

Cite this: *RSC Appl. Interfaces*, 2025, 2, 1082Received 11th February 2025,  
Accepted 19th May 2025

DOI: 10.1039/d5lf00033e

rsc.li/RSCApplInter

# Vanadium pentoxide mesoporous cathodes for Li-ion batteries†

Andrea Palumbo,<sup>a</sup> Ullrich Steiner, <sup>a</sup> Andrea Dodero <sup>\*ab</sup> and Ilja Gunkel <sup>a</sup>

The combination of micro- and nanoporosity is advantageous for Li-ion intercalation in battery electrodes. In this work, we synthesize porous 10  $\mu\text{m}$ -sized poly(styrene-vinylpyridine) block copolymer particles *via* an emulsion-based approach. The vinylpyridine-phase was then subjected to methanol swelling to enable vanadium ions infiltration, followed by calcination to obtain mesoporous vanadium pentoxide particles. These exhibited a hierarchical porosity, and electrodes manufactured from them displayed a very high specific surface area. Two liquid electrolytes were compared to manage solid-electrolyte-interface growth, which can clog nanopores. Notably, the combination of a lithium bis(trifluoromethane)sulfonimide-containing tetraethylene glycol dimethyl ether tetraglyme electrolyte with the hierarchically porous vanadium pentoxide electrodes demonstrated a substantial enhancement in cycling performance, surpassing established industry benchmarks.

## 1 Introduction

Given the increasing interest in battery technology, there is an ongoing pursuit of breakthrough materials and fabrication processes to address the rapidly expanding demand for high-performance energy storage solutions. Mesoporous materials have garnered significant attention due to their advantageous properties, including an enhanced effective surface area that facilitates ion intercalation.<sup>1,2</sup> This, in turn, exerts a direct influence on battery performance, particularly with regard to power and energy densities.<sup>3–6</sup> However, the use of entirely nanostructured materials is often impeded by their inadequate ion transport, which can be attributed to the constrained mass diffusion resulting from the substantial thickness of conventional electrodes (*i.e.*, several 100  $\mu\text{m}$ ).<sup>7,8</sup> To address this challenge, the incorporation of micrometer-sized interconnected pores into mesoporous materials has emerged as a promising solution.<sup>9,10</sup> This approach aims to enhance Li-ion diffusion across the hierarchically structured material while preserving the advantages of interconnected pores with a high surface area.<sup>11–13</sup>

In energy storage devices, mesoporous electrodes offer distinct advantages over conventional materials, including bulk

and nanopowder-based formulations.<sup>12,13</sup> The integration of high surface area with optimized ion transport pathways has been demonstrated to result in improvements in energy density and charge/discharge kinetics.<sup>9,10,14</sup> Furthermore, these structures demonstrate enhanced mechanical stability during the charge and discharge processes, resulting in a longer cycle life and superior electrochemical performance.<sup>15–17</sup> Moreover, their organized structure prevents agglomeration, a common issue in purely nanosized materials.<sup>14,15,18</sup>

A further critical challenge for nanostructured electrodes is the formation of a solid-electrolyte interphase (SEI) layer through electrolyte degradation if the electrochemical potential exceeds the electrolyte's stability. This can impede the flow of ions, leading to the accumulation of matter within the nanopores and consequently the degradation of battery performance over time.<sup>3,6,15</sup>

This study proposes a new manufacturing approach that extends for the first time the advantages of mesostructured battery electrodes to vanadium pentoxide ( $\text{V}_2\text{O}_5$ ). Vanadium pentoxide is a promising cathode material for Li-ion batteries, as it offers a high theoretical capacity, a wide voltage range, and good conductivity.<sup>19–22</sup> However,  $\text{V}_2\text{O}_5$  exhibits considerable sensitivity to volume changes during cycling, resulting in capacity degradation over short time frames and limited cyclability.<sup>23–26</sup> To address these challenges, we have developed a fabrication procedure to synthesize mesoporous  $\text{V}_2\text{O}_5$  microspheres. These microspheres are capable of effectively mitigating issues related to volume change while utilizing the inherent advantages of vanadium pentoxide. In contrast to earlier studies, which commonly employed the co-assembly of block copolymers with precursor sols followed by calcination

<sup>a</sup> Adolphe Merkle Institute, Chemin de Verdiers 4, Fribourg, Switzerland.

E-mail: andrea.dodero@unifr.ch

<sup>b</sup> Department of Chemistry and Industrial Chemistry, University of Genoa, Via Dodecaneso 31, Genoa, Italy

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d5lf00033e>



into metal oxides, the present approach starts with the oil-in-water emulsification of a block copolymer in the presence of a non-solvent.<sup>27,28</sup> The resultant mesostructured block copolymer spheres, obtained after solvent evaporation, are then swollen and selectively infiltrated with  $V^{4+}$  ions. The final step involves calcination to obtain mesoporous  $V_2O_5$  microspheres. The formation of battery electrodes is then accomplished by implementing the slurry technique, which is a prevalent method within the field.<sup>29</sup>

The structural and electrochemical properties of the resulting mesoporous  $V_2O_5$  electrodes were investigated to determine their suitability for energy storage applications. Given that the electrochemical operation of these electrodes is sensitively dependent on the electrolyte formulation, which controls the SEI formation, two electrolytes were compared to optimize device performances.<sup>30–33</sup> Notably, by combining mesoporosity with a suitable electrolyte, we achieve a synergistic effect that maximizes energy storage performance while simultaneously minimizing SEI-forming chemical reactions.<sup>2,34,35</sup>

## 2 Experimental

### 2.1 Materials

PS-*b*-P4VP with molar mass of  $M_w = 195\text{--}204\text{ kg mol}^{-1}$  was purchased from Polymer Source, Inc. PVA with a molar mass of  $M_w = 13\text{--}27\text{ kg mol}^{-1}$  and a degree of hydrolysis of 87–89% was purchased from Sigma-Aldrich. MeOH 99.9% analytical reagent grade, and  $CHCl_3$  99.8% analytical reagent grade were purchased from Fisher Scientific. Dioxane anhydrous, 99.8%, was purchased from Sigma-Aldrich.  $VOSO_4$  97% and hexadecane reagent grade 99% were purchased from Sigma-Aldrich. The standard electrolyte of 1 M  $LiPF_6$  1:1 (v/v) EC:DMC was purchased from Sigma-Aldrich. Conductive carbon black (Super C65) was kindly provided by Imerys Graphite & Carbon, Switzerland Ltd. PVDF (Kynar HSV900) was provided by ARKEMA Innovative Chemistry. NMP anhydrous 99.5% was purchased from Sigma-Aldrich. Lithium chips were purchased from Gelon LIB Group, and GF/B glass microfiber was purchased from Healthcare Life Sciences. LiTFSI 99.95% and tetraglyme 99% were purchased from Sigma-Aldrich.

