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# Applications of Ti/TiO<sub>2</sub> nanotube arrays/CeO<sub>2</sub>@PbO<sub>2</sub> and Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> electrodes for efficient electrocatalytic degradation of paraquat: cell design and comprehensive mechanistic studies

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Ti/TiO<sub>2</sub> nanotube arrays (NTA)/CeO<sub>2</sub>@PbO<sub>2</sub> and Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> electrodes were used for the electrocatalytic degradation of paraquat (PQ<sup>2+</sup>), a highly toxic and widely used herbicide. The fabricated electrodes were characterized by XPS, SEM, EDS, mapping, XRD and EIS methods. The results show that the performance of the Ti/TiO<sub>2</sub> nanotube in the electrocatalytic degradation of PQ<sup>2+</sup> is better than that of the Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> electrode. This electrode increases the production of hydroxyl radicals and degradation efficiency. The results show that the highest degradation efficiency of 75% was achieved at pH = 7, a current density of 7.8 mA cm<sup>-2</sup> and an initial concentration of 50 ppm. The intermediate species formed during the electrolysis of PQ<sup>2+</sup> were analyzed based on cyclic voltammetry, UV-vis spectroscopy and LC-MS techniques, and a possible mechanism for the degradation of PQ<sup>2+</sup> was proposed. In the second part of this study, the electrochemical behavior of PQ<sup>2+</sup> was studied, gaining a deeper insight and understanding of the redox properties and adsorption activity of this molecule.

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## Introduction

On average, 2 million tons of pesticides are used annually in the world to fight against pests, insects and weeds and herbicides are the most widely used type, accounting for 47.5% of global pesticide consumption. Paraquat (PQ<sup>2+</sup>) (1,1'-dimethyl-4,4'-bipyridinium dichloride) (also known as methyl viologen) is a non-selective broad-spectrum herbicide that has been widely used for decades. When this pollutant enters the body, it circulates through the bloodstream and is fixed in various tissues, causing serious diseases and even death. The toxicity of PQ<sup>2+</sup> has been found to be related to the production of superoxide ions.<sup>1</sup>

Various methods have been reported for the removal of PQ<sup>2+</sup> from aquatic environments. Adsorption methods are effective for the treatment of PQ<sup>2+</sup>. In these methods, adsorbents such as activated carbon,<sup>2</sup> activated bleaching earth,<sup>3</sup> modified zeolite,<sup>4</sup> methacrylic acid-modified rice husk,<sup>5</sup> clays<sup>6</sup> and montmorillonite<sup>7</sup> are typically used. The main drawback of these methods is secondary pollution. Another category of PQ<sup>2+</sup> treatment methods is advanced oxidation processes (AOPs). These methods are based on the generation and use of hydroxyl radicals (a powerful oxidant) created by chemical reactions.

These methods include heterogeneous photocatalytic processes in the presence of TiO<sub>2</sub> (ref. 8) or UV ozonation<sup>9</sup> methods for the degradation/mineralization of PQ<sup>2+</sup>. These methods do not have the drawbacks of the previous method due to the mineralization of organic pollutants. In addition to the above-mentioned methods, electrochemical advanced oxidation methods (EAOP), as a more progressive method, have also been used for the degradation of PQ<sup>2+</sup>. In these methods, the degradation of organic pollutants is done by the *in situ* electrochemical generation of hydroxyl radicals.<sup>10</sup> These methods include anodic oxidation (AO),<sup>11,12</sup> Fenton,<sup>13</sup> electro-Fenton (EF),<sup>11,13</sup> photoelectron-Fenton (PEF),<sup>11,13</sup> photoelectrooxidation.<sup>13</sup> Each of these methods has its own advantages and disadvantages. In addition, recently, Khelifi and colleagues used a novel palladium-based perovskite catalyst as a cathodic modifier in a boron-doped diamond (BDD)-assisted electro-Fenton system for the degradation of PQ<sup>2+</sup>. This electrode significantly accelerated the degradation process and led to almost complete mineralization under optimal conditions.<sup>14</sup>

Direct electrochemical methods using boron-doped diamond (BDD) electrodes have also been used to decompose PQ<sup>2+</sup>. In 2024, Teutli-Sequeira *et al.* used a commercial BDD film at circumneutral pH for PQ<sup>2+</sup> mineralization due to its lower energy and fewer chemical requirements, as well as the mechanical stability of BDD electrodes.<sup>15</sup> They succeeded in mineralizing PQ<sup>2+</sup> by more than 90%. Also, Bautista-Garcia *et al.* (2025) performed the degradation of PQ<sup>2+</sup> using the BDD-Fe

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system by the UVA-LED photoelectrooxidation method.<sup>16</sup> Using this method, they were able to remove this herbicide with an efficiency of 77% under optimal conditions. In a comprehensive and interesting study, Rabaoui *et al.* (2025) investigated the electrochemical degradation of  $PQ^{2+}$  using a BDD anode.<sup>17</sup> They investigated the effect of operational variables, including the effect of anode material, and reported that BDD electrodes showed the most efficient performance, achieving COD and TOC removal rates of 99% and 98.6%, respectively. The results of these methods are valuable, and BDD allows for the complete mineralization of organic pollutants; however, these electrodes are very expensive, which limits their use.

In order to develop the use of efficient and cost-effective Ti/TiO<sub>2</sub>/CeO<sub>2</sub>@PbO<sub>2</sub> nanotube arrays and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrodes for the degradation of persistent pollutants, in the present study, the electrocatalytic activity and degradation efficiency of these electrodes for the degradation of  $PQ^{2+}$  were investigated. The results show that the Ti/TiO<sub>2</sub>/CeO<sub>2</sub>@PbO<sub>2</sub> nanotube has better efficiency in the degradation of  $PQ^{2+}$  than that of the Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrode. We also designed a new electrochemical cell for the degradation of  $PQ^{2+}$ . Using this cell, the degradation efficiency was increased by 95% and energy consumption was reduced by 40%. In addition, in this research, we made considerable efforts to develop more active electrode materials for the degradation of  $PQ^{2+}$  and advance the frontiers of knowledge in the field of its electrochemical properties. We believe that the outcome of this research can serve as a good guide for removing this herbicide from aquatic environments. On the other hand, the results of the electrochemical studies conducted in this research lead to a deeper insight and understanding of the redox properties and adsorption activity of  $PQ^{2+}$ .

## Experimental section

### Apparatus and reagents

Chemicals used in this study, including oxalic acid, Pb(NO<sub>3</sub>)<sub>2</sub>, Ce(NO<sub>3</sub>)<sub>3</sub>, NaOH, NaF, ethylene glycol, Cu(NO<sub>3</sub>)<sub>2</sub>, HNO<sub>3</sub>, NH<sub>4</sub>F, Na<sub>2</sub>SO<sub>4</sub>, were purchased from Sigma-Aldrich and Merck. All of the chemicals were of analytical grade and used directly without further purification. Paraquat was obtained from Alborz Behsam Company, Tehran, Iran. The buffers used in this research were prepared by dissolving HClO<sub>4</sub> (for pH: 1), H<sub>3</sub>PO<sub>4</sub> (for pHs: 2, 3, 6, 7, 8), acetic acid (for pHs: 4, 5), NaHCO<sub>3</sub> (for pHs: 9, 10) and Na<sub>2</sub>CO<sub>3</sub> (for pHs: 11, 12) in deionized water and adjusting the pH value using NaOH or HCl solutions.

