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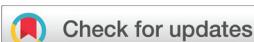


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Enhanced electrocatalytic hydrogen evolution with bimetallic Ru/Pt nanoparticles supported on nitrogen-doped reduced graphene oxide[†]

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The electrocatalytic hydrogen evolution reaction (HER) has been explored using mono- and bimetallic Pt–Ru nanoparticles (NPs) deposited onto nitrogen-doped reduced graphene oxide (NH₂-rGO) in acidic media. In this contribution, monometallic and bimetallic nanoparticles with three different Pt/Ru ratios (1/5, 1/1, and 5/1) have been used, yielding five different materials denoted as Pt_xRu_y@NH₂-rGO (x = 0, y = 1; x = 1, y = 0; x = 1, y = 5; x = 1, y = 1; x = 5, y = 1). The materials were characterized using a variety of state-of-the-art techniques, including high-angle annular dark field scanning transmission electron microscopy (HAADF-STEM), energy dispersive X-Ray spectroscopy (EDX) and X-Ray absorption spectroscopy (XAS), enabling the investigation of differences in morphology, coordination environment and oxidation state as a function of the metal composition of the graphene-supported NPs. The materials exhibited HER activity and demonstrated competitive overpotentials close to the thermodynamic limit. The initial catalytic activity of the as-synthesized materials enhances as the Pt/Ru ratio increases. Chronopotentiometry cathodic experiments showed that under reductive conditions the electrocatalytic performance is drastically impacted. Ru-rich materials were activated, whereas Pt-rich materials showed poor stability. Upon applying a reducing potential for 58 h, Pt₁Ru₅@NH₂-rGO reached the best catalytic activity with outstanding overpotentials of $\eta_0 = 0$ mV and $\eta_{10} = 3$ mV and no signs of deactivation even after 12 additional hours of electrolysis. According to DFT calculations, all nanoparticles present surface sites whose hydrogen adsorption energy is optimal for HER. In agreement with the experimental data, the Pt₁Ru₅ model shows the highest number of highly active sites, especially those involving Ru centres close to the Pt–Ru interface. Combining in-depth characterization and computational modelling, this work reveals that the synergy between the two metals, structural features, and their affinity for the support are responsible for the observed differences in catalytic activities and stabilities.

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Introduction

Molecular hydrogen, a zero-emissions fuel when burned and an excellent reservoir of excess green electricity to be fed in fuel cells, is a promising energy vector expected to have a key role in the energy transition and the mitigation of climate change.^{1–3} Unfortunately, most of the hydrogen produced in large scale nowadays is “grey hydrogen”, produced from gasification or reforming of fossil fuels, which is associated with CO₂ emissions. On the contrary, “green hydrogen” produced using renewable electricity and water needs further development.⁴ The overall water-splitting reaction consists of two half-reactions, called oxygen evolution reaction (OER) and hydrogen evolution reaction (HER). These half-reactions are thermodynamically and kinetically challenging. Sunlight can provide



the energy needed to overcome the thermodynamics, but the use of catalysts is required to overcome the kinetics. Focusing on HER, much effort has been devoted in recent years to the development of efficient electrocatalysts. Among all the reported heterogeneous HER catalysts, Pt catalysts are the most efficient ones due to the optimal Gibbs free energy of hydride absorption (ΔG_H) associated with the Pt–H bond: it is neither too weak nor too strong, allowing for efficient hydrogen activation and subsequent H_2 desorption.^{5,6} However, the corrosion of the Pt catalyst at neutral/alkaline conditions, together with its scarcity and high price, has limited its large-scale commercial application.⁷ One way to reduce the amount of material used is to maximize the active catalytic surface by using nanoparticles (NPs). In this respect, Ru NPs with Ru–H bond energies similar to those of Pt–H have recently emerged as promising candidates, demonstrating excellent activity in HER and displaying exceptional stability in both acidic and basic environments.^{8–15} One possibility is to use Pt in combination with other elements, such as Ru,^{11,16–19} as the use of bimetallic nanomaterials has often benefits in catalysis by synergistic effects between metals.^{16–18} For example, some authors have found that Ru combined with Pt solves the corrosion degradation problem of Pt in neutral and basic pH while boosting the activity to overpotentials ranging from 6 to 36 mV. This demonstrates that combining Ru and Pt is a promising strategy for achieving efficient and durable HER electrocatalysts across a wide range of pHs.¹⁸ However, these studies do not deeply analyse the atomic structure arrangements, precluding the rational design of catalysts.

Different types of bimetallic NPs can be produced depending on the synthetic protocol (Fig. 1), namely alloys, intermetallic, Janus-type or core–shell, with the prevalence of each type being governed by factors such as the metal precursors used and/or the reaction conditions applied.^{20–23} The preparation of core–shell systems can be relatively straightforward, mainly based on different decomposition rates of the metal precursors.^{24–26} However, preparing bimetallic nanostructured alloys based on transition metals while maintaining a small particle size is a difficult task. Formation of the intermetallic phases normally needs high temperatures, which can easily lead to the aggregation of the bimetallic NPs.²⁷ Various bimetallic nanoparticles have been obtained by the organometallic approach,²⁸ a wet process consisting of the hydrogenation of organometallic precursors under mild conditions.

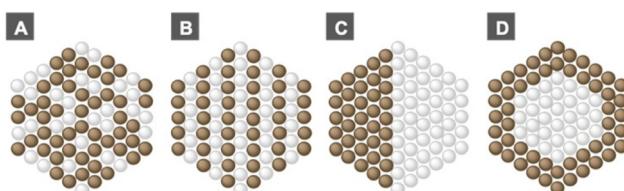


Fig. 1 Types of bimetallic NPs: (A) alloyed, (B) intermetallic, (C) Janus, and (D) core–shell structure. Yellow and grey spheres represent two different metal atoms.

Examples include RuPt bimetallic nanoparticles used for many different catalytic reactions, as this method allows fine-tuning and clean nanoparticle surface.^{26,29,30} As stated before, the choice of the metal precursor is crucial in the structure arrangement of the nanoparticles.³¹

In order to prevent the aggregation of the NPs under turnover conditions and to improve the charge transfer capability between nanocatalysts and the electrode (which in turn increases the conductivity), solid supports are commonly used.^{10,18} In this regard, conductive supports have been extensively employed to stabilize NPs.^{32–35} Due to its excellent electronic conductivity (as high as 103 S cm^{-1}) and extremely high surface area ($300\text{--}700\text{ m}^2\text{ g}^{-1}$), reduced graphene oxide (rGO) has become an ideal support for electrocatalysts.^{36,37} The presence of oxygen-containing functional groups and defects in rGO facilitates the stabilization of metal NPs on its surface. In addition, rGO can be easily doped with heteroatoms such as nitrogen, introducing new active sites and enhancing the electron-transfer properties of the graphene support.^{7,32,38} For example, it has been recently demonstrated that doping carbon supports with heteroatoms like N and P boost the catalytic performance, reaching such low overpotentials as 2 mV after activation of the Ru NPs on phosphorous-doped reduced graphene oxide.³⁸

The aim of this work is to analyse the effect of different Pt/Ru ratios on the HER electrocatalytic activity of ultrafine bimetallic NPs on nitrogen-doped reduced graphene oxide (NH_2 -rGO) prepared by the organometallic approach.³⁹ As the structural atomic organization of the nanoparticles is often limited by the analysis techniques, HAADF-STEM, EDX and XAS have been used to determine the chemical composition and the structure of the initial bimetallic NPs as well as their post-catalytic outcome. Additionally, DFT calculations have been performed to gain atomistic insight into the nanomaterials' catalytic activity.

