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Correction: Hydrothermal liquefaction vs. fast/flash pyrolysis for biomass-to-biofuel conversion: new insights and comparative review of liquid biofuel yield, composition, and properties

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Correction for 'Hydrothermal liquefaction vs. fast/flash pyrolysis for biomass-to-biofuel conversion: new insights and comparative review of liquid biofuel yield, composition, and properties' by Farid Alizad Oghyanous, *et al.*, *Green Chem.*, 2025, **27**, 7009–7041, <https://doi.org/10.1039/D5GC01314C>.

Authors have made three modifications to the published review article to provide better clarity to the discussion.

1. The beginning of the second paragraph in section 2.2.2 Hydrothermal liquefaction, has been modified to clarify the mention of organic solvent, whereby:

"Instead of utilizing the moisture of biomass as the solvent, organic solvents are also investigated in HTL as they play a key role in bio-crude oil yield. The selection of solvent affects both the temperature needed to achieve the maximum bio-crude yield in the HTL process and the overall yield of bio-crude oil." has been modified to "While HTL is conventionally defined as a TP occurring in water or aqueous media, some studies have also explored the use of organic solvents or co-solvents to enhance bio-crude oil yield and alter reaction severity. Reaction media play a critical role in determining product yield and composition; the choice of solvent can influence both the optimal reaction temperature and the resulting bio-crude oil yield."

2. Tables 1 and 2 have been modified by reporting the maximum liquid biofuel yields on a dry basis (db) whenever both the product and feedstock weights were clearly defined on a dry basis to enable more meaningful comparisons. If a different yield basis was used in the original reference, it is now explicitly indicated in parentheses in the table. Sources where the yield basis was not specified are indicated with footnote *b*.

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Table 1 Biomass elemental composition, ash content, and operational conditions for fast/flash pyrolysis of various biomass for maximizing pyrolysis oil production

Biomass	Name	C (wt%)	H (wt%)	N (wt%)	O (wt%)	Ash (wt%)	T (°C)	Residence time (s)	Particle size (mm)	Reactor type	Max. pyrolysis oil yield ^a (wt%, (db))	Ref.
Lignocellulosic biomass												
Kraft lignin	—	—	—	—	—	—	399.85	—	—	Fixed bed	24.30	55 ^b
Wood chips	—	—	—	—	—	—	499.85	—	—	—	30.20	26.00
Oat straw	44.11	5.98	0.62	43.65	5.64	500	599.85	—	—	Drop tube	57.40	56 ^b
Corn straw	43.12	6.19	1.44	35.68	13.57	600	500	0.75–2.75	0.25–0.75	—	65.40	71.10
Palm kernel shell	48.82	5.68	0.42	45.08	3.87	600	700	5.00–6.00	0.075–0.125	Entrained flow	26.30	9.41
Microalgae												
<i>Chlorella vulgaris</i>	43.75	6.07	7.86	41.61	5.54	600	500	5.00–6.00	<0.105	Entrained flow	42.48	6
<i>Scenedesmus sp.</i>	32.10	4.80	5.30	22.10	35.20	900	480	2.00	2.00	Fluidized bed	43.63	—
<i>Chlorella vulgaris</i> remnant	45.04	6.88	6.64	29.42	8.34	500	—	—	0.42–0.70	Fluidized bed	45.37	—
Macroalgae												
<i>Saccharina japonica</i>	32.89	6.17	0.93	60.01	20.21	350	<3.00	0.30–0.50	0.30–0.50	Bubbling fluidized-bed	55.00 (dry ash-free)	57
<i>Ulva lactuca</i>	33.60	5.10	3.30	28.20	29.10	550	400	0.50–2.00	<1.00	Centrifugal Thermogravimetric analyzer	28.20	41
Seaweed powder	36.44	5.14	3.72	39.36	14.71	400	500	60.00	—	—	40.21 (including water) 40.21 (including water) 37.41 (including water) 30.75 (including water) 28.40 (including water) 26.67 (including water) 65.00 (dry ash-free)	58
Municipal sludge												
Mixed activated and primary sludge	38.30	5.00	3.40	37.30	16.00	400	500	1.70	1	Fluidized bubbling bed	23.57	59
Digested sewage sludge	25.50	4.50	4.90	25.80	37.20	450	500	<1.00	0.50–3.00	Conical spouted bed	31.87	60
Sewage sludge	40.60	7.10	7.70	41.20	37.20	500	600	<100.00 ms	0.50–3.00	Conical spouted bed reactor	36.87	37.99
Food waste												
Waste fish oil	—	—	—	—	—	525	500	17.00	—	Continuous pilot plant tubular	72.83 (including water)	61
Potato peel waste	43.80	6.00	4.10	46.20	9.30	450	8.00	—	1	Laboratory auger	22.70	53.00
Potato peel waste residue	47.80	6.40	4.00	41.80	6.50	750	600.00	—	—	Oven	25.60	43
Grape seeds powder	50.90	5.40	2.50	36.90	4.10	850	850	—	—	—	28.92	62
											32.56	65 ^b

^a Maximum pyrolysis oil yield is reported on a dry basis (db). If the dry basis was not specified in the original reference, the reported yield basis (wt%) is indicated in parentheses. ^b References where the yield basis was not specified in the source.