### 2.2 Synthesis

PS-*b*-P4VP was solubilized in chloroform ( $CHCl_3$ ) at a concentration of  $20\text{ mg mL}^{-1}$  under stirring, and PVA was solubilized in deionized water at a  $5\text{ mg mL}^{-1}$  concentration at  $T = 80\text{ }^\circ\text{C}$  for several hours under stirring. Additionally, a solution of hexadecane in  $CHCl_3$  was prepared at a concentration of  $20\text{ mg mL}^{-1}$ . The BCP and hexadecane solutions were mixed in a glass vial at two ratios (*i.e.*, 70:30 and 100:0) and left under stirring for 30 minutes. The PVA solution was then added to the BCP mixture in a volume ratio of 5 to 1. An oil-in-water emulsion (*i.e.*, small droplets of oil dispersed in water) was then formed by agitating the two phases using a vortex mixer at a speed of 2000 rpm for 30 seconds.

The resulting emulsion was transferred to a covered 5 cm wide Petri dish, and 10 mL of deionized water was added to slow the rate of evaporation of chloroform. The emulsion was left undisturbed for approximately 5 days to allow for the gradual drying of the emulsion droplets, resulting in the formation of solid BCP microparticles ranging in size from 5 to 10  $\mu\text{m}$ . These were then collected, transferred to a 50 mL flask, and centrifuged at 8000 rpm for 30 minutes to separate the self-assembled polymers from the remaining supernatant.

A  $100\text{ mg mL}^{-1}$  solution of  $VOSO_4$  in MeOH was then added to the dried microparticles and the resulting suspension was stirred overnight. The addition of MeOH to the microparticles causes the P4VP domains to swell, allowing the vanadium ions to uniformly infiltrate the polymeric matrix.<sup>36,37</sup>

The mixture was finally centrifuged to remove any remaining MeOH and excess precursor. The resulting solid was transferred to a crucible and calcined at  $425\text{ }^\circ\text{C}$  for two hours in air with a gradual temperature increase at a rate of  $5\text{ }^\circ\text{C per minute}$ .

### 2.3 Slurry formulation and cells preparation

Slurries for electrode preparation were formulated by dispersing active materials, conductive carbon black (Super C65) as the conductive additive, poly(vinylidene fluoride) (PVDF, Kynar HSV900) as the binder, and 1-methyl-2-pyrrolidone (NMP) anhydrous as the solvent. The slurries were prepared with a ratio of active material:carbon black:PVDF of 7:2:1.

The slurry components were mixed thoroughly to ensure homogeneity and coated onto the current collectors using a doctor blade method. For this step a sheet film vacuum coater from MTI Corp. (MSK-AFA-II-VC) and 250 mm doctor blade were used, the coater slid the doctor blade, set at an angle of 100  $\mu\text{m}$  over a foil of aluminum paper. The coatings were subsequently dried at  $60\text{ }^\circ\text{C}$  overnight to ensure complete solvent evaporation.

The coin cells manufacturing process began with preparing the discs to insert into the coin cell from the dried slurry. With a specific tool, the hand-held disc cutter (MSK-T-12) from MTI Corp. discs of 15 mm in diameter were cut out. Subsequently, separator discs of 18 mm in diameter of Whatman glass microfiber grade GF/A filter discs with 1  $\mu\text{m}$  pore size were cut the same way. After, both the slurry and the separator disks, and the coin cell assembly materials were put in vacuum oven overnight at  $120\text{ }^\circ\text{C}$ . The cell assembly materials, all purchased from MTI Corp. composed of CR2032 Coin Cell Cases, 20 mm current collector stainless steel disks and 20 mm stainless spring disks. The items were then transferred into a glove box under Argon atmosphere with oxygen and moisture levels below 1 ppm for the cell assembly. The cell assembly took place inside the glove box, where the bottom lid of the coin cell was layered with a spring, current collector, an 18 mm lithium disk (2 mm thick), a separator soaked with 150  $\mu\text{l}$  of electrolyte solution, an active material disk, another current collector,



and a second spring. Once all the components were stacked the top lid of the coin cell was added and sealed under a mechanical manual press, from MTI corp. at a pressure of 1000 kg.

## 2.4 Instrumentation

A Tescan Mira 3 LMH scanning electron microscope was used to examine the nanoparticles. Measurements were performed with a sample-detector distance between 5 and 10 mm and accelerating voltages between 10 and 20 kV. A 2–4 nm conductive gold coating was sputtered on the samples to prevent surface charging. A FEI Tecnai Spirit TEM equipped with a 120 kV LaB<sub>6</sub> emitter was used for transmission electron microscopy. Images were acquired by a Veleta charge-coupled device (CCD) sensor at room temperature. The samples for TEM analysis were prepared inside the glove box, where the cells were first disassembled, and the electrodes were collected in a glass vial. The cathode materials were washed twice with a solution of DMC to remove the electrolyte, and the vial was again filled with DMC. The vial was removed from the glove box and sonicated for 10 min at room temperature to suspend the metal oxides in DMC. Some of this suspension was deposited on a TEM grid, which was left in fume hood for 24 h, for the DMC to evaporate.

Physisorption analysis was performed using a high-precision BET analyzer (model 110 from 3P Instruments). The sample was degassed in a liquid nitrogen bath and subjected to gas adsorption and desorption cycles at different pressures ranging from 0.05 to 0.995 atm. The BET model was used to calculate the specific surface area, while the BJH method was used to estimate the pore size distribution.

An Arbin BT 2043 multi-channel system was used for galvanostatic cycling experiments. The selected current rates, called C-rates, were varied to study the effect of different current intensities on the cycling process.

A BioLogic VMP 300 system was used for the cyclic voltammetry experiments. CV measurements involved sweeping the voltage within a material-specific range where reversible

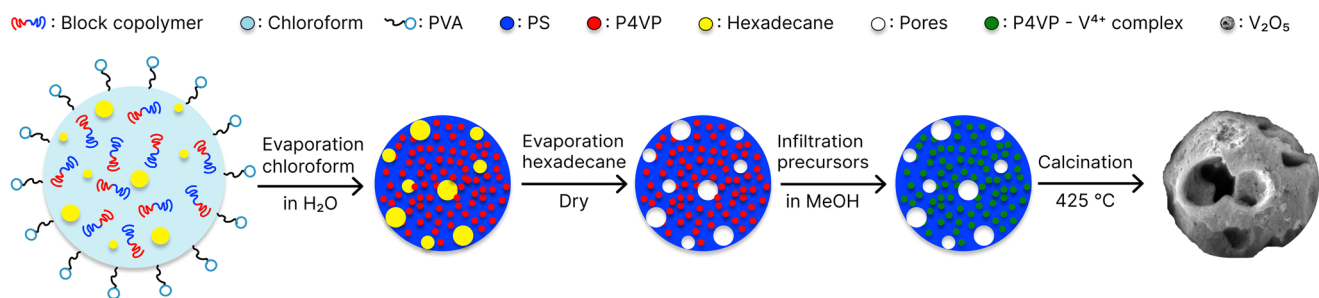
electrochemical reactions occur, typically between 1.0 and 5.0 V (*versus* Li<sup>+</sup>/Li). To gain insight into the electrochemical behavior of the material under different conditions, the analysis was performed at different scan rates, namely 0.1, 0.2, 0.5, 1.0, and 2.0 mV s<sup>-1</sup>. By systematically varying the scan rates, it was possible to study the reaction kinetics associated with the electrochemical processes.

