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Ligand-induced changes in the electrocatalytic activity of atomically precise Au₂₅ nanoclusters†

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Atomically precise gold nanoclusters have shown great promise as model electrocatalysts in pivotal electrocatalytic processes such as the hydrogen evolution reaction (HER) and carbon dioxide reduction reaction (CO₂RR). Although the influence of ligands on the electronic properties of these nanoclusters is well acknowledged, the ligand effects on their electrocatalytic performances have been rarely explored. Herein, using [Au₂₅(SR)₁₈][−] nanoclusters as a prototype model, we demonstrated the importance of ligand hydrophilicity versus hydrophobicity in modulating the interface dynamics and electrocatalytic performance. Our first-principles calculations revealed that Au₂₅ protected by hydrophilic −SCH₂COOH ligands exhibits faster kinetics in stripping the thiolate ligand and better HER activity due to enhanced proton transfer facilitated by boosted interface hydrogen bonding. Conversely, Au₂₅ protected by hydrophobic −SCH₂CH₃ ligands demonstrates enhanced CO₂RR performance by minimizing water interference to stabilize the key *COOH intermediate and lower the barrier for CO formation. Experimental validation using synthesized hydrophilic and hydrophobic ligand-protected Au₂₅ nanoclusters (NCs), such as [Au₂₅(MPA)₁₈][−] (MPA = mercaptopropionic acid), [Au₂₅(MHA)₁₈][−] (MHA = 6-mercaptopentanoic acid), and [Au₂₅(SC₆H₁₃)₁₈][−], confirms these findings, where the hydrophilic ligand-protected Au₂₅ NCs exhibit better activity and stability in the HER, while the hydrophobic ligand-protected Au₂₅ NCs achieve higher faradaic efficiency and current density in the CO₂RR. The mechanistic insights in this study provide valuable guidance for the rational design of surface microenvironments in efficient nanocatalysts for sustainable energy applications.

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1. Introduction

The electrocatalytic reactions such as the hydrogen evolution reaction (HER)^{1–4} and carbon dioxide reduction reaction (CO₂RR) have been considered cornerstones in the pursuit of sustainable ways of meeting global energy demands.^{5–7} These reactions are critical for the production of clean energy and recycling of carbon, as they enable the conversion of CO₂ into valuable chemicals and fuels and generate hydrogen as a clean energy carrier.^{8,9} Given the importance of these processes, the development of highly efficient and stable catalysts for both the CO₂RR and HER is of paramount importance. Atomically precise metal nanoclusters (NCs), renowned for their unique structures and molecule-like properties, have shown exceptional catalytic capabilities due to their quantum confinement effects and a high density of active

sites.^{10–18} Among these, [Au₂₅(SR)₁₈][−] NCs have been particularly recognized for their significant electrocatalytic activities in both CO₂ reduction^{12,19–22} and hydrogen evolution.^{23–27} The pioneering work by Kauffman *et al.*²⁸ first highlighted the ability of [Au₂₅(SR)₁₈][−] to efficiently reduce CO₂ to CO with high selectivity and low overpotential at commercially viable current densities, establishing the potential of these nanoclusters in electrocatalysis. The bimetallic PtAu₂₄(SR)₁₈ NCs, explored by Kwak *et al.*,²⁹ demonstrated remarkable catalytic activity for hydrogen production in the HER, surpassing previously reported molecular catalysts and even outperforming traditional platinum catalysts, setting a new benchmark in the field.

In the context of Au₂₅ NCs, the choice and nature of ligands are critical factors that significantly influence their stability and catalytic performance. Ligands act as the outer protective layers, not only preventing aggregation and stabilizing the nanocluster, but also modulating its electronic properties and surface chemistry.^{26,30–35} The thiol-based ligands, in particular, are widely used due to their strong S–metal bonds, which provide high stability and a straightforward preparation strategy.^{36–38} However, beyond the stabilization effect, the intrinsic properties of the ligands—such as their hydrophilicity or hydrophobicity—can profoundly affect the nanocluster's interaction with reactants and

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its overall electrocatalytic activity.³⁹ For instance, Kwak *et al.*²⁵ investigated the impact of different ligands on the HER performance and found that the 3-mercaptopropionic acid (MPS) protected Au₂₅ NC achieved a rate constant of 121 000 s⁻¹ at an overpotential of 0.7 V, which was 11 times higher than that of 1-hexanethiolate (C₆S) protected Au₂₅, highlighting the profound influence of ligand hydrophilicity on catalytic efficiency. Moreover, recent work by Yoo *et al.*⁴⁰ has shown that the introduction of hydrophobic ligands in a silver nanocluster Ag₂₅ can enhance the CO₂ reduction activity, achieving a faradaic efficiency for CO (FE_{CO}) of over 90% and a partial current density (*j*_{CO}) as high as -240 mA cm⁻² in a gas-fed membrane electrode assembly device. Despite these experimental advancements, atomic-level understanding and elucidation of the specific effects of hydrophilic versus hydrophobic ligands on the electrocatalytic performance of atomically precise NCs have been lacking. This uncertainty underscores the urgent need for a systematic investigation into how the ligand properties influence these catalytic processes. In particular, understanding these interactions is crucial for further optimizing the performance of Au₂₅ NCs and could also provide valuable insights into the rational design of nanocluster-based electrocatalysts for sustainable energy applications.

In this work, we systematically investigated the ligand effect on the interface stability and the electrocatalytic performance of Au₂₅ NCs in both acidic HER and alkaline CO₂RR processes. Utilizing hydrophilic [Au₂₅(SCH₂COOH)₁₇]⁻ and hydrophobic [Au₂₅(SCH₂CH₃)₁₇]⁻ NCs as theoretical models, we first explored how the ligand properties influence the Au-S interface dynamics, the electronic structures, and the electrocatalytic reaction kinetics *via* the constant potential calculations and *ab initio* molecular dynamics (AIMD) simulations. The results revealed that the Au-S interface is unstable at the applied electrochemical reduction potential, and hydrophilic [Au₂₅(SCH₂COOH)₁₇]⁻ exhibits faster kinetics for the stripping of the -SR ligand. Moreover, in the acidic environment, hydrophilic Au₂₅ NCs exhibit superior HER performance compared to the hydrophobic one due to the enhanced proton transfer and hydrogen evolution facilitated by the hydrophilic environment. Conversely, under alkaline conditions, hydrophobic Au₂₅ NCs show better CO₂RR activity by promoting the adsorption and stabilization of CO₂ intermediates while minimizing the water interference around the reaction interface. Our theoretical predictions are then validated through the experimental studies, where we synthesized mercaptopropionic acid-protected [Au₂₅(MPA)₁₈]⁻, 6-mercaptopropionic acid-protected [Au₂₅(MHA)₁₈]⁻, and hexanethiol-protected [Au₂₅(SC₆H₁₃)₁₈]⁻ NCs as model systems and performed the electrochemical tests. These insights provide a deeper understanding of how the ligand environments affect the electrocatalytic activities of Au₂₅ nanoclusters and offer valuable guidance for the rational design of promising nanocatalysts for electrocatalytic applications.

