# Nanoscale

## MINIREVIEW

# Advances in simulating dilute alloy nanoparticles for catalysis

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Dilute alloy (DA) catalysts, including single-atom alloys (SAAs), which are comprised of trace amounts of an active promoter metal dispersed on the surface of a selective host metal, offer exceptional activity and selectivity while utilizing precious metals more efficiently. Although most SAA and DA applications have focused on partial hydrogenation and oxidation reactions, their use has steadily expanded into more complex thermo-, photo-, and electro-catalytic processes. This progress has been largely driven by mechanistic insights derived from computational chemistry and is expected to accelerate with the advancement of artificial intelligence. This minireview discusses novel advances in simulating SAAs and DAs for catalysis applications, including *ab initio* calculations, multiscale modeling, and machine learning. Emphasis is placed on the impact of reaction conditions, promoter ensembles, and nanoparticle morphology on the stability and catalytic performance of SAAs and DAs. Finally, a perspective is offered on potential future directions of SAA and DA simulations and their extension to other systems with distinct, well-defined active sites.

## Introduction

Metal alloying has been used to improve the structural and electronic properties of heterogeneous catalysts for over a century.[1] Additionally, given the differences between the surface and bulk compositions of alloys,[2] metal alloying can decrease the use of precious, active (usually Pt-group) metals

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by diluting and dispersing them on the surface of cheaper but less active host metals (*e.g.* coinage metals). Previous studies have shown that even trace amounts of promoter metals (<1% of the catalyst composition) can enhance the catalytic properties of the host.[3,4] Thus, significant efforts have focused on developing and understanding the function of dilute alloys (DAs) for catalysis applications,[5,6] *i.e.*, alloys with much higher host concentrations relative to the promoter, with the latter being generally dispersed in small surface clusters. Among DAs, single-atom alloys (SAAs), in which isolated, single promoter atoms are scattered on the surface of the host, have gained notable attention due to their unique bifunctionality,

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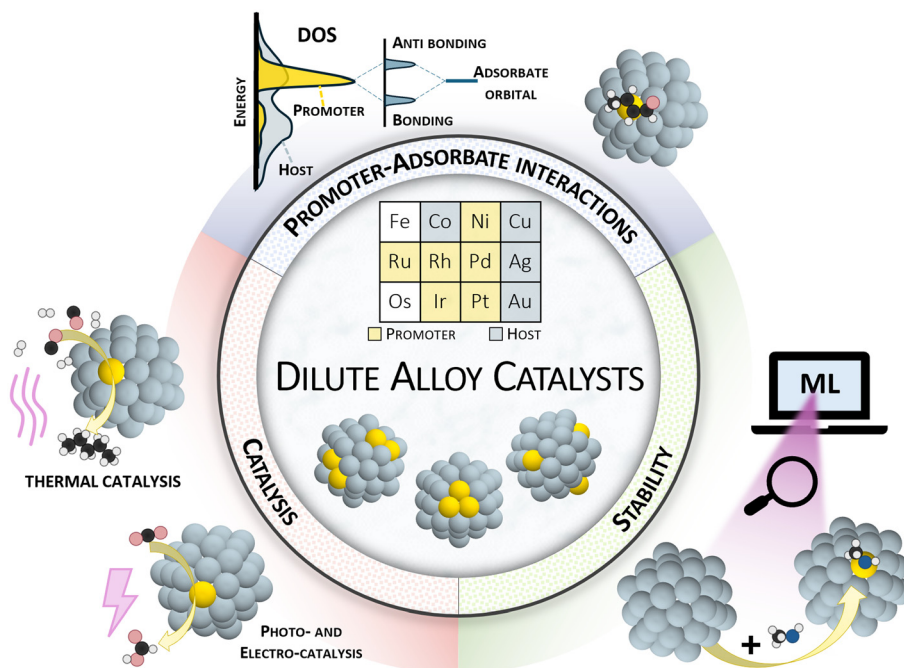
**Fig. 1** Graphical overview of recent developments in SAA and DA computational research, including insights dictating the promoter–adsorbate interactions, rapid screening of segregation trends, and catalyst discovery for thermo-, electro-, and photo-catalytic applications.

combining the high catalytic activity of the isolated promoter atoms with the weak intermediate binding of the host.[7–13]

In the design of SAA and DA catalysts, computational chemistry calculations, mainly based on density functional theory (DFT), have been pivotal in understanding the governing physicochemical phenomena leading to their desired functionality. DFT calculations have shown how, due to their bifunctionality, SAAs can escape the linear scaling relationships (LSR) that traditionally constrain the performance of mono-

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and bi-metallic catalysts.[11–13] These include the Brønsted–Evans–Polanyi (BEP) relationships,[14–17] the thermochemical scaling relationships,[18–20] and the d-band model,[21–23] all of which are well-known linear relationships for catalyst design. Moreover, DFT calculations of segregation ($E_{seg}$), *i.e.*, migration of promoter atoms from bulk to surface sites, and aggregation energies ($E_{agg}$), *i.e.*, formation of surface clusters from dispersed promoter metal atoms, have provided thermodynamic grounds on the stability of SAAs and DAs, both under vacuum and in the presence of adsorbates (*e.g.*, reaction intermediates).[24–26]

Furthermore, pairing DFT with multiscale modeling techniques has provided kinetic insights into catalytic events on the catalyst surface. For instance, by combining experimental work with DFT-parametrized kinetic Monte Carlo (kMC) simulations, Marcinkowski *et al.*[27] unveiled how spectator CO molecules can block the active Pd sites on a Pd-promoted Cu SAA, acting as a "molecular cork" that inhibits the uptake and desorption of surface H atoms. Variations of the molecular cork effect have also been investigated *via* DFT-parametrized kMC, including the desorption of hydrogen on Pt-promoted Cu SAAs,[28] as well as the coupling of methyl groups from methyl iodide on Ni- and Pd-promoted Au SAAs.[29] Additionally, based on the molecular cork effect, Pt- and Pd-promoted Cu SAAs have been proposed as hydrogen carriers.[30] Moreover, molecular dynamics (MD) simulations by Gu *et al.*[31–33] have shed light on the $H_2$ spillover mechanism on Pt-promoted Cu SAAs. Initial *ab initio* MD simulations showed how, following a dissociation step on the Pt site, one H atom migrates to the Cu host while the other atom remains trapped in the vicinity of

the promoter, inhibiting the dissociation of additional $H_2$ molecules.[31] To extend the timescale of the initial simulations, the potential energy surface was defined using a DFT-trained neural network (NN),[32] which further revealed how collisions with incoming $H_2$ molecules enable the spillover of the trapped H* atoms.[33]

It becomes apparent that SAA and DA catalysts are ideal systems for computational research because of the well-defined nature of active sites and the multiscale nature of catalytic events, thus enabling a gamut of computational techniques to be applied for their study. In this minireview, we cover recent computational insights and advances in the design of SAA and DA nanoparticles (NPs) for catalysis applications (Fig. 1). Moving forward, we use the PM–HM notation to describe SAA and DAs, where PM corresponds to the less-abundant promoter metal, while HM refers to the host metal (e.g., RuCo corresponds to Ru-promoted Co). Special attention is given to the effect of promoter-ensembles, NP morphology effects, and the emerging role of machine learning (ML) in accelerating the discovery of DA catalysts. Although we include very select experimental observations, this review article primarily focuses on computational advances guiding researchers on what is the state-of-the-art on simulations of SAAs and DAs. Hence, we point readers with an experimental interest in SAAs and DAs to remarkable reviews related to their synthesis,[10,34,35] structural analysis,[10,36] and experimental applications.[10,34–36]

# Key insights dictating promoter–adsorbate interactions

## Unique electronic structure of SAAs and DAs and its implications on adsorption

The unique properties of SAA catalysts stem from the poor electronic mixing between the isolated promoter atoms and the host-metal matrix. By analyzing the d-band projected density of states (PDOS) of Ni, Pt, Pd, Ir, and Rh-promoted SAAs having Ag, Au, and Cu as hosts, Thirumalai and Kitchin[37] showed how this poor mixing led to narrow peaks close to the Fermi level on the promoter atoms. This narrow feature has been experimentally validated by Greiner et al.[38] on a CuAg SAA and later by Hartwig et al.[39] on a PdAg SAA. Hence, the isolated promoter atoms exhibit free-atom-like electronic structures, which interact with adsorbates similar to organometallic complexes (i.e., through bonding and anti-bonding molecular orbitals).[37,38] Conversely, on mono- and intermetallic catalysts that follow the d-band model, adsorbate states are broadened and shifted from coupling with metallic sp-states, forming bonding and antibonding states by coupling with the metallic d-states.[40,41]

The narrow d-band feature of SAA promoters helps explain the high selectivity of SAA catalysts in partial hydrogenation reactions.[42,43] In this regard, Spivey and Holewinski[44] revealed how the location of the d-band promoter peak determines the selective hydrogenation of crotonaldehyde (a model α,β unsa-

turated aldehyde) on SAAs with Cu, Ag, and Au hosts (Fig. 2A and B). The hydrogenation of crotonaldehyde can occur via its carbonyl group, leading to an unsaturated alcohol, or via its alkene group, leading to a saturated aldehyde (Fig. 2B). Depending on the location of the sharp promoter d-band peak, the molecular orbitals associated with each hydrogenation pathway can be selectively hybridized (Fig. 2A). Thus, late transition metal (TM) promoters favor alkene hydrogenation, whereas earlier TMs favor carbonyl hydrogenation. Similar trends were observed by Ngan and Sautet,[45] when investigating the selective hydrogenation of acrolein (a different α,β unsaturated aldehyde) on Cu-based SAAs, i.e., early TMs hydrogenate the carbonyl group, whereas late TMs hydrogenate the alkene group. Additional work by Fung et al.[46] on Cu-based SAAs showed how the narrow d-band peaks can effectively hybridize with the C–H σ and σ* orbitals of methane, enabling its low-temperature activation. Furthermore, $CH_4$ chemisorption was found to be favored over early TM promoters, which have energetically high (electron-accepting) d-band centers.

Moving beyond the SAA into the DA limit, Monasterial et al.[47] investigated how the d-band PDOS and hydrogen adsorption change with increasing promoter-ensemble sizes (i.e., going from isolated metal promoter atoms to small promoter clusters) on Ag, Au, Cu, and Pd hosts. Overall, hybridization between promoter atoms broadens and splits the sharp d-band feature into new peaks. The number of new peaks generally matches the number of promoter atoms in the ensemble, e.g., a trimer has three peaks (Fig. 2C and D). Meanwhile, the resulting PDOS broadening depends on the promoter–promoter and host–promoter hybridization. Notably, when this broadening occurs across the Fermi level (Fig. 2D), it can lead to non-monotonic changes in hydrogen adsorption energy ($E_{ads}$), i.e., $E_{ads}$ does not scale linearly with the number of grouped promoters, despite hydrogen binding on the hollow site. This behavior is unique to DAs and contrary to their intermetallic counterparts. In a different study, Papanikolaou and Stamatakis[48] observed a similar PDOS peak broadening and splitting trend in NiCu SAA and DAs (Ni dimers and trimers). Furthermore, increasing the number of Ni atoms decreased the activation barrier ($E_{act}$) for CO, NO, and $N_2$ dissociation. This reduction could be attributed to an increased electron back-donation to the antibonding orbitals of the molecules, as the PDOS peaks of the DAs are closer to the Fermi level compared to that of the SAA case.

