


Cite this: *RSC Adv.*, 2025, 15, 25940

# Mass-balancing strategy enhances the cycling stability of rice husk-derived activated carbon-based supercapacitors in KOH electrolyte†

Dechen Liu, <sup>ab</sup> Wenli Zhang, <sup>b</sup> Haibo Lin <sup>\*b</sup> and Nan Lin <sup>\*c</sup>

Rice husk-derived activated carbon prepared *via* KOH activation usually has high specific capacitance due to its high oxygen content and high specific surface area, which is regarded as a promising candidate for supercapacitor electrodes. However, the poor cycling stability of supercapacitors based on rice husk-derived activated carbon in KOH electrolyte severely limit its commercial application. In this study, the influence of different positive-to-negative electrode mass ratios on the cycling stability of supercapacitors was systematically investigated using rice husk-derived activated carbon as electrode materials. The results show that increasing the positive-to-negative electrode mass ratios significantly enhances the cycling stability of supercapacitors. In this process, the continuous increase in positive electrode potential is effectively suppressed, which avoid the oxidation of the positive electrode. When the positive-to-negative electrode mass ratio is increased from 1 to 2, the capacitance retention of the supercapacitors significantly increases from 27.9% to 96.4% after 10 000 charge–discharge cycles. Meanwhile, the specific capacitance is only reduced by 9.1%. The supercapacitor with positive-to-negative electrode mass ratio s of 1 and 2 shows energy densities of 10.68 W h kg<sup>−1</sup> and 9.54 W h kg<sup>−1</sup> at 0.5 A g<sup>−1</sup>, retaining 46.8% and 43.4% of energy densities at 20 A g<sup>−1</sup>. Adjusting the positive-to-negative electrode mass ratio does not significantly affect the electrochemical properties of supercapacitors. Thus, this work unfolds a new strategy for enhancing the cycling stability of activated carbon-based supercapacitors in alkaline electrolytes and a viable route for practical energy storage applications of rice husk-derived activated carbon in supercapacitors.

Received 30th April 2025

Accepted 12th June 2025

DOI: 10.1039/d5ra03028e

rsc.li/rsc-advances

## Introduction

Carbon-based supercapacitors (SCs) are regarded as a promising energy storage device owing to their long cycle life, high power density, and fast charge/discharge capability.<sup>1–3</sup> Among various carbon materials, activated carbon (AC) has been widely investigated as an electrode material for SCs because of its high specific surface area, abundant raw materials, excellent electrical properties and low cost.<sup>4–6</sup> ACs with high specific surface area generally possess high specific capacitance, which endows SCs with high energy density. Therefore, significant research efforts have been dedicated to preparing ACs from various precursors to achieve high specific surface area.<sup>7–9</sup> Rice husk (RH), due to its abundance and low cost, has been extensively

employed in the preparation of activated carbons through chemical activation processes. Prior investigations have shown that KOH activation enables rice husk-derived activated carbon (RHC) to achieve exceptional specific surface areas up to 3000 m<sup>2</sup> g<sup>−1</sup>.<sup>10,11</sup> Furthermore, KOH activation simultaneously introduces abundant oxygen-containing functional groups on the surface of the ACs.<sup>12</sup> Although oxygen-containing functional groups contribute the pseudocapacitance in AC, they simultaneously compromise cycling stability, especially in the KOH electrolyte system.<sup>13,14</sup> During electrochemical processes, the unstable oxygen-containing functional groups are prone to undergo irreversible redox reactions. This not only causes a rapid decline in the capacity initially provided by these functional groups but also leads to progressive pore structure blockage in the electrode material.<sup>12</sup>

In our previous studies, comparable electrochemical degradation behavior was observed in SCs employing RHC electrodes and KOH electrolyte.<sup>15</sup> Meanwhile, it has been found that capacity fading in SCs originates from the severe oxidation of the positive electrode, which results from the continuous increase in positive electrode potential during cycling. This oxidative degradation correlates with the accumulation of oxygen-containing functional groups on the positive carbon

<sup>a</sup>Jilin Province Innovation Center for Criminal Science and Technology, Jilin Police College, Changchun 130117, China

<sup>b</sup>College of Chemistry, Jilin University, Changchun 130012, China. E-mail: lhb910@jlu.edu.cn

<sup>c</sup>State Key Laboratory of Inorganic Synthesis & Preparative Chemistry, Jilin University, Changchun, 130012, China. E-mail: nanlin@jlu.edu.cn

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d5ra03028e>



electrode surface, which catalyze parasitic side reactions. To enhance the cycle life of SCs, thermal treatment was conducted under the protection of nitrogen to reduce the oxygen-containing functional groups on RHC. However, the specific capacitance of RHCs exhibited a significant decrease after heat treatment, which would severely limit the application of RHC-based SCs.<sup>15</sup> How can the cycle life of SCs in KOH electrolytes be enhanced without sacrificing capacitive performance, and what strategies can be taken to prevent the positive electrode oxidation induced by the increasing electrode potential during cycling? Despite the ubiquity of KOH electrolytes in commercial SCs, systematic studies addressing these challenges remain scarce.<sup>16</sup>

This study proposes a mass-balancing strategy to enhance the cycling stability of SCs in alkaline electrolytes by strategically adjusting the positive-to-negative electrode mass ratio ( $m_+/m_-$ ). Four SCs with varying  $m_+/m_-$  (1, 1.25, 1.5, and 2) were fabricated using RHC as the active material for both electrodes and 6.0 mol per L KOH as aqueous electrolyte. The electrochemical performance of the SCs was systematically evaluated through electrochemical impedance spectroscopy (EIS), galvanostatic charge-discharge (GCD), and cyclic voltammetry (CV).

## Experimental

### Materials

Rice husk was sourced from a rice milling facility in Changchun City, Jilin Province. Additional chemicals (analytical grade) were procured from Sinopharm Chemical Reagent Co., Ltd. High-purity nitrogen and deionized water were used throughout the experimental procedures.

### Preparation of RHC

Firstly, the RH was thoroughly washed to remove impurities and then dried at 80 °C in an oven for 10 hours. Subsequently, the dried RH was pulverized into fine power. RH powder was subjected to carbonization at 500 °C with 10 °C min<sup>-1</sup> under a nitrogen atmosphere. The carbonization process was maintained continuously for 1 hour. The carbonized rice husk was then mixed uniformly with KOH solution at a 1 : 4 mass ratio, and the mixtures were dried at 110 °C for 24 hours. Following this, the dried mixtures were activated at 700 °C for 1 hour. The activated samples were rinsed to neutral pH with deionized water. Finally, the activated carbon dried at 110 °C for 24 hours. The final activated carbon labelled as RHC.

### Material characterization

The porous characteristics of the synthesized materials were evaluated by an ASAP 2010 Micromeritics instrument with N<sub>2</sub> adsorption at 77 K. Specific surface area was calculated *via* the Brunauer-Emmett-Teller (BET) method, while total pore volume was determined from the adsorption data at  $P/P_0 = 0.97$ . Surface chemical composition was characterized by X-ray photoelectron spectroscopy (XPS) using a Thermo VG ESCA-LAB250 surface analysis system. Survey scans and high-resolution spectra were acquired to quantify elemental

composition and oxygen-containing functional groups. The crystallinity of the sample was evaluated by X-ray diffraction (XRD, Rigaku D/max 2550). The surface morphology and pore structure were characterized using a Scanning electron microscopy (SEM; HITACHI SU8020) and transmission electron microscopy (TEM, JEOL, JEM 1200EX).