Results and discussion

The catalysts used in this contribution have been prepared through the organometallic approach, following the synthetic procedure some of us described in a previous publication.³⁹ They consist of mono- and bimetallic ligand-free Pt and/or Ru NPs supported on nitrogen-doped reduced graphene oxide (NH_2 -rGO), namely $Ru@NH_2$ -rGO, $Pt@NH_2$ -rGO, $Pt_1Ru_5@NH_2$ -rGO, $Pt_1Ru_1@NH_2$ -rGO and $Pt_5Ru_1@NH_2$ -rGO. The metal content reported for the mono- and bimetallic supported-NPs, determined by inductively coupled plasma (ICP) and X-ray fluorescence (XRF) analyses, is close to 3 wt%. Furthermore, $Pt_xRu_y@NH_2$ -rGO catalysts presented particle sizes between 1.6 and 2.1 nm (see TEM micrographs and corresponding size histograms in Fig. S1†), and were characterized by high-resolution transmission electron microscopy (HR-TEM), Raman spectroscopy, and X-ray photoelectron spectroscopy (XPS).³⁹ In this work, the bimetallic systems were additionally characterized by point-by-point high-angle annular dark-field scanning trans-



mission electron microscopy coupled with Energy-Dispersive X-ray spectroscopy (HAADF-STEM EDX) (Fig. 2) as well as synchrotron X-ray absorption spectroscopy (XAS), including both X-ray absorption near the edge structure (XANES) and extended X-ray absorption fine structure (EXAFS).

Bimetallic materials characterization

The presence of both metals in the HAADF-STEM EDX spectra for individual particles confirms the bimetallic nature of the nanoparticles (Fig. 2). However, Pt/Ru ratios that significantly deviate from the expected values, such as $\text{Pt}_1\text{Ru}_{99}$ or $\text{Pt}_{95}\text{Ru}_5$ for $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$ and $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$, were also observed (Fig. 2b and c), indicating partial segregation of the bimetallic NPs. The available EDX data for such small nanoparticles did not allow us to fully distinguish between nanoalloys or partially segregated metal clusters on individual nanoparticles due to the limitation of the technique.^{27,40,41} However, XAS data presented below coupled with this EDX structural information, support the (at least partial) metal segregation, especially for $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$, without excluding alloyed structure to some extent.

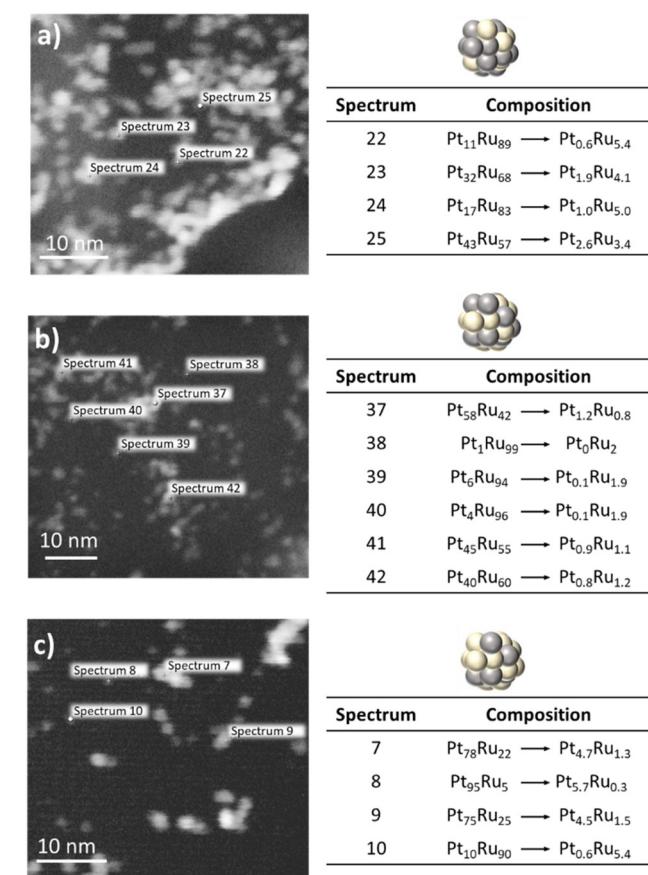


Fig. 2 TEM and HRTEM micrographs with the corresponding size distribution and HAADF-STEM images with the relative composition determined by EDX of (a), $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ (b), $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$ (c) and $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$.

According to the structural features given by electron diffraction patterns of nanoparticles, the dominant structure of all nanocatalysts was obtained. Specifically, Ru-rich catalysts, such as $\text{Ru}@\text{NH}_2\text{-rGO}$ and $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$, exhibited a hexagonal close-packed (hcp) structure, whereas Pt-rich catalysts ($\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$, $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$ and $\text{Pt}@\text{NH}_2\text{-rGO}$) presented a face-centered cubic (fcc) structure.³⁹ Moreover, the metal oxidation state and coordination environments were obtained by XANES and FT-EXAFS analysis fitting (shown in Fig. 3, S3, S4, S5, S6† and Table 1). In this way, it was possible to determine the fine structural composition of the nanoparticles. $\text{Pt}@\text{NH}_2\text{-rGO}$ exhibits an fcc structure and contains only metallic Pt. On the other hand, $\text{Ru}@\text{NH}_2\text{-rGO}$ exhibits an hcp structure, and a mixture of Ru^0 , Ru^{III} and Ru^{IV} oxidation states. It has an average Ru–Ru coordination number (C.N.) of 8.82 (1.66), and an average Ru–O C.N. of 5.03 (0.80). Knowing that the maximum coordination number of a bulk hcp structure is 12, these data suggest the presence of partially oxidized Ru NPs (*i.e.*, Ru^0 core with a RuO_x shell), as previously observed for other Ru systems.^{9–13}

Concerning bimetallic nanoparticles, $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ is the only Pt-containing system that retains the typical hcp crystal structure of Ruthenium. Pt_1Ru_5 -catalyst mainly contains metallic Ru and Pt, with an average Ru–Ru C.N. of 7.84 (1.66), and an average Pt–Pt C.N. of 4.99 (0.32). However, Ru–Pt (with

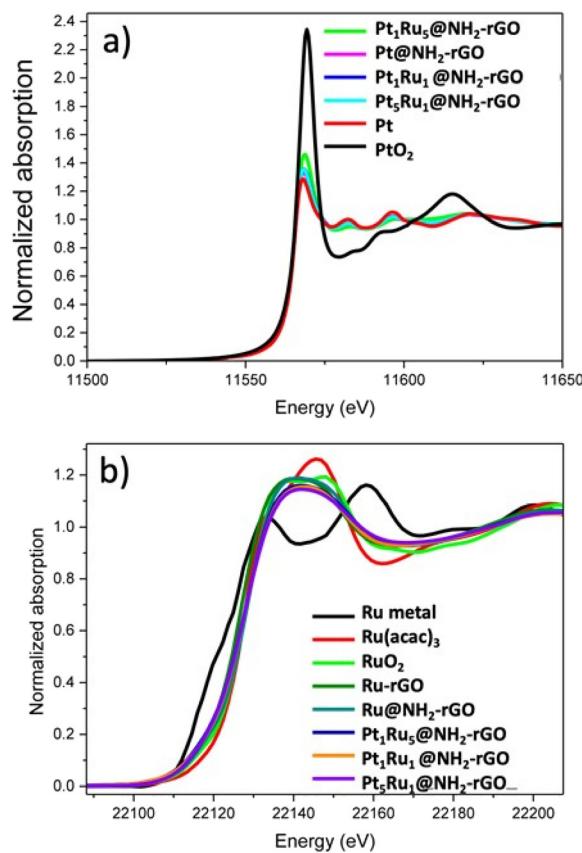


Fig. 3 XANES spectra of investigated $\text{Pt}_x\text{Ru}_y@\text{NH}_2\text{-rGO}$ (a, Pt L3 edge; b, Ru K edge).