**Table 2** Biomass elemental analysis, ash content, and operational conditions for HTL of various feedstocks for bio-crude oil production

Biomass	Name	C (wt%)	H (wt%)	N (wt%)	O (wt%)	Ash (wt%)	Solvent	T (°C)	Residence time (min)	Pressure (bar)	Max. bio-crude oil yield ^a (wt%, (db))	Ref.
Lignocellulosic biomass												
Corn stover		43.57	5.84	0.56	49.98	6.96	Water	250 300 350	0.00–60.00	75.84–234.42	22.20 at 15 min and 110.31 bar 29.25 at 0 min and pressure of 151.68 bar 17.70 at 15 min and 179.26 and 217.18 bar	97 ^b
Wheat straw		42.15	6.21	0.82	50.82	6.92	K ₂ CO ₃	375				
Eucalyptus		47.95	5.91	0.10	46.23	1.15		400	15.00	320.00	14.25 at 15 min and pressure of 196.5 and 241.31 bar 22.00 (dry ash-free) 28.00 (dry ash-free) 27.00 (dry ash-free)	98
Pinewood		49.90	6.30	0.30	42.80	0.59	—					
Rice straw		36.20	5.20	0.70	40.30	—	Milli-Q water, tap water, seawater, recycled wastewater, industrial wastewater	350	30.00	180.00	36.40 in industrial wastewater	99 ^b
Microalgae												
<i>Chlorella vulgaris</i>		52.60	7.10	8.20	32.20	7.00	Water, Na ₂ CO ₃ , HCOOH	350	60.00	—	38.00 in water (dry ash-free) 37.50 in water (dry ash-free) 31.00 in water (dry ash-free)	100
<i>Nannochloropsis occulata</i>		57.80	8.00	8.60	25.70	26.40						
<i>Spirulina</i>		55.70	6.80	11.20	26.40	7.60						
<i>Porphyridium creuentum</i>		51.30	7.60	8.00	33.10	24.40						
<i>Scenedesmus obtusus</i>		33.40	4.70	4.40	16.50	40.80	Water	250 300 350	7.00–30.00 225–270 260–280	175–225 225–270 180.00	21.50 (dry ash-free) 31.00 (dry ash-free) 35.05 (dry ash-free) 39.70 (dry ash-free)	101
<i>Chlorella</i> sp.		56.20	6.90	7.70	28.70	11.70	Water	350	1.40 5.80	—	36.80 (dry ash-free)	102
Macroalgae												
<i>Sargassum tenerium</i>		32.10	4.70	0.93	60.72	26.50	Water, C ₂ H ₅ OH	260 280 300	15.00	45.00–120.00 25.20 in C ₂ H ₅ OH 20.00 in C ₂ H ₅ OH	18.50 in C ₂ H ₅ OH 25.20 in C ₂ H ₅ OH 20.00 in C ₂ H ₅ OH	103 ^b
<i>Ulva fasciata</i>		—	—	—	—	25.40	Water	280	15.00	—	12.00	104
<i>Enteromorpha</i> sp.		—	—	—	—	23.20		280	—		7.00	
<i>Sargassum tenerium</i>		28.75	5.22	3.65	32.28	32.00	Water, 5% Na ₂ CO ₃	220 240 260 280	5.00–60.00	—	9.60 at 30 min in water 12.50 at 30 min in water 18.24 in 5% Na ₂ CO ₃ at 30 min 19.80 in 5% Na ₂ CO ₃ at 30 min 23 in 5% Na ₂ CO ₃ at 30 min	105 ^b
<i>Sargassum tenerium</i>		28.75	5.22	3.65	32.28	30.10	Water, 5% Na ₂ CO ₃	220 240 260 280	5.00–60.00	—	9.60 at 30 min in water 12.50 at 30 min in water 18.24 in 5% Na ₂ CO ₃ at 30 min 19.80 in 5% Na ₂ CO ₃ at 30 min 23 in 5% Na ₂ CO ₃ at 30 min	105 ^b
Municipal sludge												
Swine manure		46.02	6.10	2.57	45.31	11.45	Water	350	15.00	—		
Sewage sludge		51.94	7.28	8.33	32.44	25.10	Water	350	15.00	—	33.00 (dry ash-free) 37.00 (dry ash-free)	106
Mixed primary and secondary sludge		47.90	5.70	3.70	32.30	9.80	Water	350	15.00	170.00	38.50	107
Primary sludge		47.80	6.50	3.60	34.10	7.50					34.70	
Secondary sludge		43.60	6.60	7.90	25.00	16.20					20.00	
Dehydrated sewage sludge		15.60	2.30	1.00	13.70	67.40	Water, 2.28 aqueous phase; 1 water	330	30.00	250.00	30.50 in cycle 2 in water and aqueous phase (dry ash-free)	108
Food waste												
Food waste		48.18	7.3	4.52	39.73	5.40	Water	280	30.00	—	29.00	109
Food waste		47.80	5.11	4.78	42.10	3.30	Water	310 340 300 350 400	30.00 200 30.00 30.00 400	30.00 353 353 138–357 353	30.00 40.00 11.80 28.80 37.4 at 169 bar	110
Mixed synthetic food waste		56.16	8.05	2.61	33.19	4.68	Water	280–360	10.00–60.00	12–110	30.5 at 1 min 30.5 at 1 min 46.9 at 360 °C and 40 min (dry ash-free)	111