### Electrochemical measurements

The electrode was fabricated by homogenizing mixture of RHC (85 wt%), polytetrafluoroethylene (5 wt%), and carbon black (10 wt%). The electrochemical performance of SCs fabricated with different mass ratios of the positive and negative electrodes ( $m_+/m_- = 1, 1.25, 1.5$ , and 2) was evaluated employing a two-electrode configuration in 6 mol per L KOH electrolyte. In SCs, the electrode area of both the positive and negative electrodes is  $1 \times 1 \text{ cm}^2$ . The mass loading of the positive electrode is  $4 \text{ mg cm}^{-2}$ , and the mass of the negative electrode is matched according to different positive-to-negative electrode mass ratios. The electrochemical performance of the SCs was systematically evaluated using a PARSTAT 2273 electrochemical workstation (Ametek, USA) and a BTS4008 battery tester (Neware, China). CV measurement was conducted at a scan rate of  $5 \text{ mV s}^{-1}$  to characterize the capacitive behavior, while EIS analysis was carried out over a frequency range of 10 mHz to 100 kHz to study charge transfer resistance and ion diffusion characteristics. GCD tests were conducted at various current densities (0.5, 1, 2, 5, 10, 20 A g<sup>-1</sup>) within an operating voltage range of 0–1 V to characterize the SCs with varying  $m_+/m_-$  ratios. Cycling stability tests were carried out using the GCD at a constant current density of 1 A g<sup>-1</sup> and a voltage range of 0–1 V. Meanwhile, the electrode potentials were monitored during GCD cycling of SCs. When the voltage of SC is 1 V (fully charged state), the positive electrode potential attains its maximum value, which is defined as  $E_{\text{max}+}$ . Concurrently, the negative electrode potential reaches its minimum value, denoted as  $E_{\text{min}-}$ . When the voltage of SC is 0 V (fully discharged state), the potentials of both the positive and negative electrodes converge to an identical value, which is defined as the equilibrium potential  $E_e$ . During the GCD cycling of SC, the potential variation range of the positive electrode is defined as  $\Delta E_+$ , and the corresponding range for the negative electrode is defined as  $\Delta E_-$ .

The electrochemical performance of RHC electrode was studied in a three-electrode configuration with 6 mol per L KOH electrolyte, employing a Hg/HgO reference electrode (0.098 V vs. NHE) and a platinum counter electrode. The GCD was carried out within the potential variation ranges of the positive and negative electrodes at different current densities (0.5, 1, 2, 5, 10, 20 A g<sup>-1</sup>). The CV was conducted at a scan rate of  $5 \text{ mV s}^{-1}$  over a potential window of  $-1.2 \text{ V}$  to  $0.2 \text{ V}$  vs. Hg/HgO.

The specific capacitance was calculated in a two-electrode configuration using the total mass of positive and negative electrodes through CV and GCD measurements, which are performed using the following formulas respectively:

$$C_t = \frac{\int IdV}{2 \times m_t \times v \times \Delta V} \quad (1)$$



where,  $C_t$  is the specific capacitance of SC,  $m_t$  is the total mass of positive and negative electrodes,  $\int IdV$  is the area of the voltammogram curve,  $v$  is the scan rate,  $\Delta V$  is the voltage change.

$$C_t = \frac{I\Delta t}{m_t \times \Delta V} \quad (2)$$

where,  $C_t$  is the specific capacitance of SC,  $m_t$  is the total mass of positive and negative electrodes,  $I$  is the discharge current,  $\Delta t$  is the discharge time,  $\Delta V$  is the voltage change without the IR drop.

The energy density and power density of the SCs were calculated using the following formulas respectively:

$$E = \frac{1}{2} C_t \Delta V^2 \quad (3)$$

$$P = \frac{E}{\Delta t} \quad (4)$$

where,  $E$  is the energy density of supercapacitor,  $P$  is the power density,  $C_t$  is the specific capacitance of supercapacitor,  $\Delta t$  is the discharge time,  $\Delta V$  is the voltage change without the IR drop.

## Results and discussion

### Structural and chemical characteristics of RHC

Fig. 1a and b show the morphology of RHC. The hierarchical macroporous structure with varying diameters was observed on the surface of RHC. In addition, abundant micropores and mesopores were observed in RHC (Fig. 1c), which exhibits a three-dimensional cross-linked framework. Furthermore, the

highly interconnected pore network in RHC not only serves as an ion-buffering reservoir to facilitate efficient charge transport but also effectively reduces internal resistance while simultaneously offering a large accessible surface area and abundant adsorption sites.<sup>17–19</sup> XRD patterns of the RHC is shown in Fig. 1d. A broad peak centered at 43° assigned to the (002) reflections of graphitic carbon and a weak peak at 22° corresponding to the (100) lattice planes are observed in RHC, collectively indicating the presence of an amorphous carbon structure.<sup>20,21</sup> In the XRD patterns, the slope of the curve at small angles ( $\leq 15^\circ$ ) reflects the microporosity abundance within the materials, where a steeper gradient specifically indicates a higher density of micropores.<sup>22</sup>

Fig. 1e presents the  $N_2$  adsorption–desorption isotherm curve of RHC. It can be clearly observed that RHC exhibits a typical type IV isothermal adsorption–desorption curve. This indicates that RHC is mainly a microporous material. This observation aligns with the XRD patterns (Fig. 1d). Meanwhile, the RHC demonstrated an exceptionally high specific surface area of 3185 m<sup>2</sup> g<sup>−1</sup>, as determined by BET analysis with  $N_2$  adsorption at 77 K. This remarkable textural property originated from the well-developed microporous architecture during the KOH activation process.<sup>23,24</sup> The ultrahigh specific surface area engenders abundant electrochemical active sites, facilitating efficient electric double-layer formation, which empowers RHC to achieve an exceptional specific capacitance.<sup>25</sup> As shown in the inset of Fig. 1e, the pore size distribution of RHC ranges from 0.5 to 4 nm, indicating that its structure is composed of a large number of micropores and a small amount of mesopores. This result is in good agreement with the conclusion drawn from the nitrogen adsorption–desorption isotherm. The detailed porous parameters of RHC are summarized in Table S1 (in the ESI).† The chemical characteristics of the RHC were analyzed using XPS. The XPS spectrum in Fig. 1f exhibits two main peaks located at 284.8 eV (C 1s) and 531 eV (O 1s), respectively. The total oxygen content of RHC was determined based on the core energy levels of O 1s using peak intensities. The RHC has a high total oxygen content value of 8.54 at%, which is favorable for obtaining pseudocapacitance. The oxygen-containing functional groups of RHC was quantified through XPS depth profiling and elemental analysis, with detailed composition data provided in Table S2 (in the ESI).†