Table 1 Summary of EXAFS and XANES data for all as-prepared nanomaterials discussed on this work

Catalyst	Ru : Pt	Cryst. struct.	Oxidation state (%)				Coordination number						
			Ru ⁰	Ru ^{III}	Ru ^{IV}	Pt ⁰	Pt ^{IV}	Ru–Ru	Ru–Pt	Ru–O	Pt–Pt	Pt–Ru	Pt–O
Ru@NH ₂ -rGO	—	hcp	11.2 (4.9)	24.1 (9.3)	64.7 (5.4)	—	—	8.82 (1.66)	—	5.03 (0.80)	—	—	—
Pt ₁ Ru ₅ @NH ₂ -rGO	5 : 1	hcp	23.2 (3.3)	21.2 (8.4)	55.6 (9.4)	81.3 (3.5)	18.7 (2.9)	7.84 (1.66)	1.72 (1.55)	4.82 (0.95)	4.99 (0.32)	0.51 (0.18)	6.22 (0.58)
Pt ₁ Ru ₁ @NH ₂ -rGO	1 : 1	fcc	21.8 (4.8)	25.8 (8.3)	52.3 (6.5)	91.3 (1.9)	8.7 (2.3)	7.12 (1.77)	3.41 (2.11)	5.07 (0.72)	9.12 (0.61)	0.21 (0.18)	—
Pt ₅ Ru ₁ @NH ₂ -rGO	1 : 5	fcc	21.3 (7.7)	7.7 (8.5)	71.0 (7.2)	91.8 (2.9)	8.2 (2.4)	8.14 (1.77)	3.18 (1.98)	5.04 (0.66)	8.72 (0.44)	0.14 (0.09)	—
Pt@NH ₂ -rGO	—	fcc	—	—	—	93.3 (2.9)	6.7 (2.5)	—	—	—	9.18 (0.54)	—	—

a C.N. of 1.72 (1.55)) and Pt–Ru bonding (with a C.N. of 0.51 (0.18)) can also be observed. Surprisingly, Pt–O bonding (with an average coordination number of 6.22 (0.58)) was observed only in this system and not in the other Pt-containing nanoparticles. These results indicate that Pt is mostly located on the surface of these Pt-deficient NPs. This could be related to the fact that **Pt₁Ru₅@NH₂-rGO** is the only Pt-containing system that shows the hcp crystal structure. This unusual crystal structure of Pt seems to influence its reactivity towards oxidation.⁴² Thus, it can be suggested that the formation of the hcp-structured Pt in the Ru crystal structures may result in compressive strain throughout the structure to accommodate the interfacial lattice mismatch, thereby altering the surface reactivity (see DFT results below).

On the other hand, **Pt₁Ru₁@NH₂-rGO** and **Pt₅Ru₁@NH₂-rGO** show Ru–O bonding and high Ru–Ru C.N. This feature indicates that Ru is likely present at the surface of the nanoparticles and that it is partially oxidized, commonly observed in Ru nanoparticles.¹⁰ These Pt-rich samples show the typical fcc structure for Pt and there is no evidence of Pt oxidation.

The Ru–Pt C.N. (3.18 (1.98) for **Pt₁Ru₁@NH₂-rGO**; 3.41 (2.11) for **Pt₅Ru₁@NH₂-rGO**) and Pt–Pt C.N. (9.12 (0.61) for **Pt₁Ru₁@NH₂-rGO**; 8.72 (0.44) for **Pt₅Ru₁@NH₂-rGO**) are similar for the two compositions and both are higher than for **Pt₁Ru₅@NH₂-rGO** (only 1.72 (1.55) for Ru–Pt and 4.99 (0.32) for Pt–Pt). Pt–Ru C.N. are low in the two Pt-rich samples (0.14 and 0.21, for **Pt₁Ru₁@NH₂-rGO** and **Pt₅Ru₁@NH₂-rGO**, respectively). Such small Ru–Pt C.N., compared to the higher Pt–Pt C.N., seems to indicate that **Pt₁Ru₁@NH₂-rGO** and **Pt₁Ru₅@NH₂-rGO** bimetallic particles are partially core–shell segregated, or sub-cluster segregated, with regions of monometallic Pt, regions of monometallic Ru, Pt–Ru interfaces and limited alloy regions, in agreement with the observations of the point-by-point EDX analysis.

Overall, these results show that **Pt@NH₂-rGO** exhibits an fcc structure with only metallic Pt, while **Ru@NH₂-rGO** exhibits an hcp structure with a mixture of Ru⁰, Ru^{III} and Ru^{IV} oxidation states. **Pt₁Ru₅@NH₂-rGO** retains the hcp structure of Ru, with Pt being partially oxidized and mostly located on the surface of the nanoparticle. In contrast, **Pt₁Ru₁@NH₂-rGO** and **Pt₅Ru₁@NH₂-rGO** display typical fcc–Pt⁰ crystal structures with partial Ru oxidation and possible core–shell or sub-cluster segregation with regions of monometallic Pt or Ru and Pt–Ru interfaces. Different decomposition rates of the metal precursors under hydrogen during the organo-

metallic synthesis could be at the origin of the segregated structures.

Electrocatalytic performance in HER

The as-prepared mono- and bimetallic Pt and/or Ru nanoparticles were tested as catalysts for HER in 1 M H₂SO₄ aqueous solution by drop-casting their dispersion inks onto a glassy carbon rotating disk electrode (GC-RDE). Cathodic linear sweep voltammetry (LSV) tests were first performed in a typical three-electrode configuration (see Experimental section for further details) to reveal the intrinsic behavior of the catalysts. The experimental results are shown in Fig. 4 and Table 2. From the as-prepared materials, all Pt-containing catalysts showed an onset potential (η_0) close to zero. **Pt@NH₂-rGO** requires an overpotential of 12 mV to achieve a current density of -10 mA cm⁻² (η_{10}), outperforming **Pt₅Ru₁@NH₂-rGO** (32 mV), **Pt₁Ru₁@NH₂-rGO** (33 mV), **Pt₁Ru₅@NH₂-rGO** (54 mV) and **Ru@NH₂-rGO** (198 mV) catalysts. These results show a clear trend: increasing Ru loading in the catalysts leads to reduced initial hydrogen evolution activity. Therefore, **Pt@NH₂-rGO** exhibits the best performance among all **Pt_xRu_y@NH₂-rGO** catalysts. The Tafel slope values are 39, 48, 42, and 65 mV dec⁻¹ for **Pt@NH₂-rGO**, **Pt₅Ru₁@NH₂-rGO**, **Pt₁Ru₁@NH₂-rGO**, and **Pt₁Ru₅@NH₂-rGO**, respectively, which indicate a Volmer–Heyrovsky mechanism (see Fig. S9†). In contrast, **Ru@NH₂-rGO** displays the highest Tafel slope value (169 mV dec⁻¹), suggesting that the Volmer step is rate-determining.⁴³

When current-controlled bulk electrolysis at $j = -10$ mA cm⁻² were applied to the mono and bimetallic Pt or/and Ru hybrid materials, their catalytic performances were significantly altered. Higher η_{10} were observed after applying a reductive potential for **Pt@NH₂-rGO**, **Pt₅Ru₁@NH₂-rGO** and **Pt₁Ru₁@NH₂-rGO**, showing continuous deactivation over time by observing decreasing potentials during chronoamperometry experiments (Fig. S12a–c† and Table 2). Deactivation is related to the aggregation of the post-operando Pt-rich catalysts (see below). In contrast, the Ru-rich samples **Pt₁Ru₅@NH₂-rGO** and **Ru@NH₂-rGO** improve their η_{10} over time, reaching up to 3 mV and 20 mV, after 58 h and 5 h of bulk electrolysis, respectively (Fig. 4(c) and Fig. S12d, e†). These η_{10} values are comparable to the best catalysts reported in the literature (see Table S3†).