## Promoter-based trends in adsorption and spillover

In general, the preferred binding site/configuration of adsorbed species on SAAs depends on their number of dangling bonds. Species with a single dangling bond or lone pairs of electrons favor top-site adsorption, while species with two or three dangling bonds favor bridge- or hollow-site adsorption.[12,13] Furthermore, $E_{ads}$ is determined by the group number (i.e., number of valence electrons) of the promoter, often leading to U-shaped relationships.[46,47,49] Motivated by the similarities between SAAs and molecular systems, Schumann et al.[50] rationalized these U-shaped relationships
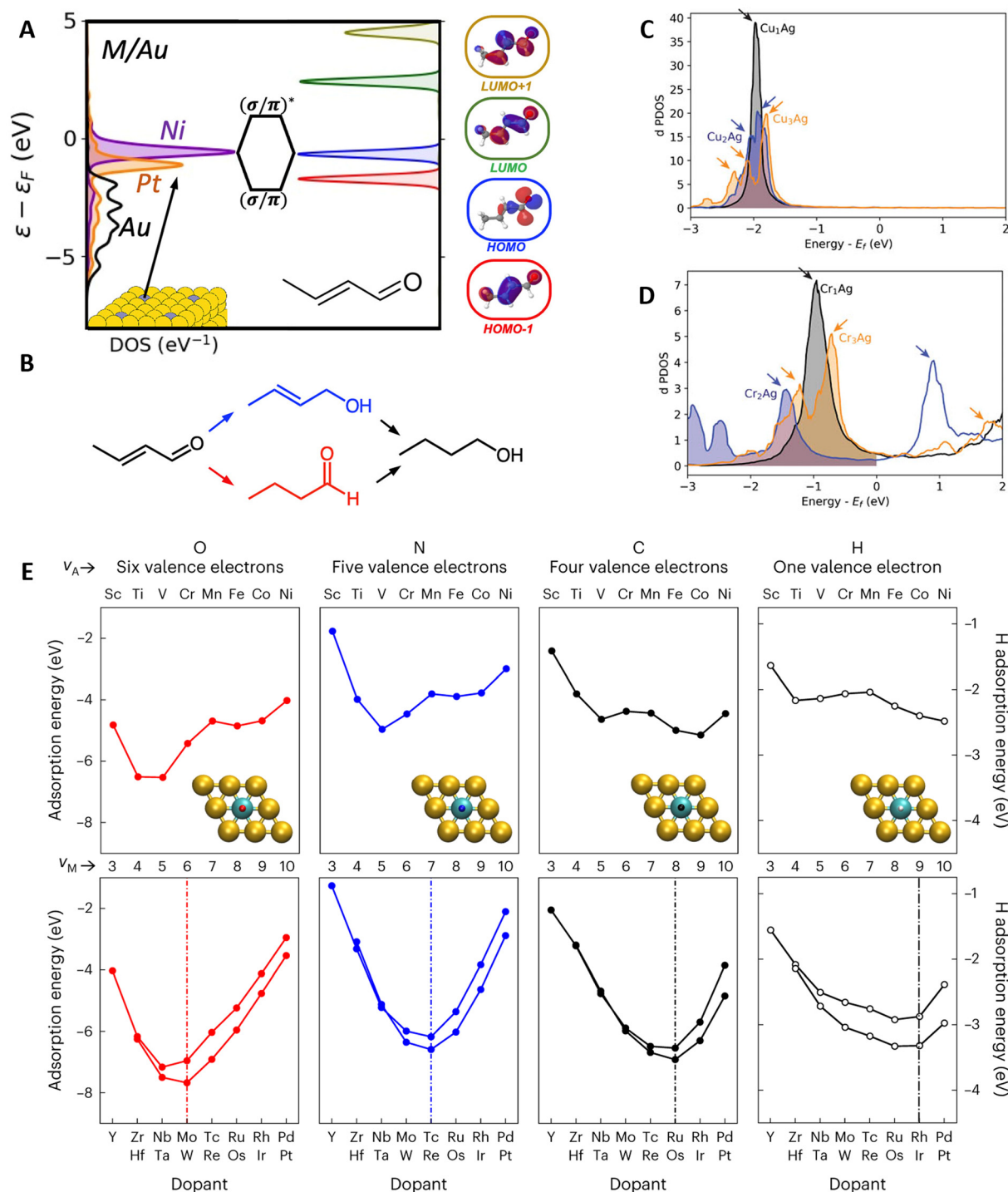
**Fig. 2** Insights on promoter–adsorbate interactions. (A) Effect of the promoter sharp peak (in the figure Ni or Pt) on the d-band PDOS and the hybridization of the molecular orbitals of crotonaldehyde. (B) The impact of the peak's location on the reduction pathways of crotonaldehyde (blue and red pathways color-matching the molecular orbitals in (A) related to the different binding configurations), reprinted (adapted) with permission from ref. 44, copyright 2021 American Chemical Society. Broadening and splitting of the sharp peak in the d-band PDOS with increasing ensemble sizes (monomers, dimers, and trimers) of (C) CuAg and (D) CrAg DAs, with arrows indicating the location of PDOS peaks, reproduced from ref. 47 with the permission of AIP Publishing. (E) Periodic trends for $E_{ads}$ of different adsorbates, highlighting the 10-electron-count rule and the deviations in 3d metal promoters. In the figure, $\nu_A$ and $\nu_M$ correspond to the valence electrons of the adsorbate and promoter metal, respectively, reproduced with permission from ref. 50.

using a simple 10-electron count rule (Fig. 2E). The 10-electron rule predicts a maximum $E_{ads}$ when the interacting valence electrons of the adsorbate and the valence electrons of the promoter add up to ten, *i.e.*, when the electrons of the adsorbate fill and saturate the d-orbitals of the promoter. It is worth noting that an adsorbate's number of interacting electrons is not necessarily equal to the number of valence electrons. For example, C* has two interacting electrons but four valence electrons, thus binding preferably on group-8 promoters (third column in Fig. 2E). Deviations from the rule can be found in 3d promoters due to spin effects and for adsorbates interacting non-covalently, like $H_2O$ and $NH_3$, which bind through electrostatic interactions.[50]

Besides adsorption, spillover (*i.e.*, the diffusion, from promoter to host sites, of small adsorbed species such as hydrogen atoms) is critical for the bifunctional operation of SAA catalysts.[11] Although spillover is entropically favored,[12] Schumann et al.[51] found that host atoms neighboring the promoter have weaker $E_{ads}$ than host atoms farther away, inhibiting the diffusion of adsorbates outside promoter-neighboring sites. Additional kMC simulations and experiments confirmed the role of this weak adsorption ring in preventing the diffusion of adsorbates deep into the host matrix. Remarkably, the discrepancy in $E_{ads}$ between host atoms decreases monotonically with the chemical group of the promoter, *e.g.*, O* binding is ~0.20 eV less favorable on Cu sites close to a Ru promoter compared to Cu sites far from it; nonetheless, this difference reduces to ~0.05 eV when Pd is the promoter. Once more, exceptions are found for 3d promoters due to spin effects and for promoters with less favorable $E_{ads}$ compared to the host.

To accelerate the prediction of spillover behavior, Réocreux et al.[52] developed a simplified linear model to compute the spillover energy (SOE), *i.e.*, the difference in formation energies of adsorbed species on host sites *versus* promoter sites. The model predicts DFT-obtained SOEs with a mean absolute error of 0.06 eV using two descriptors: (1) the charge of the promoter, relevant for saturated species that bind through electrostatic interactions, and (2) the SOE of C*, relevant for unsaturated species that bind through covalent bonds. Later work by Hannagan et al.[53] used the SOE as a key factor in designing NiCu SAA catalysts for formic acid decomposition. Moreover, SOE calculations provided insights into the poor enhancement provided by Pt promoters, which, like Ni, facilitate the rate-limiting C–H activation step but, unlike Ni, are limited by the unfavorable reverse spillover of formate intermediates from the Cu host.

## Stability of SAAs and DAs

### Thermodynamic stability of SAAs and DAs

As previously mentioned, DFT-calculated $E_{seg}$ and $E_{agg}$ values are used to predict the formation of isolated active sites on the surface both under vacuum and in the presence of adsorbates.[10,26] The stability of DA and SAA NPs is influenced by several factors, including surface energies, atomic radii, metal cohesive energies (CE), and promoter concentrations.[54–57] Additionally, metal–metal and adsorbate–metal interactions have been shown to dictate the formation of stable SAAs.[24,56,58] In this section, we particularly focus on how adsorbates, solvents, and applied potentials (in electrochemical applications) affect the overall stability of DAs and SAAs.

Metal–adsorbate interactions can lead to reverse segregation trends and/or the formation of clusters in SAAs.[24,26,56,59–61] To further understand these effects, Ouyang et al.[62] employed a combination of experiments and Monte Carlo (MC) simulations (parametrized using a DFT-fitted cluster expansion model) to study how the chemical ordering (*i.e.*, how different metal atoms occupy the lattice positions) of PdAu NPs can be tailored by varying the CO partial pressure and temperature. The strong binding between Pd and CO enhances the thermodynamic stability of Pd atoms on the surface of the alloy, promoting their segregation to the surface. Furthermore, at low CO coverage, the strong Pd-CO interaction favors the formation of Pd aggregates. On the other hand, at high CO coverages, CO–CO lateral interactions prevent Pd aggregation, dispersing them into single atoms, which is crucial in enhancing the selectivity of acetaldehyde in the partial dehydrogenation of ethanol. It is worth noting that segregation is not always induced in the presence of adsorbates, as demonstrated by Yu et al.[61] on NiCu(111) SAAs. DFT-calculated $E_{seg}$ revealed Ni segregation is favored in the presence of CO and O, whereas Ni stays in the bulk when exposed to H.

Additionally, solvent environments can influence the thermodynamic stability of DAs,[63] as solvent molecules can coordinate with the surface of metallic NPs.[64] For instance, by combining DFT calculations and experiments, Doronin et al.[65] revealed that in aqueous environments, water molecules increase the tendency of Ag to segregate to the surface of AgAu alloys (Fig. 3A). Interestingly, the effects of solvent molecules on the segregation behavior can become more pronounced under electrochemical conditions, as externally applied potentials can affect the stability of solvent molecules and intermediates on the surface.[66] In this regard, Weitzner et al.[67] investigated the stability of ten Cu(100) based SAAs *via* a hybrid atomistic-continuum approach. Surface-level phenomena were studied by pairing DFT with effective screening medium (ESM) and the electrolytic environment (1 M KOH) was implicitly considered through the reference interaction site method (RISM). Interfacial effects in the ESM-RISM scheme are bridged using a grand canonical scheme, adjusting the number of electrons and electrolyte ions according to the applied potential. Importantly, the segregation trends were found to vary across promoters when a reducing potential was applied (Fig. 3B). For instance, in the absence of adsorbates, the surface segregation of Al, Pt, and Ga promoters becomes less favorable with increasing reducing potentials, suggesting a sub-surface migration at strong cathodic conditions. Remarkably, comparing these results with a separate set of $E_{seg}$ calculations conducted in the absence of the electrolyte
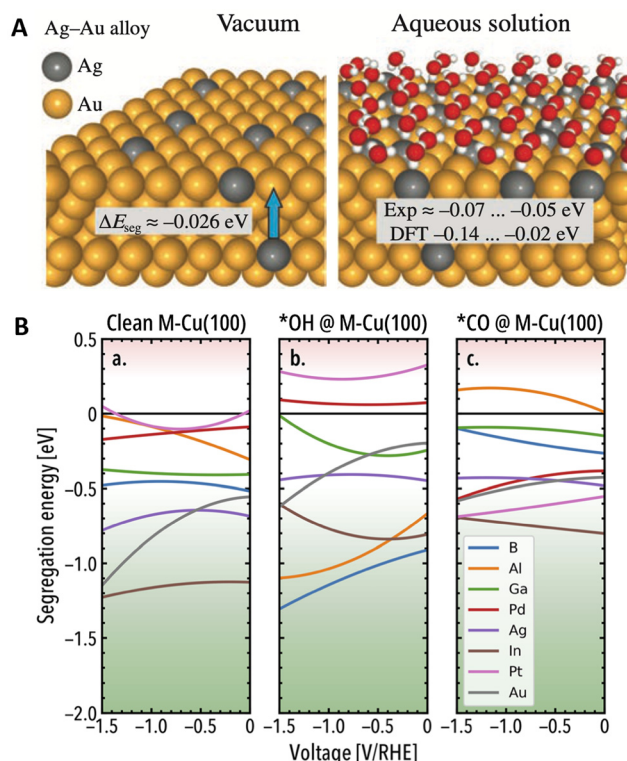
**Fig. 3** Impact of (A) aqueous solvent environments on the segregation behavior of AgAu(100) and (111) surfaces, reprinted from the Lancet (ref. 65), copyright 2020, with permission from Elsevier. (B) Applied potential effects on the surface segregation of Cu-based (100) DAs in the absence of adsorbates (a), and in the presence of OH* (b) and CO* (c) in 1 M KOH (different colors represent different promoters). Positive $E_{seg}$ values indicate the promoter prefers to remain in the bulk, whereas negative to segregate to the surface, reproduced from ref. 67 with the permission of AIP Publishing.

layer, similar segregation trends were found upon CO and OH adsorption (*e.g.*, OH drives the segregation of oxyphilic promoters like Al).

## Accelerated methods for modeling the stability of SAAs and DAs

ML has significantly advanced the study of SAAs by accelerating the prediction of formation energies,[68] $E_{seg}$,[69–71] and $E_{agg}$[72] with DFT-level accuracy. Thus far, predictive models have primarily focused on the effects of catalysis-relevant adsorbates, such as CO and H, on the segregation behavior.[71,73] For instance, Hipolito and coworkers[74] focused on identifying stable SAAs for ORR by developing a linear support vector machine regression model in the presence of O and OH groups.[74] However, one can view the SAA and DA NPs from two different perspectives, synthesis and applications, hence, the role of commonly used ligands in colloidal NP synthesis on the segregation behavior is also important. Work by Salem *et al.*[75] aimed to examine the effect of amine and thiol groups used in colloidal NP synthesis on $E_{seg}$ trends. They developed a NN multilayer perceptron model to predict $E_{seg}$ in

promoter–host metal combinations of $d^8$- (Ni, Pd, Pt) and $d^9$- (Ag, Au, Cu) SAAs on (100) and (111) facets, incorporating features that account for adsorbate effects ($E_{ads}$ on a single metal atom), structural effects (CN and atomic radius), electronic properties (electron affinity), and cohesion of metal in the bulk ($CE_{bulk}$) – inspired by the bond-centric model,[57] previously used to measure the thermodynamic stability in terms of the CE of multi-metallic NPs as a function of morphology and composition.

Similar features used by Salem *et al.*[76] in kernel ridge regression $E_{seg}$ model, trained on Pt-group metal (111), (100), (110), and (210) surfaces showed exceptional extrapolation capability to SAA NPs of varying sizes (147, 309, and 561 atoms), promoter positions (CN = 7, 8, and 9), and a metal host (Cu) that was not present in the model's training set (Fig. 4A). Similarly, Ghosh and coworkers[77] employed a random forest classifier to determine the chemical ordering in a 55-atom icosahedral binary-alloyed metallic NP consisting of wide range of metal groups, based on the change in the CE, radius, CN, and magnetism. Their model successfully determined core–shell preferences from mixed and Janus orderings, demonstrating the significance of these features in capturing the stability in SAAs.