2. Results and discussion

Ligand detachment dynamics

The removal of surface ligands from nanoclusters is a critical step in enhancing their electrocatalytic activity. Fully ligand-

protected nanoclusters, such as Au₂₅(SR)₁₈, are typically considered electrochemically inactive and exhibit significant overpotential during the electrocatalytic process.^{20,41-44} This inactivity is primarily caused by the passivating effect of the ligands, which block the access of reactants to the metal core and hinder the efficient mass and charge transfer between the nanocluster and the reactants.^{45,46} Consequently, the selective removal of ligands from specific sites on the nanocluster surface is necessary to expose the active sites. Our recent studies have provided valuable insights into the mechanism of partial ligand removal in Au₂₅(SCH₃)₁₈ NCs, where the applied reduction potential would induce the spontaneous desulfurization process *via* breaking the Au-S bonds regardless of the electrolyte environment (acidic, neutral or basic conditions).⁴⁷

Building on these prior findings, we first combined the constant potential calculations and AIMD simulations to explore how the presence of surface hydrophilic and hydrophobic ligands affects the stability of the Au-S interface under acidic electrochemical conditions. We modeled Au₂₅ NCs with ligands aligned along the z-axis, simulating the system in both explicit water slabs and an implicit solvation environment to accurately capture the realistic electrochemical conditions. Our theoretical model includes hydrophilic [Au₂₅(CH₂COOH)₁₈]⁻ and hydrophobic [Au₂₅(CH₂CH₃)₁₈]⁻ NCs (illustrated in Fig. S2†) placed in the simulation box filled with bulk water at an average density of approximately 1 g cm⁻³, which comprises 191 H₂O molecules and one H₃O⁺ ion to simulate the acidic environment.⁴⁸ To explicitly consider the electrode potential, we manually adjusted the number of extra electrons to control the applied potential *U* (more details on the constant potential calculations can be found in the ESI†). Our AIMD simulations at room temperature (300 K) revealed that the -SR ligands on both the [Au₂₅(CH₂COOH)₁₈]⁻ and [Au₂₅(CH₂CH₃)₁₈]⁻ NCs become unstable when subjected to the applied potential. In the dynamic process, the proton from the solvated H₃O⁺ ion is attracted and adsorbed onto the sulfur atom, weakening the Au-S bonds. When the potential becomes sufficiently negative, this weakening leads to the complete breakage of the Au-S bonds and the formation of the HSR molecule, as illustrated in the AIMD snapshots (Fig. 1, left). Specifically, in the case of [Au₂₅(CH₂CH₃)₁₈]⁻ NCs, the potential (*U*_{RHE} = -1.36 V) was not negative enough to facilitate proton adsorption onto the sulfur atom, leading instead to proton transfer and diffusion into the solvent (details provided in Fig. S3†). In contrast, when a lower potential (*U*_{RHE} = -1.54 V) was applied, the Au-S bonds in [Au₂₅(CH₂CH₃)₁₈]⁻ NCs were completely broken (Fig. 1b).

Fig. 1a illustrates the dynamic behavior of [Au₂₅(SCH₂COOH)₁₈]⁻ NC at an applied potential of *U*_{RHE} = -0.98 V at 300 K in an acidic environment (pH = 0). The Au¹(surface)-S²⁶ bond first rapidly breaks at around 0.12 ps with the spontaneous proton adsorption at the S site. The Au⁸(staple)-S²⁶ bond then breaks at 4.54 ps, which oscillates, reattaches, and completely breaks again at 7.25 ps, leading to bond dissociation thereafter. This eventually results in the detachment of two Au-S bonds, and in the meantime, the -SR ligand combines with a proton to desorb and dissolve into the solution as a HSCH₂COOH molecule. A similar -SR detachment process occurs for



$[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$, respectively. These plots were obtained by calculating the N_e-U and $U-G$ relationships (additional details are provided in Fig. S5†). The results indicate that the first step of the HER, the Volmer reaction, is thermodynamically favorable across the entire potential range, as evidenced by ΔG values consistently below zero. This suggests that the adsorption of protons onto the nanocluster surface with exposed Au sites occurs spontaneously. However, the second step of the HER, the Heyrovsky reaction—which involves the formation of H_2 —exhibits ΔG values greater than zero when the potential is not sufficiently negative. As the potential becomes more negative, the ΔG values gradually decrease, eventually falling below zero, indicating that the formation of H_2 becomes thermodynamically favorable only at more negative potentials. Therefore, these constant potential thermodynamic calculations lead us to conclude that, for both $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$, the formation of H_2 in the second step of the HER (Heyrovsky reaction) is the rate-determining step.

While thermodynamic calculations provide valuable insights into the feasibility of reaction steps, they often overlook the kinetic barriers that determine the rate at which these reactions proceed. To address this, we employed the slow-growth method within the framework of constrained kinetics to calculate the energy barriers associated with the rate-determining step of the HER for both $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$. Fig. 2c and d depict the energy barriers as a function of the constrained variable (CV) (Fig. S1†) at an applied potential of -0.66 V. As the constraint increases, the energy barrier

increases until it peaks at the point where two hydrogen atoms—one adsorbed at the Au bridge site and the other from H_3O^+ in the water environment—combine to form H_2 and then desorb. The analysis of the reaction pathway shows that the $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ system reaches this maximum energy barrier earlier, with a free energy of 0.42 eV, indicating a lower energy requirement for the rate-determining step. In contrast, at a similar potential, the energy barrier for the HER rate-determining step in the $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ system is higher, at 0.54 eV. These results suggest that the hydrophilic $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ nanocluster exhibits superior HER performance compared to the hydrophobic $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ nanocluster. The lower kinetic barrier in the hydrophilic $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ system facilitates a more efficient hydrogen evolution reaction. This improved performance can be attributed to the enhanced interaction between the hydrophilic ligands and the surrounding aqueous environment, which promotes the formation and desorption of H_2 , thereby making the HER process more favorable in $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$.

CO_2RR performance in an alkaline environment

We further evaluated the CO_2RR performance of dethiolated $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ by constant potential thermodynamic and kinetic calculations. The CO_2RR performance testing was carried out under alkaline conditions at $\text{pH} = 14$. Note that the alkaline environments are favorable

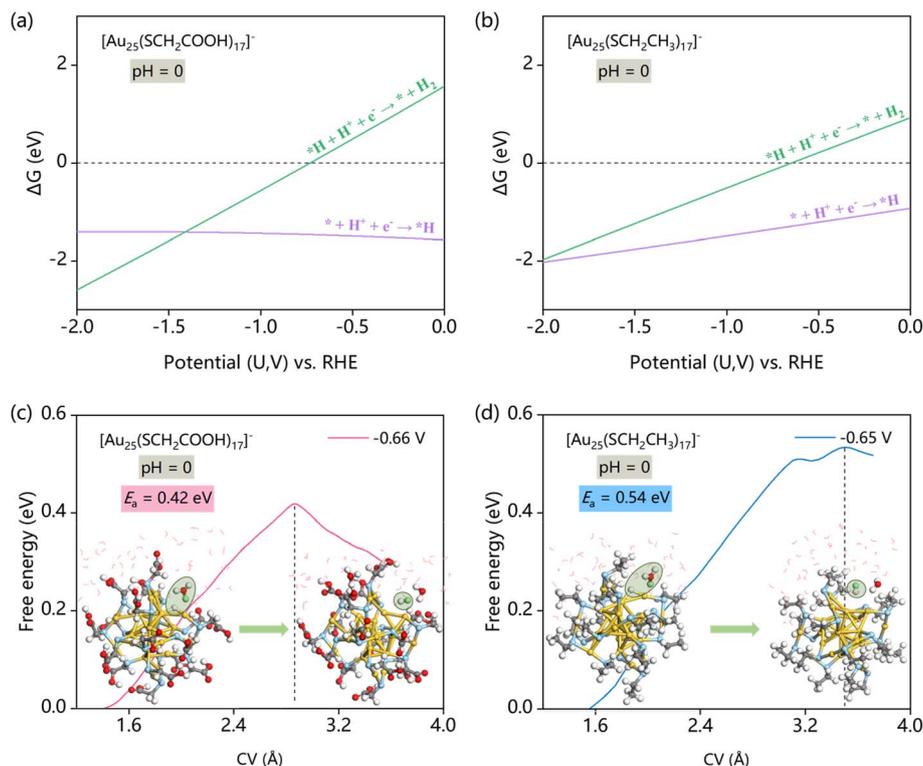


Fig. 2 Free energy changes (ΔG) for HER steps as a function of electrode potential for (a) $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and (b) $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$. Energy profiles sampled by slow-growth (SG)-AIMD for the HER rate-determining step of (c) $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and (d) $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ at similar potentials (vs. RHE) with representative initial state (IS) and final state (FS) structures.



for CO₂ reduction and significantly suppress the HER, minimizing the interference and allowing for a more targeted comparison of CO₂RR activity between the two nanoclusters.