Moreover, these low overpotentials indicate that, upon reduction, **Pt₁Ru₅@NH₂-rGO** and **Ru@NH₂-rGO** become more active in HER than in their initial state. This behavior has



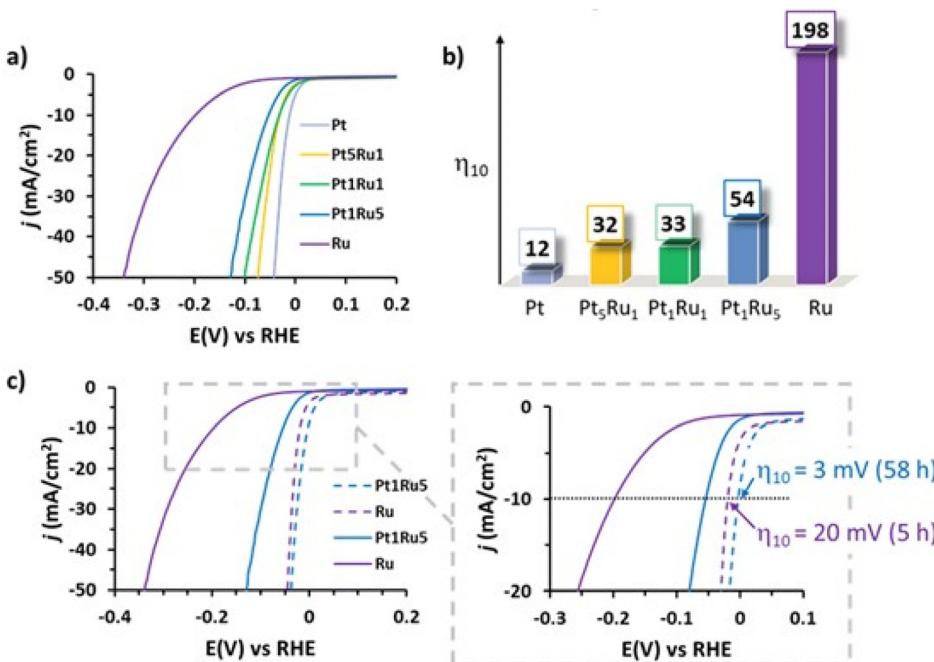


Fig. 4 (a) Linear sweep voltammetry and (b) their corresponding HER benchmarking overpotentials for all the nanomaterials employed in this work at $t = 0$ h. (c) Linear sweep voltammetry of Ru@NH₂-rGO and Pt₁Ru₅@NH₂-rGO as-synthesized (plane line) and upon applying $j = -10 \text{ mA cm}^{-2}$ until reaching an equilibrium for the activation process (dotted line). Experiments were performed in 1 M H_2SO_4 .

Table 2 Onset (η_0) and benchmarking (η_{10}) overpotentials for the HER for all the nanomaterials employed on this work upon applying $j = -10 \text{ mA cm}^{-2}$ at $t = 0$ and at the final state

Material	Time of application of $j = -10 \text{ mA cm}^{-2}$			
	$t = 0$ h		Final state	
	η_0 (mV)	η_{10} (mV)	η_0 (mV)	η_{10} (mV) (time of equilibrium)
Pt@NH ₂ -rGO	0	12	42	Continuous deactivation
Pt ₅ Ru ₁ @NH ₂ -rGO	0	32	4	Continuous deactivation
Pt ₁ Ru ₁ @NH ₂ -rGO	0	33	21	Continuous deactivation
Pt ₁ Ru ₅ @NH ₂ -rGO	0	54	0	3 (58 h)
Ru@NH ₂ -rGO	61	198	0	20 (5 h)

been observed for other passivated Ru nanoparticles,^{9,10} and it is ascribed to the reduction of the RuO₂ shell to metallic Ru⁰. Another significant difference between catalysts is the time required to reach the most active state of the catalysis, 58 h for Pt₁Ru₅@NH₂-rGO and 5 h for Ru@NH₂-rGO (see Fig. 4(c) and Table 2). If we compare Pt₁Ru₅@NH₂-rGO and Ru@NH₂-rGO, both are initially partially surface-oxidized, as inferred from XPS³⁹ and XAS data. After applying the reduction potential, the longer time needed to activate the Pt₁Ru₅@NH₂-rGO hybrid material could be attributed to either the slower hydride formation kinetics in its strained crystal structure (*vide supra*) and/or to the presence of PtO_x, which might make the reduction of RuO₂ to Ru more difficult. As expected, the Tafel slopes after activation (see Fig. S10†) for Pt₁Ru₅@NH₂-rGO

(46 mV dec⁻¹) and Ru@NH₂-rGO (38 mV dec⁻¹) are the smallest among all the catalysts, indicating the fastest reaction kinetics. Despite the long activation period, Pt₁Ru₅@NH₂-rGO shows the best activity in HER out of all the mono and bimetallic systems.

In order to study the performance at high current density, LSV measurements were performed on the Pt₁Ru₅@NH₂-rGO catalyst before and after applying chronopotentiometry at -300 mA cm^{-2} in 1 M H_2SO_4 . The overpotential required to reach a current density of -10 mA cm^{-2} (η_{10}) decreased significantly over time: starting from an initial value of 130 mV, it dropped to 12 mV after 7 hours, and further decreased to only 2 mV after 19 hours of operation.

TEM analysis was performed for the nanomaterials remaining at the electrodes after bulk electrolysis at $j = -10 \text{ mA cm}^{-2}$ (Fig. 5). Pt-rich samples (Pt@NH₂-rGO, Pt₅Ru₁@NH₂-rGO, and Pt₁Ru₁@NH₂-rGO) show obvious agglomeration, which may be due to the poor stability of Pt NPs on NH₂-rGO in acidic conditions,⁴⁴ explaining their catalytic activity loss. In contrast, TEM analyses of Pt₁Ru₅@NH₂-rGO and Ru@NH₂-rGO indicate that there is no significant change before and after catalysis, as the nanoparticles are uniformly distributed over the NH₂-rGO support. It can be concluded that the affinity of Ru for the N-doped support is higher than that of Pt, as the aggregation of Pt samples is more pronounced. In general terms, Ru exhibits greater affinity towards N than Pt, and the N-doping of the support favors Ru anchoring.^{12,44} The slower activation of Pt₁Ru₅@NH₂-rGO may be due to weaker nanoparticle-support interactions compared to those in monometallic Ru system. As

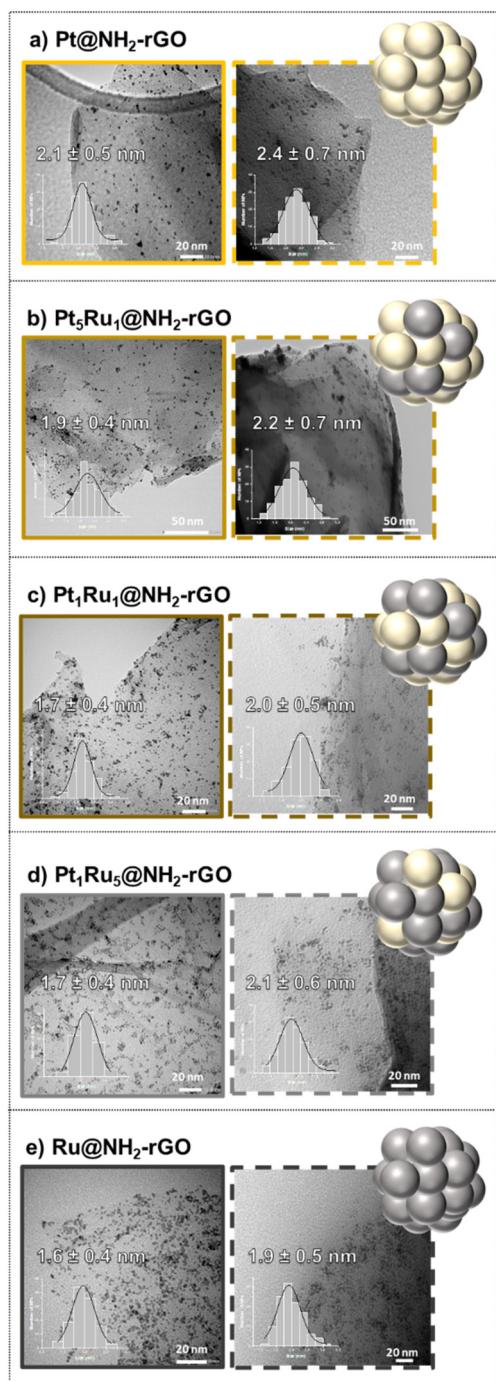


Fig. 5 TEM images of the hybrid materials before (left) and after applying the reduction potentials in 1 M H₂SO₄ (right).

a result, in the bimetallic system, it takes a longer time to transfer the electrons necessary to reduce the oxide passivation layer.