While ML provides powerful tools for predicting $E_{seg}$ and $E_{agg}$ based on metal and adsorbate descriptors, it can also be used to rapidly explore the chemical ordering (*i.e.*, stability) in SAA and DA NPs as a function of morphology and composition through the use of genetic algorithms (GA) and further address temperature effects with MC simulations.[78–86] Since the CE of the metals and the exposed surface coordination have emerged as important descriptors of stability in SAAs and DAs, one can implement the bond-centric model[57] with a GA[80] to rapidly (*i.e.*, within minutes) predict the chemical ordering of SAA and DA NPs[80,81] (*i.e.* if a promoter metal will reside on the NP surface of the metal host and at what positions, Fig. 4B). Ter-Oganessian *et al.*[87] combined MD with MC simulations, using a precise ReaxFF potential, to effectively depict bulk and surface ordering, as well as shape restructuring in PdAu NPs at various compositions, temperatures, and NP sizes (Fig. 4C). They found that at low temperatures (20 K), $AuPd_{25}$ and $AuPd_{50}$ NPs formed bulk-ordered arrangements, contrasting with more disordered states at 1000 K. Additionally, they also observed that composition plays a role in the arrangement of Au and Pd, revealing that in the $AuPd_{25}$, $D0_{22}$ bulk order was formed, while $L1_2$ was observed in the $AuPd_{50}$ case (Fig. 4C). Compositional dependent chemical orderings on PdAu NPs have been also reported by Loevlie *et al.*[81] as well as Ekborg-Tanner and Erhart.[59]

## SAA and DA surface kinetics

In the formation of SAAs *via* vapor deposition, kinetics play a crucial role in determining the final structure and composition of the alloy. During vapor deposition, promoter atoms are deposited onto a host surface where they can diffuse and interact to form the alloy.[88] The kinetics of this process, including the rate of deposition, surface diffusion of atoms, and interactions
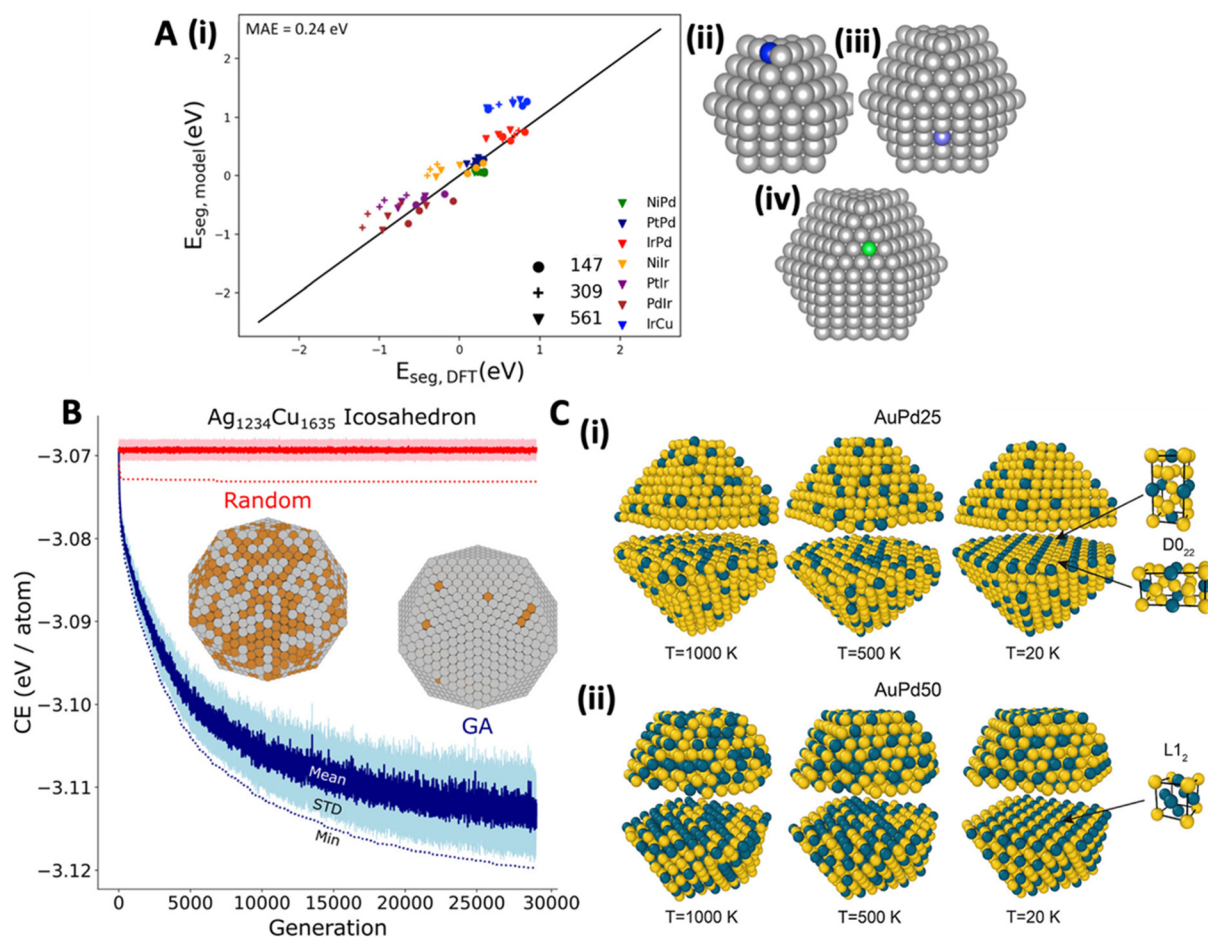
**Fig. 4** (A) (i) $E_{seg}$ predictions based on a five-feature, second order polynomial kernel ridge regression model for SAA NPs consisting of Pd, Ir, and Cu host metals. Marker styles represent the different NP sizes, while different colors represent the various SAA combinations; for instance, NiIr would indicate that Ni is the promoter and Ir is the host. Additionally, panels (ii) to (iv) illustrate the NP systems included in the extrapolation test, specifically, (ii) promoter on a CN = 7 (blue) site using 147-atom cuboctahedra, (iii) promoter on a CN = 8 (purple) site in a 309-atom cuboctahedra, and (iv) promoter on a CN = 9 (green) site in a 561-atom cuboctahedra, reproduced with permission from ref. 76. (B) Comparison between GA optimization and random search on an icosahedral $Ag_{1234}Cu_{1635}$ NP, represented by blue and red, respectively. The darker solid lines and lighter shaded areas show the mean and standard deviation for each generation, while dotted lines highlight the lowest CE at each generation, with the minimum CE structures illustrated in the figure, reproduced with permission from ref. 80, copyright 2020 American Chemical Society. (C) Chemical ordering of PdAu NPs as a function of temperature and composition (i) $AuPd_{25}$ and (ii) $AuPd_{50}$, reproduced with permission from ref. 87, copyright 2024 American Chemical Society.

between different species, significantly influence the formation of SAAs.[89] In this regard, Wang and coworkers[90] used DFT and scanning tunneling microscopy to study the different mechanisms (diffusion hoping, atomic exchange, vacancy formation, and atomic swapping; see Fig. 5A) occurring in Rh alloying on various Cu surfaces. They found that Rh atoms stay above step edges on Cu(111) and alloy directly into the terrace on Cu(100) and Cu(110). The lowest diffusion barrier for Rh was observed on Cu(111), while atomic exchange was favored on Cu(100) and Cu(110). Lower vacancy formation barriers on Cu(100), Cu(110), and Cu(211) compared to Cu(111) suggest that Rh atoms are kinetically trapped above step edges on Cu (111), while more readily integrating into the lattice on other surfaces, promoting the formation of SAAs (Fig. 5A). The impact of vacancies in the anchoring of SAA promoters has

also been investigated for other synthesis methods, including metal vacancies during galvanic replacement,[91] as well as O-vacancies during temperature annealing.[92]

In another study focusing on the segregation dynamics in NiCu(100) alloys during annealing, Garza et al.[93] performed several DFT-parametrized multiscale simulations (MD, parallel trajectory splicing, and kMC) to explore segregation across various timescales. MD simulations covered picosecond to nanosecond scales, revealing rapid vacancy diffusion and initial segregation patterns. To simulate longer timescales (up to microseconds), parallel trajectory splicing was used, which is crucial for understanding how vacancies reintegrate into the subsurface layers. kMC methods extended the analysis to second scales. The results showed that Ni migrates from the top layers during annealing, driven primarily by lattice
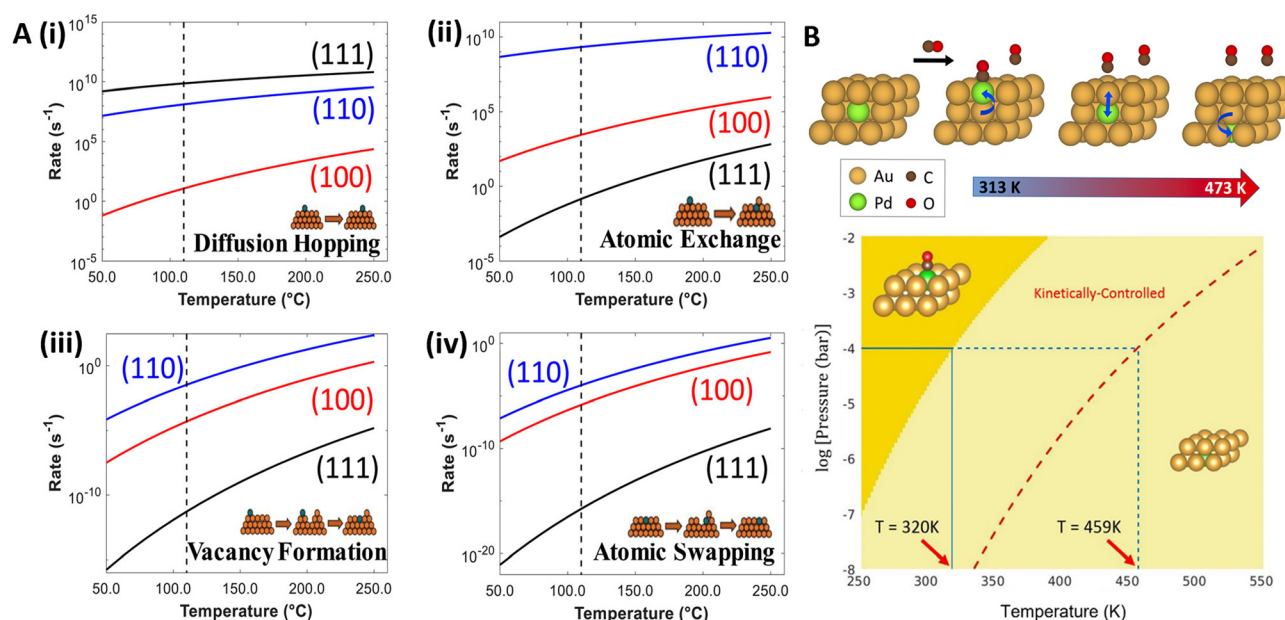
**Fig. 5** (A) Predicted rates under vacuum conditions for Cu-hosted Rh (i) hop diffusion, (ii) atomic exchange, (iii) vacancy formation (with a Rh adatom nearby), and (iv) atomic swapping, respectively, reproduced from ref. 90 with the permission of AIP Publishing. (B) DFT-constructed phase diagram, showing two phases: CO adsorption on Pd monomer (dark yellow) and subsurface Pd with no adsorption (light yellow). At the experimental CO pressure of 0.1 mbar, the thermodynamic transition, *i.e.*, CO desorption and Pd migrating to the subsurface, is expected to occur at 320 K (blue solid line); nonetheless, Pd remains kinetically trapped until a temperature of 459 K (blue dashed line) is reached, reproduced from ref. 94, copyright 2022 American Chemical Society.

vacancies. The alloy equilibrium composition that was reached within seconds, matched experimental observations with low Ni concentrations on the top layer and higher in the bulk.

The kinetics of surface segregation are also influenced by the presence of adsorbates. Zhou and coworkers[94] investigated the dynamics of surface restructuring in PdAu(111) induced by CO using experiments and DFT. At 0.1 mbar CO pressure, they observed that below 320 K, Pd monomers are stabilized on the surface by CO (Fig. 5B), which aligns with findings from Ouyang *et al.*[62] However, above 320 K, the entropic contribution of CO desorption leads to the dispersion of Pd into the subsurface as opposed to maintaining the Pd monomer on the surface, as indicated by the light-yellow region in Fig. 5B. In the kinetically influenced regime, bounded by the red dashed line, Pd monomers are trapped on the Au surface as CO desorption is unfavorable. This regime reflects the interplay of kinetic pathways influencing the persistence of CO-bound Pd monomers on the surface. Ultimately, above 459 K (dashed blue line in Fig. 5B), complete CO desorption occurs; thus, Pd is no longer favored at the surface, aligning with experimental findings. In related studies, Liu *et al.*[95] combined DFT with operando X-ray absorption fine structure spectroscopy to study the reconstruction of CuAu NP surfaces under electrochemical conditions, finding that isolated Cu atoms migrate from the corners to the (100) plane based on the reduced Cu–O CN (from 0.9 to 0.6) and higher Cu–Au CN (going from 5 to 8.3) under reduction potentials, impacting Cu–Au interactions.

## Advances in the design of SAA and DA catalysts

### Morphology effects on DA catalysis

A common assumption in the design of SAA catalysts is the facile spillover of reactants from promoter to host sites, where subsequent reaction steps occur. DFT calculations are usually limited to the most stable host facet (*e.g.*, (111) for fcc metals), neglecting the effects of surface coordination on the activity of host and promoter sites. To elucidate how surface coordination impacts the reactivity of Pt-group promoters on Cu-, Ag-, and Au-based SAAs, Papanikolaou *et al.*[48] compared the $E_{ads}$ of $N_2$, NO, and O on top of the promoter sites on the (100) and (111) facets (Fig. 6A). Contrary to the behavior observed on monometallic Pt-group metal surfaces, the SAA catalysts exhibited low structure sensitivity, as similar $E_{ads}$ were found on both facets. Remarkably, a systematic bias of ~0.1 eV favoring the less coordinated (100) facet was observed, attributed to differences in the electronic mixing of promoter and host atoms across facets. Similar trends were found for the dissociation barriers of NO, $CO_2$, and $N_2$, *i.e.*, small differences between the two SAA surfaces and lower $E_{act}$ on the (100) facet.