### The cycling stability of RHC-based supercapacitors in KOH electrolyte

To evaluate the cycling stability of RHC-based supercapacitors in KOH electrolytes, a GCD cycling test was conducted in a symmetric two-electrode configurations ( $m_+/m_- = 1$ ) at a current density of 1 A g<sup>−1</sup>. Fig. 2a shows that the capacitance retention exhibits an accelerating decline throughout the entire cycling process. In the early stages of cycling, the SC maintains high capacitance retention initially. The capacitance retention of the SC decreases slowly before 2000 GCD cycles, yet it still maintains approximately 90.1% of its initial capacitance. Subsequently, the capacitance retention undergoes accelerated degradation. After 10 000 GCD cycles, its capacitance retention

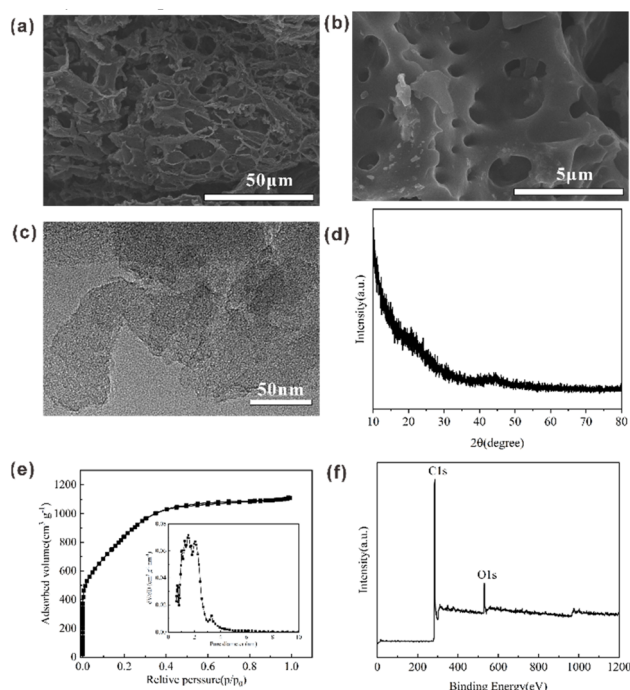


Fig. 1 (a) Low-magnification SEM image; (b) high-magnification SEM image; (c) TEM image; (d) X-ray diffraction pattern; (e)  $N_2$  adsorption–desorption isotherms (inset is the corresponding pore size distribution); and (f) XPS survey scan of RHC.



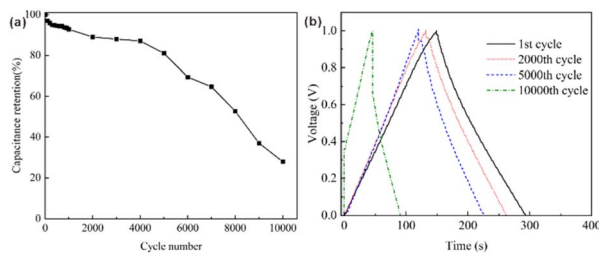


Fig. 2 (a) The capacitance retention of the symmetric supercapacitor over 10 000 cycles at  $1 \text{ A g}^{-1}$  and (b) GCD curves of the symmetric supercapacitor at different numbers of cycles at  $1 \text{ A g}^{-1}$ .

is only 27.9%, which indicates the poor cycling stability of the symmetric SC in KOH electrolyte.

Fig. 2b shows the GCD curves of the symmetric supercapacitor at different cycle numbers. At the initial stages of cycling, GCD curves show the typical behavior of electric double-layer capacitive behavior. However, after several cycles, this behavior is distorted. The poor electrochemical behavior of SC in KOH electrolyte after 10 000 cycles is clearly evidenced by pronounced GCD curve distortion. Concurrently, the high voltage drop is observed after 10 000 GCD cycles, which is associated with the increase in its internal large ion diffusion resistance.<sup>26</sup> To determine the electrode responsible for voltage drop, the electrode potentials of the positive and negative electrodes before and after cycling were recorded (Fig. S1 in the ESI).<sup>†</sup> As shown in Fig. S1,<sup>†</sup> the positive electrode potential dropped sharply when the SC changed from the charging state to the discharging state. In contrast, the negative electrode potential did not show significant changes during the cycling process. It is indicated that the voltage drop in the 10 000th GCD curve originates from the positive electrode. To further confirm this result, the electrode potentials and potential ranges at different cycles were recorded during the long-term cycling, and the detailed potential values were listed in Table 1. With increasing cycling, the positive electrode exhibited a progressive expansion in its operational potential window ( $\Delta E_+$ ), while the negative electrode demonstrated a gradual contraction ( $\Delta E_-$ ). Additionally, the  $E_{\text{max}+}$  and the  $E_{\text{min}-}$  exhibited a gradual increase after long-term cycling. Specifically,  $\Delta E_+$  exhibited a progressive increase from 0.645 V during the initial GCD cycle to 0.880 V following 10 000 cycles, while the  $E_r$  remained relatively stable. Consequently,  $E_{\text{max}+}$  exhibited an increase from 0.085 V during the initial cycle to 0.361 V following 10 000 cycles. The sustained elevation of  $E_{\text{max}+}$  induced severe oxidative decomposition of RHC, resulting in

Table 1 Electrode potentials of positive and negative electrodes in symmetric supercapacitor during 10 000 GCD cycles

Cycle number	$E_e$ (V)	$E_{\text{max}+}$ (V)	$E_{\text{min}-}$ (V)	$\Delta E_+$ (V)	$\Delta E_-$ (V)
1st cycle	−0.560	0.085	−0.915	0.645	0.355
2000th cycle	−0.550	0.111	−0.889	0.661	0.339
5000th cycle	−0.531	0.140	−0.860	0.681	0.319
10 000th cycle	−0.519	0.361	−0.639	0.880	0.120

a consequential increase in ion diffusion resistance. These findings demonstrate that the poor cycling stability of SCs originates from the continuous elevation of positive electrode potential. Therefore, suppressing the increase in the positive electrode potential during cycling is crucial to enhancing the long-term cycling stability of SCs.

### Strategy of increasing the stability of supercapacitors in KOH electrolyte

To suppress the increase in the positive electrode potential, we analyzed the fundamental energy storage mechanisms of supercapacitors. In such systems, the charge balance principle dictates that the charges stored in the positive and negative electrodes remain equal ( $Q_+ = Q_-$ ). Specifically, the charge stored by each electrode is intrinsically governed by its potential range ( $\Delta E$ ), mass ( $m$ ), and specific capacitance ( $C_s$ ), as expressed by the following relationship:<sup>27</sup>

$$Q = mC_s\Delta E \quad (5)$$

$$m_+C_{s+}\Delta E_+ = m_-C_{s-}\Delta E_- \quad (6)$$

Here,  $m_-$  and  $m_+$  demote the masses of the negative and positive electrodes,  $C_{s+}$  and  $C_{s-}$  represent their respective specific capacitances, and  $\Delta E_+$  and  $\Delta E_-$  are their potential ranges.

