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# Non-metal single atoms anchored on defective MoS<sub>2</sub>: a novel electrocatalyst for NO reduction to NH<sub>3</sub>

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The electrocatalytic nitric oxide reduction reaction (eNORR) is a highly significant because it provides a sustainable and cost-effective way to combine the elimination of nitric oxide (NO) with synthesis of ammonia (NH<sub>3</sub>). This study comprehensively investigates the performance of single non-metal atom catalysts (NM@MoS<sub>2</sub>), which are composed of single non-metal atoms that are embedded in vacancy defects in MoS<sub>2</sub>. Our results demonstrate that eight NM@MoS<sub>2</sub> catalysts (NM = B, C, N, O, P, Si, Se, and Te) exhibit remarkable thermodynamic stability. The Si, C, N, B and P@MoS<sub>2</sub> catalysts in particular effectively adsorb and activate NO molecules, displaying high catalytic activity during the subsequent protonation process. Their  $U_L$  values are 0, 0, -0.36, -0.62, and -0.70 V, respectively. Furthermore, a detailed selectivity analysis revealed that the N, P, C, and Si@MoS<sub>2</sub> catalysts exhibit high NH<sub>3</sub> selectivity. This theoretical study has effectively identified and evaluated NM@MoS<sub>2</sub> catalysts based on stability, selectivity and high catalytic activity with a focus on NO removal and NH<sub>3</sub> synthesis.

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## 1 Introduction

Fossil fuel combustion in power plants, cars and industrial facilities releases large amounts of nitrogen oxides (NO<sub>x</sub>), which endanger the environment and human health.<sup>1,2</sup> As public awareness of the pollution and health risks associated with NO<sub>x</sub> emissions increases, more stringent regulations are being enacted across various industries to limit NO<sub>x</sub> emissions.<sup>3</sup> Consequently, eliminating NO<sub>x</sub> from flue gases has become a key area of research within catalytic chemistry.

Currently, selective catalytic reduction (SCR) technology is the primary method for reducing NO<sub>x</sub> discharges.<sup>4–9</sup> However, this approach is hindered by its high energy consumption, which makes it unsuitable for widespread application. For example, the SCR process usually uses ammonia as a reducing agent and operates at temperatures between 200 and 400 °C. Meanwhile, ammonia (NH<sub>3</sub>), a vital chemical for fertilizers, pharmaceuticals, and dyes, is predominantly synthesised *via* the Haber–Bosch method, which demands intensely high temperatures (300–500 °C) and pressures (200–300 atm).<sup>10</sup>

These harsh conditions contribute to high energy costs and limit the sustainability and scalability of NH<sub>3</sub> production.

Nitric oxide (NO) typically accounts for around 95% of total nitrogen oxides (NO<sub>x</sub>) in flue gas emissions.<sup>11</sup> Recently, the electrocatalytic nitric oxide reduction reaction (eNORR) has emerged as an innovative, environmentally friendly solution for reducing NO emissions from sources such as thermal power stations, industrial facilities and vehicles. This process is advantageous because it operates at ambient temperatures, eliminating the need for high temperatures or pressures.

In addition, the eNORR process can utilize renewable energy sources like solar or wind power, boosting its environmental credentials. Another benefit of the eNORR process is its ability to produce valuable NH<sub>3</sub>.<sup>12</sup> Therefore, eNORR is a win-win strategy for synthesising valuable NH<sub>3</sub> and reducing environmental pollution. However, the success of this process depends on developing suitable catalysts that can enhance both product selectivity and catalytic activity. Currently, most eNORR catalysts are metallic in nature.<sup>13–17</sup> While these metal catalysts demonstrate excellent eNORR activity, their practical application is limited by factors such as poor durability, high cost, and low atom utilisation efficiency.<sup>18,19</sup> Given these limitations, the search for low-cost, highly selective eNORR catalysts has become urgent and necessary.

Single-atom catalysts (SACs) have drawn remarkable attention because of their exceptional catalytic performance. Single-atoms are atomically dispersed on the surface of the substrate and existing in an unsaturated state that gives them with high activity. This unique structure provides an abundance of active

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sites for reactant molecules, thereby facilitating efficient catalysis.<sup>20,21</sup> To date, numerous theoretical studies and experimental results have shown that the unsaturated active sites on the surface of catalyst materials, including SACs and surface defects, can effectively promote the eNORR.<sup>22–30</sup> However, a notable challenge arises with (TM)-based SACs, where the high mobility of surface metal atoms often leads to easy agglomeration of single metal atoms on their surfaces.<sup>31–33</sup> In contrast, surface defects are more effective and stable catalytic sites.<sup>28–30</sup>

Molybdenum disulfide (MoS<sub>2</sub>) is a typical 2D material. During the synthesis of MoS<sub>2</sub> monolayer, sulfur (S) vacancies are inevitably generated on its surface, thus exposing the underlying unsaturated molybdenum (Mo) atoms.<sup>34</sup> These S-vacancy sites on MoS<sub>2</sub> materials can provide stable catalytic active sites for eNORR.<sup>35</sup> However, in this study, we found that the intrinsic properties of monolayer MoS<sub>2</sub> with S vacancies posed certain limitations. Specifically, the three unsaturated Mo atoms exhibited excessively strong binding affinity for reactant molecules, which hindered the smooth progression of some key elementary reaction steps. For instance, the energy barrier for the NH → NH<sub>2</sub> step was found to be nearly 1.5 eV, indicating a significant kinetic barrier. This observation suggests that while MoS<sub>2</sub> with S vacancies provides a promising foundation, further modification is necessary to optimize its catalytic performance for eNORR.

In the field of gas sensing, introducing non-metal atoms into S vacancy sites of MoS<sub>2</sub> can regulate the adsorption energy of adsorbed molecules, thereby effectively improving its performance.<sup>36,37</sup> Similarly, in the context of electrocatalysis, incorporating non-metal atoms into two-dimensional (2D) materials has been shown to enhance their eNORR performance. For instance, Ali *et al.*<sup>38</sup> examined the eNORR performance of B<sub>4</sub>@g-C<sub>3</sub>N<sub>4</sub> catalysts and discovered that B<sub>4</sub> clusters anchored on g-C<sub>3</sub>N<sub>4</sub> materials could efficiently enhance eNORR with a limiting potential of −0.37 V. Zhu *et al.*<sup>39</sup> reported that a single silicon atom supported on carbon nanotubes exhibited superior catalytic activity in the eNORR, with a limiting potential of −0.25 V. Ma *et al.*<sup>40</sup> investigated the eNORR performance of phosphorus (P)-doped C<sub>2</sub>N materials and revealed their superior catalytic activity. Meanwhile, Saeidi *et al.*<sup>41</sup> demonstrated the remarkably high catalytic activity of boron-doped C<sub>3</sub>N nanosheets for eNORR. Taken together, these studies highlight the potential of single non-metal atoms as effective eNORR catalysts.

In view of this, the MoS<sub>2</sub> monolayer with an S vacancy is an ideal support, with its S vacancy sites offering robust binding sites for anchoring non-metal heteroatoms.<sup>42</sup> Leveraging this characteristic, we have constructed single non-metal atom catalysts by embedding single non-metal atoms (denoted NM) into MoS<sub>2</sub> vacancies (referred to as NM@MoS<sub>2</sub>). It is anticipated that these NM@MoS<sub>2</sub> catalysts will deliver exceptional catalytic performance in the eNORR.