In a separate study, Jiang *et al.*[96] explored the effects of surface coordination on spillover hydrogenation reactions. Specifically, the partial hydrogenation of phenylacetylene (PhC≡CH) to styrene was investigated on the (100) and (111) facets of PdCu SAAs. Experiments revealed that hydrogen spillover from the Pd
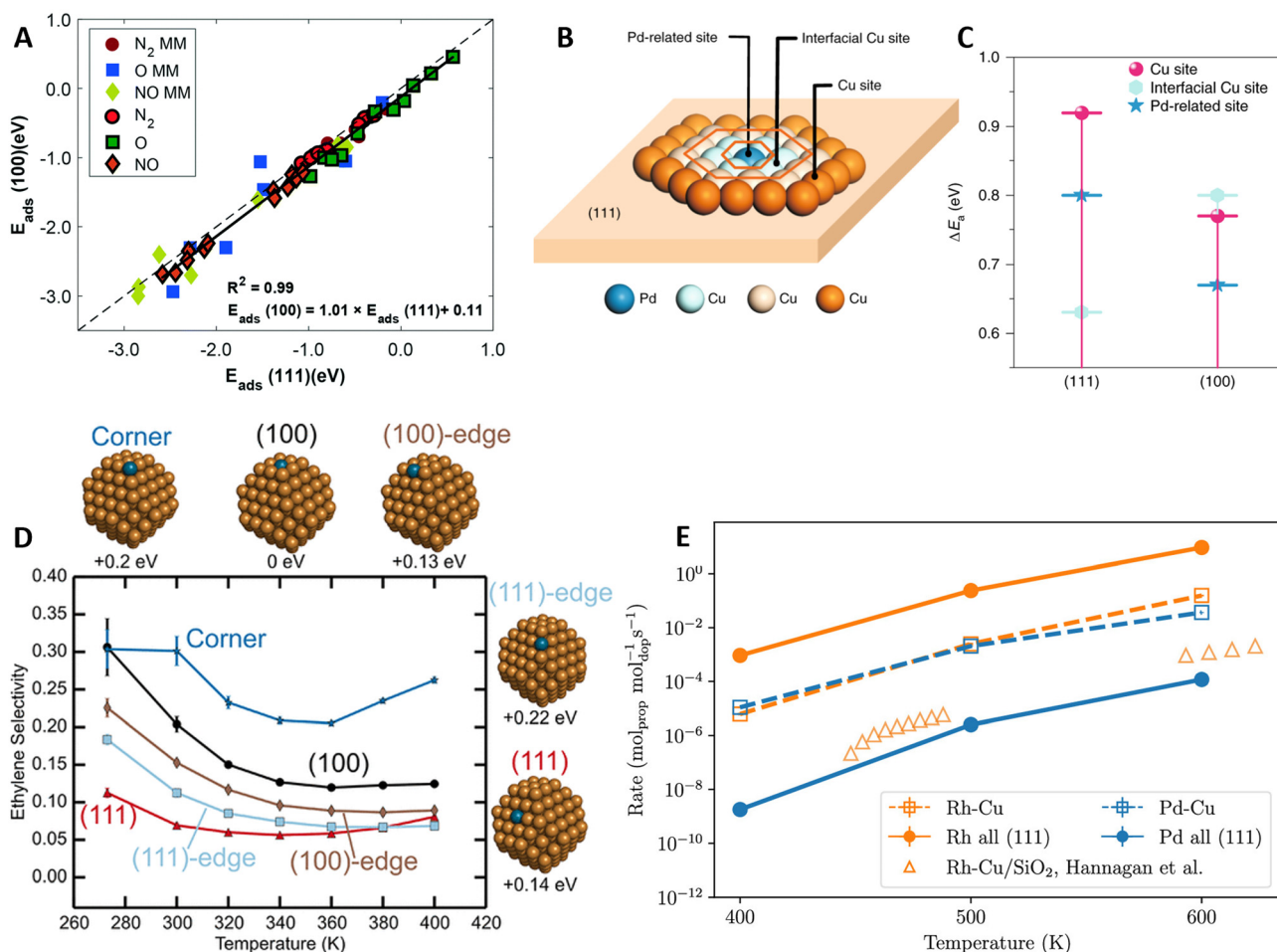
**Fig. 6** Coordination and NP shape effects in the catalytic activity of SAA and DAs. (A) Parity plot between the top-site NO, $N_2$, and O $E_{ads}$ computed on the (100) and (111) facets of SAA. For comparison, $E_{ads}$ on the preferred sites of the corresponding monometallic (MM: Pt, Pd, Rh, Ni, Ag, Au, and Cu) surfaces are included, reproduced from ref. 48 with permission from the Royal Society of Chemistry. (B) Different active sites investigated and (C) corresponding $E_{act}$ for the hydrogenation of phenylacetylene (PhC≡CH) into styrene on the (100) and (111) facets of PdCu SAA, reproduced from ref. 96 with permission of Springer Nature. (D) Selectivity changes for the partial hydrogenation of acetylene with the promoter location on PdCu SAA NPs (energies of the studied NPs relative to the minimum energy configuration are indicated below the particles), reproduced with permission from ref. 99, copyright 2019 American Chemical Society. (E) Changes in propane dehydrogenation activity with varying promoter locations, comparing RhCu and PdCu SAAs with promoters located on the (111) terrace sites (labeled "dopant all (111)"), vs. having the promoters on their most probable NP sites (labeled "dopant-Cu"), with theoretical results from ref. 101, reproduced with permission from ref. 100.

atoms into the Cu host was surface insensitive; however, the subsequent alkyne hydrogenation step was hindered on the (111) facet due to the low activity of the host sites. DFT-calculated PhC≡CH hydrogenation barriers (Fig. 6B and C) corroborated the experimental trends, with an $E_{act}$ of 0.92 eV on the Cu(111) facet compared to 0.77 eV on the (100) facet. Additionally, on the (111) facet, $E_{act}$ values were considerably lower close to the promoter (Pd sites and interfacial Cu sites), verifying that hydrogenation likely occurs in the vicinity of the Pd atoms, thus requiring higher Pd loadings compared to the (100) SAA.

Overall, the coordination of surface atoms is influenced by the morphology of the NP catalyst. Under reaction conditions, an ensemble of NP sizes and shapes is obtained, which can lead to variations in the catalytic activity compared to the most stable NP structure.[97] Furthermore, by pairing BEP relationships with kMC simulations, Jørgensen and Grönbeck[98] high-

lighted how the catalytic activity of NPs deviates from that of extended crystallographic planes due to kinetic couplings, i.e., the communication of different NP active sites through rapid adsorbate diffusion, which leads to non-linear additive rates. Focusing on the partial hydrogenation of acetylene into ethylene on a PdCu SAA, octahedral NPs exhibited considerably lower ethylene selectivity compared to the (111) extended surface (~100% selective).[99] Moreover, the predicted $C_2H_4$ selectivity varied based on the location of the Pd promoter on the NP (Fig. 6D), highlighting the importance of NP morphology in catalyst design.

Similarly, Bunting et al.[100] investigated how different promoter locations affect the propane dehydrogenation activity of RhCu and PdCu SAA NPs. Using a DFT-trained ML potential, MD simulations with transmutation MC swaps revealed that Rh favors bulk segregation, whereas Pd remains on the surface

of the NPs. Hence, although lower $E_{act}$ values were found on Rh sites compared to Pd, the larger amount of surface Pd sites led to comparable dehydrogenation rates between the two SAA NPs (Fig. 6E). It is worth noting that, for RhCu, the microkinetic modeling (mkm) predictions were higher compared to experimental rates from a separate study,[101] likely due to DFT limitations. Lastly, dehydrogenation rates were computed on idealized SAA NPs with the promoters on (111) terraces. For RhCu, this idealization resulted in a higher rate due to the higher presence of Rh atoms in the model surface, whereas, on PdCu, it underestimated the rate as less stable (but more reactive) facets were excluded from the mkm simulations.

### Designing DAs for thermal catalysis

Thermocatalytic applications of DAs have typically focused on selective (de)hydrogenation and oxidation reactions.[5,10] The design process often combines surface science experiments on well-defined surfaces, characterization and testing experiments on the synthesized catalyst, in addition to computational chemistry calculations using DFT and multiscale modeling techniques such as kMC or mkm. Recent examples include the role of hydrogen coverage on the selective (de)hydrogenation of ethyl ($C_2H_5$) over PtCu SAAs,[102] the isomerization of 1-hexene into 2-hexene on PdAu DAs,[103] the enhanced $H_2$ splitting on TiCu SAAs,[104] and the non-oxidative ethanol dehydrogenation on NiCu SAAs.[105]

Expanding on these applications, RuCo SAAs have been explored for Fischer–Tropsch synthesis[106–108] (FTS: $(2n + 1)H_2 + nCO \rightarrow C_nH_{2n+2} + nH_2O$) i.e., the polymerization of $CH_x$ groups into long-chain hydrocarbons.[109] This thermal process has potential applications in providing fuels for sectors difficult to electrify, such as aviation.[110] A current challenge in FTS for $CO_2$ utilization lies in separating the $CO_2$ effluent from the upstream reverse water gas shift step,[111–114] which can otherwise hydrogenate into methane.[115,116] In this context, temperature-programmed reactor studies by Liu et al.[107] demonstrated that RuCo SAAs can reactively separate CO from a 50/50 $CO/CO_2$ mixture via FTS at mild temperatures (Fig. 7A). DFT-computed $E_{ads}$ confirmed the SAA potential to separate the mixture, favoring CO chemisorption and limiting $CO_2$ to being physisorbed (Fig. 7B and C). Interestingly, Ru-promotion was not experimentally found to enhance the FTS activity or selectivity, which was verified by comparing the $E_{act}$ of various elementary steps on promoter and host sites. Instead, the role of the Ru atoms was found to maintain the catalyst in an active, reduced phase. Similar reducibility improvements (caused by an enhanced $H_2$ spillover) have been reported for PtNi SAAs,[117,118] demonstrating the capacity of promoters to minimize surface oxidation.

Concerning the role of support effects in DA catalysts, Guan et al.[119] highlighted how metal–support interactions between MXene and RuNi SAA NPs enhance the hydrolysis of ammonia-borane (AB: $NH_3BH_3$), resulting in uniquely higher activities compared to other RuNi SAAs, as well as MXene-supported Ru single-atom catalysts and NPs. DFT calculations confirmed that lower $E_{act}$ were found at the support-NP junc-

tion. Further Bader charge analysis revealed an electron distribution around the junction, resulting in an electron accumulation around interfacial Ru atoms, thereby favoring the binding and splitting of AB and $H_2O$. In a separate study on the hydrogenation of unsaturated aldehydes into unsaturated alcohols, Han et al.[120] showed how the Pt atoms of $Si_2O$-supported PtCu SAA NPs are stabilized at the inner metal–support interface. Remarkably, despite the Pt atoms not being exposed on the catalyst surface, experiments demonstrated that the PtCu NPs maintained a higher selectivity compared to the pure metals. The stability of the Pt atoms on the NP-support interface, due to the formation of Pt-Si bonds, was verified by DFT-computed formation energies of both free and supported $Cu_{24}Pt_1$ nanoclusters (Fig. 7D). Moreover, potential energy surface and $H_2$ $E_{act}$ calculations unveiled that, even when located two layers below the surface, the Pt atoms can modify the electronic properties of the Cu surface and enhance $H_2$ spillover.

Another key aspect in the design of DA catalysts is to identify the optimal promoter ensemble size. As previously discussed, promoter–promoter hybridization broadens and splits the d-states going from SAAs to DAs,[47,48] usually leading to higher activities at the expense of selectivity. In this context, several articles have investigated the ensemble size effects on the catalytic performance of PdAu DAs. For instance, in the selective hydrogenation of 1-hexyne into 1-hexene, experiments showed that isolated surface Pd atoms increase the activity of the Au host while maintaining a high selectivity.[121–123] However, high Pd loadings lead to the formation of Pd clusters, which decreases both activity and selectivity.[122,124] Using acetylene as a proxy to study the triple bond of 1-hexyne, Foucher et al.[124] performed DFT and mkm simulations on PdAu(111) DAs of increasing Pd-ensemble sizes (monomers, dimers, and trimers). Comparing the binding of hydrogenation reactants and intermediates, more exergonic Gibbs free energies of formation were found by increasing the ensemble size. Moreover, degree of rate control analysis showed hydrogen dissociation to be the rate-limiting step. Hence, as the cluster size increases, the adsorption of acetylene is enhanced, blocking the Pd sites for hydrogen spillover. This was reflected in the mkm-predicted reaction rates, as the rates of Pd dimers and trimers were 10% and 2%, respectively, of the rate of Pd monomers.