Fig. 3a and b show the $U-\Delta G$ plots derived from work function fitting for [Au₂₅(SCH₂COOH)₁₇]⁻ and [Au₂₅(SCH₂CH₃)₁₇]⁻, respectively (additional details are provided in Fig. S6†). These plots detail the ΔG values associated with the four key steps of the CO₂RR. Notably, the reaction of *COOH → *CO + OH⁻ exhibits the highest ΔG value when the potential is higher than -1.0 V, indicating that it is the thermodynamically most challenging step. In contrast, the other three steps show lower ΔG values, suggesting that they are either spontaneous or more easily facilitated under the same potential conditions. Therefore, we conclude that the conversion of *COOH to *CO is the rate-determining step for the CO₂RR in both the nanocluster systems.

Next, we simulated the constant potential kinetics of this rate-determining step for both nanoclusters at similar applied potentials. As depicted in Fig. 3c and d, we tracked the energy barrier as a function of the constrained variable, which corresponds to the C-O bond distance within the *COOH intermediate (Fig. S1†). The energy barrier increases as the CV constraint grows, reaching a peak when *COOH is converted into *CO, and in the meantime, the generated OH⁻ is released into the water environment. The kinetic analysis revealed that the energy barrier for the [Au₂₅(SCH₂CH₃)₁₇]⁻ NC is relatively lower, with a smoother curve and a peak barrier of 0.76 eV. In contrast, the [Au₂₅(SCH₂COOH)₁₇]⁻ NC exhibits a significantly

higher energy barrier, with free energy peaking at 1.09 eV. This higher energy input indicates that the CO₂ reduction process in [Au₂₅(SCH₂COOH)₁₇]⁻ is less efficient compared to that in [Au₂₅(SCH₂CH₃)₁₇]⁻. The superior CO₂RR performance of [Au₂₅(SCH₂CH₃)₁₇]⁻ can be attributed to the hydrophobic nature of the -SCH₂CH₃-protected nanocluster. The hydrophobic environment likely facilitates the desorption of the OH⁻ species and the formation of *CO by minimizing interactions with the surrounding water molecules. This reduced interaction lowers the energy barrier for the rate-determining step, making the reaction pathway more favorable and thereby enhancing the overall CO₂ reduction efficiency.

To further substantiate the selectivity of the CO₂RR over the HER under alkaline conditions, we performed the constrained kinetic simulations for the competitive HER process on [Au₂₅(SCH₂COOH)₁₇]⁻ and [Au₂₅(SCH₂CH₃)₁₇]⁻ NCs. The results revealed that while the Volmer reaction (water dissociation and proton adsorption) is feasible (with a barrier less than 0.7 eV) (Fig. S7†), the Heyrovsky reaction (H₂ formation) encounters insurmountable barriers, where the splitting of the second H₂O molecule and subsequent H₂ generation display progressively increasing energy barriers (Fig. S8†). This indicates that the HER is kinetically hindered under alkaline conditions, thereby ensuring high selectivity for the CO₂RR on these nanoclusters.

The catalytic performance difference in the HER and CO₂RR

The optimized local structures of the Au(surface) and Au(staple) sites for both clusters are presented in Fig. 4a and b, while the

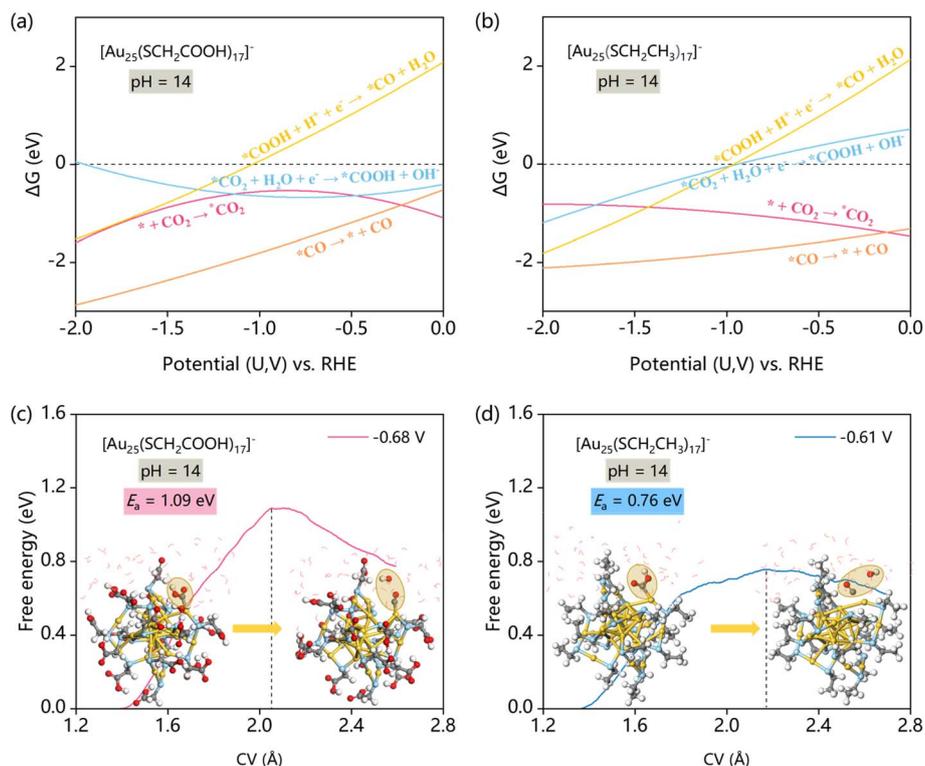


Fig. 3 Free energy changes (ΔG) for CO₂RR steps as a function of electrode potential for (a) [Au₂₅(SCH₂COOH)₁₇]⁻ and (b) [Au₂₅(SCH₂CH₃)₁₇]⁻. Energy profiles sampled by SG-AIMD for the rate-determining CO₂RR step of (c) [Au₂₅(SCH₂COOH)₁₇]⁻ and (d) [Au₂₅(SCH₂CH₃)₁₇]⁻ at similar potentials (vs. RHE) with representative IS and FS structures.



adsorption configurations of the key *H and *COOH intermediates are provided in Fig. S9.† Fig. 4c presents the radial distribution function (RDF) between the Au active sites in $[Au_{25}(SCH_2COOH)_{17}]^-$ and $[Au_{25}(SCH_2CH_3)_{17}]^-$ and the hydrogen atoms of water molecules during the rate-determining steps of the HER and CO_2RR . The solid lines represent the RDF for both Au(surface) and Au(staple) during the HER, while the dashed lines depict the RDF for Au(staple) during the CO_2RR .