It is worth noting that MoS<sub>2</sub> materials doped with non-metal atoms are known for their simple and straightforward preparation process. For instance, Ma *et al.*<sup>43</sup> demonstrated *via* theoretical calculations that CO, NO, and NO<sub>2</sub> molecules can fill S vacancies in MoS<sub>2</sub> at room temperature, thereby achieving

C, N, and O doping, respectively. This finding suggests that non-metal doping can be achieved under mild conditions. Furthermore, Song *et al.*<sup>44</sup> successfully synthesized phosphorus (P)-doped MoS<sub>2</sub> materials *via* a simple pyrolysis process, achieving remarkable oxygen reduction reaction (ORR) performance. Xie *et al.*<sup>45</sup> produced MoS<sub>2</sub> materials with different oxygen doping concentrations by controlling the hydrothermal reaction temperature; these nanosheets exhibited excellent catalytic performance in the hydrogen evolution reaction (HER). Zhang *et al.*<sup>46</sup> prepared selenium (Se)-doped MoS<sub>2</sub> materials using a hydrothermal synthesis method. They then combined these materials with reduced graphene oxide, resulting in composites that exhibited excellent catalytic activity in lithium–sulfur (Li–S) batteries. Song *et al.*<sup>47</sup> synthesized O-doped MoS<sub>2</sub> catalysts *via* pyrolysis and combined them with g-C<sub>3</sub>N<sub>4</sub>, yielding materials with exceptional ORR performance. Similarly, several pieces of experimental research highlight that boron (B)-doped MoS<sub>2</sub> catalysts synthesized by the hydrothermal route exhibit excellent catalytic performance in the electrocatalytic reduction of both nitrogen and nitrate.<sup>48–50</sup> As the positions of S atoms were replaced by non-metal (NM) atoms during the doping process, the NM-doped MoS<sub>2</sub> structure is similar to that of NM@MoS<sub>2</sub> catalysts. Therefore, these research findings offer compelling theoretical support for the experimental synthesis and stability of NM@MoS<sub>2</sub> catalysts.

In this study, we employed density functional theory (DFT) calculations to systematically analyse the performance of eight non-metal single-atom catalysts (NM@MoS<sub>2</sub>, where NM represents B, C, N, O, P, Si, Se, and Te) in the eNORR process. Firstly, we calculated the binding energies of NM@MoS<sub>2</sub> catalysts to evaluate their thermodynamic stability. We then conducted a comprehensive electronic structure analysis to see how well the catalysts could adsorb and activate NO molecules. Next, we examined the eNORR performance of these catalysts in more detail, considering critical factors such as reaction pathways and product selectivity. Finally, we examined the competitive relationship between HER and eNORR. Based on this analysis, we identified potential eNORR catalysts.

## 2 Computational methods

The Vienna *Ab Initio* Simulation Package (VASP) was used for our calculations to perform density functional theory (DFT) calculations of spin polarization.<sup>51</sup> The generalized gradient approximation (GGA) and Perdew–Burke–Ernzerhof (PBE) functional are used to describe the electron exchange and correlation terms.<sup>52</sup> The Projector Augmented Wave (PAW) was used to describe the ion–electron interactions with the energy cutoff set to 450 eV.<sup>53</sup> All atoms were fully relaxed, and the standard parameters for convergence of the energies and forces were set to 10<sup>−4</sup> eV and 0.02 eV Å<sup>−1</sup>. The DFT-D3 method was used to correct for the weak interactions between adsorbates and surfaces (van der Waals interactions).<sup>54</sup> A 4 × 4 × 1 Monkhorst–Pack *k*-point grid was used to sample the Brillouin zone during geometry optimization.<sup>55</sup> A 4 × 4 × 1 single-layer supercell is constructed to model the catalyst surface. In order to eliminate the potential influence of periodic boundary



conditions on the calculation results, a vacuum layer with a thickness of 15 Å was set in the *Z* direction of the lattice. To test the feasibility of doping MoS<sub>2</sub> with non-metal atoms (NM), the binding energy ( $E_{\text{bind}}$ ) was calculated according to eqn (1):

$$E_{\text{b}} = E_{\text{NM@MoS}_2} - E_{\text{defect}} - \mu_{\text{NM}} \quad (1)$$

Here  $E_{\text{NM@MoS}_2}$  and  $E_{\text{defective-MoS}_2}$  represent the total energies of NM atoms deposited on MoS<sub>2</sub> and MoS<sub>2</sub> with one sulphur vacancy, respectively.  $\mu_{\text{NM}}$  denotes the chemical potential of the NM atoms. For N and O atoms, it is obtained from their gas-phase (N<sub>2</sub> and O<sub>2</sub>) energies per atom. The chemical potential of all other atoms are obtained from their bulk or solid phase ( $\beta$ -rhombohedral boron for B, graphite for C, black phosphorus for P, diamond-cubic silicon for Si, grey selenium for Se, and hexagonal tellurium for Te, respectively) energies per atom. In view of the fact that the reaction process involves the transfer of protons and electrons ( $\text{NO} + 5\text{H}^+ + 5\text{e}^- \rightarrow \text{NH}_3 + \text{H}_2\text{O}$ ), we calculate the Gibbs free energy ( $\Delta G$ ) by means of the computational hydrogen electrode (CHE) model, where the free energy of the  $\text{H}^+ + \text{e}^-$  is considered to be half of the chemical potential of the hydrogen gas under standard conditions.<sup>56</sup> The standard conditions for the reaction are  $P_{\text{H}_2} = 1$  bar and a temperature of 298.15 K.  $\Delta G$  of the eNORR step was calculated using eqn (2):

$$\Delta G = \Delta E + \Delta G_U + \Delta G_{\text{pH}} + \Delta E_{\text{ZPE}} - T\Delta S \quad (2)$$

In this equation,  $\Delta E$  represents the energy change between reactants and products, which can be calculated directly from DFT.  $\Delta E_{\text{ZPE}}$  and  $T\Delta S$  are the zero-point energy and entropy changes at room temperature ( $T = 298.15$  K), respectively, which can be calculated from vibrational frequencies *via* the VASPKIT package.<sup>57</sup>  $\Delta G_{\text{pH}}$  is the pH-induced free energy change, calculated as  $\Delta G_{\text{pH}} = K_{\text{B}}T \times \text{pH} \times \ln 10$ , where  $K_{\text{B}}$  is the Boltzmann constant and pH is set to zero.  $\Delta G_U$  is the correction of  $\Delta G$  by the electrode potential  $U$ ,  $\Delta G_U = -eU$ ,  $e$  is the number of electrons transferred at each step and  $U$  is the applied voltage.

