



Cite this: *Chem. Sci.*, 2025, **16**, 329

All publication charges for this article have been paid for by the Royal Society of Chemistry

Received 2nd October 2024
Accepted 12th November 2024

DOI: 10.1039/d4sc06673a
rsc.li/chemical-science

Modulating built-in electric field *via* Br induced partial phase transition for robust alkaline freshwater and seawater electrolysis†

Lei Jin, Hui Xu, * Kun Wang, Yang Liu, Xingyue Qian, Haiqun Chen * and Guangyu He*

Repulsing Cl^- to reduce its negative effects during seawater electrolysis is a promising strategy to guard against the corrosion of high-valence metal sites. Herein, we synthesized $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ by a facile Br-induced partial *in situ* phase transition strategy. This $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ possessed intensified built-in electric field (BEF) due to large work function difference ($\Delta\phi$), demonstrating outstanding OER and HER activity in alkaline freshwater/seawater solution and exhibiting a low cell voltage for an anion exchange membrane water electrolyzer (AEMWE) system. Both experiments and theoretical results verify that the interfacial charge redistribution induced by the enhanced BEF optimizes the adsorption strength for the intermediates. Moreover, the appropriate phosphorus–oxygen anion self-transformation can protect the NiOOH active species from corrosion by repulsing Cl^- in alkaline seawater. This work not only proposes a fresh perception of the water/seawater splitting mechanism but also provides new design principles to defend active sites in seawater-to- H_2 conversion systems.

1. Introduction

Electrolysis of water powered by renewable energy constitutes a sustainable strategy for the production of transportable and green hydrogen (H_2).^{1,2} Apart from considering the expense of electrolyzers and the intermittence of renewable electricity, a supply of freshwater may be a practical problem for deploying large-scale electrocatalytic H_2 production.^{3,4} If saline water, particularly seawater—which constitutes nearly 96.5% of Earth's total water resources—could serve as an ideal feedstock for electrocatalytic H_2 production, it would help alleviate the shortage of freshwater resources. While the transformation of seawater to H_2 is an intriguing prospect, chloride ions (Cl^-) and their derivatives (such as Cl_2 or HClO/ClO^-) can significantly accelerate the corrosion or deactivation of electrocatalysts. This occurs through surface adsorption or coordination mechanisms, especially during the anodic oxygen evolution reaction (OER) associated with seawater splitting.^{5,6} Moreover, the standard thermodynamic voltage of OER is 0.48 V lower than that of the chlorine oxidation reaction (ClOR) at $\text{pH} > 7.5$. This means that superior water splitting performance can significantly suppress Cl^- transformation into Cl_2 or HClO/ClO^- . Even if the

electrode shows excellent activity in inhibiting Cl^- oxidation, Cl^- ions themselves can etch electron-poor transition metals, leading to metal leaching and a deterioration in performance.^{7,8} Therefore, the exploration and construction of catalysts that suppress the loss of reaction sites to maintain high seawater splitting activity and optimize adsorption behaviors for intermediates to safeguard the electrode against Cl^- attack are of paramount importance.

The exquisite construction of a built-in electric field (BEF) between two hetero substances with a difference in Fermi level, would be a promising way to manipulate the electronic state of active sites and stabilize the surficial dynamical adsorption balance.^{9,10} For example, a Co LDH/ Cu_3P composite can accelerate charge transport and improve active sites due to an enhanced built-in potential (E_{BI}).¹¹ Zhang *et al.* have constructed $\text{N}-\text{Ni}_5\text{P}_4/\text{CoP}$ nanowires with a strong BEF for hydrazine-assisted H_2 production.¹² Very recently, Xu *et al.* demonstrated that the enhanced BEF at the $\text{Fe}_2\text{P}/\text{NiCoP}$ interface facilitates the surface transformation of NiCoP into NiCoOOH active species, exhibiting high freshwater and seawater oxidation activity.¹³ Essentially, the constructed BEF can facilitate the division of positive and negative charges, inducing their separation in opposite directions at the heterointerface to accelerate regional charge polarization.¹⁴ Consequently, manipulating the features of the BEF can achieve an asymmetric distribution of charge that is promising for realizing the stable adsorption of intermediates on the heterointerface or active sites.¹⁵ However, while coupling transition metal phosphides (TMPs) with other components (nitrides or sulfides), charge carriers would

Key Laboratory of Advanced Catalytic Materials and Technology, Advanced Catalysis and Green Manufacturing Collaborative Innovation Center, Changzhou University, Changzhou, Jiangsu Province 213164, China. E-mail: xuhui006@cczu.edu.cn; hegy@cczu.edu.cn; chenhq@cczu.edu.cn

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4sc06673a>



experience severe localization due to the overlap of the electron cloud across the heterointerface, where the electrons are completely delocalized *via* the metal whereas the protons are still confined and greatly weaken the BEF.^{16,17} Fortunately, by manipulating the difference in the work function ($\Delta\Phi$) between TMP and other substances, the charge transfer direction across the heterointerface can be controlled.¹⁸ Based on the above discussion, it is rational and promising to simultaneously regulate the adsorption behaviors for intermediates by exquisitely designing the appropriate components with suitable work functions to control and modulate the BEF. Moreover, revealing the relationship between BEF and $\Delta\Phi$ and its effect on catalytic activity and selectivity is important.

Herein, for the first time, we have exquisitely designed and manipulated the Br-induced partial *in situ* phase transition from $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ to $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ under the phosphorization process, which strongly influences the $\Delta\Phi$. Specifically, $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$, with a large $\Delta\Phi$ (0.5 eV) compared with $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (0.3 eV), demonstrates an enhanced BEF, as confirmed by various electrochemical tests. Furthermore, *in situ/ex situ* spectroscopic investigations confirm that the enhanced BEF plays an important role in subtly tailoring the intermediates and phosphate absorption strength, which is essential for water and seawater splitting. As a result, the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst reveals remarkable OER and HER activity with low overpotentials of 196 mV and 108 mV for freshwater and 229, 203 mV for seawater, respectively, and can be used in an anion exchange membrane water electrolyzer (AEMWE) with low cell voltage. This work paves the way for synthesizing bifunctional water-splitting electrocatalysts by exquisitely designing and modulating the interfacial BEF.

2. Experimental section

2.1 Synthesis of NiFe LDH

First, 0.582 g of $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, 0.404 g of $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$, and 0.841 g of $\text{C}_6\text{H}_{12}\text{N}_4$ were weighed and fully dissolved in a Teflon autoclave with 45 mL of ethanol solution, and stirred for 2 h. After reaction for 12 h at 120 °C, a brown product (NiFe LDH) was obtained by centrifugation with ethanol and dried at 60 °C all night.

2.2 Synthesis of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$

The as-prepared NiFe LDH precursors, a small amount of hexabromobenzene (HBB) and 300 mg of $\text{NaH}_2\text{PO}_2 \cdot \text{H}_2\text{O}$ were placed in three separate positions in a ceramic boat inside a tube furnace, where $\text{NaH}_2\text{PO}_2 \cdot \text{H}_2\text{O}$ was at the midstream of the gas flow, NiFe LDH was placed on the downstream side, and one piece of HBB flake (pressurized at 14 MPa at room temperature) was located upstream. Then the temperature was raised to 350 °C for 2 h. After cooling down to room temperature, a black product consisting of thick $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ nanosheets was obtained. For the synthesis of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$, the same synthetic method was adopted as for the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ sample without the addition of HBB flake.