When the electrode masses are equal ( $m_+ = m_-$ ), an increase in  $\Delta E_+$  during cycling implies a gradual decline in the positive electrode's specific capacitance. To maintain charge equilibrium, the expansion of  $\Delta E_+$  shifts the maximum positive electrode potential toward higher values. In asymmetric configurations ( $m_+ \neq m_-$ ),  $\Delta E_+$  and  $\Delta E_-$  depend on both the electrodes' specific capacitances and the mass ratio. Thus, regulating the potential ranges (and consequently the positive electrode potential) is achievable by optimizing the  $m_+/m_-$  ratio. Eqn (5) further demonstrates that increasing the positive electrode mass ( $m_+$ ) effectively suppresses the expansion of  $\Delta E_+$ .

To validate this strategy, RHC-based SCs with varying  $m_+/m_-$  ratios (1, 1.25, 1.5, and 2) were subjected to 10 000 GCD cycles at a current density of  $1 \text{ A g}^{-1}$ . As shown in Fig. 3, increasing  $m_+/m_-$  significantly enhances cycling stability. When  $m_+/m_-$  is raised from 1 to 2, capacitance retention increases from 27.9% to 96.4%, demonstrating that optimizing the mass ratio enhances the cycling stability of SC in KOH electrolyte.

To further analyze these results, the potentials of both electrodes were monitored in SCs with varying  $m_+/m_-$  ratios after the initial cycle. As illustrated in Fig. 4a, increasing  $m_+/m_-$  reduces both the  $E_{\text{max}+}$  and the  $E_{\text{min}-}$ , thereby narrowing the  $\Delta E_+$  while expanding that of  $\Delta E_-$ . The detailed potential values at varying  $m_+/m_-$  ratios are summarized in Table 2. When  $m_+/m_-$  increased from 1 to 2,  $E_{\text{max}+}$  decreased from 0.085 V to 0.012 V, and  $\Delta E_+$  decreased from 0.645 V to 0.477 V. These trends confirm that lower  $E_{\text{max}+}$  and narrower  $\Delta E_+$  effectively suppress the rise in positive electrode potential during cycling. Fig. 4b displays the CV curve of RHC, measured within the potential window of −1.2 V to 0.2 V. Notably, the  $\Delta E_+$  range shifts to a more stable region as  $m_+/m_-$  increases from 1 to 2, confining the positive electrode within a safer operational



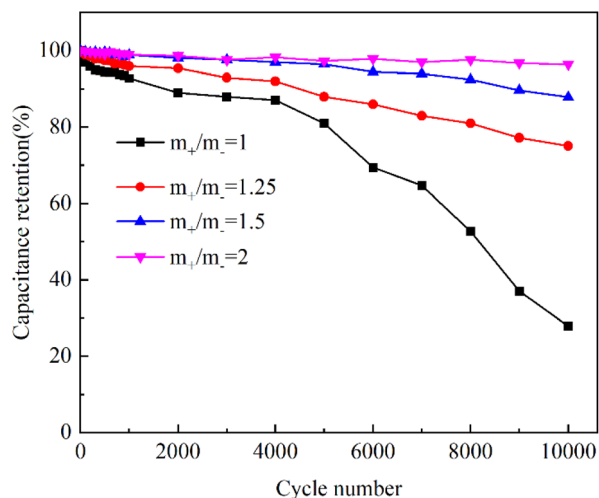


Fig. 3 Long-term cycling stability of SCs with varying  $m_+/m_-$  ratios at  $1 \text{ A g}^{-1}$  for 10 000 cycles.

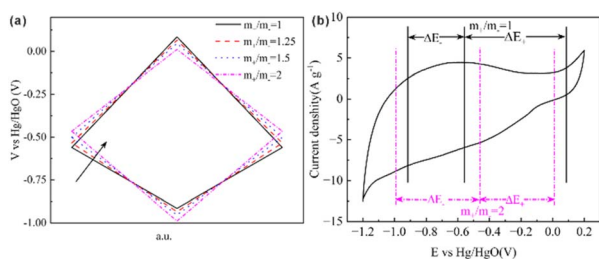


Fig. 4 (a) Evolution of potentials of both electrodes in SCs throughout the GCD testing process; (b) CV curve of RHC in three-electrode cell configuration at a scan rate of  $5 \text{ mV s}^{-1}$ .

Table 2 Electrode potentials of positive and negative electrodes in SCs with varying  $m_+/m_-$  ratios

$m_+/m_-$	$E_e$ (V)	$E_{\text{max}+}$ (V)	$E_{\text{min}-}$ (V)	$\Delta E_+$ (V)	$\Delta E_-$ (V)
1	-0.560	0.085	-0.915	0.645	0.355
1.25	-0.534	0.066	-0.934	0.600	0.400
1.5	-0.500	0.047	-0.953	0.547	0.453
2	-0.465	0.012	-0.988	0.477	0.523

window during charging. This confinement mitigates faradaic degradation caused by excessive potentials, thereby enhancing the stability of electric double-layer capacitance behaviour.

To evaluate long-term effects, potentials of both electrodes in SCs with  $m_+/m_- = 2$  were measured after 1 and 10 000 GCD

Table 3 Electrode potentials of positive and negative electrodes in the SC with  $m_+/m_- = 2$

Cycle number	$E_e$ (V)	$E_{\text{max}+}$ (V)	$E_{\text{min}-}$ (V)	$\Delta E_+$ (V)	$\Delta E_-$ (V)
1st cycle	-0.465	0.012	-0.988	0.477	0.523
10 000th cycle	-0.463	0.020	-0.980	0.483	0.517

cycles (Table 3). The negligible variation in  $E_{\text{max}+}$  confirms that increasing  $m_+/m_-$  effectively stabilizes the positive electrode potential during cycling.

XPS was employed to quantitatively analyze oxygen-containing functional groups on RHC within the positive electrode after cycling in KOH electrolyte. Survey scans (Fig. S2 in the ESI†) and high-resolution O 1s spectra were analyzed. The O 1s XPS spectrum was subjected to Shirley background subtraction and deconvoluted into four distinct chemical states (Fig. 5): adsorbed oxygen ( $530.4 \pm 0.5 \text{ eV}$ ), carbonyl groups  $\text{C}=\text{O}$  ( $531.7 \pm 0.5 \text{ eV}$ ), hydroxyl/ether moieties  $\text{C}-\text{O}-\text{OH}$  ( $532.8 \pm 0.5 \text{ eV}$ ), and carboxyl/ester functionalities  $\text{COOH}/\text{C}(\text{O})\text{O}$  ( $533.6 \pm 0.5 \text{ eV}$ ).<sup>28,29</sup> Notably, the O 1s peak area for RHC in the  $m_+/m_- = 1$  system (Fig. 5b) exceeds that in  $m_+/m_- = 2$  (Fig. 5a), indicating higher oxygen content in the former. Table 4 quantifies oxygen-containing functional groups before and after 10 000 GCD cycles. There is a sharp rise in total oxygen content from 8.54 at% to 21.22 at% for  $m_+/m_- = 1$  after 10 000 GCD cycles, compared to a marginal increase (8.54 at% to 9.12 at%) for  $m_+/m_- = 2$ . These results confirm severe RHC oxidation in the symmetric configuration ( $m_+/m_- = 1$ ), which is effectively suppressed through mass balancing ( $m_+/m_- = 2$ ).