The limiting potential ( $U_{\text{L}}$ ) is a measure of catalytic activity, calculated using eqn (3) to determine the minimum voltage required to make each reaction step exothermic.<sup>36,37</sup>

$$U_{\text{L}} = -(\Delta G_1, \Delta G_2, \Delta G_3, \dots, \Delta G_i)_{\text{max}}/e \quad (3)$$

Here,  $\Delta G_i$  denotes the Gibbs free energy for each step of the radical reaction in the eNORR process. According to this definition, the more positive the  $U_{\text{L}}$  of the catalyst, the smaller the applied voltage, indicating the higher catalytic activity. In addition, the effect caused by the solvent on  $\Delta G$  was simulated by the Poisson-Boltzmann (PB) implicit solvent model in the VASP software package.<sup>58</sup>

## 3 Results and discussion

### 3.1. NM@MoS<sub>2</sub> stability

For our study, we precisely substituted all eight non-metallic (NM) atoms, namely B, C, N, O, P, Si, Se, and Te, into sulfur (S) vacancy defects in the MoS<sub>2</sub> substrate, as illustrated in Fig. 1a. To quantitatively evaluate the stability and experimental feasibility of the

eight NM@MoS<sub>2</sub> catalysts, we first calculated their binding energies. By definition, a more negative  $E_{\text{bind}}$  indicates a stronger and more stable interaction between the NM atoms and MoS<sub>2</sub> substrate. As depicted in Fig. 1b, all NM@MoS<sub>2</sub> catalysts showed negative  $E_{\text{bind}}$  values ranging from  $-0.67$  to  $-6.81$  eV, thereby confirming their stability. In addition, the stability of the catalysts was further corroborated by calculation of the electronic localization function (ELF),<sup>59</sup> which elucidates the bonding characteristics between the NM atoms and MoS<sub>2</sub>. The ELF value of 1 (represented by the red region) indicates the presence of a strong covalent bond. As shown in Fig. 1c, there is a significant overlap of electron density between the NM atoms and the Mo atoms, with the NM–Mo bond situated in the red region, indicating the presence of covalent bond components between NM and Mo.

We further elucidate the bonding characteristics between NM and Mo by calculating the projected (pCOHP) and integral (ICOHP) crystal orbital Hamilton populations (see Fig. 2).<sup>60</sup> The left side corresponds to the antibonding orbitals of NM–Mo and the right side to the bonding orbitals in pCOHP. Notably, below the Fermi level, the NM–Mo bond states are predominantly found in the low-energy bonding region, suggesting the stability of the NM–Mo bond. Furthermore, a quantitative assessment of the NM–Mo bond strength using the ICOHP method revealed that, with the exception of the Se@MoS<sub>2</sub> ( $-4.47$ ) and Te@MoS<sub>2</sub> ( $-4.09$ ) systems, the ICOHP values for the B@MoS<sub>2</sub> ( $-5.72$ ), C@MoS<sub>2</sub> ( $-5.98$ ), N@MoS<sub>2</sub> ( $-5.82$ ), O@MoS<sub>2</sub> ( $-5.64$ ), P@MoS<sub>2</sub> ( $-4.85$ ) and Si@MoS<sub>2</sub> ( $-4.74$ ) systems were all lower than that of pristine MoS<sub>2</sub> ( $-4.70$ ). This implies that, in addition to the systems doped with Se and Te, NM–Mo bonds are stronger than S–Mo bonds. This demonstrates that covalent bonds are also formed between the NM (B, C, N, O, P and Si) atoms and the surrounding Mo atoms. Consequently, NM@MoS<sub>2</sub> can serve as a stable electrocatalyst in the eNORR process.

### 3.2. NO adsorption and activation

The adsorption and activation of NO molecules are pivotal steps in initiating the eNORR and significantly influence the subsequent protonation process. In this study, we thoroughly investigated three potential adsorption configurations of NO molecules on the surface of NM@MoS<sub>2</sub> catalysts: N-end, O-end, and NO-side, as illustrated in Fig. 3a. It is important to highlight that for the O@MoS<sub>2</sub>, Se@MoS<sub>2</sub>, and Te@MoS<sub>2</sub> catalysts, the N-end configurations stable, yet they only exhibit physical adsorption of NO molecules, as evidenced by their  $\Delta G$  (\*NO) values being greater than zero (Fig. 3b). Given their insufficient adsorption strength for NO molecules, these catalysts were deemed unsuitable for the eNORR process and were thus excluded from the list of potential eNORR candidates.

For the remaining five NM@MoS<sub>2</sub> catalysts, NO molecules preferentially adsorb in the N-end configurations on the catalyst surface, exhibiting the smallest  $\Delta G$  (\*NO) values. Notably, after structural optimization, the NO-side adsorption configurations become unstable and spontaneously transition to the N-end configurations. Once adsorbed in the N-end configuration, the N=O bond lengths increase to 1.19 Å (B@MoS<sub>2</sub>), 1.20 Å (C@MoS<sub>2</sub>), 1.20 Å (N@MoS<sub>2</sub>), 1.20 Å (Si@MoS<sub>2</sub>), and 1.23 Å



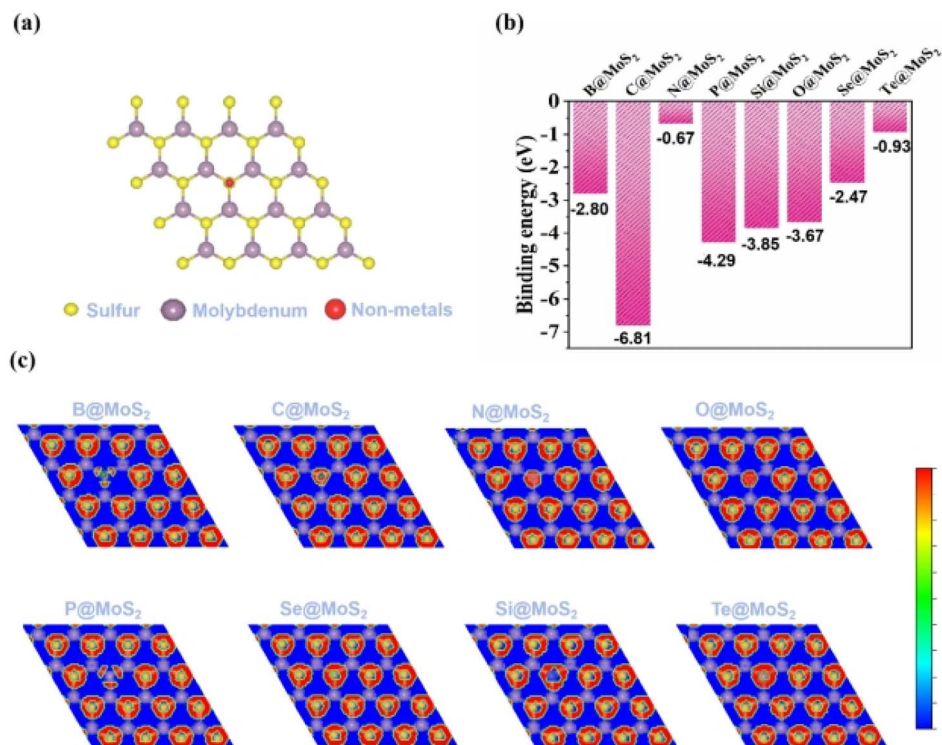


Fig. 1 (a) The modeled structure of NM@MoS<sub>2</sub> catalysts (top); (b) binding energies of NM@MoS<sub>2</sub> catalysts; (c) ELF diagram of NM@MoS<sub>2</sub> catalyst.