In the HER rate-determining step, the RDF considers both Au(staple) and Au(surface) sites because the *H adsorption occurs at both the active Au sites. The first RDF peak corresponds to the closest interactions between the Au atoms and the hydrogen atoms of surrounding water molecules, occurring around 1.7 Å. For $[Au_{25}(SCH_2COOH)_{17}]^-$, the $g(r)$ value at this peak is 3.25, whereas for $[Au_{25}(SCH_2CH_3)_{17}]^-$, it is significantly lower at 0.98. The higher $g(r)$ value for $[Au_{25}(SCH_2COOH)_{17}]^-$ indicates stronger and more frequent interactions between the Au active sites and the hydrogen atoms. This can be attributed to the hydrophilic nature of the $-SCH_2COOH$ ligands, which draw water molecules closer to the Au surface, enhancing proton transfer and interaction with active sites, thereby improving the HER performance. In contrast, the lower $g(r)$ value for $[Au_{25}(SCH_2CH_3)_{17}]^-$ reflects weaker interactions due to the hydrophobic nature of the $-SCH_2CH_3$ ligands, which repel water molecules and limit hydrogen bonding near the Au surface, thereby reducing the HER efficiency. The second RDF peak, occurring around 2.9 Å, reflects the next shell of water molecules interacting with the Au active sites. Here, the $g(r)$ value is 5.66 for $[Au_{25}(SCH_2COOH)_{17}]^-$ and 4.08 for

$[Au_{25}(SCH_2CH_3)_{17}]^-$. The higher and sharper peak for the hydrophilic cluster indicates a more ordered and denser water structure around the Au atoms, which facilitates proton transfer and H_2 formation during the HER, further explaining its superior HER performance. Conversely, the less structured water network around the hydrophobic cluster hinders efficient proton transfer, limiting its HER activity.

For the CO_2RR rate-determining step, the RDF focuses on the interaction between Au(staple) and the hydrogen atoms of water molecules because *CO_2 and *COOH adsorption as well as the conversion to *CO occur exclusively at the Au(staple) site. Interestingly, $[Au_{25}(SCH_2COOH)_{17}]^-$ also shows a higher and sharper peak compared to $[Au_{25}(SCH_2CH_3)_{17}]^-$, indicating a more ordered and dense water structure around Au(staple). However, this structured water environment may hinder the adsorption and stabilization of CO_2RR intermediates such as *COOH by increasing the energy barrier for *COOH conversion to *CO . In contrast, the less structured water environment in $[Au_{25}(SCH_2CH_3)_{17}]^-$ minimizes water interference with CO_2RR intermediates, facilitating *COOH to *CO conversion with a lower barrier and enhancing CO_2RR performance.

Fig. 4d presents the Bader charge analysis of the Au(surface) and Au(staple) sites for both nanoclusters before and after the adsorption of key intermediates (*H and *COOH) in the HER and CO_2RR . These data reveal distinct differences in how the two systems interact with reactants, helping explain their differing catalytic performances. In the * state (without adsorption), both systems show similar Bader charges on the Au(surface) (0.13), but the Au(staple) in $[Au_{25}(SCH_2COOH)_{17}]^-$

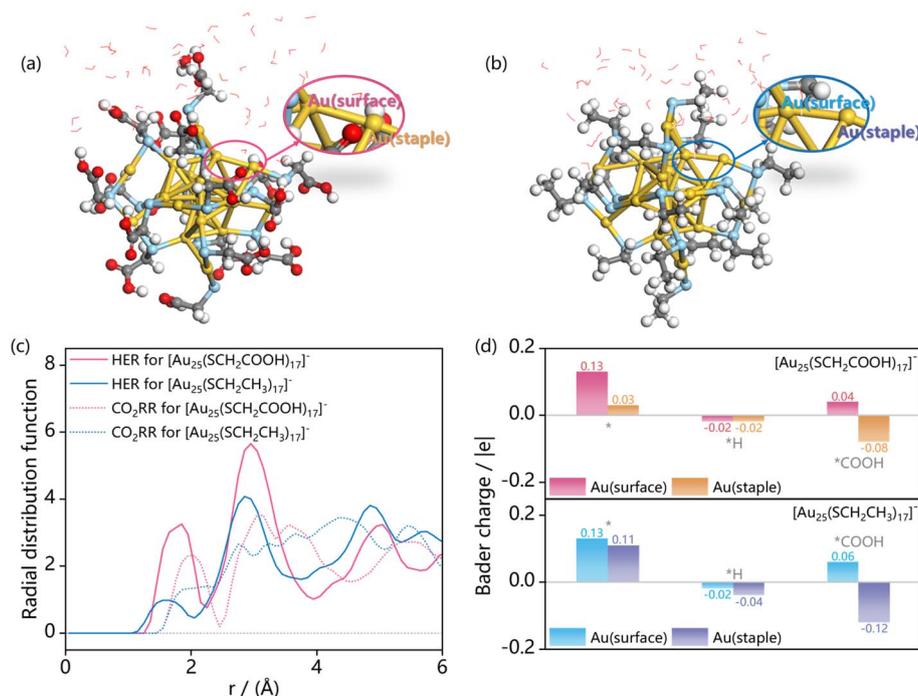


Fig. 4 Local structures of the Au(surface) and Au(staple) sites in (a) $[Au_{25}(SCH_2COOH)_{17}]^-$ and (b) $[Au_{25}(SCH_2CH_3)_{17}]^-$ NCs. (c) Radial distribution function (RDF) of Au active sites with hydrogen atoms from surrounding H_2O during the kinetic process of the rate-determining steps in the HER (solid lines) and CO_2RR (dashed lines) for $[Au_{25}(SCH_2COOH)_{17}]^-$ and $[Au_{25}(SCH_2CH_3)_{17}]^-$. (d) Bader charge analysis of Au(surface) and Au(staple) sites in the NC catalysts before and after the adsorption of key *H and *COOH intermediates in acidic HER and alkaline CO_2RR .



has a significantly lower charge (0.03) compared to $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ (0.11). The lower charge on Au(staple) in the hydrophilic cluster suggests a lower electron density, which could promote better interaction with protons facilitating proton transfer and enhancing the hydrogen evolution. When hydrogen is adsorbed (*H state), both systems exhibit negative charges on the Au sites, indicating electron transfer from H to Au. However, the Au(staple) site in $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ holds a higher negative charge (-0.04) compared to $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ (-0.02), suggesting a stronger electron interaction with hydrogen. This stronger interaction likely hinders H_2 desorption in the hydrophobic cluster, increasing the energy barrier for H_2 release. In contrast, the more balanced electron distribution in the hydrophilic cluster allows for easier H_2 desorption, contributing to its superior HER performance. In the *COOH state, a crucial intermediate for the CO_2RR , the Au(staple) in $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ shows a more negative charge (-0.12) than in $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ (-0.08). This indicates that the hydrophobic cluster better stabilizes the *COOH intermediate by receiving more electrons from the adsorbed species. This enhanced stabilization lowers the energy barrier for *COOH reduction to *CO, explaining the superior CO_2RR performance of $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$. Conversely, the less negative charge on Au(staple) in the hydrophilic cluster results in weaker stabilization of *COOH, leading to a higher energy barrier for this reduction step and contributing to its lower CO_2RR efficiency.