A model 691 pH meter (Metrohm, Switzerland) was used for pH measurements. The crystalline structure of the electrodes was investigated through X-ray diffraction (XRD, Italstructure, ADP200, Italy and GNR explorer, Italy) with a radiation source of Cu K $\alpha$  in the  $2\theta$  range of 20 to 90 at the wavelength of 0.154 nm. The elemental chemical state was analyzed using X-ray photoelectron spectroscopy (XPS, Thermo Fisher Scientific K-ALPHA) with an Al K $\alpha$  source. To evaluate the morphology of bare and modified electrodes, scanning electron microscopy (SEM, TESCAN-MIRA3-XMU) images in different magnifications were employed. For determining chemical elements and their

distribution, energy-dispersive X-ray spectroscopy (EDS) and elemental mapping assay were utilized, respectively. Electrochemical degradation and electrodeposition were performed using a DC power supply (MEGATEC MP-3005, CHINA). The UV-vis absorption spectra of the solutions were obtained using an Analytik Jena Specord 210 UV-vis spectrophotometer. Organic intermediates formed during the degradation of  $PQ^{2+}$  were analyzed using liquid chromatography-mass spectrometry (LC-MS). LC-MS analysis was conducted with a Shimadzu LCMS-2010A system equipped with a Eurospher C18 column. The mobile phase consisted of a mixture of acetonitrile (ACN) with 0.1% formic acid and water with 0.1% formic acid. For this purpose, a few milliliters of the  $PQ^{2+}$  solution were collected during electrolysis and analyzed using LC-MS in a certified laboratory. Electrochemical measurements were performed using an Auto Lab®/PGSTAT30 potentiostat/galvanostat (Eco Chemie, Utrecht, The Netherlands). Electrochemical impedance spectroscopy (EIS) was performed using Zahner Zennium and Thales software (Version of 5.0.6.1). To calculate energy consumption, the same DC power supply (MEGATEC MP-3005, China) was used to apply a constant current ( $\pm 3$  mA) and record the cell potential ( $\pm 3$  mV).

The concentration of metal ions in the catalyst was evaluated using inductively coupled plasma-optical emission spectrometry (ICP-OES; 730-ES Varian).

### Electrochemical cell

In this study, a new glass electrochemical cell with a volume of 200 ml was designed and built to achieve the lowest cost and highest efficiency of electrochemical degradation (Fig. 1). The prominent feature of this cell is the increase in the ratio of the electrode surface area to the cell volume, which increases the production of hydroxyl radicals, and as a result, increases the efficiency of the cell. In this cell, the cathode is a stainless steel mesh, with a thickness of 0.1 cm, a height of 5.0 cm and an area of 101 cm<sup>2</sup>, which is attached to the inner wall of the cell, as shown. This cell is also equipped with four plate anodes (5  $\times$  3.5 cm<sup>2</sup> and a thickness of 0.1 cm), with an area of 140 cm<sup>2</sup>, which

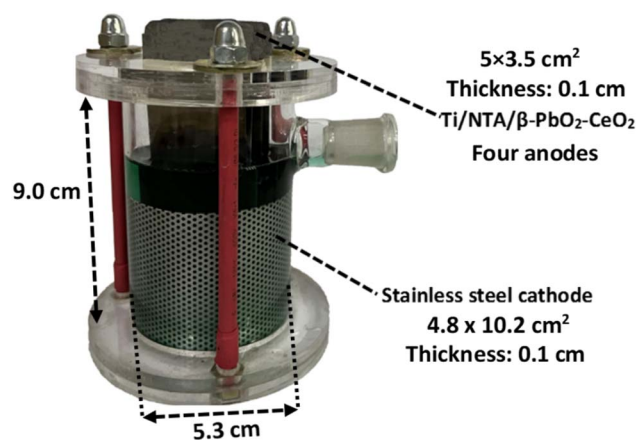


Fig. 1 Cell design for the electrochemical degradation of  $PQ^{2+}$  using the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode.



are located in the center. In this cell, the distance between the electrodes is 1 cm, and a magnetic stirrer was used to facilitate convective mass transfer during the electrocatalytic degradation of  $PQ^{2+}$ . This cell operates at current densities of 4.7 and 7.8 mA  $cm^{-2}$ .

### Pretreatment of the titanium surface

A titanium sheet (grade 1) with dimensions of 5 cm  $\times$  2 cm  $\times$  0.1 cm with an effective surface of 21 cm<sup>2</sup> was used. First, the Ti sheet was polished using sandpaper (grit 400) to obtain a smoother surface. After that, the Ti sheet was sonicated in 1 M sodium hydroxide at room temperature for 40 minutes to remove the oxides and impurities and then washed with distilled water. In the next step, the Ti sheet was immersed in boiling 30% oxalic acid for 1 hour and then washed with distilled water. The reason for using boiling oxalic acid was to effectively remove all impurities and create a sufficiently rough surface for electrochemical deposition. After that, the Ti sheet is immersed in boiling distilled water for 30 minutes to clean the surface of residual oxalic acid.<sup>18</sup> Using this method, three Ti sheets were prepared as the anode substrate, which had a total effective area of 63 cm<sup>2</sup>.

### Preparation of Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub>

In order to prepare Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub>, a cell consisting of treated Ti sheets (see previous section) as anode and two stainless steel sheets as cathode, containing Pb(NO<sub>3</sub>)<sub>2</sub> (0.5 M), Cu(NO<sub>3</sub>)<sub>2</sub> (0.2 M), HNO<sub>3</sub> (0.1 M), NaF (0.01 M) and 2.5 vol% ethylene glycol, was electrolyzed at a current density of 10 mA  $cm^{-2}$  at 65 °C for 120 min.<sup>19</sup> More details on the electrode preparation method are reported in ref. 19.

### Preparation of Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub>

In the first step to prepare Ti/NTA, the treated Ti sheets (see Pretreatment of the titanium surface section) as anode and stainless steel sheets (with the same dimensions) as cathode were placed alternately with a distance of 0.5 cm in a cell containing a solution of ethylene glycol-water (95% v/v) and 0.3% NH<sub>4</sub>F. Then, the cell was electrolyzed for 240 minutes with an

applied potential of 30 V at room temperature. After that, the titanium sheets were placed in a furnace at 450 °C for 120 minutes. In the next step, the titanium sheets were electrolyzed in an electrochemical cell containing 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> by applying a current density of 3 mA  $cm^{-2}$  for 15 minutes at room temperature.<sup>20,21</sup> In the next step, Ti/NTA electrodes as anodes and stainless steel sheets as cathodes were placed in a solution containing Pb(NO<sub>3</sub>)<sub>2</sub> (0.5 M), Ce(NO<sub>3</sub>)<sub>3</sub> (0.004 M), NaF (0.01 M) and HNO<sub>3</sub> (0.1 M) and electrolyzed at a current density of 10 mA  $cm^{-2}$  for 2 hours at room temperature.<sup>22</sup> The preparation steps of the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode are shown in Fig. 2. More details on the electrode preparation are reported in ref. 20–22.

## Results and discussion

### Electrode characterization

Understanding the structure of the electrode and tracking its structural changes during the pollutant degradation process is very important to analyze the pollutant degradation mechanism. XPS, SEM, EDS-mapping, XRD analysis and EIS were performed to investigate the electrode surface characteristics.

**XPS analysis.** XPS analysis was performed to clarify the chemical state of Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrode compositions. Fig. 3 shows the survey scan of both Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrodes. Fig. 4 shows

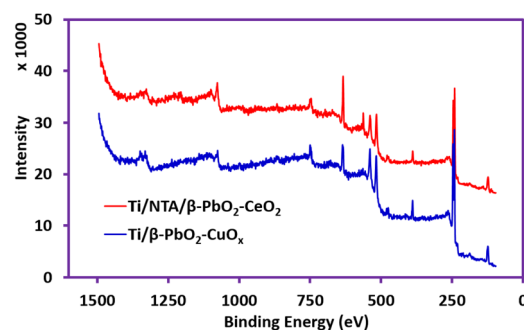


Fig. 3 XPS survey scan (between 1500 and 0 eV) of Ti-NTA-PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrodes.

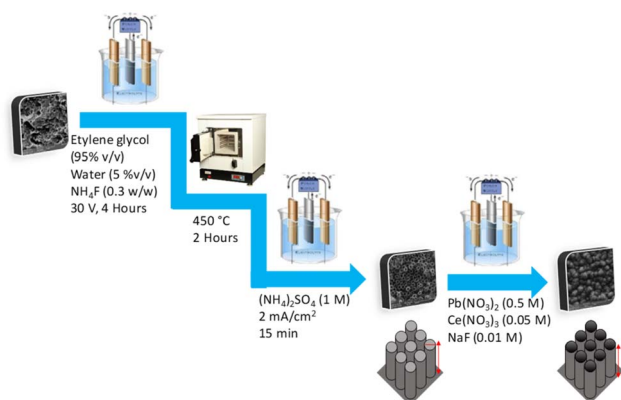


Fig. 2 Preparation steps of the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode.