CV was systematically employed to evaluate the electrochemical behaviors of SCs with varying  $m_+/m_-$  ratios in KOH electrolytes. As shown in Fig. 6a, all CV curves exhibit nearly rectangular shapes, characteristic of ideal electric double-layer capacitive behavior, confirming the dominance of non-faradaic charge storage mechanisms in the tested supercapacitors. Indicative of ideal electric double-layer capacitive behavior. The integrated area under the CV curves, which serves as a proxy for specific capacitance, displays a non-monotonic relationship with the  $m_+/m_-$  ratio. The specific capacitance reaches a maximum at  $m_+/m_- = 1.25$  and subsequently decreases as the  $m_+/m_-$  increases further. This indicates a non-monotonic dependence of the specific capacitance on the  $m_+/m_-$  ratio, peaking at an optimal mass ratio before declining with further increases. Meanwhile, the CV curves exhibited increasingly rectangular shapes with increasing  $m_+/m_-$ . Increasing  $m_+/m_-$  may induce shifts in the  $E_e$ ,  $E_+$ , and  $E_-$ . These shifts allow both electrodes to operate within adjusted potential ranges, thereby enhancing their electric double-layer capacitive characteristics through optimized charge distribution at the electrode-electrolyte interfaces.

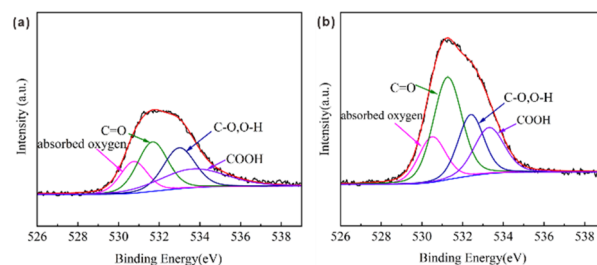


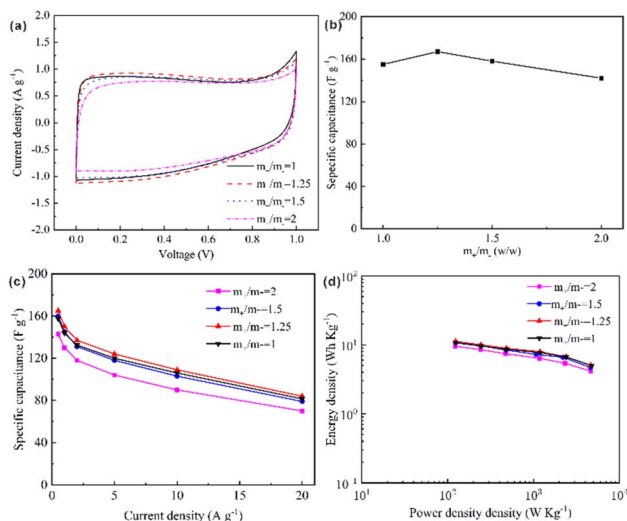
Fig. 5 High-resolution O 1s XPS spectra of RHC electrode in SCs after 10 000 GCD cycles: (a) positive electrode from SCs with  $m_+/m_- = 2$ ; (b) positive electrode from SCs with  $m_+/m_- = 1$ .



**Table 4** Characterization of oxygen-containing functional groups in RHC employed as positive electrode after 10 000 GCD cycles

Samples	Adsorbed oxygen	C=O	C–O, OH	COOH, C(O)O	Total oxygen
RHC <sub>+</sub> (2) <sup>a</sup>	1.38 at%	3.03 at%	2.40 at%	2.31 at%	9.12 at%
RHC <sub>+</sub> (1) <sup>b</sup>	2.26 at%	10.00 at%	4.84 at%	4.12 at%	21.22 at%

<sup>a</sup> The RHC in positive electrode from SCs with  $m_+/m_- = 2$ . <sup>b</sup> The RHC in positive electrode from SCs with  $m_+/m_- = 1$ .



**Fig. 6** (a) CV curves of SCs with varying  $m_+/m_-$  ratios at a scan rate of 5 mV s<sup>-1</sup>; (b) specific capacitance of SCs with varying  $m_+/m_-$  ratios at a scan rate of 5 mV s<sup>-1</sup>; (c) specific capacitance of SCs with varying  $m_+/m_-$  ratios at the different current density; (d) Ragone plots of SCs with varying  $m_+/m_-$  ratios.

Fig. 6b demonstrates the relationship between the specific capacitance of SCs and the  $m_+/m_-$  ratios. At  $m_+/m_- = 1$ , the SC achieves a specific capacitance of 155 F g<sup>-1</sup>. This value increases to a maximum of 167 F g<sup>-1</sup> at  $m_+/m_- = 1.25$ , representing a 7.7% enhancement, followed by a decline to 141 F g<sup>-1</sup> at  $m_+/m_- = 2$ . The specific capacitance of SCs decreased by about 9.1% when  $m_+/m_-$  increased from 1 to 2, which is markedly less severe than 30% capacitance loss observed in thermally treated electrodes.<sup>13</sup> It can be known that enhancing the cycling stability of RHC-based SCs in KOH electrolyte by increasing  $m_+/m_-$  is more effective compared with enhancing it through heat treatment of RHC. This strategy avoids a significant decrease in the specific capacitance of SCs. The specific capacitance of SCs is directly related to the  $m_+/m_-$  ratios and the accompanying change in the  $\Delta E_+$  and  $\Delta E_-$ . At the critical mass ratio where  $\Delta E_+ = \Delta E_-$ , the capacitances of both electrodes equilibrate, as dictated by the charge-balance relationship formalized in eqn (6).

Based on the equation employed for calculating the capacitance of a supercapacitor:<sup>30</sup>

$$\frac{1}{C_T} = \frac{1}{C_P} + \frac{1}{C_N} \quad (7)$$

$C_T$  represents the capacitance of the supercapacitor,  $C_P$  and  $C_N$  represents the capacitances of the positive and negative electrodes, respectively.

Eqn (7) demonstrates that the total capacitance of the SC is maximized when the  $C_P$  and  $C_N$  are equal. This equilibrium condition occurs at a critical mass ratio where  $\Delta E_+ = \Delta E_-$ , the capacitance of the SC reaches its maximum value. As shown in Table 2, increasing  $m_+/m_-$  reduces the  $\Delta E_+$  while expanding that of the  $\Delta E_-$ , thereby driving  $\Delta E_+$  and  $\Delta E_-$  to gradually converge toward equilibrium. This explains why the specific capacitance of SCs initially increases with increasing  $m_+/m_-$ . However, further increases in  $m_+/m_-$  will lead to progressively elevate the total electrode mass, which in turn causes the specific capacitance of SCs to decline. Therefore, the maximum specific capacitance is achieved at  $m_+/m_- = 1.25$ .