From the double layer capacitance values (C_{DL}) (Fig. S7†) obtained in a non-faradaic zone of the cyclic voltammetry experiments, the electrochemical active surface area (ECSA) and roughness factor (RF) of all $\text{Pt}_x\text{Ru}_y@\text{NH}_2\text{-rGO}$ catalysts before and after reduction (at maximum activation time) can

be estimated. With these data in hand, the specific current density (j_s) can be calculated before and after activation. These values are summarized in Table 3. Before activation, the ECSA values of $\text{Pt}@\text{NH}_2\text{-rGO}$, $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$, $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$, $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ and $\text{Ru}@\text{NH}_2\text{-rGO}$ are *ca.* 21 cm², 28 cm², 31 cm², 21 cm², and 7 cm², respectively. However, after applying the reductive potential, the ECSA significantly changes. In detail, the activated $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ and $\text{Ru}@\text{NH}_2\text{-rGO}$ samples presented an increased ECSA value (from 21 cm² to 25 cm² and from 7 cm² to 47 cm², respectively) and roughness factor (RF) values (from 105 to 125 and from 33 to 234, respectively). Although values at $\eta = 100$ mV are commonly reported in the literature, the current density for the most active materials in this work (reported in Table 3) surpassed the measurable range in our potentiostatic unit. Therefore, for comparison purposes, we analyze the specific current density values at $\eta = 50$ mV for all catalysts series. Among them, activated $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ presents the highest specific current density at $\eta = 50$ mV with a value of 0.87 mA cm⁻², in agreement with all other benchmarking parameters.

Faradaic efficiency experiments are used to quantify the percentage of electrons involved in the desired catalytic reactions (in our case, producing H₂). As shown in Fig. S8,† all the $\text{Pt}_x\text{Ru}_y@\text{NH}_2\text{-rGO}$ catalysts display faradaic efficiencies around 97–98% when performing chronoamperometry experiments at $j = -10$ mA cm⁻² for 20 min in 1 M H₂SO₄, which indicates that virtually all the electrons passing through the system are used in the HER and no side reactions take place.

For the most promising catalysts, $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ and $\text{Ru}@\text{NH}_2\text{-rGO}$, long-term stability tests were conducted after attaining maximum activation by applying bulk electrolysis (chronopotentiometry) at $j = -10$ mA cm⁻² for 12 h to evaluate their feasibility in practical applications. In Fig. S11,† the LSV curves before and after the bulk electrolysis experiments for $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ and $\text{Ru}@\text{NH}_2\text{-rGO}$ are presented. No significant changes were observed for the η_{10} overpotential values, indicating that these two catalysts are stable in 1 M H₂SO₄ in the medium-long term.

The materials were also tested in basic conditions. Chronopotentiometry experiments were conducted in 1 M NaOH (pH 14) at a constant current density of -10 mA cm⁻² (see Fig. S15 and S16†). In all cases, the catalysts exhibited higher overpotentials and Tafel slopes under alkaline conditions compared to acidic media. The overpotentials (η_{10}) measured at the stabilized state were: $\text{Ru}@\text{NH}_2\text{-rGO}$ (199 mV, stable after 9 hours), $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ (310 mV, stable after 4 hours), $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$ (288 mV, stable after 4 hours), $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$ (297 mV, stable after 2 hours), and $\text{Pt}@\text{NH}_2\text{-rGO}$ (245 mV, stable after 2 hours). This final state was probably reached after an initial deactivation process, during which the NPs with weaker adhesion to the electrode gradually detached until stabilization, as ascertained by the decrease in the ECSA values (Fig. S17–S21†). Under alkaline conditions, monometallic catalysts (especially Ru) behave better than bimetallic catalysts, indicating no synergistic effects in this case. This result is expected as it is well known



Table 3 Summary of physical-chemical and HER electrocatalytic data (in 1 M H₂SO₄) for all nanomaterials studied on this work before applying a reductive potential

Entry	Material	ϕ (nm)	η_{10} (mV)	Tafel slope (b) (mV dec ⁻¹)	j_0 (mA cm ⁻²)	ECSA (cm ²)	RF	$ j_s _{(\eta=100 \text{ mV})}$ (mA cm ⁻²)	$ j_s _{(\eta=50 \text{ mV})}$ (mA cm ⁻²)
1	Pt@NH ₂ -rGO	2.2 ± 0.4	12	39	5.16	21	106	—	0.70
2	Pt ₅ Ru ₁ @NH ₂ -rGO	1.9 ± 0.4	32	48	0.35	28	142	0.63	0.16
3	Pt ₁ Ru ₁ @NH ₂ -rGO	1.7 ± 0.4	33	42	2.19	31	156	0.31	0.11
4	Pt ₁ Ru ₅ @NH ₂ -rGO ^a	1.7 ± 0.4	54/3	65/46	1.35/0.94	21/25	105/125	0.29 /-	0.08/0.80
5	Ru@NH ₂ -rGO ^a	1.6 ± 0.4	198/20	169/38	0.66/2.86	7/47	33/234	0.07/1.18	0.04/0.27

^a Values before/after bulk electrolysis.

that Pt is not stable in alkaline media under turnover conditions.¹⁰

Atomistic interpretation

With the aim of getting atomistic insights on the catalytic activity of bimetallic Pt₁Ru₅@NH₂-rGO nanoparticles, DFT calculations were performed on three representative nanoparticle models (Pt₇₉, Ru₅₇ and Pt₁₀Ru₄₇) (Fig. 6). The bimetallic model ratio corresponds to that of the most active catalyst, Pt₁Ru₅@NH₂-rGO. The model is constructed maintaining the hcp structure of Ru and a sub-cluster segregated arrangement with Pt-Pt (4.8), Ru-Ru (7.1) and Ru-Pt (0.7) coordination numbers. That is, the experimental structure and coordination numbers were used to build the nanoparticle model (see Computational details for further information). The adsorption energies of one H on different surface sites were used, as defined by Nørskov and co-workers,⁴⁵ as descriptor for the catalytic activity of the different materials. However, a key point that remains challenging is the determination of the

amount of adsorbed H (and their distribution around the nanoparticle) at the reaction conditions. Previous contributions outlined that more than one H atom per surface metal center are adsorbed at working reductive potentials although the exact number is system dependent.^{9,10,46,47} Consequently, to obtain a fairly representative model, a multistep process was followed consisting of short *Ab initio* Molecular Dynamics (AIMD) simulations and geometry optimizations at different H coverage until the mean adsorption energy of the last H atoms becomes close to the Nørskov reference adsorption energy. Further details on the model construction can be found in the computational details section. Therefore, the following three representative models were obtained: (i) Pt₇₉H₁₀₅, (ii) Ru₅₇H₆₁ and (iii) Pt₁₀Ru₄₇H₆₅ (Fig. 6).

Different surface sites were identified according to different criteria: (i) surface metal location at the nanoparticle (A–G in Fig. 6g–i); (ii) hydrogen atoms already bonded to the metal center before the adsorption of the additional H; and (iii) presence or absence of an H atom on top of the metal center where the adsorption of the extra hydrogen takes place. All these sites were considered for the adsorption of an H atom either on top of a single center or bridging between two centers. The following nomenclature is used: $T(K_{ia})$ refers to centers where an H atom is added on top and $\mu(K_{ia}-L_{jb})$ represents H bridging between two atoms. K and L stand for the metal location at the NP (A to G), i and j specify the number of H already adsorbed (1 to 4), while a and b indicate the presence (Y = yes) or absence (N = no) of a H on top before the adsorption of the additional H atom. As an example, $T(B_{2N})$ corresponds to the adsorption on top of a metal located in B that already has two H atoms none of them on top.