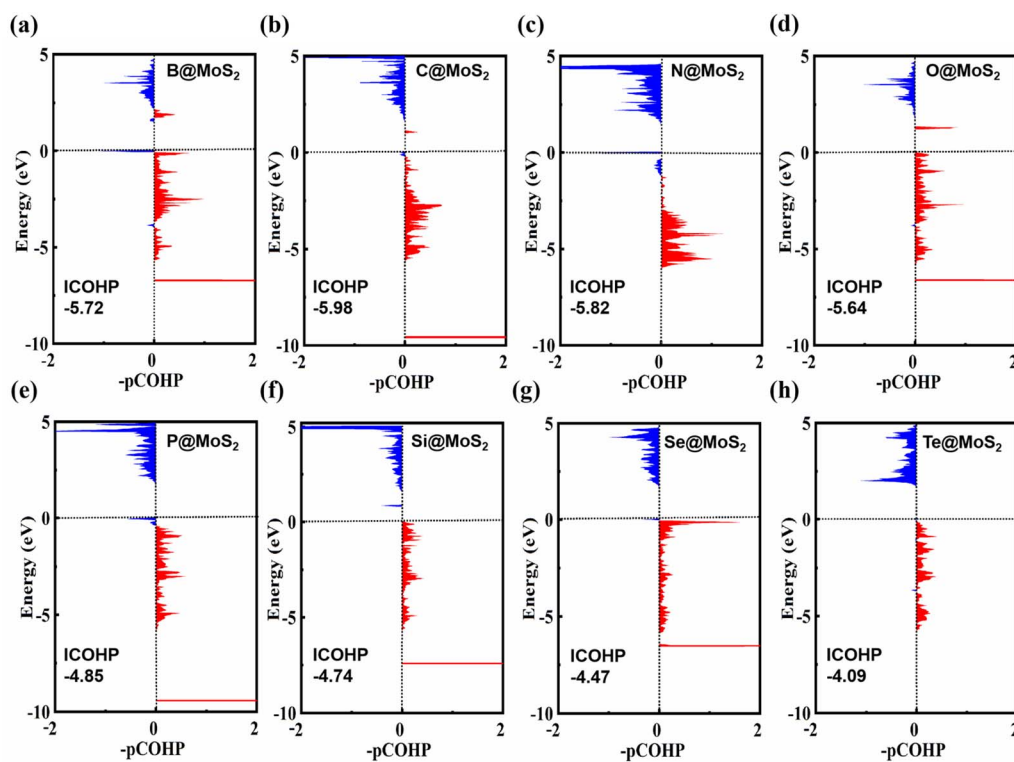


Fig. 2 COHP describes the interaction between the NM and Mo in the NM–Mo bond, while ICOHP represents the strength of this bond (the dashed line corresponds to the Fermi level). (a) B@MoS<sub>2</sub>; (b) C@MoS<sub>2</sub>; (c) N@MoS<sub>2</sub>; (d) O@MoS<sub>2</sub>; (e) P@MoS<sub>2</sub>; (f) Si@MoS<sub>2</sub>; (g) Se@MoS<sub>2</sub>; (h) Te@MoS<sub>2</sub>.



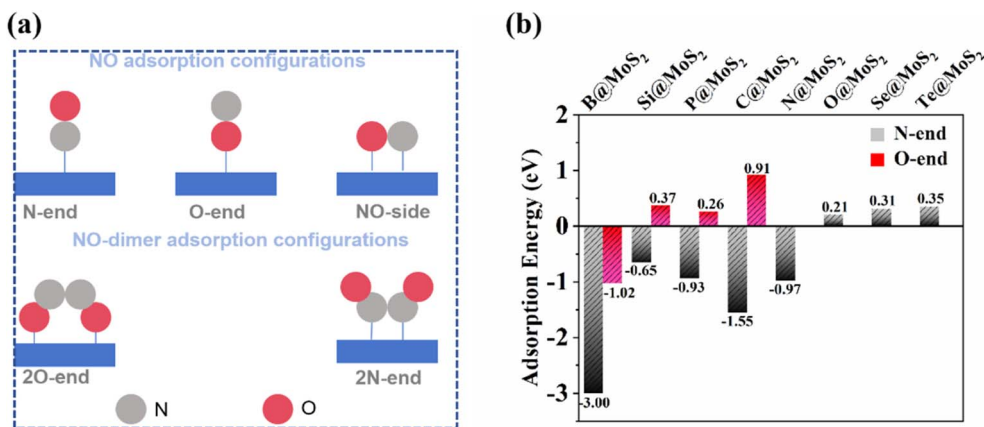


Fig. 3 (a) Possible NO adsorption configurations both high and low NO concentration; (b) NO adsorption energy on NM@MoS<sub>2</sub> catalyst.

(P@MoS<sub>2</sub>), respectively. These values are significantly longer than the bond length of 1.16 Å in the free NO molecule, indicating that the NO molecule is effectively activated upon adsorption onto the catalyst surface.

To further elucidate the active origins of these catalysts, we conducted detailed electronic structure calculations, including charge density difference (CDD) and Bader charge analysis,<sup>61,62</sup> to reveal the charge distribution between the active sites and adsorbed NO (\*NO) molecules. These analyses help explore the underlying interaction mechanisms. Additionally, we employed pCOHP, ICOHP, and partial density of states (PDOS) to gain deeper insights into the orbital contributions and chemical

bonding characteristics at the active sites. This systematic study provides a comprehensive theoretical foundation for understanding the fundamental origins of the catalysts activity.

As depicted in Fig. 4, we plotted the CDD diagram for NO adsorption on NM@MoS<sub>2</sub> catalysts. The green areas signify electron accumulation, while the red areas indicate electron depletion. A significant charge redistribution occurs between the \*NO and the catalyst surface. Specifically, electrons are primarily concentrated on the \*NO molecule, while the neighboring non-metal (NM) atoms lose electrons. Bader charge analysis further confirms this phenomenon, revealing that electrons are transferred from the NM@MoS<sub>2</sub> catalyst to the

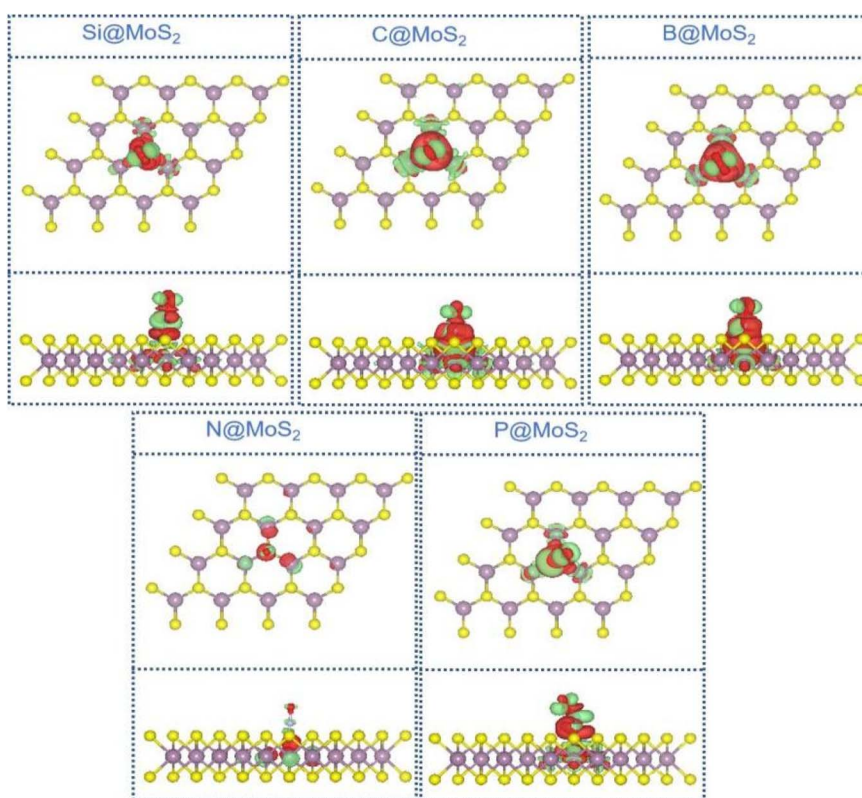


Fig. 4 CDD diagram of NO adsorption on NM@MoS<sub>2</sub> catalyst. The isosurface value is set to 0.002 e Å<sup>-3</sup>.