Fig. 6c shows the specific capacitance of SCs with varying  $m_+/m_-$  ratios under various current densities. As shown in Fig. 6c, the specific capacitance of SCs at different current densities all exhibits a trend of first increasing and then decreasing with the increase of the  $m_+/m_-$  ratio. All SCs achieve the maximum specific capacitance at  $m_+/m_- = 1.25$ , which is consistent with the results in Fig. 6b. While specific capacitance decreases with increasing current density, the decay profiles remain parallel, indicating that the mass ratio has little effect on the rate performance. The energy-power characteristics of SCs with varying  $m_+/m_-$  ratios were evaluated under different current densities. As illustrated in the Ragone plot (Fig. 6d), the SC with an  $m_+/m_-$  ratio of 1 achieves a high energy density of 10.68 W h kg<sup>-1</sup> at a power density of 124 W kg<sup>-1</sup> under a current density of 0.5 A g<sup>-1</sup>, maintaining 46.8% energy retention (5.0 W h kg<sup>-1</sup>) at 20 A g<sup>-1</sup> with a corresponding power density of 4737 W kg<sup>-1</sup>. Comparatively, the SC with  $m_+/m_- = 2$  delivers an energy density of 9.54 W h kg<sup>-1</sup> at 122 W kg<sup>-1</sup> under 0.5 A g<sup>-1</sup>, retaining 43.4% energy density (4.14 W h kg<sup>-1</sup>) at a power density of 4662 W kg<sup>-1</sup> with the current density of 20 A g<sup>-1</sup>. These results indicate that the adjustment of the  $m_+/m_-$  does not significantly alter the energy-power characteristics of the device.

The Nyquist plots of the SCs in Fig. 7a exhibit characteristic electrochemical impedance features. At high frequencies (inset in Fig. 7a), a small semicircle is observed, with its diameter along the real axis corresponding to the charge-transfer resistance ( $R_{ct}$ ).<sup>31</sup> The equivalent series resistance (ESR), derived from the high-frequency intercept of the Nyquist plot's semicircle on the real axis,<sup>32,33</sup> arises from the summation of three primary contributors: electronic resistance of the porous electrode matrix, interfacial contact resistance between the electrode and current collector, and ionic transfer resistance in the electrolyte.<sup>34,35</sup> Notably, the ESR values show minimal variation across different  $m_+/m_-$  ratios, increasing only marginally from 0.08  $\Omega$  ( $m_+/m_- = 1$ ) to 0.10  $\Omega$  ( $m_+/m_- = 2$ ). This is likely due to



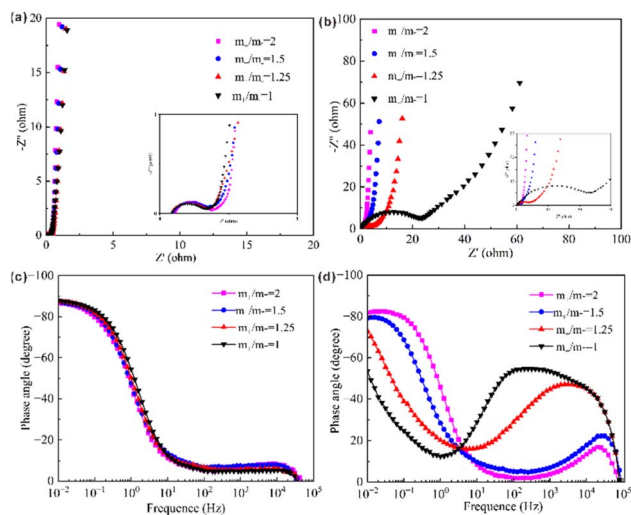


Fig. 7 Nyquist Plots of SCs with varying  $m_+/m_-$  ratios at 1st cycle (a) and 10 000th cycle (b); Bode plots of SCs with varying  $m_+/m_-$  ratios at 1st cycle (c) and 10 000th cycle (d).

increased electrode thickness at higher  $m_+/m_-$  ratios, which marginally elevates ionic diffusion pathways.<sup>36</sup> In the medium-to-low frequency range, the Nyquist plots gradually transition to near-vertical lines, with the low-frequency region approaching a  $90^\circ$  phase angle relative to the real axis. This indicates that the electrode exhibits ideal capacitive behavior.<sup>31</sup> This finding corroborates the nearly rectangular cyclic voltammograms in Fig. 6a, confirming minimal diffusion limitations and efficient ion transport kinetics even at elevated  $m_+/m_-$ . Simultaneously, the remarkably low resistance values obtained under mass-balancing strategies in this research stand in favorable contrast to the results previously reported in other papers.<sup>37–40</sup> These results highlight the viability of optimizing  $m_+/m_-$  to enhance capacitance without sacrificing the kinetic advantages critical for high-power applications. As shown in Fig. 7b, the diameter of the semicircle in the Nyquist plot gradually decreases with the increase of the  $m_+/m_-$  ratios, indicating a progressive decline in  $R_{ct}$  of the SCs. Meanwhile, as depicted in Fig. 7b, the length of sloping linear region with an approximate angle of  $45^\circ$  observed in the high-to-medium frequency range of Nyquist plot decrease with the increase of the  $m_+/m_-$  ratios. This decrease is indicative of a progressive decline in the diffusion resistance the SCs.<sup>41,42</sup> These phenomena demonstrate that increasing the  $m_+/m_-$  ratios inhibits the rise in positive electrode potential and suppresses the formation of oxygen-containing functional groups arising from oxidative degradation, thereby reducing the resistance to electron transfer from the inner carbon layer to the pore interface and accelerating the diffusion process for ions inside pores. This suppression leads to a reduction in the charge-transfer resistance at the interface between the inner carbon layer and the pore, as electrons can move more freely without being hindered by these oxygen-containing functional groups. Additionally, it accelerates the ion diffusion process within the pores. The presence of fewer oxygen-containing functional groups allows ions to diffuse

more efficiently through the pore structure of the electrode material. To further evaluate the influence of the  $m_+/m_-$  ratios on the cycle life of SCs, Bode phase angle analysis was performed pre- and post-cycling (Fig. 7c and d). Fig. 7c shows the relationship between the phase angle and frequency of SCs with varying  $m_+/m_-$  ratios at 1st cycle. It is observed that all curves exhibit no obvious differences as the  $m_+/m_-$  ratios increase. Additionally, the phase angles of these SCs approach approximately  $-90^\circ$  at low frequencies, confirming their ideal capacitive behavior. This further suggests that increasing the  $m_+/m_-$  ratios does not significantly impact the capacitive performance of SCs, which is consistent with Fig. 7a. On the contrary, the Bode plots of SCs with varying  $m_+/m_-$  ratios show obvious changes after 10 000 cycles (Fig. 7d). In the low-frequency region, the phase angle of SCs with a high  $m_+/m_-$  ratio (e.g.,  $m_+/m_- = 2$ ) still approaches  $-90^\circ$  after 10 000 cycle, while that of SCs with a low  $m_+/m_-$  ratio (e.g.,  $m_+/m_- = 1$ ) deviates significantly. This indicates that increasing the  $m_+/m_-$  ratio effectively enhances the capacitive performance of SCs after cycling. Furthermore, it confirms that the positive electrode of SCs with a high mass ratio undergoes no obvious oxidation and maintains superior ion transfer capability, consistent with the results in Fig. 7b.