^a Maximum bio-crude oil yield is reported on a dry basis (db). If the dry basis was not specified in the original reference, the reported yield basis (wt%) is indicated in parentheses. ^b References where the yield basis was not specified in the source.

3. Fig. 6 has been modified to reflect levoglucosan as the major product.

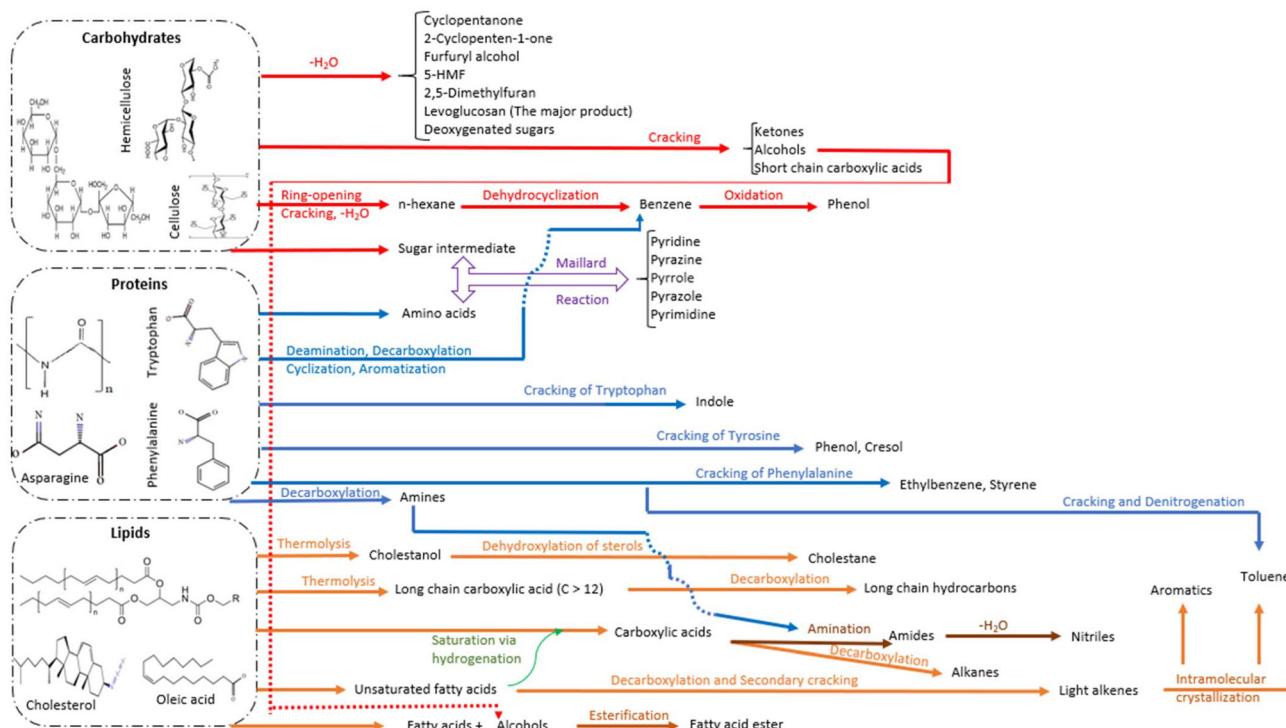


Fig. 6 Plausible reaction pathways of pyrolysis of carbohydrates, proteins, lipids, and lignin.^{138,340–344}

The Royal Society of Chemistry apologises for these errors and any consequent inconvenience to authors and readers.