\*NO molecule, with the transferred electron amounts being  $0.75e$  ( $B@MoS_2$ ),  $0.73e$  ( $Si@MoS_2$ ),  $0.70e$  ( $P@MoS_2$ ),  $0.62e$  ( $C@MoS_2$ ), and  $0.04e$  ( $N@MoS_2$ ). Additionally, a substantial electron density is concentrated between the NM atoms and the

\*NO molecule, suggesting that the newly formed NM–N bond exhibits covalent bonding characteristics.

Fig. 5a presents the PDOS plots for NO molecules after adsorption on different catalysts. It is evident that there is

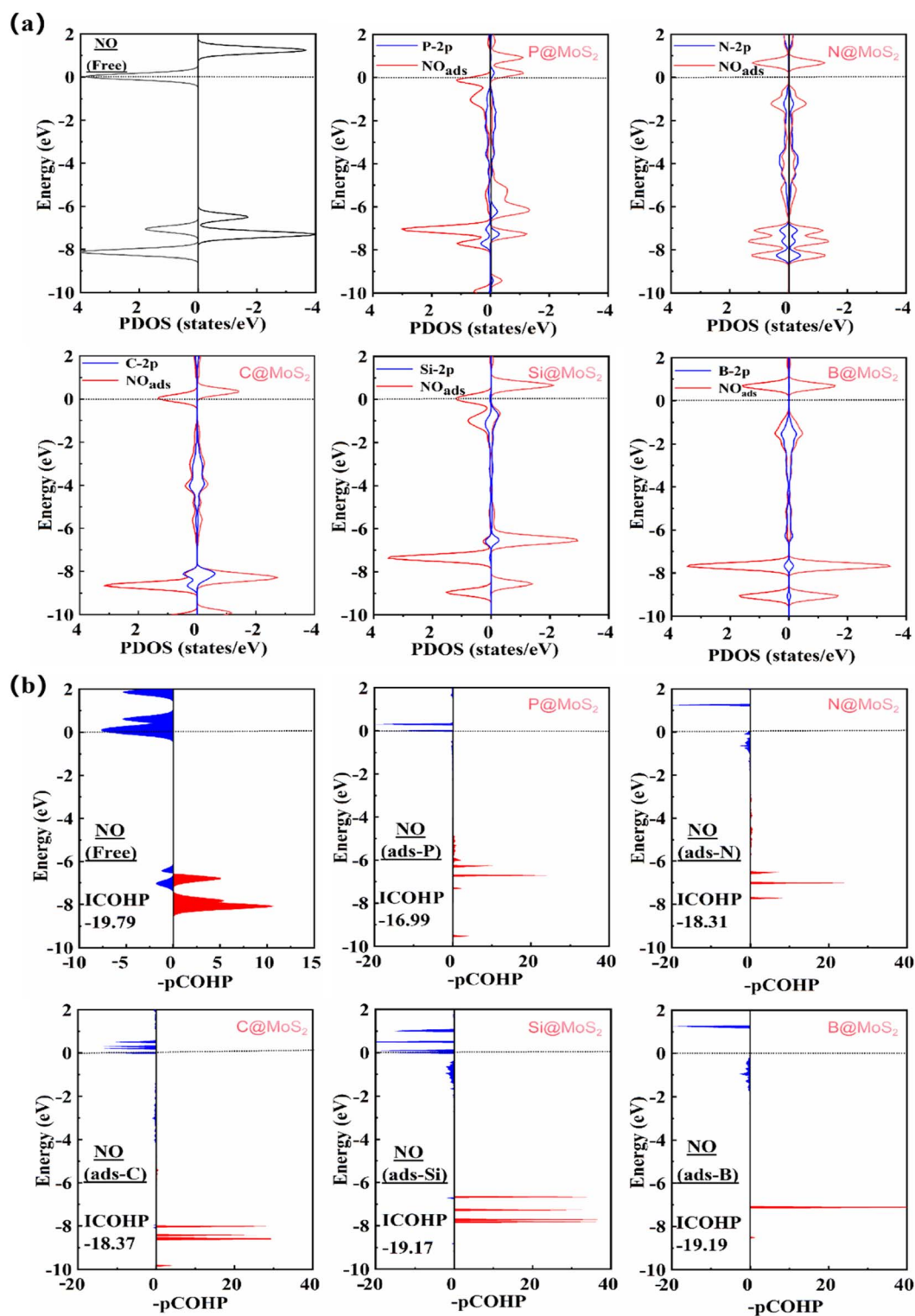


Fig. 5 (a) PDOS diagram of NO adsorption on NM@MoS<sub>2</sub> catalyst; (b) the COHP diagram of NO before and after adsorption. The left side corresponds to the antibonding orbital of the N=O bond and the right side to the bonding orbital. The labelled value of ICOHP indicates the strength of the N–O bond in the N=O bond.



significant orbital mixing between the NM-2p orbitals and the NO-2 $\pi^*$  orbitals near the Fermi energy level, indicating a strong interaction between the NO molecules and the NM atoms. Moreover, the energy of the NO-2 $\pi^*$  orbitals decreases upon adsorption due to electrons transfer from the NM-2p orbitals.

To further investigate NO activation, we plotted the COHP diagram for NO adsorption on NM@MoS<sub>2</sub> catalysts, as shown in Fig. 5b. Upon adsorption of NO molecules on NM@MoS<sub>2</sub> catalysts, the antibonding orbitals of the N=O bonds shift downward near the Fermi energy level, resulting in more antibonding states of the N=O bonds below the Fermi energy level. The integral COHP (ICOHP) values, which quantify the strength of chemical bonds, are  $-16.99$  (P@MoS<sub>2</sub>),  $-18.31$  (N@MoS<sub>2</sub>),  $-18.37$  (C@MoS<sub>2</sub>),  $-19.17$  (Si@MoS<sub>2</sub>), and  $-19.19$  (B@MoS<sub>2</sub>). These values are less negative compared to  $-19.79$  for the free NO molecule, indicating effective activation of the N=O bonds upon NO adsorption.

Based on these findings, non-metal atoms act as active sites, effectively adsorbing and activating NO molecules. Given that the N-end adsorption configurations of NO molecules is more stable, we primarily focus on discussing the eNORR behavior of NO in the N-end adsorption configuration.