In a separate study on PdAu DAs, Kaiser et al.[125] tuned the Pd-ensemble size for benzaldehyde (PhCHO) hydrogenation to benzyl alcohol (BOH). Experiments identified an optimal hydrogenation selectivity on small clusters, around 10 and 12 at% of Pd (Fig. 7E). Isolated Pd atoms exhibited minimal activity in PhCHO hydrogenation, whereas large clusters led to the hydrogenolysis of the C–O bond and the production of toluene, decreasing selectivity to BOH. DFT calculations revealed an increase in the binding strength of PhCHO hydrogenation intermediates with the Pd ensemble size, as larger parts of the aromatic ring could be stabilized (Fig. 7F). Additionally, lower C–O dissociation $E_{act}$ were found by increasing the ensemble size, thereby explaining the selectivity
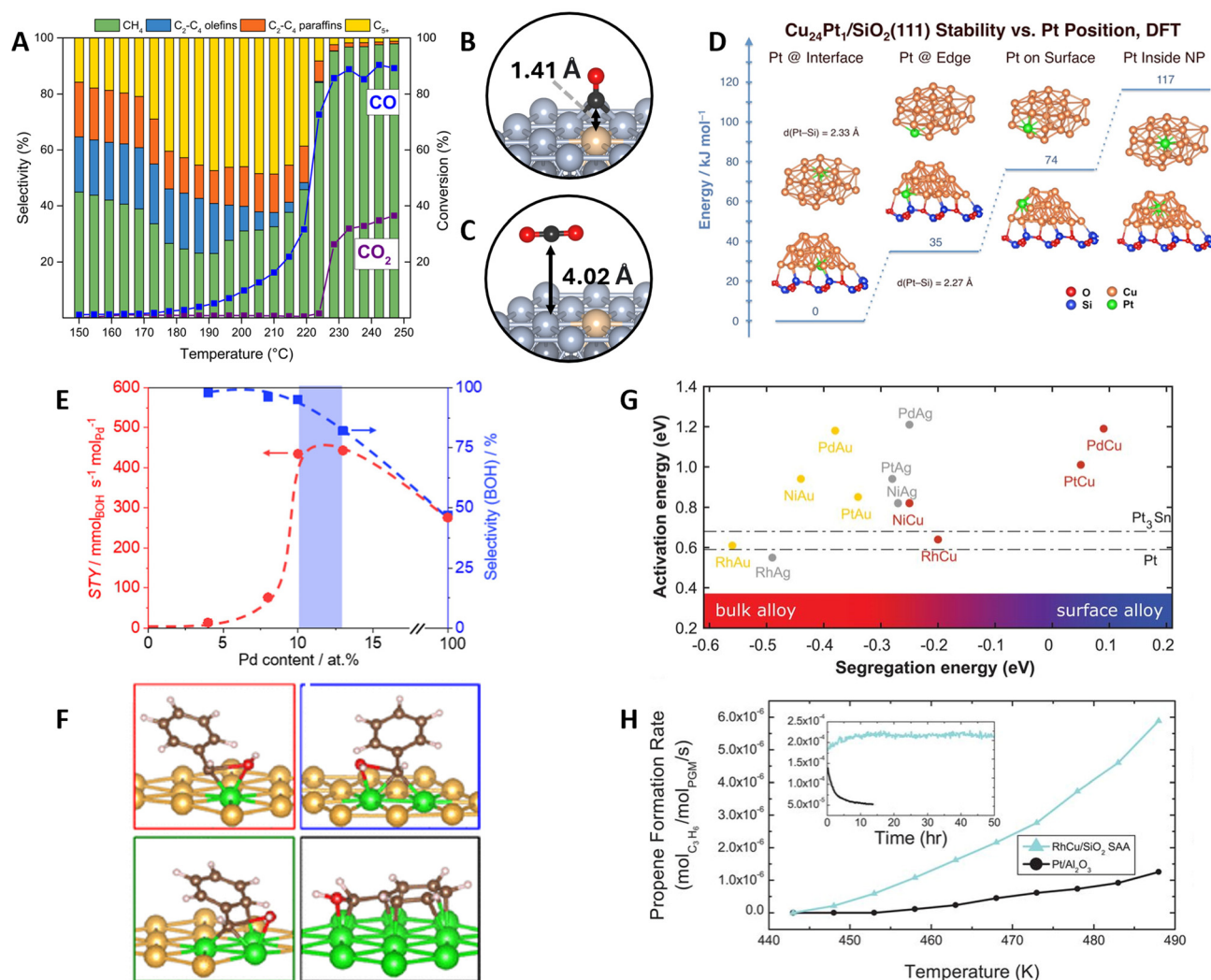
**Fig. 7** DA applications in heterogeneous thermal catalysis. (A) Programmed temperature reactor studies on the reactive separation of CO/CO$_2$ mixtures over RuCo SAA (reaction conditions: $P$ = 300 psig, H$_2$ : CO$_x$ ratio = 2.5 : 1, CO$_x$ = 50% CO/50% CO$_2$, GHSV = 84 000 mL h$^{-1}$ g$^{-1}$, $T$ = 150−250 °C, 10 °C h$^{-1}$). Side views and vertical distances for (B) CO and (C) CO$_2$ adsorption on the RuCo SAA surface, reproduced with permission from ref. 107. (D) DFT-calculated formation energies of Cu$_{24}$Pt$_1$ nanoclusters supported on SiO$_2$(111) showing the stabilization of the Pt promoter on the inner SAA-support interface, reproduced with permission from ref. 120. (E) Space−time yield (STY) and BOH selectivity as a function of Pd content on PdAu DAs (reaction conditions: $T$ = 323 K, $P$ = 5 bar, $F$(H$_2$) = 50 mL STP per min, $F$(BA) = 0.05 mL min$^{-1}$, $W_{cat}$ = 40 mg) and (F) changes in PhCHOH* C−O cleavage transition state over PdAu(111) DAs (Pd monomer, dimer, trimer) and Pd(111), reproduced with permission from ref. 125, copyright 2023 American Chemical Society. (G) Computational screening of SAA catalysts for nonoxidative propane dehydrogenation using the $E_{act}$ of the first C−H cleavage of CH$_4$ and the $E_{seg}$ as design parameters. Dash-dotted lines correspond to the $E_{act}$ on Pt(111) and Pt$_3$Sn(111) (2 × 2). (H) Reactor studies comparing the selected RhCu/SiO$_2$ SAA catalyst with Pt/Al$_2$O$_3$ (reaction conditions: 1.4 kPa of propane and 0.7 kPa of hydrogen; 90 mL min$^{-1}$ flow rate. Formation rate was normalized per mole of Pt-group metal). The figure inset corresponds to the stability test performed for 50 h at $T$ = 623 K, reproduced from ref. 101 with permission of the American Association for the Advancement of Science.

decline at higher Pd loadings. Other studies on promoter ensemble size effects include the tuning of NiAu and NiCu DAs for ethanol dehydrogenation[126] and N$_2$O decomposition,[127] respectively, as well as TiCu DAs for ethanol deoxygenation into ethylene[128] and MoNi DAs for the hydrodeoxygenation of furfural into 2-methyl furan.[129]

Moving beyond the experimental design, historically driven by chemical intuition and reliant on trial-and-error testing, the advances in high-throughput computational chemistry calculations have enabled the *in silico* design of SAA and DA cata-

lysts.[130] Through DFT-derived LSR and mkm, Zhang *et al.*[131] screened DA catalysts featuring Ag and Cu hosts, as well as TM promoter monomers and dimers for ammonia synthesis. The formation energy of N* was used as a descriptor for the LSRs, which were paired with mkm to predict turnover frequencies. Overall, higher turnover frequencies for ammonia synthesis were found on promoter dimers compared to monomers, as ensemble effects facilitate the rate-limiting N$_2$ dissociation. Hence, the predicted turnover frequency of the best-performing DA (MoAg, having Mo dimers) was three orders of magni-

tude higher compared to the best-performing SAA (NbAg). Remarkably, the predicted activity of the MoAg DA catalyst surpassed that of commercial Ru catalysts. The stability of the top-performing catalysts was verified through a combination of formation energy calculations, diffusion barrier calculations for promoter migration to subsurface and adatom sites, and *ab initio* MD simulations. Similar work involves the screening of SAA and DAs for (de)hydrogenation reactions,[132,133] methane dry reforming,[134] direct oxidation into methanol,[135] and hydrodeoxygenation reactions for bio-oil upgrading.[136,137]

A great example of simulations leading to experimental validation is from Hannagan *et al.*[101] on designing SAA catalysts for non-oxidative propane dehydrogenation. SAAs consisting of coinage-metal hosts (Au, Cu, Ag) and Pt-group metal promoters were screened based on their segregation trends and methane C–H dissociation activity (Fig. 7G). Among these, RhCu was selected as it showed a low C–H dissociation barrier comparable to industrial Pt and $Pt_3Sn$ catalysts, and the most favorable $E_{seg}$ among the Rh-promoted SAAs. Further analysis of the energetics for the full dehydrogenation of methane unveiled similar activities between RhCu SAA and Pt, but a weaker binding of coke-related intermediates ($CH_2$ and CH) on the SAA. Subsequent reactor experiments demonstrated higher propane dehydrogenation rates and coking resistance on $RhCu/SiO_2$ SAA compared to $Pt/Al_2O_3$ (Fig. 7H). Moreover, the SAA maintained a Cu-like selectivity of 100% compared to ~80% on the Pt catalyst.

## SAA application in photo- and electrochemistry

Amidst the ongoing efforts to decarbonize the chemical industry through process electrification,[138,139] SAAs have emerged as promising candidates to replace traditional noble metal electrode catalysts.[140,141] In this context, DFT calculations have provided valuable insights into catalytic activity and selectivity through the computational hydrogen electrode approximation,[142,143] which enables mapping the influence of externally applied potentials on the reaction free energies of elementary steps that include the transfer of a proton–electron pair.

In this way, DFT screening has been used to tune the selectivity of Cu-based alloys for $CO_2$ electrochemical reduction reaction ($CO_2RR$), as Cu is the only known metal catalyst to form $C_{2+}$ products.[144] By comparing the stability of $CO_2RR$ intermediates on twelve Cu(111)-based SAAs, Zhi *et al.*[145] found the O* and H* formation energies on the promoter site to describe the selectivity toward $C_1$ products requiring two electron-transfer steps (HCOOH/CO) or more ($CH_4$/ $CH_3OH$), in addition to $C_{2+}$ products (Fig. 8A). The changes in selectivity were explained by the electronic structure of the SAA catalysts, as the O* and H* formation free energies correlate with the d-band center of the promoter atoms. Later work by Jiang *et al.*[146] explored the changes in $C_1$-product selectivity of Cu(111)-based SAAs promoted with 3d TMs. Except for the late TMs, the investigated SAAs were found to activate $CO_2$. Moreover, the OH* formation free energy was found to describe the reaction free energies of common potential-deter-
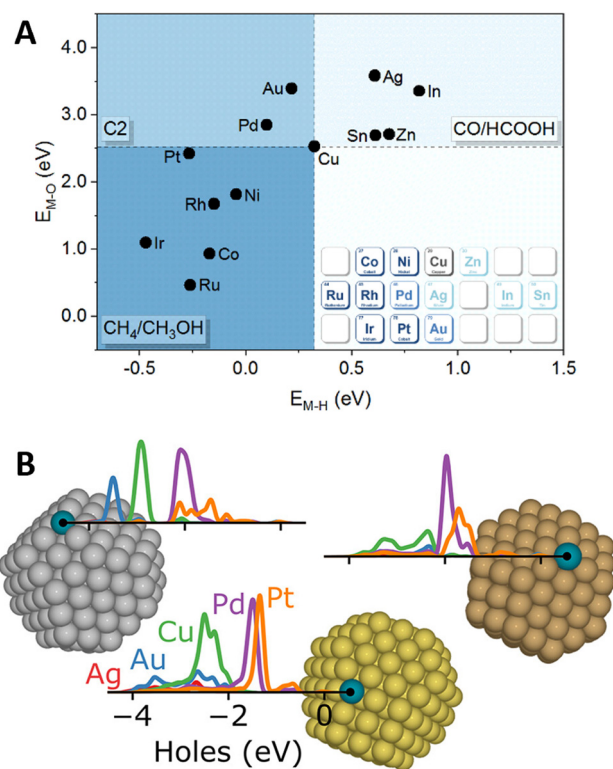


Fig. 8 Novel SAA applications in electrocatalysis and photocatalysis. (A) Favored electrocatalysis products of Cu-based SAAs based on formation free energies of O* (M−O) and H* (M−H) on the promoter site, reproduced from the Lancet (ref. 145) with permission from Elsevier. (B) Illustration highlighting the localized hot-hole distributions projected on the promoter atoms (labeled on the figure) of (from left to right) Ag, Au, and Cu NPs, reproduced with permission from ref. 154.

mining steps. Cu-based SAAs have also been explored for other reduction reactions, including the design of a WCu SAA catalyst for the co-reduction of $CO_2$ and $N_2$ to produce acetamide,[147] as well as, a PdCu SAA for the reduction of nitrate[148] and nitric oxide[149] to ammonia. Lastly, interested readers in broader electrochemical applications are encouraged to consider additional DFT and experimental work on the design of SAA catalysts for fuel cell applications[150–152] and $Li_2O_2$ battery electrodes.[153]

In the field of photocatalysis, SAAs have been investigated both as plasmonic catalysts and as co-catalysts for semiconductor materials. Addressing the role of promoters (Ag, Au, Cu, Pd, and Pt) in the plasmonic hot-carrier generation of Ag-, Au- and Cu-based SAAs, Sorvisto *et al.*[154] modeled the plasmonic-catalytic properties of 201-atom octahedral NPs (having one promoter atom on a facet or corner site) using time-dependent DFT. Although the promoters did not affect the overall plasmonic response of the NPs, local changes were observed. By analyzing the hot-carrier distributions projected on the promoter sites, the localized promoter states were found to lead to peaked hot-hole distributions (Fig. 8B), with less impact on the distribution of hot electrons. The local hot-hole distributions were further found to change with the location of the

promoter atoms on the NP (corner *vs.* terrace) and the NP size, when performing additional calculations on 309-atom Ag NPs (icosahedral and octahedral). Besides modifying local hot-carrier distributions, promoter atoms can facilitate elementary steps, boosting the overall plasmonic-catalyzed rates (*i.e.*, "antenna-reactor" catalysts). For example, Lu *et al.*[155] paired experiments with DFT calculations and unveiled the role of Co promoters in the activity of CoCu SAAs for the light-driven production of hydrogen from methanol and water.