2.3 Material characterizations and electrochemical methods

The material characterizations and electrochemical methods are documented in detail in the ESI.†

3. Results and discussion

3.1 Material synthesis and characterization

In general, thermodynamic stability can be altered when materials are doped with heteroatoms. Bromine, being more electronegative than phosphorus, was chosen as a candidate to induce the formation of a P-poor phase. The relatively large size of Br favors the creation of phosphorus vacancies due to the strain field it generates.^{19,20} As schematically illustrated in Fig. 1, an $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst could be successfully synthesized by a two-step route. Firstly, NiFe LDH nanosheets with a large surface area were obtained *via* an appropriate solvothermal pathway. Next, the NiFe LDH was completely transformed into $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (the ratio of P/Ni = 0.8) *via* a thermal phosphorization process at 350 °C. However, $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ adopts the bulk nanosheet structure, which may be attributed to the introduction of molten NaH_2PO_2 salt gas with high viscosity, causing the NiFe LDH to agglomerate easily. In addition, during the process of synthesizing $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$, a small amount of Br atoms and more P atoms first form an $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4\text{Br}_{4-x}$ intermediate. Subsequently, the remaining P atoms struggle with Br and consume each other. Eventually Br atoms are completely replaced by P atoms, causing a partial phase transition, thus forming a P-poor-phase $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ (P/Ni = 0.5) catalyst.

The morphology of the as-prepared catalysts was characterized *via* scanning electron microscopy (SEM) and transmission electron microscopy (TEM). As illustrated in Fig. 2a and S1,† the NiFe LDH exhibits a nanosheet morphology. After being subjected to a phosphorylation process, both with and without Br atoms, the synthesized $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ catalysts display a bulk nanosheet structure, attributed to the introduction of molten NaH_2PO_2 salt gas with high viscosity, causing the NiFe LDH to agglomerate easily (Fig. 2b and c). Moreover, the high-resolution TEM (HRTEM) images in Fig. 2d-f and S2a-c† show that both $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ contain common clear lattice fringes with an approximate spacing of 0.17 nm (Fig. 2e, e-1, S2c and c-1†) that are indexed to the (300) crystal plane of

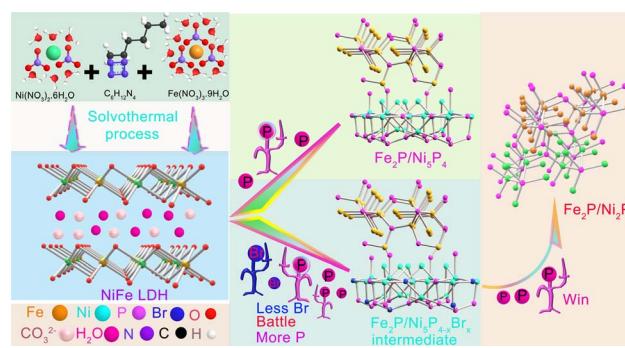


Fig. 1 Schematic illustration of the formation of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ and $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$.



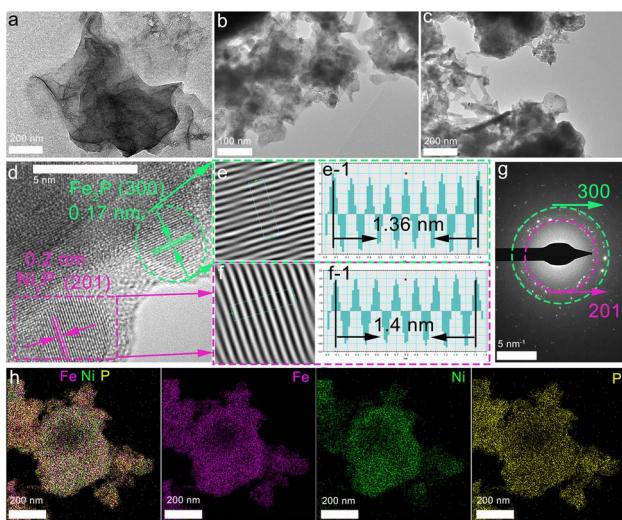


Fig. 2 TEM images of (a) NiFe LDH, (b) Fe₂P/Ni₅P₄ and (c) Fe₂P/Ni₂P. (d–f) High-resolution TEM images of Fe₂P/Ni₂P, integrated pixel intensities (e-1 and f-1) of Fe₂P and Ni₂P (taken from the green dotted rectangles in (e) and (f)). (g) SAED pattern of Fe₂P/Ni₂P. (h) Elemental mapping images of Fe₂P/Ni₂P.

Fe₂P. While, two clear lattice fringes with approximate spacings of 0.2 (Fig. 2f and f-1) and 0.22 nm (Fig. S2b and b-1†) are indexed to the (201) and (210) crystal planes of Ni₂P and Ni₅P₄ in the Fe₂P/Ni₂P and Fe₂P/Ni₅P₄ catalysts, respectively, confirming the successful fabrication of the Fe₂P/Ni₂P and Fe₂P/Ni₅P₄ structures.^{21–24} These results can be further confirmed *via* selected area electron diffraction (SAED) patterns (Fig. 2g and S2d†). Moreover, the EDS analysis of the as-synthesized Fe₂P/Ni₂P proved that Ni, Fe, and P were the main elemental components with Ni : Fe : P : Br mass ratios of 1 : 1.04 : 2.73 : 0 (Fig. S3†), which may be ascribed to a small amount of Br atoms and more P atoms first forming an Fe₂P/Ni₅P₄Br_{4-x} intermediate, and the remaining P atoms struggle with Br atoms and consume each other. Eventually, the Br is replaced by P, causing a phase transition. This result strongly proves that the Br atoms play a brief intervention role in synthesizing Fe₂P/Ni₂P. The element mapping images of the Fe₂P/Ni₂P and Fe₂P/Ni₅P₄ catalysts also confirmed the uniform dispersion of the elements of Fe, Ni and P (Fig. 2h and S2f†).