A BioLogic VMP 300 system was used for the electronic impedance spectroscopy measurements. EIS data were collected over a wide frequency range, from 1 MHz to 100 MHz, applying a voltage amplitude of 20 mV.

## 3 Results

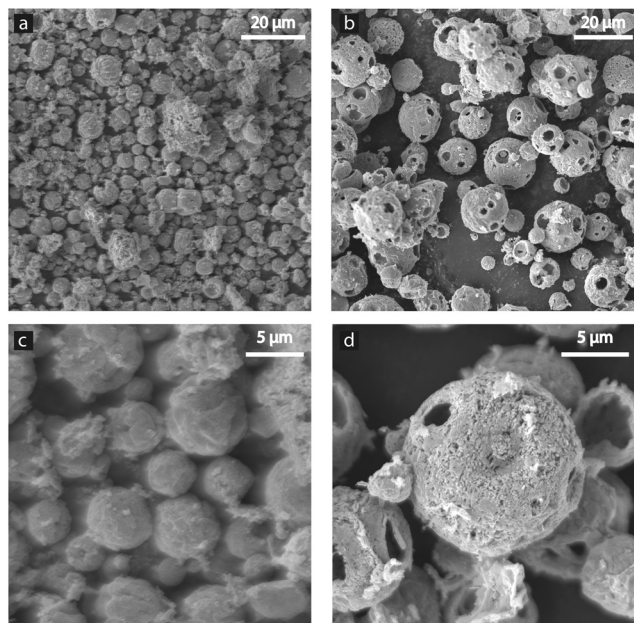
The schematic in Fig. 1 summarizes the preparation of mesoporous vanadium pentoxide microspheres. First, an oil(CHCl<sub>3</sub>)-in-water emulsion is prepared using polyvinyl alcohol (PVA) as a hydrophilic emulsifier. The CHCl<sub>3</sub> minority phase contains a polystyrene-*block*-poly(4-vinylpyridine) (PS-*b*-P4VP) diblock copolymer (BCP) with a molar mass of  $M_w = 195\text{--}204\text{ kg mol}^{-1}$ , and hexadecane. The weight ratio of BCP to hexadecane was varied between 100:0 and 70:30. The resulting emulsion was left at room temperature to allow the evaporation of CHCl<sub>3</sub> by diffusion through the water phase. The slow increase in BCP concentration within the emulsion droplets induces their self-assembly into internally nanostructured microparticles. Since hexadecane does not mix with water or the BCP, it remains within the emulsion droplets and phase separates from the macromolecular chains, creating micrometer-sized inclusions within the final particles. Drying the resulting suspensions in a vacuum oven yields a powder of *ca.* 10 μm BCP spheres containing micrometer-sized pores resulting from the evaporation of the hexadecane.

The resulting micropowder was then suspended in a methanol-containing (VOSO<sub>4</sub>·2H<sub>2</sub>O) vanadium precursor. Methanol is a solvent for P4VP but not for PS, so the P4VP phase swells selectively while the PS-*b*-P4VP spheres remain intact. The P4VP swelling allows vanadium ions to diffuse into the BCP microspheres and complex with the vinylpyridine



**Fig. 1** Schematic representation of the formation of the mesoporous vanadium pentoxide microspheres. The starting point is an emulsion of a BCP, CHCl<sub>3</sub>, and hexadecane mixture in water. As CHCl<sub>3</sub> diffuses through the water and evaporates, the organic phase shrinks, forming a self-assembled BCP phase with hexadecane inclusions. The spheres were collected and dried, causing the hexadecane to evaporate, forming micrometer-sized holes. The mesoporous spheres were exposed to a vanadium precursor dissolved in methanol, which swells the BCP and allows the precursor to infiltrate the BCP. Centrifugation, drying, and calcination at 425 °C result in mesoporous V<sub>2</sub>O<sub>5</sub> spheres.





**Fig. 2** SEM images of mesoporous  $V_2O_5$  microspheres.  $V_2O_5$  microspheres synthesized from emulsions containing different ratios of BCP to hexadecane. a and c) 100 : 0; b and d) 70 : 30. While porosity on the 10 nm scale is present in all samples, the 70 : 30 spheres exhibit micrometer-sized pores resulting from the addition of hexadecane.

groups. The infiltration is particularly aided by the microporosity of the spheres created by the evaporation of hexadecane. P4VP was chosen as one of the BCP blocks because of its strong ability to form complexes with metal ions, such as  $V^{4+}$ .<sup>38,39</sup>

Finally, the infiltrated particles were heated to 425 °C in air, causing complete evaporation of methanol, oxidation of  $V^{4+}$  to  $V_2O_5$ , and combustion of the polymer phase. The microphase-separated BCP matrix confines the growth of  $V_2O_5$  crystals during the thermal process and preserves the spherical 10 μm shape of the spheres. The resulting  $V_2O_5$  is porous on three different length scales: (1) at the 10 nm level defined by the BCP microphase morphology, (2) at the micrometer level through the pores left by the hexadecane evaporation, and (3) through the 10 μm porosity resulting from the packing of the emulsion-derived spheres.<sup>40</sup> Details of the sample preparation are given in the Experimental section.

SEM analysis was performed to evaluate the formation of microporous spheres and the effect of hexadecane addition. The SEM micrographs in Fig. 2 show the morphological variations in the synthesized  $V_2O_5$  microspheres. Fig. 2a and c shows  $V_2O_5$  microspheres in the absence of hexadecane, *i.e.* a

100 : 0 BCP to hexadecane ratio. In Fig. 2b and d, hexadecane was added during the emulsification process in a BCP to hexadecane 70 : 30 ratio. In general, Fig. 2 shows that the presence of micrometer-sized pores in the  $V_2O_5$  microsphere is clearly due to the added hexadecane. Porosimetry was used to determine the characteristic surface area and average pore size of the samples. Table 1 lists the characteristic parameters for samples synthesized with and without hexadecane addition in comparison to a commercial  $V_2O_5$  material. The two samples prepared by emulsion-induced self-assembly have specific surface areas and total pore volumes an order of magnitude higher than the commercial material. Since these values are dominated by the 10–20 nm microporosity resulting from  $V^{4+}$  infiltration into the pyridine domains of the block copolymer particles, these high values demonstrate the effectiveness of the infiltration process.