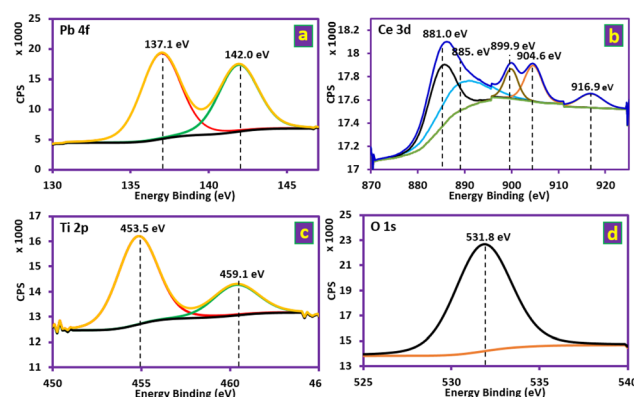


Fig. 4 Deconvoluted XPS spectra of the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode at Pb 4f, Ce 3d Ti 2p and O 1s core levels.



the high-resolution spectrum of the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode, demonstrating the successful stabilization of the tetravalent oxidation state of Pb in the nanostructured complex. Fig. 4a displays the Pb 4f core level spectrum, with binding energies (BE) of 137.1 and 142.0 eV, corresponding to Pb 4f 7/2 and Pb 4f 5/2, respectively, with a 4.9 eV spin-orbit splitting.<sup>23</sup> The Ce 3d core level spectrum (Fig. 4b) exhibits five peaks corresponding to three pairs of spin-orbit doublets. Due to the low amount of Ce in the electrode composition, one of the peaks remains unobserved.<sup>24–26</sup> Fig. 4c shows the Ti 2p core level spectrum, and the BE values of 453.5 and 459.1 eV correspond to Ti 2p 3/2 and Ti 2p 1/2, respectively, and spin-orbit splitting at 5.6 eV, indicating the oxidation state of titanium as Ti<sup>4+</sup>.<sup>27</sup> Fig. 4d shows the O 1s core spectrum with a BE of 531.8 eV, suggesting O–Pb and O–Ti bonding.<sup>28,29</sup> Fig. 5 shows the high-resolution spectrum of the Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrode. The Pb 4f core level spectrum is displayed in Fig. 5a; the BE values of 137.1 and 142.0 eV correspond to Pb 4f 7/2 and Pb 4f 5/2, respectively, with a 4.9 eV splitting, which confirms the predominant phase is the  $\beta$ -phase.<sup>28</sup> Fig. 5b depicts the Cu core level spectrum with a BE of 933.0 eV. Due to the low amount of Cu in the electrode composition, spin-orbit splitting is not observed. Fig. 5c shows the Ti 2p core level spectrum, with the BE of 456.6 and 462.8 eV and a 6.2 eV splitting, showing the Ti<sup>0</sup> state.<sup>29</sup> Fig. 5d depicts O 1s with a BE of 530.9 eV, indicative of the O–Cu bond.<sup>30</sup>

**XRD analysis.** The XRD pattern of the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode is shown in Fig. 6. The peaks with  $2\theta$  values of 31.85° (101), 36.06° (200), 48.93° (211), 62.30° (301), 66.58° (202), 74.12° (321) and 85.40° (411) correspond to  $\beta$ -PbO<sub>2</sub>. The peaks with  $2\theta = 29.7^\circ$  (111) and  $58.8^\circ$  (222) correspond to CeO<sub>2</sub> and the peak with a  $2\theta$  of 25.26° (101) corresponds to the TiO<sub>2</sub> anatase phase. All peaks are in good agreement with ICSD card 89-2805.<sup>31,32</sup> Ce doping with PbO<sub>2</sub> may be the reason for reducing the size of PbO<sub>2</sub> crystals, thereby increasing the specific surface area and electrocatalytic activity of the electrode, and can also accelerate the lifetime of the electrode.<sup>33</sup> The XRD pattern of the Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrode is also shown in Fig. 6.

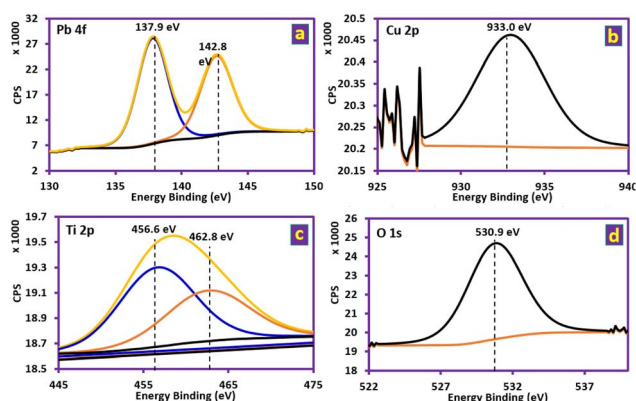


Fig. 5 Deconvoluted XPS spectrum of the Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrode at Pb 4f, Cu 2p, Ti 2p and O 1s core levels.

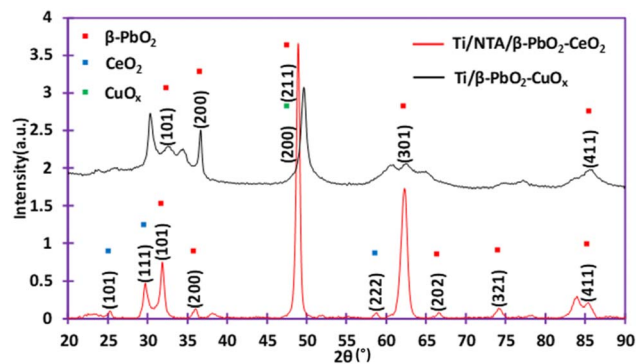


Fig. 6 Comparison of diffractograms of Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrodes.

The peaks with  $2\theta$  values of  $2\theta = 32.56^\circ$  (101),  $36.66^\circ$  (200),  $49.64^\circ$  (211),  $60.55^\circ$  (112),  $62.21^\circ$  (301),  $77.21^\circ$  (400) and  $85.88^\circ$  (411) correspond to  $\beta$ -PbO<sub>2</sub>. The peak with a  $2\theta$  value of  $2\theta = 49.64^\circ$  is attributed to the (200) plane corresponding to doped-Cu. All peaks are in good agreement with ICSD card 89-2805.<sup>34</sup> Ethylene glycol (EG) has no effect on the crystal structure of  $\beta$ -PbO<sub>2</sub>; in fact, EG surrounds the PbO<sub>2</sub> particles and prevents the growth of PbO<sub>2</sub> crystals and in addition, EG increases nucleation.<sup>19</sup> Copper reduces the crystal size. Also, copper ions prevent the deposition of metallic lead on the cathode during electrochemical deposition.<sup>35,36</sup>

The average crystallite sizes were estimated by the Scherrer formula:<sup>37</sup>

$$D = K\lambda/\beta \cos(\theta) \quad (1)$$

$D$  is the crystalline size (nm),  $K$  is Scherrer's constant (0.91),  $\lambda$  is the wavelength of radiation (0.1541874 m),  $\beta$  is the corrected half width of the diffraction peak and  $\theta$  is the diffraction angle. The calculated average grain sizes of Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrodes were 14 nm and 16 nm, respectively. The results show that the Ti/NTA/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode has a smaller crystalline size and thus a higher specific surface area, indicating better performance in electrochemical degradation.

**SEM analysis.** SEM images of Ti/NTAs/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/ $\beta$ -PbO<sub>2</sub>-CuO<sub>x</sub> electrodes are shown in Fig. 7. Fig. 7a shows the SEM image of the nanotubes and confirms that the Ti nanotubes completely cover the electrode surface. Ti/NTAs are promising substrates for deposition due to their large specific surface area, good conductivity, high chemical stability, and cost-effectiveness.<sup>38</sup> The SEM images of Ti/NTAs/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> in Fig. 7b and c at different magnifications show the crystal structure of  $\beta$ -PbO<sub>2</sub> with a uniform, crack-free, and compact cluster distribution in both electrodes.<sup>39</sup> From the SEM images and XRD analysis, it is evident that Ti/NTAs/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> has a smaller crystalline size, which indicates a greater ability for catalytic activity and better performance in electrochemical degradation.<sup>33</sup> The average inner diameter of nanotubes (using ImageJ software) was determined to be 166 nm. Fig. 7d shows the Ti (bare) electrode. Fig. 7e and f show PbO<sub>2</sub> modified with copper and ethylene glycol (EG) at different magnifications.



