh and W. Kwak, Reactive Oxygen Species Resistive Redox Mediator in Lithium–Oxygen Batteries, *Adv. Mater.*, 2025, 2415805.
 - 35 Y. Chen, X. Gao, L. R. Johnson and P. G. Bruce, Kinetics of lithium peroxide oxidation by redox mediators and consequences for the lithium–oxygen cell, *Nat. Commun.*, 2018, **9**, 767.



- 36 B. J. Bergner, C. Hofmann, A. Schürmann, D. Schröder, K. Peppler, P. R. Schreiner and J. Janek, Understanding the fundamentals of redox mediators in Li–O₂ batteries: a case study on nitroxides, *Phys. Chem. Chem. Phys.*, 2015, **17**, 31769–31779.
- 37 M. J. Trahan, S. Mukerjee, E. J. Plichta, M. A. Hendrickson and K. M. Abraham, Studies of Li–Air Cells Utilizing Dimethyl Sulfoxide-Based Electrolyte, *J. Electrochem. Soc.*, 2013, **160**, A259–A267.
- 38 D. Xu, Z. Wang, J. Xu, L. Zhang, L. Wang and X. Zhang, A stable sulfone based electrolyte for high performance rechargeable Li–O₂ batteries, *Chem. Commun.*, 2012, **48**, 11674.
- 39 F. Bardé, Y. Chen, L. Johnson, S. Schaltin, J. Fransaer and P. G. Bruce, Sulfone-Based Electrolytes for Nonaqueous Li–O₂ Batteries, *J. Phys. Chem. C*, 2014, **118**, 18892–18898.
- 40 G. A. Elia, J. Hassoun, W.-J. Kwak, Y.-K. Sun, B. Scrosati, F. Mueller, D. Bresser, S. Passerini, P. Oberhumer, N. Tsiouvaras and J. Reiter, An Advanced Lithium–Air Battery Exploiting an Ionic Liquid-Based Electrolyte, *Nano Lett.*, 2014, **14**, 6572–6577.
- 41 S. Das, J. Højberg, K. B. Knudsen, R. Younesi, P. Johansson, P. Norby and T. Vegge, Instability of Ionic Liquid-Based Electrolytes in Li–O₂ Batteries, *J. Phys. Chem. C*, 2015, **119**, 18084–18090.
- 42 N. Ryall and N. Garcia-Araez, Highly Sensitive Operando Pressure Measurements of Li-ion Battery Materials with a Simply Modified Swagelok Cell, *J. Electrochem. Soc.*, 2020, **167**, 110511.
- 43 J. P. Vivek and N. Garcia-Araez, Differences in Interfacial Reactivity of Graphite and Lithium Metal Battery Electrodes Investigated Via Operando Gas Analysis, *J. Phys. Chem. C*, 2024, **128**, 13395–13401.
- 44 F. Lepoivre, A. Grimaud, D. Larcher and J.-M. Tarascon, Long-Time and Reliable Gas Monitoring in Li–O₂ Batteries via a Swagelok Derived Electrochemical Cell, *J. Electrochem. Soc.*, 2016, **163**, A923–A929.
- 45 V. Giordani, D. Tozier, H. Tan, C. M. Burke, B. M. Gallant, J. Uddin, J. R. Greer, B. D. McCloskey, G. V. Chase and D. Addison, A Molten Salt Lithium–Oxygen Battery, *J. Am. Chem. Soc.*, 2016, **138**, 2656–2663.
- 46 P. Hartmann, C. L. Bender, M. Vracar, A. K. Dürr, A. Garsuch, J. Jürgen and P. Adelhelm, A rechargeable room-temperature sodium superoxide (NaO₂) battery, *Nat. Mater.*, 2013, **12**, 228–232.
- 47 B. B. Berkes, A. Jozwiuk, M. Vračar, H. Sommer, T. Brezesinski and J. Janek, Online Continuous Flow Differential Electrochemical Mass Spectrometry with a Realistic Battery Setup for High-Precision, Long-Term Cycling Tests, *Anal. Chem.*, 2015, **87**, 5878–5883.
- 48 G. A. Snook, A. S. Best, A. G. Pandolfo and A. F. Hollenkamp, Evaluation of a Ag|Ag⁺ reference electrode for use in room temperature ionic liquids, *Electrochem. Commun.*, 2006, **8**, 1405–1411.
- 49 A. R. Neale, R. Sharpe, S. R. Yeandel, C. Yen, K. V. Luzyanin, P. Goddard, E. A. Petruccio and L. J. Hardwick, Design Parameters for Ionic Liquid–Molecular Solvent Blend Electrolytes to Enable Stable Li Metal Cycling Within Li–O₂ Batteries, *Adv. Funct. Mater.*, 2021, **31**, 2010627.
- 50 Technical Data Sheet 1-Propyl-1-methylpyrrolidinium bis(trifluoromethylsulfonyl)imide, <https://iolitec.de/en/node/319>, 2022, date accessed: 25/03/2025.
- 51 X. Gao, Y. Chen, L. R. Johnson, Z. P. Jovanov and P. G. Bruce, A rechargeable lithium–oxygen battery with dual mediators stabilizing the carbon cathode, *Nat. Energy*, 2017, **2**, 17118.
- 52 M. Jenkins, D. Dewar, M. Lagnoni, S. Yang, G. J. Rees, A. Bertei, L. R. Johnson, X. Gao and P. G. Bruce, A High Capacity Gas Diffusion Electrode for Li–O₂ Batteries, *Adv. Mater.*, 2024, **36**, 2405715.
- 53 B. A. B. Francisco, J. P. O. Júlio, C. G. Anchieta, T. C. M. Nepel, R. M. Filho and G. Doubek, Systematic Study of O₂ Supply in Li–O₂ Batteries with High and Low Donor Number Solvents, *ACS Appl. Energy Mater.*, 2023, **6**, 5167–5176.
- 54 M. Fan, K. Liu, Q. Liu, T. Zhang, L. Lv and S. Tang, Surface Tension and Viscosity of Ternary Mixtures of *N*-Methyldiethanolamine + Sulfolane + Water, *J. Chem. Eng. Data*, 2022, **67**, 2215–2224.
- 55 R. J. Lewis, *Hawley's Condensed Chemical Dictionary*, John Wiley & Sons, New York, 14th edn, 2001.
- 56 B. D. McCloskey, A. Valery, A. C. Luntz, S. R. Gowda, G. M. Wallraff, J. M. Garcia, T. Mori and L. E. Krupp, Combining Accurate O₂ and Li₂O₂ Assays to Separate Discharge and Charge Stability Limitations in Nonaqueous Li–O₂ Batteries, *J. Phys. Chem. Lett.*, 2013, **4**, 2989–2993.
- 57 L. J. Hardwick, Concluding remarks: a summary of the Faraday Discussion on rechargeable non-aqueous metal–oxygen batteries, *Faraday Discuss.*, 2024, **248**, 412–422.
- 58 J. W. Jordan, G. Vailaya, C. Holc, M. Jenkins, R. C. McNulty, C. Puscatau, B. Tokay, A. Laybourn, X. Gao, D. A. Walsh, G. N. Newton, P. G. Bruce and L. R. Johnson, A lithium–air battery and gas handling system demonstrator, *Faraday Discuss.*, 2024, **248**, 381–391.
- 59 M. Jenkins, D. Dewar, T. Nimmo, C. Chau, X. Gao and P. G. Bruce, The accumulation of Li₂CO₃ in a Li–O₂ battery with dual mediators, *Faraday Discuss.*, 2024, **248**, 318–326.