Table 4 reports the adsorption energies of the additional H atoms that are computed about ± 10 kJ mol⁻¹ away from the ideal value proposed by Nørskov (-23.4 kJ mol⁻¹). The adsorption of all other computed sites can be found in the ESI (Table S1†). For Pt₇₉H₁₀₅, the adsorption energies range between -35.0 and $+14.7$ kJ mol⁻¹. H adsorbed on bridges and top sites that do not present previous H atoms on top present similar adsorption energies, ranging between -35.0 and -10.4 kJ mol⁻¹. For the adsorption on top sites the adsorption energy does not seem to depend much on the nanoparticle metal site environment. Conversely, sites with H atoms already adsorbed on top exhibit very weak or even unfavorable adsorp-

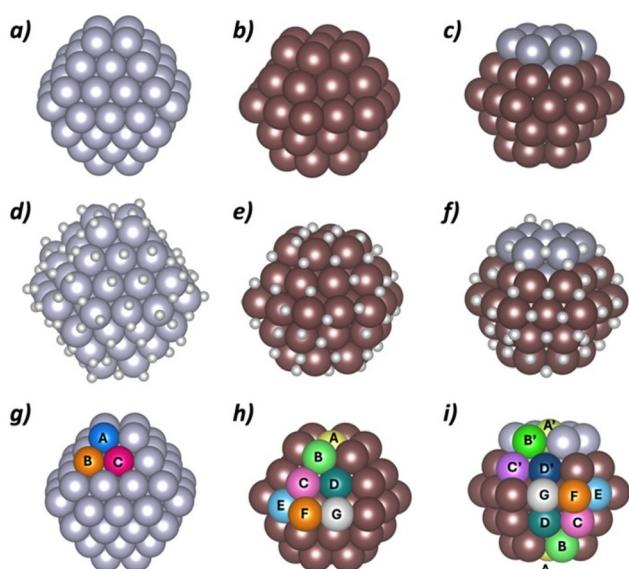


Fig. 6 Nanoparticle models used in the DFT simulations and their different sites taking metal environment as criterion: (a) Pt₇₉, (b) Ru₅₇, (c) Pt₁₀Ru₄₇, (d) Pt₇₉H₁₀₅, (e) Ru₅₇H₆₁, (f) Pt₁₀Ru₄₇H₆₅, (g) sites for Pt₇₉ model, (h) sites for Ru₅₇ model and (i) sites for Pt₁₀Ru₄₇ model.



Table 4 Representative DFT computed adsorption energies (in kJ mol^{-1}) of additional H atoms on $\text{Pt}_{79}\text{H}_{105}$, $\text{Ru}_{57}\text{H}_{61}$ and $\text{Pt}_{10}\text{Ru}_{47}\text{H}_{64}$ nanoparticles

$\text{Pt}_{79}\text{H}_{105}$		$\text{Ru}_{57}\text{H}_{61}$		$\text{Pt}_{10}\text{Ru}_{47}\text{H}_{64}$	
Site	E_{ads}	Site	E_{ads}	Site	E_{ads}
$T(\text{B}_{2\text{N}})$	-32.8 to -30.1	$\mu(\text{C}_{3\text{N}}-\text{D}_{1\text{N}})$	-30.6	$\mu(\text{C}'_{3\text{N}}-\text{D}'_{1\text{N}})$	-29.0
$\mu(\text{A}_{4\text{Y}}-\text{C}_{1\text{N}})$	-26.8	$T(\text{F}_{4\text{N}})$	-26.7 to -24.6	$T(\text{B}'_{3\text{N}})$	-28.2 to -15.2
$\mu(\text{A}_{3\text{Y}}-\text{B}_{2\text{Y}})$	-26.1	$T(\text{B}_{4\text{N}})$	-24.1 to -14.7	$\mu(\text{C}_{3\text{N}}-\text{C}_{3\text{N}})$	-24.6 to -19.6
$T(\text{A}_{3\text{N}})$	-20.4	$T(\text{C}_{4\text{N}})$	-22.9 to -9.7	$T(\text{F}_{3\text{N}})$	-21.5
$T(\text{C}_{3\text{N}})$	-16.6 to -10.4	$T(\text{F}_{3\text{N}})$	-17.4	$T(\text{B}_{4\text{N}})$	-20.5 to -11.6
				$T(\text{E}_{4\text{N}})$	-19.5
				$T(\text{F}_{4\text{N}})$	-17.4
				$T(\text{C}'_{3\text{N}})$	-15.8
				$T(\text{D}_{2\text{N}})$	-15.4

tion energies for a second H, indicating that the adsorption of a second top H atom on Pt is unlikely. Overall, the computed adsorption energies suggest that the high initial catalytic activity for HER of the synthesized $\text{Pt}@\text{NH}_2\text{-rGO}$ nanoparticles comes mainly from bridge and top sites, whose adsorption energies are close to the ideal value.

Adsorption energies of H atoms exceeding $\text{Ru}_{57}\text{H}_{61}$ coverage ranges from -46.7 and +6.8 kJ mol^{-1} . The H atoms adsorbing on bridging sites interact more strongly with the nanoparticle than those adsorbed on top position. The adsorption energies of the bridge sites range between -46.7 and -30.6 kJ mol^{-1} and thus, the values are too high to suggest that bridge H atoms are involved in HER. The adsorption energies on top sites range between -26.7 and +6.8 kJ mol^{-1} . Interestingly, the adsorption energy is dependent on the Ru surface metal coordination: corner sites (F and B) show stronger adsorption than edges (C, E, G) and face located sites (A and D). Indeed, the least coordinated sites present adsorption energies that are close to the Nørskov ideal value and suggest that they would be responsible for the high catalytic activity of activated (reduced) $\text{Ru}@\text{NH}_2\text{-rGO}$.

The additional H atoms on the $\text{Pt}_{10}\text{Ru}_{47}\text{H}_{64}$ nanoparticle present adsorption energies between -45.7 and +13.4 kcal mol^{-1} . The adsorption energies of bridge and top H atoms on Pt surface metals are similar to those found for Pt_{79} nanoparticle thus suggesting that these sites exhibit similar activity to pure metallic nanoparticles. Remarkably, the number of Pt centers without a pre-adsorbed H on top is larger on the Pt–Ru interface, thus indicating a higher concentration of Pt active sites in this region. In addition, the low coordinated Ru surface centers also present adsorption energies close to Nørskov value for very active sites. Finally, some bridge Ru sites of the interface become also active for the bimetallic system. Therefore, according to calculations, the $\text{Pt}_{10}\text{Ru}_{47}\text{H}_{64}$ nanoparticle is highly active in HER mainly due to the presence of Pt and Ru domains that keep their individual high catalytic activities. In addition, a synergic effect of the bimetallic nanoparticle seems also to be present. The Pt–Ru interface promotes the presence of new active sites: (i) a higher density of available Pt top sites; and (ii) some Ru bridge sites in the interface in which H interacts with the appropriate adsorption energy. Overall, the high performance of activated

(reduced) $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ could be attributed to the activity of the two domains, the synergy between metals and the high stability of the hybrid electrode due to the affinity of ruthenium for the $\text{NH}_2\text{-rGO}$ support.

Conclusion

In this contribution, mono- and bimetallic Pt–Ru NPs supported onto $\text{NH}_2\text{-rGO}$ have been used as electrocatalysts for HER. The $\text{NH}_2\text{-rGO}$ support facilitates the stabilization of ultra-small Pt and/or Ru NPs, which have been synthesized *via* the organometallic approach. TEM micrographs and XAS analysis confirmed the bimetallic nature of the catalysts and revealed how the nanoparticle morphology varies with the atomic composition, obtaining limited alloy regions together with segregated structures.