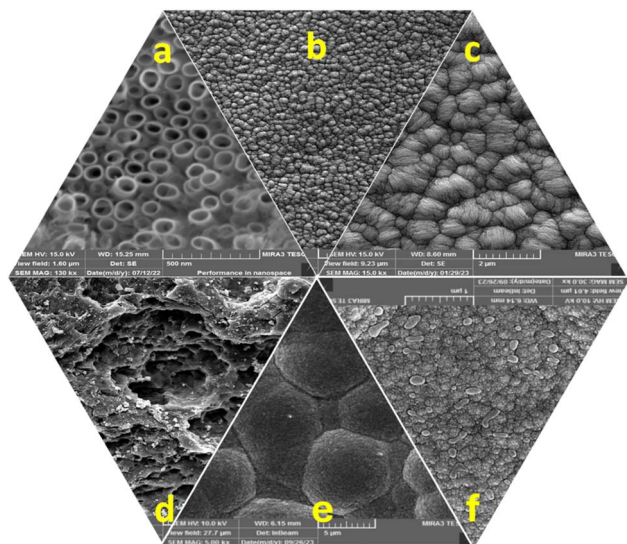


Fig. 7 SEM images of (a) TiO<sub>2</sub> nanotube arrays. (b and c) Ti/NTA/β-PbO<sub>2</sub>-CeO<sub>2</sub> in 5 μm and 2 μm magnifications, respectively. (d) Bare Ti. (e and f) Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> in 5 μm and 1 μm magnifications, respectively.

Adding copper to the composition reduces the size of the crystal structure of β-PbO<sub>2</sub>. By adding EG to the composition, the morphology undergoes substantial changes. The crystals transform into bulk structures, providing more space for the deposition of the modified layer, while the size of the lead dioxide particles decreases and nucleation increases. The addition of ethylene glycol with 2.5% v/v is the most optimal mode to modify the substrate surface.<sup>19</sup>

**EDS and mapping analysis.** The EDS pattern of Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> and Ti/NTAs/β-PbO<sub>2</sub>-CeO<sub>2</sub> electrodes are shown in Fig. 8a and c. Obviously, all elements were successfully deposited with very small amounts of Na and F elements. The addition of NaF prevents the penetration of the generated oxygen into the crystal lattice of PbO<sub>2</sub>.<sup>12</sup> In order to determine the inner surface of

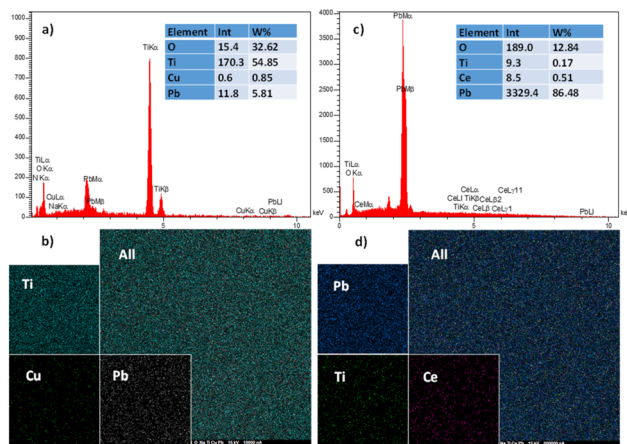


Fig. 8 (a) EDS-elemental analysis of Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub>. (c) EDS-elemental analysis of Ti/NTA/β-PbO<sub>2</sub>-CeO<sub>2</sub>. (b) Mapping analysis of Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub>. (d) Mapping analysis of Ti/NTA/β-PbO<sub>2</sub>-CeO<sub>2</sub>.

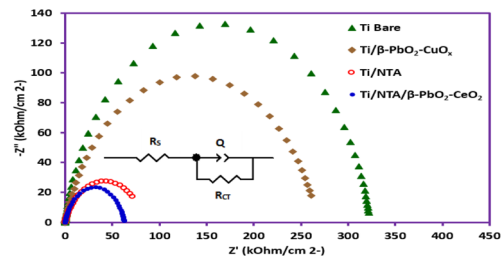


Fig. 9 Nyquist plots of different electrodes in 0.2 M KNO<sub>3</sub>. Impedance spectra were measured under the open-circuit condition with an AC potential of 50 mV from 100 kHz to 0.01 Hz at room temperature. Potential applied: for Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub>: 1.294 V. for Ti/NTA/β-PbO<sub>2</sub>-CeO<sub>2</sub>: 1.115 V. for Ti/NTA: 0.478 V and for bare Ti: 0.446 V. Electrochemical cell: undivided cell. Counter electrode: platinum wire. Reference electrode: Ag/AgCl electrode.

nanotubes and increase the accuracy of EDS analysis, the deposition was accompanied by gold doping. The EDS pattern of the Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> electrode shown in Fig. 8a confirms the presence of Pb, Cu, O and Ti elements on the electrode substrate. The absence of the carbon element indicates that EG is not deposited on the electrode surface. Mapping analysis of both electrodes (Fig. 8 parts b and d) shows complete coverage of the electrode surface by the constituent particles (as expected). It also effectively shows the dispersion and uniformity of doped elements without the accumulation of any elements in Ti/NTAs/β-PbO<sub>2</sub>-CeO<sub>2</sub> and Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> electrodes.

**Electrochemical impedance spectroscopy.** Electrochemical impedance spectroscopy was used to study the performance of electrodes in solution. The Nyquist plots of electrodes are shown in Fig. 9. The diameter of the capacitive loops in the Nyquist diagrams shows the charge-transfer resistance. In general, a smaller semicircle with a smaller diameter indicates a lower charge-transfer resistance.<sup>40</sup> As can be seen, the charge transfer resistance in the Ti/NTA electrode is much lower than that of Ti bare and Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub> electrodes. A possible explanation for this behavior can be due to the increase in the active surface in the Ti/NTA and Ti/NTA/β-PbO<sub>2</sub>-CeO<sub>2</sub> electrodes caused by the nanotubes. The equivalent circuit of the electrochemical performance of the prepared electrodes is shown in Fig. 9. In this circuit,  $R_s$  represents the solution resistance,  $Q$  represents the double layer capacitance and  $R_{CT}$  represents the charge transfer resistance. The charge transfer resistance for Ti Bare (Ti sheet), Ti/β-PbO<sub>2</sub>-CuO<sub>x</sub>, Ti/NTA and Ti/NTA/β-PbO<sub>2</sub>-CeO<sub>2</sub> are  $3.23 \times 10^2$  kΩ,  $2.68 \times 10^2$  kΩ, 84.6 kΩ and 62.7 kΩ, respectively.

### Electrochemical studies of PQ<sup>2+</sup>

Cyclic voltammogram of 1 mM solution of *N,N'*-dimethyl-4,4'-bipyridiniumdichloride (PQ<sup>2+</sup>) in water (phosphate buffer, pH = 7.0,  $c = 0.2$  M)/acetonitrile (30/70 v/v) is shown in Fig. 10, part I. As seen in the cathodic scan, two well-defined peaks, C<sub>1</sub> and C<sub>2</sub>, can be observed at potentials of -0.68 and -1.06 V, which are attributed to the stepwise reduction of PQ<sup>2+</sup> to PQ<sup>•+</sup> and PQ (Scheme 1). In the reverse scan, two anodic peaks A<sub>1</sub> and A<sub>2</sub> are clearly observed at potentials of -0.61 and -0.97 V vs. Ag/AgCl,