Regarding the use of SAAs as co-catalysts, Wang *et al.*[156] showed that AuAg SAAs enhanced the photo-oxidative coupling of methane into ethane over ZnO. Experiments demonstrated a higher activity of the SAA catalyst compared to Au and Ag NPs. Moreover, Au-loading tests revealed a uniquely high activity of isolated Au atoms in contrast to Au ensembles. DFT-calculated reaction energetics shed light on the synergy between the Ag host, relevant for $*CH_3$ coupling, and the electron-deficient Au isolated atoms. The latter were found to facilitate the diffusion of $*CH_3$ on the SAA NP, as well as the production of the $*OOH$ intermediate, critical for the C–H activation of methane. Analogous work by Pan *et al.*[157] developed a PdPt SAA co-catalyst for photocatalytic water splitting over UiO-66-$NH_2$ metal–organic frameworks, exhibiting a higher $H_2$ production rate compared to PdPt intermetallic alloys.

### ML screening of novel catalysts

The increasing momentum in the development of ML is revolutionizing the screening of heterogeneous catalysts while holding the promise of dramatically reducing if not replacing the computationally intense DFT calculations in the future.[158–160] In the field of SAAs, various ML regression models (mostly gradient-boosted trees) have been recently trained from DFT data to predict $E_{ads}$ and $E_{act}$ with high accuracy.[73,161–168] Nonetheless, the two obstacles hindering the screening of heterogeneous catalysts with ML are the limited amount of available training data and the high computational cost of generating the data.[169,170] A solution to this can be found in active learning models, which identify the most informative data points to test (*e.g.*, with select DFT calculations) and incorporate them into the model's training set, thereby iteratively improving the screening process.[169,170]

In this regard, Kayode *et al.*[171] benchmarked the efficiency of Bayesian optimization in screening SAAs for alkane conversions and $CO_2RR$, as well as bimetallic alloys for HER. In all cases, the $E_{ads}$ of activity descriptors were used as targets. Gaussian process regression was chosen for the surrogate model, used to identify (through an acquisition function) the promoter–host combinations with the highest improvements. After initializing the algorithm with a random set of catalysts, it iteratively tested and learned from promising candidates until an optimal $E_{ads}$ was found (or equivalently, an iteration threshold was reached). The algorithm identified HfCu SAA for alkane transformations, Y-promoted Ag, Cu, and Ag SAAs for $CO_2RR$, and intermetallic AgIr for HER. Moreover, the algorithm was both efficient, requiring substantially fewer DFT calculations compared to random search, and robust, as vari-

ations in the features or the initial random sample resulted in similar numbers of iterations. A different study by Feng *et al.*[172] also leveraged an active learning framework to screen across the (111), (100), (110), and (320) facets of Au, Ag, and Cu-based SAAs for the selective hydrogenation of crotonaldehyde into crotyl alcohol. The top performing TiAu(320) and (111) SAA surfaces were further investigated using mkm, corroborating their high selectivity and near 100% conversion.

## Conclusion and outlook

DAs and SAAs have gained tremendous attention over the years due to their distinct properties, leading to enhanced catalytic performance. In this minireview, we reviewed how electronic structure, thermodynamics and kinetics affect the stability and catalytic behavior of DAs and SAAs using DFT, multi-scale modeling, and ML. Regarding their stability, we specifically highlighted that the promoter–adsorbate interactions and external fields can alter the segregation and aggregation behavior in SAAs. Additionally, we discussed how kinetics may impose different stability trends compared to thermodynamics leading to metastable structures. We then dived into recent applications of ML in predicting the stability of DAs and SAAs, highlighting the emergence of physicochemical descriptors that dictate the segregation and aggregation trends. Regarding catalytic applications we discussed how the activity of DAs and SAAs is determined by the NP morphology, promoter ensembles, and surface coordination. Furthermore, we presented thermo-, electro-, and photocatalytic applications, extending beyond the spillover hydrogenation reactions commonly investigated on SAAs. The integration of computational chemistry with ML has paved the way in the accelerated screening of DA and SAA catalysts. Looking forward, we present an outlook emphasizing on the importance of using transfer learning to accurately capture adsorbate configurations in SAAs and DAs and understanding the implications of dual atom alloys (DAAs) emerging from the presence of two different heteroatom promoters on a single host metal.

### Improving ML predictions through accurate adsorbate configuration representations

Although great progress has been made in ML-predicted $E_{ads}$ in SAA and DA catalysts, solely relying on surface-level features can result in significant prediction errors due to the diverse binding configurations of adsorbates.[162,163] In this regard, graph-based models offer an alternative solution by accurately representing adsorbate configurations, which can then be used to compute the energy and forces of a given state. These can then be fed into an optimization algorithm (*e.g.*, BFGS[173]) to find the most stable adsorption configuration. However, given the limited configuration space for SAAs (compared to bimetallic catalysts of various compositions), training complex models directly on this data can be challenging. Recent progress in developing graph-based models for intermetallic catalysts, especially in transfer learning algorithms (in which the

weights of a model trained on an analogous dataset are fine-tuned with new data) is promising to reduce the amount of training data needed.[174] In this sense, the pre-trained weights, which capture general trends, can be fine-tuned to adapt to a new target.[175] Such approaches have been used to predict materials properties using graph convolutional networks[176] as well as XGBoost regression in bimetallic alloys (including SAAs).[177] For instance, the EquiformerV2 model, trained on the Open Catalyst Project database,[178] has been successfully extended to predict $E_{ads}$ of OH and O on high-entropy Ag–Ir–Pd–Pt–Ru alloys.[179] Hence, we envision that similar extensions could be applied using other graph-based models within the context of SAA and DAs.

### Dual-atom alloy catalysts and systems with isolated active sites

The great advancements made in understanding the behavior and applications of SAAs and DAs have paved the way for exploring more complex systems, such as DAAs (*i.e.*, trimetallic systems where one metal acts as the host and the other two metals act as promoters). These systems provide additional tunability and unique properties due to the interactions between two different active sites,[180] leading to enhanced performance in catalytic applications such as ethanol dehydrogenation[181] and urea electrosynthesis from nitrate and carbon dioxide.[182] However, they encounter great challenges in their synthesis.

Extending insights from SAAs to DAAs, Zhang, and co-workers[180] employed DFT to reveal that while SAAs display free-atom-like electronic states, DAAs show hybridization of these states, forming molecular-like states. This hybridization occurs from the interaction of the promoter atoms in the DAA, resulting in new electronic properties that are absent in SAAs (the latter presented in Fig. 2A). In addition to DFT, MD simulations along with multi-scale modeling, such as mkm and kMC, have been used to examine the dynamic behavior of SAAs and DAs under various conditions such as temperature, pressure, and in the presence of adsorbates. These tools provide valuable insights into the mobility of the active sites, which in turn affects their catalytic performance. The use of ML, which has opened new avenues in accelerating the screening of SAA and DA catalysts by predicting properties such as $E_{seg}$ and $E_{ads}$, can further enhance the efficiency and accuracy of identifying promising DAA catalysts in terms of their stability and catalytic activity. As a final take-home message, the complexity of SAAs and DAs can increase by changing the number of different metal promoters and designing novel nanocatalyst architectures. However, one must be very careful with the material limit (*e.g.* metal composition, ensemble sizes, *etc.*) where these systems lose their unique electronic structure and start resembling the behavior of bimetallic and/or multimetallic systems. In this regard, simulation strategies for SAA and DA screening for catalytic applications (and beyond) should be developed on systems that exhibit these unique electronic properties and the latter should be integrated as critical information on optimizing the application performance.

## Data availability

No primary research results, software or code have been included and no new data were generated or analysed as part of this review.

## Conflicts of interest

There are no conflicts to declare.

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## References

1 Y. Nakaya and S. Furukawa, *Chem. Rev.*, 2023, **123**, 5859–5947.

2 W. M. H. Sachtler and R. A. V. Santen, in *Advances in Catalysis*, ed. D. D. Eley, H. Pines and P. B. Weisz, Academic Press, 1977, vol. 26, pp. 69–119.

3 H. C. de Jongste and V. Ponec, *J. Catal.*, 1980, **63**, 389–394.

4 E. Iglesia, S. L. Soled, R. A. Fiato and G. H. Via, *J. Catal.*, 1993, **143**, 345–368.

5 J. D. Lee, J. B. Miller, A. V. Shneidman, L. Sun, J. F. Weaver, J. Aizenberg, J. Biener, J. A. Boscoboinik, A. C. Foucher, A. I. Frenkel, J. E. S. van der Hoeven, B. Kozinsky, N. Marcella, M. M. Montemore, H. T. Ngan, C. R. O'Connor, C. J. Owen, D. J. Stacchiola, E. A. Stach, R. J. Madix, P. Sautet and C. M. Friend, *Chem. Rev.*, 2022, **122**, 8758–8808.

6 M. Luneau, J. S. Lim, D. A. Patel, E. C. H. Sykes, C. M. Friend and P. Sautet, *Chem. Rev.*, 2020, **120**, 12834–12872.

7 H. L. Tierney, A. E. Baber, J. R. Kitchin and E. C. H. Sykes, *Phys. Rev. Lett.*, 2009, **103**, 246102.

8 G. Kyriakou, M. B. Boucher, A. D. Jewell, E. A. Lewis, T. J. Lawton, A. E. Baber, H. L. Tierney, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Science*, 2012, **335**, 1209–1212.

9 G. Giannakakis, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Acc. Chem. Res.*, 2019, **52**, 237–247.

10 R. T. Hannagan, G. Giannakakis, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Chem. Rev.*, 2020, **120**, 12044–12088.

11 M. T. Darby, M. Stamatakis, A. Michaelides and E. C. H. Sykes, *J. Phys. Chem. Lett.*, 2018, **9**, 5636–5646.

12 M. T. Darby, R. Réocreux, E. C. H. Sykes, A. Michaelides and M. Stamatakis, *ACS Catal.*, 2018, **8**, 5038–5050.

13 W. Li, S. E. Madan, R. Réocreux and M. Stamatakis, *ACS Catal.*, 2023, **13**, 15851–15868.

14 V. Pallassana and M. Neurock, *J. Catal.*, 2000, **191**, 301–317.

15 Z.-P. Liu and P. Hu, *J. Chem. Phys.*, 2001, **114**, 8244–8247.

16 A. Logadottir, T. H. Rod, J. K. Nørskov, B. Hammer, S. Dahl and C. J. H. Jacobsen, *J. Catal.*, 2001, **197**, 229–231.

17 T. Bligaard, J. K. Nørskov, S. Dahl, J. Matthiesen, C. H. Christensen and J. Sehested, *J. Catal.*, 2004, **224**, 206–217.

18 J. Greeley, *Annu. Rev. Chem. Biomol. Eng.*, 2016, **7**, 605–635.

19 F. Abild-Pedersen, J. Greeley, F. Studt, J. Rossmeisl, T. R. Munter, P. G. Moses, E. Skúlason, T. Bligaard and J. K. Nørskov, *Phys. Rev. Lett.*, 2007, **99**, 016105.

20 M. M. Montemore and J. W. Medlin, *Catal. Sci. Technol.*, 2014, **4**, 3748–3761.

21 B. Hammer and J. K. Nørskov, *Surf. Sci.*, 1995, **343**, 211–220.

22 B. Hammer and J. K. Norskov, *Nature*, 1995, **376**, 238–240.

23 B. Hammer and J. K. Nørskov, in *Advances in Catalysis*, Academic Press, 2000, vol. 45, pp. 71–129.

24 K. G. Papanikolaou, M. T. Darby and M. Stamatakis, *J. Phys. Chem. C*, 2019, **123**, 9128–9138.

25 Q. Fu and Y. Luo, *J. Phys. Chem. C*, 2013, **117**, 14618–14624.

26 M. T. Darby, E. C. H. Sykes, A. Michaelides and M. Stamatakis, *Top. Catal.*, 2018, **61**, 428–438.

27 M. D. Marcinkowski, A. D. Jewell, M. Stamatakis, M. B. Boucher, E. A. Lewis, C. J. Murphy, G. Kyriakou and E. C. H. Sykes, *Nat. Mater.*, 2013, **12**, 523–528.

28 M. T. Darby, F. R. Lucci, M. D. Marcinkowski, A. J. Therrien, A. Michaelides, M. Stamatakis and E. C. H. Sykes, *J. Phys. Chem. C*, 2019, **123**, 10419–10428.

29 P. Kress, R. Réocreux, R. Hannagan, T. Thuening, J. A. Boscoboinik, M. Stamatakis and E. C. H. Sykes, *J. Chem. Phys.*, 2021, **154**, 204701.

30 S. Simpson, *JCIS Open*, 2021, **3**, 100013.

31 K. Gu, F. Wei, Y. Cai, S. Lin and H. Guo, *J. Phys. Chem. Lett.*, 2021, **12**, 8423–8429.

32 K. Gu, C. Li, B. Jiang, S. Lin and H. Guo, *J. Phys. Chem. C*, 2022, **126**, 17093–17101.

33 K. Gu and S. Lin, *Angew. Chem., Int. Ed.*, 2023, **62**, e202312796.

34 B. Geng, L. Zhang, F. Wang, X. Wang, S. Song and H. Zhang, *Eur. J. Inorg. Chem.*, 2023, **26**, e202300052.

35 J. Mao, J. Yin, J. Pei, D. Wang and Y. Li, *Nano Today*, 2020, **34**, 100917.

36 T. Zhang, A. G. Walsh, J. Yu and P. Zhang, *Chem. Soc. Rev.*, 2021, **50**, 569–588.

37 H. Thirumalai and J. R. Kitchin, *Top. Catal.*, 2018, **61**, 462–474.

38 M. T. Greiner, T. E. Jones, S. Beeg, L. Zwiener, M. Scherzer, F. Girgsdies, S. Piccinin, M. Armbrüster, A. Knop-Gericke and R. Schlögl, *Nat. Chem.*, 2018, **10**, 1008–1015.