To verify this portion-limited phase-transition mechanism, X-ray diffraction (XRD) patterns of NiFe LDH, Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P were recorded first. As shown in Fig. S4,† four prominent peaks can be observed at approximately 33.5°, 34.4°, 59.9° 61.3°, attributed to the (110), (012), (101) and (113) crystal planes of NiFe LDH (JCPDS no. 40-0215), respectively.²⁵ Notably, the peaks located at 40.3°, 44.2°, 47.3°, 54.1° and 54.6° belonging to the (111), (201), (210), (300) and (211) crystal planes of Fe₂P (JCPDS no. 51-0943), respectively, which can be observed in both Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P samples,²⁶ while peaks located at approximately 31.5°, 36.1°, 40.6°, 41.4°, 43.9°, 45.1°, 47.8°, 53.9° and 56.4° belong to the (201), (104), (210), (211), (212), (204), (213), (220) and (310) crystalline planes of Ni₅P₄ (JCPDS no. 18-0883), respectively.²³ However, after a brief intervention by the Br atoms, the Ni₅P₄ phase disappears and

new peaks located at 40.8°, 44.6°, 47.3°, 54.2°, 54.9° and 74.7° correspondingly ascribed to the (111) (201), (210), (300), (211) and (400) crystal planes of Ni₂P (JCPDS no. 03-0953) can be found (Fig. 3a).²⁷ The above results confirm the successful synthesis of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P, and also strongly verify the phase transition from Ni₅P₄ to Ni₂P. Moreover, to reveal the structural characteristics and bonding properties of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P, the Fourier transform infrared (FT-IR) spectra were measured. As illustrated in Fig. 3b, two dominant absorption bands of M–P at 920 and 1024 cm⁻¹ can be observed, and one broad band at 551 cm⁻¹ is ascribed to bending vibration of the ν_4 (O–P–O) bond.^{28–30} Furthermore, to reveal the role of the portion-limited phase transition in tuning the electronic structure, electron paramagnetic resonance (EPR) spectra of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P were documented (Fig. 3c). The relatively large size of Br favors the formation of abundant P vacancies due to the strain field. Fe₂P/Ni₂P displays a pair of prominent signals, suggesting the existence of abundant unpaired electrons derived from dangling bonds in the portion-limited phase-transition structure compared with Fe₂P/Ni₅P₄, also confirming that it may form an Fe₂P/Ni₅P₄Br_{4-x} intermediate first and then phase change into Fe₂P/Ni₂P, or directly form Fe₂P/Ni₂PBr_{1-x} and Fe₂P/Ni₅P₄Br_{4-x}. However, the XRD proves the phase transition from Ni₅P₄ to Ni₂P, and EDS demonstrates that there are no Br atoms. Thus, it is directly proved that Fe₂P/Ni₅P₄Br_{4-x} is formed first and then converted into Fe₂P/Ni₂P, instead of directly forming Fe₂P/Ni₂PBr_{1-x} and Fe₂P/Ni₅P₄Br_{4-x}.^{19,20,31} In fact, numerous dangling bonds offer more accessible active sites for electrochemical water splitting.³² Accordingly, X-ray photoelectron spectroscopy (XPS) was employed to reveal the chemical composition and bonding configuration of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P. The XPS full spectra

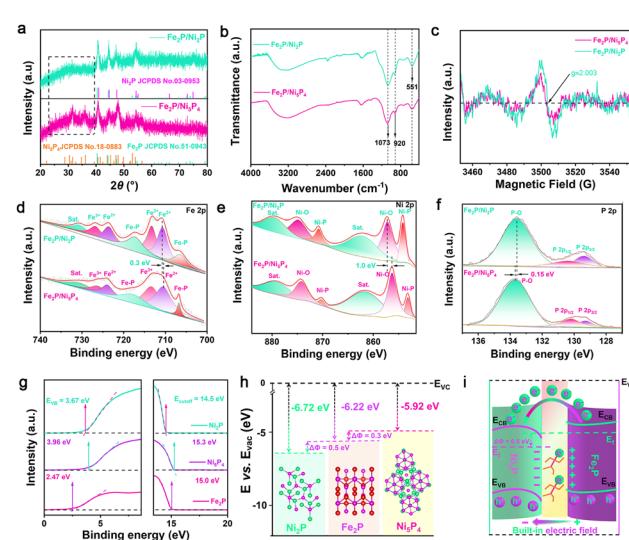


Fig. 3 (a) XRD patterns of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P. (b) FT-IR spectra of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P. (c) EPR spectra of Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P. High-resolution XPS spectra of (d) Fe 2p, (e) Ni 2p and (f) P 2p in Fe₂P/Ni₅P₄ and Fe₂P/Ni₂P. (g) UPS spectra of Ni₅P₄, Fe₂P and Ni₂P. (h) Energy-band alignment diagram of Ni₅P₄ and Ni₂P with respect to Fe₂P. (i) Schematic diagram of the BEF based on the interfaces between Fe₂P and Ni₂P.



(Fig. S5a†) reveal the coexistence of Fe, Ni and P elements, which correspond to the above elemental mapping.³³ As shown in the high-resolution Fe 2p spectrum (Fig. 3d), for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$, the prominent peak at 705.9 eV belongs to Fe-P, while three peak doublets located at (710.6 and 723.5 eV), (713.2 and 726.7 eV), and (717.2 and 730.6 eV), consistent with Fe^{2+} , Fe^{3+} , and satellite signals, respectively. The peaks of Fe 2p display a slight positive shift compared with $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$, demonstrating greater electron transfer from Fe to the P atom.³⁴ Likewise, three pairs of peaks corresponding to satellite peaks (861.1, 879.9 eV), Ni-O (855.9, 874.3 eV), and Ni-P (852.7, 870.1 eV) are also observed in the high-resolution Ni 2p spectra (Fig. 3e), which exhibit a remarkable positive shift (about 1.0 eV), implying a reduction in charge density around the metal atom.¹⁸ Meanwhile, for P 2p orbitals, the peaks located at 129.1, 130.0 and 133.6 eV in Fig. 3f are ascribed to $\text{P} 2\text{p}_{3/2}$, $\text{P} 2\text{p}_{1/2}$ and the P-O bonding state, respectively.³⁵ Compared with $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$, the peaks of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ exhibit a slight negative shift (about 0.42 eV), indicating more accumulated electrons on P due to the Br and P consuming each other and thus introducing abundant P vacancies.³⁶ These shifts confirm the abundant electron transfer from the Ni atom to the P atom compared with the Fe atom. In order to balance the charge, the Fe atom spontaneously transfers partial electrons to the Ni atom, which further confirms the electron transfers from Fe_2P to Ni_2P , thus signifying the formation of a BEF with electron-rich Ni atoms and electron-poor Fe atoms, optimizing the adsorption energy of the intermediate in the water-splitting process.