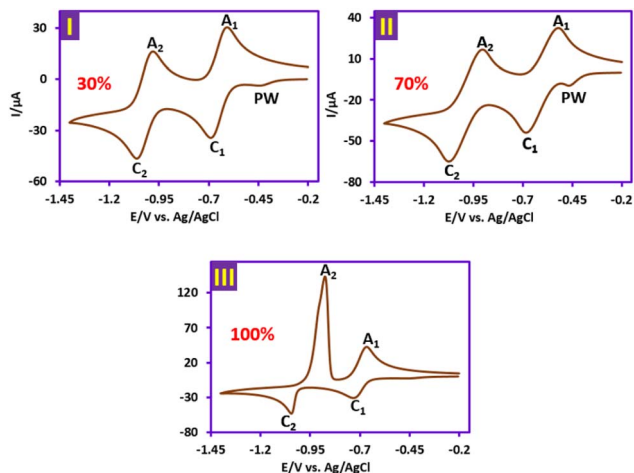
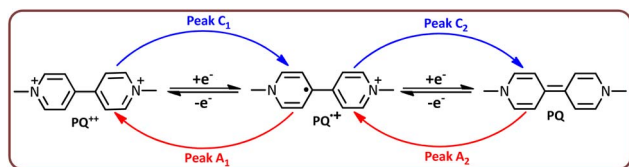


Fig. 10 Mechanism of cyclic voltammograms of 1 mM solution of  $\text{PQ}^{2+}$  in: (I) phosphate buffer solution (pH = 7.0,  $c = 0.2$  M)/acetonitrile mixture (70/30 v/v). (II) Phosphate buffer solution (pH = 7.0,  $c = 0.2$  M)/acetonitrile mixture (30/70 v/v). (III) Phosphate buffer solution (pH = 7.0,  $c = 0.2$  M): at a scan rate of  $100 \text{ mV s}^{-1}$  and room temperature. Electrochemical cell: undivided cell. Working electrode: glassy carbon electrode. Counter electrode: platinum wire. Potential scan range:  $-0.20$  to  $-1.40$  V vs. Ag/AgCl.



Scheme 1 Stepwise reduction of  $\text{PQ}^{2+}$  to  $\text{PQ}^{+}$  and  $\text{PQ}$ .

which are the counterparts of the cathodic peaks  $\text{C}_1$  and  $\text{C}_2$ , respectively.

As the water ratio increases to 70%, there is no significant change in the voltammogram shape, except for a slight increase in the pre-peak (PW) current at a potential of  $-0.46$  V (Fig. 11, part II). But in the solution without acetonitrile (100% water), the shape of the voltammogram changes significantly (Fig. 11, part III). In this condition, peak  $\text{A}_2$  shows a strong adsorption behavior and confirms that fully reduced paraquat ( $\text{PQ}$ ) (uncharged species) is strongly adsorbed in the aqueous solvent.<sup>41</sup> The effect of solution pH on the adsorption process of reduced paraquat ( $\text{PQ}$ ) was also studied, and it was found that such behavior is not observed in acidic environments. Protonation of nitrogen atoms in the structure of  $\text{PQ}$  in acidic solutions may be the main reason for the lack of strong adsorption of this molecule. Finally, our data show that the reduced form of this herbicide definitely has strong adsorption properties in neutral and alkaline solutions that should be considered in environmental assessments.

### Galvanostatic electrolysis of $\text{PQ}^{2+}$

These experiments were performed with initial concentrations of 50 and 70 ppm of  $\text{PQ}^{2+}$  at current densities of 4.7 and  $7.8 \text{ mA cm}^{-2}$

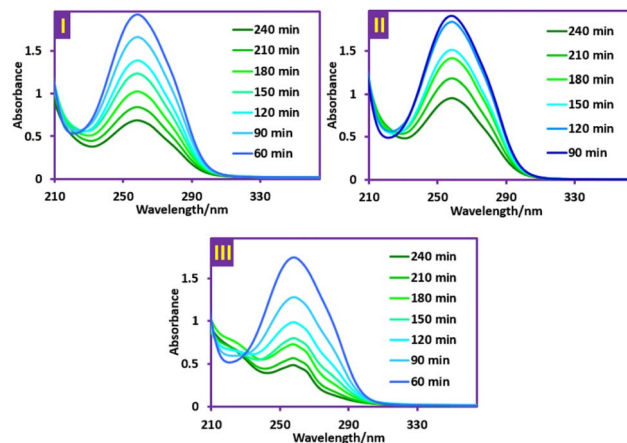


Fig. 11 UV-vis spectra of  $\text{PQ}^{2+}$  during the degradation process. (I) Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  electrode in a conventional cell. (II) Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$  electrode in a conventional cell. (III) Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  electrode in a newly designed cell. Electrolysis condition: initial concentration of  $\text{PQ}^{2+}$  is 50 ppm, current density of  $4.7 \text{ mA cm}^{-2}$ . Solvent: aqueous phosphate buffer solution (pH = 7.0,  $c = 0.2$  M).

and pHs of 2, 7 and 9. Monitoring of  $\text{PQ}^{2+}$  degradation was carried out using UV-vis spectrophotometry at a wavelength of 257 nm. The first experiments were performed to compare the efficiency of Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  and Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$  electrodes in  $\text{PQ}^{2+}$  degradation in a conventional cell. The volume of this cell was 80 ml and equipped with 3 anodes with dimensions of  $2.5 \times 4.4$  cm and an effective surface of  $64 \text{ cm}^2$  and 2 stainless steel cathodes with dimensions of  $2.5 \times 4.5$  cm. The stirring of the solution was performed by a magnetic stirrer at a constant speed. Fig. 11, parts I and II, shows the UV-vis spectra of  $\text{PQ}^{2+}$  during its degradation using Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  and Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$  electrodes, respectively. The comparison of the decrease in absorbance at the wavelength of 257 nm in Fig. 11(I) and (II) shows that the efficiency of the Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  electrode in the degradation of  $\text{PQ}^{2+}$  is higher than that of the Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$  electrode; therefore, this electrode was used in the subsequent experiments in the newly designed cell. The volume of the new cell is 170 ml and equipped with four Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  anodes with dimensions of  $3.5 \times 5.0$  cm and an effective area of  $140 \text{ cm}^2$  with a distance of 1 cm from each other and a cathode made of a stainless steel mesh that the anodes are surrounded by it (Fig. 2).

Fig. 11, part III, shows the UV-vis spectrum of the degradation of  $\text{PQ}^{2+}$  using Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  in the newly designed cell. As can be seen, the decrease in absorbance at a wavelength of 257 nm is greater than in the previous cases.

Since there is a possibility of copper, lead, and titanium ions in the solution at the end of electrolysis, the presence of these ions in the electrolyzed solution was determined using ICP-OES. The results showed that the concentration of all four ions in the solution is lower than the limit of detection of the ICP-OES instrument.

### Influence of current density

The electrochemical degradation of  $\text{PQ}^{2+}$  was investigated using two Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  and Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$  electrodes at two



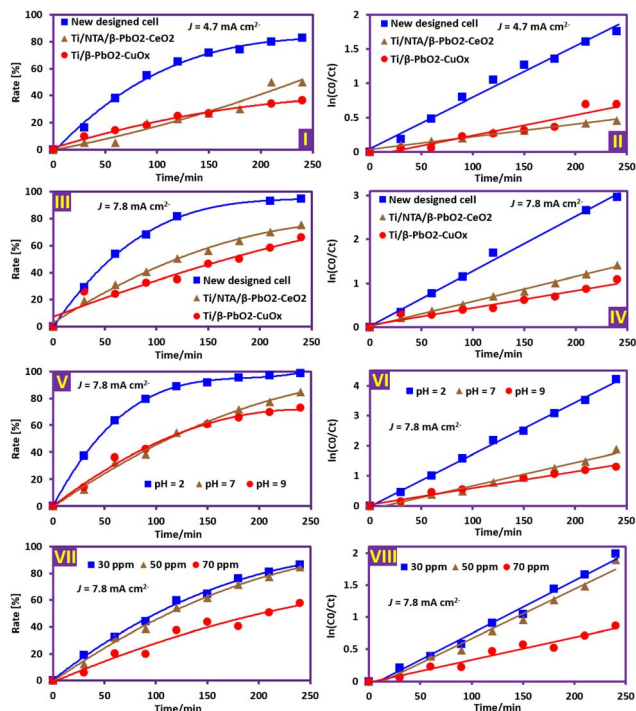


Fig. 12 Parameters affecting the electrochemical degradation of  $PQ^{2+}$ . Parts I–IV: The effect of current density and cell type. Initial  $PQ^{2+}$  concentration of 50 ppm in both conventional and newly designed cells. Parts V and VI: The effect of solution pH. Initial  $PQ^{2+}$  concentration of 50 ppm; applied current density  $7.8 \text{ mA cm}^{-2}$  in the newly designed cell. Parts VII and VIII: The effect of initial  $PQ^{2+}$  concentration. Solution pH 7; applied current density  $7.8 \text{ mA cm}^{-2}$  in newly designed cell.