### 3.3. eNORR mechanism and activity

The eNORR reaction can proceed through several potential reduction pathways, and the coverage of NO molecules plays a crucial role in determining product selectivity. As shown in Fig. 6a, at low NO coverage, the reaction involves five proton-coupled electron transfer steps, ultimately yielding NH<sub>3</sub>. By contrast, at high NO coverage, the reaction is driven by the dimerisation of NO molecules to form N<sub>2</sub>O<sub>2</sub>, resulting in the production of N<sub>2</sub>O or N<sub>2</sub> as by-products.<sup>63</sup>

We evaluated the catalytic performance of B@MoS<sub>2</sub>, C@MoS<sub>2</sub>, P@MoS<sub>2</sub>, Si@MoS<sub>2</sub>, and N@MoS<sub>2</sub> catalysts in the eNORR for

NH<sub>3</sub> synthesis based on the possible pathways shown in the reaction schematic in Fig. 6a. The results are summarized in Table S1 and Fig. 7. As shown in Fig. 7, the eNORR process begins with the adsorption of NO molecules to form \*NO species. Subsequently, the protons in the electrolyte react with \*NO to form \*HNO or \*NOH intermediates. Then sequential hydrogenation processes occur, finally yielding NH<sub>3</sub> and H<sub>2</sub>O.

As shown in Fig. 7a, the most selective pathway for the C@MoS<sub>2</sub> catalyst is Mix2, with all elementary steps being exergonic ( $\Delta G < 0$  eV). This suggests that the eNORR process can proceed spontaneously. As a result, the limiting potential ( $U_L$ ) for the C@MoS<sub>2</sub> catalyst is 0 V. For the Si@MoS<sub>2</sub> catalyst, the most favorable path is the N-end path depicted in Fig. 7b. In this pathway, the energy of each intermediate species decreases, enabling the eNORR process to occur at 0 V, meaning that the  $U_L$  for the Si@MoS<sub>2</sub> catalyst is also 0 V. For the N@MoS<sub>2</sub> catalyst, the optimal reaction path is the N-end path (Fig. 7c). Here, the energies of all elementary steps decrease, except for the final step (\*NH<sub>2</sub>  $\rightarrow$  \*NH<sub>3</sub>), which exhibits an energy increase ( $\Delta G = 0.36$  eV). This step is identified as the RDS, with a corresponding  $U_L$  of  $-0.36$  V. For the B@MoS<sub>2</sub> catalyst (Fig. 7d), the optimal reaction pathway is Mix1. Along this pathway, overcoming the energy barrier of 0.62 eV ( $\Delta G = 0.62$  eV) in the \*NO  $\rightarrow$  \*NHO step is the RDS, resulting in a  $U_L$  of  $-0.62$  V. Similarly, for the P@MoS<sub>2</sub> catalyst, the Mix1 pathway is identified as the optimal reaction pathway (Fig. 7e). Here, the energy of all elementary steps decreases, except for the NH<sub>2</sub>  $\rightarrow$  NH<sub>3</sub> step, which has an energy barrier of 0.70 eV. This step is the RDS, with a  $U_L$  of  $-0.70$  V. Under acidic conditions, the conversion of NH<sub>3</sub> to NH<sub>4</sub><sup>+</sup> is typically exergonic.<sup>64</sup> Therefore, the catalytic activity of the NM@MoS<sub>2</sub> catalysts for eNORR to NH<sub>3</sub> was evaluated without considering NH<sub>3</sub> desorption further.

Since no thermodynamic energy barrier was observed on the C@MoS<sub>2</sub> and Si@MoS<sub>2</sub> catalysts. Taking the C@MoS<sub>2</sub> catalyst as

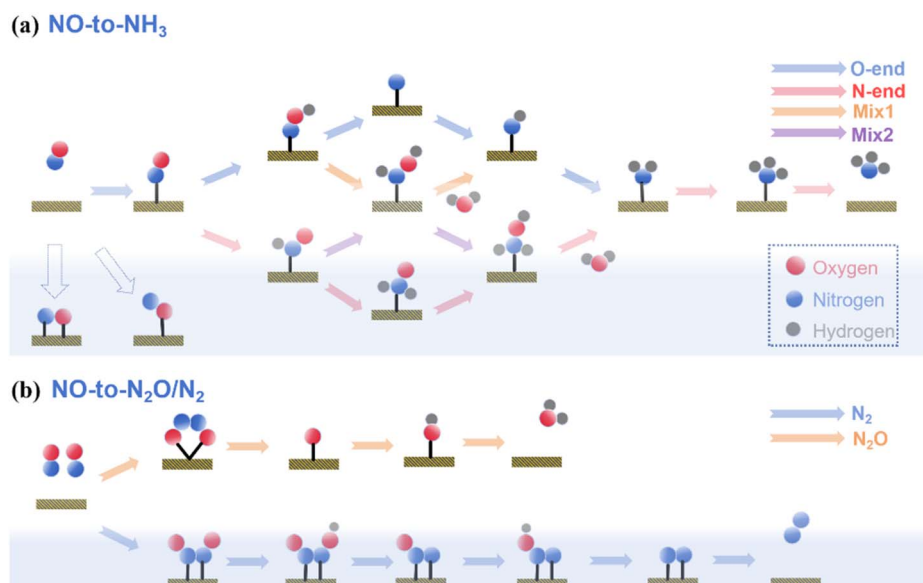


Fig. 6 Schematic illustration of possible eNORR reaction pathways; (a) pathway to the formation of NH<sub>3</sub>; (b) pathway to the formation of N<sub>2</sub>O or N<sub>2</sub>.