Generally, the charge transfer direction is closely correlated with the difference $\Delta\Phi$ in the semiconductor heterostructure.^{37,38} Ultraviolet photoelectron spectroscopy (UPS) was undertaken to analyze the values for Fe_2P , Ni_5P_4 and Ni_2P . As illustrated in Fig. 3g and Table S1,† the Φ value of Ni_2P is increased by 0.8 eV compared with Ni_5P_4 , suggesting that a brief intervention by the Br atom can decrease the Fermi level. Accordingly, the measured Φ values of Ni_5P_4 , Fe_2P and Ni_2P are 5.92, 6.22, and 6.72 eV, respectively (Fig. 3h). Compared with a relatively small $\Delta\Phi$ of 0.3 eV at the $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ heterogeneous interface, the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ interface possesses a relatively large $\Delta\Phi$ of 0.5 eV. Moreover, the Mott–Schottky (M–S) plots of Ni_5P_4 , Fe_2P and Ni_2P were calculated to construct energy diagrams. As shown in Fig. S5b–d,† Ni_5P_4 , Fe_2P and Ni_2P possess a positive slope, indicating that these catalysts are n-type semiconductors, and the flat band potentials (E_{FB}) of Ni_5P_4 , Fe_2P and Ni_2P can be tested to be 0.64, 0.59 and 0.66 (vs. Hg/HgO), respectively; thus, the conduction band potential (E_{CB}) values of Ni_5P_4 , Fe_2P and Ni_2P can be calculated as 0.64, 0.59 and 0.66 V vs. NHE ($E_{\text{NHE}} = E_{\text{Hg/HgO}} + 0.098$ V).^{39,40} Furthermore, the valence band (E_{VB}) maximum values were measured as 3.96, 2.47 and 3.67 eV for Ni_5P_4 , Fe_2P and Ni_2P , respectively. Therefore, the band gap (E_g) values of Ni_5P_4 , Fe_2P and Ni_2P were calculated as 3.32 eV, 1.88 eV and 1.5 eV by using the formula: $E_{\text{VB}} = E_{\text{CB}} + E_g$; the smaller E_g of Ni_2P (1.5 eV) confirms the faster charge transfer across the Fermi level.⁴¹ Based on the above results, the interfacial electronic structure in the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ heterojunction can be modified, and the large discrepancy in Φ forms an n–n heterojunction, where $\Delta\Phi$ would drive the charge migration from

high level to low until the heterojunction interface recovers balance.⁴² Therefore, the charge in Fe_2P will flow into Ni_2P , forming a positively charged donor. Concurrently, a BEF is formed with the orientation pointing from Fe_2P to Ni_2P (Fig. 3i). Generally, the largest $\Delta\Phi$ indicates the presence of the strongest BEF between the two semiconductors. A BEF with electron flow in a single direction can effectively adjust the charge redistribution and can concurrently induce an electron-rich Ni_2P zone and an electron-poor Fe_2P zone, thus promoting the adsorption process for intermediates and PO_4^{3-} .^{43,44}

3.2 OER and HER in freshwater

The electrochemical performance of the as-prepared catalysts was documented by a standard three-electrode system in 1 M KOH solution. For comparison, RuO_2 and Pt/C catalysts were employed as reference HER and OER catalysts, respectively. Linear sweep voltammetry (LSV) curves in Fig. 4a show that the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst displays superior electrocatalytic performance for OER and HER compared with $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ and NiFe LDH. Concretely, it requires ultra-small overpotentials of 196 and 224 mV to achieve η_{10} and η_{20} for OER (Fig. 4b), which are superior to those of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (237 and 258 mV), NiFe LDH (272 and 307 mV), and RuO_2 (327 and 389 mV). Additionally, $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ shows the highest HER activity, requiring overpotentials of only 108 and 151 mV to attain η_{10} and η_{20} , also being superior to $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (204 and 250 mV) and NiFe LDH (422 and 475 mV). These results confirm that the introduction of Br induces a phase change and constructs a stronger BEF due to the larger $\Delta\Phi$. This, in turn, substantially enhances the OER and HER activities,⁴⁵ also outperforming the majority of reported electrocatalysts (Tables S2 and S3†). The Tafel slope is usually used to reveal OER and HER kinetics, and a low Tafel

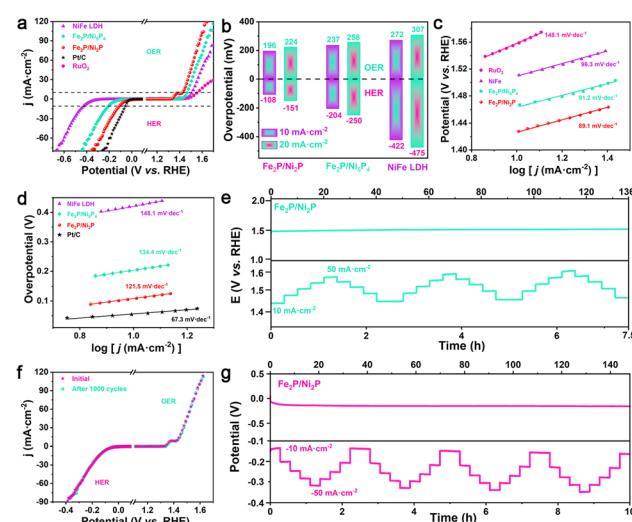


Fig. 4 (a) Electrocatalytic OER and HER performance of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and the references in 1.0 M KOH solution. (b) Overpotentials of as-prepared samples at 10 and 20 mA cm^{-2} for OER and HER. (c and d) Corresponding Tafel plots of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ for OER and HER. (e and f) Polarization curves for OER and HER after 1000 cycles. (e and g) Chronopotentiometric (CP) curves and multi-step chronopotentiometry tests results of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ for OER and HER.

slope means favorable reaction kinetics. As shown in Fig. 4c and d, the Tafel slopes of the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst are determined to be 89.1 and 121.5 mV dec $^{-1}$ for OER and HER, respectively, which are smaller than those of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (91.2 and 134.4 mV dec $^{-1}$) and NiFe LDH (96.3 and 148.1 mV dec $^{-1}$), indicating a Volmer–Heyrovsky water-splitting procedure. Moreover, the electrochemically active surface area (ECSA) was probed by using double-layer capacitance (C_{dl}) to understand the surface properties of the samples. Fig. S6 and S7 \dagger show that the C_{dl} for $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4\text{-Ov}$ are calculated to be 1.0 and 13.9 mF cm $^{-2}$ for OER and HER, respectively, suggesting a greater electrochemically active surface area. Furthermore, the electrochemical stability of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ for OER and HER was assessed *via* a cyclic voltammetry (CV) test. The LSV curve of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ after 1000 CV cycles coincides well with the initial curve, indicating its outstanding cyclability (Fig. 4f). To estimate the intrinsic OER and HER activity, Fig. S8 \dagger documents the turnover frequency (TOF) values of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and referenced samples, where $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ demonstrates higher TOF values for OER (0.029 s $^{-1}$) and HER (0.195 s $^{-1}$).^{46,47} The superb long-term stability was evaluated using chronoamperometry measurements, in which the electrochemical OER and HER activities of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ were conducted smoothly for more than 135 h without a remarkable change (Fig. 4e and g), demonstrating its high stability and good corrosion resistance properties in anodic and cathodic conditions. Multi-current curves of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ were tested by changing the current density from 10 to 50 mA cm $^{-2}$ for OER and from –10 to –50 mA cm $^{-2}$ for HER per 1000 s. The high mass transport capability and stability can be further confirmed by the instantaneous potential response of each step when different currents are applied, suggesting the superb durability and fast charge/mass transport in the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ sample.