current densities of  $4.7$  and  $7.8 \text{ mA cm}^{-2}$  and at an initial concentration of  $50 \text{ ppm}$  in conventional and newly designed cells (Fig. 12 parts I–IV). The results show that in both electrodes, the degradation efficiency and degradation rate increase with increasing current density. As the current density increases, the generation of hydroxyl radicals increases, and as a result, the pollution degradation increases. The formation of more intermediates with increasing  $PQ^{2+}$  concentration and their competition with  $PQ^{2+}$  causes the degradation efficiency to decrease with increasing concentration.<sup>18</sup>

Fig. 12 parts I–IV also compares the efficiency of  $Ti/NTA/\beta-PbO_2-CeO_2$  and  $Ti/\beta-PbO_2-CuO_x$  electrodes in a conventional cell for  $PQ^{2+}$  degradation and shows that the  $Ti/NTA/\beta-PbO_2-CeO_2$  electrode exhibits higher efficiency, especially at high current densities. Fig. 12, parts I–IV, also compares the efficiency of the new cell with a conventional cell in  $PQ^{2+}$  degradation and shows that the efficiency of the new cell is significantly higher than that of the conventional cell (Fig. 13). It is worth noting that the  $Ti/NTA/\beta-PbO_2-CeO_2$  electrode was used in both cells.

#### Influence of solution pH and $PQ^{2+}$ initial concentration

The effect of pH value on the electrochemical degradation of  $PQ^{2+}$  was investigated at pH values of 2, 7 and 9 using the  $Ti/NTA/\beta-PbO_2-CeO_2$  electrode at a current density of  $7.8 \text{ mA cm}^{-2}$

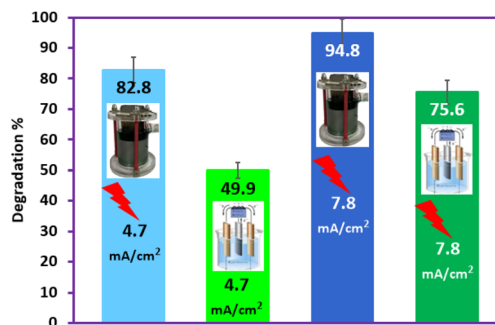


Fig. 13 Comparison of the performance of the conventional cell (con.) with the newly designed cell (new) at two current densities of  $4.7$  and  $7.8 \text{ mA cm}^{-2}$  in the degradation of  $50 \text{ ppm}$  of  $PQ^{2+}$  at pH 7.

and an initial concentration of  $50 \text{ ppm}$  (Fig. 12 parts V and VI). The results show that the degradation efficiency is higher in an acidic environment and decreases with increasing pH. Increasing the competition between the oxygen evolution reaction and hydroxyl radical generation with increasing solution pH is the main factor in decreasing the degradation efficiency in neutral and alkaline solutions. On the other hand, hydroxyl radicals exhibit a weak acid behavior ( $pK_a$  11.9 (ref. 42)) and therefore, in alkaline environments, they can react with hydroxyl ions (eqn (2)) and become less powerful oxidizing species.<sup>39,43</sup> Although the degradation efficiency of  $PQ^{2+}$  after 240 min at pH values of 2, 7, and 9 is 98.5, 84.9, and 72.9%, respectively, pH 7 was chosen as the optimum pH due to its high compatibility with the environment.

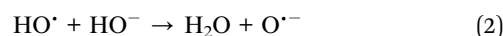


Fig. 12, parts VII and VIII, shows the effect of  $PQ^{2+}$  initial concentration on  $PQ^{2+}$  degradation by the  $Ti/NTA/\beta-PbO_2-CeO_2$  electrode in a new cell at a current density of  $7.8 \text{ mA cm}^{-2}$  at pH 7. As can be seen, the degradation efficiency and degradation rate decrease with increasing initial concentration of  $PQ^{2+}$ .

#### Influence of electrode type

In this section, the efficiency of fabricated electrodes in  $PQ^{2+}$  degradation at both current densities  $4.7$  and  $7.8 \text{ mA cm}^{-2}$  is compared (Fig. 12). The results show that the percentage of  $PQ^{2+}$  degradation after 240 minutes of electrolysis with the  $Ti/\beta-PbO_2-CuO_x$  electrode at the current density of  $4.7$  and  $7.8 \text{ mA cm}^{-2}$  is 36 and 66%, respectively; however, in such conditions, the  $Ti/NTA/\beta-PbO_2-CeO_2$  electrode has a greater efficiency, such that the percentage of  $PQ^{2+}$  degradation in the current density of  $4.7$  and  $7.8 \text{ mA cm}^{-2}$  becomes 49 and 75%, respectively. The better performance of the  $Ti/NTA/\beta-PbO_2-CeO_2$  electrode in  $PQ^{2+}$  degradation can be attributed to the larger surface area and more active sites for hydroxyl radical generation than the  $Ti/\beta-PbO_2-CuO_x$  electrode. In the newly designed cell, due to the large surface area of the electrodes and the surrounding anodes with a cylindrical cathode, the mass transfer is higher and the ohmic drop ( $IR$ ) is lower. These features enable better electrochemical degradation of  $PQ^{2+}$  compared to conventional cells.



Table 1 Observed degradation rate constant ( $k_{\text{obs}}$ ) of  $\text{PQ}^{2+}$  under different conditions

Electrode	Current density ( $\text{mA cm}^{-2}$ )	Initial concentration (ppm)	pH value	$R^2$	$K_{\text{obs}}$ ( $\text{min}^{-1}$ )
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	4.7	50	7	0.9136	0.0030
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	50	7	0.9968	0.0057
Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$	4.7	50	7	0.9821	0.0018
Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$	7.8	50	7	0.9531	0.0040
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	50	2	0.9974	0.0172
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	50	7	0.9836	0.0077
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	50	9	0.9884	0.0055
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	30	7	0.9898	0.0082
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	70	7	0.9616	0.0035
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$ in new cell	4.7	50	7	0.9858	0.0075
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$ in new cell	7.8	50	7	0.9953	0.0125

Analysis of available data shows a linear relationship between time and  $\ln(C_0/C_t)$ , confirming that the electrochemical degradation of  $\text{PQ}^{2+}$  with the electrodes fabricated in this research follows pseudo-first-order kinetics.<sup>48</sup> To obtain the necessary data, the first-order pseudo-model with the following eqn (3) has been used, where  $t$  is the time and  $C_0$  and  $C_t$  are the concentrations at the initial or a given time (ppm), respectively.  $k$  is the kinetic constant of the pseudo-first-order reaction, which is obtained from the slope of the plot of  $\ln(C_0/C_t)$  versus time ( $t$ ). The data obtained under different conditions are summarized in Table 1.

$$\ln(C_0/C_t) = -kt \quad (3)$$

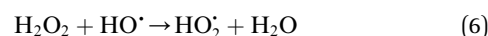
### Energy consumption

In this section, the effects of electrode type, applied current density, and cell type on electrical energy consumption (EEC) in the electrochemical degradation of  $\text{PQ}^{2+}$  is investigated. Here, EEC is described by the EE/O (electrical efficiency per log order). EE/O is defined as the electricity consumed by reducing the concentration of the pollutant by an order of magnitude. Eqn (4) is used to calculate electrical efficiency per log order (EE/O):<sup>46</sup>

$$\text{EE/O (kWh m}^{-3}\text{)} = 0.001EI t/V_s \log(C_0/C_t) \quad (4)$$

Here,  $E$  is the cell voltage (V),  $I$  is the applied current (A),  $t$  is the electrolysis time (hour),  $C_0$  is the initial concentration of  $\text{PQ}^{2+}$ ,  $C_F$  is the final concentration of  $\text{PQ}^{2+}$  and  $V_s$  is the cell volume

( $\text{m}^3$ ). The data of EE/O are listed in Table 2. These results indicate that the electrode type does not have a significant effect on EE/O; however, in both electrodes, EE/O increases with increasing current density. The occurrence of oxygen evolution reaction at a higher current density seems to be one of the important factors in increasing EE/O. Furthermore, at higher current densities, the process of converting hydroxyl radicals into hydrogen peroxide and hydroperoxyl radical increases (eqn (5) and (6)).<sup>44</sup> It should be noted that since the oxidizing power of  $\text{H}_2\text{O}_2$  and  $\text{HO}_2^\cdot$  is much lower than that of  $\text{HO}^\cdot$ ,<sup>43</sup> these compounds reduce the mineralization process and, in other words, increase EE/O. Unlike the electrode type, the cell type has a significant impact on EE/O, thus, using the cell designed in this study reduces EE/O by approximately 2.5 times.