39 C. Hartwig, K. Schweinar, T. E. Jones, S. Beeg, F.-P. Schmidt, R. Schlögl and M. Greiner, *J. Chem. Phys.*, 2021, **154**, 184703.

40 J. K. Nørskov, F. Abild-Pedersen, F. Studt and T. Bligaard, *Proc. Natl. Acad. Sci. U. S. A.*, 2011, **108**, 937–943.

41 L. G. M. Pettersson and A. Nilsson, *Top. Catal.*, 2014, **57**, 2–13.

42 F. R. Lucci, J. Liu, M. D. Marcinkowski, M. Yang, L. F. Allard, M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Nat. Commun.*, 2015, **6**, 8550.

43 M. J. Islam, M. Granollers Mesa, A. Osatiashtiani, J. C. Manayil, M. A. Isaacs, M. J. Taylor, S. Tsatsos and G. Kyriakou, *Appl. Catal., B*, 2021, **299**, 120652.

44 T. D. Spivey and A. Holewinski, *J. Am. Chem. Soc.*, 2021, **143**, 11897–11902.

45 H. T. Ngan and P. Sautet, *J. Am. Chem. Soc.*, 2024, **146**, 2556–2567.

46 V. Fung, G. Hu and B. Sumpter, *J. Mater. Chem. A*, 2020, **8**, 6057–6066.

47 A. P. Monasterial, C. A. Hinderks, S. Viriyavaree and M. M. Montemore, *J. Chem. Phys.*, 2020, **153**, 111102.

48 K. G. Papanikolaou and M. Stamatakis, *Catal. Sci. Technol.*, 2020, **10**, 5815–5828.

49 T. Dai, Z. Wang, X. Lang and Q. Jiang, *J. Mater. Chem. A*, 2022, **10**, 16900–16907.

50 J. Schumann, M. Stamatakis, A. Michaelides and R. Réocreux, *Nat. Chem.*, 2024, **16**, 749–754.

51 J. Schumann, Y. Bao, R. T. Hannagan, E. C. H. Sykes, M. Stamatakis and A. Michaelides, *J. Phys. Chem. Lett.*, 2021, **12**, 10060–10067.

52 R. Réocreux, E. C. H. Sykes, A. Michaelides and M. Stamatakis, *J. Phys. Chem. Lett.*, 2022, **13**, 7314–7319.

53 R. T. Hannagan, H. Y. Lam, R. Réocreux, Y. Wang, A. Dunbar, V. Lal, V. Çınar, Y. Chen, P. Deshlahra, M. Stamatakis, N. M. Eagan and E. C. H. Sykes, *J. Phys. Chem. Lett.*, 2023, **14**, 10561–10569.

54 L. Farsi and N. A. Deskins, *Phys. Chem. Chem. Phys.*, 2019, **21**, 23626–23637.

55 Y. Xu, G. Wang, P. Qian and Y. Su, *J. Mater. Sci.*, 2022, **57**, 7384–7399.

56 K. G. Papanikolaou, M. T. Darby and M. Stamatakis, *ACS Catal.*, 2020, **10**, 1224–1236.

57 Z. Yan, M. G. Taylor, A. Mascareno and G. Mpourmpakis, *Nano Lett.*, 2018, **18**, 2696–2704.

58 J. Yin, M. Ehara and S. Sakaki, *Phys. Chem. Chem. Phys.*, 2022, **24**, 10420–10438.

59 P. Ekborg-Tanner and P. Erhart, *J. Phys. Chem. C*, 2021, **125**, 17248–17260.

60 Q. Wang, B. Zhu, F. Tielens, D. Tichit and H. Guesmi, *Appl. Surf. Sci.*, 2021, **548**, 149217.

61 Y. Yu, Z. Liu, W. Huang, S. Zhou, Z. Hu and L. Wang, *J. Phys. Chem. Solids*, 2022, **171**, 111021.

62 M. Ouyang, K. G. Papanikolaou, A. Boubnov, A. S. Hoffman, G. Giannakakis, S. R. Bare, M. Stamatakis,

M. Flytzani-Stephanopoulos and E. C. H. Sykes, *Nat. Commun.*, 2021, **12**, 1549.

63 G. Agrahari, A. Sarkar and A. Chatterjee, *Effect of Solvent on Segregation Behavior in Pt-Ni Bimetallic Alloy*, Singapore, 2020.

64 W. Li, M. G. Taylor, D. Bayerl, S. Mozaffari, M. Dixit, S. Ivanov, S. Seifert, B. Lee, N. Shanaiah, Y. Lu, L. Kovarik, G. Mpourmpakis and A. M. Karim, *Nanoscale*, 2021, **13**, 206–217.

65 S. V. Doronin, *Mendeleev Commun.*, 2020, **30**, 288–290.

66 J. S. Jirkovsky, I. Panas, S. Romani, E. Ahlberg and D. J. Schiffrin, *J. Phys. Chem. Lett.*, 2012, **3**, 315–321.

67 S. E. Weitzner, S. A. Akhade, A. R. Kashi, Z. Qi, A. K. Buckley, Z. Huo, S. Ma, M. Biener, B. C. Wood, K. P. Kuhl, J. B. Varley and J. Biener, *J. Chem. Phys.*, 2021, **155**, 114702.

68 K. K. Rao, Q. K. Do, K. Pham, D. Maiti and L. C. Grabow, *Top. Catal.*, 2020, **63**, 728–741.

69 D. Ologunagba and S. Kattel, *Energies*, 2020, **13**, 2182.

70 D. Shin, G. Choi, C. Hong and J. W. Han, *Mol. Catal.*, 2023, **541**, 113096.

71 G. A. Sulley, J. Hamm and M. M. Montemore, *JPhys Energy*, 2023, **5**, 015002.

72 Z. Lu, S. Yadav and C. V. Singh, *Catal. Sci. Technol.*, 2020, **10**, 86–98.

73 Z.-K. Han, D. Sarker, R. Ouyang, A. Mazheika, Y. Gao and S. V. Levchenko, *Nat. Commun.*, 2021, **12**, 1833.

74 A. N. P. Hipolito, M. A. Palmero, V. Z. Ordillo, K. Shimizu, D. B. Putungan, A. B. Santos-Putungan, J. D. Ocon, S. Watanabe, K. E. S. Pilario and A. A. B. Padama, *Comput. Mater. Sci.*, 2024, **232**, 112607.

75 M. Salem, D. J. Loevlie and G. Mpourmpakis, *J. Phys. Chem. C*, 2023, **127**, 22790–22798.

76 M. Salem, M. J. Cowan and G. Mpourmpakis, *ACS Omega*, 2022, **7**, 4471–4481.

77 A. Ghosh, S. Datta and T. Saha-Dasgupta, *J. Phys. Chem. C*, 2022, **126**, 6847–6853.

78 S. Han, G. Barcaro, A. Fortunelli, S. Lysgaard, T. Vegge and H. A. Hansen, *npj Comput. Mater.*, 2022, **8**, 121.

79 Y. Yang, Z. Zhao, J. Zhu and D. Cheng, *J. Cluster Sci.*, 2020, **31**, 609–614.

80 J. Dean, M. J. Cowan, J. Estes, M. Ramadan and G. Mpourmpakis, *ACS Nano*, 2020, **14**, 8171–8180.

81 D. J. Loevlie, B. Ferreira and G. Mpourmpakis, *Acc. Chem. Res.*, 2023, **56**, 248–257.

82 J. Jung, S. Ju, P.-H. Kim, D. Hong, W. Jeong, J. Lee, S. Han and S. Kang, *ACS Catal.*, 2023, **13**, 16078–16087.

83 A. Front and C. Mottet, *Theor. Chem. Acc.*, 2021, **141**, 2.

84 M. Hua, X. Tian, S. Li, A. Shao and X. Lin, *Phys. Chem. Chem. Phys.*, 2022, **24**, 19488–19501.

85 K. Yun, H.-S. Nam and S. Kim, *Phys. Chem. Chem. Phys.*, 2020, **22**, 7787–7793.

86 M. Hua, X. Tian, S. Li, X. Zhang, A. Shao, L. Song and X. Lin, *Phys. Chem. Chem. Phys.*, 2022, **24**, 2251–2264.

87 N. V. Ter-Oganessian, Y. V. Rusalev, A. V. Motseyko, A. A. Guda and A. V. Soldatov, *J. Phys. Chem. C*, 2024, **128**, 3054–3063.

88 F. R. Lucci, T. J. Lawton, A. Pronschinske and E. C. H. Sykes, *J. Phys. Chem. C*, 2014, **118**, 3015–3022.

89 D. A. Patel, P. L. Kress, L. A. Cramer, A. M. Larson and E. C. H. Sykes, *J. Chem. Phys.*, 2019, **151**, 164705.

90 Y. Wang, K. G. Papanikolaou, R. T. Hannagan, D. A. Patel, T. A. Balema, L. A. Cramer, P. L. Kress, M. Stamatakis and E. C. H. Sykes, *J. Chem. Phys.*, 2020, **153**, 244702.

91 H. Zhang, L. Lu, K. Kawashima, M. Okumura, M. Haruta and N. Toshima, *Adv. Mater.*, 2015, **27**, 1383–1388.

92 Y.-R. Wang, Q. Zhuang, R. Cao, Y. Li, F.-Y. Gao, Z.-R. Li, Z. He, L. Shi, Y.-F. Meng, X. Li, J.-L. Wang, Y. Duan, M.-R. Gao, X. Zheng and S.-H. Yu, *Nano Lett.*, 2022, **22**, 4232–4239.

93 R. B. Garza, J. Lee, M. H. Nguyen, A. Garmon, D. Perez, M. Li, J. C. Yang, G. Henkelman and W. A. Saidi, *J. Chem. Theory Comput.*, 2022, **18**, 4447–4455.

94 C. Zhou, H. T. Ngan, J. S. Lim, Z. Darbari, A. Lewandowski, D. J. Stacchiola, B. Kozinsky, P. Sautet and J. A. Boscoboinik, *J. Am. Chem. Soc.*, 2022, **144**, 15132–15142.

95 X. Liu, C. Ao, X. Shen, L. Wang, S. Wang, L. Cao, W. Zhang, J. Dong, J. Bao, T. Ding, L. Zhang and T. Yao, *Nano Lett.*, 2020, **20**, 8319–8325.

96 L. Jiang, K. Liu, S.-F. Hung, L. Zhou, R. Qin, Q. Zhang, P. Liu, L. Gu, H. M. Chen, G. Fu and N. Zheng, *Nat. Nanotechnol.*, 2020, **15**, 848–853.

97 R. Cheula, M. Maestri and G. Mpourmpakis, *ACS Catal.*, 2020, **10**, 6149–6158.

98 M. Jørgensen and H. Grönbeck, *ACS Catal.*, 2019, **9**, 8872–8881.

99 M. Jørgensen and H. Grönbeck, *J. Am. Chem. Soc.*, 2019, **141**, 8541–8549.

100 R. J. Bunting, F. Wodaczek, T. Torabi and B. Cheng, *J. Am. Chem. Soc.*, 2023, **145**, 14894–14902.

101 R. T. Hannagan, G. Giannakakis, R. Réocreux, J. Schumann, J. Finzel, Y. Wang, A. Michaelides, P. Deshlahra, P. Christopher, M. Flytzani-Stephanopoulos, M. Stamatakis and E. C. H. Sykes, *Science*, 2021, **372**, 1444–1447.

102 R. Réocreux, P. L. Kress, R. T. Hannagan, V. Çınar, M. Stamatakis and E. C. H. Sykes, *J. Phys. Chem. Lett.*, 2020, **11**, 8751–8757.

103 J. E. S. van der Hoeven, H. T. Ngan, G. Yan, J. Aizenberg, R. J. Madix, P. Sautet and C. M. Friend, *J. Phys. Chem. C*, 2022, **126**, 15710–15723.

104 J. D. Lee, Z. Qi, A. C. Foucher, H. T. Ngan, K. Dennis, J. Cui, I. I. Sadykov, E. J. Crumlin, P. Sautet, E. A. Stach, C. M. Friend, R. J. Madix and J. Biener, *J. Am. Chem. Soc.*, 2022, **144**, 16778–16791.

105 D. A. Patel, G. Giannakakis, G. Yan, H. T. Ngan, P. Yu, R. T. Hannagan, P. L. Kress, J. Shan, P. Deshlahra, P. Sautet and E. C. H. Sykes, *ACS Catal.*, 2023, **13**, 4290–4303.

106 G. Meng, J. Sun, L. Tao, K. Ji, P. Wang, Y. Wang, X. Sun, T. Cui, S. Du, J. Chen, D. Wang and Y. Li, *ACS Catal.*, 2021, **11**, 1886–1896.

107 R. Liu, J. N. El Berch, S. House, S. W. Meil, G. Mpourmpakis and M. D. Porosoff, *ACS Catal.*, 2023, **13**, 2449–2461.

108 J. Zhao, J. Liu, Z. Li, K. Wang, R. Shi, P. Wang, Q. Wang, G. I. N. Waterhouse, X. Wen and T. Zhang, *Nat. Commun.*, 2023, **14**, 1909.

109 H. Schulz, *Top. Catal.*, 2003, **26**, 73–85.

110 O. C. Anika, S. G. Nnabuife, A. Bello, E. R. Okoroafor, B. Kuang and R. Villa, *Carbon Capture Science & Technology*, 2022, vol. 5, p. 100072.

111 M. Juneau, D. Yaffe, R. Liu, J. N. Agwara and M. D. Porosoff, *Nanoscale*, 2022, **14**, 16458–16466.

112 M. Dixit, X. Peng, M. D. Porosoff, H. D. Willauer and G. Mpourmpakis, *Catal. Sci. Technol.*, 2017, **7**, 5521–5529.