Fig. 5 illustrates the projected density of states (PDOS) and corresponding d-band centers (ϵ_d) of active Au sites for $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ NCs, along with their key intermediates involved in the HER and CO_2RR . The ϵ_d values offer valuable insights into the electronic properties of these catalysts and their interaction with reaction intermediates. In the pristine nanocluster (* state), $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ exhibits an ϵ_d of -3.34 eV, while $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ has a more negative ϵ_d of -3.61 eV. A more negative ϵ_d typically indicates a lower energy of the d-band center, which correlates with stronger binding of adsorbates. For the *H state, $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ has an ϵ_d of -3.14 eV, whereas $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ shows a more negative ϵ_d of -3.38 eV. This stronger interaction in $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ reflects tighter hydrogen binding, which could make H_2 desorption more difficult and increase the energy barrier for the HER. In contrast, the weaker interaction in $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ facilitates easier H_2 desorption, contributing to its superior HER activity. In the *COOH state, the ϵ_d for $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ is -3.65 eV, compared to a more negative ϵ_d of -3.78 eV for $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$. The more negative ϵ_d in $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ indicates stronger stabilization of the *COOH intermediate, lowering the energy barrier for *COOH to *CO conversion and enhancing the CO_2RR performance.

In summary, our above theoretical analysis revealed that the catalytic differences between $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ in the HER and CO_2RR are contributed both by their surface interaction with the water environment and their electronic properties. The RDF analysis shows that $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ with hydrophilic ligands enhances

proton transfer and H_2 desorption, leading to better HER performance. In contrast, the hydrophobic nature of $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ reduces water interaction and lowers the HER efficiency. The Bader charge and d-band center analyses reveal that $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$ strongly stabilizes the *COOH intermediate, lowering the energy barrier for *CO formation, thereby excelling in the CO_2RR , while $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ shows weaker stabilization of *COOH, leading to higher CO_2RR barriers.

Experimental validation

To validate the computational findings, which indicate that the hydrophilic ligand-protected Au_{25} cluster exhibits superior HER performance in an acidic environment, whereas the hydrophobic ligand-protected Au_{25} cluster excels in the CO_2RR in an alkaline environment, we conducted further experimental investigations. Specifically, we synthesized $[\text{Au}_{25}(\text{MPA})_{18}]^-$ as the hydrophilic model and $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ as its hydrophobic counterpart. To confirm the successful synthesis of $[\text{Au}_{25}(\text{MPA})_{18}]^-$ and $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ NCs, we conducted the UV-Vis absorption spectroscopy measurements. The UV-Vis spectra of the two Au_{25} NCs, provided in Fig. S10a and b,† exhibit distinct absorption peaks at 400 nm, 450 nm, and 670 nm, which are consistent with the characteristic optical behavior of Au_{25} NCs reported in previous studies.^{22,25}

In the HER experiments conducted in 0.5 M H_2SO_4 (Fig. 6a), $[\text{Au}_{25}(\text{MPA})_{18}]^-$ demonstrated a lower overpotential of 445 mV at a current density of 10 mA cm^{-2} compared to 541 mV for $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$, indicating an enhanced hydrogen evolution activity of the $[\text{Au}_{25}(\text{MPA})_{18}]^-$ NC. Additionally, the Tafel slope for $[\text{Au}_{25}(\text{MPA})_{18}]^-$ was slightly lower (106 mV dec^{-1}) than that of $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ (111 mV dec^{-1}), suggesting faster reaction kinetics (Fig. 6b). The stability tests over 8.5 hours of continuous operation (Fig. 6c) revealed that $[\text{Au}_{25}(\text{MPA})_{18}]^-$ maintained a stable current density, whereas $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ exhibited a reduction of about 10% in the current density, indicating that the hydrophilic $[\text{Au}_{25}(\text{MPA})_{18}]^-$ is more stable under acidic HER conditions.

For the CO_2RR performance evaluation, linear sweep voltammetry (LSV) was performed using a CO_2 flow cell with 1.0 M KOH electrolyte. As shown in Fig. 7a, the current density difference between CO_2 -saturated and N_2 -saturated electrolytes for $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ was larger than that for $[\text{Au}_{25}(\text{MPA})_{18}]^-$, indicating that $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ is more favorable for CO_2 reduction to CO. The faradaic efficiency for CO (FE_{CO}) at various potentials (Fig. 7b) showed that $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ achieved a higher FE_{CO} , reaching 97.64% at -0.48 V. In terms of the partial current density for CO production (j_{CO}) (Fig. 7c), $[\text{Au}_{25}(\text{MPA})_{18}]^-$ exhibited slightly higher values in the potential range of -0.18 V to -0.48 V, whereas $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ outperformed in the lower potential range of -0.58 V to -0.98 V. The Tafel slopes (Fig. S11†) further indicated the faster reaction kinetics for $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ (199 mV dec^{-1}) than that for $[\text{Au}_{25}(\text{MPA})_{18}]^-$ (242 mV dec^{-1}). Additionally, the turnover frequency (TOF) values (Fig. 7d) showed that $[\text{Au}_{25}(\text{MPA})_{18}]^-$ has slightly higher TOF between -0.18 V and -0.48 V, while



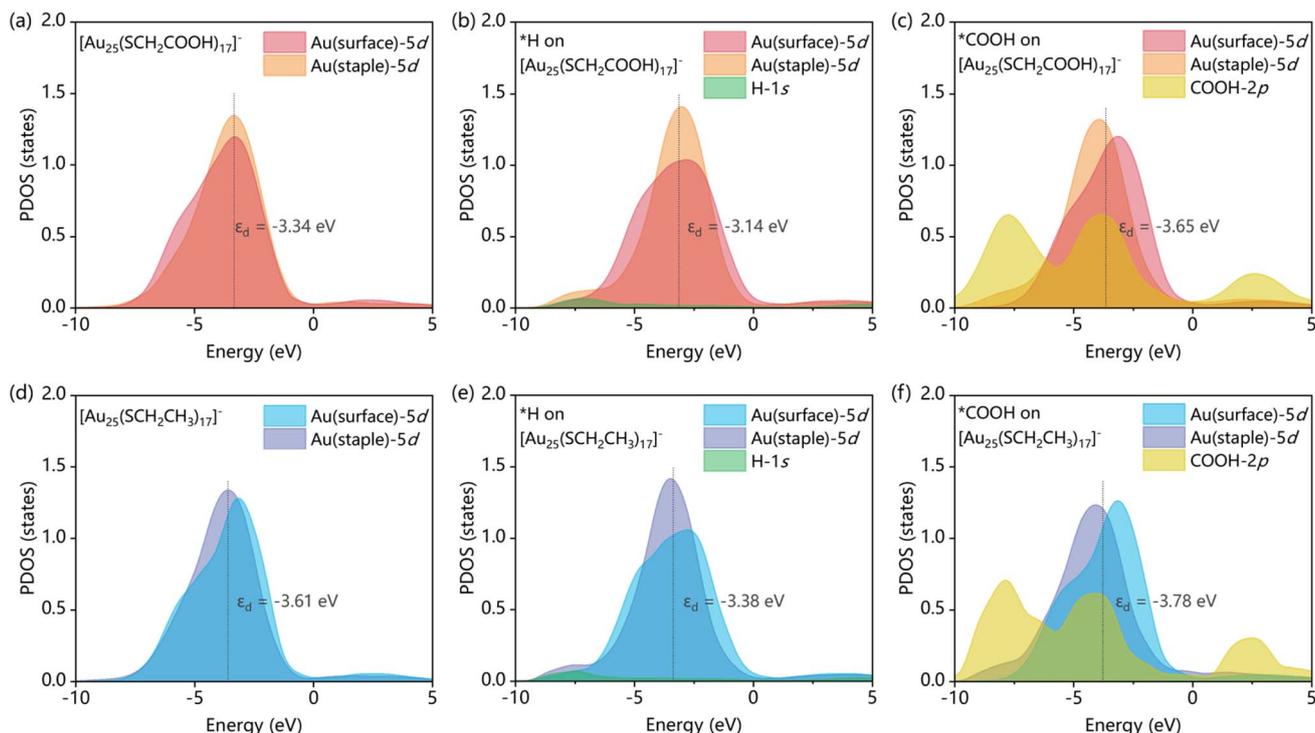


Fig. 5 PDOS and corresponding d-band centers (ϵ_d) for $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$ and $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$, and their key intermediates. (a) $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$, (b) *H adsorbed on $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$, (c) *COOH adsorbed on $[\text{Au}_{25}(\text{SCH}_2\text{COOH})_{17}]^-$, (d) $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$, (e) *H adsorbed on $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$, and (f) *COOH adsorbed on $[\text{Au}_{25}(\text{SCH}_2\text{CH}_3)_{17}]^-$.