The operating cost (OPC) of an electrochemical treatment process depends mainly on the cost of energy consumed under optimal conditions and the cost of electrodes and chemicals. The equation for the calculation of operating cost is shown below:<sup>45</sup>

$$\text{OPC} = \alpha \times \text{ENC} + \beta \times \text{CHC} + \gamma \times \text{ELC} \quad (7)$$

where ENC, CHC and, ELC are energy consumption per cubic meter of wastewater ( $\text{kWh m}^{-3}$ ), cost of chemicals ( $\text{kg m}^{-3}$ ) and consumed electrode for treatment of a cubic meter wastewater

Table 2 EE/O and OPC values for the degradation of  $\text{PQ}^{2+}$  under different conditions<sup>a</sup>

Electrode	Current density ( $\text{mA cm}^{-2}$ )	Cell volume ( $\text{m}^3$ )	Cell voltage (V)	$\log(C_0/C_F)$	EE/O ( $\text{kWh m}^{-3}$ )	OPC <sup>b</sup> (US\$ per $\text{m}^3$ )
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	7.8	0.08	10.4	0.61	0.42	3.48
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$	4.7	0.08	9.3	0.30	0.46	3.49
Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$	7.8	0.08	7.5	0.47	0.40	3.48
Ti/ $\beta$ - $\text{PbO}_2$ - $\text{CuO}_x$	4.7	0.08	6.4	0.20	0.48	3.49
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$ in new cell	7.8	0.17	9.0	1.28	0.18	3.46
Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$ in new cell	4.7	0.17	8.2	0.76	0.16	3.46

<sup>a</sup>  $\text{PQ}^{2+}$  initial concentration: 50 ppm, initial pH = 7.0 and electrolysis time of 240 min. <sup>b</sup> The cost of electrodes is not included.



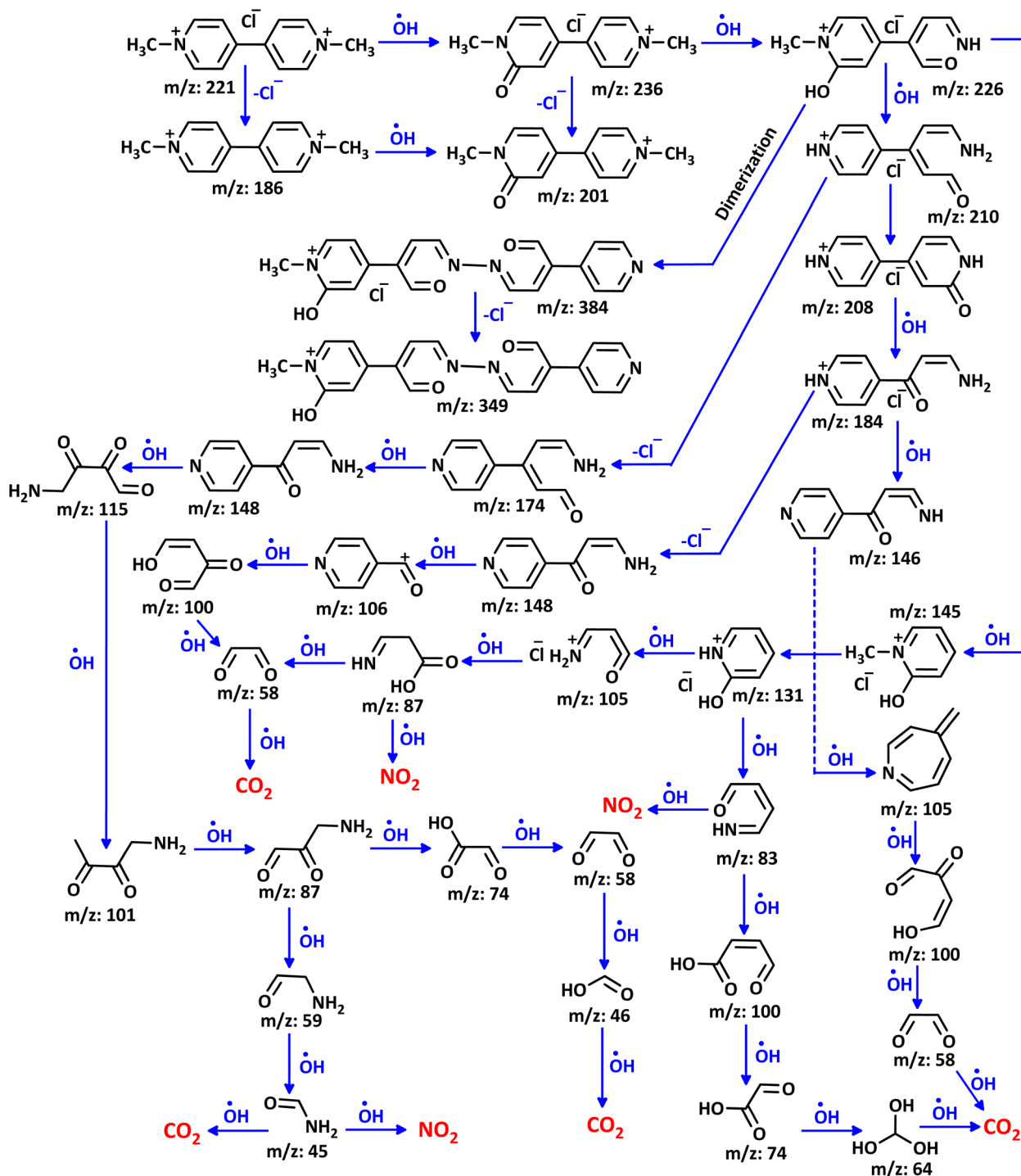
( $\text{kg m}^{-3}$ ), respectively.  $\alpha$  is the price of electricity,  $\beta$  is the price of chemicals, and  $\gamma$  is the price of electrodes.

Electricity price ( $\alpha$ ): 0.1 US\$ per kWh and therefore: ENC for Ti/NTA/ $\beta$ - $\text{PbO}_2$ - $\text{CeO}_2$  in the new cell is:  $0.16 \times 0.1 = 0.016$  US\$ per  $\text{m}^3$ . The cost of phosphate buffer ( $\beta$ ) is 3.44 US\$ per  $\text{m}^3$ . Since in electrocatalytic degradation processes, electrodes can be used for a long time and, on the other hand, only a thin layer of

catalysts and chemicals is deposited on them (the prepared chemicals and solutions can be used several times), the cost of the electrodes is negligible and has not been included in these calculations.<sup>46</sup>

Therefore:

$$\text{Operating cost (US\$ per m}^3\text{)} = 0.016 + 3.44 = 3.46 \text{ US\$ per m}^3$$



Scheme 2 Proposed mechanism for the electrochemical degradation of PQ<sup>2+</sup>. PQ<sup>2+</sup> initial concentration: 50 ppm. Initial pH: 7.0. Applied current density: 7.8 mA cm<sup>-2</sup>, in new cell at room temperature.



Other data are shown in Table 2.