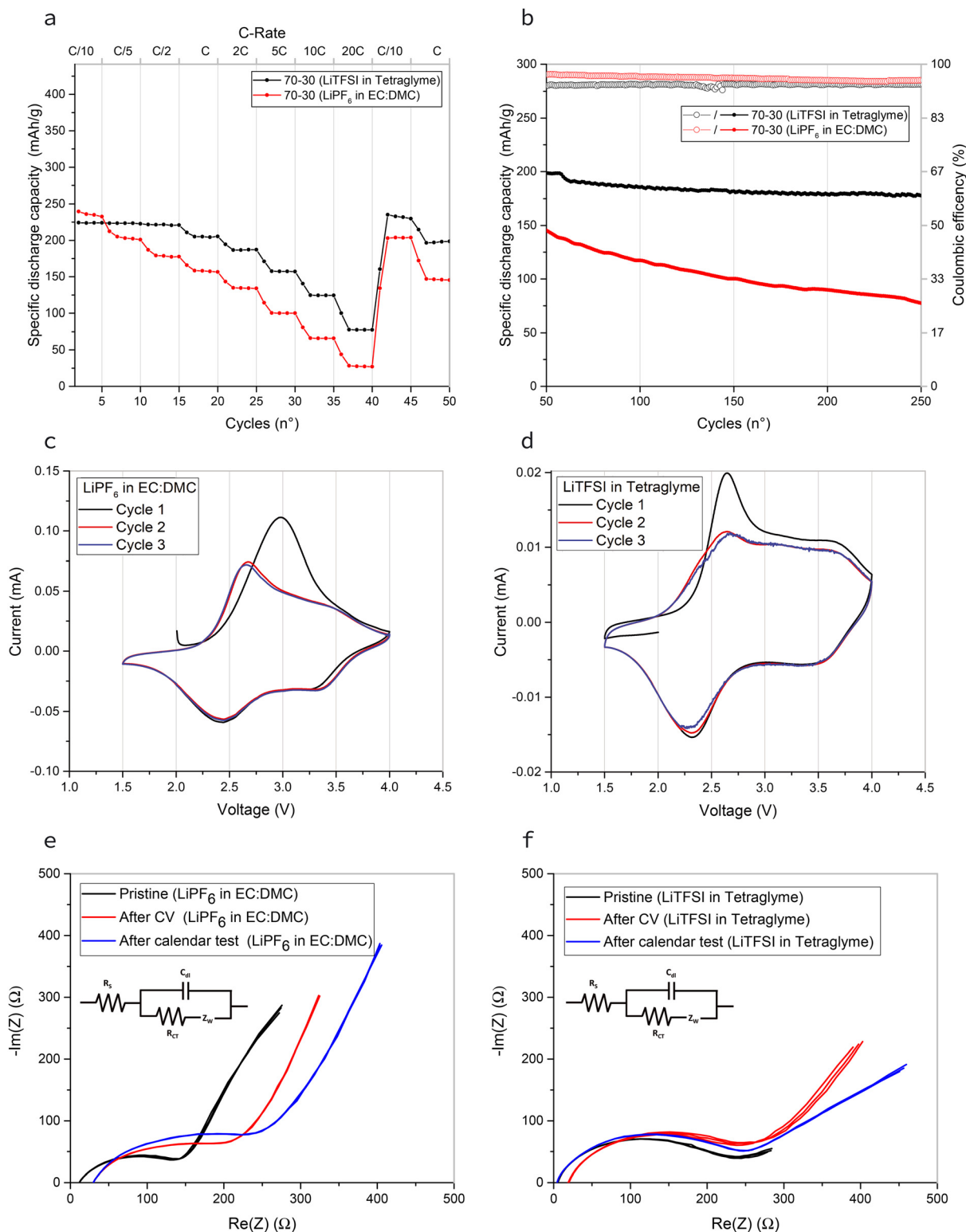
As a high-voltage cathode,  $V_2O_5$  is known to form an SEI layer when in contact with organic electrolytes.<sup>30,41,42</sup> Since SEI layers often grow during cycling, they can clog the nanopores and reduce battery performance. In a recent study, an electrolyte based on lithium bis(trifluoromethane) sulfonimide (LiTFSI) in tetraethylene glycol dimethyl ether tetraglyme (tetraglyme), 1 : 1 in mole ratio was compared to one containing lithium hexafluorophosphate ( $LiPF_6$ ) dissolved in an ethylene carbonate–dimethyl carbonate (EC : DMC) 1 M mixture.<sup>30</sup> Here we study the effect of SEI layers by comparing these two electrolytes using the  $V_2O_5$  electrode material with the highest specific surface area in Table 1, *i.e.* 70 : 30 sample.

The results of this comparison are shown in Fig. 3. In the cycling test shown in Fig. 3a, the  $V_2O_5$  70–30 sample with LiTFSI in tetraglyme exhibits exceptional stability up to a C-rate of C/2 (first 15 cycles), maintaining a specific discharge capacity of 220 mA h  $g^{-1}$  in all cycles. On the contrary, the sample with  $LiPF_6$  in EC : DMC has a higher initial discharge capacity, but it drops to 178 mA h  $g^{-1}$  when cycling at C/2. Both samples exhibit capacity decrease when the C-rate is increased to 20C. The LiTFSI in tetraglyme maintains higher capacities, reaching 77 mA h  $g^{-1}$  at 20C compared to 27 mA h  $g^{-1}$  for  $LiPF_6$  in EC : DMC. This can be attributed to the fact that while  $LiPF_6$  in EC : DMC allows for lower initial  $R_{ct}$ , its rate performance is hampered by rapid SEI growth that blocks active sites and restricts pore access, as seen in the calendar test in Fig. 3b and from the TEM images in Fig. 4c and d. In contrast, LiTFSI in tetraglyme enables more stable cycling and better high rate performance by forming a thinner, more stable SEI that preserves the mesoporous structure of the electrode (Fig. 4e and f). In addition, the

**Table 1** Porosity values of the two manufactured materials with (70 : 30) and without (100 : 0) hexadecane added during their manufacture, compared to a commercial  $V_2O_5$  material

Samples	Specific surface area (BET) ( $m^2 g^{-1}$ )	Average pore size (BJH) (nm)	Total pore volume (BJH) ( $cm^3 g^{-1}$ )
70 : 30	55.13	11.25	0.155
100 : 0	42.56	12.47	0.133
Commercial	3.14	14.9	0.015