$[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ exhibits significantly higher TOF values from -0.58 V to -0.98 V, indicating the much enhanced activity in lower potential ranges. The long-term stability tests over 8.5 hours of continuous operation demonstrated that $[\text{Au}_{25}(\text{MPA})_{18}]^-$ showed a slight decrease of around 4% in FE_{CO} and current density (Fig. 7e), whereas $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ maintained the stable FE_{CO} and current density (Fig. 7f), suggesting that the hydrophobic nanocluster is more stable under alkaline CO_2RR conditions.

Recognizing that the difference in the ligand chain length could also influence the electrocatalytic activity, we further synthesized and tested Au_{25} clusters protected by ligands with similar chain lengths. Specifically, $[\text{Au}_{25}(\text{MHA})_{18}]^-$ (MHA = 6-mercaptohexanoic acid) was chosen as a hydrophilic analog with

a chain length comparable to that of $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$. These additional experiments, detailed in the ESI,[†] provide a comprehensive analysis of how both ligand hydrophilicity and chain length affect the catalytic performance of Au_{25} NCs. The UV-Vis spectra of the synthesized $[\text{Au}_{25}(\text{MHA})_{18}]^-$ NCs exhibit distinct absorption peaks at 400 nm, 450 nm, and 670 nm (Fig. S10c[†]), confirming the successful synthesis of Au_{25} NCs.^{21,22,25}

The LSV curves were measured in a flow cell with 1.0 M KOH electrolyte (Fig. S12a[†]), revealing that $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ NCs are more favorable for CO_2 reduction to CO. In the comparison of FE_{CO} at various potentials (Fig. S12b[†]), $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ NCs demonstrate higher CO_2 reduction selectivity than $[\text{Au}_{25}(\text{MHA})_{18}]^-$ NCs, with the maximum FE_{CO} for $[\text{Au}_{25}(\text{MHA})_{18}]^-$ reaching only 88%. As shown in Fig. S12c,[†] the

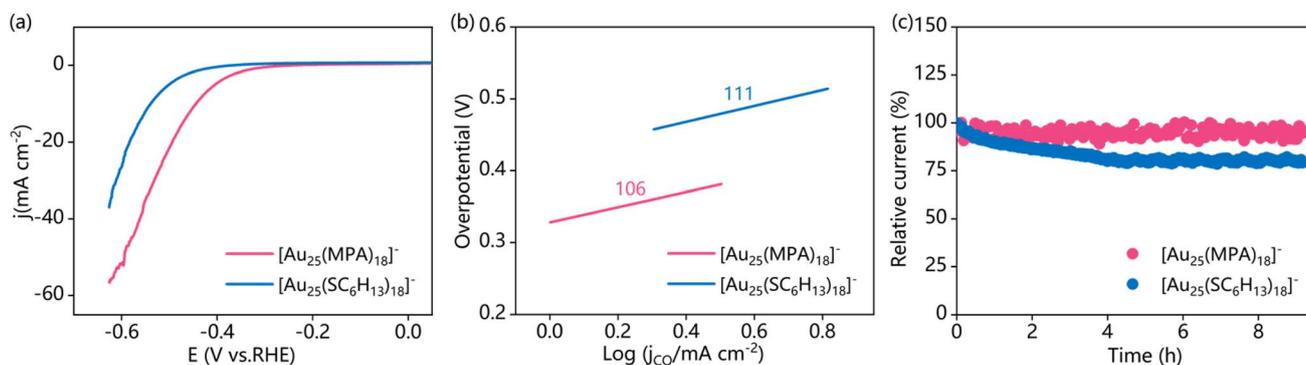


Fig. 6 Electrocatalytic HER performance in 0.5 M H_2SO_4 . (a) LSV curves of $[\text{Au}_{25}(\text{MPA})_{18}]^-$ and $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$. (b) Tafel slopes of the catalysts. (c) Chronoamperometric plots at 10 mA cm^{-2} for the HER stability testing.



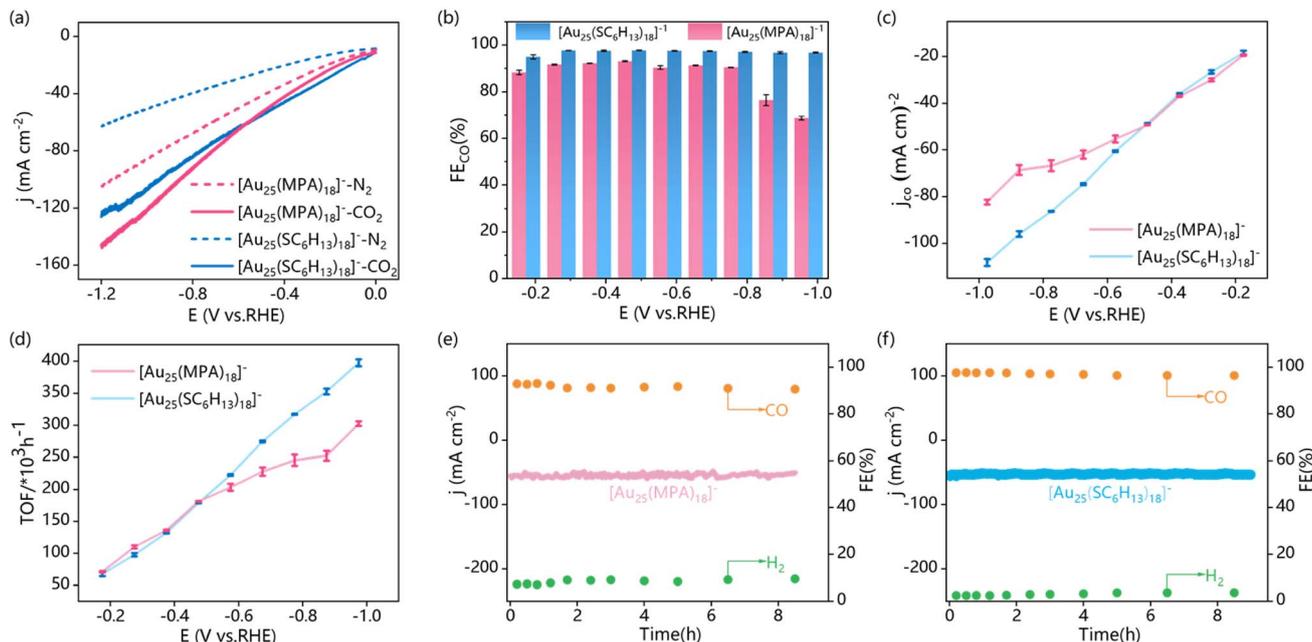


Fig. 7 Electrocatalytic CO₂RR performance in a CO₂ flow cell with 1 M KOH electrolyte. (a) LSV curves of [Au₂₅(MPA)₁₈]⁻ and [Au₂₅(SC₆H₁₃)₁₈]⁻ in N₂ and CO₂ environments. (b) Faradaic efficiency for CO (FE_{CO}) of [Au₂₅(MPA)₁₈]⁻ and [Au₂₅(SC₆H₁₃)₁₈]⁻ at different potentials. (c) Fractional current density of CO at various potentials. (d) Turnover frequency (TOF) of CO at different potentials. (e and f) Long-term stability tests of [Au₂₅(MPA)₁₈]⁻ and [Au₂₅(SC₆H₁₃)₁₈]⁻ for the CO₂RR at -0.48 V.