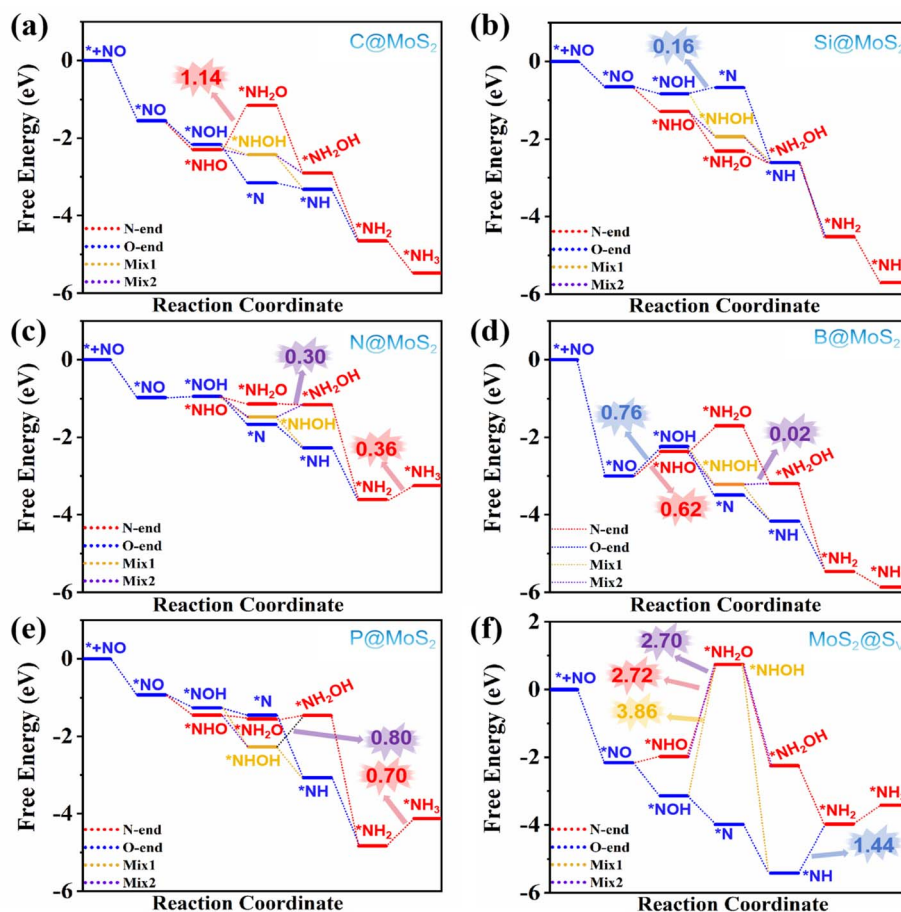


Fig. 7 Free energy diagrams of eNORR to  $\text{NH}_3$  over five  $\text{NM@MoS}_2$  catalysts and one  $\text{MoS}_2@V_s$  catalysts; (a)  $\text{C@MoS}_2$ ; (b)  $\text{Si@MoS}_2$ ; (c)  $\text{N@MoS}_2$ ; (d)  $\text{B@MoS}_2$ ; (e)  $\text{P@MoS}_2$ ; (f)  $\text{MoS}_2@V_s$ .

an example, we employed the climbing-image nudged elastic band (CI-NEB) method to calculate the energy barriers for each elementary step along the optimal reaction path of Mix2. The energy barriers ( $E_B$ ) for all elementary reaction steps are shown in Fig. S1. As shown in Fig. S1, the energy barrier (0.92 eV) for the third hydrogenation step ( $\text{NHOH} + \text{H}^+ + \text{e}^- \rightarrow \text{*NH}_2\text{OH}$ ) is higher than for the other steps. Consequently, this process constitutes the kinetically rate-determining step of this reaction pathway. However, from  $\text{NO}(\text{g})$  to the  $\text{NH}_2\text{OH}$  species, all elementary reaction steps are exergonic, with a total energy of  $-2.89$  eV. This value is higher than the kinetic energy barrier (0.92 eV), suggesting that the energies released from the previous elementary reactions are sufficient to overcome the energy barrier.

To further elucidate the impact of NM atom modification, we examined the eNORR activity of  $\text{MoS}_2$  containing sulfur vacancies ( $\text{MoS}_2@V_s$ ). For the  $\text{MoS}_2@V_s$  catalyst, the most favorable path is the O-end pathway, as depicted in Fig. 7f. Along this pathway, the  $\text{*NH} \rightarrow \text{*NH}_2$  process is the RDS with a  $U_L$  value of  $-1.44$  V. This demonstrates that the  $U_L$  values of the  $\text{NM@MoS}_2$  catalysts are substantially altered compared to the unmodified  $\text{MoS}_2@V_s$  catalyst: the  $U_L$  values of  $\text{C@MoS}_2$  and  $\text{Si@MoS}_2$  are both elevated to 0 V; the  $U_L$  value of  $\text{N@MoS}_2$  is increased to  $-0.36$  V; the  $U_L$  value of  $\text{B@MoS}_2$  is elevated to  $-0.62$  V; and the

$U_L$  value of  $\text{P@MoS}_2$  is increased to  $-0.70$  V. These analyses clearly demonstrate that NM atom modification dramatically enhances the eNORR activity of  $\text{MoS}_2$  catalysts.

Based on the above analysis, the catalytic performance of the  $\text{C@MoS}_2$  and  $\text{Si@MoS}_2$  catalysts is superior to that of the  $\text{B@MoS}_2$ ,  $\text{N@MoS}_2$ , and  $\text{P@MoS}_2$  catalysts. To elucidate the differences in catalytic activity, we conducted an electronic structure analysis of each catalyst. Fig. S2 shows the band structures of  $\text{N@MoS}_2$ ,  $\text{P@MoS}_2$ ,  $\text{B@MoS}_2$ ,  $\text{C@MoS}_2$ , and  $\text{Si@MoS}_2$ . Notably, the bandgap widths of  $\text{C@MoS}_2$  (0.97 eV) and  $\text{Si@MoS}_2$  (0.78 eV) are significantly smaller than those of  $\text{N@MoS}_2$  (1.62 eV),  $\text{P@MoS}_2$  (1.54 eV), and  $\text{B@MoS}_2$  (1.37 eV). Consequently,  $\text{C@MoS}_2$  and  $\text{Si@MoS}_2$  exhibit higher electron mobility throughout the eNORR process. This optimizes the adsorption of reaction intermediates and reduces the energy barriers of key steps, such as  $\text{*NO} \rightarrow \text{*NHO}$  or  $\text{*NH}_2 \rightarrow \text{*NH}_3$ , thereby significantly enhancing eNORR activity.

It has been well-documented that at high  $\text{NO}$  concentrations,  $\text{*NO}$  molecules can form dimers ( $\text{*NONO}$ ), as illustrated in the configuration shown in Fig. 3a. These  $\text{*NONO}$  dimers can adsorb onto the catalyst surface in either a 2O-side or 2N-side configuration, leading to the formation of by-products such as  $\text{N}_2\text{O}$  or  $\text{N}_2$  (Fig. 6b shows possible reaction pathways).<sup>63</sup> To further



investigate the catalytic behavior of eNORR at high NO concentrations, we conducted a detailed analysis of the catalytic activity for this reaction (see Table S2).

For the C@MoS<sub>2</sub>, P@MoS<sub>2</sub>, and N@MoS<sub>2</sub> catalysts, the high electronegativity of the C, P and N elements significantly inhibits electron transfer during adsorption. This results in an unstable 2N-side adsorption configuration of NONO, thereby preventing the side reaction that leads to N<sub>2</sub> formation. Additionally, the N@MoS<sub>2</sub> catalyst lacks an O-end adsorption configuration for NO monomers, which prevents \*NONO from adsorbing in the 2O-side configuration.<sup>65</sup> Consequently, the N@MoS<sub>2</sub> catalyst exclusively produces NH<sub>3</sub> as the main product while effectively suppressing the formation of N<sub>2</sub>O and N<sub>2</sub> by-products.

In contrast, on B@MoS<sub>2</sub> and Si@MoS<sub>2</sub> catalysts, we discovered that \*NONO has a preference for adsorbing on the 2O-side configuration by contrasting the adsorption energies of \*NONO in two different configurations. This selective adsorption configuration inhibits the formation of N<sub>2</sub>, thereby reducing the likelihood of N<sub>2</sub> being produced as a by-product. Therefore, we focused on the reaction pathway from \*NONO to N<sub>2</sub>O over the C@MoS<sub>2</sub>, P@MoS<sub>2</sub>, B@MoS<sub>2</sub>, and Si@MoS<sub>2</sub> catalysts, as shown in Fig. 8.

As depicted in Fig. 8, the rate-determining step (RDS) for N<sub>2</sub>O formation is the conversion of OH to H<sub>2</sub>O. The corresponding limiting potentials ( $U_L$ ) for this process are  $-0.36$  V (C@MoS<sub>2</sub>),  $-1.04$  V (Si@MoS<sub>2</sub>),  $-1.17$  V (P@MoS<sub>2</sub>), and  $-1.63$  V (B@MoS<sub>2</sub>). Based on these results, the aforementioned catalysts exhibit high selectivity for NH<sub>3</sub>, even at high NO coverage, as evidenced by  $U_L(\text{NH}_3) > U_L(\text{N}_2\text{O})$ . Furthermore, the N@MoS<sub>2</sub> catalyst demonstrates high selectivity for NH<sub>3</sub> given that the formation of \*NONO is unfavourable on this catalyst.