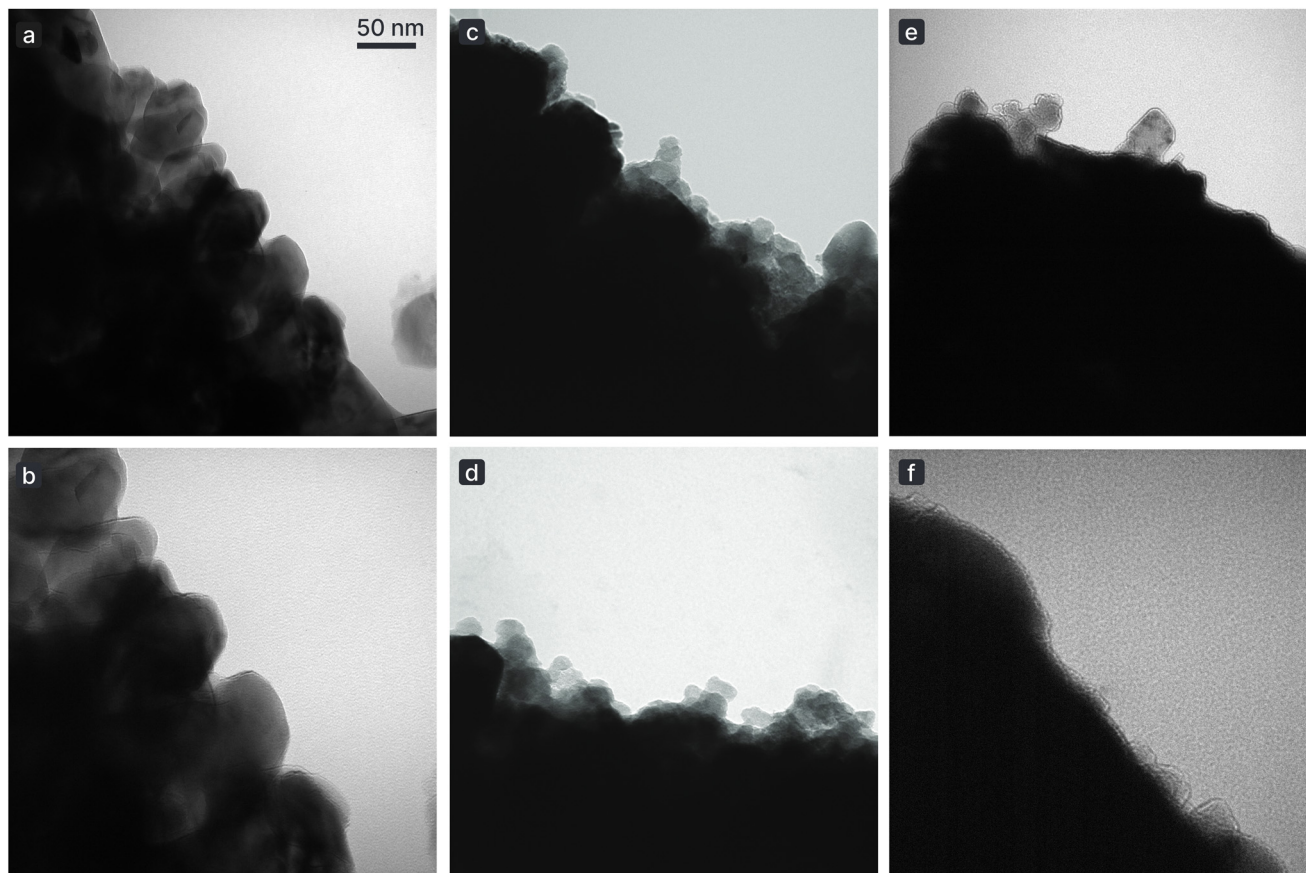


**Fig. 3** Electrochemical performance of 70:30  $V_2O_5$  electrodes using two electrolytes. (a) Cycling performance of half-cells containing LiTFSI in tetraglyme (black) and LiPF<sub>6</sub> in EC:DMC (red). (b) Calendar test of half-cells over 250 cycles at a rate of 1C. (c and d) Cyclic voltammograms of  $V_2O_5$  70:30 with LiPF<sub>6</sub> in EC:DMC and LiTFSI in tetraglyme, respectively. (e and f) Electrochemical impedance spectroscopy spectra of  $V_2O_5$  70:30 with LiPF<sub>6</sub> in EC:DMC and LiTFSI in tetraglyme, respectively.

tetraglyme is a flexible solvent and strongly coordinates with  $Li^+$ , improving solvation and desolvation kinetics at the

electrode surface, which enhances Li-ion transport at high rates.<sup>30,43–45</sup>





**Fig. 4** Transmission electron microscopy images of  $V_2O_5$  surfaces before and after electrochemical cycling. (a and b) Pristine  $V_2O_5$  70 : 30 surface with well-defined crystalline structures. (c and d) Similar  $V_2O_5$  surface after 75 cycles with  $LiPF_6$  in EC : DMC electrolyte, showing non-uniform SEI layer formation. (e and f) When  $LiTFSI$  in tetraglyme is used as electrolyte, only a few lumpy SEI aggregates separated by a very thin, uniform SEI layer are observed.

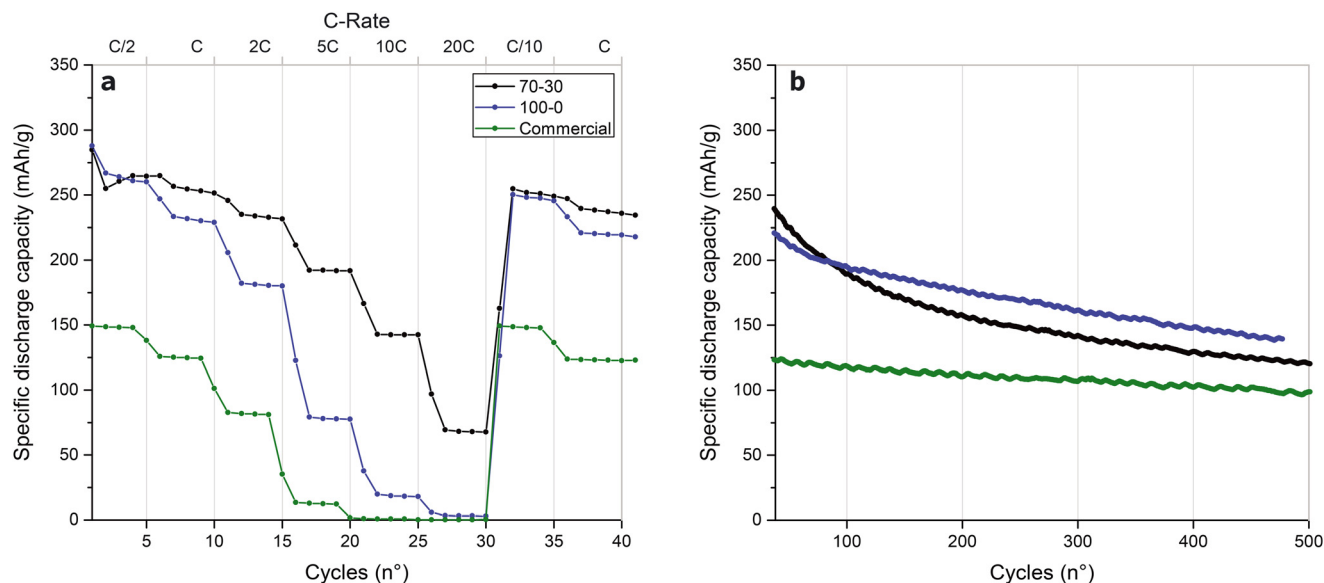
After cycling at high C rates, the rate is reduced to C/10 and C. While the  $LiTFSI$  in the tetraglyme sample returns to its initial C/10 capacity, the C/10 capacity of  $LiPF_6$  in EC : DMC is reduced to *ca.* 200 mA h  $g^{-1}$ . Fig. 3b shows a calendar test over 250 cycles at a C-rate of 1C. After an initial capacity of 200 mA h  $g^{-1}$  for 10 cycles of the  $LiTFSI$  in tetraglyme half-cell, it declines to 178 mA h  $g^{-1}$  over 250 cycles, corresponding to an 11% loss in specific capacity. The  $LiPF_6$  in EC : DMC sample declines from an initial capacity of 145 mA h  $g^{-1}$  to 77 mA h  $g^{-1}$ , a 47% capacity loss over 250 cycles.