j_{CO} of [Au₂₅(SC₆H₁₃)₁₈]⁻ NCs is up to twice as high as that of [Au₂₅(MHA)₁₈]⁻ NCs. The Tafel slopes (Fig. S13[†]) further highlight the faster reaction kinetics for [Au₂₅(SC₆H₁₃)₁₈]⁻ NCs (199 mV dec⁻¹) compared to [Au₂₅(MHA)₁₈]⁻ (498 mV dec⁻¹). Additionally, the TOF values (Fig. S12d[†]) indicate that [Au₂₅(SC₆H₁₃)₁₈]⁻ exhibits significantly higher TOF than [Au₂₅(MHA)₁₈]⁻ across various potentials.

These experimental results have well corroborated our computational predictions, confirming that the hydrophilic ligand-protected Au₂₅ NCs are more effective for the HER in acidic environments due to enhanced proton transfer facilitated by the hydrophilic ligands. Conversely, the hydrophobic ligand-protected Au₂₅ NCs demonstrate superior CO₂RR activity under alkaline conditions by promoting adsorption of CO₂RR intermediates and minimizing the water interference, thereby enhancing CO₂ reduction efficiency. Further experiments with ligands of similar chain lengths to the hydrophilic and hydrophobic Au₂₅ NCs reveal that both ligand hydrophilicity and chain length influence catalytic performance. However, the hydrophilicity of the ligands plays a dominant role in determining the overall catalytic behavior. This alignment between computational and experimental findings underscores the critical role of ligand properties in tuning the electrocatalytic performance of atomically precise metal NCs, providing valuable insights for the rational ligand design of nanocatalysts in sustainable energy applications.

3. Conclusion

In this study, we have systematically explored how the ligand hydrophilicity and hydrophobicity influence the interface

dynamics and the electrocatalytic performance of Au₂₅ NCs in important reactions such as the HER and CO₂RR. Our computations revealed that the hydrophilic [Au₂₅(SCH₂COOH)₁₇]⁻ NC exhibits faster breakage of the Au-S bond and desorption of the thiolate ligand into solution at the applied reduction potential. The dethiolated [Au₂₅(SCH₂COOH)₁₇]⁻ NC is predicted to exhibit superior acid HER activity due to enhanced proton transfer and efficient hydrogen evolution facilitated by stronger hydrogen bond interactions with water molecules. Conversely, the hydrophobic [Au₂₅(SCH₂CH₃)₁₇]⁻ NC demonstrates enhanced alkaline CO₂RR performance by stabilizing key CO₂RR intermediates and minimizing the water interference to lower the barrier for CO formation. The electrochemical experiments using synthesized [Au₂₅(MPA)₁₈]⁻ and [Au₂₅(SC₆H₁₃)₁₈]⁻ as models, which have similar ligand molecular weights, have further validated our predictions. Hydrophilic [Au₂₅(MPA)₁₈]⁻ showed better activity, lower overpotential, and greater stability in the acidic HER testing, while hydrophobic [Au₂₅(SC₆H₁₃)₁₈]⁻ achieved higher faradaic efficiency, current density, and stability in alkaline CO₂RR. Moreover, the results from clusters with similar chain lengths, such as [Au₂₅(MHA)₁₈]⁻ and [Au₂₅(SC₆H₁₃)₁₈]⁻, further corroborated our computations, highlighting that both ligand hydrophilicity and chain length influence the catalytic performance, with hydrophilicity being the dominant factor in determining the overall catalytic behavior. These results not only provide an atomic level understanding of the ligand effects on the interface dynamics and electrocatalytic performance of metal NCs, but also stimulate ligand engineering as a facile strategy to optimize the catalytic activity of nanocluster catalysts for specific catalytic targets in future electrocatalysis research.



4. Computational methods and experimental section

Ligand removal dynamics

The dynamics of ligand removal from the nanocluster were investigated using the CP2K package (version 2023.1).⁵⁰ The simulations employed the Perdew–Burke–Ernzerhof (PBE) functional within the generalized gradient approximation (GGA) in combination with the hybrid Gaussian/Plane-Wave (GPW) scheme.⁵¹ The computational domain was defined with a periodic lattice size of $23 \times 23 \times 28 \text{ \AA}^3$, including 192 water molecules to simulate the solvent environment. Molecular dynamics (MD) simulations were performed in the canonical (NVT) ensemble using Nose–Hoover thermostats to maintain a constant temperature of 300 K.^{52,53} A time step of 1.0 fs was used throughout the simulations, which were run for a total of 10 ps. Dispersion corrections were applied using the DFT-D3 method to account for van der Waals interactions.^{54,55} The electronic structure was described by density functional theory (DFT) with spin-polarization and a mixed double- ζ Gaussian and plane-wave basis set, with an energy cutoff of 400 Ry.⁵⁶

Thermodynamic calculations for the HER and CO₂RR

Spin-polarized DFT calculations were carried out using the Vienna *Ab initio* Simulation Package (VASP, version 5.4.4).⁵⁷ The exchange–correlation effects were described using the Perdew–Burke–Ernzerhof (PBE) functional within the generalized gradient approximation (GGA).⁵¹ The projector-augmented wave (PAW) method was employed to account for electron–ion interactions with a cutoff energy of 400 eV.⁵⁸ For these calculations, the computational cell was set with a lattice size of $23 \times 23 \times 28 \text{ \AA}^3$, including 50 water molecules to adapt to the specific requirements of the reaction environments. The empirical DFT-D3 dispersion correction was applied to include van der Waals interactions.⁵⁹ Brillouin zone integration was performed using a gamma centered $1 \times 1 \times 1$ k -point grid, with convergence criteria set at 0.05 eV \AA^{-1} for forces and 10^{-4} eV per cell for energy. The electrode potential was determined *via* tuning the work function (additional details are provided in the ESI†).

Dynamic calculations for the HER and CO₂RR

Ab initio molecular dynamics (AIMD) simulations were conducted using the Nose–Hoover thermostat in the canonical (NVT) ensemble at 300 K with a time step of 1 fs.^{52,60} Thermodynamic integrations and the “slow-growth” method were employed to derive the free energy profiles for the rate-determining steps in the HER and CO₂RR. The collective variable (CV) increment was set to 0.0008 \AA , and the simulation time was 3 ps. Reaction barriers and reaction energies were determined by integrating the free-energy gradients to generate the free energy profiles.^{61,62}

Chemicals and materials

Tetrachloroauric(III) acid ($\text{HAuCl}_4 \cdot 3\text{H}_2\text{O}$, >99.99%), tetraoctylammonium bromide (TOAB, 98%), 1-hexanethiol (97%), 3-

mercaptopropionic acid (MPA, 98%), 6-mercaptohexanoic acid (MHA, 98%), sodium borohydride (NaBH_4), sodium hydroxide (NaOH), potassium hydroxide (KOH), Nafion solution (5 wt%), and solvents: reverse osmosis water, methanol, ethanol, acetonitrile (CH_3CN), dichloromethane (CH_2Cl_2) and tetrahydrofuran (THF) were used. High purity (>99.999%) Ar and CO_2 gases were used.