To further investigate oxidative degradation mechanisms in positive electrodes, morphological analyses were conducted on RHC electrodes from SCs with varying  $m_+/m_-$  ratios after 10 000 GCD cycles. Fig. 8 reveals progressive surface roughening of RHC with increasing  $m_+/m_-$ , attributable to chemical etching by electrogenerated active oxygen species or gas evolution at the carbon–electrolyte interface.<sup>43,44</sup> This morphological evolution indicates that low  $m_+/m_-$  ratios induce severe oxidative damage, while elevated ratios effectively mitigate oxidation through operational potential confinement. TEM was used for further microscopic morphology analysis of RHC, and the results are shown in Fig. S4 (in the ESI).† TEM analysis of positive electrodes from low  $m_+/m_-$  configurations reveals distinct alternating bright/dark contrast regions (Fig. S4c and d†), indicative

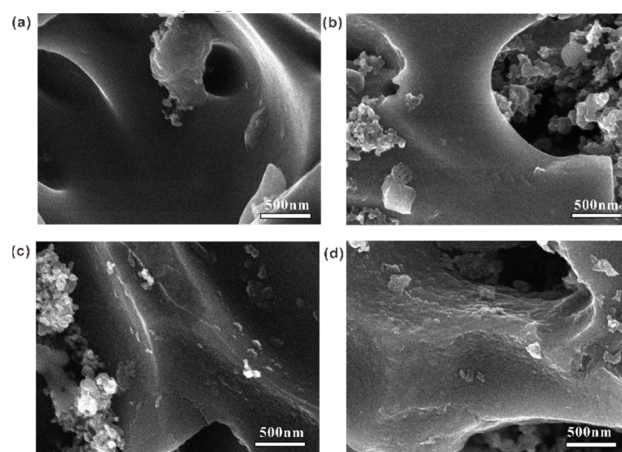


Fig. 8 SEM images of RHC in the positive electrode of SCs with varying  $m_+/m_-$  ratios at 2 (a), 1.5 (b), 1.25 (c), 1 (d) after 10 000 GCD cycles.





of heterogeneous surface degradation and pore wall collapse. This structural deterioration corresponds directly with the progressive roughening observed *via* SEM in Fig. 8, confirming oxidative damage at the nanoscale. Conversely, positive electrodes from high  $m_+/m_-$  configurations (Fig. S4a and b†) retain structural homogeneity, confirming that mass-balancing suppresses corrosive interfacial reactions.

To evaluate the effectiveness of the mass-balance strategy in the practical application of SCs, the rate capabilities of individual positive and negative electrodes were quantified within their operational potential windows. As shown in Fig. S3 (in the ESI),† both electrodes exhibit nearly identical capacitance retention profiles across current densities ( $0.5\text{--}20\text{ A g}^{-1}$ ), with <7% divergence in retention rates at all  $m_+/m_-$  ratios. This confirms that all positive and negative electrodes in SCs exhibit similar rate capabilities, indicating that the mass balance strategy does not fail during the practical operation of SCs (Detailed analysis is provided in the ESI†).

Based on the above research findings, it is evident that increasing the  $m_+/m_-$  ratios is a more effective approach for enhancing the cycling stability of RHC-based SCs in KOH electrolyte. This strategy is simple to operate and easy to implement. More importantly, the SCs still maintain excellent electrochemical performance through the mass-balancing strategy.

## Conclusions

This study systematically investigates the cycling stability and electrochemical performance of SCs employing RHC electrodes with varied mass ratios in 6 mol per L KOH electrolyte. SCs assembled with different mass loading ( $m_+/m_- = 1, 1.25, 1.5, 2$ ) demonstrate that increasing  $m_+/m_-$  effectively mitigates the rise of the positive electrode potential during GCD cycles, thereby suppressing oxidative degradation (Fig. 9). At  $m_+/m_- = 2$ , the  $E_{\text{max}+}$  stabilizes at 0.020 V after 10 000 cycles, which is much lower than 0.354 V observed at  $m_+/m_- = 1$ . This suppression correlates with reduced oxygen content in the positive electrode (9.12 at% *vs.* 21.22 at% for  $m_+/m_- = 2$  and 1, respectively).

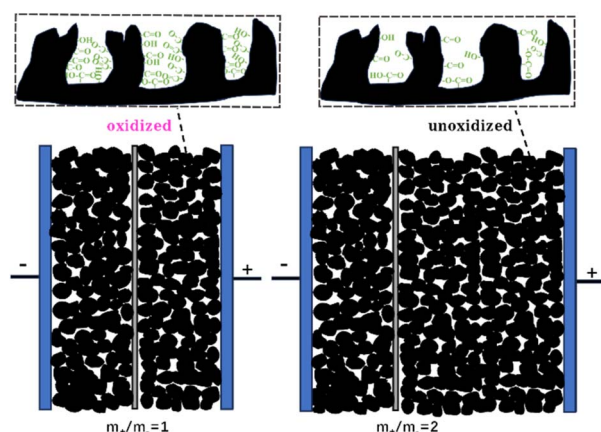


Fig. 9 Schematic of the mass-balancing strategy for suppressing the oxidation of the positive electrode.

Consequently, the SC with  $m_+/m_- = 2$  achieves excellent cycling stability (96.4% capacitance retention), starkly contrasting with the rapid degradation of the symmetric  $m_+/m_- = 1$  system (27.9% capacitance retention). Although the SC with an  $m_+/m_-$  ratio of 1.25 exhibits the highest initial specific capacitance ( $167\text{ F g}^{-1}$ ), the SC with an  $m_+/m_-$  ratio of 2 prioritizes long-term stability without sacrificing performance ( $141\text{ F g}^{-1}$ ). The SC with  $m_+/m_-$  ratios of 1 and 2 shows energy densities of  $10.68\text{ W h kg}^{-1}$  and  $9.54\text{ W h kg}^{-1}$  at  $0.5\text{ A g}^{-1}$ , retaining 46.8% and 43.4% of energy densities at  $20\text{ A g}^{-1}$ . Adjusting the  $m_+/m_-$  does not significantly alter the energy-power characteristics of the device. These findings establish electrode mass balancing as a critical strategy for enhancing the cycling stability of RHC-based SCs in alkaline electrolytes. Through adjusting the  $m_+/m_-$ , the positive electrode potential can be effectively restricted within a stable potential window. This confinement effectively suppresses the oxidation of activated carbon, which maintains the long-term performance of the RHC-based SCs. Meanwhile, the mass-balancing strategy avoids the application of energy-intensive post-treatment procedures (*e.g.*, thermal annealing) and provides a path that can be scaled up for the production of durable and high-performance AC-based SCs.

## Data availability

All data related to this work is presented in the manuscript and the ESI.†

## Author contributions

Dechen Liu: writing – original draft, visualization, methodology, formal analysis, and data curation; Wenli Zhang: investigation, methodology, writing – review & editing; Haibo Lin: supervision and project administration; Nan Lin: funding acquisition, writing – review & editing.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work was supported by the National Natural Science Foundation of China (No. 22279042), the 14th Five-Year Plan Science and Technology Project of the Ministry of Education of Jilin Province (No. JJKH20231084KJ), the Scientific Research Projects of Jilin Police College (No. jkyz202504).

## References

- 1 D. R. Lobato-Peralta, P. U. Okoye and C. Alegre, *J. Power Sources*, 2024, **617**, 235140.
- 2 Y. Wang, L. Zhang, H. Hou, W. Xu, G. Duan, S. He, K. Liu and S. Jiang, *J. Mater. Sci.*, 2021, **56**, 173–200.
- 3 W. Fan, F. Wang, X. Xiong, B. Song, T. Wang, X. Cheng, Z. Zhu, J. He, Y. Liu and Y. Wu, *NPG Asia Mater.*, 2024, **16**, 18.