Fig. 3c and d show cyclic voltammetry (CV) curves of  $LiPF_6$  in EC : DMC and  $LiTFSI$  in tetraglyme electrolytes, respectively. The CV curves show the three expected redox peaks of  $V_2O_5$  corresponding to lithium intercalation and deintercalation processes. The initial peak shift around 3.0 V (Fig. 3c) suggests SEI formation during the first cycle, a common phenomenon in lithium-ion batteries, but it is much less pronounced in the  $LiTFSI$  in tetraglyme sample shown in Fig. 3d. Subsequent cycles show the expected peaks at their characteristic voltages, indicating reproducible cycling behavior. Fig. 3e and f show electrochemical impedance spectroscopy (EIS) spectra for both electrolytes taken immediately after cell assembly (black line), after CV analysis

(red line), and after calendar testing (blue line). The EIS comparison of the pristine materials reveals that  $LiPF_6$  initially outperforms  $LiTFSI$ . This is particularly evident in the first semicircle, which actually represents the contribution of multiple overlapping semicircles. The impedance, observable on the real axis (Re), is approximately 75 ohms lower for the cells having  $LiPF_6$  as electrolyte salt compared to those with  $LiTFSI$ . This result is expected, as 1 M  $LiPF_6$  in EC : DMC is a highly efficient electrolyte, and is widely used in the field due to its excellent performance. However, its combination with mesoporous  $V_2O_5$  limits its applicability, as it promotes side reactions, such as SEI formation, significantly more than its counterpart,  $LiTFSI$  in tetraglyme, as observed from the EIS collected after cycling the cells.

First, the evolution of the charge transfer resistance ( $R_{ct}$ ) is highlighted. The  $LiPF_6$  in EC : DMC has a lower ( $R_{ct}$ , Fig. 3e) due to the higher ionic conductivity and better wetting of the electrode surface by the carbonate solvents. However, the ( $R_{ct}$ ) increases dramatically during cycling, reflecting the increasing impedance caused by the unstable SEI layer. Conversely, while  $LiTFSI$  in tetraglyme shows a higher initial ( $R_{ct}$ , Fig. 3f), it shows greater stability during cycling, consistent with the formation of a favorable SEI layer.<sup>43,46,47</sup>





**Fig. 5** Electrochemical performance of  $V_2O_5$  electrodes with different microporosities. Rate capability (a) and calendar tests (b) of  $V_2O_5$  microsphere electrodes prepared from templates made with different BCP : hexadecane ratios (70 : 30 and 100 : 0) cycled using LiTFSI in tetraglyme as electrolyte, compared to an unstructured, commercial  $V_2O_5$ .

Furthermore, the spectra reveal changes in impedance behavior across the mid-to-low frequency range, with the semicircles expanding more rapidly over cycles for the  $LiPF_6$ -based sample. This suggests a significant increase in impedance, likely due to a higher occurrence of side reactions, most notably, the growth of the SEI layer.<sup>30</sup> These changes are particularly pronounced in the  $LiPF_6$ -based system (Fig. 3e), suggesting increased electrode and charge transfer resistance after cycling. This finding supports the assumption that the SEI layer progressively grows during cycling. In contrast, in the LiTFSI-based system (Fig. 3f), the high-frequency semicircles remain similar, indicating stable charge transfer processes, likely due to an SEI layer that remains unchanged during prolonged cycling.

The origin of the different cycling behavior of the two electrolytes can be understood by evaluating the transmission electron micrographs (TEM) shown in Fig. 4. The pristine 70:30  $V_2O_5$  electrode shown in Fig. 4a and b has well-resolved 10–50 nm-sized  $V_2O_5$  crystallites prior to contact with the electrolyte. After electrochemical characterization (GC, CV, and EIS, corresponding to 75 cycles) for the same sample, the growth of an SEI layer on the  $V_2O_5$  surface is visible, as shown in Fig. 4c and d. In particular, the SEI layer covers the entire surface, but is non-uniform, with distinct thickness variations. Fig. 4e and f show the  $V_2O_5$  surface after similar cycling using the LiTFSI/tetraglyme electrolyte. While extensive SEI formation is found on isolated areas, the  $V_2O_5$  surface is predominantly covered by a uniform, nanometer-thick SEI layer, in agreement with previous reports.<sup>30</sup>

Based on these results, the interplay of micro- and nanoporosity of the  $V_2O_5$  materials reported in Table 1 is studied in detail in terms of rate capability and calendar tests with cells using LiTFSI in tetraglyme as electrolyte.

Fig. 5a shows the rate performance of three  $V_2O_5$  electrode types after three cycles of conditioning at C/20. At the low cycle rate of C/2, the two synthesized materials exhibit specific capacities of  $275 \text{ mA h g}^{-1}$ , exceeding the commercial material's  $150 \text{ mA h g}^{-1}$  capacity. However, differences between the 70:30 and 100:0 materials appear with increasing cycling rates, with a complete loss of specific capacity at 20C for the 100:0 and commercial reference materials. The 70:30  $V_2O_5$  retains a specific capacity of about  $70 \text{ mA h g}^{-1}$  at this high cycling rate. Both samples recover to a specific capacity of *ca.*  $250 \text{ mA h g}^{-1}$  when returned to a low cycling rate. This finding indicates that the low performance of the 100:0  $V_2O_5$  material at high C-rates is due to Li-ion diffusion limitation across the nanoporosity rather than irreversible SEI formation.