All PtRu-based catalysts ($\text{Pt}@\text{NH}_2\text{-rGO}$, $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$, $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$, $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$, and $\text{Ru}@\text{NH}_2\text{-rGO}$) were tested as electrocatalysts for the HER in acidic conditions. In the initial state, $\text{Pt}@\text{NH}_2\text{-rGO}$ outperformed all the other four catalysts offering the lowest overpotentials ($\eta_0 \approx 0$ mV and $\eta_{10} = 12$ mV), and lowest Tafel slope (39 mV dec^{-1}), while $\text{Ru}@\text{NH}_2\text{-rGO}$ displayed the highest overpotential ($\eta_{10} = 198$ mV) to achieve a current density of -10 mA cm^{-2} . Upon applying a reductive potential, the performances of all the catalysts changed. Deactivation was observed for the Pt-rich catalysts ($\text{Pt}@\text{NH}_2\text{-rGO}$, $\text{Pt}_5\text{Ru}_1@\text{NH}_2\text{-rGO}$, and $\text{Pt}_1\text{Ru}_1@\text{NH}_2\text{-rGO}$), which agglomerate at the surface of the carbonaceous support due to a weak affinity between the Pt metal and the support. However, activation was observed for the Ru-rich catalysts ($\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ and $\text{Ru}@\text{NH}_2\text{-rGO}$), likely indicating that the passivation shell of RuO_2 is reduced to Ru^0 , as previously reported in the literature.⁹ Finally, both $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ ($\eta_0 = 0$ mV and $\eta_{10} = 3$ mV, Tafel slope of 46 mV dec^{-1}) and $\text{Ru}@\text{NH}_2\text{-rGO}$ ($\eta_0 = 0$ mV and $\eta_{10} = 20$ mV, Tafel slope of 36 mV dec^{-1}) systems have demonstrated outstanding activity and stability for HER, showing no signs of deactivation or nanoparticle aggregation under turnover conditions for 12 h, maintaining η_{10} values comparable to the best catalysts reported in the literature and paving the way for their real-device application.



DFT calculations suggest that pure Pt and Ru nanoparticles show several active sites that are also found in the monometallic regions of the bimetallic cluster segregated catalyst **Pt₁Ru₅@NH₂-rGO**. Moreover, some additional sites at the Ru-Pt interface of **Pt₁Ru₅@NH₂-rGO** are also suggested to be active according to our calculations. Overall, the activity of the Ru-rich bimetallic systems could be attributed to three factors: (i) the high activity of the Ru and Pt domains; (ii) synergistic effects at the Pt–Ru interface with the presence of a higher density of active sites and (iii) the affinity of ruthenium for the carbonaceous support. The significant novelty and impact of this work lie in the combination of advanced synchrotron-based XANES and EXAFS analysis with DFT modelling, which enables a deep, atomic-scale understanding of the structure–activity relationship in Pt–Ru HER catalysts, offering valuable insights for the rational design of future electrocatalysts.

Experimental section

Reagents and materials

All synthesis and reagent handling procedures were performed using a standard Schlenk line, Fisher–Porter tube techniques or glove-box workstation following the procedure described in a previous publication.³⁹ The solvents used (THF, hexane) were purified and treated in solvent stills and then degassed by the freeze–pump–thaw method before use. The precursors [Ru(COD)(COT)] (COD = 1,5-cyclooctadiene; COT = 1,3,5-cyclooctatriene) and [Pt(NBE)₃] (NBE = norbornene) were purchased from Nanomeps. Hydrogen gas (Alphagaz) was purchased from Air Liquide. High-purity deionized water was obtained by passing distilled water through a nanopore Milli-Q water purification system.

Mono- and bimetallic catalyst (**Ru@NH₂-rGO**, **Pt₁Ru₅@NH₂-rGO**, **Pt₁Ru₁@NH₂-rGO**, **Pt₅Ru₁@NH₂-rGO** and **Pt@NH₂-rGO**) were synthesized according to a previous publication.³⁹

Characterization techniques

Transmission electron microscopy (TEM) and high-resolution TEM (HRTEM). Samples for transmission electron microscopy analyses were prepared by depositing one drop of colloidal reaction solution onto a carbon-coated copper grid and the characterization was performed at “Servicio de Microscopía Electrónica” of Universitat Politècnica de València (UPV) by using a JEOL JEM 1010 CX-T electron microscope operating at 100 kV and JEOL JEM 2010 electron microscope working at 200 kV.

XAS. The EXAFS signal has been analyzed using the standard equation:

$$\chi(k) = i \sum_j \frac{N_j S_0^2}{k R_j^2} f_j(k, R_j) e^{\frac{2R_j}{\lambda(k)}} e^{2k^2 \sigma_j^2} \sin(2kR_j + \delta_j(k)) \quad (1)$$

where R_j is the distance between the photo-absorber and the neighboring j -atoms, N_j is the number of neighboring atoms, S_0^2 is the passive electrons' amplitude reduction factor, $f_j(k, R_j)$

is the backscattered amplitude, λ is the photoelectron mean free path, $\delta_j(k)$ is the phase shift, and σ_j^2 is the correlated Debye–Waller (DW) factor measuring the mean square relative displacement (MSRD) between photo-absorber and back scatterer. The EXAFS data were fitted using the Artemis program of the IFFEFIT package. In the model curve, $f_j(k, R_j)$, λ , and $\delta_j(k)$ were calculated using the FEFF-8 code.⁴⁸

Transmission EXAFS measurements at Ru K-edge (22117 eV) and Pt K-edge (78 404 eV) were performed in quick-EXAFS mode at the CLAES beamline of the Spanish National Light Source, (ALBA Synchrotron, Barcelona, Spain), using a Si (311) double-crystal monochromator.⁴⁹ The incoming and outgoing photon fluxes were measured by ionization chambers filled with appropriate mixtures of N₂ and Kr gases. The second focusing mirror of the beamline has been set to have a focal point of $400 \times 300 \mu\text{m}^2$. Fitting procedure is indeed very similar to the one explained in literature.⁵⁰ Theoretical parameters like phase and amplitude functions were calculated using FEFF8.2 and experimental factors (S_0^2) derived from reference materials (RuO₂, Ru foil and Pt foil) initially fitted apart. As a consequence, a S_0^2 value of 0.79 (0.21) and 0.82 (0.34) has been set for Pt and Ru edges modelling. In the following we consider three main contributions mimicking metal–oxygen (M–O) and metal–metal (M–M) and metal–different metal (M–M1) interactions in the EXAFS fitting. More in detail, we considered an M–O coordination number, M–O bond length, and M–O Debye Waller factor for the first shell. M–M and M–M1 coordination numbers, M–M and M–M1 bond lengths, and M–M and M–M1 Debye Waller factors for the second shell. Correction to edge position E0 has found to be 5.80 (0.26) eV and 5.66 (1.33) eV for Pt L3 and Ru K edges respectively. M–O, M–M, M–M1 Debye Waller factors have been set common to all samples. Finally, all the paths included in the analysis have been weighted by the corresponding metallic and oxide fractions obtained by the LCF of the XANES. The M–O interaction has been considered in the analysis only if its value is found above 20%.

Fitting results were obtained by using the Artemis program program⁵¹ and error bars were estimated with k1/k2/k3 weighted fittings.

Electrochemical measurements

Hydrogen evolution reaction (HER) was carried out using an Origalys potentiostat in a typical three-electrode system with Ag/AgCl (Sat'd) as reference electrode (RE). A rotating disk glassy carbon electrode (RDE-GC, 0.2 cm² surface area) coated with the catalyst and a Pt rod were used as working electrode and auxiliary electrode, respectively. GC disk electrode was carefully polished before being used. The other two electrodes were rinsed with Milli-Q water and dried prior to the measurements. The speed of the RDE was set to 3000 rpm to remove the hydrogen bubbles produced during this reaction. 1 M H₂SO₄ solution was prepared by diluting 56.1 mL of 95–97% H₂SO₄ with 943.9 mL Milli Q water and pH was adjusted to 0.