- 4 H. Hu, M. Yan, J. Jiang, A. Huang, S. Cai, L. Lan and Y. Zhao, *Sci. Total Environ.*, 2024, **912**, 169141.
- 5 Z. Zhai, L. Zhang, T. Du, B. Ren, Y. Xu, S. Wang and Z. Liu, *Mater. Des.*, 2022, **221**, 111017.
- 6 B. Chen, D. Wu, T. Wang, F. Yuan and D. Jia, *Chem. Eng. J.*, 2023, **462**, 142163.
- 7 Y. Yin, Q. Liu, Y. Zhao, T. Chen, J. Wang, L. Gui and C. Lu, *Energy Fuels*, 2023, **37**, 3523–3554.
- 8 B. Xue, J. Xu and R. Xiao, *Chem. Eng. J.*, 2023, **454**, 140192.
- 9 S. Lv, L. Ma, X. Shen and H. Tong, *J. Mater. Sci.*, 2021, **56**, 1919–1942.
- 10 D. Liu, W. Zhang, H. Lin, Y. Li, H. Lu and Y. Wang, *RSC Adv.*, 2015, **5**, 19294–19300.
- 11 D. Liu, W. Zhang and W. Huang, *Chem. Lett.*, 2019, **30**, 1315–1319.
- 12 J. Castro-Gutiérrez, R. L. Canevesi, M. Emo, M. T. Izquierdo, A. Celzard and V. Fierro, *Renewable Sustainable Energy Rev.*, 2022, **167**, 112716.
- 13 P. Kurzweil, J. Schottenbauer and C. Schell, *J. Energy Storage*, 2021, **35**, 102311.
- 14 C. Qiu, L. Jiang, Y. Gao and L. Sheng, *Mater. Des.*, 2023, **230**, 111952.
- 15 W. Zhang, D. Liu, H. Lin, H. Lu, J. Xu and D. Liu, *Colloids Surf., A*, 2016, **511**, 294–302.
- 16 E. Pamaté, L. Köps, F. A. Kreth, S. Pohlmann, A. Varzi, T. Brousse and V. Presser, *Adv. Energy Mater.*, 2023, **13**, 2301008.
- 17 J. Zhao, S. Yang, P. Zhang and S. Dai, *Fuel*, 2021, **286**, 119393.
- 18 X. Tao, Y. Li, H. G. Wang, X. Lv, Y. Li, D. Xu, Y. Jiang and Y. Meng, *J. Colloid Interface Sci.*, 2020, **565**, 494–502.
- 19 X. Wei, D. Zheng, M. Zhao, H. Chen, X. Fan, B. Gao, L. Gu, Y. Guo, J. Qin, J. Wei and Y. Zhao, *Angew. Chem.*, 2020, **132**, 14747–14754.
- 20 F. Liu, F. Zhang and J. Niu, *RSC Adv.*, 2025, **15**, 2582–2590.
- 21 H. Boulrika, M. Hajamab, M. Hajji Nabih, N. Idrissi Kandri and A. Zerouale, *RSC Adv.*, 2022, **12**, 34393–34403.
- 22 Y. Liu, R. Withers and L. Norén, *Solid State Sci.*, 2003, **5**, 427–434.
- 23 C. E. Sánchez-Rodríguez, E. Tovar-Martínez and R. López-Sandoval, *Electrochim. Acta*, 2024, **507**, 145151.
- 24 Y. Li, J. Mei, L. Wu, Q. Xu and Z. Li, *Int. J. Hydrogen Energy*, 2024, **49**, 67–80.
- 25 Y. Zhu, Z. Li, Y. Tao, J. Zhou and H. Zhang, *J. Energy Storage*, 2022, **47**, 103624.
- 26 J. Wan, T. Lv, Y. Liu, X. Wang, Y. Yang, Z. Chen and T. Chen, *Adv. Funct. Mater.*, 2022, **32**, 2108794.
- 27 N. R. Chodankar, H. D. Pham, A. K. Nanjundan, J. F. Fernando, K. Jayaramulu, D. Golberg and D. P. Dubal, *Small*, 2020, **16**, 2002806.
- 28 S. Bhartiya, R. Singh, A. Singh, M. Balal, P. Bhardwaj, D. K. Kohli and M. K. Singh, *J. Solid State Electrochem.*, 2022, **26**, 2829–2839.
- 29 F. Rao, Q. Xiao, Y. Wei, J. Wang, R. Yu and D. Wang, *Chem. Res. Chin. Univ.*, 2024, **40**, 690–698.
- 30 Y. Shao, M. F. El-Kady, J. Sun, Y. Li, Q. Zhang, M. Zhu and R. B. Kaner, *Chem. Rev.*, 2018, **118**, 9233–9280.
- 31 M. Li, C. Liu, H. Cao, H. Zhao, Y. Zhang and Z. Fan, *J. Mater. Chem. A*, 2014, **2**, 14844–14851.
- 32 X. F. Sánchez-Romate, A. Del Bosque, J. Artigas-Arnaud, B. K. Muñoz, M. Sánchez and A. Ureña, *Electrochim. Acta*, 2021, **370**, 137746.
- 33 L. E. Helseth, *J. Energy Storage*, 2021, **35**, 102304.
- 34 F. Yang, J. Chu, Y. Cheng, J. Gong, X. Wang and S. Xiong, *Chem. Res. Chin. Univ.*, 2021, **37**, 772–777.
- 35 P. Mehra, C. Singh, I. Cherian, A. Giri and A. Paul, *ACS Appl. Energy Mater.*, 2021, **4**, 4416–4427.
- 36 E. G. Calvo, F. Lufrano, A. Arenillas, A. Brigandí, J. A. Menéndez and P. Staiti, *J. Appl. Electrochem.*, 2014, **44**, 481–489.
- 37 J. Cheng, Z. Lu, X. Zhao, X. Chen and Y. Liu, *J. Power Sources*, 2021, **494**, 229770.
- 38 J. K. Ou, H. W. Zhang, Y. Lei, K. Y. Li, B. Li, H. X. Deng and L. Zou, *J. Cent. South Univ.*, 2023, **30**, 419–433.
- 39 X. Pang, M. Cao, J. Qin, X. Li and X. Yang, *J. Porous Mater.*, 2022, **29**, 559–569.
- 40 S. M. Benoy, A. Hazarika, M. Bora, A. Rajbongshi, D. Sarmah, M. K. Phukan and B. K. Saikia, *ACS Appl. Energy Mater.*, 2024, **7**, 6045–6061.
- 41 A. J. Roberts and R. C. Slade, *Electrochim. Acta*, 2010, **55**, 7460–7469.
- 42 S. Sopčić, D. Antonić and Z. Mandić, *J. Solid State Electrochem.*, 2022, **26**, 591–605.
- 43 G. Milczarek, A. Ciszewski and I. Stepniak, *J. Power Sources*, 2011, **196**, 7882–7885.
- 44 T. Momma, X. Liu, T. Osaka, Y. Ushio and Y. Sawada, *J. Power Sources*, 1996, **60**, 249–253.