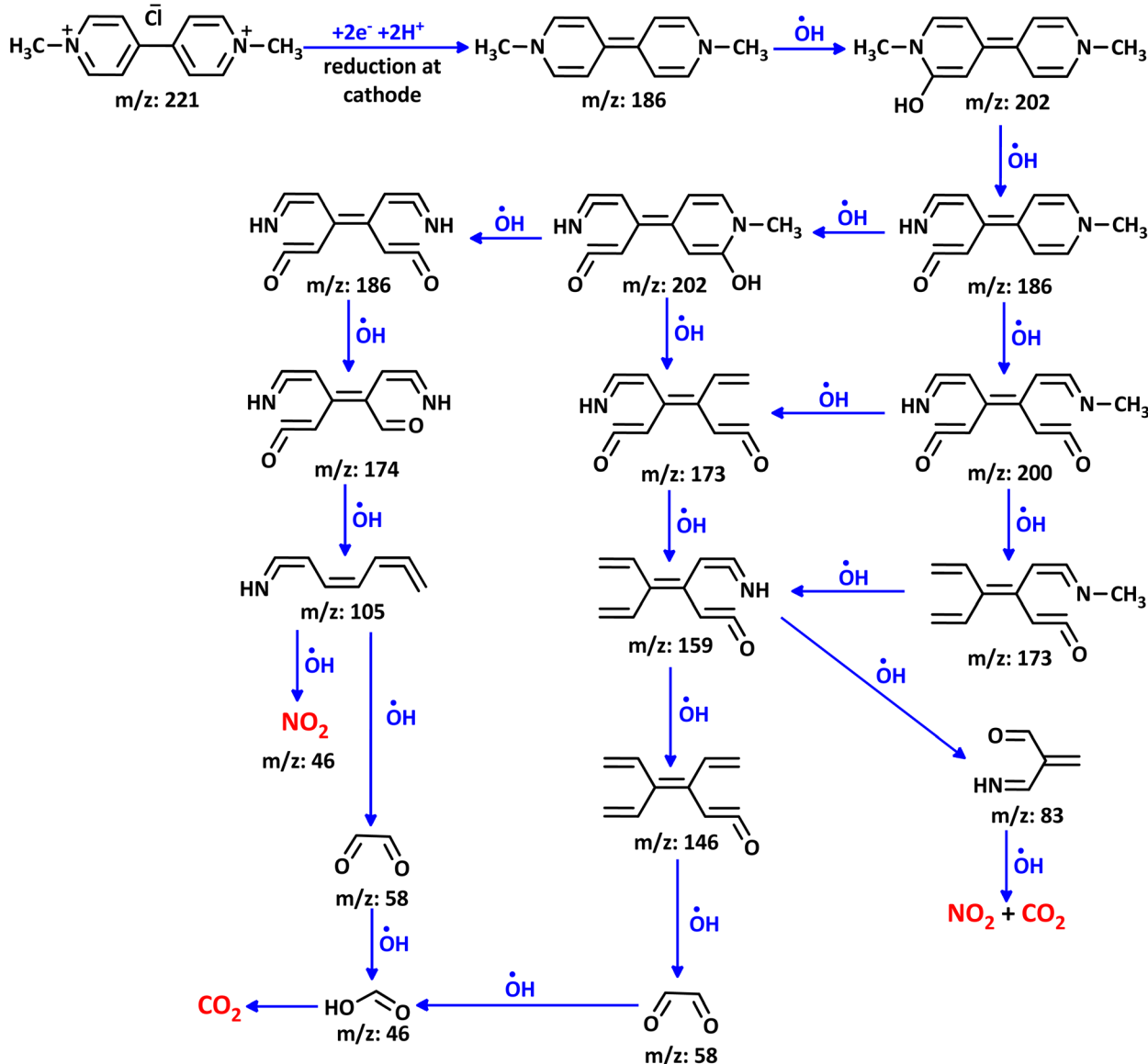
### Electrochemical degradation pathway of $PQ^{2+}$

The proposed mechanism for the electrochemical degradation of  $PQ^{2+}$  by the Ti/NTA/ $\beta$ - $PbO_2$ - $CeO_2$  electrode is shown in Scheme 2. All fragments reported in this Figure are based on data obtained from LC-MS spectra of  $PQ^{2+}$  solution during electrolysis (SI). It seems that the first step in the electrochemical degradation of  $PQ^{2+}$  is the oxidation/hydroxylation/ring opening and demethylation of  $PQ^{2+}$  by  $OH^\cdot$ , resulting in the formation of  $C_{12}H_{13}ClN_2O$  ( $m/z = 236$ ) and  $C_{10}H_{11}ClN_2O_2$  ( $m/z = 226$ ), respectively.<sup>14</sup>

Dimerization of the fragment  $C_{10}H_{11}ClN_2O_2$  ( $m/z = 226$ ), in the ionization chamber of the mass spectrometer or during electrolysis leads to  $C_{19}H_{17}ClN_4O_3$  ( $m/z = 384$ ) in the early

stages. In parallel, demethylation/oxidation and degradation of this compound produced fragments  $C_8H_9ClN_2O$  ( $m/z = 184$ ) and  $C_8H_6N_2O$  ( $m/z = 146$ ). Oxidation/degradation and rearrangement of  $C_8H_6N_2O$  lead to fragments  $C_7H_7N$  ( $m/z = 105$ ),  $C_4H_4O_3$  ( $m/z = 100$ ), and  $C_2H_2O_2$  ( $m/z = 58$ ), respectively. Further oxidation of these fragments eventually leads to  $CO_2$  and  $NO_2$ . As shown in Scheme 2, the same steps and processes ultimately lead to the formation of  $CO_2$  and  $NO_2$  in other pathways.

In addition to the mechanism proposed in Scheme 2, voltammetric results (Fig. 10) indicate that  $PQ^{2+}$  can be reduced to  $PQ$  at the cathode surface. The reduced molecule ( $PQ$ ), due to its conjugated double bonds, can react with hydroxyl radicals<sup>47</sup> to form a molecule with a mass of 202 (Scheme 3). Subsequent oxidation and addition by hydroxyl radicals transforms this molecule into the intermediates shown in Scheme 3, which are



Scheme 3 Proposed mechanism for the degradation of  $PQ^{2+}$  based on reduction.



eventually mineralized. It should be noted that all fragments reported in Scheme 3 are based on data obtained from the LC-MS spectra of the  $PQ^{2+}$  solution during electrolysis (SI).

## Conclusion

In this research, two types of electrodes, Ti/NTA/ $\beta$ - $PbO_2$ - $CeO_2$  and Ti/ $\beta$ - $PbO_2$ - $CuO_x$ , were fabricated and used for the successful degradation of  $PQ^{2+}$ . The results showed that the Ti/NTA/ $\beta$ - $PbO_2$ - $CeO_2$  electrode increases the production of hydroxyl radicals and is more efficient in  $PQ^{2+}$  degradation than the Ti/ $\beta$ - $PbO_2$ - $CuO_x$  electrode. The most important factor seems to be the doping of  $\beta$ - $PbO_2$  with  $CeO_2$ .  $CeO_2$  doping makes the  $\beta$ - $PbO_2$  grains finer, which leads to improved grain arrangement and an increase in the number of active sites for the hydroxyl radical production. Using this electrode, we were able to remove up to 75% of  $PQ^{2+}$  at pH 7, current density of  $7.8 \text{ mA cm}^{-2}$  and an initial concentration of 50 ppm. The important innovation of this study is the design of a new electrochemical cell, the use of which, due to its special design, increases the degradation efficiency by 95% and reduces energy consumption by 40%. Another interesting point of this research is the provision of a complete and detailed mechanism for the degradation of  $PQ^{2+}$  using data obtained from LC-MS experiments and the identification of different mineralization pathways for this compound. In this study, the electrochemical behavior of  $PQ^{2+}$  was also investigated using cyclic voltammetry in different water/acetonitrile mixtures. Our data show that the reduced form of  $PQ^{2+}$  (PQ) has strong adsorption properties in neutral and alkaline solutions, which should be considered in environmental assessments. These results will lead to deeper insights and understanding of the redox properties and adsorption activity of  $PQ^{2+}$ . Finally, given the ability of the current strategy to the degradation of the robust chemical structure of  $PQ^{2+}$ , it seems that this method is capable of degrading a wide range of organic pollutants. Also, the proposed method can be easily scaled up by increasing the dimensions of the designed cell.

## Ethical statement

This article does not contain any studies with animals performed by any of the authors.

## Author contributions

Davood Nematollahi: supervision, project administration, resources, writing-review and editing. Mahsa Roshani: investigation, formal analysis, and writing-original draft. Mohammad Mehdi Hashemi-Mashouf: investigation. Niloofar Mohamadighader: investigation.

## Conflicts of interest

The authors declare no conflict of interest.

## Data availability

All data generated or analyzed during this study are included in this published article and its supplementary information (SI) files. Supplementary information is available. See DOI: <https://doi.org/10.1039/d5ra06796k>.

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