Linear sweep voltammetry (LSV) at a scan rate of 10 mV s⁻¹ were carried out in an Argon-saturated 1 M H₂SO₄ aqueous



solution ($\text{pH} = 0$). Chronopotentiometry was performed by applying a current (i) of -2 mA to reach the current density (j) of -10 mA cm^{-2} . All the potentials in this work were converted to Normal Hydrogen Electrode (NHE) by adding a value of 0.199 V (reference value at 25°C)

Electrode preparation

The modified GC was prepared as follows: 1 mg of $\text{Pt}_x\text{Ru}_y@\text{NH}_2\text{-rGO}$ was dispersed in 0.5 mL of THF, and then sonicated 5 min to obtain an ink. $15 \mu\text{L}$ of the ink were loaded by drop casting on the GC, then covered with $5 \mu\text{L}$ of Nafion® solution. The Nafion® solution was prepared as follows: $40 \mu\text{L}$ of 5% Nafion®, 7.96 mL Milli-Q water and 2 mL of *n*-propanol. The working electrode was dried at room temperature with an air flow.

In the case of faradaic efficiency measurements, the FTO electrode (1 cm^2 surface area) was used as the working electrode. $25 \mu\text{L}$ of the ink was drop-casted on the surface of the FTO electrode and dried at room temperature with an air flow.

Faradaic efficiency

A two-compartment cell with a permeable membrane in the middle is used. The WE and RE were placed in the same compartment together with the Clark electrode, and the CE was placed in the second compartment. Each of the compartments was filled with 7 mL of $1 \text{ M H}_2\text{SO}_4$ solution and a magnetic stirrer. A Unisense H₂-NP Clark was employed to obtain the hydrogen gas produced during the 20 min chronopotentiometry. In the end, the Clark electrode was calibrated by adding different volumes of 99% pure H_2 , and then the amount of hydrogen was calculated according to the ideal gas law.

Double-layer capacitance (C_{DL}) and electrochemically active surface area (ECSA) determination

Double-layer capacitance (C_{DL}) was determined by applying a series of cyclic voltammetry (CV) with different scan rates in a non-faradaic zone. In this region, no redox reaction took place, and the current is due to the double layer charging. Based on this, the charging current (i_c) can be calculated. i_c equals to the product of the electrochemical double-layer capacitance (C_{DL}) and the scan rate (ν) (as shown in eqn (2)). In this experiment, the scan rates increase from 5 mV s^{-1} to 500 mV s^{-1} , keeping 10 s the potential vertex at each scan of the CV. Then Plotting i_c as a function of ν will yield a straight line whose slope equals to C_{DL} . By using the C_{DL} to divide the specific capacitance (C_s), the electrochemically active surface area (ECSA) can be determined (eqn (3)). As reported, the C_s depends on the nature of material used and solution (for C_s in $1 \text{ M H}_2\text{SO}_4$ $C_s = 13\text{--}17 \mu\text{F cm}^{-2}$). The roughness factor (RF) is the ratio of ECSA to the geometrical surface area (S) of the RDE (eqn (4)).

$$i = \nu C_{\text{DL}} \quad (2)$$

$$\text{ECSA} = \frac{C_{\text{DL}}}{C_s} \quad (3)$$

$$\text{RF} = \frac{\text{ECSA}}{S} \quad (4)$$

According to ECSA, specific current density (j_s) can be calculated as follows:

$$j_s = \frac{i}{\text{ECSA}} \quad (5)$$

where i is the current intensity at the given potential, here the given potential (η) is 100 mV .

Computational details

Models

Three nanoparticle models adapted from those existing in the literature^{9,52–55} were used to represent $\text{Pt}@\text{NH}_2\text{-rGO}$, $\text{Ru}@\text{NH}_2\text{-rGO}$ and $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ (Fig. 6a–c). $\text{Pt}@\text{NH}_2\text{-rGO}$ nanoparticles were modeled from the 1.2 nm large, truncated octahedron Pt_{79} model.^{54,55} The $\text{Ru}@\text{NH}_2\text{-rGO}$ one, with the Ru_{57} model previously used by some of us, which mainly exhibits (100) and (101) planes.^{9,52,53} Finally, the $\text{Pt}_1\text{Ru}_5@\text{NH}_2\text{-rGO}$ nanoparticles were represented with a cluster segregated $\text{Pt}_{10}\text{Ru}_{47}$ model derived from the Ru_{57} nanoparticle. This model correctly reproduces the experimentally observed nanoparticle size as well as the Pt-Pt, Ru-Ru and Ru-Pt contacts.

Both experimental¹¹ and computational^{9,46} previous contributions showed that more than one hydrogen atom per surface metal center is adsorbed at reaction conditions. However, the exact number of H varies depending on the metal model and the presence or absence of ligands. Therefore, the H content and distribution that should be included in the initial model are unknown. With the aim of determining the appropriate number of H as well as obtaining reasonable structures of the M_xH_y ($\text{M}_x = \text{Ru}_{57}$ or Pt_{79}) nanoparticle models, we use a multi-step process consisting of Ab Initio Molecular Dynamics (AIMD) simulations of at least 1.5 ps for each system (see below) and geometry optimization of a representative snapshot of the AIMD simulation. In the first step, we added 1 H per surface metal center (monolayer, $\theta = 1$) and performed the AIMD simulation. Then, we computed the mean adsorption energy of the hydrogen atoms of this monolayer at a representative snapshot of the simulation. Since this adsorption energy is larger than the ideal value suggested by Nørskov and co-workers,⁴⁵ we increased the coverage (θ) by adding 0.25 H per metal center (Table S2†). We repeated this process several times until the mean adsorption energy of the newly added H atoms became close to the ideal value. It is however worth mentioning that, with the aim of enhancing the precision of our model, once the mean adsorption energy became closer to the ideal value, we also included structures resulting from adding 0.13 H per metal center. The final models in which we computed the hydrogen adsorption energy of additional H atoms are $\text{Pt}_{79}\text{H}_{105}$, $\text{Ru}_{57}\text{H}_{61}$ and $\text{Pt}_{10}\text{Ru}_{47}\text{H}_{65}$ (Fig. 6d–f). The $\text{Pt}_{79}\text{H}_{105}$ and $\text{Ru}_{57}\text{H}_{61}$ models were selected because their H adsorption energy is the closest (but above) to the ideal value,⁴⁵ while the $\text{Pt}_{10}\text{Ru}_{47}\text{H}_{65}$ model is



constructed by adding the average H atoms per surface Ru and surface Pt found in the two pure metallic systems. Analysis of the metal coordination number as well as the number of H atoms at a given metal center allowed to determine the different surface sites. To all these sites one additional H atom was adsorbed to determine the catalytic activity of each site at reaction conditions.

Since VASP enforces three-dimensional periodicity regardless of the nature of the system, the previously described nanoparticle models were set in a 25 (Ru₅₇ and Pt₁₀Ru₄₇) or 30 (Pt₇₉) Å edge large cubic box.

Level of theory

All calculations were performed with the PBE⁵⁶ density functional as implemented in VASP.^{57,58} Dispersion forces are considered by adding Grimme's D2 empirical correction.⁵⁹ Atomic cores are described with PAW pseudopotentials^{60,61} and the valence electrons are represented with a plane-wave basis set with an energy cutoff of 500 eV. All calculations were performed at Γ point due to the dimensionality of the model. The energy convergence criteria are fixed to 10^{-5} and 10^{-4} eV for electronic and geometry relaxations, respectively. This methodology is equivalent to that previously used by some of us when modeling other Ru-based materials for HER^{9,46} as well as IrO₂ nanoparticles and their electrocatalytic activity.^{62,63}

H adsorption energies reported throughout the text are computed with respect to the reference hydrogenated nanoparticle model as proposed by Nørskov and co-workers^{45,64} as summarized in eqn (6):

$$E_{\text{ads}} = [E_{\text{MXH(Y+1)}} \cdot (E_{\text{MXHY}} + 1/2 \cdot E_{\text{H}_2})] \quad (6)$$

where $E_{\text{MXH(Y+1)}}$, E_{MXHY} and E_{H_2} are the energies of the reference nanoparticle with an additional adsorbed hydrogen atom, of the reference nanoparticle model and of the H₂ molecule, respectively.

Data availability

The data supporting this article have been included as part of the ESI.†

Conflicts of interest

There are no conflicts to declare.

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