3.3 OER and HER in alkaline seawater

With the shortage of fresh water resources in the world, seawater electrolysis and sustainable hydrogen energy have attracted increasing attention. One of the dominant challenges in seawater splitting is the chlorine evolution reaction (CER) on the anode, which is driven by the existence of Cl^- ions. This reaction competes with the OER and leads to the formation of insoluble precipitates, such as calcium hydroxide, on the catalyst surface.⁴⁸ To verify the selective inhibition of CER and shielding from impurities in seawater, the OER and HER performance of the samples were also measured in alkaline seawater solution. As shown in Fig. 5a–d, the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst requires a smaller OER η_{10} of only 229 mV with faster kinetics of 55.1 mV dec $^{-1}$ compared to $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (260 mV, 60.0 mV dec $^{-1}$), NiFe LDH (277 mV, 62.0 mV dec $^{-1}$) and RuO₂ (345 mV, 134.6 mV dec $^{-1}$), outperforming some reported electrocatalysts (Table S6 \dagger). The activity of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ is almost unaffected compared with freshwater due to the construction of a stronger BEF and the appearance of the surface of PO_4^{3-} that effectively suppresses Cl^- oxidation, indicating its highly selective inhibition and shielding from impurities.⁴⁹ In addition, $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ exhibits better HER activity, which requires overpotentials of only 203 and 247 mV to attain η_{10} and η_{20} , respectively, smaller

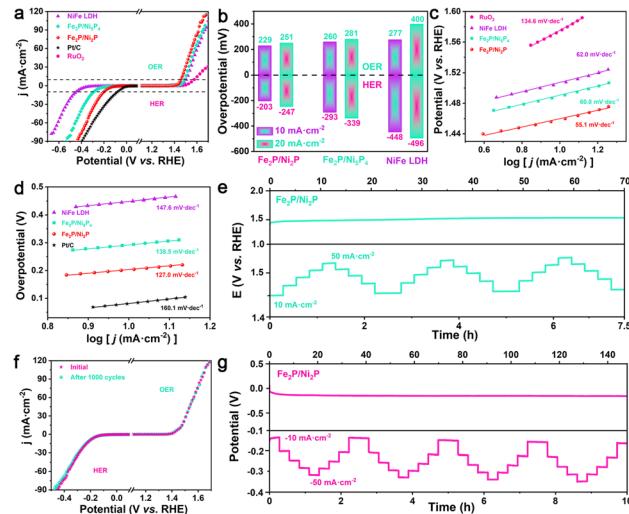


Fig. 5 (a) Electrocatalytic OER and HER performance of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and references in alkaline seawater solution. (b) Overpotential of the as-prepared samples at 10 and 20 mA cm $^{-2}$ for OER and HER. (c and d) Corresponding Tafel plots of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ for OER and HER. (e) Polarization curves for OER and HER after 1000 cycles. (f) CP curves and multi-step chronopotentiometry tests results of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ for OER and HER.

than those of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (293 and 339 mV), and NiFe LDH (448 and 496 mV). Fig. 5d demonstrates that the Tafel slope of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ is 127 mV dec $^{-1}$, which is lower than that of other as-prepared samples, indicating faster kinetics for HER. $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ displays apparent C_{dl} values of 0.71 and 13.4 mF cm $^{-2}$ for OER and HER beyond those of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (0.29 and 6.2 mF cm $^{-2}$) and NiFe LDH (0.48 and 1.5 mF cm $^{-2}$), which can be ascribed to the abundant exposed active sites of the nanosheets (Fig. S9 and S10 \dagger). The TOF values of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$, $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ and NiFe LDH follow the same trend as the apparent electrochemical activities in alkaline seawater solution (Fig. S11 \dagger). Furthermore, the cycling stability of the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ sample was further evaluated through continuous CV test, in which the LSV curves after 1000 cycles almost coincide with the initial curve, indicating its remarkable cyclability. Additionally, as shown in Fig. 5e and g, the CP test demonstrates that $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ maintains stable operation without remarkable current degradation for 70 and 140 h for OER and HER. The figures also display consecutive multi-step CP tests for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$, where the instant response in potential almost remains steady at each step. These results confirm that $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ exhibits exceptional OER/HER performance and enduring stability in harsh conditions. This is ascribed to the stronger BEF, and the existence of negatively charged anionic (PO_4^{3-}) layers that can repel Cl^- and thus protect the electrode from corrosion.

3.4 Mechanism discussion

Operando electrochemical impedance spectroscopy (EIS) was documented to gain a better understanding of the OER kinetics in the different catalyst surfaces.⁵⁰ As illustrated in Fig. 6a and d, the Nyquist plots of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ under different applied potentials were obtained, indicating various



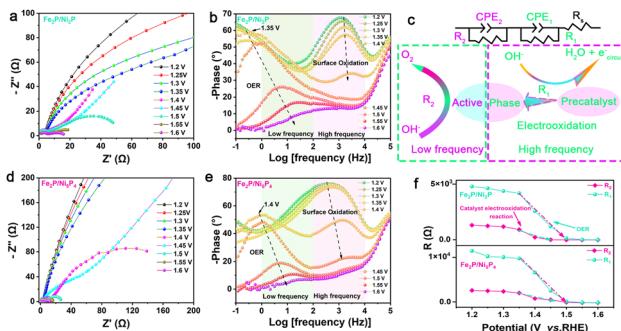


Fig. 6 (a and d) Operando Nyquist plots, (b and e) Bode-phase plots of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$. (c) Electrical equivalent circuit model used for analyzing the interfacial charge transfer. (f) Correlation of the equivalent resistances (R_1 and R_2) and potentials for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ and $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$.

electrochemical reaction properties. The equivalent circuits of two continuous electrochemical processes were employed for data fitting (Fig. 6c), and the best fitting parameters are shown in Tables S4 and S5.† The high-frequency (HF) region is considered to be the oxidation processes occurring within the electrode, whereas the low-frequency (LF) region is concerned with the asymmetric distribution of interface charges caused by the oxidized materials (Fig. 6b and e).¹⁰ R_1 and R_2 embody the oxidation resistance of the catalysts under electrochemical operation in the HF and LF zones, respectively. When the potential shifts from 1.2 to 1.6 V vs. RHE, after 1.4 V ($\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$) and 1.45 V ($\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$) in the HF region, the catalyst reconstruction concludes, R_1 becomes remarkably smaller and the OER occurs in the LF interface, indicating that $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ undergoes a severe surface electrooxidation process. Moreover, the phase angle of the LF region symbolizing the OER decreases earlier for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ (at 1.35 V) than for $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (at 1.4 V), suggesting that $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ is more susceptible to polarization. The changes in R_1 and R_2 with potentials in Fig. 6f indicate that $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ undergoes an accelerated rate of electrooxidation compared with $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$, and the OER process is faster.^{51–53}

In situ Raman techniques were conducted to explore the origin of the activity enhancement of the as-prepared black products of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ and $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalysts (Fig. 7a and b). As shown in Fig. 7c–f, the spectra of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ and $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ exhibit a prominent pair of peaks at 476 cm^{-1} (e_g bending vibration) and 554 cm^{-1} (A_{1g} $\text{Ni}^{\text{III}}\text{--O}$ stretching vibration) corresponding to characteristic peaks in the OER-active phase of $\gamma\text{-NiOOH}$ that appear at potentials of 1.5 and 1.4 V vs. RHE, respectively. No characteristic peaks assigned to FeOOH appear, suggesting Ni_2P undergoes a surface reconstruction process and is transformed into the $\text{Ni}\text{-OOH}$ active species during the OER test, while Fe_2P is still robust (white/black dotted oval frame in Fig. 7c).⁵⁴ Moreover, a weak band located in the range of $1000\text{--}1100\text{ cm}^{-1}$ can be observed in $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$, which can be ascribed to PO_4^{3-} .⁴⁹ The fitted band intensities of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ are stronger than those of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ (Fig. 7d), implying an accelerated partial phase transformation to disordered NiOOH . Furthermore, FT-IR spectra of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ were recorded to further confirm the phase transition before and after the OER test.