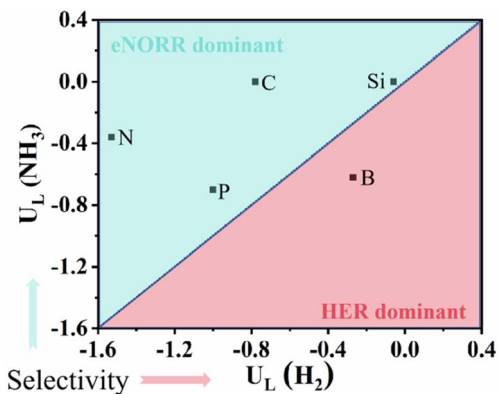


Fig. 9 The  $U_L(\text{NH}_3)$  versus the  $U_L(\text{HER})$ .

In summary, the C@MoS<sub>2</sub>, P@MoS<sub>2</sub>, B@MoS<sub>2</sub>, Si@MoS<sub>2</sub>, and N@MoS<sub>2</sub> catalysts all demonstrate excellent selectivity for NH<sub>3</sub> products under conditions of high NO coverage. This suggests that these catalysts are highly promising for the efficient synthesis of NH<sub>3</sub> *via* the eNORR process.

### 3.4. eNORR with HER selectivity

In aqueous solutions, the HER is the main competitive process for the eNORR.<sup>66</sup> Thus, we compare the  $U_L(\text{NH}_3)$  and  $U_L(\text{H}_2)$  values for the five NM@MoS<sub>2</sub> catalysts (see Fig. 9).

As shown in Fig. 9, the  $U_L(\text{H}_2)$  values on the five catalysts are as follows:  $-0.06$  V (Si@MoS<sub>2</sub>),  $-0.27$  V (B@MoS<sub>2</sub>),  $-0.78$  V (C@MoS<sub>2</sub>),  $-1.00$  V (P@MoS<sub>2</sub>), and  $-1.53$  V (N@MoS<sub>2</sub>). Our calculations reveal that, for P@MoS<sub>2</sub>, N@MoS<sub>2</sub>, C@MoS<sub>2</sub>, and Si@MoS<sub>2</sub>, the  $U_L(\text{NH}_3)$  values are notably higher than the  $U_L(\text{H}_2)$  values. At the initial potential, eNORR can effectively

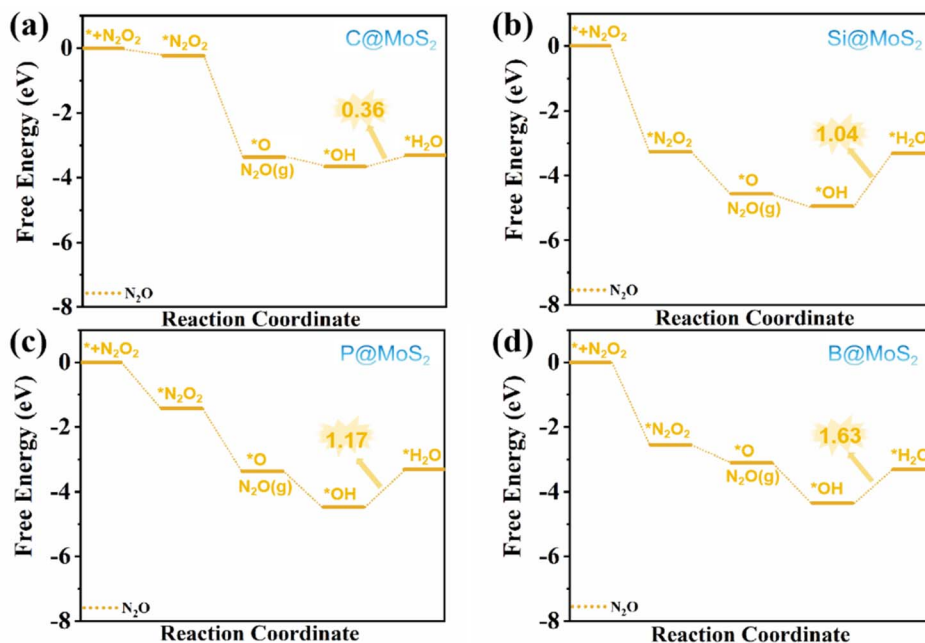


Fig. 8 Free energy diagrams of eNORR to N<sub>2</sub>O over four NM@MoS<sub>2</sub> catalysts; (a) C@MoS<sub>2</sub>; (b) Si@MoS<sub>2</sub>; (c) P@MoS<sub>2</sub>; (d) B@MoS<sub>2</sub>.



inhibit the occurrence of HER, thereby enhancing the selectivity and efficiency of eNORR.

Consequently, N, P, C, and Si@MoS<sub>2</sub> catalysts demonstrate superior performance in prioritising eNORR over HER, rendering them highly promising candidates for efficient NH<sub>3</sub> synthesis *via* eNORR.

## 4 Conclusions

In summary, we used DFT calculations to identify and screen potential catalysts for NH<sub>3</sub> synthesis *via* the eNORR. We focused on eight thermodynamically stable NM@MoS<sub>2</sub> catalysts (where NM = B, C, N, O, P, Si, Se, or Te), evaluating their ability to adsorb and activate NO molecules. Our computational results revealed that five of the catalysts (those with NM = B, C, N, P and Si) exhibited effective adsorption and activation of NO molecules and significant potential for the eNORR, with  $U_L$  values of 0 V for Si@MoS<sub>2</sub> and C@MoS<sub>2</sub>, -0.36 V for N@MoS<sub>2</sub>, -0.62 V for B@MoS<sub>2</sub>, and -0.70 V for P@MoS<sub>2</sub>. These catalysts also exhibited high NH<sub>3</sub> selectivity by suppressing HER competition and minimizing side reactions. These results demonstrate that NM@MoS<sub>2</sub> catalysts excel in terms of stability, selectivity and catalytic activity, making them highly promising eNORR candidates. This study offers fresh perspectives on the management of NO and the synthesis of NH<sub>3</sub>, and could pave the way for more efficient and sustainable catalytic processes.

## Author contributions

Yifan Liu: data curation, formal analysis, writing – original draft. Mamutjan Tursun: conceptualization, data curation, writing – review & editing. Guangzhi Hu: writing – review & editing. Abdukader Abdukayum: writing – review & editing. Chao Wu: software, computing resource, writing – review & editing.

## Conflicts of interest

There are no conflicts to declare.

## Data availability

The data supporting this article have been included as part of the SI.

Supplementary information is available: Energy Barriers ( $E_B$ ) of each elementary reaction steps for C@MoS<sub>2</sub>; band structures of NM@MoS<sub>2</sub> catalysts; at low NO coverage, free energy changes ( $\Delta G$ ) of all eNORR elementary steps for NM@MoS<sub>2</sub> (NM = B, C, N, P, and Si); at high NO coverage, free energy changes ( $\Delta G$ ) of all eNORR elementary steps for NM@MoS<sub>2</sub> (NM = B, C, N, P, and Si). See DOI: <https://doi.org/10.1039/d5ra04718h>.

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