In particular, the long-term 1C performance in the calendar test of Fig. 5b is superior to that of the commercial material. While the commercial material exhibits a capacity loss of *ca.* 20% over 500 cycles, the 100:0 and 70:30 materials show capacity losses of 38% and 48%, respectively.

### 3.1 Discussion

The combination of micro- and nanoporosity is promising for next-generation Li-ion battery electrode materials, as previously shown for cathodes<sup>14</sup> and anodes.<sup>5,9,10,48</sup> However, these previous studies were limited to stable battery chemistries in which a solid electrolyte interphase remains under control. To address this limitation, the present study focuses on exploring the micro-nanoporosity interplay for the high-voltage  $V_2O_5$  cathode. In this case, since the growth of an SEI layer during electrochemical cycling is expected to clog the nanopores of the structure, two electrolytes are compared.



A comparison of the electrochemical cycling performance of Fig. 3 with the TEM micrographs of Fig. 4 demonstrates the importance of limiting SEI growth during cycling. The stable, thin SEI layer shown in Fig. 4e and f and obtained by using the LiTFSI in tetraglyme enables better rate performance and, in particular, superior rate retention in the calendar test compared to the commonly used carbonate-based electrolyte. The uniform formation of the SEI layer with LiTFSI in tetraglyme can be attributed to the low reactivity of the tetraglyme solvent and the stable nature of the LiTFSI salt, which together suppress uncontrolled decomposition reactions at the electrode-electrolyte interface. TEM images (Fig. 4e and f) clearly show a thin, conformal SEI layer distributed uniformly across the  $V_2O_5$  surface. Unlike carbonate-based systems, which tend to form thicker and uneven SEI layers due to their higher reduction potential, as shown in Fig. 4c and d, the tetraglyme facilitates slow, surface-limited reactions. This leads to self-limiting SEI growth and maintains consistent ionic pathways during extended cycling.<sup>43,44,49</sup> In contrast to previous approaches to synthesize nanoporous microspheres to form mesoporous battery electrodes, the emulsion-based approach developed in this work allows the introduction of an additional hierarchy level into this mesoporosity in the form of micrometer-sized pores. The results reported in Fig. 5 show that this additional hierarchy level is beneficial for the rate performance of the material, further reducing the diffusion-limited Li-ion transport into and out of the mesoporous spheres. The micropores do not significantly affect the overall porosity of the material (cf. Table 1), nor the long-term performance measured in the calendar test of Fig. 5b. However, the comparison of Fig. 3b, where the cells were cycled using  $LiPF_6$  in EC:DMC as electrolyte and Fig. 5b, where the cells were cycled using instead LiTFSI in tetraglyme, shows a considerable batch-to-batch performance. In fact, the two identically prepared sample batches show different capacity retention after 250 cycles. This indicates that further optimization of the material synthesis and electrode preparation steps is needed to produce high performance mesoporous  $V_2O_5$  cathodes for Li-ion batteries.

## Conclusions

In the present work, an emulsion-based method was used to prepare block-copolymer microparticles, which were then used as templates to synthesize  $V_2O_5$  microparticles with well-defined hierarchical porosity, and finally processed into a Li-ion battery cathode using a standard slurry technique. The final electrode material possessed porosity on three hierarchical levels: (1) the 10 nm level induced by the confined  $V_2O_5$  crystallization within the BCP microphase morphology, (2) the micrometer length scale caused by the demixing of an added non-solvent (hexadecane) into the fabrication mixture, and (3) the 10  $\mu$ m length scale arising during the assembly of the microparticles into the final electrode.

Two essential conditions were identified to enable better cycling rate performance and calendar lifetime of the thus synthesized mesoporous  $V_2O_5$  electrodes. First, suppressing the growth of the SEI layer is essential to avoid clogging the nanopores. Second, the introduction of micrometer-sized pores into the microspheres improves the rate capability of the electrode compared to the material without micropores.

While our results show promising electrochemical performance using a scalable emulsion-based technique, the observed batch-to-batch variation suggests that further optimization of this technique is required.

## Data availability

Data for this article are available from the Authors upon request.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

We thank the Adolphe Merkle Foundation for funding.

## Notes and references

- 1 S.-H. Park, H.-S. Shin, S.-T. Myung, C. S. Yoon, K. Amine and Y.-K. Sun, *Chem. Mater.*, 2005, **17**, 6–8.
- 2 C. Sun, S. Rajasekhara, J. B. Goodenough and F. Zhou, *J. Am. Chem. Soc.*, 2011, **133**, 2132–2135.
- 3 F. Wang, S. Xiao, Z. Chang, Y. Yang and Y. Wu, *Chem. Commun.*, 2013, **49**, 9209.
- 4 Z. Zhou, H. Zhang, Y. Zhou, H. Qiao, A. Gurung, R. Naderi, H. Elbohy, A. L. Smirnova, H. Lu, S. Chen and Q. Qiao, *Sci. Rep.*, 2017, **7**, 1440.
- 5 J. Jeong, J. Chun, W.-G. Lim, W. B. Kim, C. Jo and J. Lee, *Nanoscale*, 2020, **12**, 11818–11824.
- 6 S. Caes, J. C. Arrebola, N. Krins, P. Eloy, E. M. Gaigneaux, C. Henrist, R. Cloots and B. Vertruyen, *J. Mater. Chem. A*, 2014, **2**, 5809–5815.
- 7 R. Tian, S.-H. Park, P. J. King, G. Cunningham, J. Coelho, V. Nicolosi and J. N. Coleman, *Nat. Commun.*, 2019, **10**, 933.
- 8 K. Fu, X. Li, K. Sun, Z. Zhang, H. Yang, L. Gong, G. Qin, D. Hu, T. Li and P. Tan, *Adv. Funct. Mater.*, 2024, **34**, 2409623.
- 9 M. G. Fischer, X. Hua, B. D. Wilts, I. Gunkel, T. M. Bennett and U. Steiner, *ACS Appl. Mater. Interfaces*, 2017, **9**, 22388–22397.
- 10 M. T. Nguyen, P. Sutton, A. Palumbo, M. G. Fischer, X. Hua, I. Gunkel and U. Steiner, *Mater. Adv.*, 2022, **3**, 362–372.
- 11 Q. Yue, H. Jiang, Y. Hu, G. Jia and C. Li, *Chem. Commun.*, 2014, **50**, 13362–13365.
- 12 J. Shao, X. Li, Z. Wan, L. Zhang, Y. Ding, L. Zhang, Q. Qu and H. Zheng, *ACS Appl. Mater. Interfaces*, 2013, **5**, 7671–7675.
- 13 Q. Wu, W. s. Miao, Y. du Zhang, H. j. Gao and D. Hui, *Nanotechnol. Rev.*, 2020, **9**, 259–273.