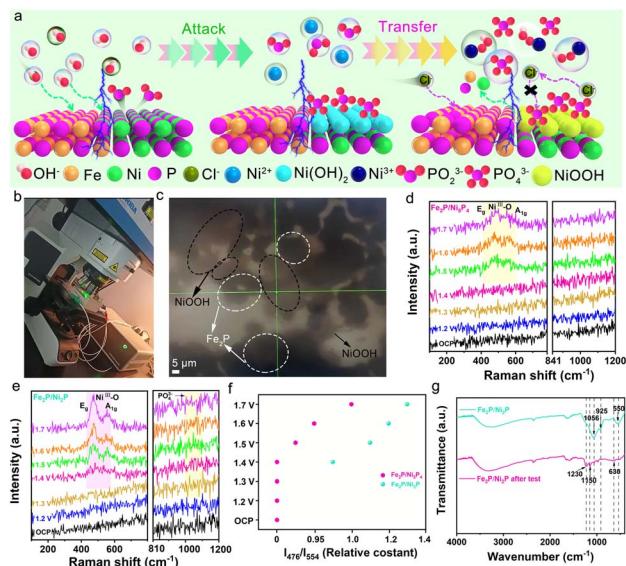


Fig. 7 (a) Schematic diagram of the possible evolution of catalyst. (b) The *in situ* Raman measurement device. (c) The image of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ in the *in situ* Raman test process. (d and e) *In situ* Raman spectra of $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ and $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ with different operating potentials (vs. RHE). (f) Comparison of the ratios of band intensity (I_{476}/I_{554}). (g) FT-IR spectra of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ before and after test.

Fig. 7g shows that the dominant absorption bands belonging to $\text{M}\text{-P}$ and ν_4 ($\text{O}\text{-P}\text{-O}$) become weaker after OER operation. Three new absorption peaks appear at 630 cm^{-1} ($\text{Ni}\text{-O}\text{-H}$), 1150 cm^{-1} (PO_4^{3-}) and 1230 cm^{-1} (NiOOH) after the reaction.^{55,56} These above results suggest that $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ will interact with OH^- to form $\text{Fe}_2\text{P}/\text{Ni}(\text{OH})_2$ first, and will then be further oxidized and evolve to $\text{Fe}_2\text{P}/\text{NiOOH}$ during the OER process ($\text{Fe}_2\text{P}/\text{Ni}(\text{OH})_2 + \text{OH}^- \rightarrow \text{Fe}_2\text{P}/\text{NiOOH} + \text{H}_2\text{O} + \text{e}^-$). The *in situ* Raman and FT-IR confirm the existence of NiOOH and the formation and adsorption of PO_4^{3-} on the electrode surface, where the negatively charged PO_4^{3-} layer can protect the active species NiOOH from corrosion by repulsing Cl^- (Fig. 7a).⁷ After the OER test, $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ shows negligible change in the XRD pattern, except that the peak intensity becomes weaker than that before the test, indicating that the electrode undergoes surface reconstruction and partial transformation into the corresponding amorphous NiOOH (Fig. S12†). It is particularly important to note that $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ displays a potential loss of 42 mV, whereas the loss of activity of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ can be ignored under 50 mA cm^{-2} for 30 h, showing that the PO_4^{3-} of the electrode surface plays a crucial role in maintaining OER active sites (Fig. S13†). In addition, partial Fe elements were dissolved from $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ in the initial period of the stability test (from 0 to 20 h), but the loss of Fe element had not remarkably increased after 20 h, showing that Fe leaching had increasingly stopped, attaining a dynamic balance process. However, the Ni element could not be detected in seawater electrolyte after 30 h of continuous operation, confirming that the formed negatively charged PO_4^{3-} layer at the electrode surface can protect the NiOOH active species from corrosion and dissolution by repulsing Cl^- ions (Fig. S14†). $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ shows a negative zeta

potential (-17.86 eV), while $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ exhibits higher surface electronegativity (-18.93 eV), indicating the adsorption of a PO_4^{3-} protective layer on the surface of catalyst (Fig. S15†). Furthermore, the active chlorine concentration in alkaline seawater solution was investigated and detected using the colorimetric method and UV/Vis spectroscopy (Fig. S16–S18†). The hypochlorite content did not increase after 30 h of CP testing, suggesting that the Cl^- evolution was significantly inhibited.⁴⁰ Corrosion polarization plots (Fig. S19†) demonstrate a higher potential and a smaller j for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ than for $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$, indicating that $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ with the strongest BEF can facilitate the adsorption of intermediates, thus showing stronger resistance against chloride corrosion.⁷ As a result, the $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ catalysts with weaker BEF dissolve successively, while $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ is very robust (Fig. S20†).

To emphasize the tremendous potential of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ for practical application, a lab-scale AEMWE device was built (Fig. 8a). The overall water-splitting (OWS) performance of the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst in the AEMWE system was documented using LSV in 1 M KOH electrolyte. As shown in Fig. 8b, the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst requires only a voltage of 1.63 V to achieve η_{10} , which is superior to other recently reported bifunctional electrocatalysts (Fig. 8c and Table S7†). Moreover, in Fig. 8d, the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst demonstrates good stability over 80 h in the AEMWE system, indicating highly promising potential for practical application. Previous tests have demonstrated that the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst exhibits excellent activity in alkaline HER, OER, and OWS, suggesting the superior all-around catalytic activity of the target catalyst. The mechanisms of improved OER and HER performance for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ can be summarized, as schematically illustrated in Fig. 8e. The large $\Delta\Phi$ will drive spontaneous electron transfer from Fe_2P to Ni_2P in heterogeneous $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$,

and concurrently a strong interfacial BEF with an asymmetric charge distribution is constructed.^{57,58} During the water-splitting process, water molecules are first adsorbed on the catalyst surface and dissociated into intermediates (Volmer step). The negative-charge-rich Ni_2P region prefers to absorb hydrogen intermediates, and subsequently generates hydrogen molecules by combining with two electrons. Meanwhile, the oxygen species are attracted by the positive-charge-enriched Ni_2P side for catalyzing OER, which facilitates the shedding of hydrogen protons by decreasing the free energy in $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$. Therefore, significant bifunctionality for OWS activity is developed. For comparison, the adsorption of hydrogen protons by Ni_2P and Fe_2P is either too strong or too weak for HER, while the high energy barrier for the shedding of hydrogen protons for OER is attributed to the conventional charge distribution.