Preparation of the $[\text{Au}_{25}(\text{MPA})_{18}]^-$ NCs

In a typical synthesis of $[\text{Au}_{25}(\text{MPA})_{18}]^-$ clusters, 4 mg of $\text{HAuCl}_4 \cdot 3\text{H}_2\text{O}$ (0.05 mmol) and 2.1 mg of MPA (0.09 mmol) were mixed in 4.7 mL of ultrapure water under mild stirring. Subsequently, 3 mL of NaOH solution (1.0 M) was added, causing the solution color to change from yellow to pale yellow. Then, 1 mL of NaBH_4 solution (0.1 M) was added dropwise, turning the solution yellowish-brown. After 3 hours of vigorous stirring, unreacted MPA and other impurities were removed using organic solvents and spin distillation, yielding highly pure MPA-protected Au_{25} nanoclusters.

Preparation of the $[\text{Au}_{25}(\text{MHA})_{18}]^-$ NCs

The procedure of the $[\text{Au}_{25}(\text{MHA})_{18}]^-$ NCs is similar to the synthesis of $[\text{Au}_{25}(\text{MPA})_{18}]^-$. 4.0 mg of $\text{HAuCl}_4 \cdot 3\text{H}_2\text{O}$ (0.05 mmol) and 4.0 mL of MHA (50 mM) were mixed in 4.7 mL of ultrapure water under mild stirring. Subsequently, 0.5 mL of NaOH solution (1.0 M) was added, causing the solution color to change from yellow to pale yellow. Then, 1 mL of NaBH_4 solution (0.1 M) was added dropwise, turning the solution yellowish-brown. After 2 h of vigorous stirring, the obtained product was purified using organic solvents to remove unreacted MHA and other impurities, yielding $[\text{Au}_{25}(\text{MHA})_{18}]^-$ nanoclusters.

Preparation of the $[\text{Au}_{25}(\text{SC}_6\text{H}_{13})_{18}]^-$ NCs

$\text{HAuCl}_4 \cdot 3\text{H}_2\text{O}$ (0.125 mmol) and TOAB (0.145 mmol) were dissolved in 14 mL of THF in a 50 mL vial. After vigorous stirring for 15 minutes, the solution color changed from orange to red. Then, 1-hexanethiol (0.625 mmol) was slowly added, and the mixture was stirred for 1 hour until the red solution turned colorless. Next, freshly prepared NaBH_4 (1.25 mmol) in 2 mL of cold water was quickly added, producing bubbles as the solution turned black, indicating the formation of gold clusters. The reaction mixture was stirred for an additional 24 hours. The product was then transferred to a 25 mL round-bottom flask and dried by rotary evaporation. The dried product was redissolved in CH_2Cl_2 , and the supernatant was transferred to another round-bottom flask and dried again by rotary evaporation. Finally, the product was washed with ethanol, collected by centrifugation, and the washing process was repeated at least 10 times to ensure the removal of impurities.

Electrochemical measurements

The electrochemical tests were conducted using a CHI 760E electrochemical workstation (CH Instruments Inc.) at room temperature. For HER testing, cyclic voltammetry (CV) and LSV curves were obtained in a three-electrode cell setup, consisting



of a glassy carbon disk electrode (GCE, diameter 5 mm, surface area 0.07 cm²) as the working electrode, polished with alumina slurry and cleaned with ethanol and deionized water. A carbon rod served as the counter electrode, and an Ag/AgCl electrode in 0.5 M H₂SO₄ was used as the reference electrode. The potential of the reference electrode was calibrated to the reversible hydrogen electrode (RHE) using the equation: $E_{\text{RHE}} = E_{\text{Hg}/\text{HgCl}_2} + (0.244 + 0.0591 \times \text{pH}) \text{ V}$ in 0.5 M H₂SO₄ solution. The working electrode for the HER was prepared by dissolving 1 mg of carbon nanotube and 1 mg of Au₂₅ NCs in 0.5 mL of CH₂Cl₂, creating an ink with 10 μL of 5 wt% Nafion. Before testing, 3.5 μL of the catalyst and 3 μL of Nafion (5 wt%) were cast onto the GCE.

The catalytic activity of Au₂₅ NCs in the CO₂RR was determined using an electrochemical workstation (CHI 600E) with a three-electrode system coupled to a CO₂ flow cell. The electrolyte solution was 1 M KOH, and the reference electrode was an Ag/AgCl electrode immersed in saturated KCl solution. An anion-exchange membrane and a platinum plate were used as the ion mobility channel and counter electrode, respectively. The working electrode was prepared by dissolving 1 mg of carbon nanotube and 1 mg of Au₂₅ NCs in 0.5 mL of CH₂Cl₂, creating a uniform dispersion ink containing 10 μL of 5 wt% Nafion solution. This solution was sprayed onto a 1 cm² gas diffusion layer (GDL) with a mass loading of 2 mg cm⁻². The potentials were converted to the RHE using the following equation:

$$E(\text{RHE}) = E(\text{Ag}/\text{AgCl}) + 0.197 \text{ V} + 0.0591 \times \text{pH}$$

Before the electrochemical CO₂ reduction reaction, the cathodic electrolyte was saturated with CO₂ for 30 minutes. The cathodic and anodic reaction chambers were separated using an anion exchange membrane. During the CO₂RR process, each electrolyte cell contained 30 mL of electrolyte, circulated at 40 rpm using a peristaltic pump. The gas products were analyzed quantitatively with a gas chromatograph (GC, Huaai 9560). The faradaic efficiency (FE) of the gas products was calculated using the formula:

$$\text{FE} = \frac{Q_i}{Q_{\text{total}}} = \frac{N_i \times Z \times F}{Q_{\text{total}}}$$

where Q_i is the charge required to form the gaseous product, Q_{total} is the total charge during the reaction, N_i is the number of moles of the product detected by gas chromatography, Z is the number of electrons transferred during the formation of the product (2 for CO and H₂), and F is Faraday's constant (96 485 C mol⁻¹).

The turnover frequency (TOF) was calculated as follows:

$$\text{TOF}(\text{h}^{-1}) = \frac{j_i/ZF}{m_i \times \omega/M} \times 3600$$

where j_i is the partial current density of the corresponding gas product, Z is the number of transferred electrons during the formation of the product (2 for CO), F is the Faraday constant (96 485 C mol⁻¹), m_i is the mass of the loaded catalyst, ω is the

relative mass fraction of Au in the catalyst, and M is the relative atomic mass of Au. Linear sweep voltammetry (LSV) was conducted in a 1 M KOH solution saturated with either N₂ or CO₂, using a scan rate of 50 mV s⁻¹.

Data availability

The data supporting this article have been included as part of the ESI.†

Author contributions

Q. T. conceived the idea. L. L. performed the theoretical calculations with help from Y. C. and F. S. X. Z. performed the experiments and analyzed the data under the guidance of L. W. L. L. wrote the manuscript with inputs from all authors. Q. T. and L. W. finalized the manuscript. All the authors approved the final version of the manuscript.

Conflicts of interest

The authors declare no competing financial interests.

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