- 14 M. G. Fischer, X. Hua, B. D. Wilts, E. Castillo-Martínez and U. Steiner, *ACS Appl. Mater. Interfaces*, 2018, **10**, 1646–1653.
- 15 Z. Chen, J. Wang, D. Chao, T. Baikie, L. Bai, S. Chen, Y. Zhao, T. C. Sum, J. Lin and Z. Shen, *Sci. Rep.*, 2016, **6**, 25771.
- 16 P. Parant, S. Picart, P. Lhuissier and C. L. Martin, *J. Eur. Ceram. Soc.*, 2020, **40**, 1613–1619.
- 17 H. Wang, R. Liu, Y. Li, X. Lü, Q. Wang, S. Zhao, K. Yuan, Z. Cui, X. Li, S. Xin, R. Zhang, M. Lei and Z. Lin, *Joule*, 2018, **2**, 337–348.
- 18 N. Yabuuchi, Y. Koyama, N. Nakayama and T. Ohzuku, *J. Electrochem. Soc.*, 2005, **152**, 1434.
- 19 A. Jain, S. R. Manippady, R. Tang, H. Nishihara, K. Sobczak, V. Matejka and M. Michalska, *Sci. Rep.*, 2022, **12**, 21024.
- 20 J. Ren, Y. Li, Z. Wang, J. Sun, Q. Yue, X. Fan and T. Zhao, *Int. J. Heat Mass Transfer*, 2023, **203**, 123818.
- 21 M. S. Whittingham, *Chem. Rev.*, 2014, **114**, 11414–11443.
- 22 P. Hu, T. Zhu, J. Ma, C. Cai, G. Hu, X. Wang, Z. Liu, L. Zhou and L. Mai, *Chem. Commun.*, 2019, **55**, 8486–8489.
- 23 Y. Zhang, Y. Luo, C. Fincher, S. Banerjee and M. Pharr, *J. Mater. Chem. A*, 2019, **7**, 23922–23930.
- 24 Y. Li, Z. Huang, P. K. Kalambate, Y. Zhong, Z. Huang, M. Xie, Y. Shen and Y. Huang, *Nano Energy*, 2019, **60**, 752–759.
- 25 Y. Rong, Y. Cao, N. Guo, Y. Li, W. Jia and D. Jia, *Electrochim. Acta*, 2016, **222**, 1691–1699.
- 26 P. Hu, P. Hu, T. D. Vu, M. Li, S. Wang, Y. Ke, X. Zeng, L. Mai and Y. Long, *Chem. Rev.*, 2023, **123**, 4353–4415.
- 27 A. Doderò, K. Djeghdi, V. Bauernfeind, M. Airoidi, B. D. Wilts, C. Weder, U. Steiner and I. Gunkel, *Small*, 2023, **19**, 2205438.
- 28 A. Escher, G. Bravetti, S. Bertucci, D. Comoretto, C. Weder, U. Steiner, P. Lova and A. Doderò, *ACS Macro Lett.*, 2024, **13**, 1338–1344.
- 29 V. Singh, S. Kuthe and N. V. Skorodumova, *Batteries*, 2023, **9**, 3390.
- 30 X. Liu, M. Zarrabeitia, B. Qin, G. A. Elia and S. Passerini, *ACS Appl. Mater. Interfaces*, 2020, **12**, 54782–54790.
- 31 E. Strelcov, J. Cothren, D. Leonard, A. Y. Borisevich and A. Kolmakov, *Nanoscale*, 2015, **7**, 3022–3027.
- 32 Z. Zhang, J. Yang, W. Huang, H. Wang, W. Zhou, Y. Li, Y. Li, J. Xu, W. Huang, W. Chiu and Y. Cui, *Matter*, 2021, **4**, 302–312.
- 33 V. S. K. Sungjemmenla, C. B. Soni, V. Kumar and Z. W. Seh, *Energy Technol.*, 2022, **10**, 2200421.
- 34 H. Alptekin, H. Au, E. Olsson, J. Cottom, A. C. Jensen, T. F. Headen, Q. Cai, A. J. Drew, M. Crespo Ribadeneyra and M.-M. Titirici, *Adv. Mater. Interfaces*, 2022, **9**, 2101267.
- 35 V. Velez, G. Ramos-Sánchez, B. Lopez, L. Lartundo-Rojas, I. González and L. Sierra, *Carbon*, 2019, **147**, 214–226.
- 36 J. G. Kennemur, *Macromolecules*, 2019, **52**, 1354–1370.
- 37 D. Kawaguchi and M. Satoh, *Macromolecules*, 1999, **32**, 7828–7835.
- 38 L. A. Belfiore, A. T. N. Pires, Y. Wang, H. Graham and E. Ueda, *Macromolecules*, 1992, **25**, 1411–1419.
- 39 Y. Chen, W. Zhao and J. Zhang, *RSC Adv.*, 2017, **7**, 4226–4236.
- 40 J. Xu, J. Li, Y. Yang, K. Wang, N. Xu, J. Li, R. Liang, L. Shen, X. Xie, J. Tao and J. Zhu, *Angew. Chem., Int. Ed.*, 2016, **55**, 14633–14637.
- 41 E. Strelcov, J. Cothren, D. Leonard, A. Y. Borisevich and A. Kolmakov, *Nanoscale*, 2015, **7**, 3022–3027.
- 42 B. Yan, X. Li, X. Fu, L. Zhang, Z. Bai and X. Yang, *Nano Energy*, 2020, **78**, 105233.
- 43 S. Cora, B. Key, J. Vaughey and N. Sa, *J. Electrochem. Soc.*, 2023, **170**, 020507.
- 44 X. Liu, M. Zarrabeitia, B. Qin, G. A. Elia and S. Passerini, *ACS Appl. Mater. Interfaces*, 2020, **12**, 54782–54790.
- 45 M. Tang, J.-C. Chang, S. R. Kumar and S. J. Lue, *Energy*, 2019, **187**, 115926.
- 46 M. Dahbi, F. Ghamouss, F. Tran-Van, D. Lemordant and M. Anouti, *J. Power Sources*, 2011, **196**, 9743–9750.
- 47 C. L. Berhaut, D. Lemordant, P. Porion, L. Timperman, G. Schmidt and M. Anouti, *RSC Adv.*, 2019, **9**, 4599–4608.
- 48 Y. Wang, X.-B. Cheng, Y.-X. Yao and R. Xu, *Adv. Energy Mater.*, 2021, **11**, 2003156.
- 49 B. N. Olana, S.-H. Pan, B.-J. Hwang, H. Althues, J.-C. Jiang and S. D. Lin, *J. Mater. Chem. A*, 2024, **12**, 3659–3670.