4. Conclusions

We have exquisitely designed and manipulated a Br-induced partial *in situ* phase transition from $\text{Fe}_2\text{P}/\text{Ni}_5\text{P}_4$ to $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ under the phosphorization process, which leads to a strong BEF due to the large $\Delta\Phi$ difference. As a result, the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ catalyst demonstrates remarkable OER and HER activity with low overpotentials of 196, 108 mV for freshwater and 229, 203 mV for seawater, respectively. Experiments and *in situ/ex situ* spectroscopic investigations confirm that the enhanced BEF plays an important role in subtly engineering absorption strength for reaction intermediates and phosphate intermediates due to an asymmetric charge distribution at the $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ interface. In particular, the existence of high-valence NiOOH and the co-existence of adsorbed PO_4^{3-} at the electrode surface confirm that the negatively charged PO_4^{3-} layer can protect the NiOOH active species from corrosion by repulsing Cl^- . Moreover, $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ also exhibits a low cell voltage for an AEMWE system. This work paves the way for synthesizing bifunctional seawater/water-splitting electrocatalysts by exquisitely designing and modulating the interfacial BEF.

Data availability

All data that support the findings of this study are included within the article.

Author contributions

Lei Jin: conceptualization, methodology, writing – original draft, data curation, visualization. Hui Xu: methodology, formal analysis, writing – review & editing. Kun Wang: data curation. Yang Liu: investigation. Xingyue Qian: formal analysis, supervision, writing – review & editing. Haiqun Chen: project administration. Guangyu He: validation, funding acquisition, resources.

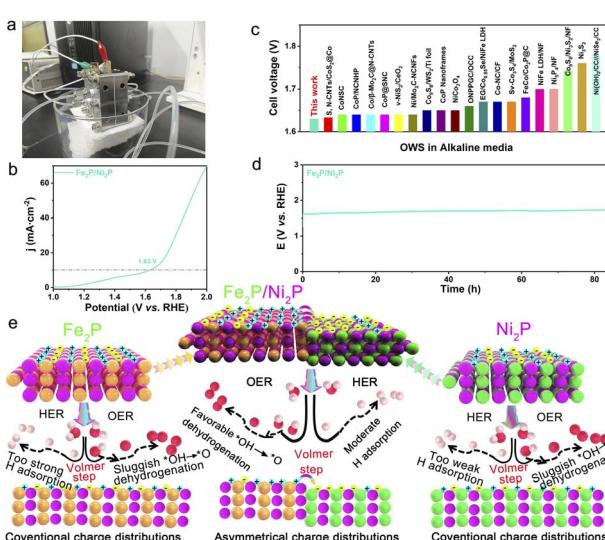


Fig. 8 (a) The AEMWE device. (b) Polarization curves of AEM water electrolyzer with $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$. (c) Comparison of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ with reported bifunctional electrocatalysts at 10 mA cm^{-2} . (d) Stability of $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}/\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ at 10 mA cm^{-2} in AEMWE. (e) Schematic illustration of OER and HER mechanisms for $\text{Fe}_2\text{P}/\text{Ni}_2\text{P}$ bifunctional electrocatalyst.



Conflicts of interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Acknowledgements

This work was financially supported by National Natural Science Foundation of China (No. 22305025, 21978026, 22078028) and the Natural Science Foundation of Jiangsu Province (BK20230640). We also thank the Analysis and Testing Center of Changzhou University for assistance in characterizations.