113 M. D. Porosoff, J. W. Baldwin, X. Peng, G. Mpourmpakis and H. D. Willauer, *ChemSusChem*, 2017, **10**, 2408–2415.

114 M. Juneau, M. Vonglis, J. Hartvigsen, L. Frost, D. Bayerl, M. Dixit, G. Mpourmpakis, J. R. Morse, J. W. Baldwin, H. D. Willauer and M. D. Porosoff, *Energy Environ. Sci.*, 2020, **13**, 2524–2539.

115 R. Liu, D. Leshchev, E. Stavitski, M. Juneau, J. N. Agwara and M. D. Porosoff, *Appl. Catal., B*, 2021, **284**, 119787.

116 R. Liu, Z. Ma, J. D. Sears, M. Juneau, M. L. Neidig and M. D. Porosoff, *J. CO2 Util.*, 2020, **41**, 101290.

117 S. Kim, J. Lauterbach and E. Sasmaz, *ACS Catal.*, 2021, **11**, 8247–8260.

118 S. Kim and E. Sasmaz, *ChemCatChem*, 2022, **14**, e202200568.

119 S. Guan, Z. Yuan, Z. Zhuang, H. Zhang, H. Wen, Y. Fan, B. Li, D. Wang and B. Liu, *Angew. Chem., Int. Ed.*, 2024, **63**, e202316550.

120 T. Han, Y. Li, T. Wu, D. M. Meira, S. Xiang, Y. Cao, I. Lee, X.-G. Zhou, D.-E. Jiang, A. I. Frenkel and F. Zaera, *ACS Catal.*, 2024, **14**, 7157–7165.

121 J. Liu, J. Shan, F. R. Lucci, S. Cao, E. C. H. Sykes and M. Flytzani-Stephanopoulos, *Catal. Sci. Technol.*, 2017, **7**, 4276–4284.

122 M. Luneau, T. Shirman, A. C. Foucher, K. Duanmu, D. M. A. Verbart, P. Sautet, E. A. Stach, J. Aizenberg, R. J. Madix and C. M. Friend, *ACS Catal.*, 2020, **10**, 441–450.

123 M. Luneau, E. Guan, W. Chen, A. C. Foucher, N. Marcella, T. Shirman, D. M. A. Verbart, J. Aizenberg, M. Aizenberg, E. A. Stach, R. J. Madix, A. I. Frenkel and C. M. Friend, *Commun. Chem.*, 2020, **3**, 46.

124 A. C. Foucher, H. T. Ngan, T. Shirman, A. Filie, K. Duanmu, M. Aizenberg, R. J. Madix, C. M. Friend, J. Aizenberg, P. Sautet and E. A. Stach, *ACS Appl. Nano Mater.*, 2023, **6**, 22927–22938.

125 S. K. Kaiser, J. E. S. van der Hoeven, G. Yan, K. R. G. Lim, H. T. Ngan, S. Garg, M. Karatok, M. Aizenberg, J. Aizenberg, P. Sautet, C. M. Friend and R. J. Madix, *ACS Catal.*, 2023, **13**, 12092–12103.

126 G. Giannakakis, P. Kress, K. Duanmu, H. T. Ngan, G. Yan, A. S. Hoffman, Z. Qi, A. Trimpalis, L. Annamalai, M. Ouyang, J. Liu, N. Eagan, J. Biener, D. Sokaras, M. Flytzani-Stephanopoulos, S. R. Bare, P. Sautet and E. C. H. Sykes, *J. Am. Chem. Soc.*, 2021, **143**, 21567–21579.

127 K. G. Papanikolaou and M. Stamatakis, *Catal. Sci. Technol.*, 2021, **11**, 3681–3696.

128 J. Shi, H. T. Ngan, P. Sautet and J. F. Weaver, *ACS Catal.*, 2023, **13**, 11244–11255.

129 L. Chen, Y. Shi, C. Chen, H. Feng, S. Wang, X. Zhang and M. Wei, *J. Phys. Chem. C*, 2022, **126**, 4319–4328.

130 R. Réocreux and M. Stamatakis, *Acc. Chem. Res.*, 2022, **55**, 87–97.

131 Y. Zhang, S. Li, C. Sun, P. Wang, Y. Yang, D. Yi, X. Wang and J. Yao, *ACS Catal.*, 2022, **12**, 9201–9212.

132 S. Liu, N. Govindarajan and K. Chan, *ACS Catal.*, 2022, **12**, 12902–12910.

133 Y. Zhang, B. Wang, M. Fan, D. Li and R. Zhang, *Fuel*, 2021, **306**, 121641.

134 S. Chen, J. Zaffran and B. Yang, *ACS Catal.*, 2020, **10**, 3074–3083.

135 R. J. Bunting, P. S. Rice, Z. Yao, J. Thompson and P. Hu, *Chem. Commun.*, 2022, **58**, 9622–9625.

136 R. Liu and W. An, *Catal. Sci. Technol.*, 2021, **11**, 7047–7059.

137 S. AlAreeqi, D. Bahamon, K. Polychronopoulou and L. F. Vega, *Fuel Process. Technol.*, 2024, **253**, 108001.

138 R. Xia, S. Overa and F. Jiao, *JACS Au*, 2022, **2**, 1054–1070.

139 K. M. Van Geem and B. M. Weckhuysen, *MRS Bull.*, 2021, **46**, 1187–1196.

140 Q. Gao, X. Han, Y. Liu and H. Zhu, *ACS Catal.*, 2024, **14**, 6045–6061.

141 Y. Da, R. Jiang, Z. Tian, X. Han, W. Chen and W. Hu, *SmartMat*, 2023, **4**, e1136.

142 J. K. Nørskov, J. Rossmeisl, A. Logadottir, L. Lindqvist, J. R. Kitchin, T. Bligaard and H. Jónsson, *J. Phys. Chem. B*, 2004, **108**, 17886–17892.

143 D. R. Alfonso, D. N. Tafen and D. R. Kauffmann, *Catalysts*, 2018, **8**, 424.

144 S. Nitopi, E. Bertheussen, S. B. Scott, X. Liu, A. K. Engstfeld, S. Horch, B. Seger, I. E. L. Stephens, K. Chan, C. Hahn, J. K. Nørskov, T. F. Jaramillo and I. Chorkendorff, *Chem. Rev.*, 2019, **119**, 7610–7672.

145 X. Zhi, Y. Jiao, Y. Zheng, A. Vasileff and S.-Z. Qiao, *Nano Energy*, 2020, **71**, 104601.

146 J.-C. Jiang, J.-C. Chen, M.-D. Zhao, Q. Yu, Y.-G. Wang and J. Li, *Nano Res.*, 2022, **15**, 7116–7123.

147 J. Wang, S. Li, Q. Liu, K. Zhao, Y. Yang and X. Wang, *ACS Appl. Mater. Interfaces*, 2023, **15**, 53436–53445.

148 C. Du, S. Lu, J.-A. Wang, X. Wang, M. Wang, H. M. Fruehwald, L. Wang, B. Zhang, T. Guo, J. P. Mills, W. Wei, Z. Chen, Y. Teng, J. Zhang, C.-J. Sun, H. Zhou, R. D. L. Smith, B. Kendall, G. Henkelman and Y. A. Wu, *ACS Catal.*, 2023, **13**, 10560–10569.

149 K. Chen, J. Xiang, Y. Guo, X. Liu, X. Li and K. Chu, *Nano Lett.*, 2024, **24**, 541–548.

150 L. Chen, X. Liang, D. Wang, Z. Yang, C.-T. He, W. Zhao, J. Pei and Y. Xue, *ACS Appl. Mater. Interfaces*, 2022, **14**, 27814–27822.

151 J. Mao, C.-T. He, J. Pei, Y. Liu, J. Li, W. Chen, D. He, D. Wang and Y. Li, *Nano Lett.*, 2020, **20**, 3442–3448.

152 M. T. Darby and M. Stamatakis, *ChemPhysChem*, 2021, **22**, 499–508.

153 E. Zhang, A. Dong, K. Yin, C. Ye, Y. Zhou, C. Tan, M. Li, X. Zheng, Y. Wang, X. Gao, H. Li, D. Wang and S. Guo, *J. Am. Chem. Soc.*, 2024, **146**, 2339–2344.

154 D. Sorvisto, P. Rinke and T. P. Rossi, *J. Phys. Chem. C*, 2023, **127**, 8585–8590.

155 W.-N. Lu, S. Luo, Y. Zhao, J. Xu, G. Yang, E. Picheau, M. Han, Q. Wang, S. Li, L. Jia, M.-X. Ling, T. Kako and J. Ye, *Appl. Catal., B*, 2024, **343**, 123520.

156 Y. Wang, G. Hong, Y. Zhang, Y. Liu, W. Cen, L. Wang and Z. Wu, *Angew. Chem., Int. Ed.*, 2023, **62**, e202310525.

157 Y. Pan, Y. Qian, X. Zheng, S.-Q. Chu, Y. Yang, C. Ding, X. Wang, S.-H. Yu and H.-L. Jiang, *Natl. Sci. Rev.*, 2021, **8**, nwaa224.

158 S. Ma and Z.-P. Liu, *ACS Catal.*, 2020, **10**, 13213–13226.

159 P. S. Lamoureux, K. T. Winther, J. A. Garrido Torres, V. Streibel, M. Zhao, M. Bajdich, F. Abild-Pedersen and T. Bligaard, *ChemCatChem*, 2019, **11**, 3581–3601.

160 J. R. Kitchin, *Nat. Catal.*, 2018, **1**, 230–232.

161 H. Feng, H. Ding, S. Wang, Y. Liang, Y. Deng, Y. Yang, M. Wei and X. Zhang, *ACS Appl. Mater. Interfaces*, 2022, **14**, 25288–25296.

162 J. Shirani, H. D. M. Pham, S. Yuan, A. B. Tchagang, J. J. Valdés and K. H. Bevan, *J. Phys. Chem. C*, 2023, **127**, 12055–12067.

163 J. Shirani, J. J. Valdes, A. B. Tchagang and K. H. Bevan, *J. Phys. Chem. C*, 2024, **128**, 4483–4496.

164 D. Wang, R. Cao, S. Hao, C. Liang, G. Chen, P. Chen, Y. Li and X. Zou, *Green Energy Environ.*, 2023, **8**, 820–830.

165 X. Zong and D. G. Vlachos, *J. Chem. Inf. Model.*, 2022, **62**, 4361–4368.

166 A. Kumar, J. Iyer, F. Jalid, M. Ramteke, T. S. Khan and M. A. Haider, *ChemCatChem*, 2022, **14**, e202101481.

167 S. Saxena, T. S. Khan, F. Jalid, M. Ramteke and M. A. Haider, *J. Mater. Chem. A*, 2020, **8**, 107–123.

168 S. Sun, G. Sun, C. Pei, Z.-J. Zhao and J. Gong, *J. Phys. Chem. C*, 2021, **125**, 18708–18716.

169 T. Mou, H. S. Pillai, S. Wang, M. Wan, X. Han, N. M. Schweitzer, F. Che and H. Xin, *Nat. Catal.*, 2023, **6**, 122–136.

170 J. A. Esterhuizen, B. R. Goldsmith and S. Linic, *Nat. Catal.*, 2022, **5**, 175–184.

171 G. O. Kayode, A. F. Hill and M. M. Montemore, *J. Mater. Chem. A*, 2023, **11**, 19128–19137.

172 H. Feng, M. Zhang, Z. Ge, Y. Deng, P. Pu, W. Zhou, H. Yuan, J. Yang, F. Li, X. Zhang and Y.-W. Zhang, *ACS Appl. Mater. Interfaces*, 2023, **15**, 55903–55915.

173 J. D. Head and M. C. Zerner, *Chem. Phys. Lett.*, 1985, **122**, 264–270.

174 L. Yang, S. Hanneke and J. Carbonell, *Mach. Learn.*, 2013, **90**, 161–189.

175 A. Ramdan, A. Heryana, A. Arisal, R. B. S. Kusumo and H. F. Pardede, *Transfer Learning and Fine-Tuning for Deep Learning-Based Tea Diseases Detection on Small Datasets*, 2020 International Conference on Radar, Antenna, Microwave, Electronics, and Telecommunications (ICRAMET), Tangerang, Indonesia, 2020, pp. 206–211, DOI: **10.1109/ICRAMET51080.2020.9298575**.

176 C. Chen and S. P. Ong, *npj Comput. Mater.*, 2021, **7**, 173.

177 X. Li, B. Li, Z. Yang, Z. Chen, W. Gao and Q. Jiang, *J. Mater. Chem. A*, 2022, **10**, 872–880.

178 L. Chanussot, A. Das, S. Goyal, T. Lavril, M. Shuaibi, M. Riviere, K. Tran, J. Heras-Domingo, C. Ho, W. Hu, A. Palizhati, A. Sriram, B. Wood, J. Yoon, D. Parikh, C. L. Zitnick and Z. Ulissi, *ACS Catal.*, 2021, **11**, 6059–6072.

179 C. M. Clausen, J. Rossmeisl and Z. W. Ulissi, *J. Phys. Chem. C*, 2024, **128**, 11190–11195.

180 S. Zhang, E. C. H. Sykes and M. M. Montemore, *Chem. Sci.*, 2022, **13**, 14070–14079.

181 P. L. Kress, S. Zhang, Y. Wang, V. Çınar, C. M. Friend, E. C. H. Sykes and M. M. Montemore, *J. Am. Chem. Soc.*, 2023, **145**, 8401–8407.

182 K. Chen, D. Ma, Y. Zhang, F. Wang, X. Yang, X. Wang, H. Zhang, X. Liu, R. Bao and K. Chu, *Adv. Mater.*, 2024, **36**, 2402160.