Notes and references

- S. Zhang, C. Tan, R. Yan, X. Zou, F. L. Hu, Y. Mi, C. Yan and S. Zhao, *Angew. Chem., Int. Ed.*, 2023, **135**, e202302795.
- B. Huang, J. Yan, Z. Li, L. Chen and J. Shi, *Angew. Chem., Int. Ed.*, 2024, **63**, e202409419.
- H. Xu, Y. Zhao, Q. Wang, G. He and H. Chen, *Coord. Chem. Rev.*, 2022, **451**, 214261.
- S. Zhao, H. Li, J. Dai, Y. Jiang, G. Zhan, M. Liao, H. Sun, Y. Shi, C. Ling and Y. Yao, *Nat. Sustain.*, 2024, **7**, 148–157.
- Y. Yang, J. Lou, Y. Zhao, J. Wei, Y. Zhou, C. Zhang, M. Wu, Y. Zhang, Q. Wang, L. Wang, T. Yang and X. Song, *Chem. Eng. J.*, 2023, **477**, 146900.
- H. Xu, K. Wang, G. He and H. Chen, *J. Mater. Chem. A*, 2023, **11**, 17609–17615.
- J. Wei, J. Lou, W. Hu, X. Song, H. Wang, Y. Yang, Y. Zhang, Z. Jiang, B. Mei, L. Wang, T. Yang, Q. Wang and X. Li, *Small*, 2024, **20**, e202308956.
- H. Xu, Y. Liu, K. Wang, L. Jin, J. Chen, G. He and H. Chen, *Inorg. Chem.*, 2024, **63**, 16037–16046.
- H. Xu, L. Yang, Y. Liu, L. Jin, K. Wang, G. He and H. Chen, *Fuel*, 2024, **377**, 132796.
- S. Zhao, Y. Wang, Y. Hao, L. Yin, C. H. Kuo, H. Y. Chen, L. Li and S. Peng, *Adv. Mater.*, 2024, **36**, 2308925.
- X. Xu, A. Cao, W. You, Z. Tao, L. Kang and J. Liu, *Small*, 2021, **17**, 2101725.
- S. Zhang, C. Zhang, X. Zheng, G. Su, H. Wang and M. Huang, *Appl. Catal., B*, 2023, **324**, 122207.
- H. Xu, L. Jin, K. Wang, L. Yang, Y. Liu, G. He and H. Chen, *Fuel*, 2024, **369**, 131716.
- X. Zhao, M. Liu, Y. Wang, Y. Xiong, P. Yang, J. Qin, X. Xiong and Y. Lei, *ACS Nano*, 2022, **16**, 19959–19979.
- J. Yao, W. Huang, W. Fang, M. Kuang, N. Jia, H. Ren, D. Liu, C. Lv, C. Liu and J. Xu, *Small Methods*, 2020, **4**, 2000494.
- H. Xu, L. Yang, L. Jin, Y. Liu, K. Wang, J. Chen, G. He and H. Chen, *J. Colloid Interface Sci.*, 2025, **677**, 158–166.
- C. Guo, H. Xue, J. Sun, N. Guo, T. Song, J. Sun, Y.-R. Hao and Q. Wang, *Chem. Eng. J.*, 2023, **470**, 144242.
- H. Xu, J. Li and X. Chu, *Nanoscale Horiz.*, 2023, **8**, 441–452.
- T. Xu, D. Jiao, L. Zhang, H. Zhang, L. Zheng, D. J. Singh, J. Zhao, W. Zheng and X. Cui, *Appl. Catal., B*, 2022, **316**, 121686.
- K. Ren, W. J. Xu, K. Li, J. M. Cao, Z. Y. Gu, D. H. Liu, D. M. Dai, W. L. Li and X. L. Wu, *Adv. Funct. Mater.*, 2024, 2415585.
- L. Jin, H. Xu, K. Wang, L. Yang, Y. Liu, X. Qian, G. He and H. Chen, *Appl. Surf. Sci.*, 2024, 159777.
- H.-M. Yang, H.-Y. Wang, S. Zhai, J.-T. Ren and Z.-Y. Yuan, *Chem. Eng. J.*, 2024, **489**, 151236.
- Y. Li, Y. Wu, H. Hao, M. Yuan, Z. Lv, L. Xu and B. Wei, *Appl. Catal., B*, 2022, **305**, 121033.
- D. Li, C. Zhou, R. Yang, Y. Xing, S. Xu, D. Jiang, D. Tian and W. Shi, *ACS Sustain. Chem. Eng.*, 2021, **9**, 7737–7748.
- H. T. Dao, S. Sidra, M. Mai, M. Zharnikov and D. H. Kim, *Chem. Eng. J.*, 2024, 150054.
- H. Liu, L. Jiang, Y. Sun, J. Khan, B. Feng, J. Xiao, H. Zhang, H. Xie, L. Li and S. Wang, *Adv. Energy Mater.*, 2023, **13**, 2301223.
- D. Yue, T. Feng, Z. Zhu, S. Lu and B. Yang, *ACS Catal.*, 2024, **14**, 3006–3017.
- J. Li, G. Wei, Y. Zhu, Y. Xi, X. Pan, Y. Ji, I. V. Zatovsky and W. Han, *J. Mater. Chem. A*, 2017, **5**, 14828–14837.
- S. Mondal, D. Bagchi, M. Riyaz, S. Sarkar, A. K. Singh, C. Vinod and S. C. Peter, *J. Mater. Chem. A*, 2022, **144**, 11859–11869.
- M. Asim, B. Maryam, S. Zhang, M. Sajid, A. Kurbanov, L. Pan and J.-J. Zou, *J. Colloid Interface Sci.*, 2023, **638**, 14–25.
- J. Zhu, J. Chi, X. Wang, T. Cui, L. Guo, B. Dong, X. Liu and L. Wang, *Nano Energy*, 2024, **121**, 109249.
- K. Wang, S. He, B. Li, H. Du, T. Wang, Z. Du, L. Xie and W. Ai, *Appl. Catal., B*, 2023, **339**, 123136.
- Y. Li, X. Yu, J. Gao and Y. Ma, *Chem. Eng. J.*, 2023, **470**, 144373.
- K. Chang, D. T. Tran, J. Wang, K. Dong, S. Prabhakaran, D. H. Kim, N. H. Kim and J. H. Lee, *Appl. Catal., B*, 2023, **338**, 123016.
- Z. Li, C. Xu, Z. Zhang, S. Xia, D. Li, L. Liu, P. Chen and X. Dong, *Adv. Sci.*, 2024, 2308477.
- X. Pei, J. Bian, W. Zhang, Z. Hu, Y. H. Ng, Y. Dong, X. Zhai, Z. Wei, Y. Liu and J. Deng, *Adv. Funct. Mater.*, 2024, 2400542.
- H. Y. Chen, L. Yang, R. X. Wang, W. J. Zhang, R. Liu, Y. Z. Yun, N. Wang, S. Ramakrishna, L. Jiao and Y. Z. Long, *Small*, 2023, **19**, 2304086.
- L. Yang, X. Cao, X. Wang, Q. Wang and L. Jiao, *Appl. Catal., B*, 2023, **329**, 122551.
- M. Gu, L. Jiang, S. Zhao, H. Wang, M. Lin, X. Deng, X. Huang, A. Gao, X. Liu and P. Sun, *ACS Nano*, 2022, **16**, 15425–15439.
- X. Yan and Z. Jin, *Chem. Eng. J.*, 2021, **420**, 127682.
- Y. Song, M. Sun, S. Zhang, X. Zhang, P. Yi, J. Liu, B. Huang, M. Huang and L. Zhang, *Adv. Funct. Mater.*, 2023, **33**, 2214081.
- P. Zhao, S. Fu, Y. Luo, C. Peng, L. Cheng and Z. Jiao, *Small*, 2023, **19**, 2305241.
- W. Chen, W. Wei, F. Li, Y. Wang, M. Liu, S. Dong, J. Cui, Y. Zhang, R. Wang and K. Ostrikov, *Adv. Funct. Mater.*, 2024, **34**, 2310690.
- S. Zhang, X. Wei, S. Dai, H. Wang and M. Huang, *Adv. Funct. Mater.*, 2024, **34**, 2311370.
- S. Zhang, Y. Wang, X. Wei, L. Chu, W. Tian, H. Wang and M. Huang, *Appl. Catal., B*, 2023, **336**, 122926.



46 S. M. El-Refaei, P. A. Russo, T. Schultz, Z. N. Chen, P. Amsalem, N. Koch and N. Pinna, *Carbon Energy*, 2023, e556.

47 Y. Shi, S. Zhou, J. Liu, X. Zhang, J. Yin, T. Zhan, Y. Yang, G. Li, J. Lai and L. Wang, *Appl. Catal., B*, 2024, **341**, 123326.

48 J. Liu, S. Duan, H. Shi, T. Wang, X. Yang, Y. Huang, G. Wu and Q. Li, *Angew. Chem., Int. Ed.*, 2022, **134**, e202210753.

49 W. Liu, J. Yu, M. G. Sendeku, T. Li, W. Gao, G. Yang, Y. Kuang and X. Sun, *Angew. Chem., Int. Ed.*, 2023, **135**, e202309882.

50 S. Fu, Y. Ma, X. Yang, X. Yao, Z. Jiao, L. Cheng and P. Zhao, *Appl. Catal., B*, 2023, **333**, 122813.

51 H.-Y. Wang, S.-F. Hung, H.-Y. Chen, T.-S. Chan, H. M. Chen and B. Liu, *J. Am. Chem. Soc.*, 2016, **138**, 36–39.

52 Y. Li, Y. Wu, M. Yuan, H. Hao, Z. Lv, L. Xu and B. Wei, *Appl. Catal., B*, 2022, **318**, 121825.

53 N. Zhang, Y. Hu, L. An, Q. Li, J. Yin, J. Li, R. Yang, M. Lu, S. Zhang and P. Xi, *Angew. Chem., Int. Ed.*, 2022, **61**, e202207217.

54 B. Wu, S. Gong, Y. Lin, T. Li, A. Chen, M. Zhao, Q. Zhang and L. Chen, *Adv. Mater.*, 2022, **34**, 2108619.

55 S. Wang, P. Yang, X. Sun, H. Xing, J. Hu, P. Chen, Z. Cui, W. Zhu and Z. Ma, *Appl. Catal., B*, 2021, **297**, 120386.

56 Z.-Y. Yu, Y. Duan, J.-D. Liu, Y. Chen, X.-K. Liu, W. Liu, T. Ma, Y. Li, X.-S. Zheng and T. Yao, *Nat. Commun.*, 2019, **10**, 2799.

57 D. Chen, R. Lu, R. Yu, Y. Dai, H. Zhao, D. Wu, P. Wang, J. Zhu, Z. Pu and L. Chen, *Angew. Chem., Int. Ed.*, 2022, **61**, e202208642.

58 W. Zhang, L. Yang, Z. Li, G. Nie, X. Cao, Z. Fang, X. Wang, S. Ramakrishna, Y. Long and L. Jiao, *Angew. Chem., Int. Ed.*, 2024, **63**, e202400888.

